



# Towards High Value-Added Recycling of Spent Lithium-Ion Batteries for Catalysis Application

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Received: 10 June 2023 / Revised: 31 December 2023 / Accepted: 20 March 2024  
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## Abstract

With the proposal of the global carbon neutrality target, lithium-ion batteries (LIBs) are bound to set off the next wave of applications in portable electronic devices, electric vehicles, and energy-storage grids due to their unique merits. However, the growing LIB market poses a severe challenge for waste management during LIB recycling after end-of-life, which could cause serious environmental pollution and resource waste without proper treatment. Pyrometallurgical, hydrometallurgical, and direct recycling of spent LIBs have been developed, guided by the “waste to wealth” principle, and were applied to LIB remanufacturing. However, some spent LIB materials with low values or great direct regeneration difficulties may not be suitable for the above options, necessitating expanded application ranges of spent LIBs. Considering their unique compositions, using waste electrode materials directly or as precursors to prepare advanced catalysts has been proposed as another promising disposal technology for end-of-life LIBs. For example, transition metal elements in the cathode, like Ni, Co, Mn, and Fe, have been identified as catalytic active centers, and graphite anodes can serve as the catalyst loading matrix. This scheme has been adopted in various catalysis applications, and preliminary progress has been made. Therefore, this review summarizes and discusses the application of spent LIB recycling materials in catalysis and classified it into three aspects: environmental remediation, substance conversion, and battery-related catalysis. Moreover, the existing challenges and possible foci of future research on spent LIB recycling are also discussed. This review is anticipated to mark the start of close attention to the high-value-added applications of spent LIB products, enhancing economic efficiency and sustainable development.

**Keywords** Spent lithium-ion batteries · Recycling · Catalyst · Environmental remediation · Substance conversion · Battery-related catalysis

## 1 Introduction

The past two decades have witnessed the wide applications of lithium-ion batteries (LIBs) in portable electronic devices, energy-storage grids, and electric vehicles (EVs) due to their unique advantages, such as high energy density, superior

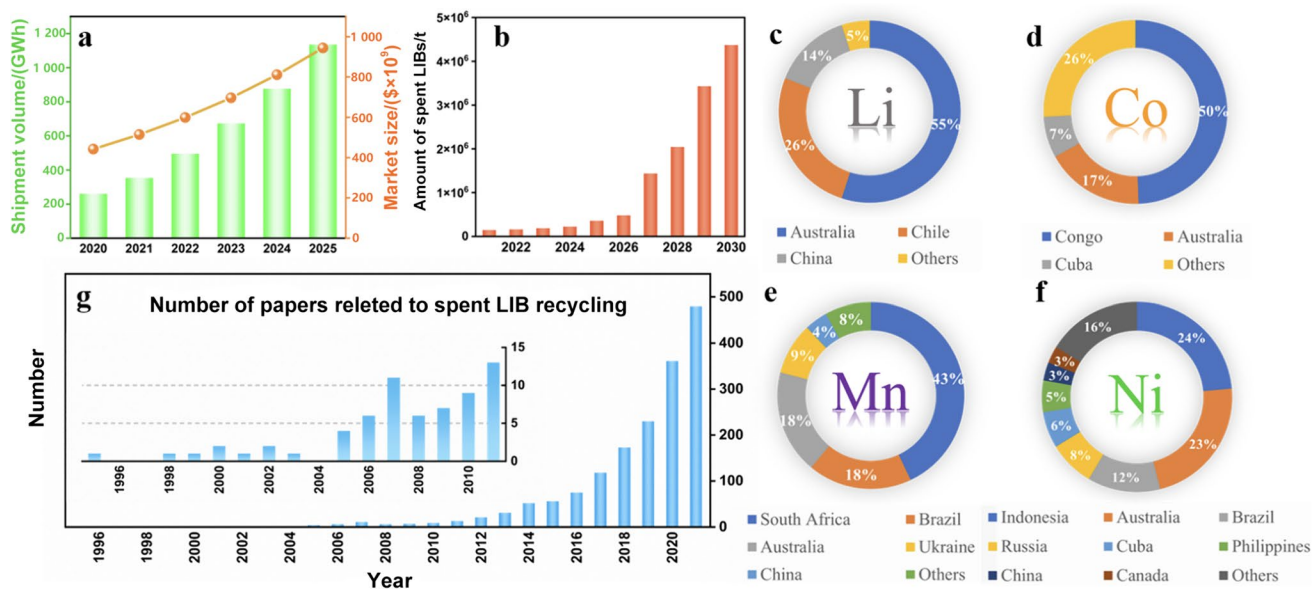
cycling durability, and low self-discharge [1–3]. As shown in Fig. 1a, the global LIB shipment volume and market size are growing rapidly and are expected to reach 1 135.4 GWh and 99.4 billion dollars in 2025 [4], respectively. LIBs comprise the cathode, anode, electrolyte, and separator, and lithium ions migrate back and forth between the cathode and anode for energy storage and release [5, 6]. The cathode materials [e.g.,  $\text{LiCoO}_2$  (LCO),  $\text{LiMn}_2\text{O}_4$ ,  $\text{LiFePO}_4$  (LFP), and  $\text{LiNi}_x\text{Co}_y\text{Mn}_z\text{O}_2$ ] often undergo irreversible phase transitions after excessive charging/discharging cycles [7–9], and the interlayer structures of the anode materials (e.g., graphite) collapse [10], which are the main causes of battery capacity decay. Consequently, the average LIB lifespan is limited to 5 to 8 years due to the intrinsic structural barriers of electrode materials. With the accelerated updating and upgrading of electronic products, a lot of LIBs are discarded before reaching their maximum service life. Therefore, tens of millions

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**Fig. 1** **a** The global LIB shipment volume and market size from 2020 to 2025 [4], respectively. **b** Forecasts of the amounts of end-of-life LIBs generated in the near future [11]. **c–f** Geographical distribu-

tion of lithium, cobalt, manganese, and nickel in the earth's crust, respectively. **g** The number of papers related to spent LIB recycling (obtained from Web of Science)

of tons of spent LIBs are expected in the next 3 to 7 years, and a cumulative 12 million tons of end-of-life LIBs from EVs are expected by 2030 (Fig. 1b) [11]. The proper disposal of these spent LIBs poses a huge challenge but also presents some opportunities. To date, most spent LIBs end up in incineration furnaces or landfills like conventional waste due to the lack of relevant standards, sufficient economic efficiency, and efficient collection and recycling channels [12–14]. Their crude incineration emits  $\text{CO}_2$  and toxic gases, exacerbating the greenhouse effect and atmospheric contamination, while their landfills leak hazardous fluorine, organic pollutants, and heavy metals, which seriously pollute soil and groundwater [15–18]. Therefore, effective recycling technologies are urgently needed for spent LIBs.

The necessary mineral resources for LIB productions, including lithium, cobalt, nickel, and manganese ores, have uneven geographical distributions and are mainly found in a few countries (Fig. 1c–f) [19, 20]. According to statistics, the global LIB market has already consumed 40% and 25% of all lithium and cobalt mining capacities, respectively [21]. Considering that the contents of many high-value metal elements, such as cobalt, lithium, copper, manganese, and nickel, in spent LIBs are higher than the corresponding natural ores, spent LIBs are regarded as mines for exploitation. Therefore, developing advanced technologies for recovering, recycling, or reusing these high-value components can mitigate resource constraints and eliminate environmental pollution while generating economic benefits [22]. However, the economic feasibility of spent LIB recycling poses a key challenge restricting its further large-scale development.

Specifically, spent LIB recycling is a complex systematic project hindered by inadequate recycling facilities and technologies [23, 24]. At present, the recycling work is mainly driven by legislative obligations, with less consideration of economic returns. Thus, developing efficient, inexpensive, and environmentally friendly spent LIB recycling methods and scaling them up is crucial in future research.

Basic academic research has always been the cornerstone of industrial applications. Based on the “waste to wealth” concept, research on spent LIB recycling has increased exponentially from 2010 to 2021. According to the scientometric analysis based on the Web of Science core database, the number of relevant studies is shown in Fig. 1g. Besides recycling, spent LIBs can be utilized through remanufacturing and repurposing. Remanufacturing and repurposing are the most economically feasible disposal methods, which also extend the utilization of spent LIBs. Theoretically, the value of spent LIBs can be maximized through remanufacturing or repurposing, followed by recycling [25]. For example, spent LIBs from EVs can be repurposed for energy storage stations, electric tricycles, and communication base stations as they retain 80% of their initial energy or power density. Spent LIBs that cannot achieve echelon utilization can be recycled for raw materials. Researchers have proposed some simple and economical regeneration methods to repair the structure and composition of spent electrode materials [26–30]. Conventional pyrometallurgy, hydrometallurgy, bio-metallurgy, or their combinations for the sustainable development of LIBs have received more attention, and many reviews have summarized these spent

LIB recycling processes and closed-loop re-fabrication of electrode materials [31–34]. The direct regeneration method, i.e., using repaired spent LIB materials for new batteries, simplifies the recycling procedure and minimizes energy inputs, thus considered a more promising approach [35–38].

Despite the numerous spent LIB recycling strategies, many obstacles hinder their large-scale application or sustainable development. Owing to the mature technology, some pyrometallurgy and hydrometallurgy methods have achieved commercialization. However, as their profit model relies on valuable metals or their derivatives, such methods are only suitable for cathode materials with valuable metals (e.g.,  $\text{LiCoO}_2$  and  $\text{LiNi}_x\text{Co}_y\text{Mn}_z\text{O}_2$ ). In addition, the Co content in LIBs gradually decreases with the development of advanced LIB technologies. That is, “high-Ni and low-Co” LIBs are gradually replacing existing commercialized LIBs, thus reducing the profit margins of pyrometallurgy and hydrometallurgy methods that motivate their sustainable development, as Co products are their main source of profit. Meanwhile, previously reported direct regeneration methods are only suitable for regenerating one single component of spent LIB materials, while cathode materials of different components, even of the same type (e.g.,  $\text{LiNi}_{0.5}\text{Co}_{0.2}\text{Mn}_{0.3}\text{O}_2$  and  $\text{LiNi}_{0.6}\text{Co}_{0.2}\text{Mn}_{0.2}\text{O}_2$ ) are not able to be regenerated with the same process. In addition, the cost-effective regeneration strategies for the relatively low-value graphite, the main material for commercial LIB anode, are comparatively lacking. Therefore, it is necessary to explore new research directions for spent LIB recycling and expand the application of spent LIB recycling products.

The main components of LIB cathode, like Ni, Co, Mn, and Fe, are common in various catalysts. Meanwhile, the crystal structure of the degraded electrode materials is not completely destructed, which has potential catalytic activities, and the vacancies or other defects in spent LIB electrode materials may also promote the catalytic kinetics. Considering these intrinsic characteristics of spent LIB electrode materials, it is promising to convert spent LIBs into catalysts, and researchers have explored the application of spent LIB recycling products in catalysis, including pollutant degradation [39], photocatalysis [40, 41], electrocatalysis [42, 43], and high-value graphene [44, 45]. Although these alternative applications of recycled spent LIB materials present novel concepts for LIB recycling, few summaries or assessments have been conducted. Thus, a comprehensive review is crucial to guiding the benign development of this field.

This review focuses on the up-to-date research progress in catalysis-related applications of spent LIB recycling products, and the review outline is illustrated in Fig. 2. First, spent LIB pretreatments, including discharging, dismantling, and separation, are discussed and summarized in Sect. 2. Second, the feasibility of using spent LIB recycling

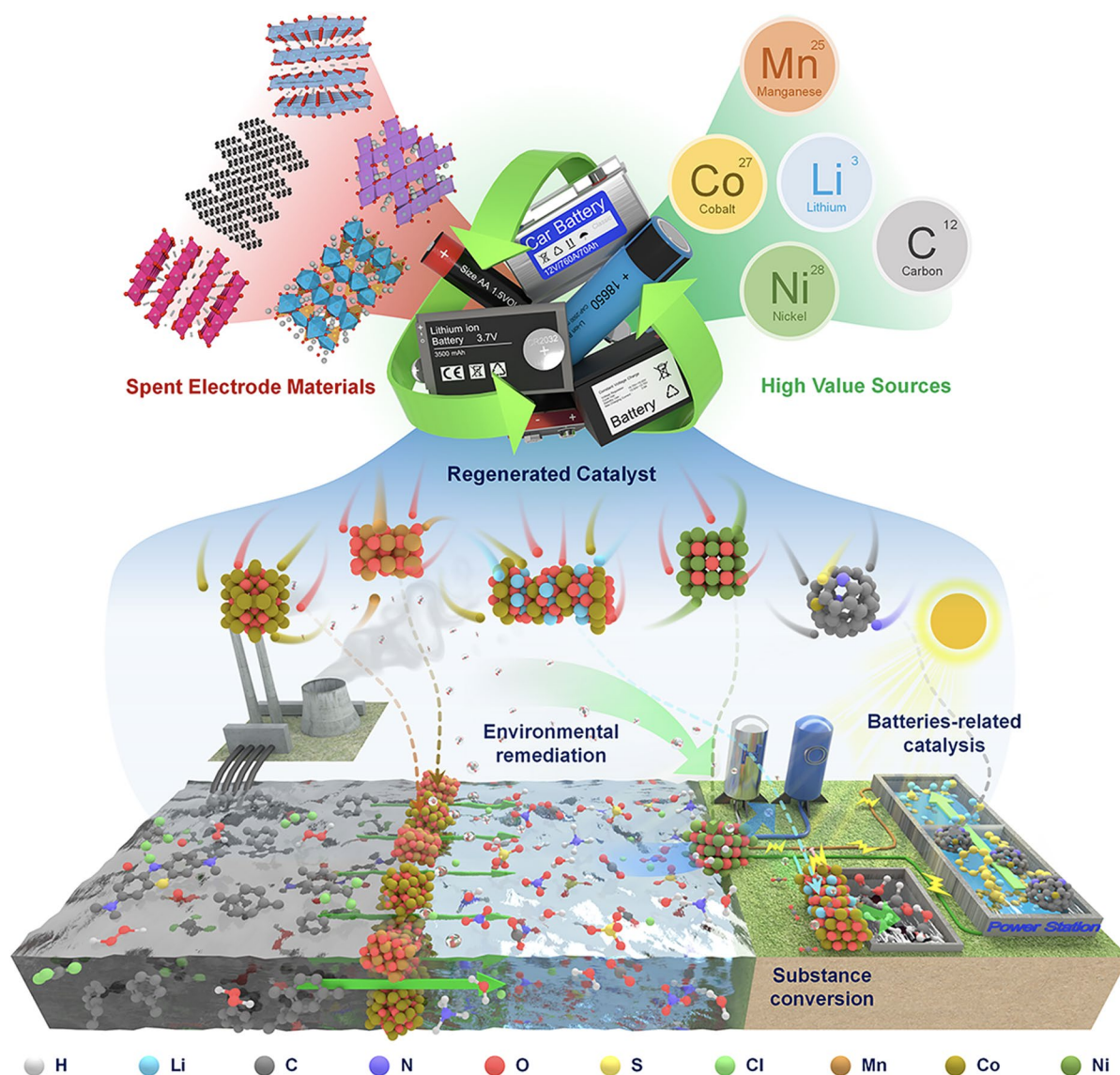
materials as catalysts is discussed in Sect. 3. In addition, the specific research progress of spent LIB recycling materials in catalysis is summarized in Sects. 4, 5, and 6, including environmental remediation [degrading pollutants from wastewater and removing volatile organic compounds (VOCs)], substance conversion (biomass, synthesis gas, and electrocatalytic water decomposition), and battery-related catalysis [metal-air batteries, fuel cells, and lithium-sulfur batteries (LSBs)], respectively. As a reminder to the involved researchers, limitations on spent LIB recycling materials for catalytic applications are analyzed in Sect. 7. Moreover, the future challenges and opportunities for LIB recycling are considered from our perspective in Sect. 8, aiming to provide a reference for related research.

## 2 Before Converting Spent LIB Materials into Catalysts

Pretreatment is vital before recycling spent LIB components, including anode materials, cathode materials, current collector, diaphragm, etc. Effective pretreatments improve recovery efficiency and reduce energy consumption for subsequent steps [24, 46, 47]. According to previous experience, the pretreatment of spent LIBs mainly involves discharge, disassembly, and separation [47, 48].

The residual electricity in spent LIBs could trigger thermal runaway and cause irreparable disaster during recycling [49]. To ensure recycling safety, discharging spent LIBs is usually the first process of pretreatments, which includes physical and chemical methods. Physical discharge relies on external load circuits to consume the remaining electricity through heat release. However, this method is only suitable for discharging a few batteries and mainly applies to lead-acid batteries instead of LIBs. Chemical discharge is the most applied way to discharge spent LIBs by immersing batteries in aqueous solutions (e.g.,  $\text{NaCl}$  and  $\text{Na}_2\text{SO}_4$ ) to release the remnant energy. Relevant results showed that spent LIBs could be safely disassembled when their voltage was below 1.5 V [state of charge (SOC) < 5%] [50]. However, high-efficiency discharge solutions usually severely corrode the battery shell, inducing safety accidents. Researchers have focused on mitigating or avoiding battery corrosion during discharging. For example, Fang et al. found that compared with other solutions, the zinc acetate solution can alleviate battery corrosion during discharging [49]. Wu et al. found that battery corrosion in electrolyte solutions can be solved using graphite electrodes instead of the battery tab for discharge [50].

At present, spent LIBs are often dismantled manually, lacking mature automatic disassembly methods [12]. Since some components of Li-ion cells react with  $\text{O}_2$  and  $\text{H}_2\text{O}$ , a



**Fig. 2** The conceptual graph of spent LIB electrode materials applied in catalysis

glove box filled with highly pure Ar atmosphere containing  $\text{H}_2\text{O}$  and  $\text{O}_2$  only in the lower parts per million range has to be utilized. Although discharging usually precedes battery disassembly, care must be taken to prevent internal circuit shorting during cell opening due to residual electricity. Therefore, an ideal cutting position has to be determined for each cell type through non-destructive techniques [e.g., X-ray analysis, X-ray computed tomography (CT), and neutron tomography] before opening spent Li-ion cells, and non-conductive tools are recommended [51]. Furthermore, it is reported that cryogenic treatment (e.g., liquid nitrogen) may reduce the risk during dismantling [52, 53].

After dismantling, effective separation of spent LIBs is essential for the subsequent precise recycling. Depending on the different physical properties (e.g., particle size,

density, weight, and magnetism) of various components (e.g., cathode, anode, current collector, and diaphragm), various physical separation methods (e.g., crushing, sifting, and magnetic separation) can be utilized, and the electrolyte can be recovered if its content is sufficiently high [51, 54]. However, most studies neglect electrolyte recovery, which can be removed by heating, organic solvent washing, or supercritical  $\text{CO}_2$  extraction [24, 25, 47].

Through appropriate discharging, dismantling, and separation, the different components of spent LIBs can be separated for subsequent precise recycling. For now, however, most of these steps are conducted manually or by human-robot co-working [12], which limits the recycling scale. Thus, innovative automatic pretreatment methods are needed for the industrialization application of spent LIB recycling.

In addition, some steps in the recycling process may involve the use of specific reagents, such as in hydrometallurgy, the use of acids and precipitants may introduce unwanted elements into the recovery products. Meanwhile, organic residues on the surface of spent LIB electrode materials, such as polyvinylidene fluoride (PVDF), are difficult to be removed completely. Some crude methods, such as calcination at high temperatures, can effectively remove these organic residues. However, this process destroys the original structure of the desired materials. Therefore, maintaining purity and avoiding new impurities are still important issues to consider. Some possible research directions are suggested as follows. First, acids with miscellaneous elements should be avoided when leaching elements, while acids containing only C, H, and O are recommended (e.g., citric acid). In terms of strategies not considering retaining the original structure of the raw materials for the desired products, the effect of high-temperature calcination pre-treatment is currently better than that of reagent pre-treatment in removing impurities. However, powerful decontamination reagents are still required, as the waste gas treatment of high-temperature calcination remains a problem, and the reagent reaction is relatively mild and easy to control. Finally, turning the impurities into treasures through clever design is also a research direction worth considering, which avoids the difficulty of removing such impurities but effectively utilizes these substances, thus eliminating the steps of subsequent treatment for them. For example, impurities like residual binder (e.g., PVDF) may serve as carbon sources to improve the electronic conductivity of the produced catalysts. Additionally, the accumulated transition metal elements on the graphite after excessive charging/discharging cycles may be exploited through appropriate designs to modify the product performance.

### 3 The Feasibility Analysis of Spent LIBs for Catalysts

Inappropriate disposal and recycling of the spent LIBs can lead to environmental degradation and severe resource waste as they contain heavy metals (e.g., cobalt, manganese, and nickel) and toxic organic electrolytes. Currently, the common idea is to regenerate LIB electrode materials from spent LIBs after disassembly and acid or high-temperature treatment for reutilization in producing new batteries [47, 55, 56]. However, traditional pyrometallurgy and hydrometallurgy methods consume extensive energy and inorganic/organic acids, making them expensive with complex follow-up procedures [57–59]. Meanwhile, regeneration does not apply to all commercial electrode materials due to their different market values. For instance, the economic benefits of recycling cheap  $\text{LiFePO}_4$  for electrode material are low.

