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DOI: 10.1038/s42003-018-0220-6

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# A minimum information standard for reproducing bench-scale bacterial cell growth and productivity

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Reproducing, exchanging, comparing, and building on each other's work is foundational to technological advances. Advancing biotechnology calls for reliable reuse of engineered organisms. Reliable reuse of engineered organisms requires reproducible growth and productivity. Here, we identify the experimental factors that have the greatest effect on the growth and productivity of our engineered organisms in order to demonstrate reproducibility for biotechnology. We present a draft of a Minimum Information Standard for Engineered Organism Experiments (MIEO) based on this method. We evaluate the effect of 22 factors on *Escherichia coli* engineered to produce the small molecule lycopene, and 18 factors on *E. coli* engineered to produce red fluorescent protein. Container geometry and shaking have the greatest effect on product titer and yield. We reproduce our results under two different conditions of reproducibility: conditions of use (different fractional factorial experiments), and time (48 biological replicates performed on 12 different days over 4 months).

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The irreproducibility of experimental results in biotechnology<sup>1</sup> and bioengineering<sup>2</sup> must be overcome to realize the potential of biology as a reliable engineering substrate<sup>3,4</sup>. The synthetic biology community has expressed a desire for experimental protocol standards<sup>5–7</sup>, supplementing existing standards for genetic modifications<sup>8</sup>. Minimum information standards have improved reproducibility for qPCR<sup>9</sup>, microarray<sup>10</sup>, and genomics<sup>11</sup> experiments, and a minimum information standard could similarly improve the reproducibility of engineered cell experiments. There have been calls to address reproducibility with reference strains<sup>5,7</sup>. While reference strains and information standards can and should coexist, information standards are more generalizable, accessible, verifiable, and maintainable. There have also been several efforts to improve reproducibility through software and automation<sup>12–15</sup>.

Biological engineering typically proceeds in three steps: genetically modifying the organism, growing the organism, and assaying its function (Supplementary Fig. 1). The conditions under which engineered cells are grown can have a large impact on the cell's performance—the relationship between a genetic modification and its function cannot be fully defined without considering the growth conditions. Here, we describe a method to systematically evaluate the effect of experimental factors on growth/productivity of engineered cells, and will recommend the development of a minimum information standard based on this method.

We hypothesize that a sufficient description of experimental factors will enable reproducible performance of engineered cells, and that we can realize this description by building a literature knowledgebase to identify factors, measuring factor effects with an appropriate orthogonal factorial experimental design, and demonstrating that controlling these factors results in reproducible growth and productivity (see Methods section for definitions of repeatability and reproducibility). This description can form the basis of a minimum information standard for growth/productivity of engineered organisms. We will test our hypothesis with two test cases using publicly available strains, *Escherichia coli* engineered to produce the small molecule lycopene, and the heterologous protein RFP.

This paper focuses on experimental factors that define and influence growth conditions for engineered cells. Genetic modifications, both intentional and those arising from evolution, are outside of our scope. Cellular assays are also outside of our scope. We focus on experimental factors at bench scale (microtiter plates and shake flasks) in batch culture mode because these formats are often the first step in most bioengineering projects, and unlike larger fermenters, microtiter plates and shake flasks do not allow for continuous monitoring and control of many factors.

This paper demonstrates that fractional factorial designs can be used to identify the experimental factors that have the greatest effect on the growth and productivity of engineered organisms. In our two test cases, we found that the geometry and shaking of the growth container have the largest effects on the growth and productivity of our organisms, and that these factor effects are reproducible. We found that we can achieve reproducible performance by carefully controlling these factors. We used these data to develop a Minimum Information Standard for Engineered Organisms Experiments (MIEO) that will help improve the repeatability and reproducibility of engineered organism experiments.

## Results

**Experimental factors and experimental design.** The factors that affect cell growth/productivity of engineered *E. coli* can be grouped into three broad categories: media; container, which is

the culture vessel within which cells are grown, such as microtiter plates or shake flasks; and other factors, including time, environment, selective agents, and inoculum (Supplementary Fig. 1). We identified 32 experimental factors that have been reported to affect cell growth/productivity (Table 1).

We evaluated these factors with orthogonal two-level fractional and full factorial experiments. Factorial designs have two main advantages compared with evaluating one factor at a time: increased precision in estimating factor effects with minimal bias from factor interactions, and the ability to detect interactions between multiple factors. Factorial designs also have some limitations: estimates of factors are limited to the levels selected for each factor<sup>16</sup>.

For our first test case, *E. coli* engineered to constitutively produce the small molecule lycopene<sup>17</sup>, we evaluated the effect of 22 factors on three responses: dry cell mass, titer, and yield (yield is the ratio of titer to dry cell mass, and is a dimensionless, scalable parameter). We chose these 22 factors because they were accessible in our laboratory and relevant to our test strain. For each factor, we selected two levels, low and high; a center level was included when possible (Table 1). We quantified the effect of each factor on the responses by the relative effect magnitude, which is the absolute value of the difference between the mean response at the two levels divided by the overall mean response.

Our experimental design consisted of 256 experimental runs organized into three groups. A run is a single combination of experimental growth conditions. Runs were grouped to answer a particular question: which factors have the largest effect on growth/productivity (Group 1), are those effects reproducible under different conditions of use (Group 2), and is a single set of conditions repeatable and reproducible over time (Group 3, see Methods for definitions of repeatability and reproducibility). Because it was logistically impossible for us to execute all of the runs in a group in one experiment, groups were divided by factor category (Group 1), factor effect (Group 2), and time (Group 3) for execution in sequential factorial experiments (Fig. 1a and Supplementary Data 1).

**Lycopene test case.** Group 1 screened factor effects and intra-category interactions in 112 runs, divided into four experiments by factor category: media composition, microwell containers, shake flask containers, and other, using  $2^{(8-3)}$ ,  $2^5$ ,  $2^4$ , and  $2^5$  orthogonal factorial designs, respectively, with appropriate randomization. These designs allowed us to estimate the main effect of each factor and to detect two-factor interactions within each category. These designs did not allow us to detect interactions between factors in different categories, which we addressed in Group 2.

Varying the factor levels for growing our strain resulted in a dynamic range of 4–12 g L<sup>-1</sup> for dry cell mass and 1–16 mg L<sup>-1</sup> for lycopene titer (Fig. 1b and Supplementary Fig. 2). We calculated the relative effect magnitude of two-factor interactions for all pairs of factors in each experiment (Supplementary File 1b), and identified the largest two-factor interactions by examining a normal probability plot of the effects (Supplementary Fig. 3). Particularly interesting two-factor interactions (Q:P, N:P, X:K) occurred between yeast extract source and magnesium sulfate (supplementing the media with 0.24 g L<sup>-1</sup> magnesium sulfate<sup>18</sup> eliminated the effect of yeast extract source) and between container factors (nonlinear interactions between shaking speed, container volume, and fill volume) (Supplementary Figs. 4–6).

