#### **ORIGINAL PAPER**



# **Removal of ammonia by bioflters with straight and wavy lamellar plates**

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#### **Abstract**

The aim of the study was to evaluate the performance of two newly developed plate-type bioflters in treating air contaminated with ammonia vapour at diferent inlet air temperatures (24, 28, and 32 °C). The bioflters had two diferent structures, straight lamellar plates (SLP) and wavy lamellar plates (WLP), with both having a built-in capillary system for humidifying the packing material made of synthetic hydrophilic fbres and wood fbre. In the packing material of the bioflters, diferent types of microorganisms were used, including bacteria, micromycetes and yeast. The efficiency of ammonia removal from the air using the biofilters with the two different plate types was investigated. The treatment efficiency of air-containing ammonia vapour reached 81.0–85.2% and 84.2–87.0% in bioflters with SLP and WLP, respectively. The highest ammonia treatment efficiency was obtained in the biofilter with WLP at 28  $^{\circ}$ C with 87.0% of ammonia being removed. The latter removal efficiency was obtained when a large population of the microorganisms was present with  $1.0 \pm 0.2 \times 10^7$ ,  $1.0 \pm 0.5 \times 10^7$ and  $1.6 \pm 0.1 \times 10^9$  CFU/g of micromycetes, yeast and bacteria, respectively. The results also demonstrated that at different temperatures of polluted air, diferent microorganisms predominated in the packing material of the bioflters.

**Keywords** Biofltration · Microorganisms · Nonwoven caulking material · Wood fbre

# **Introduction**

Ammonia is a colourless gas with a strong odour that is generated from organic waste treatment plants and other industrial sources (Baquerizo et al. [2005](#page-8-0)). The process of air purifcation through biofltration has attracted considerable attention with bioflters being used increasingly often to remove odours (Malhautier et al. [2005\)](#page-9-0), toxic materials and volatile organic compounds (VOCs), such as  $NH<sub>3</sub>$  (Chen et al. [2005](#page-9-1)), from air. Compared to traditional air treatment methods, biofltration is an inexpensive and efective air purifcation technique (Baquerizo et al. [2005](#page-8-0); Zigmontienė and Žarnauskas [2011\)](#page-9-2).

Bioflters are biological systems accommodating a variety of microorganisms, such as bacteria and fungi (Martens

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 $\boxtimes$  T. Januševičius tomas.janusevicius@vgtu.lt et al. [2001\)](#page-9-3). A bioflter is made of one or several beds consisting of activated biological or synthetic materials (Liang et al. [2000\)](#page-9-4) functioning as a medium that provides nutrients for microorganisms that form a bioflm on the surface of the material used. The pollutant is absorbed into the bioflm where aerobic biodegradation of the pollutants occurs (Chen et al. [2005\)](#page-9-1). Peat (Zilli et al. [2001](#page-9-5)), soil, wood chips or mixtures of these substances (Pagans et al. [2005](#page-9-6)) are the most common materials used in the biological removal of organic pollutants. Other materials, such as pine bark, sewage sludge, yard waste compost and other various types of waste, are used worldwide (Hort et al. [2009;](#page-9-7) Nicolai and Janni [2001](#page-9-8)). However, natural organic packing materials have a short period of usefulness and must be replaced within 3–5 years (Tymczyna et al. [2004](#page-9-9)). To avoid this issue, synthetic inert packing materials, such as plexiglass chips (Chan and Lai [2010\)](#page-8-1), polyurethane foam cubes (Van Groenestijn and Liu [2002](#page-9-10)) or others that have high durability, have also been used for biofiltration. For the efficient elimination of high VOC concentrations, the constituents in the packing materials of bioflters should be made of several diferent materials (natural and synthetic) (Hernández et al. [2010](#page-9-11)). The use of packing materials consisting of two



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diferent components provides a larger reactive surface area and greater durability than packing materials produced from a single material (Chan and Lai [2010;](#page-8-1) Liang et al. [2000\)](#page-9-4).

