RESEARCH PAPER



Recycling of Rice Husk for Preparation of Activated Carbon/Magnetite Nanocomposites for Removal of Methylene Blue from Wastewater

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Abstract

This work focuses on recycling of rice husk for production of activated carbon/ Fe_3O_4 nanocomposite. Moreover, the synthesized composites were applied for elimination of methylene blue dye from wastewater. The proposed nanocomposite can replace pure activated carbon which is expensive and has some difficulties during its reusability. First, the activated carbon was extracted by thermal and chemical activations of rice husk ash. On the other hand, the activated carbon/magnetite nanocomposite was prepared by co-precipitation method using the suitable iron salts. The qualitative phase identification of prepared composite was performed by X-ray technique (XRD) and confirmed by Fourier Transform Infrared Spectroscopy (FT-IR). The morphology and particle size of prepared activated carbon and its composite were investigated by transmission electron microscope (TEM). The batch-adsorption method was utilized for studying the elimination of methylene blue dye from wastewater. Various factors like adsorbent dosage, pH of reaction, initial dye concentration, and duration of reaction were examined. The results showed that the prepared nanocomposite was almost amorphous as indicated from XRD patterns. Also, its particle size was very small (5–10 nm) and lower than the activated carbon alone (40–80 nm). Regarding the removal percentage of methylene blue dye from waste water, 98% was the maximum obtained percentage under the condition: pH 7, adsorbent dosage 0.1 g/100 mL, 50 ppm MB and 20 min. contact time at 25 °C. Furthermore, the maximum adsorption reaction followed the pseudo-second-order type and the Langmuir isotherm model.

Highlights

- The recycling of rice husk for production of activated carbon/Fe₃O₄ was successfully conducted.
- The synthesized composites were applied for elimination of methylene blue dye from wastewater.
- The maximum removal percentages of methylene blue from wastewater was 98%.
- The adsorption reaction followed the pseudo-second-order type and the Langmuir isotherm model.

Keywords Rice husk \cdot Activated carbon/Fe₃O₄ nanocomposite \cdot Synthesis \cdot Properties \cdot Adsorption \cdot Methylene blue dye

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Introduction

Nowadays, a great interest was directed to environmental pollution to preserve the living organisms and ecological system from distortion. With the development of industry, huge amounts of liquids or solids wastes are withdrawn in the environment; especially in water systems. Water is the most important system in the environment and its corruption tends to several problems for all living organisms (Iqbal et al. 2019). There are many contaminants for water systems as nutrients (nitrogen and phosphorus), heavy metals, hydrocarbons, organic matters, microorganisms (bacteria, viruses, protozoa, and parasites), and dyes (Akpor et al. 2014; Azam

2022).

et al. 2022; Khan et al. 2019; Lima et al. 2021; Yao et al. rela

The dye fabrication is considered as an important area in the chemical industries. The global production of dyes is about 850,000 tons every year. Generally, the synthesized dyes have many applications in many industries like paper-printing, textile, pharmaceutical, food, cosmetics, and leather. During different processes of textile industry, around 10-15% of dyes are withdrawn in water (Hassaan and Nemr 2017). Therefore, a huge amount of wastewater contaminated by dyes is produced and lost during the dyes industry. Dyes are usually categorized into three types, namely, anionic, non-ionic, and cationic dyes, while they are also classified according to the function groups into azo, anthraquinone, phthalocyanine, indigo, nitro, and sulfur. The cationic dyes as methylene blue, methyl violet, and crystal violet are the most toxic ones for the environment, since it includes cyclic organic rings (Hassaan and Nemr 2017). It is well recognized that the microorganisms that live in water systems need sunlight to generate energy, but the existence of coloring source like dye leads to preventing the light to penetrate; this consequently makes inconsistency in the ecosystem (Iqbal et al. 2015). Except the vat and disperse dyes, most of the dyes can dissolve in water and contain some toxic metals like chromium, cobalt, nickel, and copper (Dawood et al. 2014). Methylene blue is a solid dye and basic in nature; it can be applied for many applications, but it has toxic effect on the microorganisms, so it should be removed from wastewater. In water, it forms methylene blue and chloride ions which can be removed by many adsorbents (El Qada et al 2006). Many approaches have been approved for wastewater treatment; these included chemical and physical approaches like coagulation-flocculation, precipitation, advanced oxidation, ion exchange, membrane filtration, etc. The most interesting method used for eliminating dyes from wastewater is the adsorption technique because of its lower price, simplicity, and high efficacy; it proceeds without sludge and waste formation, extensive commercially available adsorbents, as well as the dye can be recovered (Andreou and Pashalidis 2018; Khan et al. 2020; Qureshi et al. 2022; Dehghani et al. 2017, 2018).

