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# **Graphene-templated synthesis of sandwich-like porous carbon nanosheets for efficient oxygen reduction reaction in both alkaline and acidic media**

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**ABSTRACT Developing low-cost, high-performance electrocatalysts for the oxygen reduction reaction (ORR) is crucial for implementation of fuel cells and metal-air batteries into practical applications. Graphene-based catalysts have been extensively investigated for ORR in alkaline electrolytes. However, their performance in acidic electrolytes still requires further improvement compared to the Pt/C catalyst. Here we report a self-templating approach to prepare graphene-based sandwich-like porous carbon nanosheets for efficient ORR in both alkaline and acidic electrolytes. Graphene oxides were first used to adsorb** *m***-phenylenediamine molecules which can form a nitrogen-rich polymer network after oxidative polymerization. Then iron (Fe) salt was introduced into the polymer network and transformed into ORR active Fe–N–C** sites along with Fe, FeS, and FeN<sub>0.05</sub> nanoparticles after pyr**olysis, generating ORR active sandwich-like carbon nanosheets. Due to the presence of multiple ORR active sites. The as-obtained catalyst exhibited prominent ORR activity with a half-wave potential ~30 mV more positive than Pt/C in 0.1 mol L−1 KOH, while the half-wave potential of the catalyst was only ~40 mV lower than that of commercial Pt/C in 0.1 mol L−1 HClO4. The unique planar sandwich-like structure could expose abundant active sites for ORR. Meanwhile, the graphene layer and porous structure could simultaneously enhance electrical conductivity and facilitate mass transport. The prominent electrocatalytic activity and durability in both alkaline and acidic electrolytes indicate that these carbon nanosheets hold great potential as alternatives to precious metalbased catalysts, as demonstrated in zinc-air batteries and proton exchange membrane fuel cells.**

**Keywords:** oxygen reduction reaction, porous carbon, nanosheets, fuel cells, zinc-air batteries

## **INTRODUCTION**

With the emerging global energy crisis and the growing environmental concerns, the development of efficient and renewable energy conversion and storage devices has become a critically important research topic. Fuel cells and metal-air batteries are two of the most promising electrochemical energy conversion devices with high energy utilization and safety  $[1-5]$  $[1-5]$ . However, the lack of efficient and low-cost electrocatalysts toward oxygen reduction reaction (ORR) occurring at the cathodes of fuel cells and metal-air batteries impedes the implementation of metal-air batteries and fuel cells in practical applications [6[–10\]](#page-7-1). Although Pt-based precious metal catalysts possess the most intriguing catalytic performance in prototype devices, the high cost associated with poor durability is a severe issue preventing their further development [11,[12](#page-7-2)]. Therefore, it is urgent to develop alternative non-precious metal catalysts (NPMCs) with high electrocatalytic activity and long-term stability to promote the commercialization of metal-air batteries and fuel cells in the near future [13–[19](#page-8-0)].

Recently, NPMCs containing transition meal-nitrogencarbon (M–N–C, M=Fe, Co) sites have attracted considerable attention due to their prominent catalytic performance in alkaline media [18[–24\]](#page-8-1). In particular, Fe/Ndoped carbon electrocatalysts have been considered as a very promising family of NPMCs for ORR because of the high catalytic activity, easy access, and cheap iron resources [24[–32\]](#page-8-2). However, the ORR activity of Fe–N–C catalysts still remains deficient compared to that of Ptbased catalysts in acidic media, owing to the low density of active sites [33[–38\]](#page-8-3). Meanwhile, the specific surface

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area and porous structure of carbon-based NPMCs have influence on the accessibility of the active sites and ORR activity [39[–43](#page-8-4)]. Consequently, rational design of porous carbon structures with abundant Fe-N-C active sites is highly desired. In this context, graphene is a very intriguing candidate for constructing two-dimensional (2D) porous NPMCs [44[,45](#page-8-5)]. The 2D planar nature would be beneficial for exposing active sites on the surface and transporting/exchanging ORR-relevant species [\[46\].](#page-8-6) Moreover, the highly conductive nature of graphene could further facilitate charge transfer during ORR [\[47\].](#page-8-7) Nonetheless, metal species are difficult to be directly doped into pure graphene due to the lack of strong bonding between metal species and graphene. Due to strong coordination with amines of metal ions, it is a potentially viable approach that a layer of nitrogen-rich polymer with multiple coordination sites for metal species which can then be transformed into M-N-C sites after pyrolysis is coated on the surface of graphene [48– [50](#page-9-0)].