Bacteria, yeast and fungi are microorganisms that are most frequently applied in biofilters (Zigmontienė and Baltrėnas [2004\)](#page-9-12). Microorganism biomass is inoculated into the packing material, which is then humidifed with an activated nutrient-rich solution (Baltrenas and Zagorskis [2009](#page-8-2)). Biofltration is based on the degradation of VOCs using specifc cultures of microorganisms, such as *Pseudomonas fuorescens* (Kleinheinz et al. [1999\)](#page-9-13) and *Pseudomonas putida*. To remove VOCs from polluted air, the bacteria *Aureobasidium pullulans*, *Penicillium* sp., *Acremonium strictum*, *Gliocladium viride*, *Aspergillus versicolor* and *Cladosporium herbarum* are suitable. Zhang and Pierce [\(2009](#page-9-14)) used *Rhodococcus* bacteria to decompose VOCs, resulting in a treatment efficiency of approximately 90%. Researchers from Italy and Tunisia have also used *Rhodococcus* bacteria to remove VOCs, arguing that these bacteria can purify VOCs with a treatment efficiency fluctuating from  $81$  to  $100\%$ (Borin et al. [2006\)](#page-8-3). The number of bacteria in the packing material must vary from  $10^8$  to  $10^{10}$  CFU/g (Malhautier et al. [2005](#page-9-0)). To promote the growth of microorganisms and their ability to remove VOCs from the polluted airfow, favourable conditions for the development of the microorganisms must be ensured (Baltrėnas and Zagorskis [2010](#page-8-4)).

The biodegradation of VOCs using microorganisms depends on diferent parameters (i.e. temperature, humidity and pH in bioflters) (Yoon and Park [2002\)](#page-9-15). The air temperature in biofilters has a significant impact on the efficiency of the biofltration process as it plays an important role in the development and growth of diferent microorganisms. Thus, temperature is a crucial parameter for the efective performance of a biofilter. Asadi et al.  $(2009)$  $(2009)$  examined the efficiency of a bioflter in the removal of acetone vapour from air using *P. putida* bacteria and found that an air treatment efficiency of  $80.5\%$  was reached when the inlet air temperature in the bioflter varied from 25 to 55 °C. An investigation of an airfow polluted with toluene vapour has suggested that the most efective biodegradation of this pollutant occurs at an air temperature of 30–35 °C (Yoon and Park [2002](#page-9-15)). To remove xylene from an airfow, Lee et al. [\(2002](#page-9-16)) reported that an optimal temperature of 30-35  $\degree$ C is required. The effectiveness of biofiltration of air polluted by  $NH<sub>3</sub>$  vapour from a composting process has been assessed using an air temperature of 35 °C in the bioflter (Pagans et al. [2005](#page-9-6)). A previous study on the treatment efficiency of a biofilter showed that a high biofilter purification efficiency can be obtained when the air humidity varies between 85 and 95% and when the air temperature in the bioflter fuctuates from 25 to 35 °C (Chang and Lu  $2003$ ). When a biofilter operates at higher temperatures, the population of microorganisms that adapts to higher temperatures increases in the medium.



A reduction in the temperature of the bioflter system to ambient temperature may lead to a decrease in the population of these microorganisms and can promote the development of other microorganisms in the bioflter. Thus, to achieve optimal results, the air temperature in the bioflters should vary between 20 and 40 °C (Leson and Winer [1991](#page-9-18)).

Various bioflter designs have been used to remove VOCs from contaminated air (Farrokhzadeh et al. [2017;](#page-9-19) Lith et al. [1997](#page-9-20)). However, there is a lack of studies that apply lamellar plate-type bioflters for ammonia treatment. In addition, natural organic packing materials (Yoon and Park [2002\)](#page-9-15) often used in bioflters have low durability and are more easily susceptible to degradation than synthetic materials (Chitwood and Devinny [2001\)](#page-9-21). Therefore, two pilot platetype bioflters with straight lamellar plates (SLP) or wavy lamellar plates (WLP) were constructed in this study for use with improved packing material and its associated humidifcation system for the air biofltration of ammonia. The wood fbre used in the packing material was thermally treated to improve its durability and suitability for the growth of microorganisms. Because the developed bioflters use a capillary system to humidify the packing material, they do not require additional energy for the humidifcation of packing material. To reduce the resistance of airfow in bioflters, millimetre gaps between the plates of the packing material were made. The advantage of a lamellar plate structure is that the airfow resistance in the bioflters is reduced and no anaerobic zones remain where contaminants are not cleaned.

