Mechanochemical Synthesis of Colloidal Sulfur Particles in the $Na₂S₂O₃ - H₂(C₄H₄O₄) - Na₂SO₃ System$

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Abstract—Elemental sulfur nanoparticles (nanosulfur, S_n^0) have been obtained in a matrix consisting of sodium sulfite (diluent and a final reaction product) and succinic acid (catalyst) by mechanochemical syn-
theses via the reaction $Na_2S_2O_3 \cdot 5H_2O + H_2(C_4H_4O_4) + \zeta Na_2SO_3 = (z + 1)Na_2SO_3 + H_2(C_4H_4O_4) +$ $5H_2O + S_n^0$, at $z = 19.6$. It has been shown that free nanodispersed sulfur can be obtained by dissolving the matrix in water. The prepared samples have been characterized using a set of physical and physicochemical methods. *n* S_n^0

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INTRODUCTION

Elemental sulfur is used in, e.g., production of sul furic acid, varnishes, gunpowder, plastics, automobile tires, fertilizers, and antimicrobial agents; moreover, it is widely applied in agriculture, building, and other fields $[1-4]$.

Sodium thiosulfate may be decomposed into sodium sulfite and sulfur. La Mer et al. were the first to obtain monodisperse spherical sulfur particles from acidified $Na₂S₂O₃$ solutions [5]. Their results have been used to develop a procedure for measuring nano particle size distribution based on the Mie [6] and Pecora [7] theories of light scattering.

In recent years, communications devoted to the study of sulfur nanoparticles (nanosulfur [8]) have been appearing at an increasing rate [8–50]. As a rule, common routine methods, including dynamic light scattering, scanning and transmission electron microscopy, X-ray diffraction analysis, and energy dispersive X-ray spectroscopy, have been used in these works for studying the concentration, morphology, and structure of nanoparticles and nanostructured sys tems. Some specific methods used for studying sulfur nanoparticles should be especially noted; they include thermal analysis (thermogravimetry) [22, 23], atomic force microscopy [23], liquid chromatography [24], diffusion aerosol spectrometry using photoelectric counters of particles [17, 18], measurements of sorp tion properties [14] and ξ potential [22, 25], IR and

Raman spectroscopy [13–15, 26], UV spectroscopy [8, 24, 27], and Rayleigh resonance scattering [15, 28].

Five main methods are available for producing nanodispersed sulfur. The first method consists in the acidification of a sodium thiosulfate solution with dif ferent acids [6, 16, 19] followed by stabilization of nanoparticles with surfactants [20, 29] or electrodepo sition [30]. The second method is based on the reac tion between sulfur and solutions of sulfides or hydrox ides of ammonium and alkali or alkali-earth metals [13, 19, 21] (mechanical or ultrasonic activation of sulfur is necessary in this case) with the formation of corresponding solutions of polysulfides followed by varying the pH of the solutions and the use of corre sponding surfactants. Modifications of these two methods include the use of water-in-oil microemul sions [13, 21, 31] or reaction between hydrogen sulfide and iron chelates [14]. The third method is sulfur sub limation followed by its homogeneous [17] or hetero geneous [18] nucleation, as well as its treatment with poly(ethylene glycol)s [28, 32] or cysteine [15]. The fourth method involves the modification of sulfur sur face in surfactant solutions by successive mechanical and ultrasonic dispersing [33] (see also [34]). Finally, the fifth method represents the preparation of sulfur nanoparticles as components of composite materials [9, 26, 35–37].

In the majority of the cited works, synthesized sul fur nanoparticles had a spherical $(\alpha - S)$ or cylindrical (β-S) shape; however, they may be in the form of tubes

Reagent	$Na_2S_2O_3 \cdot 5H_2O$ prepared from standard titer		$H_2(C_4H_4O_4)$ prepared from standard titer		$Na2SO3$, reagent grade	
Weighed portion, g	1.731		0.824		17.207	
ω , rpm	100	200	300	400	500	600
W , cm/s	130	260	390	520	650	780

Initial reagents and parameters of mechanochemical synthesis of sulfur particles

[11], wires [12], and rods [28]. The spectrum of sizes of sulfur particles thus prepared is also wide (from a few nanometers to $1 \mu m$). They can be prepared in a free state, as aqueous and nonaqueous dispersions, and as components of nanocomposites. The mecha nism and kinetics of the formation and growth of sul fur particles in solutions have been studied in [38].

