RESEARCH ARTICLE

In‑situ burning of spilled hydrocarbons using multiple pool fre numerical models

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Abstract

In-situ burning is one of the methods used for oil spill cleanup. Optimising an in-situ burning method using multiple pool fres (MPF) has not been widely studied. In this study, a novel framework is proposed to assess the efectiveness of an MPF in response to oil spills on water surfaces. The framework is applied to four cases using the Fire Dynamics Simulator (FDS). It is found that an MFP can result in incomplete combustion and negative pressure efects if pools are too close to each other, thereby resulting in a reduction in the mass burning rate. However, an MFP has a higher mass burning rate of spilled oil than a single pool fre if appropriate distances among pool fres are maintained. An MFP can increase the speed of recovering the oil compared with a single pool fre due to high temperature and heat fux.

Keywords Oil spill cleanup · In-situ burning · Multiple pool fres · MPF interaction

Introduction

An oil spill is the leakage of crude oil into an area. Several sources can cause oil spills, including accidental leakage from ofshore platforms, pipelines and tankers (Galieriková and Materna [2020\)](#page-8-0). An oil spill has severe impacts on the marine environment and ecosystem, and it is considered a type of pollution (Obida et al. [2021](#page-8-1)). The oil spill adversely afects living creatures within the ocean and pollutes the ecosystem (Galieriková and Materna [2020\)](#page-8-0). The oil spill can potentially harm public health through efects on fshing and tourism. Several accidental events (examples include the Deepwater Horizon oil spill and the Castillo de Bellver oil spill) have resulted in oil spills onto ocean surfaces and have caused severe consequences. For instance, the Deepwater Horizon oil spill contaminated surface waters, the water column, deep-sea corals and benthos, nearshore and coastal ecosystems, and natural resources across fve states in the Gulf of Mexico (GoM) (Wallace et al. [2017\)](#page-8-2). In the subsequent lawsuits, the responsible party paid \$65 billion

 \boxtimes Til Baalisampang Til.Baalisampang@utas.edu.au in compensation to people who relied on the gulf for their livelihoods.

Various physical, chemical, thermal, and biological processes are applied for oil spill remediation in the aquatic environment. The oil and gas industry has commonly used four basic ways to deal with ocean spills, namely, booms to contain the oil (Grubesic et al. [2019](#page-8-3)), skimmers to remove spilled hydrocarbons (Ndimele et al. [2018](#page-8-4)), fre to burn spilled hydrocarbons (Fingas [2017\)](#page-8-5) and chemical dispersants (Nyankson et al. [2016](#page-8-6)). The in-situ burning method for thick slick can have a removal efficiency of more than 95% (Mullin and Champ [2003](#page-8-7)). It is a two-step process. The frst step involves collecting spilled oil within a boom, and the second is the controlled burn. Diferent phenomena can occur when an in-situ burning method is used with multiple pool fres (MPF). For instance, the interaction of MPF, heat fux and oil spill cleanup conditions are not fully understood. The MPF interaction mechanisms have several explanations. It is suggested that the fame leaning varies with the burning rate of the centre and outer fre while the fre merging has several criteria: fuel type, S/D, burning rate, and flame height (Jiao et al. [2019\)](#page-8-8). S/D is the ratio of the spacing between pool fre and pool fre diameter. Air entrainment is another key component to determine heat and mass fux. The relationship between heat and mass fux and the S/D ratio is diferent under air entrainment restriction. Furthermore, Vasanth et al. ([2014b\)](#page-8-9) used Computational Fluid Dynamics

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(CFD) to study the efect of varying S/D on the combustion rate. They concluded that fame temperature, fame height, and the burning rate increase with an increase in the pool diameter of the participating pools in the MPF.

Gong et al. [\(2020](#page-8-10)) studied the relationship between pool fire length to width ratio (L/W) and the temperature distribution. The study concluded that when L/W is not larger than 6, the temperature of the pool fre's centre is very similar to that of the pool edge. Meanwhile, in the larger L/W cases (L/W \geq 8), the study claimed an attenuation of the temperature near the short pool edge. The study also recorded the longitude heat fux received by a horizontally adjacent object and concluded that the heat fux reduces with the increase in horizontal distance. Shi et al. ([2017](#page-8-11)) identifed that the aspect ratio of ullage (h) to cavity size (D) with ice cavity is related to the heat release during in-situ burning. The heat release rate increases with the aspect ratio for both quasi-steady and boilover stages. The boilover stage has a higher heat release rate than the quasisteady stage, with other factors being constant. The recirculation pattern with diferent aspect ratios causes the heat release rate variation. It was concluded that the base drag tends to increase when wind speed is low during in-situ burning, gradually increasing between 1 to 1.5 m/s, and the tendency afterwards depends on the given scenario (Kong et al. [2019b](#page-8-12)). Burning efficiency increases with initial fuel layer thickness. It slightly increases with wind speed and tends to drop at higher speeds. Kong et al. [\(2019b\)](#page-8-12) suggested that the other factors that infuence the base drag length are the density of hydrocarbons and air above oil surfaces.