Container factors and glycerol had the largest effect on strain productivity (Fig. 1c and Supplementary Fig. 7). Container factors primarily affect oxygen transfer into the media, but can also affect

**Table 1 32 experimental factors that have been documented to affect cell growth and productivity**

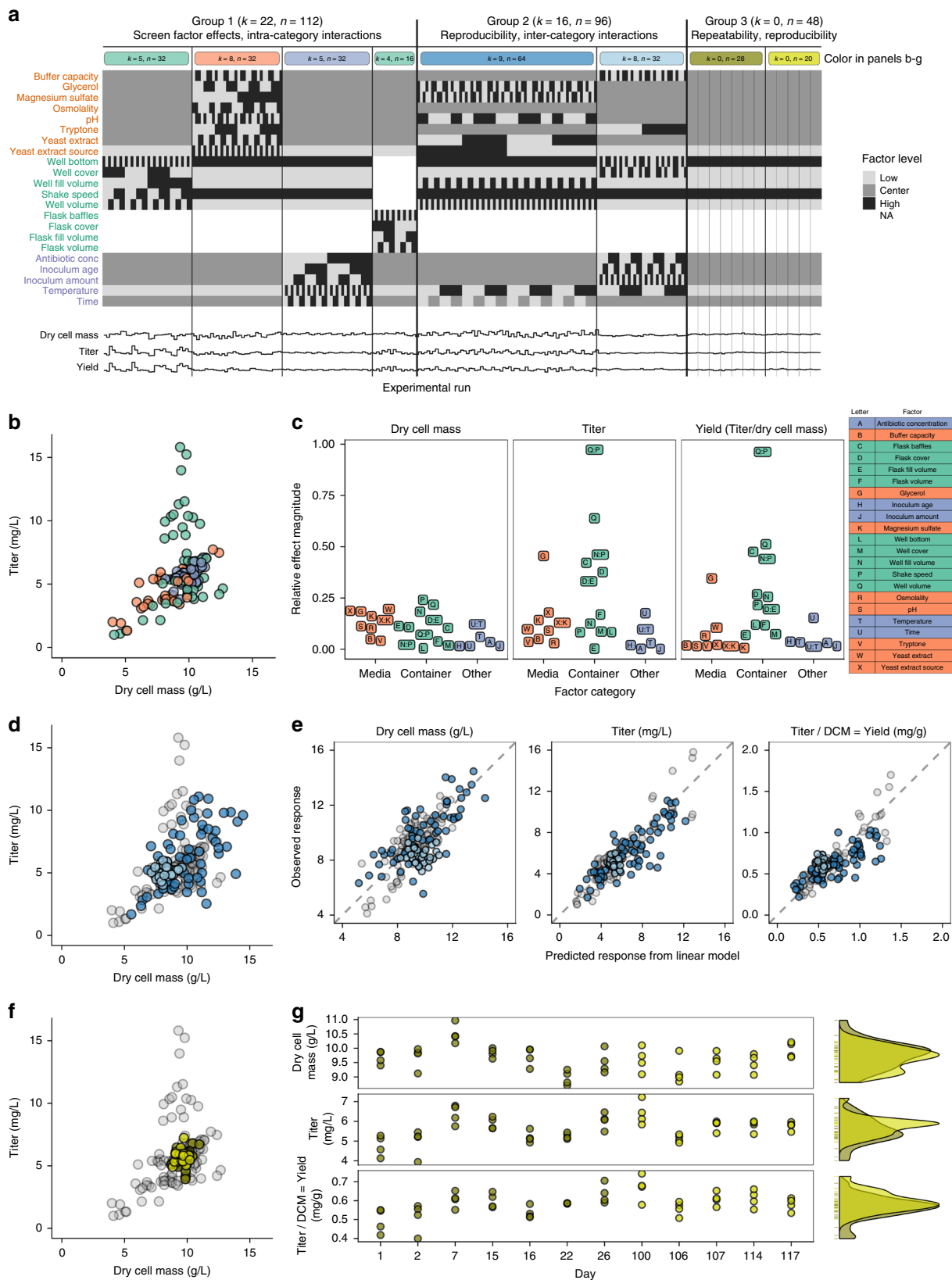
	Factor	References	Experimental factor	Low	Center	High
<b>Media</b>	<i>Components</i>					
	Media type	39–47				
	Carbon source	41,45,47–51	Yeast extract (g L <sup>-1</sup> )	20	24	28
			Glycerol (g L <sup>-1</sup> )	3	5	7
	Nitrogen source	47,52	Tryptone (g L <sup>-1</sup> )	10	12	14
	Inorganic ions	18,52,53	Magnesium sulfate (g L <sup>-1</sup> )	0	0.12	0.24
	Manufacturer	18	Yeast extract source	Sigma	---	Millipore
	<i>Properties</i>					
	pH	52,54–58	pH	6.7	7.2	7.5
	Osmolality	30,52,58,59	Buffer capacity (mmol L <sup>-1</sup> )	70	90	110
Media viscosity	60–63	Osmolality (mmol kg <sup>-1</sup> )	650	750	850	
<b>Container</b>	<i>Geometry</i>					
	Volume	21,61,64	Well volume (mL)	2.5	---	10
			Flask volume (mL)	125	---	250
	Fill volume	21,44,46,61,65–69	Well fill volume	10%	---	30%
			Flask fill volume	7.5%	---	15%
	Cover	68,70–74	Well cover	Aeraseal	---	Aluminum
			Flask cover	Foam	---	Aluminum
	Well shape	44,64,66,67				
	Well bottom	44	Well bottom	Round	---	Pyramidal
	Flask baffles	60,61,73–78	Flask baffles	Unbaffled	---	Baffled
	Baffle geometry	61				
	Surface coating	67,79				
	Container diameter	46,55				
	<i>Shaking</i>					
	Shake speed	21,44–46,61,64–68,70,79–81	Shake speed (rpm)	230	---	460
Shake diameter	46,64,65,67,79,80					
<b>Other</b>	<i>Time</i>					
	Time	40,44	Time (h)	24	48	72
	<i>Environment</i>					
	Temperature	39,40,44,58,82	Temperature (°C)	30	---	37
	Incubator O <sub>2</sub> concentration	41				
	Lab	2,51,83–85				
	Operator	85				
	<i>Inoculum</i>					
	Inoculum concentration	44,86	Inoculum amount (cells mL <sup>-1</sup> )	2 × 10 <sup>6</sup>	8 × 10 <sup>6</sup>	3 × 10 <sup>7</sup>
			Inoculum age (h)	3	16	16 + 96
Glycerol in freezer stock	87					
Cell phase at preservation	87					
Time in storage	88					
<i>Selective agents</i>						
Antibiotic type	51					
Antibiotic concentration	39,89	Antibiotic concentration (μg mL <sup>-1</sup> )	6.25	25	100	
<i>Inducers</i>						
Inducer amount	40,44,90,91					
Induction time	44,90					

The factors are grouped in three broad categories, and can be further broken down to 9 more specific categories. From this list, we selected 22 factors that were practically accessible to us in the laboratory to evaluate. For each factor, we selected two levels, low and high, for evaluation in a fractional factorial design. For quantitative factors, where possible, we added a third center level.

exchange of other gases, shear forces, and mixing within the media<sup>19–21</sup>. The biggest single effect was the interaction between well volume and shake speed. Titer was more sensitive to container factors than dry cell mass. Dry cell mass and titer were equally sensitive to media factors. Except for glycerol, yield was not sensitive to media factors—changing the media composition affected the total amount of cells that grew in the culture, but not the per-cell productivity. Time and temperature had relatively small effects at the levels used here.

