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Is filter packing important in a small-scale vermifiltration process of urban wastewater?

N. Lourenço¹ \cdot L. M. Nunes²

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Abstract Nowadays, natural resources are under increasing stress which fosters wastewater reuse planning and emphasizes on the decentralized wastewater treatment. Vermifiltration has been described as a viable alternative to treat domestic and urban wastewater, but few studies have focused on the impact of different filter packings on vermifiltration performance. This study evaluates the effect of vermicompost and sawdust in a single-stage vermifilter (VF) for urban wastewater treatment. After an acclimation period of 45 days, urban wastewater from a combined sewage collection system was applied continuously for 24 h. Earthworm stock density was of 20 $g L^{-1}$, HRT of 6 h, HLR of 0.89 m³ m⁻² day⁻¹ and OLR of 7.38 g BOD₅ day^{-1} . System performance was assessed by the removal efficiencies of BOD₅, COD, TSS, NH_4^+ , TN and TP, and fecal coliforms and helminth eggs elimination. Vermicompost (VE) and sawdust (SE) were tested, using an earthworm abundance of 20 g L^{-1} . Treatment efficiencies were 91.3% for BOD₅, 87.6% for COD, 98.4% for TSS and 76.5% for NH₄⁺ in VE, and 90.5% for BOD₅, 79.7% for COD, 98.4% for TSS and 63.4% for NH_4^+ in SE. Earthworms contributed to reduce NH_4^+ and TN removal and to increase $NO₃⁻$ concentration. No treatment was able to eliminate fecal coliforms down to guidelines values for wastewater irrigation as helminth eggs were completely

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 \boxtimes N. Lourenco nelsonlourenco@futuramb.com

Faculty of Sciences and Technology, Civil Engineering Research and Innovation for Sustainability Center, University of Algarve, Faro, Portugal

eliminated. Single-stage vermifiltration system using both filter packings is inconsistent and cannot meet EU guideline values for discharge in sensitive water bodies and WHO guidelines for irrigation with treated wastewater.

Keywords Wastewater - Vermifiltration - Vermicompost - Sawdust · Eisenia fetida

Introduction

Due to increasing world population, the natural resources are under increasing stress which fosters wastewater reuse planning and emphasizes on the decentralized wastewater treatment, especially in rural areas where high wastewater collection and treatment costs do not justify the installation of conventional wastewater treatment plants (WWTP) (Prasad and Kumar [2012\)](#page-10-0). Decentralized wastewater treatment systems involve the collection, treatment, disposal and reuse of wastewater from households, clusters of homes and isolated communities, at or near the point of generation (Li et al. [2009](#page-10-0)). Commonly, wastewater treatments must be able to reduce organic matter and nutrients concentration, but also promote fecal microorganisms' elimination (George et al. [2002\)](#page-10-0).

Vermifiltration has been described as a viable alternative to treated domestic wastewater in small clusters with good applicability in developing countries and in remote locations. Is a bio-oxidative process in which earthworms interact intensively with microorganisms within the decomposer community, increasing the stabilization of organic matter and greatly modifying its physical and biochemical properties (Liu et al. [2012\)](#page-10-0), combining filtration processes with vermicomposting techniques. Applications include small pilot-scale tests, households and

FUTURAMB[®] and Faculty of Sciences and Technology, University of Algarve, Faro, Portugal

small WWTP, opening new opportunities for treating domestic, urban wastewater and industrial wastewater due to the low cost and sustainable nature (Sinha et al. [2008\)](#page-11-0).

Earthworm species and filter media types are crucial influencing factors for the removal efficiency of vermifiltration because they are considered as the main biological components of the process and can change directly or indirectly the main removal processes of contaminants over time (Sinha [2010\)](#page-10-0).

The design parameters of vermifilters (VFs) include stocking density of earthworms (Sinha et al. [2008](#page-11-0)), filter media composition (Cardoso-Vigueros et al. [2013](#page-10-0)), hydraulic loading rate (HLR) (Kumar et al. [2015](#page-10-0)) and hydraulic retention time (HRT) (Arora et al. [2014a,](#page-10-0) [2016](#page-10-0)). Studies have been made with earthworm densities of 10 g L^{-1} (Arora et al. [2014b](#page-10-0)), 30 g L^{-1} (Arora et al. [2016](#page-10-0)) and intermediate values of 22.0 to 24.5 g L^{-1} (Tomar and Suthar [2011\)](#page-11-0) (Table 1). Typical HRT varies between 6 and 9 h and HLR between 2.0 and 3.0 m^3 m^{-2} day (Xing et al. [2005\)](#page-11-0).

Vermifilter packing material is an important design parameter for maximizing the treatment efficiency Arora et al. [\(2014b\)](#page-10-0). Filter medium materials should facilitate natural aeration (Cardoso-Vigueros et al. [2013\)](#page-10-0) and also serve as a dwelling habitat for earthworms to thrive and perform their function proficiently. Common filter packing materials include vermicompost (Arora et al. [2014b](#page-10-0), [2016](#page-10-0)), wood chips, bark, peat, straw (Li et al. [2008\)](#page-10-0) and sawdust (Lourenço and Nunes [2017\)](#page-10-0) for organic packing, and gravel, quartz sand (Lourenco and Nunes [2017](#page-10-0)), river bed gravel, mud balls, glass balls (Kumar et al. [2015](#page-10-0)), ceramsite (Xing et al. [2010\)](#page-11-0) and coal for inert packing (Wang et al. [2010](#page-11-0)). Filter packings specific surface area and porosity of filter packing materials have also been reported to impact treatment performance (Toffey [2008\)](#page-11-0). Besides, specific surface area and porosity of filter packing can affect the treatment performance of VF (Kumar et al. [2015](#page-10-0)).

In recent years, several studies regarding the removal of organic matter, nutrients and pathogens from domestic and urban wastewater using vermifiltration have been published. However, few have focused on the impact of different filter packings on vermifiltration performance.

The present study focuses on the evaluation of the performance of vermifiltration for the treatment of urban wastewater, studying sawdust and vermicompost as filter packing materials, considering a practical case study.

