



Importance of entropy generation and infinite shear rate viscosity for non-Newtonian nanofluid

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Abstract

This study addresses the novel characteristics of infinite shear rate viscosity and entropy generation in magneto-mixed convective flow of cross-nanomaterial toward a stretched surface. Moreover, analysis of current research work has been prepared for Brownian moment and thermophoresis deposition. Radiation and viscous dissipation aspects are accounted. More specifically, roles of activation energy and Lorentz force on nanofluids transportation are examined. ODEs are acquired from PDEs via implementation of suitable transformations. Numerical algorithm is implemented to tackle the nonlinear system for numerical results. Discussion on rheological parameters involved in current research work is presented through graphs. Results demonstrate the significant rise in temperature and nanoparticles concentration with the intensification of Brownian moment aspects. More specially, we perceived that entropy rate is significantly affected by radiation parameter and Brinkman number. Intensification in entropy rate is observed for rising values of magnetic parameter, radiation parameter and Brinkman number.

Keywords Cross-fluid · Entropy generation · Magnetohydrodynamic (MHD) · Activation energy · Mixed convection

List of symbols

u, v Velocity components
 x, y Space coordinates
 ρ Density of fluid
 ν Kinematic viscosity
 μ Dynamic viscosity
 n Power law index
 B_0 Uniform magnetic field strength
 $(\rho c)_f$ Heat capacity of fluid

T Ratio of heat capacity
 $(\rho c)_p$ Effective heat capacity
 α Thermal diffusivity
 σ^{**} Stefan–Boltzmann constant
 D_T Thermophoresis effect
 k_f Thermal conductivity
 c_p Specific heat capacity
 m^* Mean absorption coefficient
 D_B Brownian motion
 T Temperature
 T_∞ Ambient temperature
 C_∞ Ambient concentration
 T_w Surface temperature
 C_w Surface concentration
 k_r^2 Reaction rate
 E_a Activation energy
 Γ Time material constant
 β^* Ratio of viscosities
 C Concentration
 m Fitted rate constant
 c Dimensional constant
 U_w Stretching velocity
 η Dimensionless variable
 We Weissenberg number
 Pr Prandtl number

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M	Magnetic parameter
Nr	Buoyancy ratio parameter
λ	Mixed convection parameter
R	Thermal radiation parameter
Nb	Brownian motion parameter
Nt	Thermophoresis parameter
Ec	Eckert number
Sc	Schmidt number
σ	Dimensionless reaction rate
E	Dimensionless activation energy
δ	Temperature difference parameter
τ_w	Wall shear stress
q_w	Wall heat flux
f	Dimensionless velocities
θ	Dimensionless temperature
ϕ	Dimensionless concentration
N_G	Entropy generation rate
α_2	Dimensionless temperature ratio variable
α_1	Dimensionless concentration ratio variable
L	Diffusive variable
Br	Brinkman number
C_{fx}	Skin friction
Nu_x	Local Nusselt number
Re_x	Local Reynolds number

1 Introduction

In today's world, the ever-increasing consumption of energy demands preservation in its transportation and utilization. More specifically, nanotechnology is proved to be the best mean of heat transportation and preservation among the thermal sources. Thermo-physical properties of working liquid have a great impact on the efficiency of thermal systems. Nanofluids (NFs) are obtained by mixing solid nanoparticles (NPs) in the base liquids (BLs) which have considerably greater thermo-physical properties as compared with base liquids (BLs). The achieved NFs have distinct chemical and physical features than traditional BLs. Furthermore, NFs have vital role in the improvement of cooling rate with superior thermal efficiency. Khan and Khan [1] considered rheological properties of NPs for Oldroyd-B fluid with heat sink-source. Sheikholeslam et al. [2] studied the aspects of NPs for CuO–water NFs with Lorentz forces. Khan and Khan [3, 4] reported characteristics of non-Newtonian fluid in the presence of NPs. Waqas et al. [5] deliberated characteristics of non-Newtonian fluid with appliance of NPs. Khan et al. [6] analytically analyzed properties of 3D Burgers nanofluid (NF) by considering revised heat flux relation. Khan and Khan [7] investigated appliance of NPs for Burgers NFs in the presence of heat sink-source. Hayat et al. [8] analyzed Lorentz forces and porosity aspects to investigate appliance of NFs for exponentially stretched surface. Ahmad et al. [9]

numerically analyzed features time-dependent Sisko NF. Khan et al. [10] described gyrotactic microorganisms for Burgers NF with appliance of NPs. Waqas et al. [11] numerically conveyed characteristics of Williamson fluid accounting Brownian motion and thermophoresis aspects. Khan et al. [12] scrutinized radiation and Lorentz force aspects on 3D Carreau NF utilizing zero flux relation at stretched surface. Waqas et al. [13] reported properties of heat sink-source and stratified flow for Oldroyd-B NF. Sohail et al. [14] considered properties of convectively heated surface for time-dependent second grade NF in the presence of Lorentz force and zero mass flux relation. Khan et al. [15] analytically investigated properties of NPs for generalized Burgers fluid with chemical phenomenon. Animasaun et al. [16] reported the appliance of thermoelectric and Lorentz force for CuO–water NF. Recent analysis on NFs subjected to distinct flow aspects is reported in Refs. [17–42].

The bonding between the chemical components is loosening by catalysis. The catalytic reactions occur in both homogeneous/heterogeneous reactions. In homogeneous catalytic reaction system, both the catalytic materials lie in the same phase space like (gas, liquid or solid). However, in the heterogeneous process, the catalytic material lies in different phase space. Nowadays, there are wide applications of catalysts in industrial processes. More common examples that are in the agricultural and industrial process are fog formation, production of polymer, etc., when we need to start a binary chemical process, we require the minimum amount of energy, i.e., activation energy. The binary chemical process is a reaction process that occurs in two steps. Basically, the binary chemical reactions are common in both vapor and liquid deposition process. The mass transportation with chemical reaction and activation energy has industrial applications such as an oil reservoir, chemical engineering, oil emulsion, coating of metallic objects and glasses, manufacturing of electronic devices. Khan et al. [43, 44] reported properties of chemical process for non-Newtonian fluids. Mahanthesh et al. [45] considered aspects of Lorentz's force and chemical processes for NF utilizing vertical plate. Characteristics of chemical processes and modified heat flux relation were deliberated by Sohail et al. [46]. Hayat et al. [47] described features of Lorentz's force and chemical reactive species for third grade fluid. Irfan et al. [48] considered characteristics of variable conductivity and heat sink-source for non-Newtonian fluid with chemical processes. Khan et al. [49] characterized entropy generation and activation energy (AE) aspects for NF. Khan et al. [50] reported properties of AE and radiation for 3D flow of cross-NF with chemical processes. Waqas et al. [51] numerically analyzed properties of Darcy–Forchheimer and activation energy for NF in cylindrical surface. Khan et al. [52] reported appliance of chemical processes and radiative flow for cross-fluid.