In Group 2, we evaluated the reproducibility of factor effects and screened inter-category interactions in 96 runs. We split the

factors into two experiments based on the results from Group 1: nine factors that had large effects on the responses, and eight factors that had small effects on the responses, using 2<sup>(9–3)</sup> and 2<sup>(8–3)</sup> orthogonal fractional factorial designs, respectively (Fig. 1d). We trained a linear model with the Group 1 data to predict responses from these factors (Supplementary Note 1 and Supplementary Data 1). We then tested this model by using it to predict the responses in Group 2 (Fig. 1e). These results show that the factor effects are predictable by a linear model, reproducible under different conditions of use, and that there were no measureable two-factor interactions



between factors in different categories (Supplementary Fig. 8 and Data 1d).

In Group 3, we evaluated the repeatability and reproducibility of the growth/productivity at a single set of factor levels (centerpoint levels) in 48 runs. Four replicate runs were

performed on each of 12 different days over 4 months: 7 days in the first month and 5 days in the fourth month (Fig. 1f, g). The variance within each of the 12 days was homogeneous (Supplementary Table 1). The repeatability within a single day (mean repeatability standard deviation (SD)) was 3.5% for dry

**Fig. 1** Repeatability and reproducibility of factor effects on cell growth and lycopene productivity. **a** Experimental design table with 22 factor rows, and 256 experimental run columns. Colored bars at the top correspond to color of points in other panels.  $k$  is the number of factors varied, and  $n$  is the number of runs, in a group or experiment. The three responses, normalized to range from 0 to 1, are given below. **b** Dynamic range of lycopene titer and dry cell mass observed in Group 1 experiments. **c** Relative effect magnitude of all 22 factors on all three responses, colored by factor category. **d** Dynamic range of lycopene titer and dry cell mass observed in Group 2 experiments. **e** Factor effects observed in Group 1 are reproducible in Group 2. Gray points are Group 1 data used to train a linear model (dry cell mass  $r^2 = 0.66$ , titer  $r^2 = 0.85$ , and yield  $r^2 = 0.87$ ). Blue points are Group 2 used to test a linear model (dry cell mass  $r^2 = 0.46$ , titer  $r^2 = 0.71$ , and yield  $r^2 = 0.56$ ). **f** Dynamic range of titer and dry cell mass observed in Group 3 centerpoint replicates. **g** Centerpoint replicates plotted as a function of day on which they were run show no trends over time (left). Density plots (smoothed histograms) of response distribution in the first 26 days (dark yellow) and last 17 days (light yellow) overlap

cell mass, 7.2% for titer, and 8.2% for yield. The reproducibility between the first and fourth month (reproducibility SD) was 4.9% for dry cell mass, 11.4% for titer, and 11.4% for yield. The distribution of the data from the two months was similar, with month only accounting for 2.3% (dry cell mass), 4.9% (titer), and 8.7% (yield) of the variance with the population, as determined by an analysis of variance (Fig. 1g). These results show that using our method to identify and control experimental parameters allowed us to reproduce our results over time.

**RFP test case.** For our second test case, we evaluated the effect of 18 factors on the dry cell mass, titer, and yield of *E. coli* BW25113 engineered to constitutively express the heterologous protein RFP<sup>22</sup>. We did not include the four shake flask factors, as these were not accessible in our laboratory for this test case. We observed similar results as with lycopene, except for different relative effect magnitudes of the container factors on titer (Supplementary Figs. 9–16 and Supplementary Data 2). We speculate that these differences may be due to differences in the utilization of oxygen in the bio-synthetic pathways of the two products—lycopene is derived from central metabolism, and RFP is a heterologous protein.

## Discussion

We have determined a sufficient description of experimental factors that enabled repeatable and reproducible measurements of growth and productivity of two engineered *E. coli* strains. This demonstrates proof-of-principle of our approach, and is a step toward the creation of a minimum information standard for growth conditions of engineered organisms, which would support interoperability of engineered parts and enable assessment of reproducibility<sup>5,23</sup>.

Experimental growth conditions are frequently specified and documented by free-form text, such as the methods sections of most journals. These unstructured narratives are problematic because it is left to the authors to decide what information to include, and they can be difficult to parse. We propose developing a Minimum Information Standard for Engineered Organism Experiments (MIEO), using a method such as that described here, to address this issue. MIEO should be useful for any biological engineer who is planning experiments, reporting results, comparing results, or reproducing results within and between organizations.

To maximize the success of MIEO, we will incorporate lessons about modularity and simplicity learned from previous minimum information checklists. MIEO will be a modular checklist<sup>11,24,25</sup>, capturing information in nine categories (Table 2). The factors that should be included in each category will be different in each experiment (Supplementary Note 2). Categories will be designated as required or optional for reporting, similar to other standards<sup>9,11</sup>. Categories are optional because they can be derived from other categories, or are not applicable in every situation. MIEO is intended to be compatible with any cell type, and any downstream assay, complementing the existing suite of minimum information checklists<sup>25</sup>.

**Table 2** Minimum Information Standard for Engineered Organism Experiments (MIEO) v0.1, with Group 3 factors and levels as an example (Fig. 1a)

MIEO category	Factor	Level
Media components (R)	Yeast extract	24 g L <sup>-1</sup>
	Yeast extract source	Sigma Y1625-250G, Lot SLBR9838V
	Glycerol	5 g L <sup>-1</sup>
	Magnesium sulfate	0.12 g L <sup>-1</sup>
	Tryptone	12 g L <sup>-1</sup>
	Potassium phosphate	2.28 g L <sup>-1</sup>
	Dipotassium phosphate	12.7 g L <sup>-1</sup>
	Sodium chloride	6.63 g L <sup>-1</sup>
	Water	D1 water (18 MΩ-cm)
	Media properties (O)	pH
Buffer capacity		90 mmol L <sup>-1</sup>
Osmolality		750 mmol kg <sup>-1</sup>
Container geometry (R)	Type	96-well plate
	Well shape	Square
	Well bottom	Round
	Well volume	2.5 mL
	Fill volume	10% (0.25 mL)
	Cover	AeraSeal
Container shaking (R)	Shaking speed	460 rpm
	Shaking diameter	12.5 mm
	Shaking mode	Orbital
Time (R)	Growth time	48 h
Environment (R)	Temperature	30 °C
	Relative humidity	80%
Selective agents (O)	Antibiotic type	Chloramphenicol
	Antibiotic concentration	25 μg mL <sup>-1</sup>
Inoculum (R)	Concentration at inoculation	OD <sub>600</sub> = 0.01
	Age of inoculum at inoculation	16 h
Inducers (O)	None	None

The nine MIEO factor categories are given, along with whether their reporting is required (R) or optional (O). Factors and their level are reported

One of the key factors that determine the adoption of a minimum information standard is simplicity<sup>26</sup>. We will aim for simplicity by limiting the standard to nine categories of information, and by including both human-readable/writable (e.g., a table created in word-processing or spreadsheet software) and machine-readable/writable (e.g., XML) implementations. While a machine-readable/writable format has obvious appeal, the cost of adopting such a standard can be prohibitive for some. We have created an example checklist based on the centerpoint experimental conditions used in this paper (Table 2).

Standards development is best as a community-driven bottom-up effort, not a top-down prescription<sup>27,28</sup>. We encourage other members of the biotechnology community to contribute to the development of this standard (<http://jimb.stanford.edu/mieo/>).

In our experiments, we found that the geometry and shaking of the growth container had the largest effect on productivity. These factors warrant special consideration, because they are often tied to large capital expenditures, and can be difficult to change. Given their nonlinear effects, if factor levels cannot be matched in different labs, then expectations about reproducibility should be adjusted accordingly.