Materials and methods

Raw wastewater

The wastewater used in the study came from the urban WWTP of Messines, Algarve, with a served population of 6000 inhabitants which receives wastewater from a combined sewage collection system designed to transport both rain water and sewage together. All samples were collected

Table 1 Reported wastewater type, origin and operational parameters

Parameter	Sinha et al. (2008)	Cardoso-Vigueros et al. (2013)	Arora et al. (2014b)	Arora et al. (2016)	Kumar et al. (2015)	Tomar and Suthar (2011)
Wastewater type	Municipal wastewater	Domestic wastewater	Synthetic wastewater	Synthetic wastewater	Synthetic wastewater	Urban wastewater
Wastewater origin	WWTP	Toilets	Locally produced	Locally produced	Locally produced	Wastewater stream
Filter packing material	Garden soil, gravel	Domestic organic wastes, vermicompost, volcanic stones, gravel	Vermicompost, sand and gravel	Vermicompost, riverbed gravel, gravel	Vermicompost, riverbed gravel	Stones, sawdust, dried leaves, soil mixed with stones and pebbles
Earthworms species	Mix of Eisenia fetida, P. <i>excavatus</i> and Eudrillus euginae	Eisenia spp.	Eisenia fetida	Eisenia fetida	Eisenia fetida	Perionyx sansibaricus
Stock density of earthworms $(g L^{-1})$	10	10	18	30	16.5	$22 - 24.5$
HRT(h)	$1 - 2$	0.18		6		
HLR (m^3) m^{-2} day)			1.3	1.0	2.5	

on May 13 after the preliminary wastewater treatment. Wastewater used in the study was the same wastewater used in all experiments. No rain was registered during the days before wastewater collection. Wastewater physical– chemical and microbiological characterization is shown in Table 2.

Reactor structure

Reactor modules were constructed in PVC containers with a total volume of 25 L (Fig. [1](#page-3-0)) closely following the treatment scheme used in previous studies (Taylor et al. [2003\)](#page-11-0). Experiments were made using vermicompost produced from municipal organic solid waste as the filtering material provided by a specialized company $(FUTURAMB^@)$. Vermicompost occupied the top 16.0 cm, underneath which was installed an inert filter constituted of 7.0 cm of gravel and 6.0 cm of quartz sand. Percolating water was collected in an equalizer located below the filtering materials. Experiments were made using vermicompost produced from municipal organic solid waste as the packing material, and sawdust produced in a local woodshop which was easily available and could be utilized without any prior treatment. Reactors were covered with a lid, leaving sufficient room and opening as to allow natural aeration. An irrigation system was attached on top of the vermifilter made from 0.5-cm-diameter regular network of HDPE flexible plastic pipes. Pipes were perforated with 0.2-cm-diameter holes separated by 2.0 cm, for wastewater irrigation, and were kept 3 cm above the filter surface to ensure optimal wastewater distribution, the creation of drop overflow, and thereby increase aerobic conditions. Gravel was separated from the equalizer by a stainless steel mesh (diameter $= 0.4$ cm). Quartz sand was separated from gravel and from vermicompost or sawdust

Table 2 Characterization of the vermicompost and sawdust filter media (mean concentration \pm standard deviation)

Parameter	Vermicompost	Sawdust
Bulk density (kg m ^{-3})	600 ± 0.00	238.66 ± 0.00
Porosity $(\%)$	73.7 ± 0.30	84.0 ± 0.00
Particle size (mm)	$< 0.1 - 3.0$	$< 0.1 - 6.0$
pH(H ₂ O)	6.82 ± 0.01	5.38 ± 0.06
EC (μ S cm ⁻¹)	2530 ± 2.00	99.0 ± 1.20
Organic matter $(\%)$	56.48 ± 0.01	77.4 ± 0.05
TOC $(\%)$	32.76 ± 0.04	45.0 ± 0.05
$TN(\%)$	3.64 ± 0.02	0.50 ± 0.05
C/N ratio	9.0 ± 0.03	90.0 ± 0.00
$TP (mg kg^{-1})$	3769 ± 0.4	< 0.05
TK (mg kg^{-1})	7150 ± 0.08	0.11 ± 0.01

by a stainless steel mesh (diameter $= 80$ um). Physical– chemical characterization of vermicompost and sawdust is shown in Table 2. Parameters were determined by a commercial laboratory. The effluent from each VF was collected in the equalizer from where samples were taken. From here, recirculation was made with the help of a pump (Q_r) and mixed with raw wastewater as (Q_w) to be feed to the top of the filters $(Q_w + Q_r)$.

Process acclimation

Moisture content was held constant after placing the reactors to field capacity following procedures used by the company that provided the earthworms and the filter packing for acclimation of the earthworms. For this purpose, filters were flushed with recirculating water for 30 days. After this time, VF was flushed and recirculated permanently for 45 days with wastewater collected from urban WWTP of Messines, Algarve, to allow the growth of heterotrophic microorganisms in the filter packing. Each filter was fed, by pumping raw wastewater from a PVC container. The flow was also adjusted to permit the optimum moisture conditions for the survival of the earthworms.

Experimental design and operational conditions

After filter acclimation, four treatments were tested for packing material, identified as filter using vermicompost without earthworms (V), filter using vermicompost with the addition of earthworms (VE), filter using sawdust without earthworms (S), and filter using sawdust with the addiction of earthworms (SE). Influent wastewater flow, Q_w , and recycling flow, Q_r , were adjusted to obtain a constant Q_{mix} equal to 0.04 m³ day⁻¹, as this was the optimal flow for maintaining the ideal moisture of the filter. Hydraulic retention time (HRT) was fixed at 6 h following previous experiments not shown here. Experiments were made for a period of 24 h with permanent continuous wastewater recirculation. Samples for chemical analysis were taken at the onset of the experiment from the influent wastewater and at the end of the treatment period from the treated effluent. Organic loading rate (OLR) was measured as g BOD₅ day⁻¹. Recirculation ratio was related to Q_r and Q_w and was fixed at 0.72. These parameters were determined using the following equations.

$$
HRT = V/Q_w \tag{1}
$$

 $OLR = Q_w \times BOD_5$ (2)

$$
HLR = Q_w/A \tag{3}
$$

Recirculation ratio = $Q_{\rm r}/Q_{\rm w}$ (4)

Fig. 1 Reactor unit design

where V (m³) is the volume of the reactor, Q_w (m³ day⁻¹) is the influent wastewater flow rate, BOD_5 (mg L^{-1}) is the organic matter concentration in influent wastewater, HLR is the hydraulic loading rate $(m^3 m^{-2} day^{-1})$, Q_{mix} $(m^3 \text{ day}^{-1})$ is the sum of Q_w and recirculating flow, Q_r (Table 3), and A (m²) is the reactor's surface area.