Using the newly developed bioflters with SLP and WLP, the aim of this study was to assess the efficiency of the biofltration process of ammonia-contaminated air while maintaining diferent air temperatures and cultures of microorganisms in the bioflter. The second aim of this study was to assess the impact of the waviness of the plates in the bioflter on air treatment efficiency.

The effectiveness of the biofilters was studied at Vilnius Gediminas Technical University. Identifcation and quantifcation of the microorganisms were performed at Nature Research Centre (Vilnius, Lithuania). All experiments were performed between 2015 and 2019.

# **Materials and methods**

For this study, bioflters used as biological air treatment equipment were constructed (Fig. [1](#page-2-0)). The output of the bioflters with SLP (Fig. [1a](#page-2-0)) and WLP (Fig. [1](#page-2-0)b) reached  $100 \text{ m}^3/\text{h}$ .

Table [1](#page-3-0) shows the technical characteristics of the bioflters. The packing material was made of hydrophilic synthetic texture [i.e. nonwoven caulking material (NWCM)] with a mass of 400–500  $g/m^2$  and thermally treated (in a steam explosion reactor at 235 °C and under 32 bars



<span id="page-2-0"></span>**Fig. 1** Schemes of the lamellar structure bioflters equipped with a capillary system for humidifying the packing material. **a** Biofltration system made with straight lamellar plates. **b** Biofltration system made with wavy lamellar plates. [1](#page-2-0)—The inlet duct of the contami-

nated air; 2—valve; 3—blower; 4—electric heater with the thermostat; 5—sampling sites (X1—before the bioflter, X2—after the bioflter); 6—air duct of the purifed air; 7—temperature sensor; 8 plates; 9—perforated plate

of pressure) wood fbre (WF) attached to both sides of the NWCM. Both types of the bioflters had a structure of 44 plates arranged next to each other at a distance of  $4 \pm 0.2$  mm. The capillary effect promotes the humidification of packing material when the water rises through the pores of the WF and NWCM with small distances between the plates.

The length, height and thickness of a single plate were 0.8 m, 1.3 m and 0.01 m, respectively, while the length, width and height of the equipment were 0.85 m, 0.7 m and 2.0 m, respectively.

## **Operating principle of bioflters with straight and wavy lamellar plates**

Figure [1](#page-2-0) shows the schemes of the bioflters with SLP and WLP. The ammonia-contaminated air was supplied to the bioflter through the inlet duct (1). The inner diameter of the inlet duct was 40 mm. A valve (2) installed in the inlet duct controlled the airfow rate. To measure the studied parameters, a sampling site was generated in the inlet duct. The contaminated airfow passed to the casing equipped with the biofltration system. Through a perforated plate (9), the airfow was distributed



No.	Parameter	Parameter value
1.	Biofilter dimensions $(l \times b \times h)$	$0.85 \times 0.70 \times 2.00$ m
2.	Biofilter cartridge dimensions $(l \times b \times h)$	$0.80 \times 0.65 \times 1.30$ m
3.	The packing material of biofilters	Lamellar plates
4.	Biofilter output	$100 \text{ m}^3/\text{h}$
5.	Temperature of biomedium	$24 - 32$ °C
6.	Humidity of packing material	70-80%
7.	pH of biomedium	7.0
8.	Contaminant	Ammonia
9.	Initial concentration	$300 \text{ mg/m}^3$

<span id="page-3-0"></span>**Table 1** Technical characteristics of bioflters

throughout the entire packing material. The contaminated air moved between the plates of the packing material immersed in a solution and arranged at a distance of  $4 \pm 0.2$  mm from each other towards the outlet. The treated airfow passed to the outlet duct (6), which had an inner diameter of 96 mm and was discharged. To measure the studied parameters, an opening (X2) in the outlet duct was made. The humidity of the packing material, the temperature of the liquid medium and airfow were regularly maintained. The temperature of the liquid medium was regulated with the aid of an electric heater (4), whereas the air temperature was controlled using a channel heater installed under the blower (3) of the supplied air.