The challenges facing the reproducibility of experimental data in biology are momentous. The results shown in this paper demonstrate a method for reproducing key experimental results over time and under different conditions of use. A well-implemented and widely adopted minimum information standard would improve the repeatability and reproducibility of engineered organism experiments. Experimental reproducibility would advance biological engineering toward becoming a more reliable and predictable engineering discipline.

## Methods

**Strain engineering.** The parent strain for both test strains used in this paper was *Escherichia coli* BW25113 ( $\Delta(\text{araD-araB})567 \Delta\text{lacZ4787}(\text{rrnB-3}) \lambda^- \text{rph-1} \Delta(\text{rhaD-rhaB}) 568 \text{ hsdR514}$ ) obtained from the Yale Coli Genetic Stock Center (New Haven, CT). For production of lycopene, the parent strain was transformed with plasmid pAC-LYC<sup>17</sup>, a gift from Francis X. Cunningham Jr (Addgene plasmid #53270). For production of RFP (mRFP1), the parent strain was transformed with plasmid pFAB3992<sup>22</sup>, a gift from Drew Endy (Addgene plasmid #47823). Plasmid sequences (Supplementary Data 3) and maps (Supplementary Fig. 17) are available online. All reagents used in this paper with manufacturer, product, and lot numbers are available online (Supplementary Table 2).

pAC-LYC was received transformed in *E. coli* Top10 in an agar stab (Addgene plasmid #53270). A plate of lysogeny broth (LB) agar (10 g L<sup>-1</sup> tryptone, 5 g L<sup>-1</sup> yeast extract, 10 g L<sup>-1</sup> sodium chloride, and 15 g L<sup>-1</sup> bacto agar) with 25 µg mL<sup>-1</sup> chloramphenicol was streaked with a sterile pipette tip dipped into the agar stab, and incubated overnight at 37 °C. A single colony was picked, and grown overnight in 5 mL of LB (10 g L<sup>-1</sup> tryptone, 5 g L<sup>-1</sup> yeast extract, and 10 g L<sup>-1</sup> sodium chloride) with 25 µg mL<sup>-1</sup> chloramphenicol. The plasmid was prepared using the manufacturer's provided protocol. Plasmid identity was confirmed by digestion with Pst1-HF (Supplementary Fig. 18).

The parent strain was received on a dehydrated paper disk. The disk was placed on an LB agar plate using sterilized forceps, and rehydrated with one drop of LB. A sterile pipette tip was used to streak the moisture from the disk, and the plate was incubated overnight at 37 °C. A single colony was carefully picked with a sterile pipette tip and inoculated into 5 mL of LB, which was incubated overnight for 16 h at 37 °C, shaking at 250 rpm with a 25 mm shaking diameter (Thermo Fisher Forma Model 440 Orbital Shaker). In total, 20 µL of the overnight culture was used to inoculate 2 mL of fresh LB, which was then incubated in the same incubator for 2 h. The cells were resuspended in 100 µL of 100 mM of ice-cold sterile-filtered calcium chloride solution in a 1.5 mL microcentrifuge tube. In total, 1 µL of pAC-LYC prepared plasmid (approximate concentration 90 ng µL<sup>-1</sup>) was added to the cell suspension, and the cells were incubated on ice for 30 min. The cells were heat-shocked in a 42 °C water bath for 30 s, and then incubated on ice for 2 min. In total, 400 µL of SOC media was added to the cells, and they were incubated at 37 °C with gentle mixing for 1 h. In total, 25 µL of the cell solution was pipetted onto an LB agar plate with chloramphenicol and incubated overnight at 37 °C. A single colony was picked from the agar plate, incubated in 5 mL of LB with chloramphenicol, and grown for 4 h. In total, 750 µL of the culture was mixed with 750 µL of 50% sterile-filtered glycerol in a cryovial for long-term storage at -80 °C. All lycopene-producing cells used in this paper were derived from this glycerol stock.

pFAB3992 was received transformed in *E. coli* BW25113 in a frozen glycerol stock. A plate of LB agar with 24 µg mL<sup>-1</sup> kanamycin was streaked with a sterile pipette tip streaked across the glycerol stock, and incubated overnight at 37 °C. A single colony was picked from the agar plate, incubated in 5 mL of LB with kanamycin, and grown for 4 h. In total, 750 µL of the culture was mixed with 750 µL of 50% sterile-filtered glycerol in a cryovial for long-term storage at -80 °C. All RFP-producing cells used in this paper were derived from this glycerol stock.

**Cell culture.** LB agar plates with the appropriate antibiotic (25 µg mL<sup>-1</sup> chloramphenicol or 50 µg mL<sup>-1</sup> kanamycin) were streaked with a sterile pipette tip from glycerol stocks, and incubated overnight at 37 °C. Plates were stored, wrapped in Parafilm M (Bemis NA, Neenah WI), at 4 °C for up to 2 weeks, after which they were discarded. All cultures were grown in variants of Terrific Broth (TB), which has a baseline composition of 24 g L<sup>-1</sup> yeast extract, 12 g L<sup>-1</sup> tryptone, 5 g L<sup>-1</sup> glycerol, 0.17 mol L<sup>-1</sup> KH<sub>2</sub>PO<sub>4</sub>, and 0.72 mol L<sup>-1</sup> K<sub>2</sub>HPO<sub>4</sub><sup>29</sup>. These values were used as centerpoint values for media composition. We modified this recipe by adding magnesium sulfate to supplement deficient magnesium content in the yeast extract<sup>18</sup>, and adding sodium chloride to adjust the osmolality<sup>30</sup>.

Every experiment began with a liquid starter culture. A single colony was picked from the agar plate, inoculated into 4 mL of TB with appropriate antibiotic in a plastic-capped 16 × 100-mm glass culture tube (VWR 47729-576), and grown for 16 h at 37 °C, shaking at 250 rpm with a 25-mm shaking diameter. This culture was diluted with phosphate-buffered saline (PBS) to an OD<sub>600</sub> = 0.5 (as measured in a BRAND semi-micro polystyrene cuvette on a WPA Bioware CO8000 Cell Density Meter), and was then used as the starter culture for inoculating the experimental runs. A fresh starter culture was prepared on each day on which an experimental run was started. All experimental runs started on the same day were inoculated from the same starter culture, except for cultures with different inoculum age. For the inoculum age of 3 h, a 50 µL aliquot of the 16 h starter culture was taken and used to inoculate 4 mL of fresh media in a glass culture tube, and returned to the incubator for 3 h, then removed, and diluted to OD<sub>600</sub> = 0.5. This culture was in exponential phase at the time that it was removed from the incubator. For the inoculum age of 16 + 96 h, after the usual 16-h incubation, the starter culture was stored at 4 °C for 96 h, and then removed and diluted to OD<sub>600</sub> = 0.5 for use.

For cultures with varying pH or varying buffer capacity, media composition was determined by simultaneously solving the Henderson-Hasselbach equation:

$$\text{pH} = \text{pKa} + \log_{10} \left( \frac{[A^-]}{[HA]} \right) \quad (1)$$

and the equation for buffer capacity:

$$\text{Buffer capacity} = [A^-] + [HA] \quad (2)$$

for  $[A^-]$  and  $[HA]$ , where  $A^-$  is the conjugate base,  $HA$  is the conjugate acid, and pKa for phosphate buffers is 6.86<sup>31</sup>. Solving these two equations for the baseline TB composition gives pH = 7.5 and buffer capacity = 90 mM. Adding the remaining media components lowered the pH by 0.3–0.5 pH units. In designing the experiments, we aimed for pH of 7.0, 7.5, or 8.0. We measured the pH of the media with a pH meter, and found that the actual pH was ~6.7, 7.2, or 7.5, respectively.