Eisenia fetida (Bouché [1972\)](#page-10-0) is one of the most commonly used species for soil pollution and vermifiltration research (Taylor et al. [2003](#page-11-0)). It has been shown to process organic solid wastes with high efficiency, be very proficuous, and can adapt to various environmental factors, including temperature and moisture levels (Edwards and Arancon [2004\)](#page-10-0). The earthworms were provided by a company specialized in vermicomposting $(FUTURAMB^{\circledast})$ and previously installed on plastic boxes with coffee grounds at adequate moisture content for 15 days. No signs of disease and stress in the individuals were found. A stocking density of 20 g L^{-1} was used, following previous unpublished studies made at FUTURAMB[®]. The individuals were placed on the top of the organic filter material and were allowed to install for an acclimation period of 15 days.

During experiments, wastewater was applied continuously for 24 h. All filters were frequently monitored for foul odors, smooth percolation of wastewater through the vermicompost, and clogging. General earthworm behavior, including agility, movement, stress and health conditions, was also monitored. After this period, 200 cm^3 of treated wastewater samples was collected from the equalizer and kept in the cold $(4 \degree C)$ until analysis.

Sampling and chemical and microbiological analysis

For each treatment, samples were obtained at the beginning and at the end of the treatment. Samples of raw wastewater were taken from the feeding tank, and samples of treated wastewater were taken from the equalizers (Fig. 1). All samples were analyzed immediately after sampling for pH, EC, five-day biochemical oxygen demand $(BOD₅)$, chemical oxygen demand (COD), total suspended solids (TSS), NH_4^+ , NO_2^- , NO_3^- , total nitrogen (TN), PO_4^{3-} , total phosphorus (TP), fecal coliforms (FC) and helminth eggs. For the analysis, 5 L on each treatment was collected from the equalizer and three replicates were made for each parameter.

pH and EC were analyzed using a HANNA HI98129 meter with a precision and range ± 0.01 and 0.00–14.00 for pH, $\pm 2\%$ and 0.0–3999 to μ S cm⁻¹ for

Table 3 Hydraulic parameters used in the experiments

Q_{mix} (m ³ day ⁻¹)	$Q_{\rm r}$ (m ³ day ⁻¹)	μ day ⁻¹⁵ $Q_{\rm w}$ (m ³)	$Q_{\rm r}/Q_{\rm mix}$	HRT(h)	HLR $(m^{3} m^{-2} day^{-1})$	OLR (g BOD_5 day ⁻¹)
0.13	0.09	0.04			0.89	7.00 5د. ا

EC and the later converted automatically by the equipment do total dissolved solids (TDS) in the range 0–2000 mg L^{-1} . This later parameter was obtained from EC by a conversion factor of 0.5 . BOD₅ was analyzed using an $OxiTop^{\otimes}-C$ respirometric system with incubation at constant temperature for 5 days (APHA [1998\)](#page-10-0) with a precision, and range of $\pm 1\%$. tCOD was analyzed with a photometer (NOVA 60, Merck) with a precision and range of ± 5.0 mg L⁻¹ and 25-1500 mg L⁻¹ based on the permanganate method (APHA [1998](#page-10-0)). Dissolved fractions were determined after filtrating through a Whatman[®] 40-um cellulose filter paper as dissolved COD (sCOD). Particulate COD fraction, pCOD, was obtained as the difference between total, tCOD, and soluble, sCOD. TSS was determined by filtrating the sample through a Whatman[®] 40 -µm cellulose filter paper, drying to a constant weight at 105° C, and weighting (APHA [1998\)](#page-10-0). NH₄⁺ was quantified by photometry using a HANNA HI733 m with a precision and range of ± 1.0 mg L⁻¹ and 0.0-99.9 mg L⁻¹, respectively. NO_2 ⁻ was analyzed with a HANNA HI708 photometer based on the ferrous sulfate method with a precision and amplitude range of ± 3.0 mg L⁻¹ and 0–150 mg L^{-1} , and NO_3 ⁻ was analyzed with a HANNA HI96786 photometer based on the cadmium reduction method with a precision and range of ± 5.0 mg L⁻¹ and 0–100 mg L^{-1} . TN analysis was performed through oxidative digestion of all nitrogenous compounds to nitrate based on the persulfate method using (APHA [1998](#page-10-0)). PO_4^{3-} analysis was made using a HANNA HI717 photometer based on the heteropolymolybdenum blue method with a precision and range of ± 1.0 mg L⁻¹ and 0–30 mg L^{-1} . TP was obtained by oxidative digestion of organic matter followed by a colorimetric reaction based on the ascorbic acid method (APHA [1998\)](#page-10-0). FC were analyzed based on membrane filtration, subsequent culture on a chromogenic coliform agar medium with determination by the most probably number (MPN) per 100 mL^{-1} , and Ascaris lumbricoides were analyzed as the number of target organisms in the sample (Number 100 mL⁻¹) (APHA [1998\)](#page-10-0). FC removal efficiency (K_{FC}) was calculated using Eq. (5) as proposed by Arora et al. [\(2014a](#page-10-0)), where C_i and C_f are the wastewater FC initial and final FC, respectively.

$$
K_{\rm FC} = \text{Log}_{10}(C_{\rm i}/C_{\rm f})\tag{5}
$$

Statistical analysis

One-way analysis of variance (ANOVA), followed by Tukey's test at a significance level of $\alpha = 0.05$, was made to check for differences between treatments. T test was also performed to compare means. The statistical package $SPSS^{\circledast}$ 17.0 was used in the analysis.

Results and discussion

Earthworms showed good survival in the filter using vermicompost (VE) and in the filter using sawdust (SE) during the whole experiment, as individuals accommodated to the experimental conditions with no evidence of decrease in population numbers. Individuals meandered throughout all the volume of the organic filter packing, while not trying to escape, meaning that wastewater was not toxic and the environment was suitable. In our study, during the first 15 h, wastewater percolated smoothly into all reactors, but some clogging was observed in the control filter using vermicompost without earthworms (V) after that period, as indicated by an abnormal accumulation of wastewater on the surface of the filter bed. No clogging was reported in the remaining filters during the whole experiment: vermicompost with earthworms (VE), control filter with sawdust without earthworms (S), and filter with sawdust and earthworms (SE).