Main objective of the present attempt is to examine aspects of infinite shear rate viscosity and entropy generation for mag-neto-mixed convective flow of cross-nanomaterial toward a stretched surface. Colloidal analysis for cross-fluid is scruti-nized by considering Buongiorno relation. Transportation of heat-mass analysis is studied by utilizing activation energy and Brownian moment aspects. More specifically, aspects of viscous dissipation are considered here. System of PDE's is transformed to one and then solved by implementing MAT-LAB tool bvp4c. Important physical quantities are discussed through tables and graphs.

2 Problem structure

Here, characteristics of infinite hear rate viscosity and entropy optimization rate in mixed convective flow of cross-nanofluid are analyzed. Viscous dissipation activation energy aspects effects are accounted in mathematical formulation. More spe-cifically, colloidal analysis of cross-nanofluid is permeated through Lorentz's force aspects. Characteristics of thermopho-resis and Brownian movement are accounted here. Governing equations for considered flow are

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0, \tag{1}$$

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = \nu \frac{\partial^2 u}{\partial y^2} \left[\beta^* + (1 - \beta^*) \frac{1}{1 + (\Gamma \frac{\partial u}{\partial y})^n} \right] + \nu(1 - \beta^*) \frac{\partial u}{\partial y} \frac{\partial}{\partial y} \left[\frac{1}{1 + (\Gamma \frac{\partial u}{\partial y})^n} \right] - \frac{\sigma^* B_0^2}{\rho_f} u + g [A_1 (T - T_\infty) + A_2 (C - C_\infty)], \tag{2}$$

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \frac{\nu}{c_p} \left(\frac{\partial u}{\partial y} \right)^2 \left[\beta^* + (1 - \beta^*) \frac{1}{1 + (\Gamma \frac{\partial u}{\partial y})^n} \right] + \alpha \frac{\partial^2 T}{\partial y^2} + \tau \frac{D_T}{T_\infty} \left(\frac{\partial T}{\partial y} \right)^2 + \tau D_B \frac{\partial C}{\partial y} \frac{\partial T}{\partial y} - \frac{1}{(\rho c)_f} \frac{16\sigma^{**} T_\infty^3}{3k^*} \frac{\partial^2 T}{\partial y^2}, \tag{3}$$

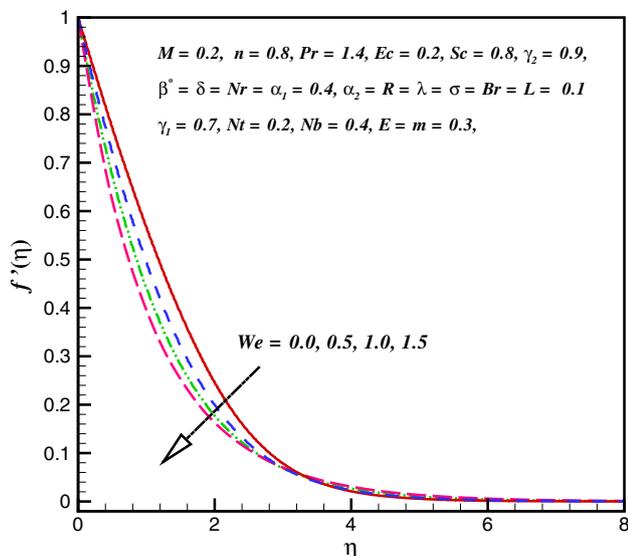


Fig. 1 $f'(\eta)$ via We

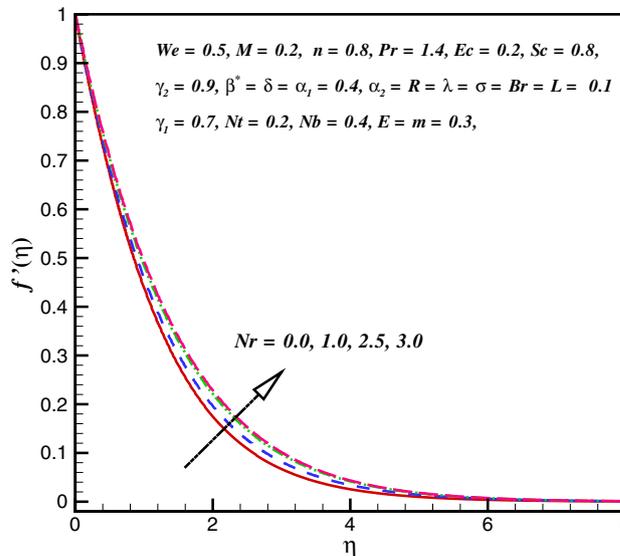


Fig. 2 $f'(\eta)$ via Nr

$$u \frac{\partial C}{\partial x} + v \frac{\partial C}{\partial y} = \frac{D_T}{T_\infty} \frac{\partial^2 T}{\partial y^2} + D_B \frac{\partial^2 C}{\partial y^2} - k_r^2 (C - C_\infty) \left(\frac{T}{T_\infty} \right)^m \exp \left(-\frac{E_a}{\kappa T} \right), \quad (4)$$

$$(0) = -\gamma_1 [1 - \theta(0)], \quad \theta(\infty) \rightarrow 0, \quad (12)$$

$$\phi'(0) = -\gamma_2 [1 - \phi(0)] \quad \phi(\infty) \rightarrow 0. \quad (13)$$

Non-dimensional form of variables occurring in Eqs. (8)–(13) is given below

$$M = \frac{\sigma^* B_0^2}{\rho_f c}, \quad Nr = \frac{gA_2(C_w - C_\infty)}{gA_1(T_w - T_\infty)} = \frac{Gr_x^*}{Gr_x}, \quad \lambda = \frac{gA_1(T_w - T_\infty)}{c^2 x} = \frac{Gr_x}{Re_x^2},$$

$$Pr = \frac{\nu}{\alpha}, \quad R = \frac{4\sigma^{**} T_\infty^3}{k_f m^*}, \quad Nb = \frac{\tau D_B (C_w - C_\infty)}{\nu}, \quad Nt = \frac{\tau D_T (T_w - T_\infty)}{\nu T_\infty}, \quad \sigma = \frac{kr^2}{c}, \quad (14)$$

$$Ec = \frac{c^2 x^2}{c_p (T_w - T_\infty)}, \quad We = \frac{\Gamma cx}{\nu}, \quad Sc = \frac{\nu}{D_B}, \quad E = \frac{E_a}{\kappa T_\infty}, \quad \delta = \frac{T_w - T_\infty}{T_\infty}, \quad \beta^* = \frac{\mu_\infty}{\mu_0}.$$

with constraints

$$u = U_w = cx, \quad v = 0, \quad -k \frac{\partial T}{\partial y} = h_f (T_f - T),$$

$$D_B \frac{\partial C}{\partial y} = h_\phi (C - C_\phi) \quad \text{at } y = 0, \quad (5)$$

$$u \rightarrow 0, \quad T \rightarrow T_\infty, \quad C \rightarrow C_\infty \quad \text{as } y \rightarrow \infty. \quad (6)$$