For cultures with varying osmolality, the osmolality of all the media components was calculated assuming complete dissociation of ionic species, and the empirically determined osmolality of yeast extract and tryptone of 6 mmol L kg<sup>-1</sup> g<sup>-1</sup>. Sodium chloride was added to increase the osmolality to the desired level<sup>30</sup>. The osmolality of 12 different media solutions, as measured by the Wescor Vapro 5520 Vapor Pressure Osmometer, was within 7% of the target value (Supplementary Table 3).

The growth of our test strains for the factorial experiments (Fig. 1a and Supplementary Fig. 9a) was performed under the conditions listed in Table 1 and Supplementary Data 1-2, and the growth of our test strains for the centerpoint replicates was performed under the conditions listed in Table 2. The full experimental design table, with all settings for each run, is available online (Supplementary Data 1-2). Stocks of each individual media component were prepared at 10X concentration of the centerpoint value with DI water except for magnesium sulfate and dipotassium phosphate, which were purchased. Stocks were sterilized by an autoclave except for glycerol, which was sterilized by a 0.22 µm syringe filter (Whatman Puradisc FP30). The position of each run on a plate, and the order in which the runs were set up and sampled, was randomized.

Four different types of container covers were used (Supplementary Table 2 and Data 1, 2). Microwell plates were covered with either the gas-permeable, adhesive AeraSeal membrane (E&K Scientific), or the AeraSeal membrane and a gas-impermeable aluminum foil tape (Bio-Rad). The AeraSeal membrane was first applied to prevent direct contact between the liquid media and the aluminum foil tape. Shake flasks were covered with either the gas-permeable silicone foam covers (Bellco Glass), or two layers of gas-impermeable aluminum foil secured with ParaFilm wrapped around the base of the neck of the flask.

**Assay calibration.** Our absorbance assay for lycopene was calibrated using a 1mg lycopene standard (Sigma, L9879-1MG, Lot# SLBS4759 and SLBV5371). The lyophilized standard was stable for only 48 h after being dissolved in solvent. A 1:1:1 (v/v/v) mixture of methanol, acetone, and dichloromethane was the solvent for the calibration. The mixture was prepared by mixing 30 mL each of the three solvents. The lycopene standard was dissolved in 40 mL of solvent in a 50 mL polypropylene Falcon tube by shaking and vortexing for 10 min until the standard dissolved. The tube was covered with aluminum foil to minimize exposure to light. In total, 240 µL of the standard solution was diluted with 2.76 mL of solvent to create a solution with nominal concentration 2 µg mL<sup>-1</sup>. This solution was transferred to a Hellma Analytics 6030-10-10 cuvette (10 mm path length), along with 3 mL of solvent transferred to a second cuvette to serve as a blank. The background-subtracted absorbance of the standard solution was measured to determine its concentration using reported values of the absorbance peaks and molar extinction coefficients of lycopene in the three solvents<sup>1</sup> (Supplementary Table 4).

We used the lycopene standard to calibrate our Molecular Devices SpectraMax i3 plate reader. An absorbance spectrum showed that the three absorbance peaks for lycopene were at 449 nm, 475 nm, and 507 nm (Supplementary Fig. 19a). We prepared solutions ranging in concentration from 0 to 8 µg mL<sup>-1</sup> from the main standard solution. We dispensed five 200 µL aliquots of each solution and a solvent blank into randomized wells on a polypropylene clear-bottom 96-well plate. We

measured absorbance of the plate at 475 nm and 507 nm, and used these values to generate a calibration curve (Supplementary Fig. 19b). This calibration was performed twice, 4 months apart, and similar curves were obtained in both calibrations. We averaged the slope of the two curves for calibrating lycopene absorbance measurements.

To calibrate measurements of optical density at 700 nm (because RFP absorbs at 600 nm<sup>2</sup>) on the plate reader to dry cell mass, we inoculated 50 mL of TB in a 250 mL shake flask with a single colony of cells, and incubated it for 24 h. From this culture, we created six different 20 mL cultures of cells in 50 mL Falcon tubes with OD<sub>700</sub> ranging from 1 to 6, using PBS for the dilutions. We removed 250 µL from each and diluted again with 1 mL of PBS. We added five 200 µL aliquots from each dilution and a PBS blank to a randomly assigned well on a clear-bottom polystyrene 96-well plate, and measured the OD<sub>700</sub> for each well.

Falcon tubes with the 20 mL cultures were centrifuged at 6000 × g for 10 min. The supernatant was removed, the cells were resuspended in PBS, and washed. The cells were centrifuged again at 6000 × g for 10 min, the supernatant was poured off, and all remaining liquid aspirated. The tubes were placed uncovered in a drying oven at 105 °C for 24 h. The tubes were then removed, covered, and allowed to cool to room temperature. The dried cell pellets were carefully removed and weighed on a balance with 0.1 mg of precision. The absorbance measurements and cell pellet masses were used to generate a calibration curve (Supplementary Fig. 20). The calibration was performed twice, and we averaged the slopes of the two curves to calibrate OD<sub>700</sub> to dry cell mass.

**Assay performance.** At the conclusion of the experimental growth time, a 250 µL aliquot from each culture was assayed for dry cell mass and titer. The 250 µL aliquot (in a deep-well 96-well plate) was diluted with 1 mL of PBS. A 40 µL aliquot of the diluted cells was transferred into 160 µL of PBS in a clear-bottom polystyrene 96-well plate and mixed. Absorbance at 700 nm was measured on a Molecular Devices SpectraMax i3 plate reader. For cells expressing RFP, fluorescence was also measured on the plate reader with excitation at 585 nm and emission at 625 nm.

For cells expressing lycopene, which accumulates in the cytoplasmic membrane<sup>32</sup>, the remaining 1210 µL of the diluted cells were transferred to a 1.5 mL microcentrifuge tube, and centrifuged on an Eppendorf MiniSpin microcentrifuge with F-45-12-11 rotor at 1100×g (4000 rpm) for 4 min. The supernatant was aspirated, and then lycopene was extracted using a modified version of a previously published protocol<sup>33</sup>. In total, 250 µL of methanol was added, and the tubes were vortexed vigorously for 5 s to break up the cell pellet. A pipette tip was then used to further break up the pellet. In total, 250 µL of acetone was added, and the tubes were vortexed vigorously for 5 s again. Then, 250 µL of dichloromethane was added, the tubes were vortexed vigorously for 5 s, and then allowed to incubate at room temperature for 10 min to complete the extraction of lycopene from the cell pellets. The tubes were centrifuged at 12,000 × g (13,400 rpm) for 5 min to pellet the cell debris, and then 200 µL aliquots were transferred to randomly assigned wells on a clear-bottom polypropylene 96-well plate, along with four aliquots of solvent blanks. During the aliquoting process, the plate was covered with a polypropylene plate cover to minimize evaporation, which is a concern when working with small volumes of volatile solvents. Absorbance at 475 nm, 507 nm, and 600 nm was measured in the plate reader. Lycopene does not absorb at 600 nm. Absorbance at 600 nm was used to detect the presence of contamination in the samples. The calibration curves were applied to measurements of absorbance at 475 nm and 507 nm to estimate lycopene concentration at these two absorbance peaks, and then averaged to determine the lycopene concentration in the sample.

