

Eco‑Friendly Corrosion Inhibition of AA2024 in 3.5% NaCl Using the Extract of *Linum usitatissimum* **Seeds**

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Abstract Inhibitive efect of the extract of *Linum usitatissimum* seeds (*ELUS*) on the corrosion of the aluminum alloy AA2024 immersed in NaCl solution (3.5%) was studied by potentiodynamic polarization (PDP), electrochemical impedance spectroscopy (EIS) and electrochemical noise measurement (EN) techniques. *ELUS* effectively inhibited the corrosion of $AA2024$ with efficiency ranges from 65 to 82% for the corresponding *ELUS* concentrations from 80 to 1200 ppm. PDP showed that *ELUS* works as a cathodic inhibitor for aluminum in 3.5% NaCl solution. EIS showed that the corrosion process was governed by the charge transfer resistance (R_{ct}) , where R_{ct} values gradually increase with the increase in *LU* concentration. The results of EN are in a good agreement with the PDP and EIS results. Also, SEM confrms the electrochemical results.

Keywords Corrosion · GC–MS · EN · EIS

1 Introduction

Generally, all industrial metals sufer from corrosion. It does not only cost the economy 3–4% of gross national product $[1]$ $[1]$ but also affect human health and safety. It has a rising efect from overdesign to maintenance to the failure of equipment and fnally causes a shutdown.

Aluminum alloys have been extensively used in many industries such as cars, pipes, construction, batteries and aircraft. Aluminum alloy 2024-T3 is well known in aerospace applications due to its high strength to weight ratio and good fatigue resistance [[2](#page-11-0)]. However, the inhomogeneous distribution of intermetallic particles within the aluminum matrix generates local galvanic cells that afect the corrosion resistance.

Compact, adherent and continuous oxide flm is developed on aluminum upon exposure to the atmosphere or aqueous solutions. This flm is responsible for the corrosion resistance in a dry atmosphere. However, it cannot protect aluminum exposed to severe environments. Moreover, aluminum may be used in neutral solutions containing pitting agents such as chloride ions. Hence, anti-corrosion measures should be applied. One of these measures is the use of inhibitors, which is an efficient method for metal protection. Numerous researches have been conducted to present efective inhibitors suitable for diferent corrosive media [[3–](#page-11-1)[8\]](#page-11-2). Some of these inhibitors have negative impact on the environment such as chromates [\[9](#page-11-3)]. A considerable number of inorganic inhibitors have good metal protection performance with low toxicity; however, most of these inhibitors are expensive [[3\]](#page-11-1). Green chemistry, economics and waste treatment all favor the use of environmental-friendly inhibitors such as organic corrosion inhibitors (especially those from natural sources), which became, nowadays, of practical interest. Metal protection by these organic inhibitors comes from the fact that they adsorb on the metal surface forming a protective layer against corrosive species in the media $[10]$ $[10]$. The efficiency of an inhibitor depends on many factors such as the nature of the metal surface, the type of corrosive media and the chemical structure of the inhibitor. The chemical structure of the organic inhibitor and its charge density are crucial since they dictate the mode of adsorption

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on the metal surface and the number of metal-surface-active centers that could be covered [[4](#page-11-6), [11](#page-11-7)].

Linum usitatissimum is one of the oldest known cultivated plants, and it was found in ancient Egyptian tombs. It has been used in textile and paper industries. Edible oil is extracted by pressing the *L. usitatissimum*' seeds where the rest (solid residues) can be used for feeding cattle.

This study aimed to investigate the inhibition efficiency of the extract of *Linum Usitatissimum* seeds (*ELUS*) on the corrosion of AA2024 in NaCl solution (3.5%) as a corrosive media. Three electrochemical applications were applied for the investigation: potentiodynamic polarization (PDP), electrochemical impedance spectroscopy (EIS) and electrochemical noise (NE) measurements. IR, chromatography analyses, optical imaging, SEM and EDX mapping were applied to give more understandings for inhibition behavior.