The diverse fields of nanodispersed sulfur applica tion are based on its unique properties. Its bactericidal properties are employed in biotechnologies [4, 22, 23, 25], antiviral and antitumor activities are used in med icine [25, 32, , 34, 39, 40], pesticidal and fungicidal functions find application in agriculture [33, 41–43], its hydrophobicity is used in building [38, 44–46], and its electrochemical properties are employed in power engineering [9, 20, 26, 35–37, 47]. Sometimes, it is used in catalysis [10] and analytical chemistry [48]. Numerous allotropic modifications of sulfur are also widely used [49].

In this work, the method (which was described in our previous works [50, 51]) of system dilution with a side final product of the reaction
Na.S.O. : 5H.O + vC .H.O. + z Na.SO.

$$
Na2S2O3 \cdot 5H2O + yC4H6O4 + zNa2SO3
$$

= (z + 1)Na₂SO₃ + yC₄H₆O₄ + 5H₂O + S_n⁰. (1)

is, for the first time, proposed to be used for mecha nochemical synthesis of nanodispersed sulfur.

Here, succinic acid $C_4H_6O_4$ and Na_2SO_3 play the roles of a catalyst and a diluent. Nanosulfur $\boldsymbol{\mathrm{S}}_n^0$ must be formed due to the decomposition of very unstable thiosulfuric acid according to the following scheme
 $[16, 38, 52]$: [16, 38, 52]:

$$
S_2O_3^{2-} + 2H^+ \rightleftarrows H_2S_2O_3 \rightarrow H_2SO_3 + S,
$$

\n
$$
S + S \rightleftarrows S_2 + S... \rightleftarrows S_{n-1} + S \rightarrow S_n,
$$

\n(2)

where S_n is a nucleus of a critical size.

EXPERIMENTAL

Mechanical activation (MA) was performed in a Pulverisette planetary-type ball mill (Fritsch GmbH, Germany) with a cage rotation rate regulated in the range of 100–600 rpm and an apparatus made of hard ened stainless still (cylinder volume was 500 cm³ and the number of steel balls with a radius of 0.5 cm and a density of 7.8 $g/cm³$ was 109). The stoichiometric

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coefficients in MA reaction (1) for the catalyst and diluent were $y = 1$ and $z = 19.6$, respectively.

The key parameter of the MA process in a plane tary-type mill is relative rate *W* of interaction of grind ing bodies, i.e., balls and cylinder walls [50]. Let R_1 and R_2 be the radii of the cage (distance between the axes of planetary movement, $R_1 = 6.2$ cm) and the cylinder (R_2 = 5.0 cm), respectively, and ω_1 and ω_2 be the angular rotation rates of the cage and the cylinder, respectively (in the used mill, they rotate in opposite directions at $|\omega_1| = |- \omega_2| = |\omega| = 2\pi\omega$, where ω is the rotation frequency). In this case, the geometric and kinematic factors are $\Gamma = R_1/R_2 = 6.2/5 = 1.24$ and $K = \omega_1/\omega_2 = -1$, respectively. Angle φ of ball detachment from the cylinder wall is determined by the rela tion $\cos \varphi = (1 + K)/\Gamma = 0$; hence, $\varphi = 90^\circ$. In this case, *W* and its normal (W_n) and tangential (W_t) components at the moment of a collision of grinding bod ies linearly depend on ω as follows:

$$
|W| = W = 2πω1R2[(K + 1)2 + Γ2
$$

- 2Γ(K – 1)cos φ + (Γ + 1)²]^{0.5}
= 2πωR₂[Γ² + (Γ + 1)²]^{0.5},

$$
Wn = |W|sin φ = W, Wt = |W|cos φ = 0.
$$
 (3)

The characteristics and weighed portions of the ini tial reagents used for the mechanochemical synthesis nanodispersed sulfur via reaction (1) and the *W* values, which correspond to different rotation frequencies ω , as calculated by relations (3), are listed in the table.

In crystal-hydrate-containing systems, mecha nochemical processes occur in the so-called mild con ditions with release of H_2O [53, 54]. Therefore, to provide its removal from the reaction mixture, MA of the initial mixtures was performed without the packing strip of the mill cylinder at a balls-to-mixture weight ratio of $445.16/19.762 = 22.5$. Note that, according to relation (1) and the data in the table, the yield of nan odispersed sulfur was expected to be 0.224 g.