Herein, we report the graphene-templated synthesis of sandwich-like porous carbon nanosheets in which each graphene nanosheet is encapsulated by a porous carbon shell with multiple dopants (i.e., N, S, and Fe–N) and embedded nanoparticles (i.e., Fe, FeS, and  $FeN<sub>0.05</sub>$ ). Crosslinked poly(*m*-phenylenediamine) (P*m*PDA) layer was initially formed on graphene oxides (GO) as nitrogen sources and anchoring sites for  $Fe<sup>3+</sup>$  ions. After adsorption and pyrolysis of  $Fe<sup>3+</sup>$  ions, porous carbon nanosheets with a high surface area (1105  $m^2$   $g^{-1}$ ) can be obtained (hereafter referred to as the P*m*PDA-GR-Fe catalyst). P*m*PDA contains more nitrogen content than polyaniline and polypyrrole, which can provide more nitrogen sources and coordination sites for Fe and thus could potentially enhance the electrocatalytic performance. In addition to N-doping, S could also be introduced into the carbon nanosheets during the oxidative polymerization process by using ammonium persulfate (APS) as the oxidant. In this way, the doping step is simplified while the element utilization efficiency is improved. Moreover, the existence of nanoparticles such as Fe, FeS, and  $FeN<sub>0.05</sub>$ could further boost the ORR activity by tuning the redox properties of surrounding carbon layers embedded with active sites [\[51\].](#page-9-1) Consequently, the resulting P*m*PDA-GR-Fe catalyst exhibited prominent ORR activity as well as excellent long-term stability both in alkaline and acidic media, surpassing those of commercial Pt/C catalyst (20 wt% Pt, Johnson Matthey). To assess the potential of this ORR catalyst for practical applications, the P*m*PDA-GR-Fe catalyst was further assembled as cathodes for a zincair battery and a proton exchange membrane fuel cell (PEMFC), respectively. Both results indicated that the P*m*PDA-GR-Fe catalyst exhibited excellent ORR activity in real electrochemical devices, suggesting that the reported catalyst is very promising for practical applications.

## **EXPERIMENTAL SECTION**

## **Synthetic procedures**

In a typical synthesis, 1 g *m*-phenylenediamine (*m*PDA) dissolved in 30 mL 1 mol L<sup>−</sup><sup>1</sup> HCl solution was mixted with a 50 mL GO solution containing 45 mg GO. Meanwhile, 4 g ammonium persulfate (APS) was dissolved in 50 mL 1 mol L<sup>−</sup><sup>1</sup> HCl solution. Both solutions were cooled to 4°C. Then, the APS solution was slowly added to the mixed *m*PDA/GO solution with vigorous stirring. After reaction for 8 h, the dark colored product was washed to be neutral with water several times. Finally, dried P*m*PDA-GO powder was obtained after vacuum drying for 12 h at 80°C. The dry powder of P*m*PDA-GO (0.1 g) was added into a 0.08 mol L<sup>-1</sup> Fe  $(NO<sub>3</sub>)<sub>3</sub>$  solution. After ~24 h, the solvent was removed using a rotary evaporator. Then, the resulting powder was heated at 900°C under  $N_2$  atmosphere for 2 h. Subsequently, the pyrolyzed sample was added into 1 mol  $L^{-1}$ HCl solution at 80°C for 12 h followed by centrifugation and washing with deionized water. This step was performed to remove electrochemically inactive and unstable species. Finally, the obtained powder was pyrolyzed at the same temperature for 2 h, leading to the final catalyst denoted as P*m*PDA-GR-Fe.

## **Materials characterization**

Scanning electron microscopy (SEM) was performed on a FEI SIRION200 microscope. High-resolution transmission electron microscopy (HRTEM) was conducted on a JEM-ARM 200F Atomic Resolution Analytical Microscope operating at an accelerating voltage of 200 kV. Powder X-ray diffraction (PXRD) patterns were obtained using a Japan Rigaku DMax-γA rotation anode X-ray diffractometer. The  $N_2$  adsorption-desorption experiments were carried out using the Belsorp-max instrument. X-ray photoelectron spectroscopy (XPS) measurements were performed on an X-ray photoelectron spectrometer (Thermo ESCALAB 250).