There are many industrial and biomass wastes that can be utilized as sources for the production of adsorbents for removing a variety of contaminates or toxic materials from water and wastewater (Besharati et al. 2018). One of the most important biomasses is the rice husk which after burning it forms rice husk ash. It includes reactive carbon and silica, so it can be used as excellent source for production of activated carbon which contains many groups on its surface as –COOH, –OH, –NH₂, etc., that make it a significant adsorbent for dyes and heavy metals (Besharati et al. 2018; Sugashini and Begum 2015). AC as adsorbent for dyes has high surface area, porosity, and adsorption capacity, but it is relatively expensive and it has difficulties during its usability. Thus, its production from waste materials in the presence of magnetic materials is recommended to overcome these drawbacks.

The application of nanoscale magnetic particles has attracted the attention of many researchers. Extremely, nanoparticles have favorable characteristics such as more atoms are located on their surfaces and they have a remarkable high surface area (Andreou and Pashalidis 2018; Suri et al. 2010). Magnetite and magnetic carbon nanoparticles have attracted a great interest in the field of environmental remediation due to their advantages as high thermal and mechanical stability as well as they can be rapidly separated from the solution by installing a magnetic separator (Kitkaew et al. 2018; Chen et al. 2018).

The main objective of the current work is to prepare activated carbon/magnetite nanocomposites to be utilized as adsorbent for removing of methylene blue from wastewater. The activated carbon was first extracted from rice husk waste, and then mixed with aqueous solution of iron slats to precipitate activated carbon/magnetite nanocomposites. The prepared nanocomposites were applied as adsorbents to remove methylene blue dye from wastewater by adsorption method. All parameters like reaction pH, duration of reaction, adsorbent dosage, and dye concentration were examined. Furthermore, type and order of reaction were estimated.

Materials and Experiments

Materials

First, the rice husk ash was prepared by burning the Egyptian rice husk, collected from different farms, in a muffle furnace for 2 h under argon atmosphere to be ready for preparation of activated carbon. Representative sample (50 kg) was collected from different farms in Egypt then quartered for many times until getting the final repressive sample (5 kg). While, the iron salts as $FeSO_4 \cdot 7H_2O$ and $FeCl_3 \cdot 6H_2O$ NaOH, cationic-methylene blue dye, HCl, and H_3PO_4 were supplied by Sigma-Aldrich, USA. The wastewater sample was supplied by Abu Rawash treatment plant, Cairo, Egypt. The properties of wastewater sample are illustrated in Table 1.

Chemical Preparation of Activated Carbon/Fe₃O₄ Nanocomposite

First, the activated carbon was prepared by thermal and chemical activation methods described elsewhere (Cheenmatchaya and Kungwankunakorn 2014; Zawrah et al. 2019, 2020). The prepared carbon was milled by high-energy ball mill model MTI SFM-1(QM-3SP2), to obtain nanopowder.

Table 1 Properties of wastewater sample

Property	Unit	Value
pН	_	7.78
Conductivity	μS/cm	883
Total dissolved solids (TDS)	mg/L	427
Total suspended solids (TSS)	mg/L	17
Chemical oxygen demand (COD)	mg/L	15
Biochemical oxygen demand (BOD ₅)	mg/L	10
Oil & grease (O&G)	mg/L	4
Ammonia as nitrogen (NH ₃ –N)	mg/L	10
Nitrate as nitrogen (NO_3^-)	mg/L	1
Sulfide (S)	mg/L	0.5
Phosphate	mg/L	3

To prepare the proposed composite, 4 g FeSO₄.7H₂O and 8 g FeCl₃ were mixed with 300 mL deionized water and warmed at 90 °C. 4 g of prepared nanoactivated carbon was mixed with iron dissolved salts. 200 mL of 2.5 M NaOH was dropped-wise slowly to precipitate magnetite during 2 h completely. The prepared activated carbon/Fe₃O₄ nanocomposite was washed by deionized water and separated by centrifuging. This method depends on decantation of liquid and then collecting the precipitate. Finally, the prepared nanocomposite was dried in heating-drier at 60 °C for 24 h. Figure 1 shows the schematic presentation for preparation method of activated carbon/Fe₃O₄ composite. This method gives high productive efficiency (Altıntıg et al. 2017).