A mixture was subjected to the mechanical treat ment under conditions that excluded cylinder over heating in the following regime: initially, MA was per formed at rotations rates of 140, 210, 280, and 350 rpm (14 min at each rate, 56 min in all); then, the cylinder was opened, inspected, and restacked; after that, the MA was carried out at 420, 490, 560, and 600 rpm (8, 4, 2, and 1 min, respectively, 15 min in all). After the experiment was completed (the total duration of MA was 71 min), the product (18.207 g) was removed from the cylinder. Thus, the yield was $18.207/19.762 \approx 92\%$.

Free sulfur particles were obtained from the MA product by washing with water. The solubilities of pos sible products of MA in water have the following val ues: sodium thiosulfate, 70.1% (20°C); succinic acid, 5.8% (20°C); sodium sulfite, 20.82% (19.9°C); and sulfur is almost insoluble. The MA products used in an amount of $2.5 \times 4 = 10$ g were a fortiori soluble in $15 \times$ $4 = 60$ mL water placed into four centrifuge tubes. Thus, powder in an amount of 105 mg was obtained for analytical studies.

X-ray diffraction (XRD) analysis of the samples was carried out with a D8 ADVANCE diffractometer (Bruker AXS) using monochromatic radiation of cop per. The measurements were performed in the follow ing regime: X-ray tube voltage of 40 kV at a current of 40 mA, scanning step $2\theta = 0.02^{\circ}$, and the time information acquisition at a point of 1 s. The XRD data were processed as described in [51] using the EVA.exe and PCPDFWIN softwares and the PDF-2 database, as well as by the method of the Reference Intensity Ratio.

The thermal analyses (thermogravimetric analysis (TGA) and differential scanning calorimetry (DSC)) were carried out in nitrogen with an STA 449 *F3* instrument (Netzsch, Germany) up to 1000°C at a heating rate of 10°/min.

Examination of the samples by scanning electron microscopy (SEM) was performed with a Quanta 3D 200i microscope (FEI, United States) operating at an accelerating voltage of 15 kV. The samples under examination were applied onto conducting carbon sticky tape.

Examination of the samples by transmission elec tron microscopy (TEM) was carried out with a JEM- 1011 microscope (JEOL, Japan) equipped with a Morada digital camera (Olympus, Japan). A sample (10 mg) resulting from MA was placed into a tube with hexane (3 mL), and a droplet of the obtained suspen sion was applied onto a collodion-coated copper grid. Sulfur particles washed from side products of the syn thesis were applied onto a grid from the suspension before the second decantation. Morphology and sizes of the particles were determined with a resolution below 5 nm at an accelerating voltage of 100 kV.

The sizes of sulfur nanoparticles were also deter mined by dynamic light scattering (DLS) at an angle of 90° using a 90Plus spectrometer (Brookhaven Inst., United States) equipped with a 35-mW solid-state laser (LaserMax, United States) operating at wave length of 658 nm. Scattered photons were accumu lated by a high-sensitivity detector based on an ava lanche photodiode (Perkin Elmer). Hydrodynamic diameter d_z of particles averaged over scattered intensity was calculated under the assumption of their spherical shape as an average result of 100 measure ments (ten series consisting of ten measurements each) by the Stokes–Einstein formula $d_z = kT/3\pi\eta D$. The values of viscosity η and refractive index of a dis persion were taken equal to those of the dispersion medium (water). Photon accumulation time during one measurement was 10 s, while the number of pho tons used for plotting the autocorrelation function was 10⁵-10⁶. In addition, the average light intensity scattered at an angle of 90° (static (Rayleigh) light scatter ing) was measured using the Debye Plot option as a number of photons (pulses) arriving at the detector per 1 s. The measurements were performed at 20 ± 0.1 °C. The diffusion coefficient directly measured with the instrument is *z*-averaged (averaged over intensity). For a polydisperse system containing *i* number of components with different sizes, *z*-averaged diffusion coeffi cient D_z is calculated in terms of the monomodal analysis using the 90Plus software as follows:

$$
D_z = \frac{\sum_i I_i D_i}{\sum_i I_i}.
$$

Expressing D_i via corresponding diameters and taking into account that intensity *I* of light scattered by particles is, according to the Rayleigh theory, propor tional to their number concentration N_i and six-powered diameter *d*, we obtain

$$
d_z = \frac{\sum_i I_i}{\sum_i \frac{I_i}{d_i}} = \frac{\sum_i N_i d_i^6}{\sum_i N_i d_i^5}.
$$

As follows from the derived expression, in the DLS method, the contribution from large particles of a polydisperse system to the d_z value may appear to be determining. More "recognized" number-average diameter d_n is a derived quantity: $d_n = \sum N d / \sum N$.