2 Experimental Work

2.1 Specimen Preparation

A sheet of aluminum alloy (AA2024, composition in wt%: Mn(1.28), pb(0.064), Zn(0.006), Ti(0.029), Cu(0.81), Si(0.381), Fe(0.57) and Al(96.65%)), was obtained from Q-panel™. The sheet was pressed-cut into coupons each with dimensions $2.0 \text{ cm} \times 5.0 \text{ cm} \times 0.1 \text{ cm}$. Coupons were degreased and cleaned with ethanol and allowed to dry and then stored in a desiccator until their use in corrosion experiments [\[5](#page-11-8)]. The corrosive solution (3.5% aqueous NaCl, Sigma-Aldrich) and all other solutions were prepared using deionized water.

2.2 Preparation of Inhibitor

The seeds of *L. Usitatissimum* were purchased from a local market, Cairo, Egypt. For extraction, 50 g of the seeds was washed with deionized water and then was soaked in water/ ethanol solution in a closed vial $(v/v = 80:20, 200 \text{ ml})$, which was kept in an oven at 90 °C for 4 h. The vial was then removed from the oven and was left to cool to the room temperature. The produced solution was fltrated, and the filtrate was dried by heating $(50 °C)$ under vacuum for 24 h. The produced dry extract powder of the *ELUS* inhibitor was then collected, weighed and stored at 4 °C until the use. For each corrosion experiment, without any further purifcation or processing, a specifed amount of *ELUS* was directly added to the corrosive medium.

2.3 Characterization Studies

The Agilent 5975T LTM GC/MSD with a stationary phase DB-5H30mx with 0.319 mm \times 0.10 µm of phase thickness

was used to analyze the *ELUS. ELUS* powder was dissolved in 1, 2 dichloroethane solvent forming the analyte solution. Helium was used as the carrier gas, and a sample of analyte solution $(1 \mu l)$ was injected into the column at an initial temperature of 50 °C. Heating was programmed to increase the temperature up to 150 °C at 5 °C/min rate. The temperature of the mass detector was 250 °C where the MS detector was operated. The mass spectrum of the sample was compared with the internal standard mass spectrum (Mass Spectral Database NIST/EPA/NIH) to defne the unknown components. Based on the total area values of the identifed peaks, the percentage of each component was determined by the relative area of each peak.

To determine the functional groups of the inhibitor, a dry certain amount of *ELUS* was thoroughly mixed with KBr powder and then pressed to form a transparent disk. The IR spectrum of this disk was recorded in the range of 400–4000 cm^{-1} with an automatic signal gain that collected by 500 scans at 4 cm−1 resolution using the FTIR spectrometer (JASCO Model 4100, Japan). The background spectrum was recorded from the clean empty cell at 25 °C and was taken into consideration during analysis of the *ELUS* sample.

The surface morphology of the coated metal samples was investigated using scanning electron microscope (SEM, Carl Zeiss EVO-10) equipped with an energy-dispersive X-ray spectroscopy (EDS) analyzer.

2.4 Electrochemical Characterization Studies

Potentiostat/galvanostat with three-electrode type cell was used for electrochemical corrosion experiments using Gamry™, model reference 600. For all experiments, the ratio of corrosive solution volume to sample surface area is not less than 40 ml/cm².

For each experiment, a freshly prepared AA2024 coupon was used as working electrode, saturated calomel electrode as a reference electrode and platinum as the auxiliary electrode. The potentiodynamic polarization experiments were performed after immersion of the working electrode for at least 30 min in the corrosive solution. The potentiodynamical polarization curves were obtained in the potential ranges of – 250 to − 250 mV with respect to open-circuit potential (*OCP*) at a scan rate of 0.5 mV/s.