The ratio $BOD₅/COD$ is one important way to assess the biodegradability of wastewater, as in a raw urban wastewater the BOD5/COD ratio varies between 0.3 and 0.8 (Tchobanoglous et al. 2003). Besides, with a BOD₅/COD ratio of 0.5, wastewater is considered to be easily treatable by biological processes (Tchobanoglous et al. [2003\)](#page-11-0). Also, the common BOD5/COD ratio in a treated wastewater varies between 0.1 and 0.3 (Henze and Comeau [2008](#page-10-0)). In a typical urban wastewater, $BOD₅$, COD and TSS have average concentrations of 350, 750 and 400 mg L^{-1} , respectively (Henze and Comeau [2008](#page-10-0)) (Table [4\)](#page-5-0). Comparing our results with the results from the literature (Table [4\)](#page-5-0), BOD_5 $(210 \pm 10.0 \text{ mg L}^{-1})$, COD $(450 \pm 10.0 \text{ mg L}^{-1})$ and TSS (158 \pm 3.46 mg L⁻¹) were all lower than published ones. This could be justified by solids sedimentation in the PVC container during the study. The BOD₅/COD ratio found for the wastewater was 0.47 indicating good biodegradability (Tchobanoglous et al. [2003\)](#page-11-0).

The content of the individual nutrients in wastewater should correspond to the bacteria needs, and there should be a balanced relationship between carbon, nitrogen and phosphorus, as this is crucial to the effectiveness of the biodegradation processes. The concentration of NH_4^+ $(46.4 \pm 0.26 \text{ mg L}^{-1})$ obtained was similar to values referred by Henze and Comeau [\(2008](#page-10-0)) of 45 mg L^{-1} , supporting the argument that it could be mainly from domestic sources as urine or cleaning agents. Nearly 75% of the TN in a typical urban wastewater is NH_4^+ and the majority (70–90%) comes from urine, while the final 20% comes from cleaning agents, disinfectants and food wastes (Hughes et al. [2008\)](#page-10-0). Fecal coliforms concentration $(5.7 \times 10^8 \pm 3.98 \times 10^1 \text{ MPN } 100 \text{ mL}^{-1}$, Table [4\)](#page-5-0) was relatively high if compared with the literature (George et al. [2002\)](#page-10-0).

Parameter	Value ^a	Typical values			
		Henze and Comeau (2008)	USEPA (2004)	Tchobanoglous et al. $(2003)^*$	
pH	8.48 ± 0.03	n.a.	n.a.	n.a.	
BOD_5 (mg L^{-1})	210 ± 10.0	350	221	300	
COD (mg L^{-1})	450 ± 10.0	750	580	650	
TDS (mg L^{-1})	532 ± 5.00	n.a.	n.a.	n.a.	
Turbidity (NTU)	148.3 ± 7.51	n.a.	n.a.	n.a.	
TSS $(mg L^{-1})$	158 ± 3.46	400	243	500	
NH_4^+ -N (mg L^{-1})	49.4 ± 0.31	45	9	n.a.	
NO_2 ⁻ -N (mg L ⁻¹)	2.0 ± 0.75	0.2	$\Sigma < 1$	n.a.	
NO_3 ⁻ -N (mg L ⁻¹) ^{**}	0.2 ± 0.12			n.a.	
TN (mg L^{-1})	68.3 ± 0.31	60	51	70	
$PO_4^{3-}P$ (mg L ⁻¹)	16.3 ± 0.75	10	n.a.	n.a.	
TP (mg L^{-1})	5.7 ± 0.12	15	9	15	
BOD ₅ /tCOD	0.47 ± 0.03	0.47	0.38	0.44	
COD/NH_4^+ -N	9.1 ± 0.23	16.7	64.4	17.2	
FC (MPN 100 mL ⁻¹)	$5.7 \times 10^8 \pm 3.98 \times 10^1$	1.0×10^{12} **	1.0×10^{7}	2.2×10^{6}	
Helminth eggs (No. L^{-1})***	8.00 ± 6.24	13	n.a.	n.a.	

Table 4 Characterization of influent wastewater and typical values from literature data

n.a. Not available

* Average concentration

** Converted by mass equation

*** As total coliforms

**** As Ascaris lumbricoides eggs

^a Mean concentration \pm standard deviation

Treatments showed a good efficiency for removing BOD5, COD and TSS from wastewater (Tukey's test, $p < 0.05$ $p < 0.05$, Table 5). BOD₅, COD and TSS values in all treatments met the EU standards (Directive 91/271/EEC, May 21, 1991) for wastewater discharge, namely of 25 mg L^{-1} , or a minimum removal of 70–90% for BOD₅, 125 mg L^{-1} or a minimum removal of 75% for COD and 35 mg L^{-1} or a minimum removal of 90% for TSS. Removal efficiencies for BOD₅ were $91.27 \pm 0.55\%$ in VE, 96.19± 0.00% in V, 90.48% in SE and 92.06% in S as removal efficiencies for COD were $87.56 \pm 0.45\%$ in VE, $86.67 \pm 0.89\%$ in V, $79.70 \pm 0.92\%$ in SE and $77.63 \pm 1.80\%$ in S. As for TSS, removal efficiencies were $98.42 \pm 0.00 \pm 0.55\%$ $98.42 \pm 0.00 \pm 0.55\%$ $98.42 \pm 0.00 \pm 0.55\%$ in VE, V, SE and S (Table 5). Dissolution of earthworm castings may have contributed to increase BOD₅ values in VE and SE (18.33 \pm 1.15 mg L^{-1} and 8.00 \pm 0.00 mg L^{-1}) compared to V and S (20.0 \pm 1.00 mg L⁻¹ and 16.67 \pm 1.15 mg L⁻¹). Vermifiltration contributed to higher COD removal in treated wastewater $(56.0 \pm 2.0 \text{ mg L}^{-1} \text{ in VE and } 91.33 \pm 1)$ 4.2 mg L^{-1} in SE, Table [5](#page-6-0)). COD removal efficiency was lower compared to BOD_5 (91.27% in VE and 90.48% in SE for BOD_5 and 87.56% in VE and 79.70% in SE for COD, Table [5](#page-6-0)), due to the fact that earthworms are mainly responsible for the removal of biodegradable substances. In comparison, Sinha et al. ([2008\)](#page-11-0) reported removal of TSS in the ranges of 90–92 and 90–95%, for COD and BOD₅, respectively. Xing et al. [\(2010](#page-11-0)) reported that the presence of earthworms was responsible for about 57–79% reduction in TSS in wastewater, which was lower than the values obtained here. The vermifilter system with sawdust was less efficient in reducing turbidity from wastewater (2.28 NTU \pm 0.08 in SE and 1.17 NTU \pm 0.14 in S), and earthworms in fact contributed to increase turbidity (3.94 NTU \pm 0.16 in VE and 2.28 NTU \pm 0.08 in SE) comparing to the systems without earthworms (V and S) $(Table 6)$ $(Table 6)$.