Considering the following transformations

$$\eta = y \sqrt{\frac{c}{\nu}}, \quad v = -\sqrt{c\nu} f(\eta), \quad u = cx f'(\eta)$$

$$\theta(\eta) = \frac{T - T_\infty}{T_f - T_\infty}, \quad \phi(\eta) = \frac{C - C_\infty}{C_\phi - C_\infty}. \quad (7)$$

Conservation law of mass is verified identically, and remaining flow expressions become

$$[\beta^* \{1 + (Wef'')^n\}^2 + (1 - \beta^*) \{1 + (1 - n)(Wef'')^n\}] f''' - [1 + (Wef'')^n]^2 [f'^2 + ff'' + \lambda(\theta + Nr\phi)] = 0, \quad (8)$$

$$\left(1 + \frac{4}{3}R\right) \theta'' + Pr \left[f\theta' + Nb\theta'\phi' + Nt\theta'^2 + Ec f'^2 \beta^* + (1 - \beta^*) \frac{Ec f''^2}{1 + (Wef'')^n} \right] = 0, \quad (9)$$

$$\phi'' + Sc \left[f\phi' + \frac{Nt}{Nb} \theta'' - \sigma(1 + \delta\theta)^m \phi \exp \left(-\frac{E}{1 + \delta\theta} \right) \right] = 0, \quad (10)$$

$$f(0) = 0, \quad f'(0) - 1 = 0, \quad f'(\infty) \rightarrow 0, \quad (11)$$

3 Quantities of physical interest

In this section, we express surface drag force (C_{fx}) and heat/mass transfer rates (Nu_x, Sh_x) in dimensional forms

$$C_{fx} = \frac{\tau_w}{\rho U_w^2}, \quad (15)$$

$$Nu_x = \frac{xq_w}{k(T_w - T_\infty)}, \quad (16)$$

$$Sh_x = \frac{xj_w}{D_B(C_w - C_\infty)}, \quad (17)$$

where

$$\tau_w = \mu \frac{\partial u}{\partial y} \left[\beta^* + (1 - \beta^*) \frac{1}{1 + \left(\Gamma \frac{\partial u}{\partial y} \right)^n} \right], \quad (18)$$

$$q_w = -k \frac{\partial T}{\partial y}, \quad J_w = -D_B \frac{\partial C}{\partial y}. \quad (19)$$

From Eq. (15) to (17), one obtains

$$C_{fx} Re_x^{1/2} = \left[\beta^* + (1 - \beta^*) \frac{1}{1 + (Wef''(0))^n} \right] f''(0), \quad (20)$$

$$Nu_x Re_x^{-1/2} = - \left[1 + \frac{4}{3}R \right] \theta'(0), \quad Sh_x Re_x^{-1/2} = -\phi'(0). \quad (21)$$

Where $Re_x = \frac{xU_w}{\nu}$.

4 Entropy generation

Here, dimensional form of entropy generation is expressed as

$$S_G = \frac{k_f}{T_\infty^2} \left[1 + \frac{16\sigma^* T_\infty^3}{3k_f k^*} \right] \left(\frac{\partial T}{\partial y} \right)^2 + \frac{\mu}{T_\infty} \left(\frac{\partial u}{\partial y} \right)^2 \left[\beta^* + (1 - \beta^*) \frac{1}{1 + \left(\Gamma \frac{\partial u}{\partial y} \right)^n} \right] + \frac{\sigma^* B_0^2 u^2}{T_\infty} + \frac{R_D}{C_\infty} \left(\frac{\partial C}{\partial y} \right)^2 + \frac{R_D}{T_\infty} \left(\frac{\partial T}{\partial y} \frac{\partial C}{\partial y} \right). \tag{22}$$

In dimensionless, one has

$$N_G = \alpha_1 \left[1 + \frac{4}{3} R \right] \theta'^2 + Br \left[\beta^* + \frac{(1 - \beta^*)}{1 + (We f'')^n} \right] f''^2 + MB r f'^2 + \frac{\alpha_2}{\alpha_1} L \phi'^2 + L \theta' \phi', \tag{23}$$

where

$$Br = \frac{\mu U_w^2}{\kappa \Delta T}, \quad \alpha_1 = \frac{\Delta C}{C_\infty}, \quad \alpha_2 = \frac{\Delta T}{T_\infty}, \tag{24}$$

$$N_G = \frac{\nu T_\infty S_G}{\kappa C \Delta T}, \quad L = \frac{R_D (C_w - C)}{k_f}.$$

Mathematically, *Be* is defined as

$$Be = \frac{\text{Entropy generation subject to heat and mass transfer}}{\text{Total entropy generation}}, \tag{25}$$

$$Be = \frac{\alpha_1 \theta'^2 + \frac{\alpha_2}{\alpha_1} L \phi'^2 + L \theta' \phi'}{\alpha_1 \theta'^2 + Br \left[\beta^* + \frac{1 - \beta^*}{1 + (We f'')^n} \right] f''^2 + MB r f'^2 + \frac{\alpha_2}{\alpha_1} L \phi'^2 + L \theta' \phi'} \tag{26}$$

5 Graphical consequences and physical argument

Here, our objective is to analyze the consequences of sundry non-dimensional variables on velocity, temperature, concentration, surface drag force, entropy optimization rate, Bejan