Mesophilic microorganisms were used in the bioflters developed in this study. Mesophiles are microorganisms that develop at temperatures from 20 to 45 °C (Schiraldi and De Rosa [2014](#page-9-22)). Because the optimum growth temperature of most of these organisms ranges from 25 to 37 °C (Abdel-Banat et al. [2010\)](#page-8-6), the assays were conducted at temperatures suitable for the development of mesophilic organisms (24, 28 and 32 °C). The tests were performed in the laboratory premises. Ammonia was evaporated using an electric stove, and the released ammonia vapour was supplied through a duct into the bioflter.

In the bioflter, the air was heated to the desired temperature by heating elements. The same temperatures (24, 28 and 32 °C) were also maintained in the reservoir at the bottom of the bioflter biomedium, which humidifes the bioflter plates via the capillary efect.

#### **Determining liquid medium pH and temperature**

The porous plates of the packing material were immersed into the liquid medium (biomedium) saturated with nutrients. Table [2](#page-3-1) shows the composition of used biomedium. The pH of the biomedium was maintained using buffer solutions. The pH value and temperature were measured daily.

The nutrients used in the medium were selected based on literature (Chang and Lu [2003](#page-9-17); Den et al. [2004](#page-9-23); Chen et al. [2005](#page-9-1); Trejo-Aguilar et al. [2005;](#page-9-24) Liao et al. [2008](#page-9-25); Ryu et al. [2010](#page-9-26); Lebrero et al. [2013\)](#page-9-27).

<span id="page-3-1"></span>

# **Determining air temperature and humidity in the bioflter**

The measurements of air temperature and humidity in the bioflter were performed using a TESTO 400 instrument. The air temperature and humidity were measured at fve sites evenly distributed over the packing material and were monitored at airfow inlets and outlets 500 mm from the opening of the airfow inlet.

## **Determining packing material humidity**

The humidity of the packing material was measured using a M0290 moisture meter at five sites each day of the experiment. All the measurements were performed in triplicate.

# **Activation of packing material and determination of biofiltration efficiency**

The ammonia-contaminated air was supplied through the packing material of the bioflter. The airfow rate between the plates reached 0.16 m/s on average and was measured and monitored on a daily basis using a Testo 400 airfow instrument with an accuracy of  $\pm 0.01$  m/s.

Both native and introduced microorganisms were used in this study. Cultures of microorganisms were selected by performing separate assays using microbial cultures capable of efficiently breaking down ammonia. Eight strains of micromycetes (*A. strictum* 1–40-L, *A. versicolor* BF-4, *Aureobasidium pullulans* BF-58, *Cladosporium* sp. L-7 pp, *Penicillium* sp. BF-2, *G. viride* BF-81, *Stachybotrys* sp. BF-90 and *C. herbarum* 7KA), two strains of yeast (*Exophiala* sp. and *Aureobasidium pullulans* BIA1.1.2) and two strains of bacteria (*Rhodococcus* sp. 30 and *Bacillus subtilis* 28) were selected. The microorganisms were inoculated on biopacking material by seeding, and 2 L of active solution containing the selected microorganisms was sprayed onto the packing material. The average concentration of each microorganism in the solution was  $10^8$  CFU/g.

The study was divided into three stages (at temperatures of 24, 28, and 32  $^{\circ}$ C). Before exploring the efficiency of the bioflter to purify the air from the abovementioned pollutant, the microorganisms were acclimated for 15 days. The



concentration of the pollutant was  $300 \pm 25$  mg/m<sup>3</sup>. Ammonia-contaminated air was supplied to the bioflters each day of the experiment. Following the acclimation period, investigation of the biofiltration efficiency and quantification of the microorganisms in the packing material using the ammonia vapour-polluted air were performed for additional 10 days.