Earthworms significantly degrade the wastewater organics by enzymatic action in their gut, helping in the degradation of several compounds which could not be decomposed by microorganisms (Sinha [2010](#page-10-0); Malek et al. [2012](#page-10-0)). This may explain the higher COD efficiencies obtained in VE and SE, where microbial stimulation, biodegradation and enzymatic degradation of solid wastes by earthworms work simultaneously (Sinha [2010](#page-10-0)). In fact, vermifiltration is effective due to the biological, physical and chemical reactions, including the adsorption of molecules and ions, oxidation–reduction in organic matter, and

Table 5 Parameters and efficiencies¹ for the different treatments

Parameters and efficiencies¹ for the different treatments

the synergetic effects of earthworms with microorganisms (Bouché and Soto [2004\)](#page-10-0).

The higher removal $BOD₅$ and COD efficiencies in VE compared to SE may be related to the higher C/N content in sawdust compared to that of vermicompost $(45.0 \pm 0.05\%$ to $32.76 \pm 0.04\%$, Table [2\)](#page-2-0) since more carbon content (as carbonaceous $BOD₅$) from sawdust may have been released to the wastewater. Specific surface area and porosity of filter packing are one of the factors that affect the treatment performance of biological filtration (Toffey [2008\)](#page-11-0). A filter packing with low granulometry improves biomass accumulation and attains higher treatment efficiency as compared to the performance of media with low specific surface area (Taylor et al. [2003\)](#page-11-0). Since vermicompost has lower granulometry compared to sawdust (Table [2\)](#page-2-0), its higher specific surface may have created better conditions for microorganisms to survive and grow. This could justify the significantly higher $BOD₅$ removal efficiencies (Tukey's test, $p < 0.05$) in VE $(91.27 \pm 0.55\%)$ and V (96.19 \pm 0.00%). As organic solid particles are retained in the pores of the filter packing, high removal efficiencies for TSS are usually obtained (Sinha et al. [2008\)](#page-11-0). In our experiments, there was no significant difference in TSS removal efficiency in systems with or without the presence of earthworms (Tukey's test, $p > 0.05$), indicating that the removal process is essentially physical.

In our study, compared with raw wastewater $(46.4 \pm 0.26 \text{ mg L}^{-1})$, NH₄⁺ concentrations decreased in all experiments $(11.60 \pm 0.15 \text{ mg L}^{-1} \text{ in VE},$ 8.57 ± 0.32 mg L⁻¹ in V, 18.08 \pm 0.76 mg L⁻¹ in SE and 2.54 \pm 0.31 mg L⁻¹ in S, Table 5). Vermifiltration contributed to decrease NH_4^+ removal efficiency (Tukey's test, $p < 0.05$) (76.51 \pm 0.24% at VE and 63.40 \pm 1.19% at SE) as V had an efficiency of $82.64 \pm 0.50\%$ and S had an efficiency of $94.86 \pm 0.48\%$ (Table 5). NH₄⁺ is generated by organic nitrogen mineralization leading to ammonia emissions being the first inorganic nitrogen form produced during biological wastewater treatment (Henze and Comeau [2008\)](#page-10-0). Vermicasts increase nutrient content in soil (Edwards et al. [2011\)](#page-10-0) as N cycling is directly influenced by earthworms. In their studies, Kadam et al. ([2009\)](#page-10-0) concluded that NH_4^+ , as the dominant type of N in domestic wastewater, was removed through rapid adsorption by the filter packing and subsequently converted into $NO₃⁻$ through nitrification. The increase in NH₄⁺ on VE and SE compared with V and S may be due to the ion leachate from earthworm castings during treatment. Besides, vermicompost packing may have contributed to increase NH_4^+ due to the fact the vermicompost is mainly constituted by earthworm castings and is rich in heterotrophic bacteria which increase organic nitrogen mineralization (Sinha et al. [2008\)](#page-11-0). Also, the excess of ammonium

Table 6 BOD₅/COD and COD/ NH_4^+ -N, nutrient concentration¹, and pH, TDS and turbidity¹ for the different treatments

¹ Mean concentration \pm standard deviation. Values followed by the same letter within each line are not significantly different (ANOVA; Tukey's test, $\alpha = 0.05$)

in wastewater may contribute to earthworm' stress (Hughes et al. [2008\)](#page-10-0). The former authors reported ammonium concentration of 25 mg L^{-1} in treated effluent after vermifiltration and a LC50 of 1.49 mg L^{-1} and a 0% survival rate above 2.0 mg L^{-1} . The low toxicity of ammonium in our study may be attributed to the rapid conversion of ammonium to nitrate.

All treatments contributed to decrease $BOD₅/COD$ ratios (Tukey's test, $p < 0.05$), but in the presence of earthworms the $BOD₅/COD$ ratios were higher $(0.33 \pm 0.03$ and 0.22 ± 0.02 in VE and SE, and 0.13 ± 0.01 and 0.17 ± 0.02 in V and S, respectively (Table 6). This may be due to the release of dissolved organic compounds from the vermicastings. When comparing the two filter materials, no significant difference was found in BOD₅/COD ratio (Tukey's test, $p > 0.05$). Degradation of organic fractions of wastewater produces some acidic species of mineralized organic materials $(CO₂)$, NH_4^+ , NO_3^- and organic acids) which play an important role in shifting of pH of treated water. This may justify the decrease in pH in all treatments. Besides, vermifiltration contributed to decrease pH from raw wastewater $(7.85 \pm 0.04$ at VE and 8.22 ± 0.00 at SE, Table 6). Edwards et al. (2011) (2011) and Arora et al. $(2014b)$ $(2014b)$ have reported the influence of earthworms in making pH converge to neutrality in soil, solid organic wastes treatment and vermifiltration. Hughes et al. ([2008\)](#page-10-0) have also found that vermicompost as filter packing has high buffering capacity for pH.