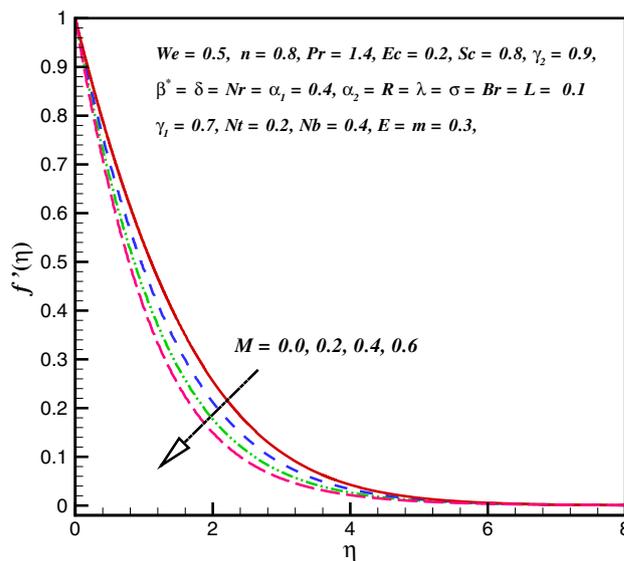


Fig. 4 *f'(\eta)* via *M*

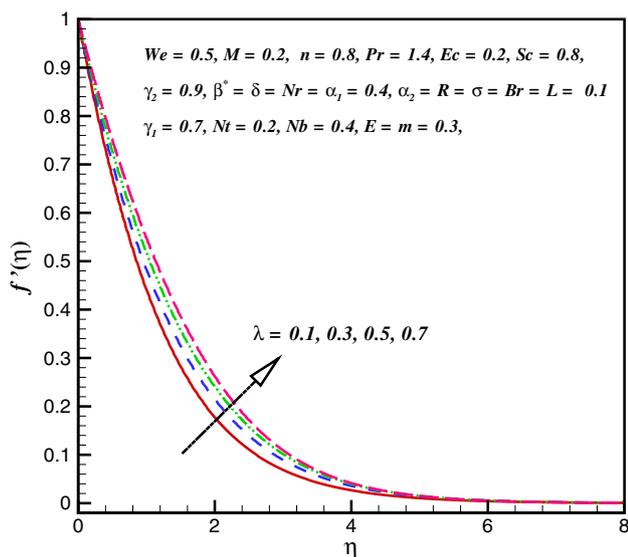


Fig. 3 *f'(\eta)* via λ

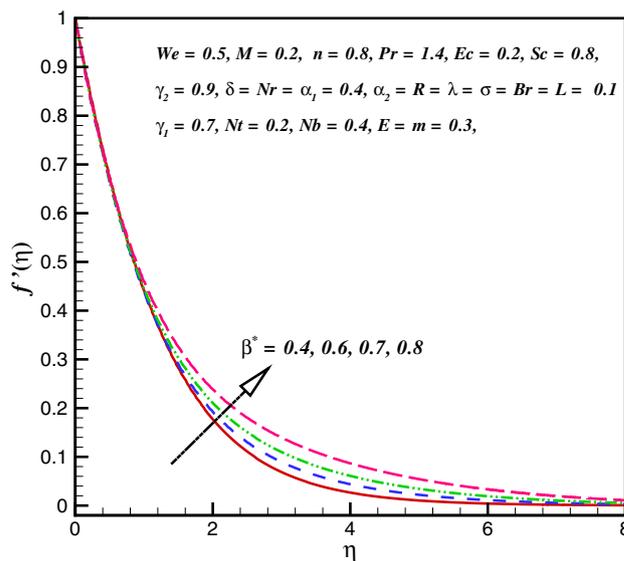


Fig. 5 *f'(\eta)* via β^*

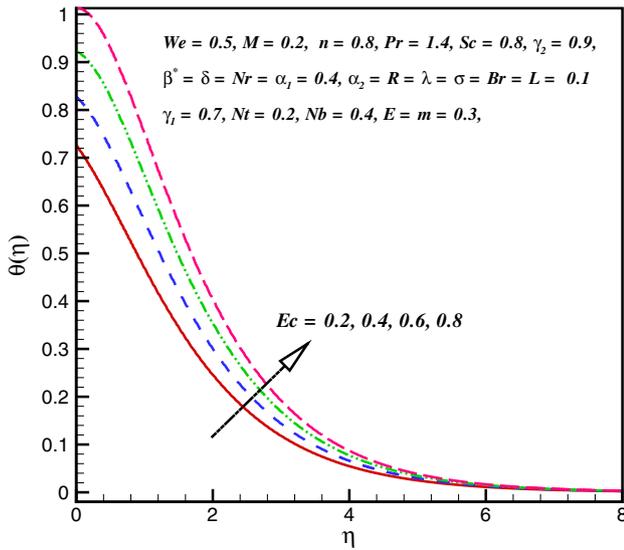


Fig. 6 $\theta(\eta)$ via Ec

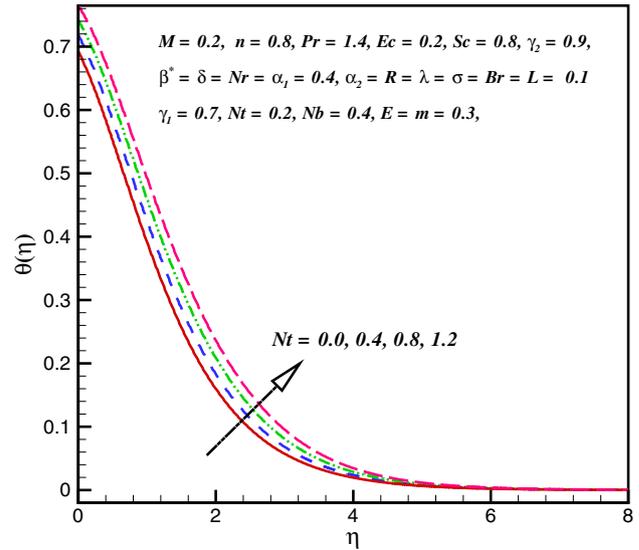


Fig. 8 $\theta(\eta)$ via Nt

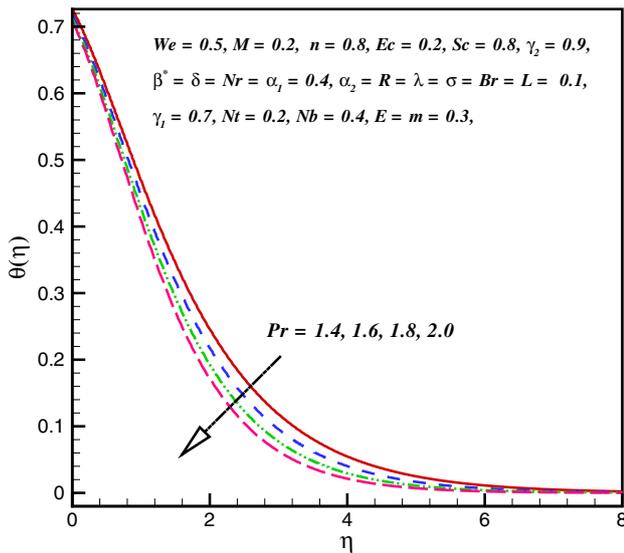


Fig. 7 $\theta(\eta)$ via Pr

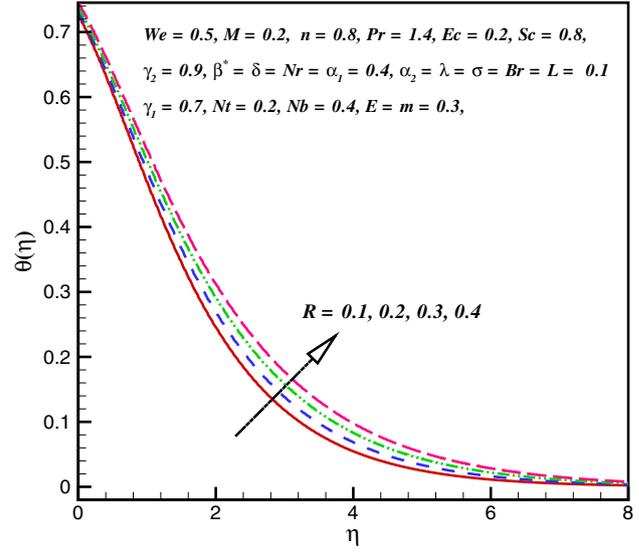


Fig. 9 $\theta(\eta)$ via R

number and heat/mass transfer rate. System of nonhomogeneous ODEs Eq. (8)–(10), (23) and (26) subjected to conditions given in Eq. (11)–(13) is solved by using MATLAB tool bvp4c.