Investigation of Activated Carbon and Its Composite with Fe₃O₄

To identify the qualitative phase composition and nature (crystalline or amorphous) of prepared nanoactivated carbon and its composite with magnetite, X-ray diffractometer model Philips PW1390, Holland, was used. To confirm the material composition and detect the functional groups, Fourier transform infrared spectroscopy was applied via the KBr

pressed disc method. The spectra were recorded on Mattson 1000, Unicam infrared spectrophotometer, UK, in the range (400–4000 cm⁻¹). The particle size and shape of fabricated nanoactivated carbon and its composite with magnetite were tested by transmission electron microscopy, model Philips, EM, 208, Holland. It provides excellent knowledge about the internal structure of materials like crystal structure, shape and size of grains, as well as the stresses in the structure.

Adsorption Study

The adsorption of methylene blue on activated carbon/ magnetite nanocomposite was performed. First, a typical methylene blue solution with concentration 1000 mg/L was prepared without addition of composite as a control sample. Specific amounts of prepared composite were mixed with 100 mL of prepared methylene blue solution to prepare several samples with different composite dose. These samples were put on a shaker at 150 rpm at room temperature. Many factors, such as duration of reaction (0-60 min.), composite amount (50–350 mg/100 mL), pH of reaction (3-10), and concentration of methylene blue (5-150 mg/L), were investigated. At the end of each experiment, the samples were filtered on Whitman filter paper No. 40 to separate the composite. The remained amount of methylene blue was evaluated by spectrophotometer type Perkin-Elmer lambda 25, at 665 nm. The percent of removed methylene blue in solution was considered according to the following formula

Removal,
$$\% = \frac{C_0 - C_f}{C_0} \times 100.$$

Since, C_0 and C_f (mg/L) are the original and ultimate dye concentrations, respectively.

The kinetic of adsorption reaction was examined by pseudo-first-order and pseudo-second-order models. The kinetic terms were estimated for each model by the suitable known formula. According to the drown results, the linear correlation coefficient (R^2) determined using the linear





regression was detected to identify the accurateness of proposed model. In general, when it is close to one, the model is fitting for the reaction. Furthermore, the obtained data were analyzed by Langmuir and Freundlich isotherms. All parameters related to these isotherms were evaluated.

Results and Discussion

Properties of Prepared Activated Carbon and Its Composite with Fe₃O₄

Phase Identification of Prepared Composite

X-ray is a principal non-destructive tool for identifying the crystal structure and type of crystalline phases qualitatively for minerals, elements, and inorganic compounds after comparison of the acquired data with reference database. There is a specific diffraction pattern for each material which should match with the fingerprints of reference database. Figure 2 shows XRD patterns of prepared activated carbon and activated carbon/magnetite nanocomposite. It is well recognized that the ash of rice husk is composed mainly of amorphous carbon and silica; their percentages depend on the method of pyrolysis and the applied atmosphere. As seen in the patterns, low intensity peaks are detected, indicating that both materials are semi-crystalline or amorphous. Both materials exhibit small peaks of amorphous silica and carbonaceous materials. The patterns exhibit broad peak at 2-theta equal 22° which is corresponding to silica. The peaks of carbonaceous structures (hexagonal graphitic-carbon like reflections) are detected at 2-theta 25° and 43° (Omri et al. 2013). Some new and very small characteristic peaks



Fig.2 XRD patterns of activated carbon and activated carbon/Fe $_3O_4$ nanocomposite

at 2-theta equal of 35.3° , 42.9° , and 62.5° are appeared in the pattern of activated carbon/Fe₃O₄ nanocomposite. These peaks are characteristics for Fe₃O₄ (Ai et Al. 2011). Very small peaks at 2-theta equal of 24.2° , 35.7° , 40.9° , 49.5° , 54.1° , and 63.3° are also appeared in the pattern of composite; these peaks are typical peaks of rhombohedra-centered hematite (Reza and Ahmaruzzaman 2015).