The efficiency of ammonia removal was calculated by measuring the inlet and outlet ammonia concentration. The concentration of the pollutant was determined using a MiniRAE 2000 photoionization detector. The ammonia removal rate (the amount of ammonia removed per hour, R), space velocity (the relationship between volumetric fow and volume of packing material, SV) and air cleaning efficiency (the percentage of ammonia removed, RE) were determined using the following equations (Kim et al. [2000](#page-9-28); Taghipour et al. [2006](#page-9-29)):

$$
R = \text{SV}(C_{\text{in}} - C_{\text{out}}), g \text{NH}_3/\text{m}^3/\text{h}
$$
 (1)

$$
SV = \frac{Q_{\text{in}}}{V_{\text{packing material}}}, 1/h
$$
 (2)

$$
RE = \left(1 - \frac{C_{\text{out}}}{C_{\text{in}}}\right) \times 100\%
$$
 (3)

where *R* is removal rate,  $g/m^3/h$ ;  $C_{in}$  is inlet ammonia concentration,  $g/m^3$ ;  $C_{\text{out}}$  is outlet ammonia concentration,  $g/m^3$ m<sup>3</sup>; SV is space velocity, 1/h;  $Q_{\text{in}}$  is volumetric flow rate, m<sup>3</sup>;  $V_{\text{packing material}}$  is volume of packing material,  $m^3$ ; and RE is air cleaning efficiency,  $%$ .

Before activating the packing material, the absorption of ammonia in water with biogenic elements was evaluated. Subsequently, experiments were repeated by inoculating the microorganism cultures into the bioflters.

## **Identifcation and quantifcation of the microorganisms in the packing material**

Packing material (1 g) was collected to identify and quantify microorganisms. Micromycetes were plated on an agar-solidifed beer wort medium in Petri dishes that were incubated at 28 °C for 6–7 days. Subsequently, pure micromycetes cultures were identifed using classical methods and descriptions for fungi (Ellis [1971](#page-9-30); Pitt [1979;](#page-9-31) Pečiulytė and Bridžiuvienė [2008](#page-9-32); Watanabe [2010](#page-9-33)). Yeast was plated on Rose Bengal CAF agar (Lioflchem, Italy) and Sabouraud agar with chloramphenicol (Lioflchem, Italy) in Petri dishes at 28 °C for 3–4 days. Yeast was identifed using an Api 20 C AUX (bioMérieux, France) system. To culture bacteria from the tested samples, selective agar-solidified cetrimide (*Pseudomonas* (cetrimide) agar), nutrient agar and agar-solidifed *Bacillus cereus* media were prepared. For seeding, bacterial suspensions at 1:10, 1:100, 1:1000, 1:10,000, 1:100,000, 1:1,000,000, 1:10,000,000,

1:100,000,000, 1:1,000,000,000 and 1:10,000,000,000 were prepared. Suspensions (0.1 ml) were poured onto the Petri dishes and rubbed with a spatula. Seeds were incubated at 28 °C for 2–4 days. The cultured bacteria were identifed considering their morphological, physiological and biochemical properties and compared with those reported in the literature. Bergey's Manual of Systematic Bacteriology was also used to identify bacteria (Palleroni [1984;](#page-9-34) Garrity [2005](#page-9-35)).

#### **Statistical analysis**

Microsoft Excel was used for statistical analysis. The measurements were repeated three times, and the mean and standard deviation of values were calculated. A one-way ANOVA test  $(p<0.05)$  was used to differentiate between the means of diferent microorganisms present at diferent temperatures.

# **Results and discussion**

Throughout the study, the air temperature in the bioflters was  $24 \pm 1$ ,  $28 \pm 1$  and  $32 \pm 1$  °C. By adjusting the inlet air temperature, the efect of air temperature on the degree of ammonia vapour removal was monitored (Figs. [2](#page-5-0), [3\)](#page-5-1). The temperature of the treated air difered slightly from the air temperature in the bioflters. In some cases, the temperature of the inlet air was higher to maintain a stable air temperature in the bioflters because the inlet air stream fowed through the 25-cm layer of water and became cooler. A supplied air temperature greater than 40 $\degree$ C may result in the death of the microorganisms unless thermophilic microorganisms are cultured in the bioflter (Leson and Winer, [1991](#page-9-18)).