Figure 1 captures influence of We on $f'(\eta)$. Here, we noticed that for larger values of We the $f'(\eta)$ is decreased. Figure 2 depicts outcomes of Nr on velocity profile ($f'(\eta)$). Clearly, $f'(\eta)$ enhances against Nr . Figure 3 disclosed the effect of λ on velocity profile ($f'(\eta)$). Here, one can note that $f'(\eta)$ is raised against λ . In fact, buoyancy forces rise for larger λ due to which velocity of cross-liquid intensifies.

Variation of velocity profile ($f'(\eta)$) through magnetic parameter M is examined in Fig. 4. Obviously, $f'(\eta)$ decreased by M . Lorentz force has direct relation with magnetic parameter M . Thus, for higher values of M , the Lorentz force enhances and consequently more resistance decays the fluid motion. Figure 5 shows aspects of β^* on $f'(\eta)$. For higher estimation of β^* , the velocity of cross-nanofluid intensifies.

Behaviors of Ec (Eckert number), Pr (Prandtl number), Nt (thermophoresis parameter) R (radiation parameter) and β^* (ratio of the infinite shear rate viscosity to the zero shear rate viscosity) on $\theta(\eta)$ are sketched in Figs. 6, 7, 8, 9 and 10.

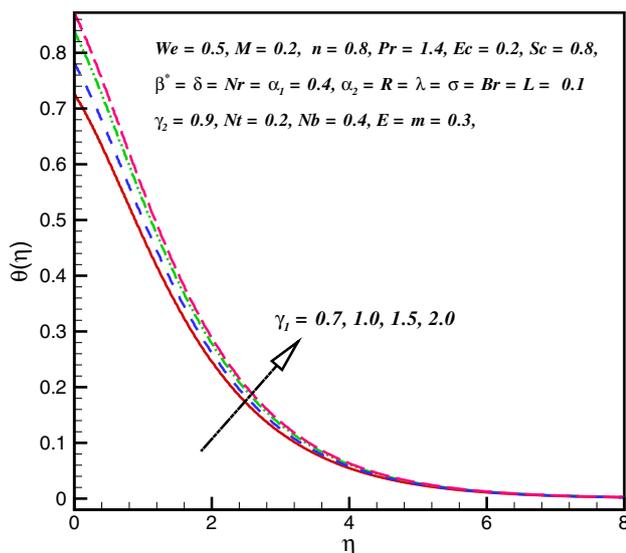


Fig. 10 $\theta(\eta)$ via γ_1

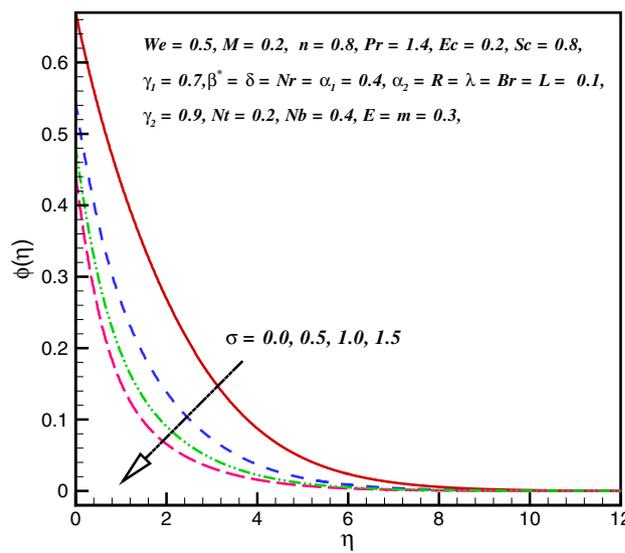


Fig. 12 $\phi(\eta)$ via σ

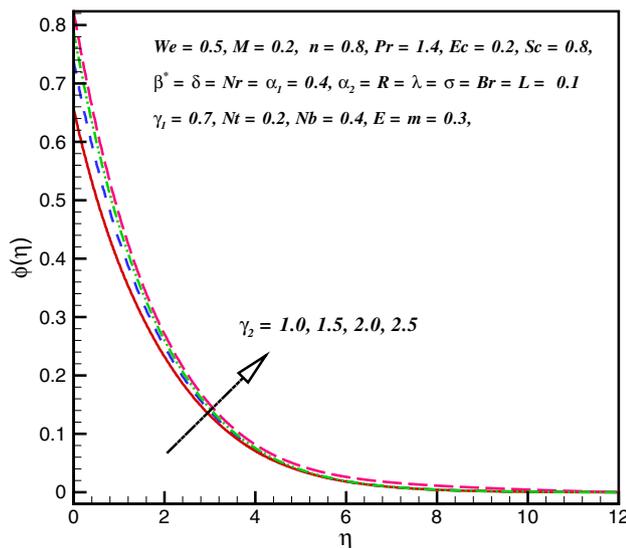


Fig. 11 $\phi(\eta)$ via γ_2

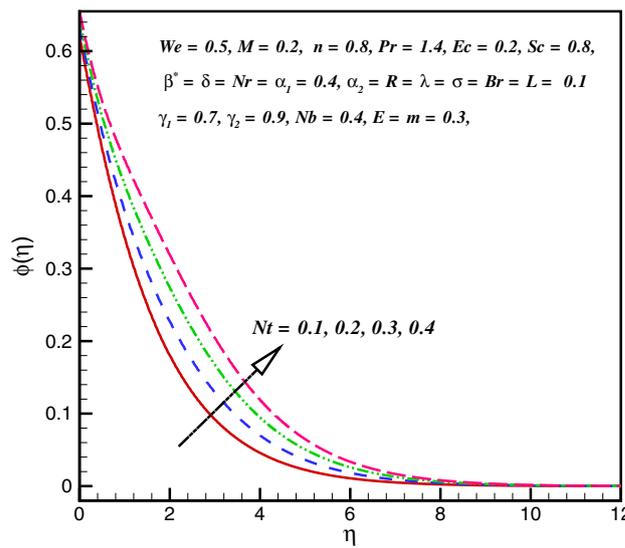


Fig. 13 $\phi(\eta)$ via Nt

Figure 6 addresses the Ec impact on $\theta(\eta)$. Clearly, cross-nanoliquid thermal field remarkably enhances via Ec . In fact, Ec is the ratio between KE (kinetic energy) and enthalpy difference. Consequently, larger Ec generates more resistance in liquid motion and therefore $\theta(\eta)$ intensifies. Figure 7 shows the behaviors of Pr on $\theta(\eta)$. It is perceived that $\theta(\eta)$ declined for larger Pr . Physically, thermal diffusivity deteriorates for large Pr and consequently, $\theta(\eta)$ decreases. Aspects of Nt on $\theta(\eta)$ are shown in Fig. 8. An increase in Nt leads to an enhancement in $\theta(\eta)$. Physically, reason behind this trend of Nt is the gap between reference and surface temperature. For larger Nt , this gap rises and consequently the kinetic