In addition to LIB remanufacturing, recycling and reusing spent LIBs for producing other advanced functional materials, such as catalysts, has attracted increasing attention. Spent LIBs with unique components (graphite anode and  $\text{LiCoO}_2$ ,  $\text{LiMn}_2\text{O}_4$ ,  $\text{LiFePO}_4$ , and  $\text{LiNi}_x\text{Co}_y\text{Mn}_z\text{O}_2$  cathodes) contain large amounts of valuable metals, such as lithium, iron, nickel, cobalt, manganese, copper, aluminum, and high value-added carbon materials. These residual components in the spent electrode materials could serve as core elements of functional catalysts, which has exhibited promising application aspects in catalysis. Appropriate recycling and reprocessing methods can be adopted to prepare corresponding metal compounds (e.g., oxides, sulfides, phosphides, and oxyhydroxides), multi-element alloys, carbon-based composites, and  $\text{g-C}_3\text{N}_4$  materials, which are common catalysts in advanced oxidation, electrocatalysis, photocatalysis, and molecular catalysis [60–63].

The specific feasibility of converting spent LIB electrode materials into advanced catalysts for environmental remediation-related catalysis, battery-related catalysis, and substance conversion catalysis are as follows. (1) Water and air pollution, especially the organic pollutants harmful to human health, are serious issues faced by environmental remediation. Using the spent  $\text{LiFePO}_4$  with rich Fe resources or other spent electrode materials to synthesize ferrite-type materials like Fenton or Fenton-like reagents for wastewater treatment has become a possible promising solution, which can catalyze the oxidation of organic compounds into small molecular substances. Replacing noble metal catalysts with transition metal-based catalysts for VOC oxidation is becoming a mainstream research direction in tackling air pollution. Using spent LIB electrode materials with rich transition metal resources to synthesize corresponding oxides (e.g.,  $\text{CoO}_x$  and  $\text{MnO}_x$ ) usually exhibits superior catalytic performance. (2) Substance conversion catalysis, including water splitting with oxygen evolution reaction/hydrogen evolution reaction, electrocatalytic carbon dioxide reduction, and biomass conversion, must overcome the high reaction energy barrier and thus consume large amounts of energy. Therefore, developing advanced catalysts is critical. Noble metal catalysts have shown excellent catalytic performance in substance conversion. However, the high prices and limited reserves of noble metals prevent their further large-scale application. Developing low-cost, non-precious metal-based catalysts to reduce the reaction energy barrier and enhance reaction efficiency is a prerequisite for further development in this field. Transition metal compounds have proven excellent catalytic properties comparable to noble metal catalysts by rational structural design and controlled synthesis process. Thus, developing advanced recycling technologies to transform spent LIB materials into efficient catalysts can effectively utilize a large number of LIB wastes and boost the development of advanced catalysts, demonstrating

superior economic values and promising applications. (3) Different from those of traditional “rocking-chair” batteries, LSBs, metal-air batteries, and fuel cells are closely related to catalytic reactions, while carbon-based material and transition metal compounds are promising catalysts for these types of batteries. Spent LIB electrode materials with various transition metals and graphite closely related to the above catalyst materials of transition metal and carbon-based material compounds can be used to prepare battery-related catalysts by rational design and controllable synthesis. Meanwhile, as commercial cathode materials with unique crystal structures have potential catalytic activity, spent cathodes with volume changes, defect sites, and strains might promote electro-catalytic kinetics.

## 4 Environmental Remediation Related Catalysis

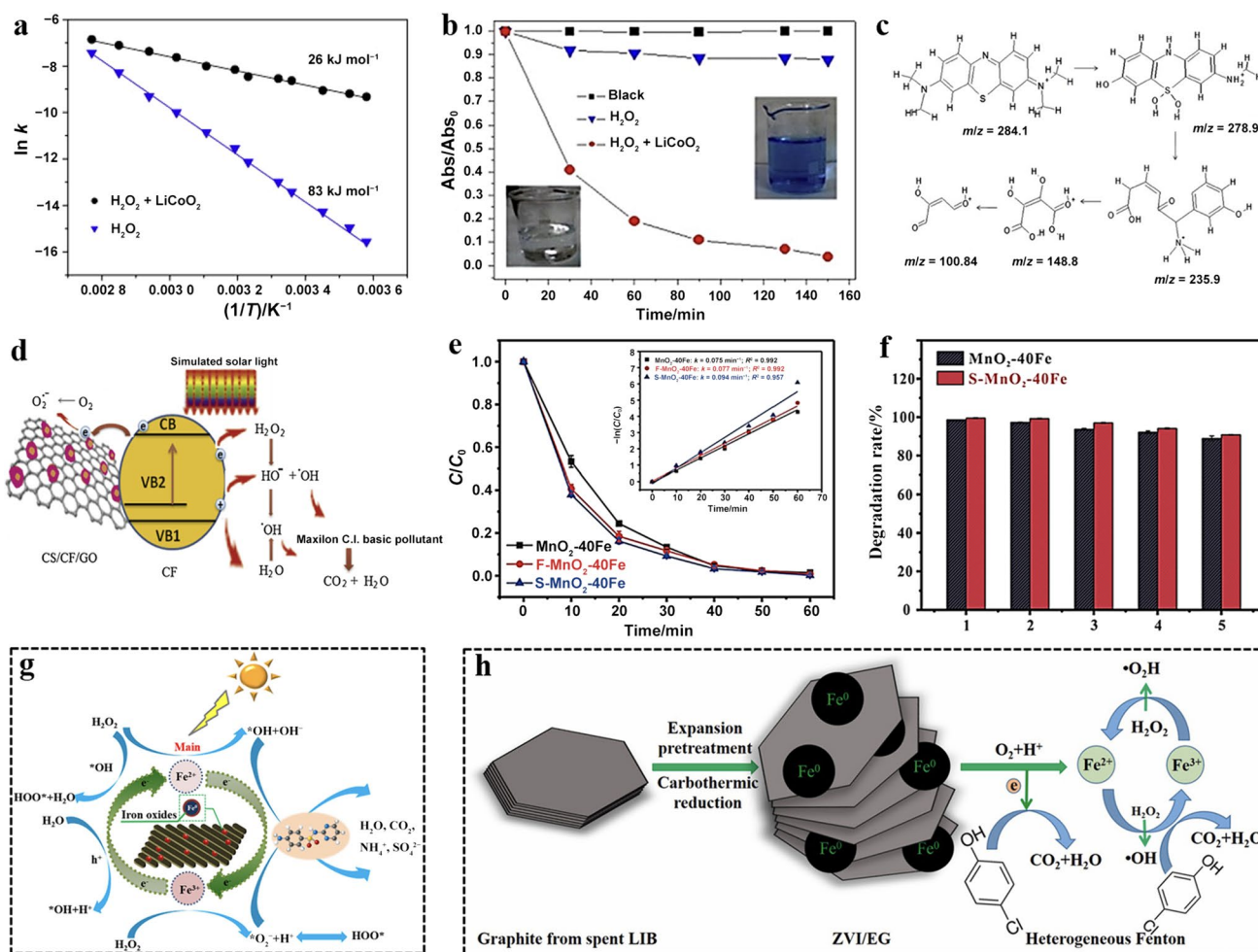
Environmental problems, especially water and air pollution, have become serious issues globally. Most organic pollutants (synthetics, plastics, pesticides, dyes, etc.) are difficult to be degraded naturally and can penetrate into crops through contaminated air, water, and soil, ultimately causing carcinogenic and teratogenic damage to humans and other organisms [64, 65]. Degrading the organic pollutants in sewage and air has aroused great attention. It is imperative to develop effective methods for removing these pollutants from the environment. Using appropriate catalysts to accelerate the degradation of these pollutants is considered as one of the most promising and practical way. In the meantime, spent LIB recycling is an important topic for environmental protection [66], while the abundant resources in spent LIBs, such as graphite and metal elements, are expected to serve as ideal catalyst raw materials. The “waste to wealth” concept has always been at the forefront of green chemistry research. Therefore, using spent LIBs as raw materials to prepare advanced catalysts for organic matter degradation in polluted water and air fulfills two purposes with one action. Existing studies have proved the feasibility and bright prospect of this approach, and the research progress is summarized and discussed, hoping to inspire follow-up research.

### 4.1 Application in Wastewater Treatment

Advanced oxidation is a classical chemical oxidation method, mainly including Fenton and Fenton-like methods, ultrasonic oxidation, ozone oxidation, photocatalytic oxidation, wet oxidation, wet catalytic oxidation, persulfate advanced oxidation, supercritical water oxidation, and other oxidation technologies, which can degrade organic compounds into small molecular substances through chemical reaction and further mineralize them into  $\text{CO}_2$  and  $\text{H}_2\text{O}$

[67–69]. With high efficiency, strong operability, wide adaptability, and less secondary pollution, advanced oxidation is considered promising for wastewater treatment [70, 71]. In 1894, Fenton discovered that organics can be rapidly oxidized in a mixed solution of  $\text{Fe}^{2+}$  and  $\text{H}_2\text{O}_2$  [72], i.e., the standard Fenton reagent, which has been widely studied and applied. The superior oxidizing property of this mixed system can be attributed to the presence of  $\text{Fe}^{2+}$ , which can promote the decomposition of  $\text{H}_2\text{O}_2$  to produce  $\text{HO}\cdot$  with strong oxidation capacity [73]. To further improve the organics removal effect based on the standard Fenton reagent, researchers developed various Fenton-like reagents with similar mechanisms by changing and coupling reaction conditions and improving reaction mechanisms, such as modified Fenton reagent, optical Fenton reagent, electric Fenton reagent, and ligand Fenton reagent [74].

Due to their intrinsic catalytic properties, some LIB materials could act directly as catalysts for specific reactions. In 2015, Goncalves et al. [75] proposed the degradation of methylene blue (MB) using spent LIB cathodes and the corresponding catalyst components containing  $\text{LiCoO}_2$  (83% by weight), carbon (14.5% by weight) and others ( $\text{Al}$ ,  $\text{Al}_2\text{O}_3$  and  $\text{Co}_3\text{O}_4$ , 2.5% by weight) obtained by heat treatment to remove organic solvents. The activation energy ( $E_a$ ) values derived from the angular coefficient of the  $\ln k$  vs.  $1/T$  plot for MB degradation are  $83 \text{ kJ mol}^{-1}$  and  $26 \text{ kJ mol}^{-1}$  with pure  $\text{H}_2\text{O}_2$  and coupled with spent LIB cathode (Fig. 3a), respectively, which is the main reason for the approximate 200 times faster speed in the absence of light when spent LIB cathode was used instead of pure  $\text{H}_2\text{O}_2$  (Fig. 3b). Generating superoxide radicals ( $\text{O}_2^{\cdot-}$ ) to promote the aromatic ring rupture and MB degradation is considered as the catalysis mechanism induced by the spent LIB cathode (Fig. 3c). This work promotes the application of end-of-life LIBs as catalysts for wastewater treatment. Guo and colleagues have realized the direct utilization of  $\text{LiFePO}_4$  cathode materials from spent LIBs as photo-Fenton photocatalysts for the photodegradation of methyl orange (MO) with the help of low-molecular-weight organic acids (oxalic acid,  $\text{H}_2\text{C}_2\text{O}_4$ ), constituting a unique approach for the application of low-value  $\text{LiFePO}_4$  waste. In the UV-LFP-oxalate system with  $20 \text{ mg L}^{-1}$  LFP and  $2 \text{ mmol L}^{-1}$  oxalate,  $50 \text{ mg L}^{-1}$  MO was almost completely decomposed within 14 min, whereas only slight MO degradation was observed in the UV-LFP and UV-oxalate systems. The accelerated photodegradation of MO by oxalate can be attributed to the generation of the strong oxidizing agent  $\cdot\text{OH}$  and other oxidative free radicals through the catalysis of LFP, indicating that LFP could be an excellent photocatalyst for MO degradation by oxalate [76]. Another idea for reusing spent  $\text{LiFePO}_4$  cathodes is proposed by Xu and colleagues [77], who synthesized iron hydroxyphosphate composites (FPOH) from waste  $\text{LiFePO}_4$  through hydrothermal treatment. FPOH exhibited



**Fig. 3** **a** The  $\ln k$  vs.  $1/T$  for the degradation of  $3 \text{ mg L}^{-1}$  MB and  $0.2 \text{ mol L}^{-1}$   $\text{H}_2\text{O}_2$  with and without spent Li-BCT; **b** the visual aspect of MB degradation in the presence of spent Li-BCT; **c** the MB catalysis degradation mechanism. Reproduced with permission from Ref. [75]. Copyright © 2015, Elsevier Ltd. **d** Proposed mechanism of photodegradation at the solid-liquid interface with the solid state catalyst. Reproduced with permission from Ref. [80]. Copyright © 2016, Elsevier B.V. **e**, **f** First-order kinetics and degradation effect

of  $\text{MnO}_2\text{-40Fe}$ ,  $\text{S-MnO}_2\text{-40Fe}$  and  $\text{F-MnO}_2\text{-40Fe}$ ; **g** multi-faceted photo-Fenton process mechanism of  $\text{MnO}_2\text{-40Fe}/\text{H}_2\text{O}_2/\text{light}$  system. Reproduced with permission from Ref. [83]. Copyright © 2021, Elsevier B.V. **h** Schematic of the zero-valent iron supported on expanded graphite and the mechanism of the degradation of 4-chlorophenol in water. Reproduced with permission from Ref. [86]. Copyright © 2021, Elsevier Ltd

exceptional Fenton-like catalytic performance in MB degradation while showing good adsorption performance for heavy metal lead. The catalytic ability of FPOH gradually decreased with the increase of organic dye concentration, where  $10 \mu\text{mol mol}^{-1}$  MB could be completely removed in 24 h, and the MB removal rate in  $20 \mu\text{mol mol}^{-1}$  reached 65% with 5 mL of  $\text{H}_2\text{O}_2$  and  $1 \text{ g L}^{-1}$  of FPOH. In addition, FPOH can be reused with even better catalytic performance due to the more dispersed particles after recycling.

In addition to using spent LIB cathode materials for catalyzing pollutant degradation directly, the Li, Co, Ni, and Mn resources from spent LIB recycling can also serve as raw materials to synthesize ferrite, which has been used as catalysts in the heterogeneous photo-Fenton process to

degrade wastewater pollutants [78, 79]. The oxidation reaction of  $\text{CoFe}_2\text{O}_4$  with  $\text{H}_2\text{O}_2$  produces radicals ( $\cdot\text{OH}$ ) at the solid-liquid interface with the solid-state catalysts (chitosan/ $\text{CoFe}_2\text{O}_4$ /graphene oxide: CS/CF/GO) for the degradation of Maxilon C.I. basic dye (Fig. 3d) [80]. Compared with homogeneous photo-Fenton reactions, the heterogeneous process can prevent sludge formation by iron hydroxide precipitation, expand the reaction pH range, and produce more hydroxyl radicals with strong chemical oxidation abilities. With these merits, Moura et al. [81] synthesized cobalt ferrite using the commercial reagents ( $\text{CoFe}_2\text{O}_4\text{-R}$ ) and recycled cobalt from the spent LIB cathode materials ( $\text{CoFe}_2\text{O}_4\text{-LIBs}$ ) via a co-precipitation method and applied them as the heterogeneous

photo-Fenton catalysts to degrade MB. Structure analysis showed that  $\text{CoFe}_2\text{O}_4$ -LIBs and  $\text{CoFe}_2\text{O}_4$ -R had similar phase structures and microstructures. Moreover, they exhibited considerable discoloration efficiency of 87.7% for  $\text{CoFe}_2\text{O}_4$ -LIBs and 87.3% for  $\text{CoFe}_2\text{O}_4$ -R when used as catalysts for MB degradation, demonstrating the efficiency and capability of heterogeneous photo-Fenton catalysts obtained from spent LIBs for preventing environmental pollution and promoting recycling process sustainability. Another class of copper ferrite photocatalysts has also been synthesized ( $\text{CuFe}_2\text{O}_4$ ) by Rocha et al. using copper recycled from spent LIBs for MB decolorization in a heterogeneous photo-Fenton process [82]. The  $\text{CuFe}_2\text{O}_4$  exhibited a superior catalytic effect with a 96.1% decolorization efficiency after 45 min and could easily be separated from the water medium. In comparison,  $\text{Fe}_2\text{O}_3/\text{Fe}_3\text{O}_4$  experiments were conducted under the same conditions, where the MB discoloration efficiency was only 77.5%. It should be noted that there is a considerable amount of  $\text{Fe}_2\text{O}_3$  (45.7% of the total) in the synthesized  $\text{CuFe}_2\text{O}_4$  from spent LIBs, and the combination of  $\text{CuFe}_2\text{O}_4$  and  $\text{Fe}_2\text{O}_3$  phases contributes to the photocatalysis because of their band gap energy. Loading  $\text{Fe}_2\text{O}_3$  on  $\text{CuFe}_2\text{O}_4$  enhanced its photocatalytic activity in the visible light range.

Besides ferrite-type materials, Chen et al. [83] prepared  $\text{MnO}_2/\text{Fe}(0)$  composite catalysts via a hydrothermal process by reclaiming Mn from the spent LIB cathode ( $\text{LiMn}_2\text{O}_4$ ). They synthesized  $\text{MnO}_2/\text{Fe}(0)$  with various  $\text{MnO}_2:\text{Fe}(0)$  molar ratios using commercial reagents first, and the optimal catalytic activity for sulfadiazine degradation was observed under the ratio of 40:1 ( $\text{MnO}_2$ -40Fe). Then, the spent LIB cathode and fresh LIB cathode were used to prepare the  $\text{MnO}_2/\text{Fe}(0)$  under the optimal conditions, denoted as S- $\text{MnO}_2$ -40Fe and F- $\text{MnO}_2$ -40Fe, respectively. Further analysis and comparison found that among  $\text{MnO}_2$ -40Fe, S- $\text{MnO}_2$ -40Fe, and F- $\text{MnO}_2$ -40Fe, the S- $\text{MnO}_2$ -40Fe delivers the highest sulfadiazine degradation efficiency (99.6%) with a rate constant of  $0.094 \text{ min}^{-1}$  (Fig. 3e, f). The enhanced catalytic activity of S- $\text{MnO}_2$ -40Fe is ascribed to oxidation state changes, phase transition, and charge density of  $\text{MnO}_2$  during inter-phasing Li ions with  $\text{MnO}_2$ -40Fe at the discharge stage. Compared to  $\text{MnO}_2$ -40Fe, the S- $\text{MnO}_2$ -40Fe showed enhanced reactivity and stability for sulfadiazine degradation after being repeatedly used five times, which can be attributed to the retard of  $\text{MnO}_2$  dissolution because of the binder used in spent cathode materials. As shown in Fig. 3g, a multi-faceted photo-Fenton process mechanism is proposed based on mass spectroscopic data with the final products of  $\text{CO}_2$ ,  $\text{H}_2\text{O}$ ,  $\text{NH}_4^+$ , and  $\text{SO}_4^{2-}$ .