The error in the calculation of d_n may be substantial. Note that the "reference" method of particle size determination from TEM data enables one to directly find only d_n . Other distributions are also derived parameters, which are calculated with a much larger error. Therefore, the TEM and DLS data may be com pared only within the framework of equivalent averag ings. For monodisperse samples, $d_n = d_z$, while, for polydisperse ones, $d_n < d_z$. In the monomodal analysis, which implies the existence of a single mode, the auto correlation function is processed by the cumulant method using the 90Plus software. The average hydro dynamic diameter and polydispersity are determined from the first and second cumulants, respectively; therewith, the nanoparticle size distribution is approx imated by a lognormal dependence.

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Fig. 1. Diffraction pattern of a mixture (2.1 g; $y = 1$, $z = 2$) of reagents for reaction (1) prepared in an agate mortar of the Pulverisette mill: (*1*) Na₂SO₃, (*2*) Na₂S₂O₃ · 5H₂O, and (*3*) C₄H₆O₄.

RESULTS AND DISCUSSION

X-ray Diffraction and Thermal Analyses

Initially, we tried to carry out reaction (1) an a Pul verisette homogenizer/grinder (Fritsch GmbH, Ger many) equipped with an agate mortar and a ball 9.2 and 7.1 cm in diameter, respectively, at $y = 1$ and $z = 2$ (mixture weight was 2.1 g). The XRD data are illus trated in Fig. 1. It can be seen that the reaction has not been realized, because the lines assigned to the initial reagents and, possibly, succinic acid derivatives (anhy drous and hydrated sodium succinate) are predomi nantly observed.

Figure 2 depicts the diffraction patter of the prod ucts of MA of the initial mixture in a Pulverisette 6 planetary-type mill. It can be seen that the lines attrib uted to sodium sulfite playing the role of a diluent pre vail because of the high dilution parameter. At the same time, the low content of, e.g., sulfur, whose theoretical yield from reaction (1) is as low as 0.224 g $(1.13 \text{ wt } \% \text{ in the MA product})$, makes it impossible to correctly identify the presence of its phase from the XRD data.

The XRD data on a powder obtained from an MA product by treatment with water are presented in Fig. 3a. The processing of these data have shown that this sample represents monophase sulfur $(\alpha - S)$ with size of coherent-scattering regions $L \approx 75$ nm and the following parameters of unit cell (\AA) $a = 10.4430 \pm$ 0.0030, $b = 12.8499 \pm 0.0034$, $c = 24.4427 \pm 0.0060$, which have appeared to be somewhat larger than $a =$ 10.4370, *b* = 12.845, *c* = 24.369 Å characteristic of ref erence sulfur (Fig. 3b).

Moreover, comparative thermal analysis was per formed for samples of ordinary sulfur (extrapure grade, Technical Certificate TU 6-09-2546-77) and the same powder of nanodispersed sulfur (Fig. 4, curves *1*, *2*, respectively). The obtained TGA/DSC curves suggest that sulfur nanoparticles have higher

Fig. 2. Diffraction pattern of a reaction mixture (19.134 g; $y = 1$, $z = 19.6$) after MA in a Pulverisette 6 mill: (*I*) Na₂SO₃, (*2*) $C_4H_6O_4$ (?), and (3) S (?).

temperatures of the $\alpha \rightarrow \beta$ transformation and complete evaporation, but lower temperatures of the onset of evaporation and polymerization at the same melting temperatures of these two samples. It is worth espe cially noting that the magnitudes of the thermal effects of melting and polymerization for nanodispersed sulfur are markedly lower than those for ordinary sul fur are.

Measurements of Sulfur Nanoparticle Sizes

Analysis of SEM micrographs (Fig. 5) has con firmed the sulfur nanoparticles sizes calculated from the XRD data (Fig. 3) for a mechanically activated sample (Fig. 5a). Because of the close atomic masses of the components, the SEM images are insufficiently contrasted; however, their detailed examination leads us to conclude that the issue is particles with sizes of nearly 100 nm. Another picture is observed for sulfur particles resulting from the treatment of a mechani cally activated sample with water and deposited onto a

substrate from a suspension before the second decan tation (Fig. 5b). In this case, the particle sizes are sub stantially larger than 100 nm; however, according to the XRD data, the size of their coherent-scattering regions is $L \approx 75$ nm (Fig. 3a).