## **Electrochemical measurements**

All electrochemical measurements were performed in a

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three-electrode system using a PGSTAT302N electrochemical workstation (Metrohm Autolab) at room temperature. A 5.0 mm glassy carbon rotating disk electrode (PINE Research Instrumentation, USA) served as the substrate for working electrode. A platinum sheet and saturated calomel electrode served as the counter and reference electrodes, respectively. The reference electrode was calibrated with respect to reversible hydrogen electrode (RHE) before each experiment. The glassy carbon electrode was thoroughly cleaned before each test. To prepare the working electrode, 2 mg of the catalyst was dispersed in 1 mL ethanol and sonicated to get a homogeneous ink, followed by adding 10 μL 5% Nafion solution. Then, the catalyst ink was drop-casted on the glassy carbon electrode and dried at room temperature (catalyst loading: ~0.2 mg cm<sup>−</sup><sup>2</sup> in alkline media, ~0.4 mg cm<sup>−</sup><sup>2</sup> in acidic media).

For ORR measurements, the cyclic voltammetry (CV) experiments were performed in  $Ar/O<sub>2</sub>$  saturated 0.1 mol  $L^{-1}$  KOH and 0.1 mol  $L^{-1}$  HClO<sub>4</sub> at room temperature with a scan rate of 10 mV s<sup>-1</sup>. Rotating disk electrode (RDE) tests were performed in  $O<sub>2</sub>$  saturated 0.1 mol  $L^{-1}$  KOH and 0.1 mol  $L^{-1}$  HClO<sub>4</sub> with a scan rate of 10 mV s<sup>-1</sup>. The electron transfer number during ORR was calculated by Koutecky-Levich equation. Rotating ringdisk electrode (RRDE) measurements were carried out to determine the four-electron selectivity according to the previous report [\[25\].](#page-8-8)

## **Zinc-air battery and fuel cell tests**

Zinc-air batteries were assembled in home-made cells. For example, a zinc-air battery was assembled by pairing the as-synthesized catalyst ink loaded on a porous carbon paper electrode (0.5 mg cm $^{-2})$  with a Zn foil in 6 mol  $\text{L}^{-1}$ KOH. PEMFC cathode catalyst was P*m*PDA-GR-Fe with a loading mass of 4 mg cm<sup>−</sup><sup>2</sup> or 60 wt% Pt/C from Johnson Matthey with a loading mass of 0.8 mg cm<sup>−</sup><sup>2</sup> . To enhance protonic conductivity, 60 wt% of Nafion content in cathode catalyst layer was used. The anode catalyst was 60 wt% Pt/C with a loading mass of 0.8 mg  $\rm cm^{-2}$ , and the Nafion content in anodic catalyst layer was 30 wt%. The catalyst layer in the anode and the cathode was brushed on the gas diffusion layer (Sunrise Power Inc. China) based on Toray 060 carbon paper. Then, the membrane electrode assembly (MEA) was prepared by hot-pressing the electrodes and Nafion 211 membrane with an active area of 1.0 cm<sup>2</sup>. Fuel cell polarization curve was tested at 80°C on a fuel cell test system (Model 850e, Scribner Associates Inc.).  $H_2$  and  $O_2$  flow rates were 300 mL min<sup>-1</sup> at 100% RH, and no back pressure was applied (i.e., the



<span id="page-2-0"></span>**[Scheme 1](#page-2-0)** Schematic illustration for the preparation of sandwich-like heteroatom-doped carbon nanosheets. Graphene oxides were first used as the template to adsorb *m*-PDA followed by an *in situ* polymerization process. Subsequently, after adsorbing  $Fe<sup>3+</sup>$  ions, the polymer coated graphene oxides were subjected to pyrolysis and acid leaching, leading to the final P*m*PDA-GR-Fe catalyst.

 $O<sub>2</sub>$  and  $H<sub>2</sub>$  partial pressure was about 0.53 bar since the saturation water vapor pressure at 80°C is ca. 0.47 bar).

## **RESULTS AND DISSCUSIONS**

The P*m*PDA-GR-Fe catalyst was prepared following the procedures schematically shown in [Scheme 1.](#page-2-0) Briefly, *m*-PDA monomers were first adsorbed onto GO surface due to π–π interactions, hydrogen bonding and electrostatic interactions (Fig. S1). Subsequently, P*m*PDA layer was formed on GO surface by *in situ* polymerization using APS as the oxidant to yield the P*m*PDA-GO hybrid. As shown in Fig. S2, the thickness of the sheet-like structure is ~4 nm, indicating the P*m*PDA layer successfully coated on GO. P*m*PDA-GO was then mixed with proper amount of ferric nitrate solution for 24 h to introduce Fe species into the hybrid. After drying, the mixed sample was subjected to pyrolysis at 900°C in  $N_2$  atmosphere for 2 h. The pyrolyzed product was leached in hot HCl solution to remove unstable and electrochemically inactive species. Finally, the leached sample was annealed under the same temperature for 2 h to afford the P*m*PDA-GR-Fe electrocatalyst with a sandwich-like structure.