Compared with valuable spent cathode materials, the cheaper graphite anode gets less attention, and only a few works have reported graphite recovery from spent LIBs, such as attaching to the adsorbent, graphene synthesis,

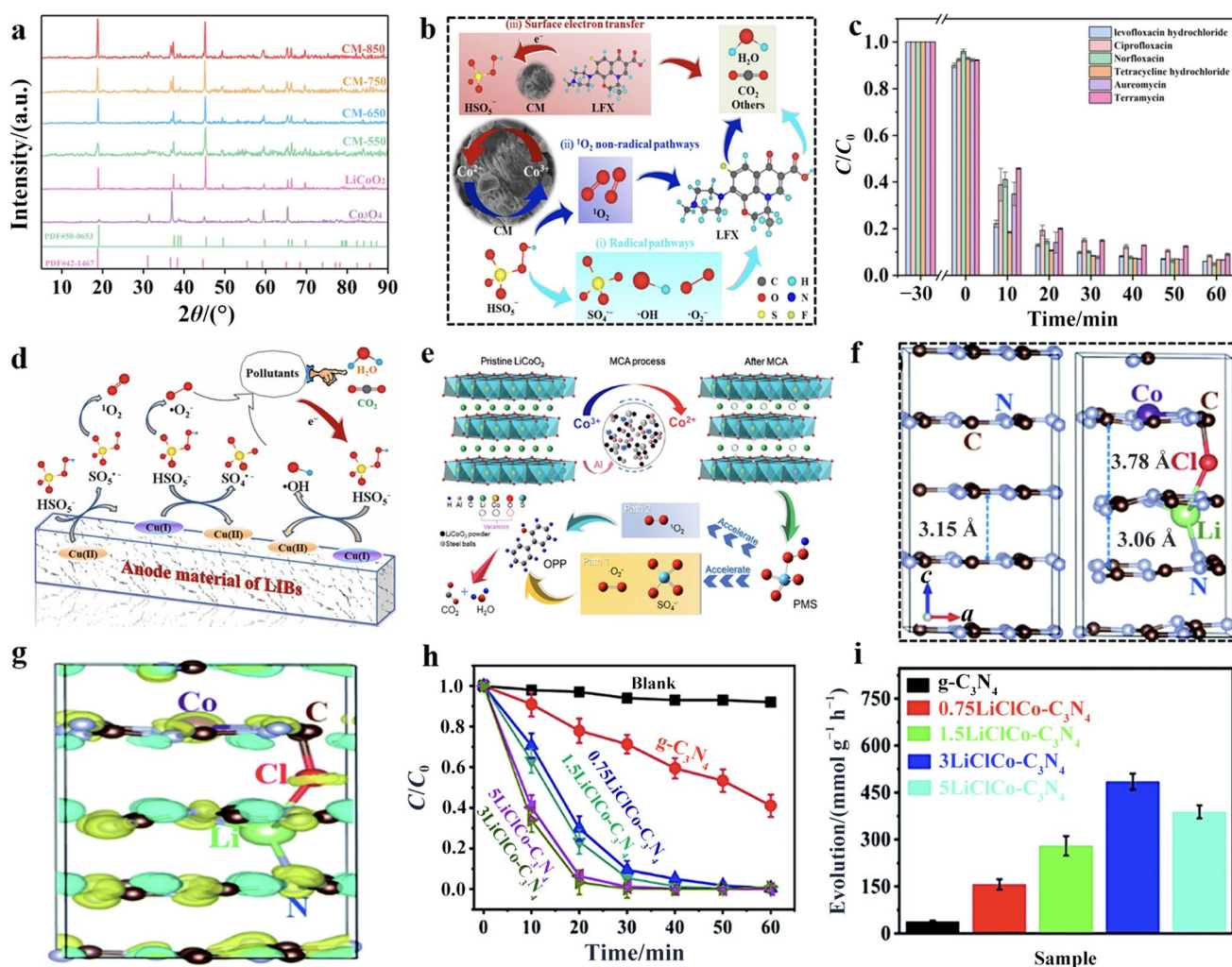
electrode materials, film materials, and sensors [84, 85]. Considering the high purity, good layer structure, and electrical conductivity of graphite in spent LIB anodes, recycling it for synthesizing advanced carbon materials is a promising option. Chen et al. [86] prepared zero-valent iron/carbon composites from wastes [ $\text{Fe}_2\text{O}_3$  from mill scale and spent graphite (SG) from LIBs] and commercial  $\text{Fe}_2\text{O}_3$  and graphite, respectively, through carbothermic reaction (denoted as ZVI/C-X and ZVI/C) and used them as catalysts for ibuprofen degradation by Fenton reaction from water. The results showed that ZVI/C-X and ZVI/C exhibited considerable catalytic performance, and ZVI/C-X exhibited low Fe-lixiviation and high stability, maintaining activity even after four consecutive cycles of use at a very low concentration of iron ions in solution after the reaction. ZVI/C-X particles have larger sizes than ZVI/C particles with the same ZVI content, which may facilitate their separation from the reaction media if needed. This work provides a new possibility for recovering graphite from spent LIBs to serve catalysis applications. This strategy was also adopted recently by Guan et al. [86] to prepare catalysts for the 4-chlorophenol (4-CP) removal from water by heterogeneous Fenton reactions, where the ferric chloride and graphite from spent LIBs were used as precursors to synthesize zero-valent iron supported with expanded graphite (ZVI/EG) (Fig. 3h). ZVI/EG delivers comparable activity to others previously reported while showing promising prospects, with the removal rate of ZVI/EG reaching  $0.0527 \text{ min}^{-1}$ , higher than the  $0.00008 \text{ min}^{-1}$  with  $\text{Fe}^{2+}$  ions and  $\text{H}_2\text{O}_2$  reported by Jin et al., and the  $0.016 \text{ min}^{-1}$  with mesoporous carbon activated peroxydisulfate reported by Yang and colleagues [87, 88]. Moreover, the 4-CP removal percentage remained high even in the sixth cycle, demonstrating its considerable stability. However, these two efforts of recycling SG for catalysts did not utilize the structural or compositional advantages of SG over commercial graphite. The performance of catalysts prepared with recycled graphite resembles those synthesized directly from commercial raw materials. Examples in subsequent sections show the unique uses of SG for catalysis.

Advanced oxidation based on peroxymonosulfate (PMS) is also extensively utilized to remove organic pollutants from wastewater because of its high potential and mild pH requirement. Transition metal oxides (e.g., Fe, Co, Cu, and Mn-based materials) are recognized as appropriate catalysts to activate PMS and generate free radicals for contaminant degradation, which generate sulfate radical anion ( $\text{SO}_4^{\cdot-}$ ) with high redox potential (2.5–3.1 V) to degrade most contaminants in water into small molecules [89]. The spent LIB cathode materials cover a wide variety of transition metal species mentioned above, which can be used as low-cost raw materials to synthesize catalysts for PMS activation, thus arousing great interest. Based on this principle, Pi et al. [90] synthesized the  $\text{CoFeO}_2$ @carbon nitride



(CoFeO<sub>2</sub>@CN) composite catalyst using Co from spent LIBs. The CoFeO<sub>2</sub>@CN composite exhibited good catalytic activity and recyclability for levofloxacin (LVF) degradation by the activation of PMS, where about 90% of the LVF was degraded in the optimal system, and the LVF degradation efficiency remained above 70% following five cycles. Thus, they have confirmed that SO<sub>4</sub><sup>2-</sup> served the dominant active species in the catalyst system, capable of extending to the removal of refractory compounds. Zhao et al. [91] developed a facile calcination method at various temperatures by preparing a catalyst using cathode materials recovered from spent LIBs to activate PMS for degrading antibiotics in wastewater. The X-ray diffraction (XRD) patterns in Fig. 4a prove that the obtained series catalysts (CM-X)

comprise 94% LiCoO<sub>2</sub> and 6% Co<sub>3</sub>O<sub>4</sub>, respectively. When used to degrade levofloxacin hydrochloride (LFX), CM-850 exhibited the optimal catalytic property with a removing efficiency of 94% under 400 mg L<sup>-1</sup> catalyst dosage, 0.5 mmol L<sup>-1</sup> PMS concentration, and an initial pH of 4.65. The mechanism exploration verified that the varied valence of Co<sup>2+</sup>/Co<sup>3+</sup> underpinned PMS activation, while SO<sub>4</sub><sup>2-</sup> and non-radical <sup>1</sup>O<sub>2</sub> were of critical significance in LFX degradation (Fig. 4b). Moreover, they also used the as-prepared catalysts to degrade five other types of antibiotic pollutants in wastewater, including terramycin, norfloxacin, ciprofloxacin, aureomycin, and tetracycline hydrochloride, yielding certain degradation effects (Fig. 4c). This work brings inspiration to the high value-added application of spent LIB recycling



**Fig. 4** **a** XRD patterns of pure Co<sub>3</sub>O<sub>4</sub> and LiCoO<sub>2</sub>, and CM catalysts; **b** the possible mechanism of PMS activation and LFX degradation in the CM/PMS system; **c** adaptability investigation of CM/PMS system on antibiotic pollutants degradation. Reproduced with permission from Ref. [91]. Copyright © 2020, Elsevier B.V. **d** The proposed reaction mechanism of PMS activation and RhB degradation in AM/PMS system. Reproduced with permission from Ref. [92]. Copy-

right © 2021, Elsevier B.V. **e** Schematic of MCA and degradation of OPP. Reproduced with permission from Ref. [93]. Copyright © 2021, American Chemical Society. **f, g** The optimal g-C<sub>3</sub>N<sub>4</sub> and obtained stable LiClCo-C<sub>3</sub>N<sub>4</sub> structure with charge difference distribution; **h, i** photocatalyst for RhB degradation and hydrogen evolution of 3LiClCo-C<sub>3</sub>N<sub>4</sub>, respectively. Reproduced with permission from Ref. [99]. Copyright © 2021, The Royal Society of Chemistry

materials. Except for preparing catalysts from spent cathode materials, Zhao and co-workers also synthesized a copper oxide and graphite carbon (CuO/C) catalyst from recycled spent LIB anode materials to activate PMS for degrading a wide range of organic contaminants (Fig. 4d), which exhibited excellent catalytic effects. In particular, the rhodamine B (RhB) degradation rate reached 100% in 13 min under the catalysis of CuO/C in the solution through the PMS activation. The admirable oxidation and degradation abilities of this catalyst/PMS system are generally attributed to the produced  $\text{SO}_4^{\cdot-}$  and  $^1\text{O}_2$ , and the catalytic performance of this system was determined by the rate of Cu(II) reduction to Cu(I), where the SG base accelerated the redox cycle of Cu(II)/Cu(I), promptly activating PMS to produce reactive oxygen species (e.g.,  $\text{HO}^\cdot$ ,  $\text{SO}_4^{\cdot-}$ , and  $^1\text{O}_2$ ) for degrading pollutants [92].

Although using spent LIB electrode materials as catalysts for advanced oxidation has attracted increasing attention, the catalytic efficiency and utilization rate remain limited. To achieve efficient utilization of the spent cathode and avoid wasting aluminum resources, Dang et al. [93] used aluminum foils in the cathode of spent  $\text{LiCoO}_2$  batteries as reducing agents to convert part of  $\text{Co}^{3+}$  into  $\text{Co}^{2+}$  during the mechanochemical activation (MCA) process (Fig. 4e). The obtained  $\text{Co}^{2+}$  could serve as the active center to activate PMS efficiently and improve the catalytic effect. Furthermore, the degradation rate of *o*-phenylphenol could reach 100% within 30 min. To further simplify the catalyst manufacturing process and save costs, Wang et al. [94] investigated the effect of the lithiation extension on the catalytic activity, concluding that the catalytic activity increased as the lithiation depth extended. Based on this, they directly used the recycled active  $\text{LiMn}_2\text{O}_4$  component from spent LIBs for PMS activation for decomposing RhB, where approximately 98.2% of RhB was degraded within 30 min, and the catalytic decomposition efficiency still reached 94.8% after 10 cycles.

Photocatalytic oxidation is another advanced oxidation method in wastewater treatment for recalcitrant and toxic organic compound degradation [95, 96], where advanced catalysts play a key role in improving energy utilization efficiency and promoting the thorough degradation of organic pollutants. The photocatalysts with heterostructures exhibit improved catalytic ability due to the regulated electronic structure and efficient photoinduced electron-hole pair separation process [97]. Spent LIB electrode materials with complex compositions can be used to prepare the hetero-structured photocatalysts. Many Co-based oxides have been synthesized from spent LIB cathodes to serve as efficient photocatalysts for decomposing textile dye and antibiotics in wastewater [91, 98]. Niu et al. [99] regulated the  $\pi$ -conjugated structure of *g*- $\text{C}_3\text{N}_4$  using the spent  $\text{LiCoO}_2$  cathode,  $\text{NH}_4\text{Cl}$ , and melamine. The as-prepared

$\text{LiClCo-C}_3\text{N}_4$  catalyst exhibited a unique crystal structure (Fig. 4f) composed of Co–N, Cl–C, Li–Cl, and Li–N bonds, which could boost the charge migration and separation between *g*- $\text{C}_3\text{N}_4$  layers (Fig. 4g). In order to achieve the optimal catalytic effect, they regulated the usage amount of spent  $\text{LiCoO}_2$  (denoted as 5 $\text{LiClCo-C}_3\text{N}_4$ , 3 $\text{LiClCo-C}_3\text{N}_4$ , 1.5 $\text{LiClCo-C}_3\text{N}_4$ , and 0.75 $\text{LiClCo-C}_3\text{N}_4$ ). When used as a photocatalyst for RhB degradation and hydrogen evolution, the as-prepared 3 $\text{LiClCo-C}_3\text{N}_4$  showed superior catalytic performance with 12.6 and 15.3 times higher than those of pristine *g*- $\text{C}_3\text{N}_4$  (Fig. 4h, i). Furthermore, Zhang et al. [100] synthesized a graphene oxide-copper composite material from the spent anode graphite and copper foils in the LIB anode and studied their photocatalytic degradation performance on MB. Within the graphene oxide-copper composite, the graphene oxide acted as a carrier, which improved the catalytic activity and greatly increased the degradation rate of CuO on MB due to the large specific surface area and oxygen groups. Moreover, adding an electric field can significantly improve the catalytic degradation efficiency because more active free radicals can be produced. Furthermore, the graphite from the spent LIB anode can also be used to synthesize a series of graphene-based materials for catalytic ozonation of organic pollutants [101]. These works revealed a synergetic concept of recycling wastes as high-efficiency photocatalysts for environmental protection.

In general, end-of-life LIB electrode materials, including various commercial cathode and graphite anode, can be used directly or indirectly for advanced catalysts through calcination or hydrothermal regenerative processes and applied to pollutant degradation in wastewater through different catalytic reaction technologies. This unique strategy solves the huge challenges of spent LIB recycling and improves the water environment quality, thus warranting more attention in future research. Moreover, catalysts derived from spent LIBs are limited to metal oxides at present, and many other types of catalysts, such as alloys, single-atoms, and transition metal chalcogenides, can be developed from spent LIBs, leaving huge space for development and application.

## 4.2 Application in Volatile Organic Compounds Removal

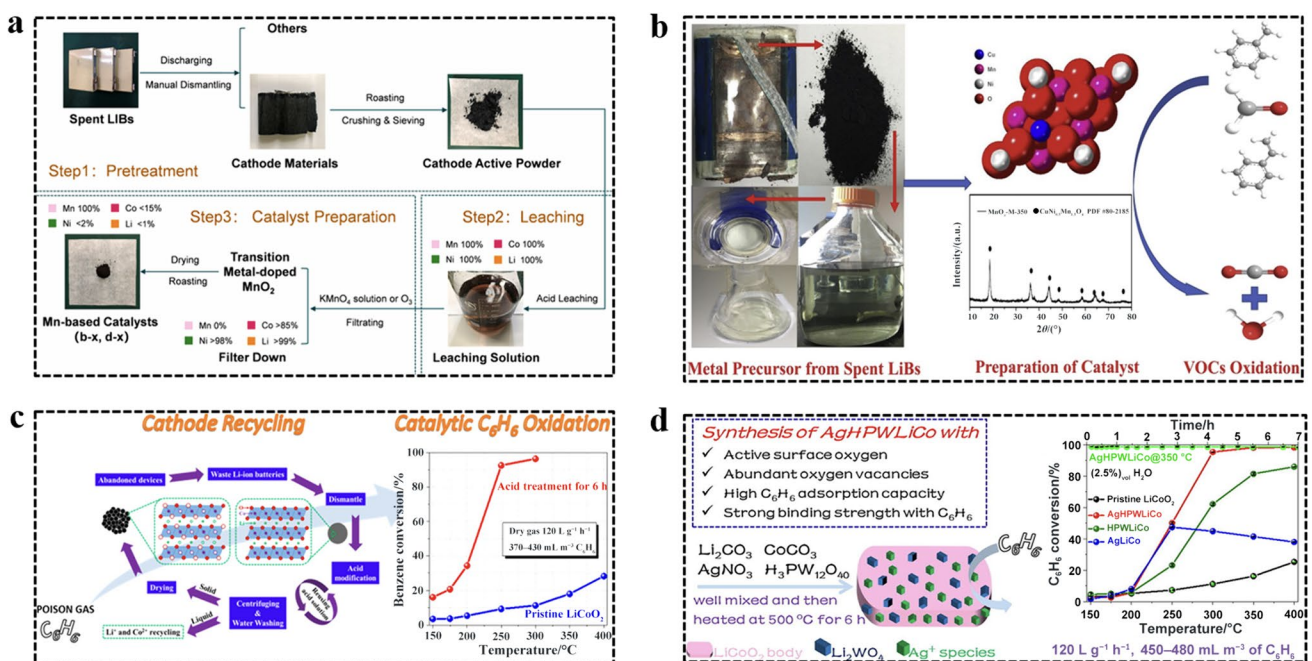
VOCs are mainly derived from the incomplete combustion of fossil fuels and the escape of industrial products during manufacturing and application [102]. They are considered culprits of air pollution and the main harmful substances causing great damage to human health [103, 104]. Many techniques have been developed to control VOC emissions, such as adsorption, thermal combustion, photocatalytic degradation, plasma degradation, and catalytic oxidation [105]. Among them, catalytic oxidation is the most promising due to the harmless end products, high activity, and low price

[106]. Previous studies have shown that noble metals exhibit superior catalytic performance for VOC oxidation, but their widespread application is hindered by the high cost [107]. In contrast, transition metal compounds have become common high-performance catalysts for VOC removal due to their low cost and excellent low-temperature catalytic performance [108]. Therefore, it is feasible to utilize spent LIB cathodic material-derived transition metals to synthesis catalysts, which shows a promising application prospect.

As proof of concept, Guo et al. [109–112] synthesized a series of manganese-based metal oxide catalysts from spent LIB cathode materials using the impregnation, hydrothermal, co-precipitation, and combustion methods to catalyze VOC oxidation (Fig. 5a, b), which showed excellent catalytic activity due to the high-valence metal ion, high concentration of active oxygen species, and large specific surface area. Potassium permanganate and ozone have been used to thoroughly oxidize spent LIBs for selective and efficient manganese recovery, and transition metal-doped  $\text{MnO}_2$  has been prepared for the catalytic oxidation of VOCs. The manganese recovery rate could reach about 100%, and the recovery rates of cobalt, nickel, and lithium were below 15%, 2%, and 1%, respectively. Introducing nickel, cobalt, and copper into manganese oxides significantly affected the catalytic performance compared to the substitute of lithium and aluminum. Consequently, Mn-based multi-oxide catalysts from spent LIBs exhibited better catalytic performance in toluene and

formaldehyde removal than pure manganese oxides owing to their lower crystallinity, more defects, larger specific surface area, more oxygen vacancies, and better low-temperature redox abilities [109]. They further synthesized a series of manganese oxide catalysts modified by other elements (e.g., Fe, Bi, and Ce) and demonstrated that introducing appropriate amounts of these elements can enhance the catalytic performance of manganese oxides in VOC removal, which can be attributed to the lower crystallinity, larger specific surface area, small particle size, higher amount of active oxygen species and  $\text{Mn}^{4+}$  ions, and better low-temperature reducibility [111]. Besides  $\text{MnO}_x$ , Mn-based composite perovskite was also considered an effective candidate for VOC removal. Since ternary LIBs contain abundant metals such as manganese, cobalt, and nickel, spent ternary LIBs are considered promising sources of metal precursors for the preparation of Mn-based composite perovskite [112].

In addition to Mn-based oxides, cobalt-based oxides derived from spent LIBs also attracted attention in catalytic VOC oxidation [113]. Dai et al. [114] used an acid treatment method to improve the catalytic activity of spent  $\text{LiCoO}_2$  for benzene oxidation (Fig. 5c). The as-prepared acid-modified  $\text{LiCoO}_2$  catalyst showed O, Co, and Li vacancies, facilitating gaseous benzene adsorption and subsequent activation. The part of  $\text{Co}^{3+}$  leached out from the  $[\text{CoO}_6]$  octahedra in  $\text{LiCoO}_2$  by  $\text{HNO}_3$  solution via the disproportionation reaction with the deintercalation of interlayer  $\text{Li}^+$  ions is the reason



**Fig. 5** a, b The research scheme of catalyst preparation from spent LIBs. Reproduced with permission from Refs. [109, 110]. Copyright © 2019 and 2020, Elsevier B.V. c Process of the LCO cathode recycling and the catalytic effect on the  $\text{C}_6\text{H}_6$  oxidation. Reproduced with

permission from Ref. [114]. Copyright © 2019, American Chemical Society. d Synthetic method of  $\text{AgHPWLiCo}$  and the catalytic effect on the  $\text{C}_6\text{H}_6$  oxidation. Reproduced with permission from Ref. [115]. Copyright © 2019, Elsevier B.V.

for vacancy formation. Liu et al. [115] (Fig. 5d) synthesized a  $\text{LiCoO}_2$  catalyst modified by Ag and phosphotungstic acid with considerable performance on the catalytic oxidation of benzene vapor, indicating the potential of using cathode materials like  $\text{LiCoO}_2$  as the raw materials to synthesize catalysts. Further, they proposed a simple and facile water treatment procedure to activate the recycled  $\text{LiCoO}_2$  cathode materials from spent LIBs for promoting gaseous benzene oxidation. Water washing eliminated the chemically absorbed oxygen and surficial lattice oxygen, and the bulk lattice oxygen was thereby exposed and became more reachable to the gaseous benzene, which could oxidize benzene efficiently at high temperatures [116]. These strategies provided new concepts for deriving catalysts from spent LIB electrode materials for VOC degradation. However, these concepts are still in their infancy, with many opportunities and challenges.