The EIS tests were performed at room temperature by a three-electrode assembly. A saturated calomel electrode was used as a reference electrode, platinum as a counter electrode and freshly prepared AA2024 as the working electrode. The EIS tests were performed using a Gamry reference 600 instrument in a frequency range of 10^5 – 10^{-2} Hz with an amplitude of 10 mV peak to peak, using AC signal at *OCP*. Inhibition efficiency (η) is calculated using [\[12](#page-11-9)]:

$$
\eta = \frac{(R_{ct} - R_{ct}^o)}{R_{ct}} \times 100
$$

where R_{ct}^o and R_{ct} (Ω cm²) are the charge transfer resistance in the absence and in the presence of inhibitor, respectively.

The electrochemical noise technique was also used in this study. The electrochemical potential (V_i_{noise}) and current $(I_i_{noise}$) noises were simultaneously determined in a freely corroding system employing two nominally identical working electrodes of the same area $(2.0 \text{ cm} \times 5.0 \text{ cm} \times 0.1 \text{ cm})$, and a saturated calomel reference electrode was placed in middle distance between the two working electrodes. The noise data were recorded for 1800 s at a sampling frequency of 1 Hz. All data analysis was performed using EAS410 Gamry software.

3 Results and Discussion

3.1 Inhibitor Characterization

ELUS was analyzed by GC/MS, and the resulting chromatogram is given in Fig. [1](#page-2-0). The retention times of the most intense peaks with the corresponding suggested compounds are presented in Table [1](#page-2-1). These are organic compounds and constitute 97.1% of the extract. The mass spectra of these compounds (not shown) indicate their chemical structures where most of them are fatty acids.

The FTIR spectrum of *ELUS* is presented in Fig. [2](#page-3-0). The spectrum indicates the groups of the above compounds collectively. The broad peak at 3429.8 cm^{-1} can be assigned to O–H stretching. CH₂ and CH₃ stretching appear at 2855 and 2930 cm⁻¹, respectively [[13\]](#page-11-10). The peak at 1631.8 cm⁻¹ may be attributed to the stretching mode of C=O group, and peak at 1388 cm⁻¹ represents the deformation of CH₂ and/or CH₃

Table 1 Composition of *ELUS*

[[14\]](#page-11-11). The peak at 1351.1 represents the C–H bending. Also, a peak at 1117.5 should correspond to C–O stretch. The peak at 1597.5 is attributed to N–H of the amino group [\[15](#page-11-12)]. The peak at 2954.6 is related to the amide group. Almost all of these groups are well-known constituents of the fatty acids indicated by GC/MS analysis.

3.2 Corrosion Measurements of Aluminum in 3.5% NaCl

The inhibition effect of *ELUS* on the aluminum corrosion in 3.5% NaCl solution was investigated by potentiodynamic polarization, electrochemical impedance spectroscopy and electrochemical noise (EN) techniques as given below.

3.2.1 Potentiodynamic Polarization (PDP)

Anodic and cathodic polarization curves of AA2024 immersed in 3.5% NaCl solutions, in the absence and presence of diferent concentrations of *ELUS*, are shown in Fig. [3](#page-3-1). It can be seen in the fgure that the increase

Fig. 1 Chromatogram of *ELUS*

Fig. 2 FTIR spectra of LU powder

Fig. 3 Tafel plots of aluminum in 3.5% NaCl with diferent concentrations of ELUS inhibitor at room temperature

in *ELUS* concentration caused more negative corrosion potentials. The cathodic branches shifted, with respect to that of the blank sample, to the lower current density region, which resulted in a significant decrease in *I*_{corr}. On the other hand, the anodic current densities did not considerably afect by the presence of *ELUS* when compared to the blank solution. This phenomenon clearly indicates that *ELUS* acts as a cathodic inhibitor for aluminum in 3.5% NaCl solution [[16–](#page-11-13)[18](#page-12-0)].

Table [2](#page-3-2) summarizes the electrochemical kinetic parameters of Tafel extrapolations (E_{corr} , β_c , β_a , I_{corr} , $I\text{E}\%$). We note from the table that the increase in *ELUS* concentration results in a considerable regular decrease in corrosion current density (I_{corr}) and a regular increase in inhibition efficiency (*IE*%) where inhibition efficiency of 82% was achieved by using 1200 ppm of *ELUS*.