energy of nanoparticles enhances. So, $\theta(\eta)$ intensifies. $\theta(\eta)$ is raised against R . These features are reported in Fig. 9. Effect of γ_1 on $\theta(\eta)$ is depicted in Fig. 10. It can be seen from Fig. 10 that $\theta(\eta)$ intensifies via γ_1 . Physical reason behind this trend of γ is that less resistance is faced by the thermal wall which causes an enhancement in convective heat transfer to the fluid.

Rheological properties of Sc (Schmidt number), γ_2 (concentration Biot number), σ (dimensionless reaction rate), N_t (thermophoresis parameter), N_b (Brownian motion parameter) on concentration $\phi(\eta)$ are explored in Figs. 11, 12, 13, 14 and 15. Figure 11 captures influence of γ_2 on $\phi(\eta)$. Here,

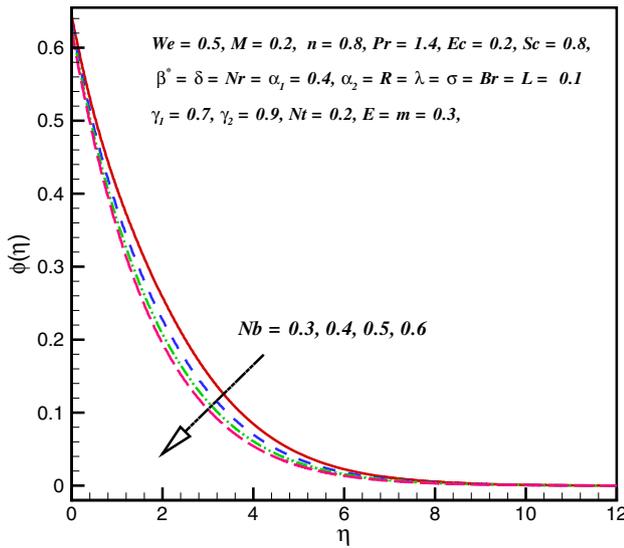


Fig. 14 $\phi(\eta)$ via N_b

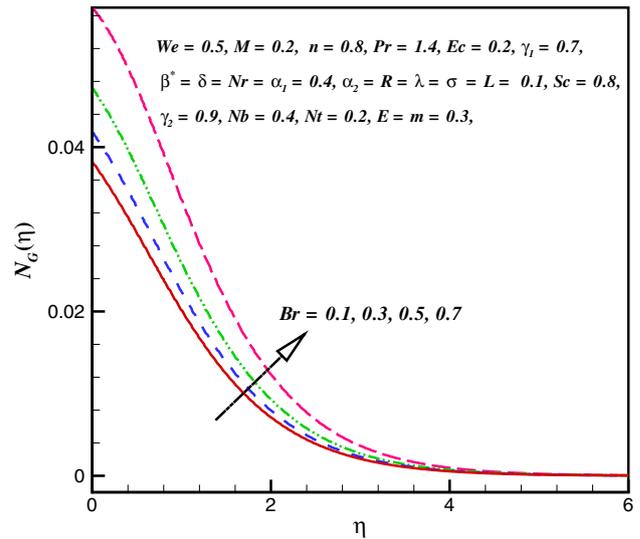


Fig. 16 $N_G(\eta)$ via Br

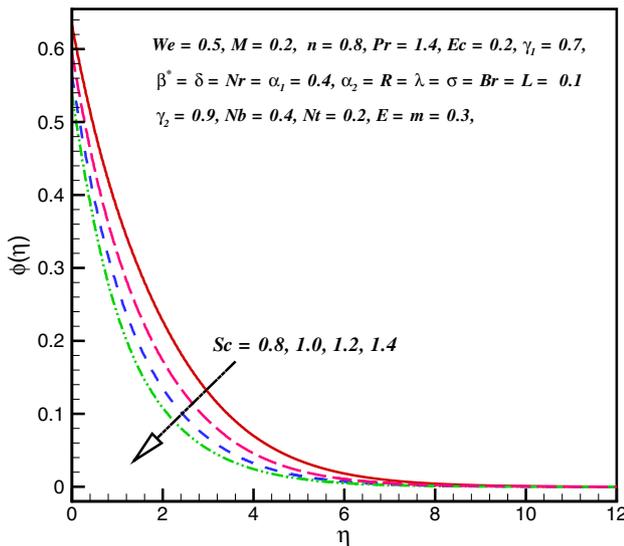


Fig. 15 $\phi(\eta)$ via Sc

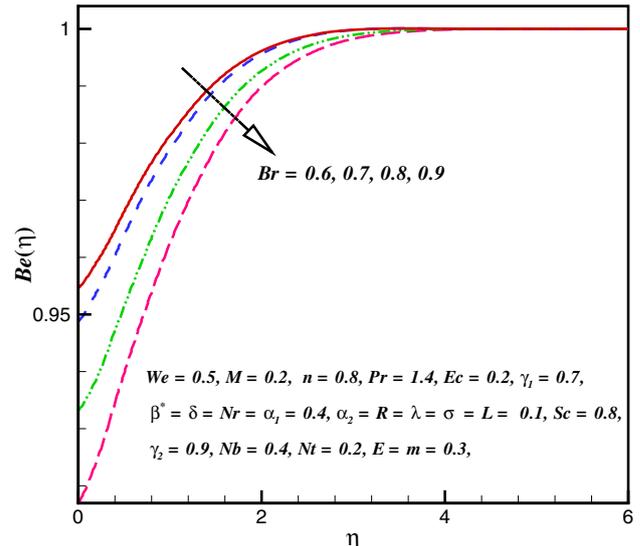


Fig. 17 $Be(\eta)$ via Br

we noted that for larger values of γ_2 the $\phi(\eta)$ is augmented. Figure 12 describes the influence of σ on $\phi(\eta)$. Concentration $\phi(\eta)$ deteriorates via σ . Figures 13 and 14 demonstrate the behavior of N_t and N_b on concentration $\phi(\eta)$. Concentration of cross-nanoliquid $\phi(\eta)$ is enhanced with larger N_t , while $\phi(\eta)$ declines for greater N_b . In fact, when we rise N_t gap of temperature between surface and at infinity intensifies due to which nanofluid moves from higher temperature to lower temperature. Consequently, $\phi(\eta)$ intensifies. Effects of Sc on $\phi(\eta)$ are reported in Fig. 15. Clearly, $\phi(\eta)$ deteriorates via larger Sc .