In conclusion, the latest research progress in using spent LIBs to prepare advanced catalysts for environmental remediation (wastewater treatment and VOC removal) is summarized and discussed from the aspects of regeneration methods, catalytic performance, and catalytic reaction mechanism. Hopefully, this summary can be of reference significance to the subsequent research. Furthermore, the recycling of spent LIB materials for environmental remediation catalysts and the corresponding performance are shown in Table 1.

These examples show the feasibility and prospect of converting spent LIB materials into catalysts, which alleviates the environmental hazards caused by spent LIBs while realizing their high-value utilization. However, this approach is not mature, and it faces many challenges. Firstly, most studies on recycling spent LIB materials as catalysts are based on hydrometallurgy or pyrometallurgy, that is, extracting elements from spent LIB materials and synthesizing catalysts using their simple substances or compounds as raw materials, which does not have much competitive advantages over directly using commercially available raw materials. Typically, there is no performance difference between catalysts synthesized from recycled or non-recycled raw materials, and the advantages of using spent LIB materials in catalysis have not been fully exploited. Meanwhile, previous research mentioned that the crystal structure and defects may benefit the catalytic effect. More studies on the catalytic properties of spent LIB materials are needed. Furthermore, the application of the catalysts in these reports is relatively narrow, i.e., most reports studied the catalytic effects on particular pollutants, while there are various pollutants in actual sewage and exhaust gas, necessitating multifunctional catalysts. Therefore, researchers are recommended to develop and study the catalytic effect of catalysts on the degradation of various pollutants in follow-up studies. In addition, a comparison between catalysts synthesized from recycled and

non-recycled materials is necessary, whereas the comparison between the newly developed and commercial catalysts also provides useful information. Hence, researchers are suggested to always add a commercial catalyst as a comparison when quantifying catalyst performance so that readers can better understand the performance of newly developed catalysts.

## 5 Spent LIB-Derived Catalysts for Substance Conversion

### 5.1 Oxygen/Hydrogen Evolution Reaction (OER/HER) Related Catalysis

Electrolytic water decomposition is the most promising method for hydrogen production as the hydrogen generated from electrolysis represents a non- $\text{CO}_2$  emission process and is often referred to as green hydrogen, which involves OER and HER [117, 118], respectively. Water electrolysis to produce hydrogen usually requires efficient catalysts. However, the application of noble-metal catalysts (e.g., platinum, ruthenium, and iridium) is limited due to their scarce storage and high cost [119]. Developing non-precious metal-based catalysts with low cost to reduce the reaction energy barrier and enhance the reaction efficiency is a prerequisite for further development in this field. Transition metal compounds have been proven to have excellent catalytic properties comparable to noble metal catalysts by rational structural design and controlled synthesis process. Therefore, the most common LIB cathode materials have potential catalytic activity for OER/HER due to the presence of transition metals such as cobalt, nickel, manganese, and iron, which can also be used as precursors to prepare various transition metal compounds to substitute noble-metals as electrocatalysts, which has aroused academic attention [120, 121]. According to the different types of cathode materials, this section summarized the latest progress of electrocatalyst preparation using  $\text{LiCoO}_2$ ,  $\text{LiFePO}_4$ , and ternary  $\text{LiNi}_{1-x-y}\text{Co}_x\text{Mn}_y\text{O}_2$  (NCM) as raw materials, respectively, covering synthetic method, catalytic efficiency, and mechanism.

#### 5.1.1 Spent Co-Based LIBs as Catalyst Sources

Among the various transition metals, cobalt-based materials exhibit better electrocatalytic performance than other non-noble metal materials [122].  $\text{LiCoO}_2$ , as an important class of cobalt-based oxides, has been widely used in LIB cathode materials due to the high specific capacity, long cycle life, and high potential, which usually has two main types of spinels and layered crystal structures. As the cathode active material, LCO with layered structures allows smooth intercalation and extraction of lithium ions during

**Table 1** Recycling of spent LIB materials for environmental remediation catalysts and corresponding performance

Spent material types	Regenerative methods	Catalyst	Application	Catalytic reaction mechanism	Performance	References
LiCoO <sub>2</sub>	Heated to 200 °C for 5 h	Li-BCT (83% LiCoO <sub>2</sub> , 14.5% C, 2.5% Al, Al <sub>2</sub> O <sub>3</sub> and Co <sub>3</sub> O <sub>4</sub> )	Degradation of methylene blue	The generation of superoxide radicals	Reduced activation energy (26 kJ mol <sup>-1</sup> ) and increased velocity constant (203 × 10 <sup>-4</sup> min <sup>-1</sup> )	[75]
LiFePO <sub>4</sub>	Direct utilization	LFP (LiFePO <sub>4</sub> )	Degradation of methyl orange	The increased production of ·OH radicals and other active free radicals	Removal reaches 50 mg L <sup>-1</sup> at pH=4	[76]
	Hydrothermal treatment	FPOH (iron hydroxyphosphate)	Degradation of methylene blue	Fenton-like catalysis	Removal reached 65% in 20 μmol mol <sup>-1</sup>	[77]
LiCoO <sub>2</sub>	Co-precipitation method	CoFe <sub>2</sub> O <sub>4</sub> -LIBs (CoFe <sub>2</sub> O <sub>4</sub> and Fe <sub>2</sub> O <sub>3</sub> )	Degradation of methylene blue	Heterogeneous photo-Fenton catalysis	Discoloration efficiency reached 87.7% at pH=3	[81]
Current collector	Co-precipitation method	CuFe <sub>2</sub> O <sub>4</sub> -LiB (CuFe <sub>2</sub> O <sub>4</sub> and Fe <sub>2</sub> O <sub>3</sub> )	Decolorization of methylene blue	Heterogeneous photo-Fenton catalysis	Decolorization efficiency reached 96.1% in 45 min	[82]
LiMn <sub>2</sub> O <sub>4</sub>	Hydrothermal process	MnO <sub>2</sub> /Fe(0)	Decolorization of sulfadiazine	Multi-faceted photo-Fenton catalysis	Degradation efficiency reached 99.6% with 0.094 min <sup>-1</sup>	[83]
Graphite	Carbothermic reactions	ZVI/C-X (Fe and C)	Removal of ibuprofen	Fenton catalysis	Removal reached 76.7%	[86]
Graphite	Carbothermic reduction	ZVI/EG (Fe and C)	Removal of 4-chlorophenol	Heterogeneous Fenton catalysis	Removal reached 97% in 1 h	[86]
LiCoO <sub>2</sub>	Hydrothermal and carbonization	CoFeO <sub>2</sub> @CN	Degradation of levofloxacin hydrochloride	PMS-based advanced oxidation	Removal > 90%	[90]
LiCoO <sub>2</sub>	Calcination method	CM catalyst (94% LiCoO <sub>2</sub> and 6% Co <sub>3</sub> O <sub>4</sub> )	Eliminate antibiotics	PMS-based advanced oxidation	Removal reached 94% for levofloxacin hydrochloride	[91]
Graphite	Calcination process	CuO/C	Degradation of organic contaminants	PMS-based advanced oxidation	Removal reached 100% for rhodamine B	[92]
LiCoO <sub>2</sub>	Mechanochemical activation	LiCo <sub>x</sub> O <sub>y</sub> (Co: 2+)	Degradation of <i>o</i> -phenylphenol	PMS-based advanced oxidation	The degradation rate reached 100% within 30 min	[93]
LiMn <sub>2</sub> O <sub>4</sub>	Washing-recycling process	LiMn <sub>2</sub> O <sub>4</sub>	Degradation of rthophenylphenol	PMS-based advanced oxidation	Decomposition efficiency reached 94.8% after 10 cycles	[94]
LiCoO <sub>2</sub>	One-pot sintering	LiClCo-C <sub>3</sub> N <sub>4</sub>	Degradation of rhodamine B	The generation of H <sup>+</sup> , O <sub>2</sub> <sup>-</sup> , and ·OH	Degradation rates reached 15.3 times higher than pristine g-C <sub>3</sub> N <sub>4</sub>	[99]
LiNi <sub>x</sub> Co <sub>y</sub> Mn <sub>z</sub> O <sub>2</sub>	Acid leaching and calcination	MnO <sub>x</sub> -M-350 (CuNi <sub>0.5</sub> Mn <sub>1.5</sub> O <sub>4</sub> )	VOCs oxidation	Mars-van-Krevelen mechanism	Over 90% conversion rates for toluene, ethylbenzene, and formaldehyde	[110]
LiCoO <sub>2</sub>	Disproportion reaction	H-LiCo-6	Catalytic C <sub>6</sub> H <sub>6</sub> oxidation	Mars-van-Krevelen mechanism	Benzene conversion > 90% at 350 °C	[114]
LiCoO <sub>2</sub>	Thermal treatment	AgHPWLiCo	Catalytic C <sub>6</sub> H <sub>6</sub> oxidation	Mars-van-Krevelen mechanism	Benzene conversion ~ 95% at 300 °C	[115]

charging and discharging. However, after excessive cycles of charge and discharge, the layered structure degrades to a spinel structure, leading to a decline in reversible capacity and representing a manifestation of material failure. Yet, the opposite is true in catalysis, where the spinel structure exhibits higher catalytic activity than others and deliver superior performance in OER and HER [123]. Therefore, spent LCO is considered a promising advanced electrocatalyst and has received more attention recently. Moreover, it is generally believed that the  $\text{Co}_3\text{O}_4$  formed after delithiation is the actual active substance, and the high OER activity is also ascribed to the oxidation of cobalt ions and phase transition during the  $\text{Li}^+$  extraction process [124]. After repeated charging/discharging cycles, the lattice volume undergoes obvious changes and generates more defects and strains of LCO, further promoting the electrochemical catalytic kinetics [125].

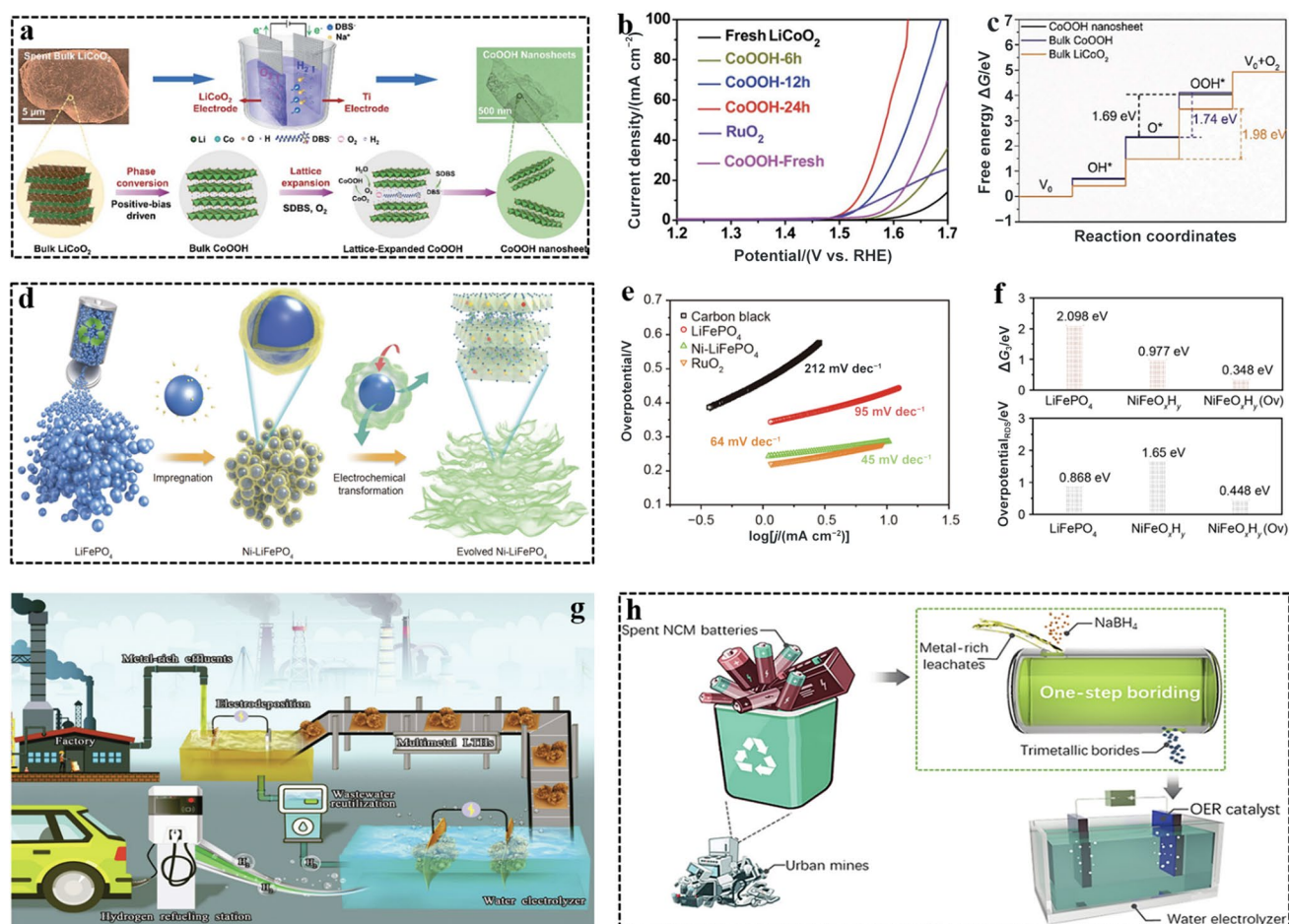
Specially, Chen et al. [126] reported a simple method to use the spent LCO cathode as OER catalysts. They discovered that with an increased number of cycles, a new phase of  $\text{Li}_{1-x}\text{CoO}_2$  formed, and the LCO surface was corroded during the  $\text{Li}^+$  insertion and extraction processes, contributing to a larger specific surface area of the catalysts. In addition, the OER catalytic activity of recycled LCO increased with the number of cell cycles. Recycled LCO after 500 cycles (2.8 V to 4.3 V at 0.5 C) showed improved OER catalytic activity with a reduced onset potential of 1.52 V and accelerated the current increase compared with the original LCO. It delivered a current density of  $9.68 \text{ mA cm}^{-2}$  at 1.65 V, approximately 3.8 times that of the pristine LCO. Meanwhile, it maintained the original catalytic activity after repeating the potential cycling test for 1 000 cycles. This study provides a simple and effective method to prepare catalysts from spent LIBs. High-temperature (HT)-LCO is also an important cathode material for LIBs with a hexagonal and layered structure [127]. Pegoretti et al. [128] extracted Co from the spent LCO cathode and prepared  $\text{Co}(\text{OH})_2$  as the precursor. After mixing with stoichiometric  $\text{Li}_2\text{CO}_3$  and calcinated at  $800^\circ\text{C}$  for 5 h, HT-LCO was obtained. The synthesized HT-LCO has considerable potential as a cathode material and exhibited promising OER catalytic effects. The as-prepared HT-LCO as an OER catalyst delivered a lower onset potential of 0.35 V than Ni and Pt plates (over 0.5 V). According to the Tafel plot and Nyquist diagrams, the activation energy of HT-LCO for OER was  $28.0 \text{ kJ mol}^{-1}$  with a transfer charge resistance of  $1.55 \Omega$ , which was regarded as excellent compared to other Co-based materials. These data indicate that HT-LCO is expected to be an excellent OER catalyst. However, the proposed recycling strategy ignored the recycling of lithium and has a large energy consumption, which still requires improvements. Huang et al. [129] developed an environmental-friendly and energy-efficient strategy to exfoliate strong Li–O interplanar bonding into

ultra-thin  $\text{CoOOH}$  nanosheets from the spent LCO cathode with synergistic action of phase conversion and lattice expansion (Fig. 6a). Due to the sheet morphology, larger spacing, and exposed surface, the as-prepared ultra-thin  $\text{CoOOH}$  catalyst provided more electrocatalytic active sites for OER, delivering superior performance with a low Tafel slope of  $53.8 \text{ mV dec}^{-1}$  and a small overpotential of 305 mV at  $10 \text{ mA cm}^{-2}$  after long-term electrolysis for 65 h, superior to some advanced OER catalysts (e.g., fresh  $\text{LiCoO}_2$  and commercial  $\text{RuO}_2$ ) (Fig. 6b). In addition to LCO, a wide variety of layered cathode materials can be successfully converted into ultrathin nanosheets with this strategy, which can be further applied to OER catalysis. Besides, the Li in spent LCO was recycled as  $\text{Li}_3\text{PO}_4$  for re-utilization. Further research revealed that the  $\text{CoOOH}$  catalyst with a modest content of oxygen vacancies and thinner nanosheets requires a lower Gibbs free energy difference during catalysis (Fig. 6c). Natarajan et al. [120] proposed a facile way to synthesize spinel microsphere  $\text{MnCo}_2\text{O}_4$  catalysts from Co-rich (like LCO) and Mn-rich (like  $\text{Li}_x\text{MnO}_{x+1}$ ) spent LIBs without using surfactant. The  $\text{MnCo}_2\text{O}_4$  catalyst exhibited outstanding OER activity in an alkaline medium and maintained its catalytic ability after reusing in water electrolytes. Furthermore, it exhibited comparable activity to commercially available OER catalysts, such as  $\text{RuO}_2$ ,  $\text{Co}_3\text{O}_4$ , and  $\text{MnO}_2$ . Although not requiring surfactant, some chemical reactants in this study, like acetic acid, were still required, and the calcination temperature of  $650^\circ\text{C}$  consumed more energy, also regarded as an issue faced by traditional hydrometallurgy. In addition to using high-temperature sintering to synthesize catalysts from spent LIBs, other more straightforward strategies must be developed to reduce energy consumption. Caspar et al. [130] prepared an efficient Co-based catalyst (cobalt-aluminum borate) from spent cobalt-based LIBs to hydrolyze  $\text{NaBH}_4$  for hydrogen production. This strategy does not require calcination, and the synthesis process could be achieved at relatively low temperatures. The average oxidation state of the prepared Co-based catalyst was 2.45, making it an inert catalyst at room temperature. However, when heated to  $70^\circ\text{C}$ , the catalytic performance was improved, and the rapid hydrogen production could reach  $49.3 \text{ L min}^{-1} \text{ g}^{-1}$  (Co), with each Co atom generating at least  $1.2 \times 10^7$  hydrogen molecules. However, improving the long-term stability of this type of catalyst still needs further research, and using strong acid is also one of the most important issues hindering the practical application of such methods. Recently, hydrometallurgical methods tend to use less environment-polluting and more easily degradable organic acids as leaching agents. Arif et al. [131] utilized citric and lemon peel extracts to recover lithium cobalt oxide from waste LIBs, and the recovered cathode material was used as an OER catalyst. Liu et al. [132] used mild organic acids (glycine & ascorbic acid) to recover Co from spent

LIBs and synthesize cobalt nitride composite material (CoN-Gr-2) with the shape of 3D sea-urchin through hydrothermal method. The CoN-Gr-2 exhibited excellent performance as a bi-functional catalyst for OER and HER. When adopting CoN-Gr-2 as both anode and cathode materials for overall water splitting (in  $1.0 \text{ mol L}^{-1}$  KOH electrolyte), the assembled cell achieved a current density of  $10 \text{ mA cm}^{-2}$  at  $1.61 \text{ V}$ , close to that of Pt/C||RuO<sub>2</sub> benchmark ( $1.60 \text{ V}$ ). These methods help to further solve environmental pollution and generate good economic benefits. However, high temperature calcination with high energy consumption was inevitable in the pretreatment or subsequent resynthesis.

### 5.1.2 Spent LFP as Catalyst Sources

Pure LFP cathode materials possess poor active sites, weak intrinsic activity, and low conductivity, contributing to their inferior catalytic activity, which renders them unavailable for direct application. For this reason, the recovery of spent LFP-based LIBs as electrocatalysts is limited. Cui et al. [133] proposed a wetness impregnation method featuring facile and economic attributes to convert spent LFP into NiFe oxy/hydroxide catalyst with high catalytic activity for OER. Specifically, this catalyst was recycled from spent LFP cathode material, which was scraped in a  $\text{Ni}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$  solution and evolved into defect-rich  $\text{NiFeO}_x\text{H}_y$  nanosheets during OER (Fig. 6d). The evolved  $\text{NiFeO}_x\text{H}_y$  showed better catalytic activity than the original LFP and RuO<sub>2</sub>



**Fig. 6** **a** Schematic illustration of the in situ positive-bias driven exfoliation of  $\text{LiCoO}_2$  into  $\text{CoOOH}$ ; **b** polarization curves of various catalysts; **c** the Gibbs free energy profiles for the OER pathway. Reproduced with permission from Ref. [129]. Copyright © 2022, The Royal Society of Chemistry. **d** Schematic illustration of the proposed regeneration route for spent  $\text{LiFePO}_4$ ; **e** the Tafel plots  $\text{Ni-LiFePO}_4$ ,  $\text{RuO}_2$ , spent  $\text{LiFePO}_4$  and carbon black; **f** the free energy change ( $\Delta G_3$ ) for the generation of  $^*\text{OOH}$  in different models and the theoretical overpotentials for different models. Reproduced with per-

mission from Ref. [133]. Copyright © 2021, Science China Press and Springer-Verlag GmbH Germany. **g** Schematic illustration of resource utilization of battery industrial wastewater. Reproduced with permission from Ref. [135]. Copyright © 2022, The Royal Society of Chemistry. **h** Schematic illustration on the synthesis of magnetic NCMB OER electrocatalysts from the spent LIB leachate via a facile boriding process. Reproduced with permission from Ref. [136]. Copyright © 2021, The Royal Society of Chemistry

benchmark catalyst, with a reduced overpotential of 285 mV at 10 mA cm<sup>-2</sup> and a Tafel slope of 45 mV dec<sup>-1</sup>. Its stability was well-maintained at 10 mA cm<sup>-2</sup> for 14 h. The enhanced catalytic performance was attributed to the structural evolution and the introduction of the Ni promoter. The evolved nanosheets provided rich sites for reagents and products, and the numerous defects greatly boosted the OER kinetics. Furthermore, the addition of Ni optimized the free energy of \*OOH intermediates, activating the Fe site effectively. The rich oxygen defects promoted oxygen desorption and synergistically improved the catalytic performance of LFP (Fig. 6e, f). This work corroborated the likelihood of converting spent LFP into high performance electrocatalyst. The spent LFP can be activated through appropriate modification, providing a new reference for designing advanced catalysts from a sustainable perspective of spent LIB recycling.