The detailed microstructure was further examined by using SEM and transmission electron microscope (TEM). As shown in Fig. 1a and d, GO could successfully act as the template to form sheet-like structure by *in situ* polymerization *m*PDA monomers into P*m*PDA on the surface of GO. Meanwhile, the 2D sheet-like structure still retained after pyrolysis to yield P*m*PDA-GR [\(Fig. 1a,](#page-3-0) [d\)](#page-3-0). After introducing Fe into the polymer network, many visible pores and nanoparticles were formed after carbo-

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<span id="page-3-0"></span>**[Figure 1](#page-3-0)** (a, d) SEM and TEM images of P*m*PDA-GR. (b, e) SEM and TEM images of P*m*PDA-GR-Fe before acid leaching. (c, f) SEM and TEM images of the final P*m*PDA-GR-Fe catalyst. The FeS nanoparticles encapsulated in graphitic carbons were identified with the index crystal plane displayed in the inset in (f).

nization ([Fig. 1b](#page-3-0), e). However, after acid leaching process, almost all of the visible nanoparticles that exposed to the outside of the nanosheets disappeared in P*m*PDA-GR-Fe and some large pores are clearly seen ([Fig. 1c](#page-3-0)), suggesting that introducing Fe species is beneficial for the formation of porous structures. Although nanoparticles could not be observed in SEM image as shown in [Fig. 1c](#page-3-0), TEM image [\(Fig. 1f](#page-3-0)) clearly indicates the presence of nanoparticles with sizes of tens of nanometers in the final sandwich-like structure. The inset in [Fig. 1f](#page-3-0) shows a typical nanoparticle with the spacing of the crystalline lattices in two directions, 0.48 and 0.51 nm, respectively, corresponding to (101) and (010) planes of the FeS phase [\[52\]](#page-9-2). Moreover, the crystalline carbon layer can be easily identified as the (002) plane of graphitic carbon with an interlayer spacing of 0.34 nm. The encapsulated FeS nanoparticles could activate the surrounding graphitic layers, making the outer carbon layers highly active toward ORR [53,[54](#page-9-3)].

Elemental mapping results ([Fig. 2](#page-3-1)) demonstrate that both C and N are uniformly distributed in the carbon nanosheets. The strong Fe element signals exist in the areas of nanoparticles, indicating the formation of Febased nanoparticles during pyrolysis. Meanwhile, S element was observed from the mapping results which also distributed over the carbon nanosheets. By comparing the Fe and S mapping images, we could find that there are other Fe-based nanoparticles other than FeS. As shown in powder X-ray diffraction (PXRD) patterns [\(Fig. 3a\)](#page-4-0), the diffraction peaks can be assigned to the FeS, Fe, and  $FeN<sub>0.05</sub>$ , which are consistent with the elemental mapping results. Raman spectra (Fig. S3) reveal the characteristic G and D bands of carbon, corresponding to the graphitic



<span id="page-3-1"></span>**[Figure 2](#page-3-1)** HAADF-STEM image of the P*m*PDA-GR-Fe catalyst and the corresponding EDX elemental mapping images for C, Fe, O, N, and S elements.

and disordered or defect carbons, respectively. Elemental analysis (EA) and inductively coupled plasma mass spectrometry (ICP-MS) indicated that the C, N, S, O, and Fe contents in P*m*PDA-GR-Fe were 88.42, 4.94, 1.31, 3.53, and 1.33 wt%. The steep increase in  $N_2$  uptake at the low pressure region suggested the existence of abundant micropores. Brunauer-Emmett-Teller (BET) surface area of PmPDA-GR-Fe measured by N<sub>2</sub> sorption/desorption isotherms is 1,105  $m^2$  g<sup>-1</sup> with an average pore size of  $\sim$ 0.54 nm ([Fig. 3b\)](#page-4-0). Compared to the sample before acid leaching, introducing Fe species into the P*m*PDA-GR-Fe could significantly improve the surface area and pore volume. The high specific surface area has been shown to be beneficial for promoting catalytic activity [\[55\].](#page-9-4) XPS revealed the presence of C (89.91 at%), N (3.94 at%), S (1.11 at%), O (4.66 at%), and Fe (0.48 at%) (Fig. S4a). The Fe content measured from XPS is lower than that obtained from ICP-MS (1.33 wt%), indicating that the Fe species are partially embedded within the sandwich-like structure. The high-resolution N 1s spectrum (Fig. S4b) can be deconvoluted into several peaks at 398.5, 399.5, 400.3, 401.3, and 403.9 eV, which can be assigned to pyridinic N (24.3%), Fe–N (4.6%), terminal graphitic N (10.3%), central graphitic N (54.1%) and oxidized N  $(6.7%)$ , respectively  $[28]$ . The high content of pyridinic and graphitic N which are also identified in the X-ray near-edge structure spectrum of N K-edge (XANES, Fig. S5a) should be beneficial for ORR [56,[57](#page-9-5)]. The S 2p spectrum of P*m*PDA-GR-Fe can be fitted into three peaks ([Fig. 3c\)](#page-4-0). Two major peaks at 163.9 and 165.0 eV are assigned to S  $2p_{3/2}$  and S  $2p_{1/2}$  peaks for the -C-S-Ccovalent bond of thiophene-type sulfur owning to the spin-orbit splitting [\[58\].](#page-9-6) The remaining peak belongs to the oxidized S. The –C–S–C– configuration was also