Confirming the Composition by FT-IR

FT-IR is a diagnostic tool utilized to identify the functional groups in organic and inorganic materials. This tool determines the absorption of infrared radiation by the material against wavelength. For each functional group in the material, there are characteristic adsorption bands which are detected from IR spectrum. FT-IR spectra of prepared activated carbon and activated carbon/magnetite nanocomposite are presented in Fig. 3. It is clear that FT-IR spectrum of activated carbon exhibits four bands at 3456, 2907, 1620, and 1089 cm^{-1} The bands at about 3456 and 1620 cm^{-1} are ascribed to the stretching- and bending-vibration frequencies of OH group for adsorbed water molecule, respectively. Also, the band at 1620 cm^{-1} might assign to C=C or C=O bonds of aromatic ring or carboxylic acid typically for carbonaceous material. The detectable small band at about 2907 cm⁻¹ is attributed to the existence of aliphatic C-H stretching of CH, CH₂, and CH₃ groups intermingled with the surface of carbon. The band at 1089 cm^{-1} is attributed to C-O-stretching vibration in RCOOH, ROH, PhOH, ROR, and RCOOR due to the oxidation of carbon. For activated carbon/Fe₃O₄ nanocomposite, the FT-IR spectrum exhibits all aforementioned bands in addition to two bands at 780 and



Fig.3 FT-IR spectra of activated carbon and activated carbon/Fe $_{3}\!O_{4}$ nanocomposite

466 cm⁻¹ but the band at 3456 cm⁻¹ is intense due to the formed hydrated Fe_3O_4 . The new formed bands are corresponding to iron oxides. These results are in agreement with the results obtained by Reza and Ahmaruzzaman (2015).

TEM of Prepared Activated Carbon and Activated Carbon/ Magnetite Composite

Figure 4 depicts TEM images of the extracted activated carbon and activated carbon/magnetite nanocomposite. It can be seen that the activated carbon (Fig. 4a) has homogeneous particle shape and size. The particles are mostly spherical with a few longer particles; their sizes are ranged between 40 and 80 nm. It is well known that the rice husk ash includes nanosilica particles, so the prepared activated carbon includes amorphous silica nanoparticles. On contrast, TEM image (Fig. 4b) of the activated carbon/Fe₃O₄ nanocomposite indicates the existence of inner components as black nanoparticles, namely, Fe_3O_4 (Sun et al. 2015). The overall morphology and size of this sample are homogenous. All the particle sizes are under 100 nm and reach less than 5 nm. The incorporation of Fe_3O_4 in the activated carbon leads to disperse of the particle and decrease the size. In addition, iron oxide can interact with the surface of activated carbon by chemical bonding which leads to change in the surface morphology of activated carbon/Fe₃O₄ nanocomposite (Darezereshki et al. 2013).

Adsorption Study of Methylene Blue by Activated Carbon/Fe₃O₄ Nanocomposite

To investigate the methylene blue removal efficiency by activated carbon/Fe $_3O_4$ nanocomposite, adsorption studies were

conducted under different conditions as pH, contact time, adsorbent dosage, and initial dye concentration.

Effect of pH on Methylene Blue Dye Removal

It is well known that the pH of solution medium is significant parameter for evaluation of the adsorption efficiency during the adsorption process. It is almost effect on the dissociation of function groups existing on the surface of adsorbent, the amount of charges on surface, and adsorbent structure. It can also effect on the rate of ionization for adsorbate molecule and it is responsible for the high- or low-sorption efficiency of adsorbent (Crini et al. 2007).

Figure 5 shows the relationship between the pH and the removal percentage of methylene blue by activated carbon/ Fe_3O_4 nanocomposite. It is appeared that the removal percentage rises gradually with raising the pH value and reaches its optimum value (95%) at pH 7 after which the removal



Fig.5 Effect of pH on removal of MB by activated carbon/Fe $_3O_4$ nanocomposite (0.1 g adsorbent, 2 h contact time, 50 mg/L MB, at 25 °C)