Kong et al. [\(2019a\)](#page-8-13) studied in-situ burning on open water, stating that the average fame height increases with oil pool diameter in a quasi-steady stage. The burning process is separated into four stages with diferent fame heights and shapes. Only the pool centre has evaporation of the fuel and visible flame due to the significant cooling effect on the sidewall. The experiment also investigated the burning structure on open water and steel vessel and their diferences. It concluded that air recirculation mixes oil vapour into entraining air, enhancing burning and fame height. In addition, Dasgotra et al. [\(2021\)](#page-8-14) analysed the efect of water mist on multiple pool fres using the Fire Dynamics Simulator (FDS). They claimed that the efectiveness of water-mist fre suppression systems is afected mainly by operational parameters such as S/D ratio, ceiling clearance, nozzle discharge rate, and water mist particle size.

In the past, the efectiveness of an in-situ burning method has been studied considering single pool fres. There is a greater interest in understanding the prospect of using MPF for effective in-situ burning. Although in-situ burning seems to be a straightforward method to clean the spilled oil on the ocean surface, several characteristics of this approach are not thoroughly studied. Weng et al. [\(2004\)](#page-8-15) developed an empirical model to estimate the merged fame height considering the efect of separation distance in multiple fre scenarios. They

claimed that more fre sources could lead to higher fame height with the same heat release rate. Vasanth et al. [\(2014a\)](#page-8-16) reviewed MPF accidents and catalogued the controlled experiments that have been done to understand the mechanism and impact of MPFs. In the past, some of the infuencing parameters such as pool size, number of pools and distance between pools have not been extensively investigated to evaluate the efficiency of the in-situ burning method. Moreover, the interacting efect of multiple fres needs to be examined to assess the overall efficacy of using MPF in an in-situ burning method. The current study aims to investigate the characteristics and the infuencing parameters for an efective in-situ burning method. Although oil spills can occur on land, the present study focuses on hydrocarbon spills on the water surface.

"Section [2](#page-1-0)" presents the developed methodology and validation of the model. "Section [3](#page-1-1)" illustrates a case study. "Section [4](#page-1-2)" provides the results and discussion of this case study, and "Section [5](#page-2-0)" presents the conclusions of this study.

Methodology

A novel methodology has been developed to examine the efectiveness of an MPF and its interaction to clean spilled oil from an ocean surface. Each step of the methodology is illustrated in Fig. [1](#page-2-1). The study of MPFs and interactions are conducted through numerical simulation. Among the available CFD tools for fre modelling, the FDS is selected to simulate scenarios because it has been widely validated and verifed against diferent scenarios (Baalisampang et al. [2017a](#page-8-17); Lim et al. [2019](#page-8-18)). Each step of the methodology is explained in detail in the following section.

Identifcation of infuencing parameters for in‑situ burning

An in-situ burning method is one of the many solutions to handle oil spills. It is considered an efficient method to clean oil spills, including in ice-covered conditions (Ventikos et al. [2004](#page-8-19)). Currently, in-situ burning is qualifed with its burning efficiency and mass burning rate (Rojas-Alva et al. [2020](#page-8-20)). However, the goal of the present study is to provide additional indicators to accurately identify other infuencing parameters and evaluate their impacts on the in-situ burning technique. This steps identifes various infuencing parameters for in-situ burning through an extensive literature review.

Simulation of a single pool fre

The second step focuses on assessing the infuencing parameters defned in step 2.1 using the FDS. The FDS code has been employed for modelling characteristics of MPFs in several studies, such as Weng et al. (2004) (2004) and Salehi et al.

Fig. 1 Proposed methodology to investigate the MPF performance to clean spilled oil from an ocean surface

[\(2021](#page-8-21)). The vital infuencing parameters that can be considered are dimensions of pool fre, such as its diameter, oil thickness, and combustion condition (Kong et al. [2019a\)](#page-8-13). Oil thickness and diferent sources of crude oil are the examples expected to afect fre performance (Fritt-Rasmussen et al. [2012](#page-8-22)). The heat release rate (HRR), mass-loss rate, and fre temperature are the factors that can assess fre performance. This step helps to defne and evaluate infuencing parameters for MPF interaction analysis.