For the concentration 80 ppm of inhibitor, from the table the recorded corrosion current density is higher than that of the blank sample (0 ppm) and it is worthy to comment on that behavior. There is always a threshold inhibitor concentration (minimum efective concentration) above which inhibition starts to perform in a regular manner with concentration [[19\]](#page-12-1). Below this concentration, on the contrary, a serious corrosion could occur because the amount of inhibitor is not adequate to cover the whole surface of the metal surface, resulting in the build-up of two areas: the inhibitorcovered area and the bare area. Under this circumstance, the bare area behaves as an anode with respect to the cathodic reaction (reduction of oxygen). When the cathodic has a greater area than the anodic area (which called "unfavorable area ratio"), the corrosion process accelerates rather than being inhibited [\[20\]](#page-12-2). This phenomenon can be confrmed by observing the optical image of the corresponding sample

Fig. 4 Images of AA 2024 immersed in 80 ppm ELUS: **a** optical image and **b** SEM magnifcation of selected area

Fig. 5 Nyquist plots AA2024 in 3.5% NaCl solution with diferent *ELUS* concentrations at room temperature

surface (Fig. [4](#page-4-0)a) where the two areas can be easily distinguished (arrows 1 and 2). For arrow 1, the surface is bright metallic and shows numerous pits. For arrow 2, on the other hand, the surface is dark, indicating that the surface is covered with the inhibitor and no pitting was optically observed. By investigating the bright metallic area using SEM imaging, Fig. [4](#page-4-0)b clearly shows the pits (red arrows). These observations are in consistent with that 80 ppm is less than the threshold concentration of inhibitor.

3.3 Electrochemical Impedance Spectroscopy (EIS)

Nyquist plots of AA2024 in 3.5% NaCl in the absence and in the presence of various concentrations of *ELUS* are shown in Fig. [5](#page-4-1). The most marked observation to emerge from the fgure is that all the plots are semicircles (in the absence and in the presence of the inhibitor). From the fgure, the diameter of the capacitive loop increases, i.e., the impedance of the inhibited substrate increases, with the increase in the inhibitor concentration. Sample with 80 ppm shows exception which concurs well with the PDP results.

The impedance plots have a capacitive loop that covers the whole range of frequency under uninhibited condition. Under inhibited condition, the Nyquist plot consists of a larger capacitive loop at high frequencies and an inductive loop at low frequencies. The appearance of the inductive loop at low-frequency range, with inhibitor, suggests the adsorption of inhibitor molecule $[21-23]$ $[21-23]$ $[21-23]$. The capacitive loop at high frequency is related both to the charge transfer resistance of the corrosion process and to the double-layer capacitance.

The Bodes plots (impedance and phase in Figs. [6](#page-5-0), [7\)](#page-5-1) confrm the Nyquist plot results where the impedance increases as the *ELUS* concentration increases. Also, the phase plot reveals a single time constant, which increases with the increase in *ELUS* concentration [[24\]](#page-12-5). Besides, the inductive loop was presents in the impedance plot, in Fig. [6,](#page-5-0) as a decrease in impedance at low-frequency range.

Fig. 6 Impedance plots of AA2024 in 3.5% NaCl solution with different *ELUS* concentrations at room temperature

Fig. 7 Phase angle plots of AA2024 in 3.5% NaCl solution with different *ELUS* concentrations at room temperature

Fig. 8 Equivalent circuits used for numerical ftting of the *EIS* data (**a**) in the absence and (**b**) in the presence of *ELUS*

In an attempt to understand the corrosion behavior of the *ELUS* inhibitor, *EIS* data were ftted to equivalent circuits, as shown in Fig. [8,](#page-5-2) where R_s is the solution resistance, R_{ct} is the charge transfer resistance, C_{dl} is the double-layer capacitance