Fig. 4 TEM images of activated carbon (a) and activated carbon/Fe $_3O_4$ composite (b)

percentages are constant. The control samples give negligible removal percentages. At lower pH value (i.e., pH 3), there are positive charges on the surface of activated carbon/ Fe_3O_4 nanocomposite; these lead to rivalry between H⁺ ion and dye cation to touch the surface. Ultimately, the active sites on the activated carbon/Fe₃O₄ nanocomposite's surface are covered typically by the H⁺ ion and to a certain degree by the dye molecules. Therefore, the H⁺-ion limits the reaction between the cationic-methylene blue molecules (MB⁺) and the surface of activated carbon/Fe₃O₄ nanocomposite. This repulsive force delays the interaction of cationic MB⁺ molecules with the activated carbon/Fe₃O₄ nanocomposite's surface (Shah et al 2015). At pH 7, the positive charges on the surface of activated carbon/Fe₃O₄ nanocomposite decrease, so the cationic MB⁺ molecules have chance to adsorb on the active sites of adsorbent and reach their maximum. At pH more than 7, the active sites are full covered by methylene blue molecules, so there is no more adsorption can be occurred.

Effect of Composite Dosage on the Adsorption of Methylene Blue Dye

The influence of adsorbent dose on removal of MB by activated carbon/Fe₃O₄ nanocomposite is displayed in Fig. 6. As seen in the figure, the optimum dose for maximum adsorption of MB is 1 g after which very small decrease in removal percentage is occurred. This can be explained as: by increasing the amount of adsorbent up to 1 g, the active sites available for adsorption process increase which results in an increase in MB dye removal efficiency. After increasing the absorbent dose more than 1 g, the adsorption percentage of MB dye is relatively decreased till constancy. This is due

to agglomeration of activated carbon/Fe₃O₄ nanocomposite nanoparticles and decreasing the surface area as well as the active sites (Gundogdu et al. 2012).

Effect of Adsorption Time on Removing of Methylene Blue

The effect of interaction time on removal of MB dye by activated carbon/Fe₃O₄ nanocomposite is shown in Fig. 7. It is clear from the figure that very fast adsorption rate is detected by removing of more than 80% of MB during the first 5 min; then, the adsorption speed is increased gradually until the equilibrium is attained. This means that the application of the proposed composite in the adsorption process is more effective. It can be also seen from the figure that there is no significant variation in removal percent of MB dye after 40 min contact time due to saturation of the active sites which does not allow further adsorption to take place (Lopez et al. 2010).

Effect of Initial MB Concentration on Its Adsorption by Activated Carbon/Fe₃O₄ Nanocomposite

Figure 8 displays the dependence of MB dye removal percentage by activated carbon/Fe₃O₄ nanocomposite on its initial concentration (10–150 ppm). It is obvious that, as the initial dye concentration increases, there is a decrease in adsorption efficiency of dye from aqueous solution. The maximum dye removal percent (98%) is obtained up to 45 ppm dye concentration. The removal percentage becomes 96% with 50 ppm dye concentration. This is because there are limited available active sites, whereas the quantity of dye molecules rises with increasing original dye concentration. This leads to the consumption of active sites quickly,



Fig. 6 Effect of adsorbent dosage on removal of MB by activated carbon/Fe₃O₄ nanocomposite, (2 h contact time, 50 mg/L MB, at 25 °C)



Fig. 7 Effect of contact time on removal of MB dye by activated carbon/Fe₃O₄ nanocomposite (0.1 g adsorbent, 50 mg/L MB, at 25 °C)



Fig. 8 The effect of initial MB dye concentration on its removal by activated carbon/Fe₃O₄ nanocomposite (pH 7, adsorbent dosage 0.10 g/100 mL, and 20 min contact time at 25 °C)

Table 2 The kinetic parameters for adsorption of MB dye onto activated carbon/Fe $_3O_4$ nanocomposite

Pseudo-first-order quantities		Pseudo-second-order quanti- ties		
$K_1 ({\rm min}^{-1})$	0.115	K_2 (g/mg/min)	0.055	
$q_{\rm e}$ (mg/g)	5.8	$q_{\rm e} ({\rm mg/g})$	47.6	
R^2	0.9886	R^2	0.9996	

that affects on the removal percentage of the dye (Singh and Dawa 2014).

Application on Real Wastewater Examples

To inaugurate the validity of the suggested process, the process was applied for removal of MB in a real wastewater samples provided by Abu Rawash influent (Giza Governorate, Egypt). Two concentrations of MB dye (10 and 40 ppm) were spiked to the tested wastewater samples. The removal of MB dye from spiked solutions was successfully performed and up to 98% removal was achieved. Excellent removal percentage indicates that the complex matrix of wastewater samples does not interfere with the removal of MB.