Before inoculating the microorganisms, the ammonia absorption in water with nutrients reached  $75.0 \pm 2\%$  $75.0 \pm 2\%$  $75.0 \pm 2\%$ . Figures 2 and  $\overline{3}$  show the efficiency of the biofiltration process in the bioflters from 1 to 10 days after the acclimation period. Temperature is one of the most important factors determining the intensity of biochemical reactions and the growth of microorganisms (Leson and Winer [1991](#page-9-18)). At temperature of 24 °C, the purifcation of ammonia through the packing material made of NWCM and WF ranged from 81.0 to 84.0% and from 84.5 to 86.0% in the bioflters with SLP and WLP, respectively (Figs. [2,](#page-5-0) [3\)](#page-5-1). Increasing the temperature to 28 °C resulted in a slight but significant increase in filtration efficiency, ranging from 82.5 to 85.2% (Fig. [2](#page-5-0)) and 85.0–87.0% (Fig. [3\)](#page-5-1) in the bioflters with SLP and WLP, respectively. At 32  $\degree$ C, the air purification efficiency of the bioflter with the SLP ranged from 82.0 to 83.3% (Fig. [2](#page-5-0)), while that of the bioflter with WLP ranged from 84.2 to  $86.0\%$  (Fig. [3\)](#page-5-1). The effect of the temperature in the biofilters (between 24 and 32 °C) only slightly afected the ammonia removal efficiency. According to many studies, the optimum temperature for mesophilic microorganisms is between 20 and 35 °C (Delhoménie and Heitz [2005\)](#page-9-36). Signifcantly higher



<span id="page-5-0"></span>**Fig. 2** Dependence of air treatment efficiency on the time and air temperature of the bioflter with straight lamellar plates



<span id="page-5-1"></span>**Fig. 3** Dependence of air treatment efficiency on the time and air temperature of the bioflter with wavy lamellar plates

ammonia purification efficiency was obtained in the biofilter with WLP. In this type of bioflter, the path of the treated air was increased. Compared to the bioflter with SLP, the treated air was retained longer in the bioflter with WLP, enabling longer contact with the packing material. Blázquez et al. ([2017\)](#page-8-7) studied the treatment of  $NH<sub>3</sub>$  using a laboratory-scale biotrickling filter under different ammonia concentrations. When NH<sub>3</sub> contact time with a packed bed was long (at inlet air rate of 38.4 m/h), nitrifcation rate was twofold higher than that observed at short  $NH_3$  contact time (at inlet air rate of 844 m/h) owing to a better distribution of ammonia through the packed bed (Blázquez et al. [2017](#page-8-7)).

In the diferent types of bioflters, diferent tendencies of microorganisms' growth in the packing material were observed. When fltering ammonia from air in the bioflter with SLP, 2.0–9.6  $\times$  10<sup>6</sup>, 4.2  $\times$  10<sup>6</sup> to 5.6  $\times$  10<sup>7</sup> and 3.1  $\times$  10<sup>7</sup> to  $2.5 \times 10^8$  CFU/g of micromycetes, yeast and bacteria were observed at 24 °C, respectively (Fig. [4\)](#page-6-0). When the temperature was increased to 28 °C, a significant increase in the contents of all microorganisms was observed (for example, yeast levels increased to  $8.0 \times 10^8$  CFU/g). However, increasing the temperature to 32 °C had no signifcant impact on the growth of microorganisms in the packing material. In the bioflter with SLP at 32 °C, the population of microorganisms varied from  $1.0 \pm 0.2 \times 10^6$  to  $1.0 \pm 0.3 \times 10^8$  CFU/g of micromycetes and

When fltering ammonia in the bioflter with SLP, the composition of the types of micromycetes varied greatly depending on temperature. The fungus *Chaetomium* was dominant at 24 °C, whereas the fungus *Geotrichum* sp. was dominant at 28 °C. At the latter temperature, there were also many unidentifed bacteria present that were resistant to the antibiotic chloramphenicol. At 32 °C, the inoculated micromycete *C. herbarum* predominated.

The yeast *Exophiala jeanselmei* grew best at 24 °C. During the removal of ammonia at 28–32 °C, the number of *Ex. Jeanselmei* decreased. In contrast, during the removal of ammonia in the bioflter with SLP, other species of yeast were not detected.