Fig. 9 Changes in charge transfer resistance and double-layer capacitance of aluminum in 3.5% NaCl solution with a diferent concentration of *ELUS* at room temperature

and *L* is an inductive element. In this study, a leaking capacitor, constant phase element (*CPE*), is used instead of the pure capacitor for double-layer capacitance. The capacitance value can be calculated according to the following equation:

$$
C_{dl} = \frac{Y_0 \omega^{n-1}}{\sin(n\pi/2)}\tag{1}
$$

where Y_0 is the *CPE* constant, ω is the angular frequency (rad/s) and *n* is the *CPE* exponent. The *CPE* becomes pure capacitor when $n = 1$.

The change of both charge transfer resistance and doublelayer capacitance of AA2024 in 3.5% NaCl solutions with a diferent concentration of *ELUS* is demonstrated in Fig. [9.](#page-5-3) From the figure, R_{ct} generally displays a significant increase with the increase in *ELUS* concentration, while C_{d} shows an insignifcant decrease. It is important to note that the corrosion inhibition of AA2024 depends mainly on the charge transfer resistance rather than the double-layer capacitance, which may be related to the adsorbed *ELUS* molecules on the aluminum surface (Table [3\)](#page-6-0).

3.4 Electrochemical Noise (NE) Measurement

Electrochemical noise technique has many advantages such as its capability to diferentiate between the diferent types of corrosion (uniform, crevice, and pitting), and it is applied without any external effect to the corroded sample $[25, 26]$ $[25, 26]$ $[25, 26]$ $[25, 26]$. The main corrosion type of AA2024 in chloride containing solutions is the pitting; therefore, it was decided to use NE in this study. The noise resistance (R_n) is determined in the time domain as the ratio of the standard deviation of potential noise (σ_V) to that of current noise (σ_l) is given by the following equation:

$$
R_n = \frac{\sigma_V}{\sigma_I} \tag{2}
$$

Table 3 EIS ftting parameters with ELUS concentrations

where

$$
\sigma_V = \sqrt{\frac{\sum_{i=1}^{n} (V_i - m_v)^2}{n}} \quad m_v = \frac{\sum_{i=1}^{n} V_i}{n}
$$
 (3)

$$
\sigma_{I} = \sqrt{\frac{\sum_{i=1}^{n} (I_{i} - m_{i})^{2}}{n}} \quad \text{and} \quad m_{i} = \frac{\sum_{i=1}^{n} I_{i}}{n}
$$
 (4)

The tendency of DC was detached before the analysis of noise data in time domain. It is claimed that DC trend can cause inaccuracy in the calculation of noise resistance from time-domain analysis [\[27,](#page-12-8) [28\]](#page-12-9). Among diferent trend removal methods, the moving average removal (MAR) method was used in this study [[29](#page-12-10), [30](#page-12-11)]. The main feature of MAR method is a de-trending by subtracting a local average from the raw noise data. Any data point in the series, V_i , is a combination of the real noise component and the DC trend component:

$$
V_i = V_{i,\text{noise}} + V_{i,\text{DC}} \tag{5}
$$

 $V_{i, \text{noise}}$ is the real noise, and it is required for noise resistance calculation where V_i , $_{DC}$ is the DC trend component,

Fig. 10 Time records of electrochemical current noise associated with AA2024 exposed to 3.5% NaCl solution with 240 ppm of *ELUS* at room temperature: (**a**) before and (**b**) after removal of DC trend (MAR parameter $p = 64$)

Fig. 11 Time records of electrochemical current noise associated with AA2024 exposed to 3.5% NaCl solution with: **a** 0, **b** 80, **c** 240, **d** 400, **e** 800 and **f** 1200 ppm of *ELUS* inhibitor at room temperature

which has to be removed. The V_i , $_{DC}$ values can be calculated according to the following equation:

$$
V_{i,DC} = \frac{\sum_{i-p}^{i+p+1} V_i}{2p+2}
$$
 (6)

where p is an integer value that can be 3, 10, 16, 32, 50 or 64 [[27,](#page-12-8) [28\]](#page-12-9). In this study, p values were taken = 64 to avoid over-flter of long lifetime electrochemical events [[28](#page-12-9)]. The DC trend in the voltage–time record can, therefore, be removed, and the random fluctuation $V_{i, \text{noise}}$ can be deduced as:

