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Techno-economical and Experimental Analysis of Biodiesel Production from Used Cooking Oil

Sumitkumar Joshi¹ · Pradipkumar Hadiya¹ · Manan Shah¹ · Anirbid Sircar¹

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Abstract

Fossil fuel shortage is a major challenge worldwide. Therefore, research is currently underway to investigate potential renewable energy sources. Among the most of alternate energy sources for fossil fuel, biodiesel is more attractive and feasible energy source. The production of biodiesel from waste vegetable oil offers a triple-facet solution: economic, environmental, and waste management. In this work, a techno-economic analysis of a process that produces biodiesel from used cooking oil obtained from Pandit Deendayal Petroleum University (PDPU) canteen. The main aim is to recycle and reuse as an alternative for diesel fuel in the campus. Here, biodiesel is produced from used cooking oil through classical alkali-catalyzed transesterification. The important process parameters are alcohol-to-oil ratio, reaction time, temperature, and catalyst concentration were determined in biofuel research lab of PDPU. Results of these experiments suggest that 9:1 methanol-to-oil ratio, 50 min reaction time, 60 °C temperature, and 1.0 wt.% catalyst concentration were the optimum parameters for biodiesel production. A maximum conversion of used cooking oil to biodiesel above 93% was achieved in laboratory condition. Estimations of the unit production cost and fixed capital investment for this capacity have been calculated in detail. The fixed cost is 273,000 INR for the designed plant will have a capacity of 1000 L per day. The overall production cost of biodiesel is 28.55 INR/L. The payback period is around 3.5 year. Based on the observation that the raw materials cost is less than 5% of the total production cost. The main conclusions are that a plant with this capacity is feasible to produce biodiesel which is helpful as an alternative to diesel fuel and solve the environmental problems related to disposal.

Keywords Transesterification · Biodiesel · KOH · Economical analysis

Introduction

Fuel is an important backbone of the world's economy. The most basic requirement for human survival and activities is energy. In the present world, fossil fuels availability decreasing drastically, which increase the price of fossil fuels. Fossil fuels perform an important role in the

Manan Shah manan.shah@spt.pdpu.ac.in

> Sumitkumar Joshi sumitkumar.jbt15@spt.pdpu.ac.in

Pradipkumar Hadiya pradipkumar.hbt15@spt.pdpu.ac.in

Anirbid Sircar Anirbid.sircar@spt.pdpu.ac.in

¹ School of Petroleum Technology, Pandit Deendayal Petroleum University, Gandhinagar, Gujarat, India development of industrial growth, transportation purpose, and agricultural area and also satisfy other basic needs (Agarwal et al. 2012). Energy demand keeps increasing day to day due to increase in population, industrialization, and fast modernization (Alcantara et al. 2000). Therefore, the future energy demand is moving toward renewable and sustainable energy sources. Different renewable energy sources, like solar energy, geothermal energy, wind energy, energy from biomass etc., can be used as alternative energy sources in place of fossil fuels (Saravanan et al. 2014, 2015; Biofuel for transport 2006). Biodiesel seems to be more efficient compared to other renewable energy sources.

The current generation energy demand is satisfied by fossil fuel, which is non-renewable and limited. It also emits sulfur and many other contaminants (NOx, SOx, CO, volatile organic compound) to the environment which creates many serious problems like global warming, acidification, deforestation, ozone depletion, Eutrophication, and photochemical smog (Senthilkumar et al. 2014; Demirbas and Balat 2006; Demirbas 2008; Hama et al. 2011). These environmental related problems can be eliminated by replacing the petroleum-based fuel with a biodiesel. Whereas Biodiesel is completely free from sulfur and emits fewer amounts of pollutants. Oilseed, sunflower, soybean, and Carthamus tinctures are included in an edible seed oil and plantation crops genus Jatropha and genus Pongamia are include in non-edible seed oil for the production of biodiesel (Kalu et al. 2011; Haas et al. 2006). Considering the deficiency of edible oils and unsustainability of non-edible oils in countries like India, therefore waste cooking oil is the best feedstock for biodiesel production.

The use of waste cooking oil as raw material reduces biodiesel production cost by about 60–70%. It is noticed that the prices of biodiesel will be reduced approximately to the half with the use of low-cost raw material (Meneghetti et al. three moles of methanol react with; Meng et al. 2008; Mittelbach and Enzelsberger 1999). Moreover used cooking oils can be easily available. The use of non-edible plant oil when compared with edible oil is very important because of the tremendous demand for edible oil as food, and they are more expensive to be used as fuel at present (Sarkar et al. 2012). The land required for growing non-edible oilseeds as feedstock for the biodiesel production competes with the use of land for food production (Patil et al. 2010). So comparing non-edible oil as feedstock for biodiesel production, used cooking oil is more suitable.