Carbon-to-nitrogen ratio in raw wastewater plays an important role in wastewater treatment and is measured by the COD/NH₄⁺-N ratio change (Cardoso-Vigueros et al. [2013\)](#page-10-0). Vermifiltration had a significant influence in COD/ NH_4^+ -N ratio (Tukey's test, $p < 0.05$). For TN removal, rates by nitrification may be improved when carbon-tonitrogen ratios in wastewater are in between 5:1 and 10:1 (Roy et al. [2010](#page-10-0)). The filter with vermicompost and

earthworms showed the highest nitrification (Tukey's test, $p < 0.05$), as the lowest COD/NH₄⁺-N, 4.8 ± 0.22 mg L^{-1} , was obtained in VE (Table 6). Nitrification coupled with denitrification seems to be the major N removal process involved in many vermifiltration systems, while insufficient available organic C (as COD) is considered to be responsible for the inhibition of denitrification (Sinha et al. 2008). NO_2^- is an intermediate product of nitrification, and its concentration in wastewater is usually negligible (Henze and Comeau [2008](#page-10-0)). Comparing vermicompost and sawdust, the first contributed do increase $NO_2^ (3.2 \pm 0.68 \text{ mg L}^{-1})$ in VE and 3.5 ± 0.92 mg L⁻¹ in V) and also to increase NO₂⁻ relatively to raw wastewater (0.2 \pm 0.12 mg L⁻¹). No statistically significant difference was obtained between treatments and NO_2 ⁻ concentration (Tukey's test, $p > 0.05$, Table 6). In nitrification, the adsorbed NH₄⁺ is subsequently converted to $NO₃⁻$, carried out by autotrophic bacteria using molecular oxygen as an electron acceptor (Zhang et al. [2005\)](#page-11-0). Nitrification step for NH_4^+ removal led to a substantial increase in NO_3^- in VE and V as no NO_3 ⁻ was found in SE and S (Table 6). NO_3 ⁻ concentration increased in the treatment using vermicompost with VE registering 4.9 \pm 0.29 mg L⁻¹ and V registering 1.5 ± 0.21 mg L⁻¹ (Table 6), in comparison with raw wastewater $(0.2 \pm 0.12 \text{ mg L}^{-1})$ (Table [4\)](#page-5-0). The presence of earthworms contributed to increase $NO₃⁻$ from 0.2 ± 0.12 mg L⁻¹ in raw wastewater to 4.9 ± 0.29 mg L⁻¹ in VE and 1.5 \pm 0.21 in SE (p < 0.05, Table 6). Vermicompost is rich in nitrifying bacteria which help effluent mineralization (Sinha et al. [2008](#page-11-0)). This aspect is also supported by Cardoso-Vigueros et al. [\(2013](#page-10-0)) who found a positive correlation between earthworm density and nitrifying bacteria, helped by abundant oxygen due to the burrowing action of earthworms. At the same time, earthworms excrete polysaccharides, proteins and other nitrogenous compounds as they mineralize nitrogen in wastewater (Sinha [2010\)](#page-10-0). The highest rates of mineralization occur in the vermicasts, which greatly enhances the availability of inorganic nutrients.

The presence of earthworms contributed to decrease TN removal efficiency (Tukey's test, $p < 0.05$) $(12.40 \pm 4.40\%$ at VE and 86.34 \pm 0.84% at SE) as V had an efficiency of $67.80 \pm 0.00\%$ and S had an efficiency of $97.07 \pm 0.00\%$ (Table [5](#page-6-0)). Also, when comparing both filter packings, vermicompost (VE and V) contributed to reduce TN removal efficiency (Tukey's test, $p < 0.05$, Table [5](#page-6-0)).

In the present study, $PO₄^{3–}$ concentrations decreased in all treatments relatively to raw wastewater (Tukey's test, $p\lt 0.05$), while no statistically significant difference was obtained for PO_4^{3-} between VE and V (Tukey's test, $p > 0.05$, Table [6\)](#page-7-0). The presence of earthworms did not help to improve TP removal as no statistically significant difference was obtained between treatments and TP (Tukey's test, $p > 0.05$, Table [5\)](#page-6-0). Vermicompost contributed to increase TP concentration compared to raw wastewater $(11.7 \pm 0.58 \text{ mg L}^{-1})$ in VE and 11.7 ± 0.58 mg L⁻¹ in V) (Table [5\)](#page-6-0). On the contrary, sawdust contributed to reduce TP from raw wastewater with 0.6 \pm 0.00 mg L⁻¹ in SE and 0.065 \pm 0.00 mg L⁻¹ in S (Table [5\)](#page-6-0). Due to this, TP removal efficiencies in treatments using vermicompost were negative $(-105.88 \pm 10.18\%$ at VE and $-105.88 \pm 10.18\%$ at V) (Table [5](#page-6-0)). TP removal in SE and S suggests that sawdust may have contributed to remove organic and $PO₄³⁻$ from wastewater due to absorption of inorganic constituents by different biological or non-biological components. Moreover, in the filters with sawdust it was possible to observe a statistically significant difference between SE and S (Tukey's test, $p < 0.05$, Table [6](#page-7-0)) with SE ending with higher PO_4^{3-} concentration $(1.3 \pm 0.01 \text{ mg L}^{-1})$ than S $(0.03 \pm 0.06 \text{ mg } L^{-1})$. PO₄³⁻ increase during vermifiltration is due to enzymatic and microbial activity due to the presence of earthworms (Hait and Tare [2011](#page-10-0)). Increase in TP concentration during vermifiltration has been reported by other authors (Cardoso-Vigueros et al. [2013;](#page-10-0) Arora et al. [2016;](#page-10-0) Kumar et al. [2015\)](#page-10-0). The vermicastings can increase the levels of nutrients in vermifilter effluents more significantly, as indicated above, which can explain the negative removal efficiencies obtained for TP in our study.

According to EU standards, VE and V exceeded total nitrogen and total phosphorus emission limits of 15.0 and 2.0 mg L^{-1} , respectively. According to this regulation, these two parameters are especially important in sensitive water bodies and fundamental nutrients responsible for eutrophication processes. Nutrient increase is also supported by the fact that earthworms contributed to increase ion concentration in treated effluent since TDS was 476 ± 5.31 mg L⁻¹ in VF and 423 ± 5.31 mg L⁻¹ in SE,

compared with 418 ± 2.89 mg L⁻¹ in V and 363 ± 1.00 mg L⁻¹ in S. This is also supported by the fact that pH followed the mineralization process and oxidation of organic compounds as expected (Table [6\)](#page-7-0).