### 5.1.3 Spent NCM as Catalysts Sources

NCM, with low cost, high energy density, and good thermal stability, has gained increasing attraction as an alternative to LiCoO<sub>2</sub> cathode materials. A growing number of EVs, hybrid EVs, and energy storage equipment use NCM batteries as power sources, increasing the quantity of spent NCM batteries. Considering the high-value elements such as Ni and Co, efficient recycling of NCM has become the focus of academia and industry [134]. The industrial techniques of battery recovery include pyrometallurgy and hydrometallurgy. In the recycling process, hydrometallurgical recovery is more energy-saving, environmentally friendly, and efficient than pyrometallurgical recovery. Despite these advantages, industrial wastewater remains in this treatment. More environmentally friendly recycling and high-value utilization of NCM are urgently necessitated. Chen et al. [135] developed an economical and facile strategy to synergistically recover and reuse metal ions (99.19% of Co, 99.15% of Mn, and 99.38% of Ni) from spent LiNi<sub>x</sub>Co<sub>y</sub>Mn<sub>1-x-y</sub>O<sub>2</sub> in industrial wastewater after hydrometallurgy (Fig. 6g). They extracted NiCoMn layered triple hydroxides (LTHs) with a hierarchical nanoflower structure from wastewater using electrodeposition. The electrodeposited electrode material was an efficient bifunctional catalyst for HER and OER. Additionally, it could be directly used to catalyze hydrogen production by electrolyzing the post-electrodeposition wastewater. As an HER catalyst, the optimal LTHs showed consistent catalytic activity with the Pt/C. In contrast, when catalyzing the OER, its catalytic performance was even better than the commercial RuO<sub>2</sub> due to the unique structure with considerable catalytic active sites and rich crystalline/amorphous phase boundaries. Encouraged by the excellent HER and OER catalysis performance, they further applied LTH||LTH couple to electrolyze post-electrodeposition wastewater for hydrogen production. This couple showed

higher efficiency than the RuO<sub>2</sub>||Pt/C couple, affording 10 mA cm<sup>-2</sup> at voltages of 1.58 V vs. 1.62 V. Moreover, they also developed a one-pot boriding method to prepare magnetic mixed metallic borides as catalysts for efficient OER from the spent LiNiCoMnO<sub>2</sub> batteries (Fig. 6h) [136], attaining an overpotential of 372 mV at 500 mA cm<sup>-2</sup> with superior cycling stability. It also outperformed the RuO<sub>2</sub> catalyst at high current densities, and the current density of the prepared catalyst at 1.53 V was 2.31 times higher than of RuO<sub>2</sub> catalyst. The excellent OER catalytic performance was attributed to the formation of core@shell structured tri-metal boride@(oxy)hydroxide nanostructures induced by boron etching. The current density remained stable for 12 h with a small loss (~5%) on the electrode.

Multi-metal oxide catalysts have excellent properties thanks to active site filling and electronic structure optimization. For example, Yang et al. [137] proposed an MCA method for selective recovery of Ni<sub>0.5</sub>Mn<sub>0.3</sub>Co<sub>0.2</sub>(OH)<sub>2</sub> catalyst from spent LiNi<sub>0.5</sub>Mn<sub>0.3</sub>Co<sub>0.2</sub>O<sub>2</sub> cathodes. After ball milling, the mixed spent LiNi<sub>0.5</sub>Mn<sub>0.3</sub>Co<sub>0.2</sub>O<sub>2</sub> and Na<sub>2</sub>S·9H<sub>2</sub>O, Ni<sub>0.5</sub>Mn<sub>0.3</sub>Co<sub>0.2</sub>(OH)<sub>2</sub> nanoparticles were obtained. Deionized water was used to leach the Li species, and Li<sub>2</sub>CO<sub>3</sub> can be precipitated using Na<sub>2</sub>CO<sub>3</sub> as a precipitant. The production of Ni<sub>0.5</sub>Mn<sub>0.3</sub>Co<sub>0.2</sub>(OH)<sub>2</sub> nanoparticles with increasing active sites exposed by MCA improved OER activity. It exhibited comparable OER activity to the commercial IrO<sub>2</sub>. For instance, at a current density of 10 mA cm<sup>-2</sup>, the required overpotentials of Ni<sub>0.5</sub>Mn<sub>0.3</sub>Co<sub>0.2</sub>(OH)<sub>2</sub> nanoparticles and IrO<sub>2</sub> reached 0.28 V and 0.29 V, respectively. Furthermore, Lv et al. [138] developed an environmentally friendly and holistic method to promote spent LIB de-lithiation based on the direct current electric field (Fig. 7a). In the de-lithiation process, the lithium ions could be effectively recovered as Li<sub>3</sub>PO<sub>4</sub> with simultaneous H<sub>2</sub> production. The de-lithiated electrode material (Li<sub>1-δ</sub>Ni<sub>0.5</sub>Co<sub>0.2</sub>Mn<sub>0.3</sub>O<sub>2</sub>) obtained a superior electrocatalytic performance. This improvement was ascribed to the high specific surface area of recycled cathode material, the abundant lattice oxygen and the increased oxidation state of Ni. Notably, the sample with the maximal de-lithiation degree exhibited relatively poor OER performance. The authors ascribed this phenomenon to the following two reasons: (i) the electrode materials partially peeled off from the conductive substrate due to the serious structural collapse after deep de-lithiation, leading to increased resistance; (ii) the electrophilic behavior of the de-lithiated materials were enhanced, favoring the adsorption of the hydroxyl group, yet over strong interaction hindered the electrocatalytic activity. This indicates that a relatively complete structure favors spent LIB materials as eligible catalysts.

Electrocatalytic oxygen production is a four-electron process with a higher reaction barrier than HER (two-electron process). This barrier serves as the rate-determining step in



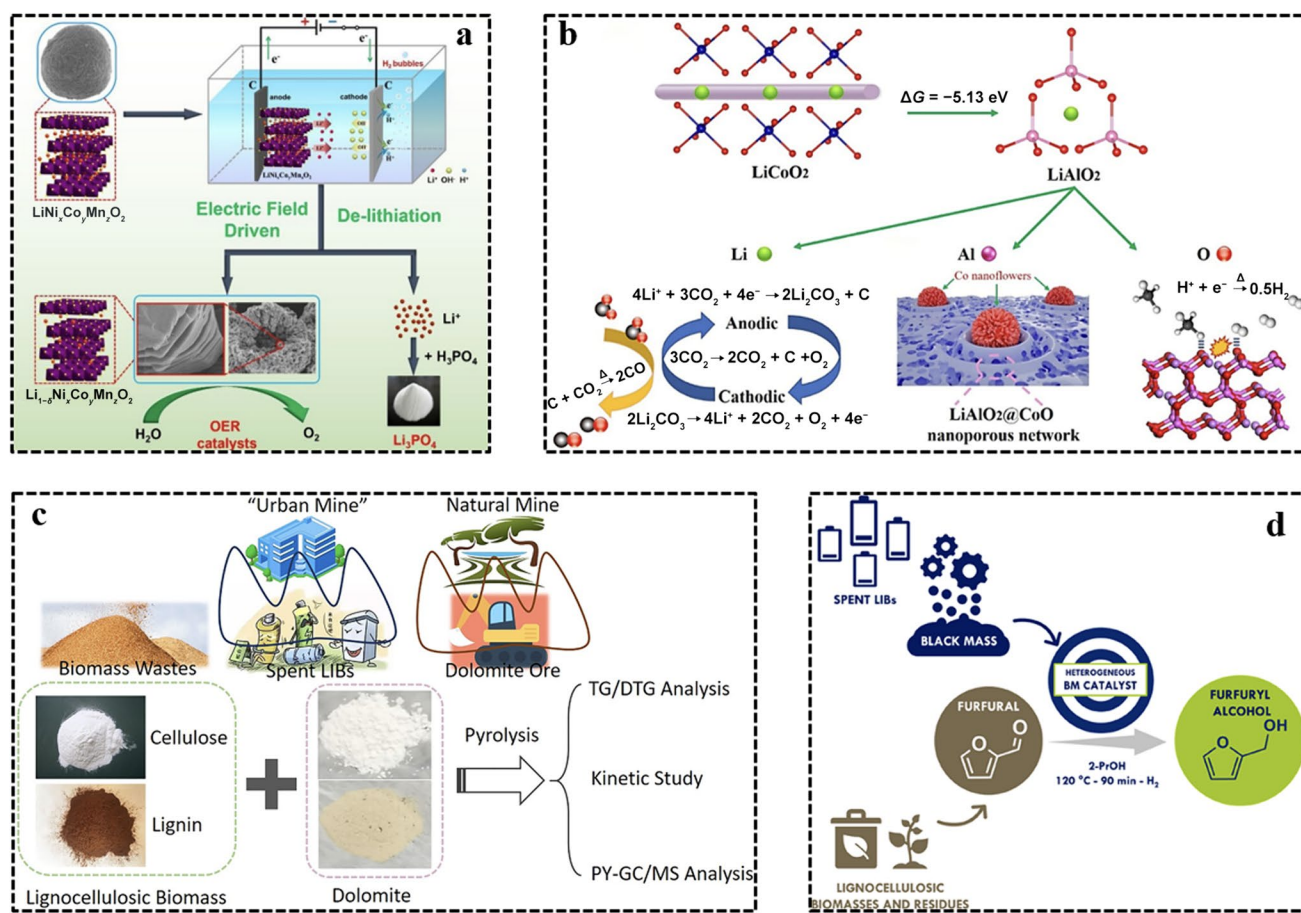
the overall water splitting. Accordingly, most research on the spent LIB electrode material-derived catalysts focuses on the catalytic performance of OER, leaving a research gap on the examples for HER, which is paramount in many fields. The commercial Pt/C catalyst exhibits excellent HER performance at a high cost. Thus, developing affordable and efficient HER catalysts is the premise of hydrogen production by water electrolysis. Waste LIB electrode materials with diverse valuable resources provide opportunities to prepare advanced HER catalysts, deserving more scholarly attention. Moreover, the in-depth mechanism of the OER and HER catalysts derived from spent LIBs remains inadequately explored. Furthermore, the research on the spent LFP recycling as catalysts is scarce. Additionally, its element cost is much lower than other LIBs, such as LCO and NCM, making pyrometallurgical or hydrometallurgical techniques to extract valuable elements unsuitable for spent LFP. The recycling path of spent LFP should be expanded, and converting it into catalysts to realize high-value applications is promising.

## 5.2 Syngas Preparation-Related Catalysis

Electrocatalytic CO<sub>2</sub> reduction syngas technology is effective in utilizing CO<sub>2</sub> resources and ideal for the sustainable synthesis of gas at room temperature, making it the current research hotspot based on the global targets for carbon neutrality [139, 140]. Materials recycled from spent LIBs can be used for hydrogen and oxygen preparation by water electrolysis and catalysis for the syngas preparation. For example, CO<sub>2</sub> can be converted into syngas (CO and H<sub>2</sub>) using catalysts for CO<sub>2</sub> reduction reaction and HER [141]. Some studies proposed new routes for the utilization of the recovered products to catalyze the preparation of syngas. These ideas help solve the problem of spent LIB recycling and promote effective CO<sub>2</sub> use, presenting great significance to achieving the “carbon peak and carbon neutral” [142, 143].

Based on the above endeavors, Wang et al. [144] studied the influence of metal ratio in the Li-Co-Mn-Ni on electrochemical performance. They studied the difference among pristine NCMs with various metal ratios. On this basis, they found that the NCM622 (Ni:Co:Mn = 6:2:2) exhibited the best performance on catalyzing OER with the lowest Tafel slope of 82.3 mV dec<sup>-1</sup> and the largest exchange current density of 0.215 mA cm<sup>-2</sup>. The recycled NCM showed a consistent Tafel area and slope, indicating that the proved beneficial performance of Li, Ni, and Co to OER activity varied; in addition, the NCM with a relatively high cobalt ratio performed better despite the decreased activity due to elevated ratio of Mn. The influence of Li and Ni was not elucidated. Besides, thermal treatment temperature, time, and atmosphere were also discussed, and it was demonstrated that the NCM performance could be improved by

proper heat treatment. The recycled material was applied as an anode catalyst in CO<sub>2</sub> electrolysis to produce CO, presenting a promising choice in industrial application with an excellent current efficiency of 97% under a high current density of 32 mA cm<sup>-2</sup> at 2.25 V and an energy efficiency of 63%. Yu et al. [145] recycled Al foils and LiCoO<sub>2</sub> electrode materials from waste LIBs as catalysts to convert wood chip pyrolysis gas into hydrogen-rich gas. The introduction of the Al element promoted the in-situ atomic replacement reaction, fixed the volatile lithium elements, and transformed LiCoO<sub>2</sub> into LiAlO<sub>2</sub> with a higher melting point. The perfect Co nanoflower structure and stable CoO nanopore network were improved under the substitution reaction, forming an in-situ assembly catalytic structure with enhanced adsorption capacity, in line with the Li-CO<sub>2</sub> battery system with an 11.31 mmol g<sup>-1</sup> hydrogen production rate and a 65.79% volume fraction, and the volume fraction of syngas (H<sub>2</sub> + CO) reached 91.82%. This marks a 90% improvement in the purity of the syngas prepared from Co-based catalytic materials for the first time. In addition, the in-situ assembled catalytic structure is eventually degraded to Co and LiAlO<sub>2</sub>, allowing for ready recycling through the sorting method and avoiding the pollution of heavy metals from the waste catalysts (Fig. 7b). Spent LIB recycling mainly centers on cathode and anode materials. However, other components (such as electrolytes) are also valuable to be recycled and will greatly threaten the environment without appropriate treatment. In recycling spent LIB cathode or anode materials, the residual electrolytes typically decompose thermally under high-temperature conditions, producing toxic gases. For this reason, reasonable treatment and utilization of the gas emitted during recycling is promising. Jung et al. [146] investigated the thermal decomposition behavior of the widely used battery electrolyte LiPF<sub>6</sub> in ethyl carbonate and ethyl methyl carbonate (EC/EMC = 1/2 by volume). LiPF<sub>6</sub> pyrolysis was validated to yield different gaseous products (H<sub>2</sub>, CO, CH<sub>4</sub>, C<sub>2</sub>H<sub>4</sub>, and CO<sub>2</sub>), which are difficult to separate. Based on the above analysis, finding an effective catalyst from the components of spent LIBs is significant for their reasonable recycling. In this context, the cathode material NCM 811 (LiNi<sub>0.8</sub>Co<sub>0.1</sub>Mn<sub>0.1</sub>O<sub>2</sub>) was found to be highly active for syngas formation and can be directly deployed as catalysts. This attribute mainly arises from the presence of Ni, Co, and Mn alloys (oxides), widely known as C–C, C–H, and C–O bond catalysts, respectively. At high temperatures, it shows the ability to convert the entire liquid compound into syngas (H<sub>2</sub> and CO). The synergistic action of the catalyst with CO<sub>2</sub> boosted CO generation. Given that the metallurgical process for battery operates at near 1300 °C, the thermolysis of battery electrolyte can be incorporated to maximize the recovery of organic and metallic compounds in spent batteries. However, the catalytic mechanism of cathode materials, e.g., NCM being directly used as catalysts for syngas formation,



**Fig. 7** **a** Schematic illustration of the electric field driven de-lithiation process for recycling the ternary  $\text{LiNi}_x\text{Co}_y\text{Mn}_z\text{O}_2$  electrode materials. Reproduced with permission from Ref. [138]. Copyright © 2020, Elsevier B.V. **b** Schematic illustration of the pyrolysis catalytic mechanism of sorption-enhanced in-situ-assembled porous structure. Reproduced with permission from Ref. [145]. Copyright © 2021,

Elsevier B.V. **c** Schematic diagrams of recycling spent ternary LIBs for the dolomite modification and the application. Reproduced with permission from Ref. [149]. Copyright © 2021, Elsevier Ltd. **d** Schematic illustration of the catalyst from spent LIBs for biomass-derived aldehydes and ketones. Reproduced with permission from Ref. [151]. Copyright © 2022, American Chemical Society

needs more in-depth studies to guide the follow-up research and practical application.

### 5.3 Biomass Conversion-Related Catalysis

In the context of the ongoing consumption of fossil fuel sources and increasing energy demand, it is urgent to find new energy sources. Biomass is vital in the energy market due to its high efficiency in pyrolysis for the preparation of desired syngas and bio-oil, electricity generation, and heat processing, in which catalysts play an important role [147]. Some examples demonstrated that recycled metal oxides from spent LIBs could be applied in biomass pyrolysis and conversion. Chen et al. [148] utilized spent ternary LIB cathodes to study the pyrolysis characteristics of cellulose and lignin, which showed good thermostability even at high temperatures ( $700^\circ\text{C}$ ). They added catalysts prepared from spent LIBs to the biomass through one-step (direct mixing)

and two-step (impregnation-drying) methods. The latter included citric acid leaching of the spent cathode material, mixing of the solution with biomass, and the mixture drying. Consequently, it improved the catalytic effect on biomass pyrolysis, prominently reduced the content of cellulose-derived anhydrosugars, and increased the ketone levels by virtue of dehydration and decarboxylation. This method has a high potential for biomass pyrolysis or gasification in promoting the catalytic cracking (i.e., hydrogen transfer) of lignin-derived phenols (tar surrogates) to hydrocarbons and aliphatics (e.g., ketones). Besides, Wang et al. [149] used the leaching solution derived from the spent ternary LIBs for the modification of dolomite (Do), which can catalyze biomass pyrolysis (Fig. 7c). The modified Do exhibited excellent performance in reducing the activation energy and upgrading the volatile products. For the cellulose and lignin pyrolysis, the activation energy was noticeably decreased from 201 and  $180 \text{ kJ mol}^{-1}$  to 80 and  $75 \text{ kJ mol}^{-1}$ , respectively. It

was ascribed to significant facilitation of the modified Do, which converts anhydrosugars into small-molecule components (e.g., ketones). In addition, changes occurred in the production of phenols (50% vs. 5.8%) and hydrocarbon (0.6% vs. 30.3%). This newly synthesized catalyst for biomass pyrolysis presents a good opportunity to valorize spent LIBs and biomass wastes. Different from the above examples, effective catalysts can also be prepared without the leaching process, which usually need the assistance of acids. Fuentes et al. [150] prepared a mixed oxide (Co/RZnO) by milling the recycled oxides ZnO (RZnO) from spent alkaline batteries and CoO (RCoO) from spent LIBs. The mixed oxides were used to investigate the chemical recycling of polyethylene terephthalate into bis(2-hydroxyethyl)ethylene terephthalate (BHET). The Co/RZnO showed excellent catalytic performance, which was attributed to the presence of weak and strong acid sites, its overall higher concentration of acid sites and the synergistic effect between  $\text{Co}_3\text{O}_4$  and ZnO. The yields of BHET monomer were 80% (Co/RZnO), 50% (RZnO), and 10% (RCoO), respectively.

The mixture of anodic and cathodic materials from mechanical shredding of spent LIBs is called “black mass (BM)”. The simple and crude use of hydrometallurgy and pyrometallurgy to recycle this material can cause a serious waste of resources since the carbon-based anode can be burned out due to high temperatures. A reasonable recycling design is necessary to avoid this waste and reuse the anode materials such as graphite rationally. Paone et al. [151] converted the BM into an efficient heterogeneous catalyst for the selective hydrogenation of biomass-derived furfural and various biomass-derived aldehydes and ketones (Fig. 7d). The BM was filtered to homogenize the particle sizes and remove solid impurities (e.g., Al and Cu pieces), ball milled, calcined under atmospheric conditions at 600 °C for 6 h to erase traces of binder materials, and reduced at 500 °C for 6 h under  $\text{H}_2$  flow to obtain the desired catalyst. Under the catalysis of the prepared catalyst, furfural could be fully converted into furfuryl alcohol, the sole reaction product, at 120 °C for 90 min in the presence of molecular hydrogen under batch conditions. These studies present new routes for recovering and utilizing spent LIBs as the catalysts for biomass decomposition and conversion. However, most examples are limited to hydrometallurgy or pyrometallurgy-like methods, weakening the advantages of the original structure of spent LIB materials.