The TEM images of a mechanically activated sam ple and sulfur particles isolated from it are shown in Fig. 6. As can be seen from Fig. 6a, the sizes of sulfur particles in the mechanically activated sample are 20– 80 nm, while their morphology agrees with that described in the literature (see, e.g., [55]). The sizes (as large as 300 nm) and morphology of washed sulfur particles (Fig. 6b) differ from those observed for the mechanically activated sample, seemingly because of recrystallization processes (seeded growth and the development of the spherical shape at the expense of smaller particles) during the preparation of particles.

Information on the behavior of sulfur nanoparti cles after the dissolution of the mechanically activated sample in water (Fig. 7) has been obtained by DLS.

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Fig. 3. Diffraction patterns of (a) sulfur washed out of a mechanically activated sample and (b) reference sulfur (PDF 83-2285).

The data presented in Fig. 7a show that the effective hydrodynamic diameter of particles immediately after the sample dissolution (within the initial 24 h) does not change significantly, probably because the solution contains succinic acid anions, which play the role of a surfactant stabilizing the sulfur nanodispersion. Then, the size of the nanoparticles begins to dramatically increase, and, in 3 days, after the particles reach sizes of several microns, their hydrodynamic diameters begin to strongly decrease. In addition, the obtained dispersion was heated to 40 and 70°С. During the ini tial 2 h of exposure at these temperatures, the hydro dynamic diameter of the particles did not increase noticeably as well.

As has been mentioned above, the intensity of the Rayleigh light scattering is proportional to the product of nanoparticle concentration and six-powered parti-

cle diameter. Therefore, at the initial stage, the exper imental time dependence of the scattered light inten sity has a more complex pattern (Fig. 7b), while a drastic decrease in the intensity is observed in 24 h due to partial sedimentation of the particles. The obtained data lead us to conclude that the obtained sulfur hydrosol is relatively stable during the initial 24 h, which must be taken into account when using it in practice. Coagulation then begins in the system, and the sol loses its stability with respect to aggregation and, judging by the abrupt fall in the scattered light intensity, to sedimentation as well.

The DLS and TEM data have also be compared (Fig. 8). Comparison has been performed using the number-average values of the particle diameter. It can be seen from the figure that sulfur particles in the sol have smaller sizes than those after the deposition onto

Fig. 4. TGA/DSC curves for (*1*) ordinary sulfur and (*2*) sulfur particles washed out of a mechanically activated sample.

the substrate. Seemingly, when the samples are pre pared for TEM examination, sulfur nanoparticles additionally grow, most likely with involvement of gravitational forces during the first centrifugation at 7000 rpm.

CONCLUSIONS

A short review of the literature data on the proper ties and the methods for investigation and production of sulfur nanoparticles (nanosulfur) has been pre sented. A method has, for the first time, been proposed for mechanochemical synthesis of nanodispersed sulfur in a sodium thiosulfate pentahydrate/succinic acid system involving dilution with a water-soluble final reaction product, sodium sulfite. Using X-ray diffrac tion and thermal analyses, it has been shown that washing of mechanical activation product with water leads to the isolation of finely dispersed sulfur particles with a size of coherent-scattering regions equal to 75 nm and thermal properties somewhat different from those of ordinary sulfur.

Electron microscopy and dynamic light scattering have been employed to determine the sizes of sulfur particles in the product of mechanical activation (below 100 nm) and in the free state (as large as 300

Fig. 5. SEM images of (a) a mechanically activated sample and (b) sulfur particles washed out of this sample.

Fig. 6. TEM images of (a) mechanically activated sample assembles from different regions of visual field at 100000× magnification and sulfur particles washed out of this sample $(200000\times)$ (b).

Fig. 7. Panel (a): time dependences of (*1*) d_z and (*2*) d_n for particles of sulfur sol obtained by dissolving a mechanically activated sample in water and panel (b): time dependence of intensity *I* of light scattered by this sol.

Fig. 8. Sulfur particle size distributions obtained using (*1*) DLS and (*2*) TEM. Dependences have been normal ized by 100% with respect to the maximum point. Experi ments were performed 30 min after the sulfur sol was pre pared.

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nm) and to establish that, during the preparation of free sulfur, its particles acquire a spherical shape.

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