**Data analysis.** All raw and processed data are available online (Supplementary Data 4), at doi: 10.6084/m9.figshare.6848957, and <https://github.com/arielhecht/cell-metrics>. Absorbance and fluorescence measurements were collected through the Molecular Devices SoftMax Pro 6.4 software. All data analysis was performed in R with the FrF2<sup>34</sup> package for fractional factorial design and analysis, tidyverse<sup>35</sup> packages for data transformation, and the ggplot2<sup>36</sup> package for figure generation.

Repeatability is the closeness of the agreement between the results of successive measurements of the same measurand carried out under the same conditions of measurement<sup>37</sup>. Reproducibility is the closeness of the agreement between the results of measurements of the same measurand carried out under changed conditions of measurements (which may include principle of measurement, method of measurement, observer, measuring instrument, reference standard, location, conditions of use, or time)<sup>37</sup>. We evaluated reproducibility under changed conditions of use and time.

In this paper, we define titer as the amount of product produced (mg of lycopene or arbitrary fluorescence units of RFP) per volume of culture. We define dry cell mass as the mass of dry cells per volume of culture. We define yield as the ratio of the amount of product produced per mass of dry cells, which is the quotient of titer over yield.

Relative effect magnitude is the absolute value of the difference between the mean response at each level divided by the overall mean response. For one factor,

$X_i$ , at two levels,  $-$  and  $+$ , with one response  $Y$ , the relative effect magnitude is

$$REM_{X_i} = \left| \frac{\bar{Y}_{X_i+} - \bar{Y}_{X_i-}}{\bar{Y}} \right| \quad (3)$$

For two factors,  $X_i$  and  $X_j$ , the relative effect magnitude is

$$REM_{X_i X_j} = \left| \frac{\bar{Y}_{X_i+ X_j+} + \bar{Y}_{X_i- X_j-} - \bar{Y}_{X_i+ X_j-} - \bar{Y}_{X_i- X_j+}}{\bar{Y}} \right| \quad (4)$$

**Code availability.** All R scripts used to generate the experimental designs and analyze the experimental data are available online at <https://github.com/arielhecht/cell-metrics>.

## Data availability

Source data for Fig. 1 and Supplementary Figs. 2–16 have been provided in Supplementary Data 4. All data are available online at <https://doi.org/10.6084/m9.figshare.6848957.v1><sup>38</sup>. All other data supporting the findings of this study are available from the corresponding author on request.

Received: 3 May 2018 Accepted: 29 October 2018

Published online: 06 December 2018

## References

- Baker, M. 1,500 scientists lift the lid on reproducibility. *Nature* **533**, 452–454 (2016).
- Beal, J. et al. Reproducibility of fluorescent expression from engineered biological constructs in *E. coli*. *PLoS ONE* **11**, e0150182 (2016).
- Andrianantoandro, E., Basu, S., Karig, D. K. & Weiss, R. Synthetic biology: new engineering rules for an emerging discipline. *Mol. Syst. Biol.* **2**, 2006.0028 (2006).
- Endy, D. Foundations for engineering biology. *Nature* **438**, 449–453 (2005).
- Munson, M., Munro, S. & Salit, M. Synthetic biology standards consortium kick-off workshop report (2015).
- Wu, G. et al. Metabolic burden: cornerstones in synthetic biology and metabolic engineering applications. *Trends Biotechnol.* **34**, 652–664 (2016).
- Galdzicki, M., Munro, S., Boyle, P. & Ubersax, J. *A Vision for a Synthetic Biology Standards Consortium*. (Synthetic Biology Leadership Excellence Accelerator Program, 2013).
- Galdzicki, M. et al. The synthetic biology open language (SBOL) provides a community standard for communicating designs in synthetic biology. *Nat. Biotechnol.* **32**, 545–550 (2014).
- Bustin, S. A. et al. The MIQE guidelines: minimum information for publication of quantitative real-time PCR experiments. *Clin. Chem.* **55**, 611–622 (2009).
- Brazma, A. et al. Minimum information about a microarray experiment (MIAME)-toward standards for microarray data. *Nat. Genet.* **29**, 365–371 (2001).
- Field, D. et al. The minimum information about a genome sequence (MIGS) specification. *Nat. Biotechnol.* **26**, 541–547 (2008).
- Bates, M., Berliner, A. J., Lachoff, J., Jaschke, P. R. & Groban, E. S. Wet lab accelerator: a web-based application democratizing laboratory automation for syntheticbiology. *ACS Synth. Biol.* **6**, 167–171 (2017).
- Aquarium. v.2.4.2 Available at <http://klavinslab.org/aquarium/> (University of Washington, 2018).
- Autoprotocol. v.5.1.0 Available at <http://autoprotocol.org> (Transcriptic, Inc., 2018).
- Anthra OS Documentation. v.0.5 Available at <https://docs.antha.com> (Synthace, Ltd., 2018).
- Box, G. E. P., Hunter, J. S. & Hunter, W. G. *Statistics for Experimenters: Design, Innovation, and Discovery*, 2nd edn (Wiley, 2005).
- Cunningham, F. X., Sun, Z., Chamovitz, D., Hirschberg, J. & Gantt, E. Molecular structure and enzymatic function of lycopene cyclase from the cyanobacterium *Synechococcus* sp strain PCC7942. *Plant Cell* **6**, 1107–1121 (1994).
- Studier, F. W. Protein production by auto-induction in high density shaking cultures. *Protein Expr. Purif.* **41**, 207–234 (2005).
- Eibl, R., Kaiser, S., Lombriser, R. & Eibl, D. Disposable bioreactors: the current state-of-the-art and recommended applications in biotechnology. *Appl. Microbiol. Biotechnol.* **86**, 41–49 (2010).
- Kirk, T. V. & Szita, N. Oxygen transfer characteristics of miniaturized bioreactor systems. *Biotechnol. Bioeng.* **110**, 1005–1019 (2013).