During the acclimation period, the bacteria *B. subtilis*, *B. cereus*, *P. putida*, *P. fuorescens*, *Rhodococcus* sp. and *Staphylococcus aureus* predominated in the packing material of the bioflter with SLP. In most cases, the bacteria *B. subtilis*, *S. aureus*, *P. fuorescens*, *P. aeruginosa* and *Methylobacterium* sp. grew at 24 °C and the bacteria *B. subtilis*, *Rhodococcus* sp., *P. fuorescens*, *S. aureus* and *Methylobacterium* sp. grew at 28 °C. Moreover, the bacteria *B. subtilis*, *Pseudomonas aeruginosa*, *S. aureus*, *P. putida*, *Enterobacter* sp. and *Micrococcus* sp. grew at 32 °C. Interestingly, the inoculated bacterium *B. subtilis* grew at all temperatures during the process of ammonia vapour removal. Borowski et al. ([2017](#page-8-8)) used different types of bacteria in a microbial-mineral preparation for ammonia removal and observed that the most resistant strains of bacteria are *B. subtilis* and *P. fuorescens* during storage at 4 °C. Chung et al. [\(2001](#page-9-37)) studied the treatment of NH<sub>3</sub> and H<sub>2</sub>S using bioflters containing the bacteria *Arthrobacter oxydans* and *P. putida*, and they reported that ammonia and hydrogen sulphide removal is greater than 95 and 90%, respectively.

The variation in temperature in the bioflter with WLP did not signifcantly infuence the growth of microorganisms in the packing material. At 24 °C, the microorganism content in the packing material in the pilot-scale bioflter with WLP reached  $10^6 - 10^8$  CFU/g (Fig. [5\)](#page-7-0). While filtering ammonia at 28 °C, the content of yeast and microscopic fungi fluctuated from  $10<sup>6</sup>$  to  $10^7$  CFU/g. The content of bacteria did not exceed  $10^9$  CFU/g at 28 °C during the ammonia fltering process. At 32 °C, however, the content of microscopic fungi and yeast remained stable at  $10^7$  CFU/g, and the content of bacteria was  $10^9$  CFU/g.

During acclimation period, the fungus *Trichoderma* was dominant. After the microorganisms of the packing material were adapted to the ammonia, the fungus *Trichoderma* was replaced with micromycetes *Chaetomium* sp. and *Stachybotrys* sp. At the beginning of the ammonia vapour fltering process at 24 °C, however, *Trichoderma* sp. appeared again with *Chaetomium* sp., while it was close to the levels of *Geotrichum* sp at 28 °C. Furthermore, these micromycetes remained at the higher temperature of 32 °C where *Stachybotrys* sp. micromycetes could also be detected.

The adaptation of yeast in the packing material consisting of WLP to ammonia resulted in the number of yeast colonies *E. jeanselmei* being low. While removing ammonia vapour at 24–32 °C, only individual colonies of yeast *E. jeanselmei* were observed.

The removal of ammonia vapour showed that the number of bacterial species varied slightly at diferent temperatures. The bacteria *B. subtilis*, *P. fuorescens, S. aureus*, *P. putida* and *Rhodococcus* sp. were predominant at all investigated temperatures. Within the ammonia adaptation period, the bacterium *Burkholderia convexa* grew in addition to the abovementioned bacteria. At 24 and 28 °C, along with the previously mentioned bacteria, *P. aeruginosa* and *B. cereus*

<span id="page-6-0"></span>**Fig. 4** Changes in the number of microorganisms in the bioflter with straight lamellar plates during ammonia purifcation at temperatures of 24, 28 and 32 °C



Days after acclimation period of the microorganisms at different temperatures

<span id="page-7-0"></span>**Fig. 5** Changes in the number of microorganisms in the bioflter with wavy lamellar plates during ammonia purifcation at temperatures of 24, 28 and 32 °C



were predominant, and micromycetes began to develop. At 32 °C, the bacteria *B. convexa*, *Enterobacter* sp. and *Erwinia* sp. began to grow. At all investigated temperatures for ammonia removal, the inoculated bacterium *B. subtilis* grew.

Although the average number of diferent microorganisms in the bioflter with WLP was observed to be lower than that observed in the biofilter with SLP, the cleaning efficiency of this type of bioflter was higher. Thus, the bioflter design may have had a more significant contribution to  $NH<sub>3</sub>$  degradation than the number of microorganisms.