Evaluate infuencing parameters

Based on the single pool fre's simulation outcomes, infuencing parameters for MPF interaction analysis are evaluated. MPF interaction is the focus of the current study. The interaction mechanism varies with numerous factors. A previous study showed that the ratio between pool diameter and spacing is related to the interaction (Jiao et al. [2019](#page-8-8)). The interactions are evaluated using mass burning and heat

feedback rates in the study. MPF interaction can occur in various environmental conditions. Buist et al. ([2011\)](#page-8-23) revealed that in-situ burning could be possible at even very low temperatures such as -17 °C. However, MPF interaction is more difficult under such harsh conditions, which requires a proper evaluation of the most infuencing parameters. This step helps flter out the factors that do not cause signifcant impacts on MPF interaction.

Simulate MPF by varying each infuencing parameter

After evaluating the most infuencing parameters, several MPF scenarios are generated and simulated according to the proposed infuential factors using the FDS code. This step considers a combination of diferent parameters which aims to create outcomes for each identifed parameter.

Simulate and evaluate the efects of all infuencing parameters in in‑situ burning

The infuence of each identifed parameter is assessed while keeping other factors constant using the simulation results. In this way, the overall efects of all infuencing parameters are evaluated, and correlations can be developed for an efective in-situ burning technique.

Validation

The numerical model is validated with a large-scale pool fre experiment conducted by Sjöström et al. [\(2015\)](#page-8-24). The study

Fig. 2 Experiment setup where sensors are placed in four directions at 0, 5 and 10 m from the pool edge

stated that the total HRR is 488 ± 24 MW. The fire temperatures are recorded at set distances from the fre's edge in four directions using thermocouples. Thermocouples are placed at 0, 5, and 10 m from the pool edge in each direction, as shown in Fig. [2.](#page-2-2) The simulation setup has maximum width and length of 50 m. The maximum distance between the pool fre edge is 17.5 m by keeping the fre at the centre. The circle is the pool fre with a radius of 9 m. The simulation duration is 2000 s. The simulation setup was precisely matched with all the experiment parameters to increase the accuracy.

Temperatures recorded by thermocouples are compared with experimental results, as shown in Fig. [3](#page-3-0). The results from the simulation showed that there is a slight diference between the experiment and the simulation. The maximum percentage diference is 7.6% which is within an acceptable range.

Case study

The proposed methodology is applied to generic case studies. A key component of the simulation is the water surface. Thus, the thermal properties of seawater are considered. The seawater surface with a 1-m depth is applied to the simulation to incorporate the efects of oil–water interfaces. The pool fre is afected by the characteristics of seawater, including the specifc heat of seawater, the emissivity, and the heat of vaporisation. The specifc heat is considered as 3.85 kJ. kgK, and the emissivity is used as 0.9 (Sharqawy [2013](#page-8-25); Sudhamshu et al. [2016](#page-8-26)). Another factor for seawater is the heat of vaporisation, which is selected as 2300 kJ/kg (Sharqawy et al. [2010](#page-8-27)). In an in-situ burning method, fre-resistant fabric booms and steel freproof booms are used to contain the fre (Buist et al. [1999\)](#page-8-28). Though prevailing waves and harsh environmental conditions afect the dynamics of the oil–water interfaces, fxed pool positions are considered in this study.

In the simulation, the geometry dimension is 50 m \times 50 m \times 20 m. However, the simulation domain is

Table 1 Comparison among four cases

considered 100 m \times 100 m \times 40 m for accurate results. The circular pool fre with a diameter of 10 m is considered. It is possible to increase the fre size to 20 m or more to simulate the oil spill (Fritz [2003\)](#page-8-29). All the faces are kept open except the sea surface. The z-min is the bottom face that is the sea surface. The HRR of the fire is selected as 1000 kW/m^2 . The ambient temperature is set as 20 °C with zero wind speed. It is assumed that the fres are under open area conditions, and there is no other obstruction. When the water content of the oil is higher than 25%, most of the oil slick is incombustible. The usual method is to use a towed freproof fence to capture the leaked crude oil and concentrate it to form a stable pool with a considerable thickness to resist harshness. This study considers MPF models for multiple pools on the surface of offshore water only.