Transesterification is a well-established chemical reaction in which alcohol reacts with triglycerides of fatty acid (cooking oil) in the presence of a catalyst (Agarwal et al. 2012; Malhotra and Das 2003; Sivakumar et al. 2015). The greater conversion of used cooking oil into biodiesel can be reached by using methanol. The transesterification reaction can be catalyzed by either acid or base catalyst. The most common means of production is base-catalyzed transesterification (Alcantara et al. 2000; Sinha et al. 2008). There are four important factors which affect the transesterification process: alcohol-to-oil molar ratio, catalyst concentration, temperature, reaction time (Alcantara et al. 2000; Saravanan et al. 2014, 2015; Saka and Isayama 2009). When comparing to other alcohols, methanol is highly preferable because of its low cost and better advantages (Deepalakshmi et al. 2014).

Different sources of biofuel production (Biofuel for transport 2006):



Benefits of biofuel (Biofuel for transport 2006):

| Economic impacts | Sustainability Fuel diversity Increased number of rural manufacturing jobs |
|-----------------------|--|
| | Increased investments in plant and equipment |
| | International competitiveness Reducing the dependency on imported petroleum |
| Environmental impacts | Greenhouse gas reductions Reducing air pollution Biodegradability Higher combustion efficiency Improved land and water use Carbon sequestration |
| Energy security | Domestic targets Supply reliability Reducing the use of fossil fuels Ready availability Domestic distribution Renewability |

Materials and Methods

Biodiesel is produced from natural and renewable sources such as vegetable oil, fat (Shimada et al. 2002). In this study, waste cooking oil collected from Pandit Deendayal Petroleum University cafeteria was used to produce biodiesel. The initial FFA (free fatty acid) content was 3.384%. The chemicals and reagents like methanol, KOH and phenolphthalein



Fig. 1 Experimental setup for biodiesel production from waste cooking oil. Apparatus: (1) distillation apparatus, (2) electrostatic heated stirring plate, (3) three necked round-bottomed flask, (4) thermometer, (5) condenser, and (6) separator funnel

(99.0% pure) required for transesterification reaction were obtained from Merk, Mumbai.

The waste cooking oil obtained was filtered initially. To remove water content, it was heated in a hot-air oven at 80 °C for 4 h. Now, this water-free cooking oil is ready for the transesterification process. Now, take 108 mL (100 g) waste cooking oil in a three-necked round-bottomed flask, which is equipped with a magnetic stirrer and water cooled condenser. The waste cooking oil was heated at 50 °C and the desired amount of methanol and catalyst without preheating were added to begin transesterification with stirring for the required reaction time. After completion of the process, the whole mixture is cooled down and settled down in a separating funnel. The experimental setup was shown in Fig. 1.

In transesterification reaction, three moles of methanol react with one mole of triglyceride to give three moles of fatty acid methyl ester (biodiesel). The empirical formula for the biodiesel transesterification reaction is given below.



Fig. 2 Effect of catalyst concentration on biodiesel yield

Results and Discussions

Effect of Catalyst

The amount of catalyst plays an important role in the conversion efficiency of the transesterification process. The catalyst quantity varied from 0.5 to 2.0 wt.% for seven different values (0.5, 0.75, 1.0, 1.25, 1.5, 1.75, and 2.0 wt.% of KOH). Figure 2 shows the variation of biodiesel yield with different catalyst concentrations. Optimum condition was achieved at 1.0 wt.% KOH, which produced more than 86% biodiesel yield. As higher catalyst concentration beyond 1.0 wt.% the yield decreased due to the saponification reaction (Omar and Amin 2011; Wang et al. 2007). Basicity of the catalyst used because of the base components only increases the biodiesel yield when compared with acid catalysts.

Effect of Temperature

To study the effect of temperature on the transesterification process. This process has taken place in 40 °C, 50 °C, 60 °C, 70 °C. The effect of temperature on biodiesel yield was shown in Fig. 3. However, the boiling point of Methanol is 64.7 °C which is higher than the reaction temperature. This can lead to the decrease in the biodiesel production due to sudden evaporation of Methanol.

$$\begin{array}{c} O \\ \parallel \\ CH_2O - C - R \\ \parallel \\ CHO - C - R \\ \parallel \\ O \\ \parallel \\ CHO - C - R \\ \parallel \\ O \\ \parallel \\ H \\ CHO - C - R \\ \parallel \\ O \\ \parallel \\ Alcohol \\ Chalyst \\ Alcohol \\ Catalyst \\ CH_2O - C - R \\ H \\ CH_2OH \\ CH_2O - C - R \\ CH_2OH \\ CH_2OH$$



Fig. 3 Effect of temperature on biodiesel yield



Fig. 4 Effect of methanol-to-oil ratio on biodiesel yield

Effect of Methanol-to-Oil Molar Ratio

The molar ratio of methanol to waste cooking oil is the main factor, which affects the conversion efficiency of the transesterification process by increasing methanol-to-waste cooking oil ratio, the yield of biodiesel has also increased up to a particular optimum molar ratio (Soetaert and Vandamme 2008; Yaakob et al. 2012). Figure 4 suggests that how the yield of biodiesel varies with methanol-to-waste cooking oil ratio. The maximum conversion efficiency of the transesterification process is achieved when the molar ratio of methanol to waste cooking oil is 9:1 for 1.0 wt.% concentration of KOH and 60 °C reaction temperature. The further molar ratio increased beyond the optimum dosage, biodiesel yield will be decreased due to reversible reaction and mixture become more viscous.