21. Maier, U., Losen, M. & Büchs, J. Advances in understanding and modeling the gas–liquid mass transfer in shake flasks. *Biochem Eng. J.* **17**, 155–167 (2004).
22. Mutalik, V. K. et al. Precise and reliable gene expression via standard transcription and translation initiation elements. *Nat. Methods* **10**, 354–360 (2013).
23. Parks, S. et al. *Developing standards to support the synthetic biology value chain*. (RAND Corporation, 2017) <https://doi.org/10.7249/RR1527>.
24. Sansone, S.-A. et al. A strategy capitalizing on synergies: the Reporting Structure for Biological Investigation (RSBI) working group. *OMICS* **10**, 164–171 (2006).
25. Taylor, C. F. et al. Promoting coherent minimum reporting guidelines for biological and biomedical investigations: the MIBBI project. *Nat. Biotechnol.* **26**, 889–896 (2008).
26. Brazma, A. Minimum Information About a Microarray Experiment (MIAME)—successes, failures, challenges. *ScientificWorldJournal* **9**, 420–423 (2009).
27. Brazma, A., Krestyaninova, M. & Sarkans, U. Standards for systems biology. *Nat. Rev. Genet.* **7**, 593–605 (2006).
28. Quackenbush, J. et al. Top-down standards will not serve systems biology. *Nature* **440**, 24 (2006).
29. Terrific Broth. *Cold Spring Harb. Protoc.* **2006**, pdb.rec8620 (2006).
30. Record, M. T., Courtenay, E. S., Cayley, D. S. & Guttman, H. J. Responses of *E. coli* to osmotic stress: large changes in amounts of cytoplasmic solutes and water. *Trends Biochem. Sci.* **23**, 143–148 (1998).
31. Nelson, D. L. & Cox, M. M. *Lehninger Principles of Biochemistry* (W 2012).
32. Wang, G.-S., Grammel, H., Abou-Aisha, K., Sägesser, R. & Ghosh, R. High-level production of the industrial product lycopene by the photosynthetic bacterium *Rhodospirillum rubrum*. *Appl. Environ. Microbiol.* **78**, 7205–7215 (2012).
33. Blatt, A. & Lohr, M. Extraction and analysis of carotenoids from *Escherichia coli* in color complementation assays. *Bioprotocol* **7**, e2179 (2017).
34. Grömping, U. R Package FrF2 for creating and analyzing fractional factorial 2-level designs. *J. Stat. Softw.* **56**, 1–56 (2014).
35. Wickham, H. & Grolemund, G. *R for Data Science: Import, Tidy, Transform, Visualize, and Model Data*. (O 2017).
36. Wickham, H. *ggplot2: Elegant Graphics for Data Analysis (Use R!)* (Springer, 2016).
37. Taylor, B. N. *Guidelines for evaluating and expressing the uncertainty of NIST measurement results*. <https://doi.org/10.6028/NIST.TN.1297> (National Bureau of Standards, 1994).
38. Hecht, A., Filliben, J., Munro, S. & Salit, M. A minimum information standard for reproducing bench-scale bacterial cell growth and productivity data sets. *figshare* <https://doi.org/10.6084/m9.figshare.6848957.v1> (2018).
39. Marini, G. et al. Experimental design approach in recombinant protein expression: determining medium composition and induction conditions for expression of pneumolysin from *Streptococcus pneumoniae* in *Escherichia coli* and preliminary purification process. *BMC Biotechnol.* **14**, 1 (2014).
40. Muntari, B., Amid, A., Mel, M., Jami, M. S. & Salleh, H. M. Recombinant bromelain production in *Escherichia coli*: process optimization in shake flask culture by response surface methodology. *AMB Express* **2**, 12 (2012).
41. Losen, M., Frölich, B., Pohl, M. & Büchs, J. Effect of oxygen limitation and medium composition on *Escherichia coli* fermentation in shake-flask cultures. *Biotechnol. Prog.* **20**, 1062–1068 (2004).
42. Moser, F. et al. Genetic circuit performance under conditions relevant for industrial bioreactors. *ACS Synth. Biol.* **1**, 555–564 (2012).
43. Paliy, O. & Gunasekera, T. S. Growth of *E. coli* BL21 in minimal media with different gluconeogenic carbon sources and salt contents. *Appl. Microbiol. Biotechnol.* **73**, 1169–1172 (2007).
44. Islam, R. S., Tisi, D., Levy, M. S. & Lye, G. J. Framework for the rapid optimization of soluble protein expression in *Escherichia coli* combining microscale experiments and statistical experimental design. *Biotechnol. Prog.* **23**, 785–793 (2007).
45. Micheletti, M. et al. Fluid mixing in shaken bioreactors: implications for scale-up predictions from microlitre-scale microbial and mammalian cell cultures. *Chem. Eng. Sci.* **61**, 2939–2949 (2006).
46. Meier, K. et al. Correlation for the maximum oxygen transfer capacity in shake flasks for a wide range of operating conditions and for different culture media. *Biochem Eng. J.* **109**, 228–235 (2016).
47. Singh, V. et al. Strategies for fermentation medium optimization: an in-depth review. *Front. Microbiol.* **7**, 2087 (2016).
48. Ehrenberg, M., Bremer, H. & Dennis, P. P. Medium-dependent control of the bacterial growth rate. *Biochimie* **95**, 643–658 (2013).
49. Hempfling, W. P. & Mainzer, S. E. Effects of varying the carbon source limiting growth on yield and maintenance characteristics of *Escherichia coli* in continuous culture. *J. Bacteriol.* **123**, 1076–1087 (1975).
50. Bennett, B. D. et al. Absolute metabolite concentrations and implied enzyme active site occupancy in *Escherichia coli*. *Nat. Chem. Biol.* **5**, 593–599 (2009).
51. Kelly, J. R. et al. Measuring the activity of BioBrick promoters using an *in vivo* reference standard. *J. Biol. Eng.* **3**, 4 (2009).
52. Neidhardt, F. C., Ingraham, J. L. & Schaechter, M. *Physiology of the Bacterial Cell: A Molecular Approach*. (Sinauer Associates Inc, 1990).
53. Neidhardt, F. C., Bloch, P. L. & Smith, D. F. Culture medium for enterobacteria. *J. Bacteriol.* **119**, 736–747 (1974).
54. Cladera-Olivera, F., Caron, G. R. & Brandelli, A. Bacteriocin production by *Bacillus licheniformis* strain P40 in cheese whey using response surface methodology. *Biochem Eng. J.* **21**, 53–58 (2004).
55. Seletzky, J. M. et al. Scale-up from shake flasks to fermenters in batch and continuous mode with *Corynebacterium glutamicum* on lactic acid based on oxygen transfer and pH. *Biotechnol. Bioeng.* **98**, 800–811 (2007).
56. Maurer, L. M., Yohannes, E., Bondurant, S. S., Radmacher, M. & Slonczewski, J. L. pH regulates genes for flagellar motility, catabolism, and oxidative stress in *Escherichia coli* K-12. *J. Bacteriol.* **187**, 304–319 (2005).
57. Presser, K. A., Ratkowsky, D. A. & Ross, T. Modelling the growth rate of *Escherichia coli* as a function of pH and lactic acid concentration. *Appl. Environ. Microbiol.* **63**, 2355–2360 (1997).
58. *Escherichia coli and Salmonella: Cellular and Molecular Biology (2 Volumes)*. (ASM Press, 1996).
59. Rojas, E., Theriot, J. A. & Huang, K. C. Response of *Escherichia coli* growth rate to osmotic shock. *Proc. Natl. Acad. Sci. USA* **111**, 7807–7812 (2014).
60. Delgado, G., Topete, M. & Galindo, E. Interaction of cultural conditions and end-product distribution in *Bacillus subtilis* grown in shake flasks. *Appl. Microbiol. Biotechnol.* **31**, 288–292 (1989).
61. Running, J. A. & Bansal, K. Oxygen transfer rates in shaken culture vessels from Fernbach flasks to microtiter plates. *Biotechnol. Bioeng.* **113**, 1729–1735 (2016).
62. Klöckner, W. et al. Correlation between mass transfer coefficient kLa and relevant operating parameters in cylindrical disposable shaken bioreactors on a bench-to-pilot scale. *J. Biol. Eng.* **7**, 28 (2013).
63. Giese, H. et al. Liquid films on shake flask walls explain increasing maximum oxygen transfer capacities with elevating viscosity. *Biotechnol. Bioeng.* **111**, 295–308 (2014).
64. Duetz, W. A. & Witholt, B. Oxygen transfer by orbital shaking of square vessels and deepwell microtiter plates of various dimensions. *Biochem Eng. J.* **17**, 181–185 (2004).
65. Duetz, W. A. et al. Methods for intense aeration, growth, storage, and replication of bacterial strains in microtiter plates. *Appl. Environ. Microbiol.* **66**, 2641–2646 (2000).
66. Funke, M., Diederichs, S., Kensy, F., Müller, C. & Büchs, J. The baffled microtiter plate: increased oxygen transfer and improved online monitoring in small scale fermentations. *Biotechnol. Bioeng.* **103**, 1118–1128 (2009).
67. Hermann, R., Lehmann, M. & Büchs, J. Characterization of gas-liquid mass transfer phenomena in microtiter plates. *Biotechnol. Bioeng.* **81**, 178–186 (2003).
68. Liu, Y.-S., Wu, J.-Y. & Ho, K. Characterization of oxygen transfer conditions and their effects on *Phaffia rhodozyma* growth and carotenoid production in shake-flask cultures. *Biochem Eng. J.* **27**, 331–335 (2006).
69. Kensy, F., John, G. T., Hofmann, B. & Büchs, J. Characterisation of operation conditions and online monitoring of physiological culture parameters in shaken 24-well microtiter plates. *Bioprocess Biosyst. Eng.* **28**, 75–81 (2005).
70. Chavez, M., Ho, J. & Tan, C. Reproducibility of high-throughput plate-reader experiments in synthetic biology. *ACS Synth. Biol.* **6**, 375–380 (2017).
71. Zimmermann, H. F., John, G. T., Trauthwein, H., Dingerdissen, U. & Huthmacher, K. Rapid evaluation of oxygen and water permeation through microplate sealing tapes. *Biotechnol. Prog.* **19**, 1061–1063 (2003).
72. Sieben, M., Giese, H., Grosch, J.-H., Kauffmann, K. & Büchs, J. Permeability of currently available microtiter plate sealing tapes fail to fulfil the requirements for aerobic microbial cultivation. *Biotechnol. J.* **11**, 1525–1538 (2016).
73. Gupta, A. & Rao, G. A study of oxygen transfer in shake flasks using a non-invasive oxygen sensor. *Biotechnol. Bioeng.* **84**, 351–358 (2003).
74. Freedman, D. in *Methods in Microbiology*. (eds Norris, J. R. & Ribbons, D. W.) Vol. 2 Chapter VI, 175–186 (Academic Press Inc, 1970).
75. McDaniel, L. E., Bailey, E. G. & Zimmerli, A. Effect of oxygen supply rates on growth of *Escherichia coli*. *Appl. Microbiol.* **13**, 109–114 (1965).
76. Büchs, J. Introduction to advantages and problems of shaken cultures. *Biochem Eng. J.* **7**, 91–98 (2001).
77. Henzler, H. J. & Schedel, M. Suitability of the shaking flask for oxygen supply to microbiological cultures. *Bioprocess Eng.* **7**, 123–131 (1991).
78. Schiefelbein, S. et al. Oxygen supply in disposable shake-flasks: prediction of oxygen transfer rate, oxygen saturation and maximum cell concentration during aerobic growth. *Biotechnol. Lett.* **35**, 1223–1230 (2013).
79. Maier, U. & Büchs, J. Characterisation of the gas-liquid mass transfer in shaking bioreactors. *Biochem Eng. J.* **7**, 99–106 (2001).