In summary, we discussed the application of catalysts derived from spent LIBs in substance conversion, including electrolytic water splitting, syngas preparation, and biomass conversion, an interdisciplinary subject of energy and environment. Furthermore, the spent LIB material recycling as catalysts for substance conversion and the corresponding performance are shown in Table 2. Most proposed strategies are hydrometallurgy or pyrometallurgy-like types, i.e.,

extracting the useful elements (Ni, Co, and Mn) by acid leaching or conversion of the spent LIB cathode materials into metal oxides by calcinating and using the recycled compounds to synthesize desired catalysts. In principle, such strategies are more universally applicable and have the potential to reuse spent LIBs. Nevertheless, some intrinsically good properties of spent LIB materials for catalysis are lost in the rough recycling. In awareness of this deficiency, researchers have tried non-structurally destructive or low-structurally destructive strategies using spent LIBs materials as catalysts. These attempts present attractiveness and competitiveness and achieve comparable catalytic performance under certain circumstances. Despite these yields, such research is still lacking, highlighting the importance of exploring catalytic mechanisms on this basis.

## 6 Battery-Related Catalysis

With the ongoing advancement in new energy technologies, electrochemical energy storage devices with fast and convenient characteristics have attracted much attention. Different from traditional “rocking-chair” batteries, such as LIB and sodium-ion batteries, a variety of new-generation battery technologies, including LSBs, metal-air batteries, and fuel cells (power generation), are related to catalytic reactions [152–154]. Developing advanced catalysts is crucial for the performance improvement of these battery systems and has gained increasing attention and progress. For LSBs, the electrode catalysts mainly include metal-free catalysts (e.g., carbon-based materials and polymers) [155, 156], metal-based catalysts [157], and hetero-structure catalysts [158]. For metal-air batteries, in addition to precious metals and their oxides, carbon-based metal-free and transition metal-based materials are two kinds widely used as bifunctional catalysts for electrode reactions [159]. As for fuel cells, the commercial electrode catalyst is Pt/C, and non-noble metal catalysts are currently being developed for cost reduction and sustainability, targeting transition metals and their compounds [160]. In general, carbon-based materials and transition metal compounds are promising catalysts for the three kinds of battery technologies above.

The Li, Co, Ni, and Mn elements in spent LIB cathode materials, Al and Cu from current collectors, and graphite from anodes are related to the above catalyst materials with regard to transition metal compounds and carbon-based materials. Meanwhile, considering the unique crystal structures of existent commercial cathode materials, they merits potential catalytic activity, and the volume changes, defect sites, and strains in spent cathodes might promote the electro-catalytic kinetic process [161]. Additionally, the SG anode still preserves the fusion graphite structure after extended charging and discharging cycling and is qualified

to prepare advanced carbon materials, such as graphene, to support catalysts [162]. To sum up, the application of recycled products from spent LIBs to battery-related catalysis technology, such as LSBs, fuel cells, and metal-air batteries, is worth exploring with profits and feasibility. In this chapter, we will summarize and discuss its classification in detail.

## 6.1 LSB Related Catalysis

LSBs have become a competitive candidate for next-generation energy storage devices due to their high theoretical energy density and eco-friendly features of sulfur. Based on the  $S_8 + 16Li^+ + 16e^- \rightarrow 8Li_2S$  conversion reaction, LSBs exhibit a high theoretical capacity of 1 675 mAh g<sup>-1</sup> and an energy density of 2 567 Wh kg<sup>-1</sup>, which is five times higher than that of commercially available LIBs (387 Wh kg<sup>-1</sup> for LiCoO<sub>2</sub>/graphite batteries) [163]. Despite such a benefit, the fast capacity degradation stemming from the sluggish redox reaction kinetics and shuttle of fatal lithium polysulfides (LiPSs) hinder the implementation of LSBs [164]. Various rational design strategies have been proposed, involving inserting interlayers and introducing electrocatalytic sulfur host materials to solve or alleviate these issues. Manthiram's team [165] used interlayers to suppress the shuttle effect in 2012 by presenting a conductive multi-walled carbon nanotube paper between the cathode and the separator. The paper acted as a pseudo-upper current collector, improving the cyclability of LSBs, and its role is shown in Fig. 8a. On this basis, carbon-based, metal-based, and polymer-based interlayers have been extensively studied to ameliorate the electrochemical performance of LSBs.

However, the preparation methods of these functional materials are usually environmentally harmful, costly, and complicated with application barriers. Additionally, the abundant graphite and metal resources in spent LIBs present a good choice for the preparation of LSB catalysts and have received increasing attention. Based on the idea of turning waste into treasure, Xu et al. [166] prepared a functional interlayer to enhance polysulfide trapping and catalytic performance for LSBs by utilizing waste graphite recycled from spent LIB anode materials (Fig. 8b). The as-prepared SG showed more polar functional groups, defects, and porous structure compared to artificial graphite (AG) (Fig. 8c, d). Compared with AG, the SG possessed unique physical and chemical properties. For one thing, the porous structure and defects provided numerous adsorption sites to restrict soluble polysulfides. For another, the electrolyte decomposition introduced substantial polar functional groups on the graphite surface, facilitating polysulfide adsorption and electrolyte wetting. Transition metal elements can also anchor polysulfides, enhance electrical conductivity, and boost polysulfide conversion kinetics, such as Ni, Co, and Mn, which were introduced into SG owing to the cathode active

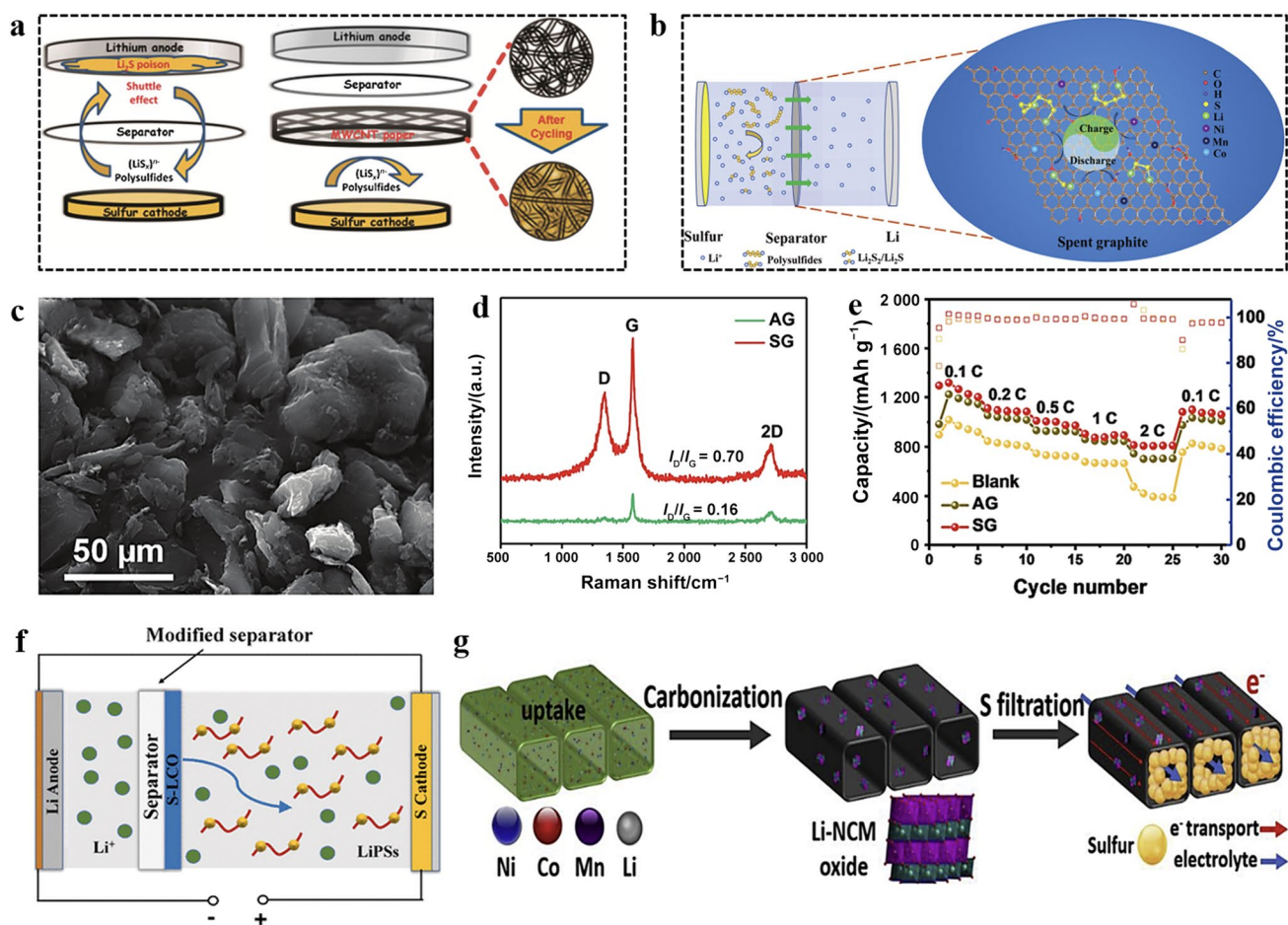
material dissolution. Accordingly, applying the SG-modified separators for LSBs achieved superior cycling stability (low capacity-decay of 0.08% per cycle over 500 cycles at 1 C). In addition, it exhibited excellent rate performance with high reversible specific capacities of 1 317 and 813 mAh g<sup>-1</sup> at 0.1 C and 2 C, higher than those of cells assembled with bare polypropylene and AG-modified separators (Fig. 8e).

Besides spent anode materials, cathode materials with unique layer structures are applicable to modify the LSB separators, as verified by Liu and co-workers [167]. In particular, the spent LiCoO<sub>2</sub> was coated on a commercial polypropylene separator (Fig. 8f), accelerating the redox reactions and suppressing the LiPS diffusion due to the spinel Co<sub>3</sub>O<sub>4</sub>. The assembled LSBs with spent LiCoO<sub>2</sub> delivered a high capacity retention of 74.68% at 1 600 mA g<sup>-1</sup> over 200 cycles and superior rate capability. In addition to the modification of the functional separator to improve the performance of LSBs, developing advanced sulfur host materials, such as carbonaceous materials and metallic compounds with exceptional attributes, is a popular strategy. Yang et al. [168] employed SG without complex treatment from spent LIBs for the LSB cathode. The SG/S cathode exhibited an initial discharge capacity of 1 377 mAh g<sup>-1</sup> at 0.2 C and outstanding cycling stability of capacity retention of 765 mAh g<sup>-1</sup> after 500 cycles with a decay rate of 0.006% per cycle. The electrochemical performance is enhanced since the SG surface possesses abundant functional polar groups and metal elements during repeated charging/discharging, displaying excellent electronic conductivity and promoting the LiPS conversion kinetics efficiently. With the goals of efficient recovery of the ternary cathode (Li-NCM) and the effective performance improvement of LSBs, Liu and colleagues developed a natural sphagnum uptake of spent Li-NCM-based LIBs as host to load sulfur, as shown in Fig. 8g [169]. The obtained cathode exhibited high sulfur ratios (64% of the total electrode and 80% of the active material mass); additionally, it benefited from the chemical encapsulation and hierarchical structural stabilization, delivering a good specific capacity of 700 mAh g<sup>-1</sup> after 300 cycles.

Considering the key scientific problems of the LiPS shuttle effect and the slow electrode reaction kinetics faced by LSBs, the functional modification of separators and the introduction of sulfur host materials from spent LIB cathodes and anodes were proposed to enhance the electrochemical performance. This field emerges with limited research, and the results obtained previously demonstrate its application prospects with in-depth development, such as combination with other LSBs for traditional catalysts and advanced treatment of spent cathode and anode materials to prepare graphite-supported metallic compound catalysts by direct mixing. These studies have been well-designed to convert spent LIB materials into catalysts, enabling reasonable use

**Table 2** Recycling of spent LJB materials for substance conversion catalysts and corresponding performance

Spent material types		Regenerative methods		Catalyst	Application	Performance	References
LiCoO <sub>2</sub>		Electrochemical activation		Li <sub>1-x</sub> CoO <sub>2</sub>	OER	Delivering a current density of 9.68 mA cm <sup>-2</sup> at 1.65 V after 500 cycles	[126]
LiCoO <sub>2</sub>		Leaching and calcination		HT-LiCoO <sub>2</sub>	OER	Delivering a higher anodic peak potential of 0.35 V	[128]
LiCoO <sub>2</sub>		In situ positive-bias driven exfoliation		CoOOH nanosheet	OER	Delivering a low Tafel slope of 53.8 mV dec <sup>-1</sup> and a small overpotential of 305 mV at 10 mA cm <sup>-2</sup> after 65 h long-term electrolysis	[129]
LiFePO <sub>4</sub>		Electrochemical transformation		NiFeO <sub>x</sub> H <sub>y</sub>	OER	Delivering a low overpotential of 285 mV at 10 mA cm <sup>-2</sup> and a small Tafel slope of 45 mV dec <sup>-1</sup> well-maintained for 14 h	[133]
LiNi <sub>1-x-y</sub> Mn <sub>x</sub> Co <sub>y</sub> O <sub>2</sub>		Electrodeposition		NiCoMn layered triple hydroxides	OER and HER	Delivering a low voltage of 1.583 V to drive 10 mA cm <sup>-2</sup> for the wastewater electrolysis	[135]
LiNiCoMnO <sub>2</sub>		One-pot boriding method		NiCoMnBs	OER	Delivering an overpotential of 372 mV at 500 mA cm <sup>-2</sup> , remained stable for 12 h running	[136]
LiNi <sub>1-x-y</sub> Mn <sub>x</sub> Co <sub>y</sub> O <sub>2</sub>		Acidic leaching, precipitation, hydrothermal and calcination		MnCo <sub>2</sub> O <sub>4</sub>	OER	Delivering an overpotential of 358 and 400 mV at 5 and 10 mA cm <sup>-2</sup>	[120]
LiNi <sub>0.5</sub> Mn <sub>0.3</sub> Co <sub>0.2</sub> O <sub>2</sub>		Mechanochemical activation method		Ni <sub>0.5</sub> Mn <sub>0.3</sub> Co <sub>0.2</sub> (OH) <sub>2</sub>	OER	Delivering an overpotential of 280 mV at 10 mA cm <sup>-2</sup>	[137]
LiCoO <sub>2</sub>		Thermal treatment		LiAlO <sub>2</sub> @CoO	Convert wood chip pyrolysis gas into hydrogen-rich gas	The yields and volume fractions of H <sub>2</sub> are 11.31 mmol g <sup>-1</sup> and 65.79%, and the volume fraction of synthetic gas reaches 91.82%	[145]
LiNi <sub>0.8</sub> Co <sub>0.1</sub> Mn <sub>0.1</sub> O <sub>2</sub>		Thermal treatment		LiNi <sub>0.8</sub> Co <sub>0.1</sub> Mn <sub>0.1</sub> O <sub>2</sub>	Syngas formation using CO <sub>2</sub> -assistance	Highly active for syngas formation ≤ 500 °C	[146]
LiNi <sub>1-x-y</sub> Mn <sub>x</sub> Co <sub>y</sub> O <sub>2</sub>		Acidic leaching and calcination		Ni, Co, Mn-modified dolomite	Biomass pyrolysis	Decreasing the apparent activation energy for cellulose and lignin pyrolysis, inhibiting the production of phenols and enhancing the production of hydrocarbons	[149]
LiCoO <sub>2</sub>		Acidic leaching and calcination		Co/RZnO	Glycolysis of poly(ethylene terephthalate)	The catalytic efficiency reached 80%	[150]
LiNi <sub>1-x-y</sub> Mn <sub>x</sub> Co <sub>y</sub> O <sub>2</sub>		Calcination		Ni-Mn-Co oxides	Reductive upgrading of biomass derived furfural	Complete conversion of furfural into furfuryl alcohol is achieved after 90 min at 120 °C under 10 <sup>6</sup> Pa H <sub>2</sub> in 2-propanol	[151]



**Fig. 8** **a** Schematic cell configuration of rechargeable LSBs without & with interlayer. Reproduced with permission from Ref. [165]. Copyright © 2012, The Royal Society of Chemistry. **b** Schematic of LSBs assembled with spent-graphite-modified separator; **c**, **d** SEM and Raman spectra of AG and SG; **e** the rate performance from 0.1 to 2 C of Li-S batteries with different separators. Reproduced with permission from Ref. [166]. Copyright © 2021, The Royal Society of

Chemistry. **f** Schematic diagram of separator modification by spent LiCoO<sub>2</sub>. Reproduced with permission from Ref. [167]. Copyright © 2022, American Chemical Society. **g** Schematic diagram of a naturally sphagnum uptake of spent Li-NCM based LIBs as host to load sulfur. Reproduced with permission from Ref. [169]. Copyright © 2019, Elsevier Ltd

of the inherent catalytic properties of those materials failed in LIBs. Pertinent research in this field is encouraged.

## 6.2 Fuel Cells Related Catalysis

Fuel cells as an energy conversion device with high power generation efficiency (theoretically 85%–90% without restricted by the Carnot cycle), environmentally friendly, high energy density and wide source of fuel, are considered the fourth-generation power generation technology to convert chemical energy into electrical energy, following hydro, thermal, and nuclear power. Typically, the fuel cell is composed of a cathode, anode, electrolyte, and external circuit. The oxygen reduction reaction (ORR) at the cathode with a high energy barrier determines the system kinetics. Developing advanced catalysts to reduce energy consumption is

the cornerstone of the large-scale commercial application of fuel cells. Pt-based catalysts with excellent catalytic activity are popular in fuel cells [170, 171]. Cui et al. [172] tuned the catalytic activity of Pt catalysts by utilizing the widely tunable lattice constant of LIB electrode materials as the catalyst support (Fig. 9a). Modifying the electronic structure of the catalyst can improve activities. In contrast, either compressive or tensile, the lattice strain can alter the surface's electronic structure and upgrade the catalyst activities. During the charging/discharging process, LIB electrode materials undergo volume changes by depositing small Pt nanoparticles onto the LiCoO<sub>2</sub> or Li<sub>0.5</sub>CoO<sub>2</sub> substrate surfaces and controlling the charging and discharging states of these substrates. Consequently, the ORR activities of Pt nanoparticles in an alkaline solution achieved approximately 90% improvement or more than 40% decrease under compressive

and tensile strain, respectively. However, the scarcity and high cost of Pt resources limit its further large-scale application, presenting an urgent need to explore alternatives.