Variations of N_G (entropy generation) and Bejan number (Be) through Br (Brinkman number), L (diffusive variable),

M (magnetic parameter), α_1 (dimensionless concentration ratio variable), α_2 (dimensionless temperature ratio variable) and R (thermal radiation parameter) are presented through Figs. 16, 17, 18, 19, 20, 21, 22, 23, 24. Figures 16 and 17 examined the characteristics of Br on N_G and Be . Clearly, N_G are boosted via larger Be , while Be declines for greater Be . Physically, greater Br provides low thermal conduction to nanofluid and consequently, N_G intensifies for larger Br . Outcomes of L (diffusive variable) on N_G are disclosed in Fig. 18. N_G declines for higher values of L . Figures 19 and 20 depict outcomes of M (magnetic parameter) on N_G (entropy generation) and Be (Bejan number).

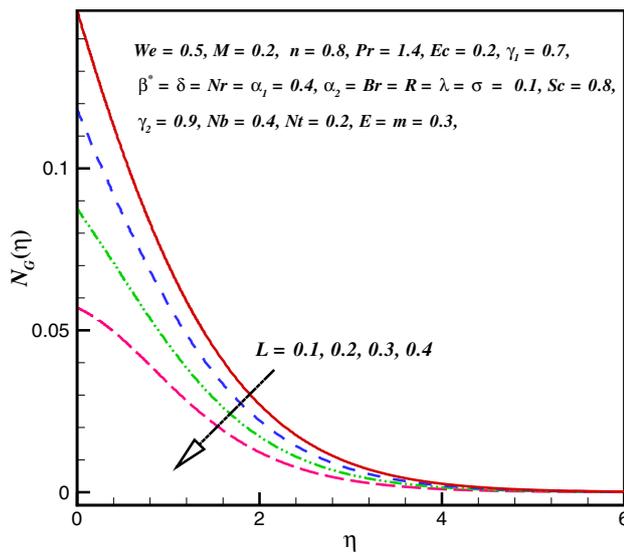


Fig. 18 $N_G(\eta)$ via L

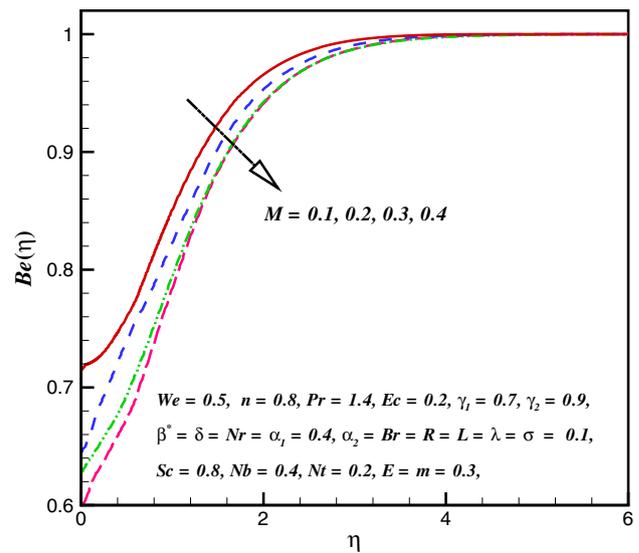


Fig. 20 $Be(\eta)$ via M

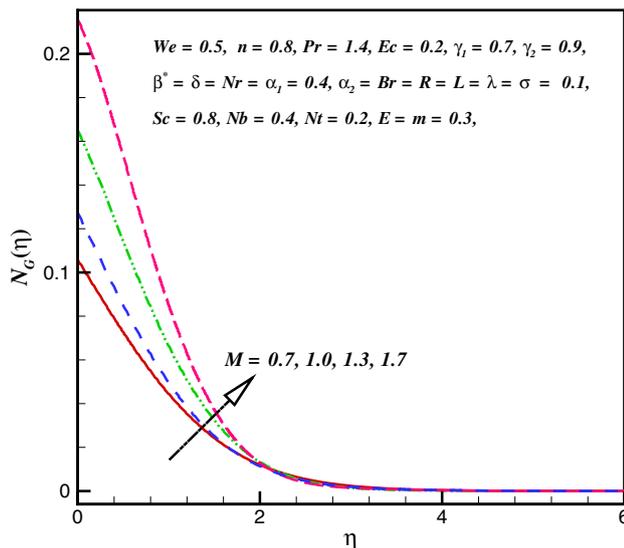


Fig. 19 $N_G(\eta)$ via M

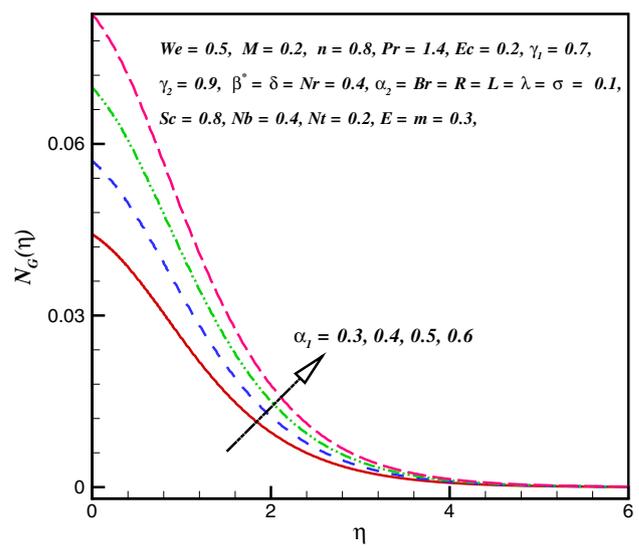


Fig. 21 $N_G(\eta)$ via α_1

Clearly, N_G boosts against M , while Be deteriorates for M . Greater estimation of M (magnetic parameter) offers more resistance to the motion of fluid in system and therefore, heat in the system intensifies. Consequently, entropy rate rises. Impact of α_1 (dimensionless concentration ratio variable) and α_2 (dimensionless temperature ratio variable) on entropy rate N_G is presented in Figs. 21 and 22. Here, N_G is an increasing function of α_1 and α_2 . Figures 23 and 24 report the impact of R (thermal radiation parameter) on N_G and Be . Clearly, N_G shows rising trend for R , while opposite trend is detected for Be . In fact, rise in R produces greater inertial force, so viscous force deteriorates and therefore the entropy rate intensifies.