<span id="page-4-0"></span>[Figure 3](#page-4-0) (a) PXRD patterns of P*m*PDA-GR-Fe before and after acid leaching. (b) N<sub>2</sub> adsorption-desorption isotherms and corresponding pore size distribution (inset) of P*m*PDA-GR-Fe before and after acid leaching. Deconvoluted XPS spectra of (c) S 2p and (d) Fe 2p peaks for the P*m*PDA-GR-Fe catalyst.

confirmed by the XANES result (Fig. S5b) [\[59\].](#page-9-7) Moreover, the S L-edge XANES spectra and S 2p spectra for P*m*PDA-GR-Fe (Fig. S6) before and after acid leaching showed that the –C–S–C– covalent bond can be stable in the acid solution. According to previous studies, –C–S–C– is beneficial for enhancing the catalytic activity of ORR [60,[61](#page-9-8)]. The high-resolution Fe 2p spectrum of P*m*PDA-GR-Fe ([Fig. 3d\)](#page-4-0) can be divided into three peaks for FeN*<sup>x</sup>* (711.1 eV), FeS (724.03 eV), and Fe (708.1 eV) with a satellite peak at 716.8 eV [\[53\]](#page-9-9). The peak at 711.1 eV suggested the existence of Fe-N species which are active sites for ORR [28[,62\]](#page-9-10).

The ORR activity of P*m*PDA-GR-Fe was first evaluated in alkaline media. CV was carried out in  $O<sub>2</sub>$ - and Arsaturated 0.1 mol  $L^{-1}$  KOH using commercial Pt/C (20 wt%, Johnson Matthey). As shown in Fig. S7a, no obvious peak is observed in Ar-saturated 0.1 mol L<sup>-1</sup> KOH electrolyte, while an obvious cathodic peak can be observed in O<sub>2</sub>-saturated electrolyte, indicating that the PmPDA-GR-Fe catalyst is highly active toward ORR. The peak at 0.90 V from P*m*PDA-GR-Fe is much higher than that of Pt/C (0.83 V, Fig. S7b), suggesting excellent ORR activity of the P*m*PDA-GR-Fe catalyst. Meanwhile, as shown in [Fig. 4a,](#page-5-0) the linear sweep voltammetric (LSV) curves confirm that P*m*PDA-GR-Fe exhibits prominent electrocatalytic activity with an onset potential ( $E_{onset}$ ) of  $\sim$ 1.02 V and a half-wave potential ( $E_{1/2}$ ) of  $\sim$ 0.88 V. These values are higher than those of Pt/C tested under the same conditions ( $E_{\text{onset}} \sim 1.0 \text{ V}$  and  $E_{1/2} \sim 0.85 \text{ V}$ ). In contrast, the samples that directly pyrolyzed without iron adsorption or without using graphene as the template exhibited relatively poor performance [\(Fig. 4a](#page-5-0)), suggesting that both Fe and graphene are indispensable to achieve prominent ORR activity. [Fig. 4b](#page-5-0) shows the Tafel plots of both P*m*PDA-GR-Fe and commercial Pt/C catalysts derived from [Fig. 4a](#page-5-0). The P*m*PDA-GR-Fe catalyst exhibits a Tafel slope of 67 mV dec<sup>-1</sup> which is lower than that of the Pt/C catalyst (70 mV dec<sup>-1</sup>), indicating P*m*PDA-GR-Fe has a good kinetic process for ORR. The average electron transfer number (*n*) calculated from the RRDE measurements [\(Fig. 4c](#page-5-0)) at all potentials is 3.98 which is close to the value calculated from the Koutechy-Levich  $(K-L)$  equation  $(n=4, Fig. S8)$ , confirming the desired four-electron oxygen reduction pathway. RRDE results also showed that the  $H_2O_2$  yield remained below 3.6% at all potentials and dropped to 0.7% at 0.8 V *vs*. RHE, indicating the P*m*PDA-GR-Fe catalyst has extremely high ORR catalytic efficiency. Moreover, the catalyst also showed high stability for ORR. The stability of P*m*PDA-GR-Fe and Pt/C catalysts were investigated at