To improve the added value of end-of-life LIBs, Liivand et al. [173] used spent LIB graphite as a precursor material for preparing graphene oxide, followed by doping to obtain nitrogen-doped graphene. It was found that the nitrogen-doped graphene from the spent LIBs showed higher electrocatalytic activity toward ORR than commercial nitrogen-doped graphene. This is attributed to the increased content of active nitrogen species and the presence of carbon vacancies on the graphene surface. Specifically, the ORR onset potential for the nitrogen-doped graphene prepared by the spent LIBs and the commercial nitrogen-doped graphene were 0.867 V and 0.797 V, respectively. After injecting 3 mol L<sup>-1</sup> methanol into the O<sub>2</sub>-saturated 0.1 mol L<sup>-1</sup> KOH solution, the current of the experimental sample exhibited a smaller decrease than the commercial one (16.5% vs. 33%), indicating that the spent LIB-derived nitrogen-doped graphene has a better catalytic long-term performance. Warczak et al. [174] proposed a hydrogen peroxide (H<sub>2</sub>O<sub>2</sub>) generation method using the leached LIB waste powder as the catalyst, showing higher electrocatalytic activity toward ORR than the unmodified glassy carbon. When assembled at a liquid-liquid interface, the waste powder increased the efficiency of H<sub>2</sub>O<sub>2</sub> generation by about 20 times. The H<sub>2</sub>O<sub>2</sub> has been applied as a fuel and oxidant in fuel cells [175, 176], suggesting that the as-prepared catalyst has the potential to be applied in fuel cells. Besides, Ruan and colleagues [177] prepared graphene nanosheets using SG anode from LIBs via a low-cost and green synthesis route (Fig. 9b). Especially, oxidation efficiency was improved by introducing a 5:1 mixture of H<sub>2</sub>SO<sub>4</sub>/H<sub>3</sub>PO<sub>4</sub> and increasing KMnO<sub>4</sub> content in the graphite recycled from spent LIBs. Subsequently, high-quality graphene was obtained through a combined method of glucose reduction and annealing. The spent LIB-derived nitrogen-doped graphene exhibited favorable activity and stability for ORR, better than the Pt/C (Fig. 9c). The activity of nitrogen-doped graphene degraded about 7%, lower than that of the Pt/C catalyst (near 20%) in the durability test. Ruan's group [178] also prepared Fe-N-doped carbon catalyst for ORR by recycling graphite anode from spent LIB. The SG recycled from spent LIB anodes was used as a carbon carrier and doped with N and Fe via simple pyrolysis with polyaniline and iron salt. As a result, this catalyst displayed excellent ORR catalytic activity in 0.1 mol L<sup>-1</sup> KOH solution with an onset potential of 0.91 V vs. RHE and a half-wave potential of 0.8 V vs. RHE. Under the same conditions, the durability and methanol resistance of the as-prepared Fe-N-doped carbon catalyst from spent LIBs exceeded those of a 20%Pt/C commercial catalyst. Furthermore, the prepared catalyst had better ORR catalytic stability than the commercial 20%Pt/C, and they maintained initial

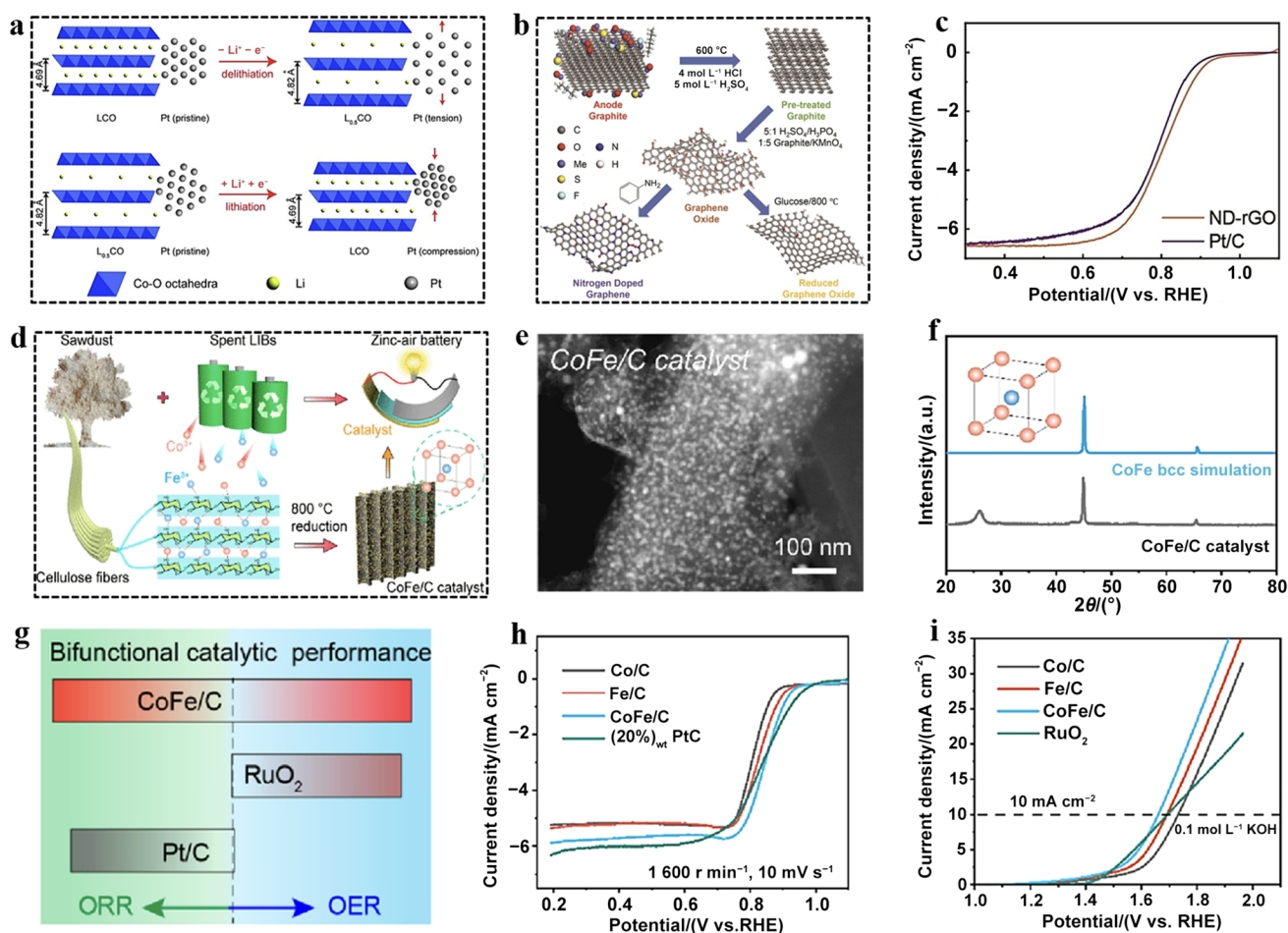
currents of 93% and 82% after running at a fixed potential of 0.38 V for 36 000 s.

The above findings indicated that the recycled products from spent LIB anodes can be transformed into catalysts for the ORR and applied to the catalysis for fuel cells. On the bright side, the affordable spent anode graphite is mainly used as ORR reaction catalysts for fuel cells in these samples, achieving the high-value recycling of the resource. Notably, recycling spent cathode as catalysts for ORR remains a research gap. To realize "closed-loop" recycling, more attention should be directed to the waste cathode materials, which contain high-value metals and can be used as precursors to prepare metal-based catalysts for fuel cells. For example, Ruan and colleagues proposed the employment of iron salt to synthesize the desired catalyst [178]. The spent LFP is rich in iron, presenting the potential of applying the iron in LFPs to replace the iron salt.

### 6.3 Metal-Air Battery-Related Catalysis

As an emerging battery technology with a high theoretical energy density and safety, metal-air batteries, consisting of metal anode and air cathode [179], have received more attention. The sluggish kinetics process of ORR and OER at the air cathode hinders its further large-scale application. Developing bifunctional catalysts with high activity for ORR/OER is crucial for improving the performance of metal-air batteries [180, 181]. The excellent performance of transition metal-based catalysts (e.g., Co, Ni, Fe, and Mn) for OER/ORR has been proved. LIB electrode materials with abundant transition metals can act as bifunctional electrocatalysts or catalyst precursors for metal-air batteries such as Zn-air and Li-air batteries. Manthiram et al. [182] have reported that LiCoO<sub>2</sub> synthesized at 400 °C with a spinel structure exhibited superior OER and ORR activity and relatively long service life, making it suitable to be a bifunctional electrocatalyst for rechargeable metal-air batteries. In 2020, Jin et al. [183] also used the LFP materials as Fe and P sources to react with ZIF-8 for the preparation of Fe-N-P co-doped carbon nanotube encapsulated Fe<sub>2</sub>P nanoparticles (C-ZIF/LFP) for efficient ORR. The C-ZIF/LFP catalyst showed superior ORR activities under alkaline and acidic conditions. It achieved a high half-wave potential of 0.74 V in acidic electrolytes, a half-wave potential of 0.88 V in alkaline electrolytes, and a peak power density of 140 mW cm<sup>-2</sup> in Zn-air batteries. The above analysis indicated that the LiCoO<sub>2</sub> and LFP electrode materials can act as precursors to prepare metal-air battery catalysts, delivering superior performance.

Spent LIB electrode materials with valuable transition metals have gained growing attention for catalysis in metal-air batteries. Our team has conducted studies based on the zinc-air battery catalysts and the reuse of spent LIBs [184,



**Fig. 9** **a** Schematic of the lattice constant change of LCO substrates and how the lattice strains are induced to Pt NPs. Reproduced with permission from Ref. [172]. Copyright © 2016, American Association for the Advancement of Science. **b** Preparation process of the nitrogen doped graphene and reduced oxide; **c** LSV of ND-rGO at 1 600 r min<sup>-1</sup> and scanning rate of 0.005 V s<sup>-1</sup> as compared to the Pt/C. Reproduced with permission from Ref. [177]. Copyright

© 2021, Wiley-VCH GmbH. **d** Schematic diagram of design of the CoFe/C catalyst from spent LIBs; **e–g** STEM image, XRD spectrum and related crystal structure, and the bifunctional catalytic performance of the CoFe/C catalyst, respectively; **h, i** ORR curves and OER polarization curves of the related catalysts. Reproduced with permission from Ref. [184]. Copyright © 2022, American Chemical Society

[185]. We reported a highly efficient bifunctional CoFe/C catalyst for zinc-air batteries using sawdust as the hosting agent to anchor recycled Co and Fe from spent LIB cathode materials, followed by simple carbonization (Fig. 9d) [184]. The as-prepared CoFe/C catalyst showed uniformly dispersed CoFe nanoparticles on the sawdust-based carbon after annealing (Fig. 9e) due to the hydroxyl groups in sawdust and electrostatic attraction between the Fe<sup>3+</sup>/Co<sup>3+</sup> cations. The electron redistribution in the CoFe/C catalyst induced by the Fe atoms were all isolated into single sites by the Co atoms (Fig. 9f), contributing to the consistent ORR/OER performance of CoFe/C with the commercial catalysts (Fig. 9g). When using as-prepared CoFe/C as the ORR and OER catalyst, it delivered a 0.85 V half-wave potential and a

1.66 V overpotential at 10 mA cm<sup>-2</sup> (Fig. 9h, i). The assembled zinc-air batteries with CoFe/C catalyst on the cathode showed a noticeably large power density of 199.2 mW cm<sup>-2</sup> and a long cycling stability of 350 h. Moreover, we developed a rapid thermal radiation process through rational design to prepare the NiMnCo-based catalyst from spent LiNi<sub>1-x-y</sub>Mn<sub>x</sub>Co<sub>y</sub>O<sub>2</sub> cathodes for highly efficient zinc-air batteries (Fig. 10a) [185]. The as-prepared NiMnCo-activated carbon catalyst exhibited a unique core-shell structure involving spinel NiMnCoO<sub>4</sub> in the shell and face-centered cubic Ni in the core with the redistributed electronic structure of NiMnCoO<sub>4</sub> to decrease the energy barrier for OER/ORR. The corresponding characterizations and simulation structure are shown in Fig. 10b–d. The synergistic effect



between the NiMnCoO<sub>4</sub> and the Ni core was proved by the density functional theory calculations. It was elucidated that the NiMnCoO<sub>4</sub> shell provided efficient active sites for the ORR/OER processes, and the Ni core redistributed the NiMnCoO<sub>4</sub> shell electronic structure (Fig. 10e, f). In the case of zinc-air battery cathode catalyst, the obtained NiMnCo-activated carbon catalyst delivered a low voltage gap of 0.72 V at the initial three cycles, high power density of 187.7 mW cm<sup>-2</sup>, and superior cycling stability of 200 h at 10 mA cm<sup>-2</sup> (Fig. 10g–i). These results provide an economical and environmentally friendly way for spent LIB disposal and metal-air battery development.

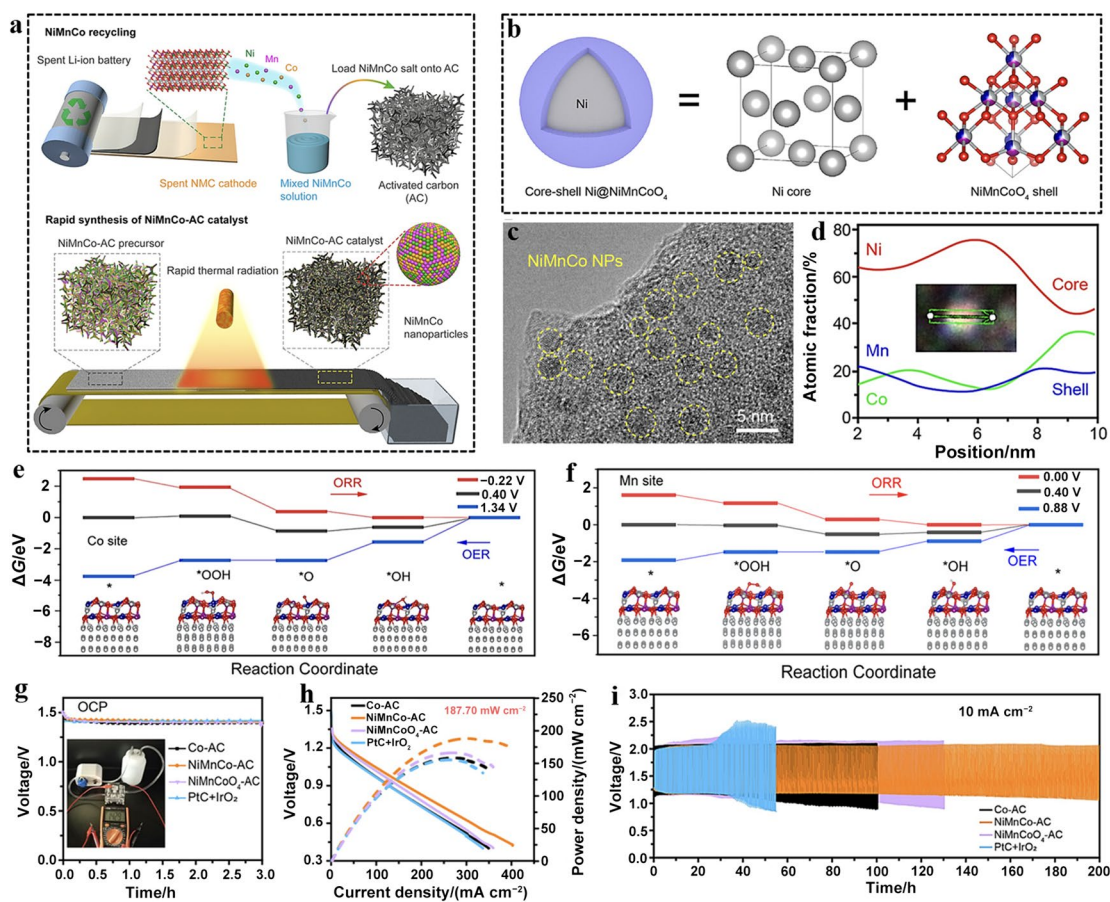
Wei et al. [186] also recycled Ni-Co-Mn oxides from spent LIBs to prepare bifunctional air electrodes, which realized 100% regeneration of Co, Ni, and Mn from the spent cathodes via a thermal treatment. Additionally, the Ni-Co-Mn oxides changed from an  $\alpha$ -NaFeO<sub>2</sub>-type structure to a spinel one after being heated at 600 °C. The regenerated Ni-Co-Mn oxides showed excellent bifunctional catalytic activities towards OER and ORR in aqueous KOH electrolyte; when applied to a zinc-air battery cathode, their calculated energy efficiency was approximately 75%. Yang et al. [187] reported an ultrafast method to regenerate LiCoO<sub>2</sub> from spent LIBs into the carbon layer/Co<sub>3</sub>O<sub>4</sub> cathode for rechargeable zinc-air batteries. The spent LiCoO<sub>2</sub> was converted into nanosized Co<sub>3</sub>O<sub>4</sub>, and the cathode polymer binder (such as PVDF) was carbonized into a graphitized carbon layer after ultrafast high-temperature shock treatment. The graphitized carbon layer enhanced the electronic conductivity, and the nanosized Co<sub>3</sub>O<sub>4</sub> boosted active sites. Consequently, the as-prepared carbon layer/Co<sub>3</sub>O<sub>4</sub> catalyst delivered efficient catalytic activities, exhibiting a low OER overpotential of 245 mV at 10 mA cm<sup>-2</sup>, and the ORR onset potential reached 0.90 V. Furthermore, the assembled aqueous zinc-air battery displayed high power density (131 mW cm<sup>-2</sup>) and excellent cycling durability. The above representative reports have laid a foundation for the application of waste LIB electrode materials in advanced metal-air batteries. On this basis, a growing body of research, such as innovative synthesis methods, in-depth mechanism exploration, and excellent energy storage performance investigation, will arise.

To meet the increasing demand for energy supply and environmental quality requirements in the context of refined social civilization, various advanced energy storage technologies beyond LIBs are developed and await extensive application. This chapter concludes the latest progress of spent LIB electrode materials for battery-related catalysis, including LSBs, fuel cells, and metal-air batteries. They can solve the problems of environmental damage caused by improper disposal of end-of-life LIBs and improve the electrochemical performance of the waste effectively to improve its practical

value. The recycling of spent LIB electrode materials for battery-related catalysis and the corresponding performance are summarized in Table 3.

Currently, calcination and acid leaching are the main methods for battery-related catalyst preparation. Considering high energy consumption and the risk of secondary pollution, greener regeneration methods have become the focus of future research. Some studies pioneeringly proposed the rational use of spent LIB materials by simplifying the recycling process and maximizing the structural and elemental advantages of failed materials. Despite these insightful contributions, many important issues remain. For example, the assumption that the defects in spent materials serve as sites promoting the catalytic performance lacks experimental evidence, deserving elaboration, and advanced characterizations.

Furthermore, impurities in spent LIB materials may affect the intrinsic or apparent performance of batteries. For example, the unknown impurity quantity interferes with the quantification of the active substance in the electrode, hindering the determination of the actual properties of the active materials. In addition, the impurities influence the electric conductivity of the catalysts or electrodes, impacting the charge transfer and the reaction kinetics. Moreover, the potential effect of the catalyst surface impurities on the gas diffusion layer can change the gas adsorption and desorption rates, leading to variations in the reaction rate. The unremoved impurities such as binder (e.g., PVDF) may improve the catalytic performance by retarding the dissolution of the prepared catalysts from spent LIBs [83]. The binder can also be rationally utilized to improve catalyst performance; for instance, Yang et al. [187] carbonized it to enhance product conductivity. These examples infer that the impurities can be turned into treasure, as discussed in Sect. 2. New impurities introduced during recycling also have a potential impact on battery performance. Zheng et al. [188] realized the importance of this aspect and studied the effects of sulfide introduced during hydrometallurgical recycling on the synthesized NCM622 cathode materials. The findings indicated that the sulfide impurity had a limited impact on the battery performance. Such studies can guide the screening of suitable reagents in recycling. However, research in this regard is lacking. Additionally, the number of impurities differs and cannot be controlled. This means that despite the consequence of impurities, it is difficult to ensure the batch uniformity of the products, hampering large-scale production. In this sense, the two directions of fine sorting and utilizing various spent LIB components need to be developed in tandem. The mechanism of impurities in catalysts affecting the performance of batteries remains



**Fig. 10** **a** Schematic of the fabrication process of the NiMnCo-AC catalyst from spent LIBs; **b** identified core-shell structure of the NiMnCo nanoparticle; **c**, **d** HRTEM image and line-scan profiles of the NiMnCo-AC catalyst; **e**, **f** Gibbs free energy diagrams of ORR/OER on the Co sites and Mn sites of Ni(111)@NiMnCoO<sub>4</sub>(110); the elec-

trochemical performance of ZABs with various catalysts; **g** the open-circuit potential of primary ZABs at the initial 3 h; **h** the *i*-*v* polarization and power density curves of ZABs; **i** cycling performance of ZABs at the current density of 10 mA cm<sup>-2</sup>. Reproduced with permission from Ref. [185]. Copyright © 2022, the Author(s)

underexplored, and its in-depth discussion will aid the effective utilization of components and the analysis of the catalyst failure mechanism.

Besides, the quantity of defects or the degree of degradation of spent LIB materials is not controllable for the decommissioned batteries. For this reason, the strategies relying on the original properties of spent LIB materials may exhibit limited versatility. By contrast, methods with structurally destructive properties, such as pyrometallurgy and hydrometallurgy, may ignore the different states of raw materials. The reason for this is that they primarily extract valuable elements into metallic compounds and use them for subsequent synthesis. In other words, for the battery material recovery in different states as catalysts, hydrometallurgy, and pyrometallurgy methods can ensure the product purity. For the strategies that rely on the initial structure of the spent LIB materials, the application of such methods needs strict classification of raw materials, putting forward requirements for the spent battery classification of the recycling industry

chain upstream. In addition, developing the evaluation and detection technology of the spent battery status is also necessary to improve the recycling efficiency in the industrial chain downstream. It is recommended to distinguish between different types and states of spent batteries before the recovery processes. Generally, developing highly versatile strategies and effectively utilizing the advantage of failed materials still need significant endeavors.

## 7 Limitations on Recycling Spent LIB Materials for Catalytic Applications

The examples above suggest that recycling spent LIB materials for catalytic purposes is feasible and promising. However, this path has some limitations, reminding researchers to continually upgrade recycling technologies and expand their applications.