Removal of pathogens is one of the main objectives when treating wastewater for discharge in water bodies or reuse for irrigation. Fecal coliforms typical concentration in raw wastewater is usually between 10^6 and 10^8 MPN 100 mL^{-1} depending on both raw wastewater composition and treatment efficiency (George et al. [2002\)](#page-10-0). Ascaris lumbricoides eggs are a good indicator of parasitological quality as 99.9% of removal must be achieved (WHO [2006](#page-11-0)). All *fecal* coliforms (concentration, Log_{10} FC, K_{FC} and k_{FC}) and helminth eggs parameters during the study are given in Table [7.](#page-9-0) $Log₁₀ FC$ values were all between the values reported by WHO [\(2006](#page-11-0)) with 4.70 ± 0.01 in VE, 4.78 \pm 0.03 in V, 4.72 \pm 0.02 in SE and 3.26 \pm 0.24 in S. No statistically significant difference was obtained for $Log₁₀$ FC value between VE and V treatments (Tukey's test, $p > 0.05$). In filter with sawdust, vermifiltration did not contribute to decrease $Log₁₀ FC value$ (Tukey's test, $p > 0.05$). No statistically significant difference was obtained for K_{FC} and k_{FC} values between treatments (Tukey's test, $p > 0.05$). Ascaris lumbricoides eggs were all removed of 100% in all experiments (Table [7](#page-9-0)). Based on fecal coliforms concentration in raw wastewater and the maximum concentration permitted by WHO ([2006\)](#page-11-0) of 6–7 $Log₁₀$ units for unrestricted irrigation, it is possible to predict that the minimal K_{FC} and k_{FC} values in the final effluent obtained from vermifiltration should be 5.91 and 11.70, respectively.

Working with vermifiltration, Arora et al. [\(2014a,](#page-10-0) [b\)](#page-10-0) studied the removal of E. coli from urban wastewater having obtained a reduction from a mean $Log₁₀$ value of 4.48 MPN 100 mL⁻¹ to 2.80 MPN 100 mL⁻¹. Using vermicompost as filter packing, Arora et al. ([2016\)](#page-10-0) obtained an effluent wastewater with a mean $Log₁₀$ value of 2.50 MPN 100 mL^{-1} starting from an influent wastewater of 5.48 MPN 100 mL^{-1} . In their studies, Kumar et al. [\(2015](#page-10-0)), using as filter packing, vermicompost and river bed material, vermicompost and wood coal, vermicompost and glass balls, and vermicompost and mud balls, reported a reduction in fecal coliforms of 3.4 ± 0.67 , 2.9 ± 0.88 , 2.6 ± 0.45 and 2.6 ± 1.05 Log₁₀ MPN 100 mL^{-1} .

Guidelines for wastewater reuse in irrigation indicate a pH between 6.0 and 9.0, a $BOD₅$ concentration \leq 10 mg L⁻¹ (for food crops consumed uncooked) or \leq 30 mg L⁻¹ (for non-food crops and food crops consumed after processing), a TSS concentration between \leq 30 mg L⁻¹ (for processed food crops) and, for fecal coliforms and helminth eggs, a maximal MPN of 10^3 100 mL⁻¹ (or 3.0 Log₁₀) and 1 unit L⁻¹, for

Table / Tecal complime in acalca wastewatch						
Parameter	VE	V	SE	S		
FC		$5.07 \times 10^{4b} \pm 1.53 \times 10^{3}$ $6.03 \times 10^{4c} \pm 4.04 \times 10^{3}$ $5.3 \times 10^{4b} \pm 3.00 \times 10^{3}$ $2.0 \times 10^{3a} \pm 1.00 \times 10^{3}$				
Log ₁₀ FC value	$4.70^{\rm b} \pm 0.01$	$4.78^{\rm b} \pm 0.03$	$4.72^b \pm 0.02$	$3.26^a \pm 0.24$		
K_{FC}	$3.693^a \pm 0.01$	$3.618^a \pm 0.03$	$3.674^{\rm a} \pm 0.03$	$5.139^b \pm 0.24$		
$k_{\rm FC}$	$7.484^a \pm 0.03$	$7.320^a \pm 0.06$	$7.445^{\rm a} \pm 0.05$	$10.412^b \pm 0.49$		
Helminth eggs removal efficiency η (%)	$100.00^a \pm 0.00$	$100.00^a \pm 0.00$	$100.00^a \pm 0.00$	$100.00^a \pm 0.00$		

Table 7 Fecal coliforms¹ in treated wastewater

Mean concentration \pm standard deviation. Values followed by the same letter within each line are not significantly different (ANOVA; Tukey's test, $\alpha = 0.05$)

agricultural irrigation (USEPA [2004](#page-11-0)). For pathogens only, WHO ([2006\)](#page-11-0) indicates a maximum MPN of 10^3 100 mL⁻¹ (for unrestricted use), a maximum MPN of 10^4 100 mL⁻¹ for restricted use and ≤ 1 No. L⁻¹ for helminth eggs. In all experiments, pH and TSS comply with these limits. As for BOD5, all treatments attained the limit concentration for non-food crops and crops consumed after processing $(\leq 30 \text{ mg } L^{-1})$, but only vermicompost without earthworms attained the limit concentration for food crops consumed uncooked $(\leq 10 \text{ mg } L^{-1})$ (Table [6](#page-7-0)). Also, none of the experiments reduced fecal coliforms to less than $10³$ MPN 100 mL⁻¹ or a Log₁₀ value less than 3.0 (Table 7). All treatments removed helminth eggs with an efficiency of 100%. This could be related due to the destruction of the three layers of protective shells that constituted helminth eggs. Nevertheless, all values related to fecal coliforms and helminth eggs were in accordance with the proposed by WHO ([2006\)](#page-11-0) for primary and secondary wastewater treatment technologies.

The results using single-stage vermifiltration were not completely positive since the efficiencies obtained for some of the parameters were still short to attain the EU regulation for discharges in sensitive water bodies (TN and TP) and USEPA and WHO guidelines for irrigation (fecal coliforms). The removal efficiencies were nonetheless higher than those registered in similar conditions as, e.g., in Arora et al. (2016) (2016) , with 85.5% for BOD₅, 77.8% for COD and 82.2% for TSS. As for NH_4^+ , high removal efficiencies with VF may be only attainable with vertical stage VF since Yang et al. ([2015\)](#page-11-0) reported an increase in NH_4^+ removal with the depth of filter packing. Fecal coliform removal efficiencies here obtained do not meet guidelines as a maximal MPN of 10^3 100 mL⁻¹ for irrigation through VF has shown to not attain such level of use.