<span id="page-5-0"></span>**[Figure 4](#page-5-0)** (a) LSV curves of PmPDA-GR, PmPDA-Fe, PmPDA-GR-Fe, and Pt/C in O<sub>2</sub>-saturated 0.1 mol L<sup>−1</sup> KOH. (b) Tafel plots obtained from the RDE measurements on P*m*PDA-GR-Fe and Pt/C catalysts. (c) The peroxide yield and the calculated electron transfer number of P*m*PDA-GR-Fe in O2-saturated 0.1 mol L<sup>−</sup><sup>1</sup> KOH measured during ORR from RRDE tests. (d) Chronoamperometric responses of P*m*PDA-GR-Fe and Pt/C catalysts at 0.75 V. Electrode rotation speed, 1,600 rpm; scan rate, 10 mV  $s^{-1}$ .

0.75 V in  $O_2$ -saturated electrolyte for 20,000 s [\(Fig. 4d](#page-5-0)). About 86% of the original current density was retained for the P*m*PDA-GR-Fe catalyst, whereas Pt/C catalyst displayed a much higher current loss of ~33%, clearly indicating superior stability of the P*m*PDA-GR-Fe catalyst. Furthermore, after adding methanol to the electrolyte, no significant change was observed in the CV curve of P*m*PDA-GR-Fe (Fig. S9a), implying the newly synthesized catalyst was inert to the methanol crossover effect, while Pt/C was rather vulnerable to methanol (Fig. S9b). These results demonstrate that P*m*PDA-GR-Fe catalyst has much better selectivity and stability than the commercial Pt/C catalyst toward ORR in alkaline media.

To further investigate the potential application of P*m*PDA-GR-Fe catalyst in PEMFCs, ORR activity of the PmPDA-GR-Fe catalyst was examined in 0.1 mol L<sup>-1</sup> HClO4. CV curves in Fig. S10 reveal that the P*m*PDA-GR-Fe catalyst also possesses excellent ORR activity in acidic electrolytes. The peak potential at 0.75 V *vs*. RHE of P*m*PDA-GR-Fe is very close to that of Pt/C (0.83 V). The LSV curves in [Fig. 5a](#page-6-0) confirm that P*m*PDA-GR-Fe exhibits excellent ORR activity with  $E_{\text{onset}}$  of ~0.94 V *vs*. RHE and  $E_{1/2}$  of ~0.79 V *vs*. RHE. These values are comparable to those of Pt/C tested under the same conditions ( $E_{\text{onset}} \sim 0.96 \text{V}$  and  $E_{1/2} \sim 0.83 \text{ V}$ ). In addition, the mass activity of PmPDA-GR-Fe catalyst was 10.8 A g<sup>-1</sup> at 0.80 V, which is very competitive compared to previous studies (Table S1). Control experiments indicated that both graphene and Fe were crucial to achieve such high ORR activity in acidic electrolytes ([Fig. 5a\)](#page-6-0). Accordingly, Tafel plots in [Fig. 5b](#page-6-0) show that the P*m*PDA-GR-Fe catalyst has a Tafel slope of 80 mV dec<sup>-1</sup> which is very close to that of the Pt/C catalyst (77 mV dec<sup>-1</sup>). The average electron transfer number (*n*) calculated from the RRDE measurements at all potentials was 3.93, which confirmed the four-electron oxygen reduction process ([Fig. 5c\)](#page-6-0). RRDE results also showed that the  $H_2O_2$  yield remained below 4.1% at all potentials and dropped to 1.9% at 0.8 V *vs*. RHE, indicating the P*m*PDA-GR-Fe catalyst has excellent ORR catalytic efficiency even in acidic media. Moreover, parallel stability tests revealed that the P*m*PDA-GR-Fe catalyst possessed much higher stability and better methanol tolerance than Pt/C catalyst (Fig. 5d and S11), implying that P*m*PDA-GR-Fe is more stable than Pt/C toward PEMFC applications.