Features for n (Power law index), M (magnetic parameter), Ec (Eckert number), Pr (Prandtl number), N_r (buoyancy ratio parameter), N_t (thermophoresis parameter) R (radiation parameter) and β^* (ratio of the infinite shear rate viscosity to the zero shear rate viscosity) on skin friction ($Re^{1/2} C_{fx}$) Nusselt and number ($Nu_x Re_x^{-1/2}$) are computed in Tables 1 and 2. Here, we observed that surface drag force boosts via larger We and M , whereas it declines for larger λ , n and β^* . Table 2 is prepared to point out aspects of numerous physical parameters on ($Nu_x Re_x^{-1/2}$). It is scrutinized that transportation rate of heat intensifies via larger Pr , whereas it decays for larger Ec , N_t and N_b .

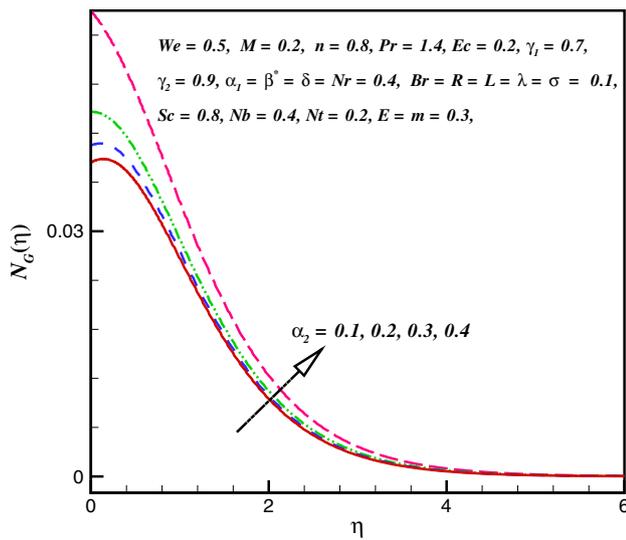


Fig. 22 $N_G(\eta)$ via α_2

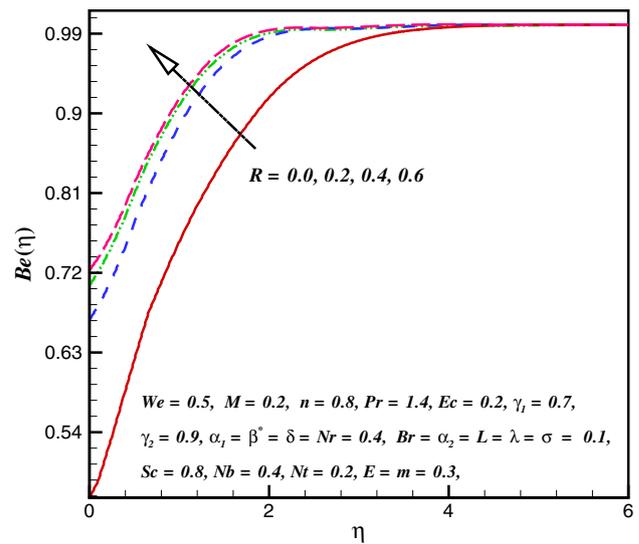


Fig. 24 $Be(\eta)$ via R

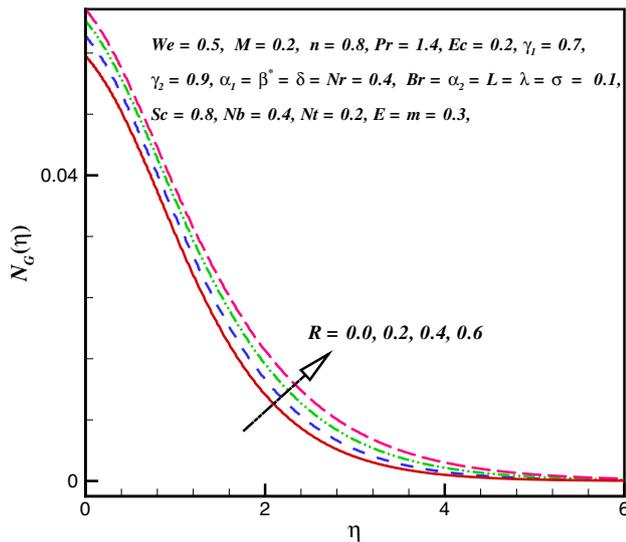


Fig. 23 $N_G(\eta)$ via R

6 Concluding remarks

We have the following significant observations.

- Lorentz’s force for cross-nanoliquid is used as resistive force which controls the liquid motion.
- Velocity is increasing function of β^* .
- Temperature $\theta(\eta)$ intensifies via N_t and N_b , while it is reduced with Pr .
- Enhancement in $\phi(\eta)$ (Concentration) occurs for augmented values of E (activation energy).
- N_G (rate of entropy generation) boosts for larger Br (Brinkman number), M (magnetic parameter), α_1 (dimensionless concentration ratio variable), α_2 (dimensionless temperature ratio variable) and R (thermal radiation parameter); however, it decayed via larger L (diffusive variable).
- Bejan number (Be) rises for greater estimation of R (thermal radiation parameter), while it deteriorates for Br (Brinkman number).

Table 1 Surface drag force ($Re^{1/2}C_{fx}$) via different estimation of physical parameters

We	n	λ	β^*	M	Nr	$-Re^{\frac{1}{2}}C_{fx}$
0.5	0.1	0.1	0.4	0.1	0.2	1.018466
0.8						1.9379354
1.0						1.8971728
1.2	0.2					0.8544199
	0.5					0.7075146
	0.8					0.5757617
		0.2				0.8001096
		0.3				0.6210907
		0.5				0.5359078
			0.6			0.9033084
			0.8			0.8808326
			1.0			0.8649508
				0.3		0.7913559
				0.5		0.8234892
				0.7		0.8827631
					0.3	0.858133
					0.4	0.8596886
					0.5	0.8822489

Table 2 Computational outcomes for rate of heat transfer ($Re^{-1/2}Nu$)

β^*	Pr	Ec	Nt	Nb	R	$Nu_x Re^{-\frac{1}{2}}$
0.0	0.2	0.1	0.2	0.4	0.5	0.202193
0.1						0.18603
0.2						0.178439
0.4	0.5					0.228093
	0.7					0.25841
	0.9					0.284055
		0.3				0.163207
		0.7				0.147585
		0.9				0.108134
			0.5			0.169995
			0.8			0.169995
			1.0			0.168315
				0.5		0.170431
				0.6		0.169881
				0.7		0.169451
					0.8	0.20144
					1.0	0.181581
					1.2	0.175118

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