**Table 3** Recycling of spent LIB materials for battery-related catalysts and corresponding performance

Spent material types	Regenerative methods	Catalyst	Application	Performance	References
Graphite	Without further treatment	Graphite	Li-S batteries (separator)	968 mAh g <sup>-1</sup> with a low decay rate of 0.08% per cycle over 500 cycles at 1 C	[166]
LiCoO <sub>2</sub>	Crystal-nondestructive process	S-LCO (LiCoO <sub>2</sub> +Co <sub>3</sub> O <sub>4</sub> )	Li-S batteries	74.68% capacity retention over 200 cycles at 1 600 mA g <sup>-1</sup>	[167]
Graphite	Without further treatment	Graphite	Li-S batteries (sulfur host)	765 mAh g <sup>-1</sup> with a low decay rate of 0.006% per cycle over 500 cycles at 0.5 C	[168]
LiNi <sub>x</sub> Co <sub>y</sub> Mn <sub>z</sub> O <sub>2</sub>	Carbonization	Li-NCM oxide	Li-S batteries	700 mAh g <sup>-1</sup> after 300 cycles	[169]
Graphite	Thermal treatment	NG-Bat (nitrogen-doped graphene)	Fuel cells	ORR onset potential reached 0.867 V, and had a better catalytic long-term performance	[173]
Graphite	Acidic leaching and calcining	Graphene nanosheets	Fuel cells	Onset potential of 0.91 V, half-wave potential of 0.81 V and limiting current density of 6.6 mA cm <sup>-2</sup> , with a better catalytic stability than Pt/C	[177]
Graphite	Pyrolysis with polyaniline and iron salt	Fe-N-doped carbon	Fuel cells	Onset potential of 0.91 V and half-wave potential of 0.8 V, and had a better ORR catalytic stability than commercial 20%Pt/C	[178]
LiCoO <sub>2</sub> and LiFePO <sub>4</sub>	Acidic leaching and calcining	CoFe/C	Zinc-air batteries	Half-wave potential of 0.85 V, overpotential of 1.66 V at 10 mA cm <sup>-2</sup> , and power density of 199.2 mW cm <sup>-2</sup> with a long cycling stability of 350 h	[184]
LiNi <sub>1-x-y</sub> Mn <sub>x</sub> Co <sub>y</sub> O <sub>2</sub>	Acid leaching and radiative heating processes	NiMnCo-activated carbon (NiMnCo-AC)	Zinc-air batteries	High power density of 187.7 mW cm <sup>-2</sup> and superior cycling stability of 200 h at 10 mA cm <sup>-2</sup>	[185]
LiNi <sub>x</sub> Co <sub>y</sub> Mn <sub>z</sub> O <sub>2</sub>	Alkali leaching and calcining	Ni-Co-Mn oxides	Zinc-air batteries	Energy efficiency reached 75%	[186]
LiCoO <sub>2</sub>	High temperature shock process	Carbon layer/Co <sub>3</sub> O <sub>4</sub> composite	Zinc-air batteries	ORR onset potential reached 0.90 V and high power density of 131 mW cm <sup>-2</sup>	[187]

First, converting spent LIB materials into catalysts has limitations in element types. The possibility of such conversion is limited by the original material elements (mainly including Li, Ni, Co, Mn, Fe, Al, Cu, O, P, and C) and structure. Although it can be modified by introducing other elements (such as N), this path is less applicable than direct synthesis. The resynthesis after precise extraction of each element can solve this problem, but this approach sacrifices the structural advantages of the spent LIB materials that are conducive to catalysis. Second, given that the catalyst dosage is much smaller than that of electrode materials in production and application, converting all the spent materials into catalysts is impractical. It is more suitable for treating those materials that are difficult to handle with conventional recycling strategies such as hydrometallurgy or pyrometallurgy. In addition, the “LIB to LIB” path, namely the resynthesis or regeneration of spent LIB materials into new LIB materials, can be repeated to form a closed loop by adjusting the recycling process within a reasonable range. In terms of the path of “LIBs to catalysts”, after the catalysts recycled from spent LIB materials are deactivated, advancing new technologies to restore their activity or recycle them for other purposes is necessary, and the recycling of such catalysts presents a scarcity of research.

## 8 Conclusion and Perspective

The rise of electronic and electric devices such as mobile phones and EVs has increased the demand for rechargeable batteries with high capacity, suitable size, and weight. Among different rechargeable batteries, LIBs stand out due to their high energy density, low self-discharge, and prolonged lifespan, displaying wide application in various fields. In the context of falling global crude oil reserves, people pay more attention to environmental issues. EVs will gradually replace gasoline vehicles, boosting the demand for LIBs. It has been expected that each batch of power batteries will usher in the renewal, leading to a mass of end-of-life LIBs for recycling. Researchers have been dedicated to developing battery recycling technologies in response to this situation. To satisfy growing global energy demand and accomplish sustainable energy development goals, using the recovered products of spent LIBs in preparing catalysts in academia and industry is promising.

With appropriate recycling approaches, the waste materials can be recovered as metals and compounds or reutilized as functional materials such as catalysts for various applications. Regarding the application of spent LIB recycling in catalysis, this paper reviewed it in three main aspects: pollutant degradation catalysis, substance conversion catalysis,

and direct application of spent LIB recycled products in new battery-related catalysis. Some research studies demonstrated that the catalytic capacity of the recovered cathode or anode materials even exceeded that of the commercial catalysts after modification (Table 4). Due to chemical reactions and physical changes in the battery charging and discharging process, some recycled products without modification could also have good catalytic performance for specific catalytic reactions. The application of battery recycling in catalysis is insightful. In other words, it can be extended to other areas, and the recovered materials' properties in specific aspects may be better than the traditional ones with measurable treatments.

The high-value recovery of spent LIBs for catalyst application is promising, and more breakthroughs in this area will arise. Research on LIB recycling is still limited, leaving many crucial issues unsolved. The remaining challenges and perspectives are summarized as follows (Fig. 11):

- I. Development of recycling strategies for the whole LIB components. Currently, the research of LIB recycling mainly involves the regeneration and utilization of cathode materials using pyrometallurgy, hydrometallurgy, and direct recovery, including  $\text{LiCoO}_2$ ,  $\text{LiMn}_2\text{O}_4$ , LFP, and  $\text{LiNi}_x\text{Co}_y\text{Mn}_z\text{O}_2$ . The recycling of other components of the batteries, such as anode, electrolyte, separator, and current collector, is neglected and should be highlighted due to their unique values. The high-purity Cu and Al foils used in current collectors can be recycled and used in metallurgy to prepare alloy materials or reused for current collector productions. For the SG anode with good carbon matrix structure and electrical conductivity, its recycling for advanced carbon material synthesis is promising. The electrolyte contains considerable organic solvents, inorganic salts, and additives, which can be recycled to synthesize chemicals and are environmentally friendly. In this sense, developing advanced technologies to recycle whole LIB components is a research direction and an important way to realize a circular economy.
- II. National policy and industrial standard formulation. After decades of development, the LIB industry has mature laws and regulations to ensure its reasonable operation. In contrast, the spent LIB recycling market is at a disruption stage due to the lack of relevant management and industry standards. For this reason, a unified standard formulation is necessary to ensure the sustainable development of the battery recycling industry. The corresponding policies and regulations should include the following principles: governments should create incentives and subsidies to encourage sustainable recycling, and the industry should

set purity standards for recycled products and strict requirements for the treatment of pollutants generated in this process.

- III. Recycling process customization for various cathode materials. Cathode materials have different cost values due to the difference in their preparation technologies and composition. Typical recycling technologies, such as pyrometallurgy and hydrometallurgy, use high-temperature calcination and acid leaching. They are characterized by huge energy consumption and high environmental risk, making them unsuitable for all kinds of cathode materials. For example, the economic benefits of either pyrometallurgical or hydrometallurgical recovery are low since its processing spending is higher than the material value (even the affordable  $\text{LiFePO}_4$  and  $\text{LiMn}_2\text{O}_4$ ). Additionally, cathode materials contain high-value metals (e.g., nickel and cobalt), which can be economically feasible using typical processes. Developing direct recovery technology is novel to reduce cycling costs. Hence, cost control should be an important index of battery recycling technology, and this cost should be lower than the value of the recycled products to promote the development of this technology. Customizing different recycling processes for various cathodes is an important prerequisite for intelligent recycling in the future.
- IV. Application expansion of recycled materials. The mainstream application of the spent LIBs after recovery is the reparation of electrode materials. Despite the insightful catalysis usage reviewed in this article, the application of battery-recycled products is limited. With the development of battery recycling technology, recycled products should be applied to more fields, such as medical apparatus and instruments, intelligent manufacturing, ironmaking, and steelmaking.
- V. Technology development beyond LIBs. LIBs occupy the major power battery and energy storage battery markets, and developing sustainable recycling methods is effective in solving the environmental risks and resource waste due to substantial end-of-life LIBs. In response to resource shortages and growing market demands, advanced energy storage technologies can be developed, including sodium/potassium-ion, lithium/sodium-sulfur, and metal-air batteries. These electrochemical energy storage devices can be employed in combination with LIBs or alone. Furthermore, they present diversified, safe, and green alternatives for energy supply and promote the sustainable development of new energy.
- VI. Development of non-structurally destructive and green lithium extraction methods. In addition to Ni, Co, Mn, and Fe elements commonly used for catalysts, the Li element in spent LIBs is also valuable. Most works focused on recycling the spent LIBs as catalysts and neglected the recycling of Li. Many effective methods for Li extraction in academia and industry, such as hydrometallurgy, are available. Researchers used acidic solvent systems, such as inorganic acid ( $\text{H}_2\text{SO}_4$ ,  $\text{HCl}$ , etc.) or organic acid ( $\text{H}_2\text{C}_2\text{O}_4$ ,  $\text{CH}_3\text{COOH}$ , etc.), to convert Ni, Co, and Mn into precipitates, allowing for the retention of Li in the solution. Subsequently,  $\text{Na}_2\text{CO}_3$  and  $\text{Na}_3\text{PO}_4$  solutions were added to precipitate Li salt. The wetting process requires strong acid or alkaline leaching agents to dissolve the components completely, and the raw materials input is large, potentially causing environmental pollution due to the waste liquid after leaching. The deep eutectic solvent (DES) leaching method for spent LIB recycling has attracted wide attention. DES has green, highly efficient, and recyclable attributes. DES systems such as the betaine hydrochloride-ethylene glycol system and choline chloride-urea have been introduced to replace the traditional leaching process, featuring high environmental friendliness and lower costs. Despite these strengths, the hydrometallurgy process will destroy the original composition and structure of battery electrode materials, inactivating the catalyst activity. It is worth investigating how to extract lithium from the spent cathode materials without damaging its structure, so that it can then be converted into a catalyst.
- VII. Catalyst service life extension. Long service life is an important indicator for the commercial application of catalysts. During usage, the efficiency of catalysts decreases, retarding the catalytic process. This leads to decreased economic benefits of the device's working process and even operation failure. Catalyst replacement is crucial to ensuring that the economic benefits of the components are higher than the rated value. This tedious process will be costly and time-consuming. If not handled properly, the heavy metal ions in the LIB-derived catalysts can also cause environmental pollution. The decline of catalyst life is attributed to many reasons, mainly including catalyst poisoning by poor service environment. The high-temperature thermal effect expands the particle size of the active components in the catalyst, reducing the specific surface area. Subsequently, the impurities in the reaction raw materials cover the active sites on the catalyst surface. The catalyst lifespan depends on the guaranteed service life under normal operating conditions proposed by the manufacturer, the actual operating conditions, and usage methods.

**Table 4** Catalysts recycled from spent LIB materials that perform better than industrial ones and corresponding performance

Application	Spent material types	Catalyst	Industrial catalyst	Performance	References
OER	LiCoO <sub>2</sub>	Ultra-thin CoOOH nanosheets	RuO <sub>2</sub>	Recycled: mass activity of 99.2 A g <sup>-1</sup> at 1.6 V, overpotential of 305 mV after 65 h at 10 mA cm <sup>-2</sup> ; RuO <sub>2</sub> : 45.1 A g <sup>-1</sup> at 1.6 V, overpotential of 367 mV after 23 h at 10 mA cm <sup>-2</sup>	[129]
OER	LiNi <sub>x</sub> Co <sub>y</sub> Mn <sub>z</sub> O <sub>2</sub>	NiCoMn layered triple hydroxides	RuO <sub>2</sub>	Recycled: affords 10 mA cm <sup>-2</sup> at an applied potential of 1.58 V; RuO <sub>2</sub> : affords 10 mA cm <sup>-2</sup> at an applied potential of 1.62 V	[135]
OER	LiNi <sub>x</sub> Co <sub>y</sub> Mn <sub>z</sub> O <sub>2</sub>	NiCoMnBs	RuO <sub>2</sub>	Recycled: affords 46.99 mA cm <sup>-2</sup> at an applied potential of 1.53 V, overpotential of 318 mV at 100 mA cm <sup>-2</sup> ; RuO <sub>2</sub> : affords 20.32 mA cm <sup>-2</sup> at an applied potential of 1.53 V, overpotential of 501 mV at 100 mA cm <sup>-2</sup>	[136]
OER	LiNi <sub>x</sub> Co <sub>y</sub> Mn <sub>z</sub> O <sub>2</sub>	Ni <sub>0.5</sub> Mn <sub>0.3</sub> Co <sub>0.2</sub> (OH) <sub>2</sub> nanoparticles	IrO <sub>2</sub>	Recycled: overpotential of 0.28 mV at 10 mA cm <sup>-2</sup> ; IrO <sub>2</sub> : overpotential of 0.29 mV at 10 mA cm <sup>-2</sup>	[137]
ORR	Graphite	Nitrogen-doped graphene	Nitrogen-doped graphene	Recycled: onset potential of 0.867 V for ORR, current reduction of 16.5% after the injection of 3 mol L <sup>-1</sup> methanol into the O <sub>2</sub> -saturated, 0.1 mol L <sup>-1</sup> KOH solution; Commercial nitrogen-doped graphene: onset potential of 0.797 V for ORR, current reduction of 33% after the injection of 3 mol L <sup>-1</sup> methanol into the O <sub>2</sub> -saturated, 0.1 mol L <sup>-1</sup> KOH solution	[173]
ORR	Graphite	Graphene nanosheets	Pt/C	Recycled: onset potential of 0.91 V for ORR half-wave potential of 0.81 V, limiting current density of 6.6 mA cm <sup>-2</sup> , activity degradation of 7% in the durability test; Pt/C: performance in onset potential, half-wave potential, limiting current density are worse than the recycled one (no specific data), activity degradation of 20% in the durability test	[177]
ORR	Graphite	Fe-N-doped carbon	20%Pt/C	Recycled: half-wave potential of 0.80 V, maintained an initial current of 93% after running at a fixed potential of 0.38 V for 36 000 s; 20%Pt/C: half-wave potential of 0.79 V, maintained an initial current of 82% after running at a fixed potential of 0.38 V for 36 000 s	[178]

In application, besides costs, the downtime-induced losses of catalysts due to catalyst replacement should also be considered. Some catalyst can be regenerated after being poisoned. However, after multiple regenerations, irreversible changes occur, leading to lower efficiency of the catalytic process than the specified

indicators, indicating catalyst degradation. When designing and preparing catalysts from waste LIB electrode materials, specific application scenarios and possible influencing factors of the catalyst should be underscored, and targeted design should be carried

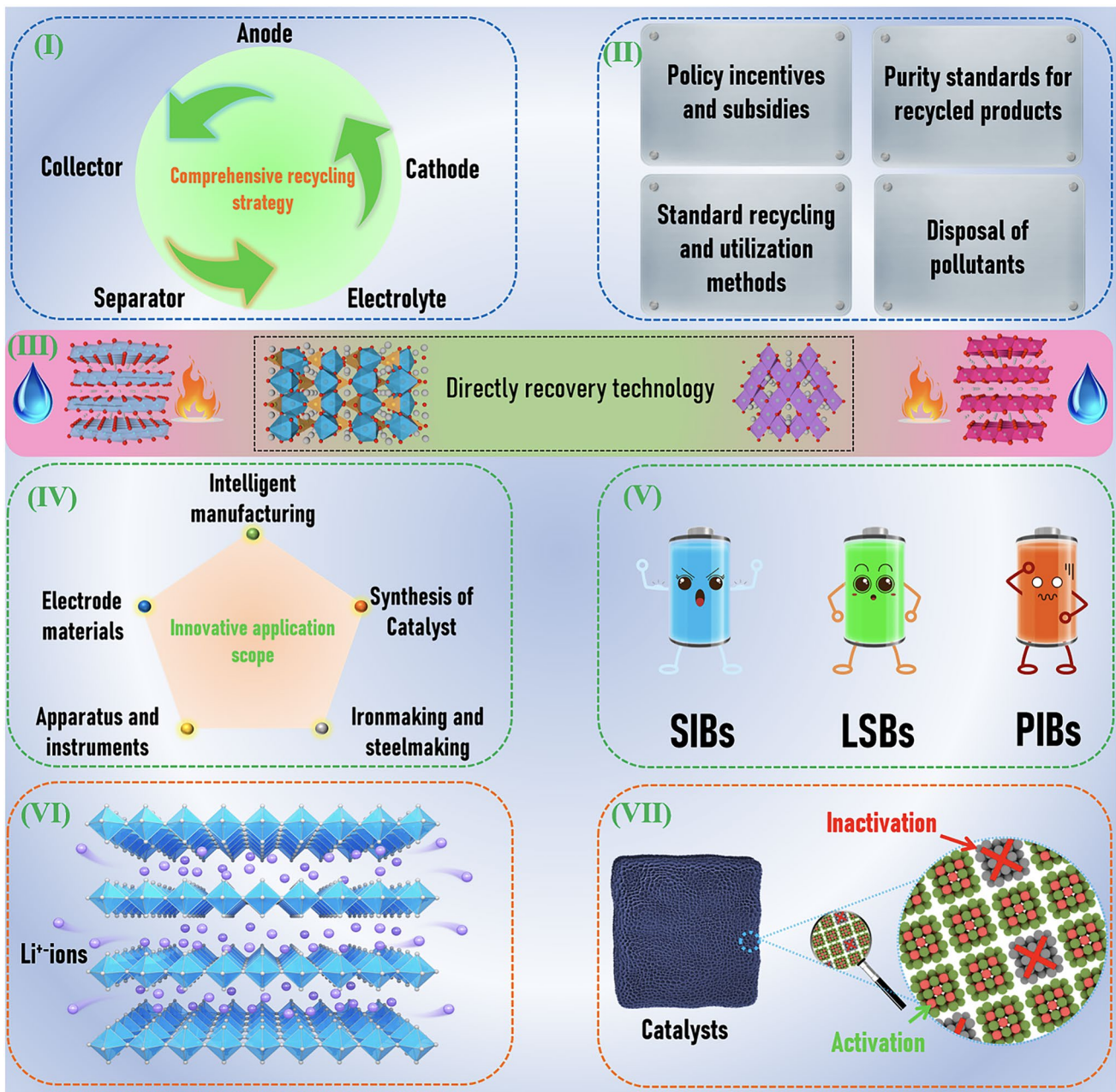


Fig. 11 Proposed perspectives for spent LIB recycling in the future



**Fig. 12** Schematics of toward recycling-oriented configuration and closed-loop design rule in practical spent LIB recycling

out to maximize the service life of the synthesized catalyst.

- VIII. **Toward recycling-oriented configuration design.** Considering resource scarcity and environmental pollution, spent LIB recycling has gained increasing attention. The model, specification, size, and composition of commercial LIBs have huge differences, hindering the development of large-scale recycling equipment as well as economical and sustainable battery recycling systems. In this sense, the upstream battery recycling industry should develop new types of batteries featuring easy recycling. Specifically, battery production should follow the closed-loop design rules to boost recycling performance and critically assess the possible recycling-oriented design of battery configuration, electrodes, and materials for recycling (Fig. 12).

**Acknowledgements** This work was supported by the National Natural Science Foundation of China (No. 52072205), Joint Funds of the National Natural Science Foundation of China (U21A20174), Shen-zhen Science and Technology Program (KQTD20210811090112002), Guangdong Innovative and Entrepreneurial Research Team Program (2021ZT09L197), Start-up Fund, and Interdisciplinary Research and Innovation Fund of Tsinghua Shenzhen International Graduate School, the Tsinghua Shenzhen International Graduate School-Shenzhen Pengrui Young Faculty Program of Shenzhen Pengrui Foundation (SZPR2023007), and the Natural Science Foundation of Sichuan Province (2023NSFSC1128) and Project of Southwest University of Science and Technology (20zx7142).

**Author contributions** R.S., B.W., and D.T. contributed equally to this review. Conceptualization: G.Z.; Formal analysis and investigation: R.S., B.W., and D.T.; Writing—original draft preparation: R.S., B.W., and D.T.; Writing—review and editing: X.W. and G.Z.; Funding acquisition: X.W. and G.Z.; Supervision: X.W. and G.Z.



## Declarations

**Conflict of interest** The authors declare no conflict of interest.

**Ethical approval** All authors certify that they have no affiliations with or involvement in any organization or entity with any financial interest or non-financial interest in the subject matter or materials discussed in this manuscript.

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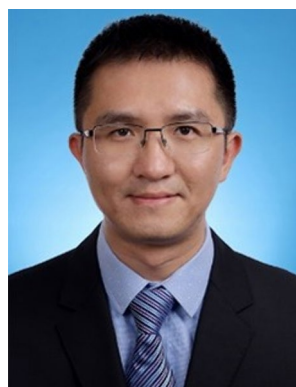
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