Obviously, the P*m*PDA-GR-Fe catalyst exhibits attractive ORR performance both in alkaline and acidic media, which is among the best reported ORR electrocatalysts that are active in both electrolytes (Table S2). Our control experiments confirmed that acid leaching was necessary to expose the catalytic sites by removing electrocatalytically inactive species (Fig. S12). Moreover, polyaniline (PANI) was used as the polymer precursor to form the PANI-GR-Fe catalyst, which was investigated under the same conditions. Electrocatalytic tests indicated that the catalyst prepared using PANI as the precursor



<span id="page-6-0"></span>**[Figure 5](#page-6-0)** (a) LSV curves of P*m*PDA-GR, P*m*PDA-Fe, P*m*PDA-GR-Fe, and Pt/C in O2-saturated 0.1 mol L<sup>−</sup><sup>1</sup> HClO4. (b) Tafel plots obtained from the RDE measurements on P*m*PDA-GR-Fe and Pt/C catalysts. (c) The peroxide yield and the calculated electron transfer number of P*m*PDA-GR-Fe in O2-saturated 0.1 mol L<sup>−</sup><sup>1</sup> HClO4 during ORR measured from RRDE tests. (d) Chronoamperometric responses of P*m*PDA-GR-Fe and Pt/C catalysts at 0.7 V. Electrode rotation speed, 1,600 rpm; scan rate, 10 mV  $s^{-1}$ .

exhibited much inferior ORR performance (Fig. S13). Thus, P*m*PDA is indispensable to achieve the prominent ORR activity.

Subsequently, thiocyanate ion (SCN<sup>−</sup> ) poisoning experiments were carried out to determine whether M-N-C is the active species in ORR. SCN<sup>−</sup> ions are known to strongly coordinate with metal ions to form stable complexes and hence poison the metal containing active sites in acidic conditions [\[28\].](#page-8-9) As shown in Fig. S14, the ORR activity of P*m*PDA-GR-Fe was remarkably declined after adding SCN<sup>−</sup> into 0.1 mol  $L^{-1}$  HClO<sub>4</sub>, indicating that Fe–N–C species are the primary active species for ORR. Meanwhile, to probe the possible S-doping on the catalytic activity of P*m*PDA-GR-Fe, the P*m*PDA-GO sample was washed more than 10 times to minimize the content of S in the sandwich-like carbon nanosheets while ensuring that the polymerization process was not affected. EA and ICP-MS were used to quantify the variation of each element in the final catalyst. The C, N, S, O and Fe contents in P*m*PDA-GR-Fe after thorough purification were 88.08, 5.05, 0.65, 4.24 and 1.27 wt%, respectively. The S content obviously decreased compared to the original P*m*PDA-GR-Fe catalyst. The reduction of the S content in the catalyst caused a dramatic loss in ORR activity (Fig. S15), though the chemical nature of each element was largely unchanged (Fig. S16). Therefore, the presence of S could be beneficial for enhancing ORR activity [41[,47,](#page-8-7)[51\]](#page-9-1). Moreover, electrochemical impedance spectroscopy (EIS) (Fig. S17) revealed that the graphenetemplated sandwich-like carbon nanosheets generally showed a much lower charge-transfer resistance than the control samples without graphene in both alkaline and acidic media, which could account for the observed prominent ORR activity of the P*m*PDA-GR-Fe catalyst. Furthermore, control experiments indicated that appropriate amounts of GO should be used to form the optimal sandwich-like structure (Fig. S18). Thus, the existence of multiple dopants, high surface area and unique sandwichlike structure with encapsulated conductive graphene sheets leads to the high-performance P*m*PDA-GR-Fe catalyst.

Based on the appealing ORR activity of the P*m*PDA-GR-Fe catalyst in electrochemical tests, we further carried out preliminary tests by using the P*m*PDA-GR-Fe as cathode catalyst both in a two-electrode zinc-air battery and a PEMFC. The open-circuit voltage  $(V_{OC})$  of P*m*PDA-GR-Fe was 1.47 V with a peak power density of 280 mW cm<sup>-2</sup>, surpassing the Pt/C cathode tested under the same conditions (1.45 V and 170 mW  $cm^{-2}$ , [Fig. 6a\)](#page-7-3). The specific capacity of the battery using P*m*PDA-GR-Fe as the cathode catalyst normalized to the mass of consumed Zn was 869 mA h  $g^{-1}$  at the discharge density of 50 mA cm<sup>-2</sup> and 813 mA h  $g^{-1}$  at the discharge density of 100 mA cm<sup>−</sup><sup>2</sup> (Fig. S19), outperforming the battery as-