Effect of Reaction Time

The reaction time was studied for different time intervals. Figure 5 shows the effect of reaction time. The yield of biodiesel is about 93%, when reaction time is 50 min. By increasing the reaction time beyond this optimum reaction



Fig. 5 Effect of reaction time on biodiesel yield

time, the yield of biodiesel will decrease (Ying and Chen 2007).

Economic Analysis

Economic reasons have been one of the major obstacles in the use of biodiesel. Biodiesel derived from vegetable oil feedstock is more expensive than petrodiesel (Zhang et al. 2003; Yaakob et al. 2013; Apostolakou et al. 2009). Nevertheless, biodiesel produced from waste cooking oil is attractive for being a renewable resource and produced from the inexpensive feedstock. In this economic study, the effect of economic criteria like capital cost, manufacturing cost, and biodiesel production cost was estimated. The process economics for a biodiesel production was evaluated and established from waste cooking oil produced by the cafeteria of Pandit Deendayal Petroleum University. The fixed cost is 273,000 INR for the designed plant will have a capacity of 1000 L per day. Figure 6 represents the detailed flow chart of the economical analysis of biodiesel production from waste cooking oil.

Raw Materials Cost

The raw material cost (CRM) consists of the cost of used cooking oil, the cost of methanol, the cost of catalyst KOH solutions. The estimation of the cost of the used cooking oil is based on the overall material balance of the process. We collected used cooking oil from PDPU canteen so the feedstock cost for the biodiesel plant was considered as 0 INR. The price of methanol is 28 INR/L. We can calculate the cost of the catalyst KOH is 50 INR per kg.

Utilities and Operating Labor Cost

The cost of the utilities (CUT) consists of the cost of electricity and the cost of steam. It is estimated through the energy balances of the process that the utility consumption is approximately 17.77 INR/L production of biodiesel. The



operating labor cost is approximately 1.20 INR/L production of biodiesel (Table 1).

Conclusion

cooking oil

Biodiesel was obtained from waste cooking oil by transesterification. The optimum parameter value for catalyst concentration was 1.0 wt.% of KOH; reaction temperature was 60 °C; methanol-oil ratio was 9:1; reaction time was 50 min for the yield of maximum biodiesel which was 93% of used cooking oil.. The total cost of producing 1 L of biodiesel from waste cooking oil is 28.55 INR. This offers an unexpected source of income from waste cooking oil rather than disposing of it as a waste product. Basic concepts are presented and problems, potential solutions are discussed. This work stresses the importance of improving profits by reducing solid waste and pollution. With this work, it can

Table 1 Annual cost estimation for the batch process with a capacity of 400 ton per year

| Material cost | | In INR |
|-----------------------------|---|---------|
| (1) Feedstock cost (FC) | Waste cooking oil | 0.00 |
| (2) Consumables (C) | Based on material balance of laboratory studies | 3.27 |
| (3) Utility cost (UC) | | 14.50 |
| Variable cost (VC) | (FC+C+UC) | 17.77 |
| (4) Maintenance | 4% of VC | 0.71 |
| (5) Labor cost (LC) | Based on estimation | 2.00 |
| (6) Lab cost | 20% of LC | 1.2 |
| (7) Supervision | 20% of LC | 1.2 |
| (8) Overhead | 50% of LC | 3.00 |
| (9) Insurance and tax | 6% of LC | 0.36 |
| Fixed cost | [4+5+6+7+8+9] | 8.47 |
| Direct production cost | VC + fixed cost | 26.47 |
| (10) General overhead + R&D | 5% of direct production cost | 2.08 |
| Total production cost | [1+2+3+11] | 8.55 |
| Unit production cost | Estimated biodiesel produced per day 1000 L | 28.55/L |

be concluded that it is possible to integrate the waste cooking oil into productive processes to obtain biodiesel and reduce the cost of the biodiesel generated. In addition, it will be possible to integrate used cooking oil into a production process without continuing to generate impacts on the environment.

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Data Availability Availability of data and materialAll relevant data and material are presented in the main paper.

Compliance with Ethical Standards

Conflict of interest The authors declare that they have no competing interests.

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