Adsorption Kinetics Studies of MB by Activated Carbon/ Fe₃O₄ Nanocomposite

The adsorption kinetic of methylene blue dye by activated carbon/Fe₃O₄ nanocomposite surfaces was recognized by examining the pseudo-first-order and pseudo-second-order kinetics models. The obtained results of kinetic parameters for MB adsorption on activated carbon/Fe₃O₄ nanocomposite are illustrated in Table 2 and presented in Figs. 9 and 10. It is indicated that the estimated q_e value obtained from



Fig. 9 Pseudo-first-order model for the adsorption of MB dye onto activated carbon/Fe₃O₄ nanocomposite (pH 7, adsorbent dosage 0.10 g/100 mL, 20 ppm MB, and 20 min contact time at 25 $^{\circ}$ C)



Fig. 10 Pseudo-second-order model for the adsorption of MB dye onto activated carbon/Fe₃O₄ nanocomposite (pH 7, adsorbent dosage 0.10 g/100 mL, 20 ppm MB, and 20 min contact time at 25 $^{\circ}$ C)

pseudo-first-order and pseudo-second-order kinetics models are 5.8 and 47.6 mg/g, respectively. Moreover, it can be observed from Figs. 9 and 10 that the correlation coefficient (R^2) of pseudo-second-order model $(R^2 = 0.9996)$ is greater than that of pseudo-first-order model $(R^2 = 0.9886)$, indicating that the adsorption of MB onto activated carbon/Fe₃O₄ nanocomposite is fitting sound with the pseudo-second-order model. This means that the adsorption is chemisorption process, i.e., the electro-static interaction between the electrons in methylene blue dye molecules and activated carbon/Fe₃O₄ nanocomposite is the rate-limiting step (Phihusut and Chantharat 2017; Abuzerr et al. 2018).

Adsorption Isotherms of MB Dye onto Activated Carbon/ Fe₃O₄ Nanocomposite

It is well recognized that the Langmuir and Freundlich adsorption isotherm models are the most common ones utilized to describe the equilibrium relationships between adsorbent and adsorbate interface in the adsorption process. Both of them are applied to examine the removal efficiency mechanism of methylene blue by activated carbon/Fe₃O₄ nanocomposite. The Langmuir model supposes that the adsorbate adsorbed homogenously in monolayer on equal sites of adsorbent, i.e., once an adsorbate species occupies a site, no more adsorption is occurred at that site. The Langmuir formula could be expressed as follows:

$$\frac{C_{\rm e}}{q_{\rm e}} = \frac{1}{Q_0 b} + \frac{1}{Q_0} C_{\rm e},$$

where q_e is the amount of adsorbed methylene blue on activated carbon/Fe₃O₄ nanocomposite at equilibrium (mg/g), Q_o is the quantity of adsorbed MB monolayer on composite, *b* is the adsorption equilibrium constant or Langmuir constant; it is associated with the adsorption energy (L/mg) and C_e is the equilibrium concentration (mg/L).

Figure 11 shows the linear relationship of specific adsorption (C_e/q_e) and the equilibrium concentration (C_e) (mg/L) for the adsorption of methylene blue by activated carbon/ Fe₃O₄ nanocomposite given the Langmuir model. The Langmuir coefficients Q_0 and b can be estimated using the slope and intercept of the curve and are illustrated in Table 2. The Langmuir constant b (l/mg) can be correlated with the dimensionless constant (separation factor R_1) that is presented by the next formula (Hao et al. 2018)

$$R_1 = \frac{1}{1+bC_0},$$

where C_0 is the primary concentration of dye (mg/L). The R_1 values are used to define the kind of adsorption depending on its value range: $R_1 > 1$ means unwanted adsorption, $0 < R_1 < 1$ gives favorable adsorption, $R_1 = 0$ means irreversible adsorption, and $R_1 = 1$ means linear adsorption. In the



Fig. 11 Langmuir isotherm plot for MB adsorption on activated carbon/Fe₃O₄ nanocomposite

current study, the obtained R_1 value is 0.0139 which means that the adsorption is favorable. Also, according to the higher R^2 value (0.9923) for Langmuir isotherm model, this means that the chemical adsorption is the predominant mechanism, i.e., the methylene blue might chelate with numerous groups on the surface-activated carbon/Fe₃O₄ composite. Furthermore, the maximum Langmuir adsorption efficiency of methylene blue on activated carbon/Fe₃O₄ nanocomposite is calculated as 49.5 mg/g (Altıntıg et al 2017). This result indicates that the adsorption capacity of the prepared nanocomposite is increased due to increasing the surface area and micropores volume by incorporating of Fe₃O₄.