<span id="page-7-3"></span>**[Figure 6](#page-7-3)** (a) Polarization and power density curves of the Zn–air battery assembled using P*m*PDA-GR-Fe and commercial Pt/C (20 wt%) as the cathode catalysts. (b) Polarization and power density curves of the PEMFC using P*m*PDA-GR-Fe and commercial Pt/C (60 wt%) as the cathode catalysts.

sembled with Pt/C at the same mass loading. On the other hand, [Fig. 6b](#page-7-3) shows the fuel cell polarization curve and power density plot in the PEMFC using P*m*PDA-GR-Fe catalyst. The maximal power density can reach 630 mW cm<sup>−</sup><sup>2</sup> at cell voltage of 0.55 V and current density of 1,700 mA  $\rm cm^{-2}$ . The performance is very competitive to the Pt/C catalyst. Note that these preliminary fuel cell results could be further improved after optimizing the MEA assembly and the fuel-cell testing conditions. These results strongly prove that the as-obtained P*m*PDA-GR-Fe catalyst holds great potential for applications in real electrochemical devices such as zinc-air batteries and fuel cells.

## **CONCLUSIONS**

In conclusion, we successfully demonstrated a facile method to synthesize novel sandwich-like porous carbon nanosheets using graphene as the template. In this method, GO was introduced to build the sandwich-like structure with P*m*PDA coated on both sides of the GO surfaces *via in situ* polymerization. The P*m*PDA could coordinate with the  $Fe<sup>3+</sup>$  ions to generate Fe–N active sites. Meanwhile, the introduced Fe could dramatically increase the specific surface area by forming removable nanoparticles during pyrolysis. Moreover, the S element introduced during the polymerization process is beneficial for enhancing ORR activity. Thus, this approach could create a high density of active sites by formation of various dopants on the carbon layers. More importantly, the unique planar porous structure is helpful for exposing the active sites and mass transport. Furthermore, EIS results indicate that the encapsulated graphene could significantly reduce the charge transfer resistance. These attractive features enable the P*m*PDA-GR-Fe catalyst to exhibit excellent ORR activity in both alkaline and acidic media. We further showed that the P*m*PDA-GR-Fe catalyst can be successfully employed as a promising cathode catalyst both in Zn-air batteries and PEMFCs.

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**Author contributions** Xu H and Wang T conceived and designed the research. Wang T, Wang J, Wang X, Yang J performed the experiments. Wang T, Yang J, Wang X, Yang J, Liu J and Xu H participated in the interpretation of experimental results. All authors participated in the general discussion.

**Conflict of interest** The authors declare no conflict of interest.

**Supplementary information** Experimental details are available in the online version of the paper.

## **SCIENCE CHINA Materials ARTICLES**



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## 石墨烯模板法制备类似三明治结构的多孔碳纳米片用于高效催化酸**/**碱性条件下氧还原反应的研究

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摘要 开发低成本, 高性能氧还原反应(ORR)电催化剂对于燃料电池和金属空气电池的规模化应用至关重要. 基于石墨烯的碳催化剂已经 被广泛用于碱性电解质中的ORR. 然而, 与Pt/C催化剂相比, 石墨烯基催化剂在酸性电解质中的性能仍然需要进一步提升. 在这个工作中, 我们发展了一种非常高效的模板方法来制备基于石墨烯的具有三明治结构的多孔碳纳米片电催化剂, 其在碱性和酸性电解质中均具有非 常好的ORR催化性能. 首先, 被氧化石墨烯吸附的苯二胺分子通过氧化聚合形成富氮聚合物网络, 接着铁(Fe)盐被吸附到聚合物网络中, 并 且在热解之后形成ORR活性位点Fe-N-C以及Fe, FeS和FeNo.。纳米颗粒, 最终得到类似三明治结构的碳纳米片ORR电催化剂. 由于这种结 构中存在较高密度的ORR活性位点, 所获得的催化剂显示出非常高效的ORR活性, 在0.1 mol L<sup>−</sup><sup>1</sup> KOH中半波电位比Pt/C高30 mV. 更重要 的是, 在0.1 mol L<sup>−</sup><sup>1</sup> HClO4中, 催化剂的半波电位仅比Pt/C低约40 mV. 这种独特的平面三明治结构可以在催化反应中暴露出丰富的ORR活 性位点, 同时, 石墨烯层和多孔结构可以提高电导率以及促进传质, 这两者对于实现高活性ORR催化至关重要. 在碱性和酸性条件中, 突出 的电催化活性和耐久性表明这些碳纳米片作为贵金属基ORR催化剂的替代物具有很大的潜力, 优秀的锌空气电池和质子交换膜燃料电池 性能直接证实这种材料在实际电化学能源转化装置中也非常有应用前景.