Cases

Four cases are considered by varying number of pools, size and S/D and the variables are shown in Table [1.](#page-3-1) In case 1, three identical pool fres are considered with S/D 1. In case 2, the distances between pools are reduced, keeping everything the same. The size of the fre can infuence the characteristics of the fre interaction. Thus, fve diferent

Fig. 4 Positions of the thermocouples to record the net temperature

pool sizes are considered in case 4. In case 3, the pool size and S/D are changed.

In case 4, the number of fres varies in each simulation, starting with 1 to 3 fres. The case aims to compare the efectiveness of a standalone pool fre and an MPF based on the temperature recorded at the fxed location, as shown in Fig. [4](#page-3-2). The spacing between sensors and fre is 5 m for all three simulations.

Mesh independence analysis

CFD results depend on mesh sizes, and thus, a mesh independence analysis needs to be conducted for accurate results (Baalisampang et al. [2017b](#page-8-30)). The mesh independence analysis is performed using three mesh sizes based on the maximum temperature recorded by thermocouples. Three thermocouples (THCP05-07) are placed at the centre of the fres, and three thermocouples are located between two fres (THCP02-04), as shown in Fig. [4.](#page-3-2) A thermocouple (THCP01) is placed at the centre of all three fres to record the thermal performance and interactions. An extra thermocouple is placed at the height of 19 m vertically above the THCP01 to measure the net temperature of the merging fames. The positions of thermocouples and the three pools are given in Table [2.](#page-4-0)

Three mesh numbers considered for the mesh independent analysis are 400,000, 1,350,000 and 4,556,250. The overall accuracy improvement is less than 3%, with the expense of 10 times more simulation time. The slight diference in the result indicates that the 400,000 mesh number model has sufficient accuracy for the study. Hence, the further increase in mesh number is not cost-efective.

Results and discussion

The results obtained from each case are used to compare the efects of the interaction of fres which are discussed in the following section.

Comparison between case 1 and case 2

In case 2, distances between pools are greater than those of case 1. To identify the interaction of fres, air velocity is used as an indicator based on the drag direction of the fre. Figure [5](#page-4-1) shows the horizontal velocity of air. The magnitudes of velocity in the two cases are diferent. The horizontal velocity in case 1 is higher than in case 2. It is observed that the fames of the two fres tend to gather in the middle. The inclination is signifcant in case 1 because of the lower air density between the fres. The air velocity distribution indicates that fres drag at a higher velocity when pools are closer to each other. The increase in horizontal velocity proves the increase of fre interaction caused by reducing the spacing between fres. The spacing between fre is a signifcant factor to infuence fre interaction.

Fig. 5 Pool fres with air velocity in the horizontal direction. (**a**) case 1 and (**b**) case 2

Fig. 6 Comparison of temperature stability for case 1 and case 2

Temperature in each fre

Figure [6](#page-5-0) demonstrates the temperature of three pool fires. The average temperature of the three fre pools in case 1 is 2260 ℃ and 2324 ℃ in case 2. However, the temperatures in case 1 are relatively less stable than in case 2. The potential reason for less stable temperature in case 1 is that the interaction of fre is relatively strong. Therefore, the temperature variation in case 1 is more prominent than in case 2.

Temperatures between two fres

Figure [7](#page-5-1) shows the temperatures recorded by thermocouples which are placed between two pool fres. THCP01 is located at the centre of three fres. Temperatures in case 2 are lower than those of case 1. The reduction of distance between fres has increased the fre interaction, which resulted in increased temperature.

Net temperature after merging into one fame

For an illustrative purpose, the temperature at the height of 19 m from the middle of three fres is recorded to investigate the net temperature of merging fres. However, the temperature can be compared at any height after a merging point. The temperature range for case 2 is 100 to 140 °C, while the temperature for case 1 is up to 240 $^{\circ}$ C, as shown in Fig. [8.](#page-6-0) The temperature can refect the interaction among these fres. In case 2, the combined temperature is much lower than in case 1 because of longer distances among fres, and fames do not wholly merge. The higher temperature in case 1 implied that fres joined at a lower height with increased interaction.

Fig. 7 Temperatures recorded at the equidistance from fres

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Analysis of the impact of pool fre size on thermal performance (case 3)

Five simulations of diferent fre sizes are considered. All three fre sizes are identical in each simulation. Thermocouples 05, 06 and 07 are placed at the centre of fres, and five extra thermocouples are placed between the fires, as shown in Fig. [9.](#page-6-1) The distances between thermocouples and fre edges are kept constant in each simulation. The purpose of THCP01 to THCP04 is to observe the fre interaction impacts on thermal performance and the corresponding effects caused by fire size.