Regarding the Freundlich model, it assumes that the adsorption is happened on heterogeneous surfaces and mono- or multi-layers are formed according to the quantity of methylene blue adsorbed at equilibrium. The Freundlich linear formula can be expressed by the next one

$$\ln q_{\rm e} = \ln K_{\rm f} + \left(\frac{1}{n}\right) \ln C_{\rm e},$$

where $K_{\rm f}$ is practically correlated to the adsorption capacity and 1/n is the adsorption strength. When n > 1, this means favorable adsorption (Omri et al. 2013; Aranfil and Kilduff 1999). By plotting $\ln q_e$ against $\ln C_e$ (Fig. 12), the intercept $\ln K_{\rm f}$ and slope 1/n can be estimated. The values of $K_{\rm f}$, n and the linear regression correlation (R^2) for Freundlich model are presented in Table 3; their values are 0.064, 1.73, and 0.941, respectively. According to the values of linear regression correlation (R^2) in Langmuir and Freundlich isotherms, it is indicated that they are high and reach closely to one, but Langmuir is relatively higher, indicating that it is slightly fits well than the Freundlich model (Porkodi and Kumar 2007; Dhmees et al. 2019; Alhogbi et al. 2021). Generally, it can be concluded that the activated carbon/Fe₃O₄ nanocomposite is a good adsorbent for methylene blue dye owing to the existence of high active sites and electro-static interaction



Fig. 12 Freundlich isotherm plot for MB adsorption on activated carbon/Fe₃O₄ nanocomposite

Table 3 Langmuir and Freundlich parameters for adsorption of MB dye on activated carbon/ Fe_3O_4 nanocomposite

Langmuir isotherm		Freun- dlich isotherm	
\overline{Q} (mg/g)	49.5	$K_{\rm f}$	0.064
b (L/mg)	64.5	Ν	1.73
R^2	0.9923	R^2	0.968
R_{I}	0.0139		



Fig.13 Methylene blue after treatment with activated carbon/Fe $_{3}O_{4}$ nanocomposite

between its surface negative charge and cationic-methylene blue dye. Figure 13 shows the color of methylene blue after treatment with activated carbon/Fe₃O₄ nanocomposite at optimum conditions. The left flask contains methylene blue before treatment, while the right flask contains the remaining solution after removing of methylene blue by the proposed adsorbent; it is mostly clear like pure water. It is worth to mention that existence of common ions $(K^+, Na^+, and Ca^{2+})$ in water surface can affect slightly on the adsorption process, since they can compete with the contaminants and decrease their adsorption (Hassaan and Nemr 2017; Iqbal et al 2015; Dawood et al. 2014; El Qada et al. 2006). Compared to many effective adsorbents published in the literatures (El Qada et al. 2006), the proposed activated carbon/magnetite nanocomposites have also good efficiency for removing of methylene blue from water.

Conclusion

In this article, activated carbon/Fe₃O₄ nanocomposite was successfully prepared utilizing rice husk as a source of activated carbon and iron salts as source for Fe₃O₄. This composite was also utilized successfully as adsorbent for removing of methylene blue from wastewater by fast and simple adsorption technique. The prepared magnetic composite could be well dispersed in water and can be easily separated by a magnet from the aqueous solution after adsorption of the dye. The optimized parameters for the adsorption process were: 0.1 g/100 mL of adsorbent dosage, pH 7, dye concentration 50 ppm, and contact time of 20 min. The maximum adsorption capacity for activated carbon/Fe₃O₄ was 49.5 mg/g and the maximum removal percentage of methylene blue dye from real wastewater samples reached 98%. The kinetic study indicated that the reaction proceeded by pseudo-second-order model reaction mechanism, while the Langmuir isotherm model was the predominant mechanism.

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Declarations

Conflict of interest The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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