80. Kensy, F. et al. Oxygen transfer phenomena in 48-well microtiter plates: determination by optical monitoring of sulfite oxidation and verification by real-time measurement during microbial growth. *Biotechnol. Bioeng.* **89**, 698–708 (2005).
81. Betts, J. I. & Baganz, F. Miniature bioreactors: current practices and future opportunities. *Microb. Cell Fact.* **5**, 21 (2006).
82. Ratkowsky, D. A., Lowry, R. K., McMeekin, T. A., Stokes, A. N. & Chandler, R. E. Model for bacterial culture growth rate throughout the entire biokinetic temperature range. *J. Bacteriol.* **154**, 1222–1226 (1983).
83. Augustin, J.-C. & Carlier, V. Lessons from the organization of a proficiency testing program in food microbiology by interlaboratory comparison: analytical methods in use, impact of methods on bacterial counts and measurement uncertainty of bacterial counts. *Food Microbiol.* **23**, 1–38 (2006).
84. Bremser, W., Lücke, F. K., Urmetzer, C., Fuchs, E. & Leist, U. An approach to integrated data assessment in a proficiency test on the enumeration of *Escherichia coli*. *J. Appl. Microbiol.* **110**, 128–138 (2011).
85. Jarvis, B., Hedges, A. J. & Corry, J. E. L. Assessment of measurement uncertainty for quantitative methods of analysis: comparative assessment of the precision (uncertainty) of bacterial colony counts. *Int. J. Food Microbiol.* **116**, 44–51 (2007).
86. Ramírez, J., Gutierrez, H. & Gschaedler, A. Optimization of astaxanthin production by *Phaffia rhodozyma* through factorial design and response surface methodology. *J. Biotechnol.* **88**, 259–268 (2001).
87. Fonseca, F., Béal, C. & Corrieu, G. Operating conditions that affect the resistance of lactic acid bacteria to freezing and frozen storage. *Cryobiology* **43**, 189–198 (2001).
88. Clement, M. T. Effects of freezing, freeze-drying, and storage in the freeze-dried and frozen state on viability of *Escherichia coli* cells. *Can. J. Microbiol.* **7**, 99–106 (1961).
89. Sieben, M. et al. Testing plasmid stability of *Escherichia coli* using the Continuously Operated Shaken BIOreactor System. *Biotechnol. Prog.* **32**, 1418–1425 (2016).
90. Xie, L., Hall, D., Eiteman, M. A. & Altman, E. Optimization of recombinant aminolevulinic synthase production in *Escherichia coli* using factorial design. *Appl. Microbiol. Biotechnol.* **63**, 267–273 (2003).
91. Stricker, J. et al. A fast, robust and tunable synthetic gene oscillator. *Nature* **456**, 516–519 (2008).

## Acknowledgements

The authors would like to thank Drew Endy for hosting us in his laboratory and providing helpful insights and conversations, Steve Lund for helpful discussions regarding experimental design, Amar Ghodasara for helpful discussions regarding lycopene assays, Noah Spies for helpful discussions regarding data analysis, and Tobias Meyer and Arnold Hayer for assistance with osmolality measurements. The authors would like to thank the parti-

cipants and leaders of the Synthetic Biology Standards Consortium for providing inspiration for this work. Certain commercial equipment, instruments, or materials are identified in this report to specify adequately the experimental procedure. Such identification does not imply recommendation or endorsement by the National Institute of Standards and Technology, nor does it imply that the materials or equipment identified are necessarily the best available for the purpose.

## Author contributions

A.H. developed the concept, designed experiments, collected the data, analyzed the data, and wrote the paper. J.F. assisted with designing the experiments and analyzing the data. S.A.M. supervised the work, and assisted with developing the concept and designing experiments. M.S. supervised the work, and assisted with developing the concept, designing experiments, and analyzing the data. J.F., S.A.M., and M.S. edited the paper.

## Additional information

**Supplementary information** accompanies this paper at <https://doi.org/10.1038/s42003-018-0220-6>.

**Competing interests:** The authors declare no competing interests.

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