Two infuencing factors are used for this analysis. The frst one is the spacing between fres directly related to the interaction. Another factor is the size of the pool fre. The fre size reduction can provide high S/D with equal spacing between fre edges. Therefore, S/D is adjusted by changing the fre size. The temperature of all three fres has reduced with the increase in pool diameters from 2.5 to 7.5 m, as illustrated in Fig. [10.](#page-7-0) The decrease in temperature has indicated the incomplete combustion of the fres. Hence, the interaction has caused insufficient airflow for complete combustion, reducing the temperature of fres. However, the reduction in the S/D has enhanced the fre interaction. In the current study, it is observed that when the diameter of pools is greater than 7.5 m, there is no linear relationship between temperature and pool diameter, as shown in Fig. [10](#page-7-0).

The temperatures at the central location from the two fres are recorded. The temperatures recorded by THCP01 to THCP04 are similar since the temperature is obtained on the water surface. The temperature decreases gradually from the diameter of 2.5 to 7.5 m, as shown in Fig. [11.](#page-7-1) The increase in

Fig. 9 The distances between thermocouples THCP01-04 and pool edge remain unchanged to 2.5 m. THCP (at 19 m height) and THCP01 are the same in all simulations since they are the central point of each simulation

Fig. 10 The temperature at the centre of the fres with diferent pool diameters

Fig. 11 Temperatures at mid-distance from two fres including at 19 m height

Fig. 12 Impacts of the number of fres on net temperature. The results show that multiple pool fres can increase the speed of cleaning oil spills

fre interaction has created negative pressure that drags heat towards the space between fres, increasing their temperature. The negative pressure effects had a larger thermal impact than incomplete combustion when the diameters were 2.5 to 7.5 m. Hence, a slight increase in temperature is obtained. However, the temperature reduces when the diameters are greater than 7.5 to 10 m. It confrms that the mass-loss rate increases at a certain S/D ratio, which decreases after that (Ji et al. [2016](#page-8-31)). For the diameters 10 to 12.5 m, both incomplete combustion and negative pressure efects contribute to the thermal impacts. There is only a slight temperature variation when the pool diameter is between 10 to 12.5 m.

Impacts of number of fres in thermal performance (case 4)

Temperatures recorded at 5 m away from the pool boundary are compared considering 1, 2, and 3 fres, as shown in Fig. [12.](#page-7-2) This indicates that the average temperature increases with an increase in the number of fres. It is found that the increase rates are 4.7% and 12.06% for two fres and three fres, respectively, compared with a single fre. It demonstrates that the speed of oil spill cleanup can be improved using multiple pool fres during in-situ burning.

Conclusions

In-situ burning is an efficient method for cleaning oil spills from water surfaces. A novel framework has been proposed to evaluate the efficacy of a multiple pool fire (MPF) in optimising the oil spill cleaning process. The temperature from an MPF is used to assess the efects on the burning rate of the spilled oil. The Fire Dynamics Simulator (FDS) software is used in the current study considering 4 cases. The numerical model was validated, which shows a good agreement with the experimental result. Case 1 and case 2 assessed the impact of changes in distance between pool fres. The fre interaction increases with smaller pool spacing. The temperatures recorded by the thermocouple kept at the centre of all pools provided evidence of stronger pool fre interaction.

Case 3 investigated the thermal performance of diferent pool fre sizes with the same spacing between fre edges. The temperature at the centre of the fre indicated the pool fre has incomplete combustion, leading to a reduction in temperature for fre with diameters 2.5 to 10 m. However, the temperature increases when the fre diameter is further increased. The temperature recorded between fres is also not linearly related to fre diameter and the ratio of the spacing between fres to fre diameter (S/D). The temperature of pool fre initially increased between 2.5 to 7.5 m but reduced when the diameter was 7.5 to 10 m. There are no significant changes in temperature for the fre with diameters of 10 to

12.5 m. The major infuencing factors are the negative pressure effect and incomplete combustion.

In case 4, the effectiveness of a single pool fire and multiple pool fre in cleaning up oil spills is investigated. It is found that the net temperature at the middle point of pools increases with the increase in the number of fres. The total mass burning rate was higher in an MPF than that of a single pool fre. Thus, the MPF can improve the overall mass burning rate and speed up the oil spill cleaning process. Consideration of the efects of actual ocean conditions such as wave motion and oil slick thickness in the current framework can be the future direction of the study.

Availability of data and material (data transparency) The simulation data is available upon request.

Code availability Not applicable as no datasets were generated or analysed during the current study.

Declarations

Conflicts of interest The authors declare that they have no competing interests.

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