Determining the changes in the number of various microorganisms is important to understand the ammonia fltration process. The results obtained in this study showed that the assayed microorganisms (micromycetes, yeasts and bacteria) adapted to a packing material consisting of WF and NWCM in developed bioflters with SLP and WLP. The microorganisms in the packing materials of bioflters efectively degraded ammonia and were stable under diferent temperatures for relatively long biofltration conditions. The presence of a large number of bacteria, which had less infuence on the physical properties of packing material, allowed for the effective elimination of  $NH<sub>3</sub>$ from the air. In both bioflters, the number of yeast decreased from 1 to 10 days after the acclimation period at 28 °C. At this temperature, bacteria were predominant, suggesting that they significantly contributed to  $NH<sub>3</sub>$  degradation.

 $NH<sub>3</sub>$  may lower the durability of the biopacking material. Therefore, microscopic analysis of the structure of NWCM specimens of the tested bioflters was performed. NWCM specimens were assayed before and after the use of the bioflters for ammonia removal at different air temperatures with  $NH<sub>3</sub>$ concentration of 300 mg/m<sup>3</sup> and an airflow rate of 100 m<sup>3</sup>/h.

Figure [6](#page-8-9) shows the images of the surfaces of both NWCM sides. The images were magnified  $6 \times$  and  $25 \times$ , and they were acquired using a Motic optical microscope. The NWCM comprised a woven base from a flat 1-mm-wide



thread and smaller diameter fbre attached to the base. One side of the NWCM had a small amount of fbre and was named "base", and the other side was named "fbre". No extraneous formations were observed in the unprocessed specimens of the noncaulking material (Fig. [6a](#page-8-9)). After treatment with ammonia vapour, however, small quantities of a brown dispersible material were present on both sides of the SLP and WLP (Fig. [6b](#page-8-9)).

Electronic microscopy allowed determination of the structure of the materials used in this study (Fig. [7\)](#page-8-10). The results demonstrated that small 15- to 25-µm-thick flaments comprised a major part of the NWCM. The spacing between the flaments was 5–10 times larger than their thickness, allowing for bioflm formation and avoiding anaerobic zones that can inhibit the growth of microorganisms. The disordered deployment of the flaments increased the specifc surface area of the packing material and therefore the volume of the biomedium in it.

The results showed that an increase in the working time of the NWCM had no impact on its structure, which remained stable. However, an increase in operation time resulted in the increased amount of new brown-coloured formations on the side of the NWCM (Fig. [6\)](#page-8-9). These formations were observed on the NWCM of the bioflter with both SLP and WLP.

## **Conclusion**

The results obtained in this study showed that the cartridge of the bioflter consisting of wavy NWCM plates was superior to a bioflter consisting of straight plates. The results demonstrated that at an airfow rate of 0.16 m/s, the ammonia vapour removal efficiency reached  $81.0-85.2\%$  in the bioflter with SLP. When the bioflter with WLP was used, the efficiency of ammonia vapour removal reached 84.2–87.0%. In the bioflter with WLP, the contact time <span id="page-8-9"></span>**Fig. 6** The surface of NWCM of the bioflters after treatment with ammonia vapour **a** magnified  $6 \times$ . **b** magnified  $25 \times$ 





**Fig. 7** Structure of the nonwoven caulking material (magnified  $25 \times$ )

<span id="page-8-10"></span>between the packing material and the air contaminated with ammonia was 1.5 times longer, leading to increased air treatment efficiency. The wavy lamellar plate-type biofilter was  $\sim$  2–3% more efficient, and the structure was more rigid and stable, enabling it to retain more uniform spacing between the plates. Considering the reduction in ambient air pollution, a bioflter with WLP is benefcial because the manufacturing costs of straight and wavy NWCM plates are similar and the WF coating technology used is the same.

To achieve the air treatment efficiencies in the present study, an optimum mode for bioflter operation was maintained as follows: pH of 8.6, airfow humidity greater than 90%, aqueous medium temperature of 28–32 °C and airfow rate no greater than 0.16 m/s between the plates. Considering the growth of microorganisms in the packing materials of the pilot bioflters used in this study, 28 °C was the optimal temperature for the development of the microorganisms.

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#### **Compliance with ethical standards**

**Ethical approval** This article does not contain any studies with human participants or animals performed by any of the authors.

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