Fig. 11 (continued)

A similar procedure can be applied to calculate $I_{i,\text{noise}}$. Figure [10](#page-6-1) demonstrates an example of DC drift removal of current data. Figure [10](#page-6-1)a shows the DC current before trend removal, and Fig. [10b](#page-6-1) shows both the DC trend and the noise data using MAR method with $p = 64$. Extracted real current

 $V_{i,\text{noise}} = V_i - V_{i,\text{DC}}$ and voltage data noise were investigated in the time domain to calculate the noise resistance *Rn*.

> Figure [11](#page-7-0) demonstrates the electrochemical current noise of AA2024 immersed in 3.5% NaCl solution with diferent concentrations of *ELUS*. It can be observed that the amplitude of current noise (represents the activity of corrosion process) shows a strong correlation with increasing inhibitor concentration where it sharply decreases with the increase

Fig. 12 Change of noise resistance (R_n) of AA2024 with the concentration of *ELUS* inhibitor in 3.5% NaCl

Fig. 13 SEM images of aluminum after immersion in 3.5% NaCl solution for 24 h in the absence of *ELUS*

in the inhibitor concentration (with exception of 80 ppm). Moreover, the frequency of fuctuations of the current noise, which represents the frequency of events (i.e., pitting), also decreases with the increase in the inhibitor concentration [\[29\]](#page-12-10). The continuous decrease in current noise seems to be related to improving the flm formed on the metal surface due to adsorption of inhibitor.

The height of fuctuations of the blank sample appears to be less than that of 80 ppm of *ELUS*; however, the frequency of fuctuation of the blank sample is greater than that of 80 ppm *ELUS*. These results indicate that the blank sample experiences a uniform corrosion with a slight pitting than that of 80 ppm of *ELUS*. Moreover, by increasing the inhibitor concentration more than 80 ppm, both the frequency of noise and noise height gradually decrease indicating inhibition of corrosion process. These results are in line with both EIS and PDP results.

The noise resistance (R_n) of AA2024 in 3.5% NaCl solution with a diferent concentration of *ELUS* is presented in Fig. [12](#page-9-0). The figure demonstrates a continuous increase in R_n with *ELUS* concentration except for 80 ppm case. Besides, the R_n values are comparable to that of R_{ct} that calculated from EIS data ftting. These results will be confrmed by studying the surface morphology of both blank and 1200 ppm *ELUS* samples in the next section.

Generally, the aluminum oxide layer cannot protect the surface from corrosion in severe corrosive environments such as 3.5% NaCl. In such corrosive media, AA2024 undergoes pitting corrosion. The pitting of aluminum is mainly due to its low negative potential and the presence of Cl−. The mechanism of the pitting corrosion of Al in neutral NaCl medium includes reduction of oxygen as a cathodic reaction as follows:

$$
1/2O_2 + H_2O + 2e^- \to 2OH^-
$$
 (8)

The alkalinity would increase due to the production of hydroxide group. The presence of weak fatty acids may decrease the effect of this alkalinity.

The anodic reactions that take place in this neutral solution are assumed as one of the following reactions [[8–](#page-11-2)[10](#page-11-4)]:

$$
Al + 3H_2O \rightarrow Al(OH)_3 + 3H^+ + 3e^-
$$
 (9)

$$
Al + 2H2O \rightarrow AlO(OH) + 3H+ + 3e-
$$
 (10)

$$
Al + 3/2 H_2O \rightarrow Al_2O_3 + 3H^+ + 3e^-
$$
 (11)

This follows the formation of $Al(OH)^{+2}$ which will react with chloride ion to form a soluble complex as follows:

$$
Al(OH)^{+2} + Cl^{-} \rightarrow Al(OH)Cl^{+} + 3H^{+} + 3e^{-}
$$
 (12)

The concentration of Cl− increases the production of the soluble complex ions $(AI(OH)Cl⁺)$ and consequently magnifes the corrosion rate of aluminum [\[31\]](#page-12-12). In addition, the presence of the intermetallic particles, mainly AI_2MgCu which cover 3% of the aluminum alloy surface, plays an important role in the corrosion process. The intermetallic particles form cathodic sites with respect to the aluminum matrix, and this change in the electrochemical activities of alloy composition forms micro-galvanic cells leading to pitting corrosion [[32\]](#page-12-13).

The above corrosion mechanism of aluminum can be inhibited by means of depositing a barrier layer that hinders the difusion of electrolyte toward the aluminum surface and/ or formation of an insoluble salt over the aluminum surface. This can be achieved by adsorption of an organic inhibitor such as the *ELUS*. Also, the water sparingly soluble fatty acid (extract content) can replace the Cl− during interaction with aluminum hydroxide.

Fig. 14 EDX mapping of AA2024 sample after immersion for 24 h in 3.5% NaCl solution in the absence of *ELUS*

Fig. 15 SEM images of aluminum after immersion in 3.5% NaCl solution for 24 h: (**a**) in the presence of inhibitor 1200 ppm *LU* and (**b**) in the presence of inhibitor (magnifed)

4 Scanning Electron Microscopy (SEM)

Through the use of SEM, we were able to investigate in detail the surface morphology of diferent samples. SEM analysis was conducted for both bare and inhibited samples. The SEM image (Fig. [13\)](#page-9-1) displays AA2024 surface after immersion in 3.5% NaCl for 24 h with no *ELUS* inhibitor. Severe pitting corrosion can be clearly observed covering the whole sample surface. The EDX elemental mappings analysis of a selected pit within the surface is presented in Fig. [14](#page-10-0). It is clear from the elemental maps that corrosion products within the pit are mainly aluminum chloride. In addition, copper and magnesium, representing the intermetallic particles, appeared within the pit. These intermetallic particles have diferent potential than that of aluminum matrix initiating pitting corrosion. These results have further strengthened our confdence in the mechanism of corrosion suggested above.

The surface morphology of inhabited sample was also studied using SEM technique. The SEM images, as shown in Fig. [15,](#page-10-1) show the surface of AA2024 sample with 1200 ppm *ELUS* after 24 h of immersed in 3.5% NaCl. Neither corrosion products nor pitting can be observed from SEM images. It can be concluded that the presence of *ELUS* suppressed the corrosion process due to the formation of an adsorbed flm of *ELUS* on the surface of AA2024. This flm prohibits or hinders the oxygen reduction reaction on the metal surface and therefore protects AA2024 from pitting and uniform corrosions in 3.5% NaCl solution. Finally, the results of SEM analysis are consistent with previous electrochemical results.

5 Conclusions

A new green inhibitor was extracted from of *L. Usitatissimum* (*ELUS)* seeds and used to inhibit the corrosion of AA2024 in artifcial seawater. The kinetics of corrosion inhibition are based on the results obtained from the polarization study, EIS, EN measurements and morphology study (optical and SEM). The efficiency of corrosion inhibition increased with increasing the inhibitor (*ELUS)* concentration. Polarization study reveals that *ELUS* acts as a cathodictype inhibitor. According to EIS results, the charge transfer resistance governed the corrosion process. The results of *EN* measurements showed that *ELUS* provides protection against pitting corrosion of aluminum in the presence of chloride ions. The *EN* results are confrmed by SEM and EDX analysis. EN results are compatible with the measurements of potentiodynamic and *EIS*. The inhibition action was achieved via adsorption of the *ELUS* compounds on the surface of AA2024.

conducting SEM.

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