Table 8 resumes the parameters removal efficiencies obtained in the literature. Comparing these data with the values obtained in our study, the best removal efficiency for $BOD₅$ (96.19% working with filter with vermicompost without earthworms) was just lower than efficiencies obtained by Sinha et al. [\(2008](#page-11-0)), 98%, and Cardoso-Vigueros et al. ([2013\)](#page-10-0) (99%). For COD, the best removal efficiency (87.56% working with filter with vermicompost and earthworms) was just lower than the obtained by Cardoso-Vigueros et al. [\(2013](#page-10-0)), 92%, and for TSS, in all treatments, removal efficiency (98.42%) was higher when compared with the literature. When analyzing the NH_4^+ removal, the value obtained in filter with vermicompost and earthworms, 76.51%, was lower than the efficiencies obtained by Cardoso-Vigueros et al. [\(2013](#page-10-0))—98%, and Arora et al. ([2016\)](#page-10-0)—90%. In what concerns TP, Cardoso-

Table 8 Treatment efficiencies obtained in the literature using VF

Parameter	Sinha et al. (2008)	Cardoso-Vigueros et al. (2013) Arora et al. (2016) Arora et al. $(2014a)$			Kumar et al. (2015)
BOD ₅	98%	99%	86%	76%	81%
COD	45%	92%	78%	67%	72%
TSS	90%	97%	82%	-	75%
NH_4 ⁺		98%	90%		76%
TN		78%			
TP		a	a	-	a
Fecal coliforms*			2.82	2.70	3.40

* As Log10 FC value

^a Authors reported an increase in TP final concentration

Vigueros et al. (2013), Arora et al. (2016) and Kumar et al. (2015) all registered increases in TP concentration in treated effluent, which is in line with our results. The latter two authors obtained in their studies treated effluent with less than a $Log₁₀$ of 3.0 of fecal coliforms, which clearly surpasses our results.

Conclusion

Vermicompost and sawdust showed high treatment efficiency for BOD5, COD and TSS. Moreover, the values using single-stage vermifiltration were not completely positive given that the efficiencies obtained for TP and TN were still above EU guideline values for discharge in sensitive water bodies, and fecal coliforms were above the WHO guideline value for irrigation.

Earthworms contributed to reduce treatment efficiencies for BOD₅, NH_4^+ and TN and to increase treatment efficiency for COD. In vermicompost, earthworms contributed to increase $NO₃⁻$. Comparing with raw wastewater, vermicompost contributed to increase TP. No treatment eliminated fecal coliforms down to guidelines values for wastewater irrigation, but helminth eggs were completely eliminated.

In order to attain EU guideline values for discharge in sensitive water bodies and WHO guideline values for irrigation, alternative treatment technologies are needed, namely sequential vermifiltration systems or vermifilters followed by wetlands, working as hybrid systems suited for small communities.

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References

- APHA (1998) Standard Methods for the examination of water and wastewater. American Public Health Association, American Water Works Association, Water Environmental Federation, twenty ed. Washington
- Arora S, Rajpal A, Kumar T, Bhargava R, Kazmi AA (2014a) A comparative study for pathogen removal using different filter media during vermifiltration. Water Sci Technol 70:996–1003. doi[:10.2166/wst.2014.318](http://dx.doi.org/10.2166/wst.2014.318)
- Arora S, Rajpal A, Kumar T, Bhargava R, Kazmi AA (2014b) Pathogen removal during wastewater treatment by vermifiltration. Environ Technol 35:2493–2499. doi[:10.1080/09593330.](http://dx.doi.org/10.1080/09593330.2014.911358) [2014.911358](http://dx.doi.org/10.1080/09593330.2014.911358)
- Arora S, Rajpal A, Kazmi AA (2016) Antimicrobial activity of bacterial community for removal of pathogens during vermifiltration. J Environ Eng. doi:[10.1061/\(ASCE\)EE.1943-7870.](http://dx.doi.org/10.1061/(ASCE)EE.1943-7870.0001080) [0001080](http://dx.doi.org/10.1061/(ASCE)EE.1943-7870.0001080)
- Bouché MB (1972) Lombriciens de France, Ecologie et systématique, 1st edn. INRA, Paris
- Bouché MB, Soto P (2004) An industrial use of soil animals for environment: the treatment of organically polluted water by lombrifiltration. In: Proceedings of the XIVth international colloquium on soil zoology and ecology. University of Rouen, Mont Saint Aignan, pp 1–13
- Cardoso-Vigueros L, Ramírez-Camperos E, Garzón-Zúñiga M (2013) Evaluation of a pilot vermifilter for the treatment of wastewater. Ing Agrı´c Biosist 5(2):33–44. doi:[10.5154/r.inagbi.2013.10.003](http://dx.doi.org/10.5154/r.inagbi.2013.10.003)
- Edwards CA, Arancon NQ (2004) The use of earthworms in the breakdown of organic wastes to produce vermicomposts and animal feed protein. In: Earthworm ecology. CRC Press, Boca Raton, pp 345–438
- Edwards CA, Arancon NQ, Sherman RL (2011) Vermiculture technology: earthworms, organic wastes, and environmental management, 1st edn. CRC Press, Boca Raton
- George I, Crop P, Servais P (2002) Fecal coliform removal in wastewater treatment plants studied by plate counts and enzymatic methods. Water Res 36:2607–2617. doi:[10.1016/S0043-](http://dx.doi.org/10.1016/S0043-1354(01)00475-4) [1354\(01\)00475-4](http://dx.doi.org/10.1016/S0043-1354(01)00475-4)
- Hait S, Tare V (2011) Vermistabilization of primary sewage sludge. Bioresour Technol 102:2812–2820. doi:[10.1016/j.biortech.2010.](http://dx.doi.org/10.1016/j.biortech.2010.10.031) [10.031](http://dx.doi.org/10.1016/j.biortech.2010.10.031)
- Henze M, Comeau Y (2008). Wastewater characterization. Biol Wastewater Treat Princ Model Des 33–52
- Hughes RJ, Nair J, Ho G (2008) The toxicity of ammonia/ammonium to the vermifiltration wastewater treatment process. Water Sci Technol 58:1215–1220. doi:[10.2166/wst.2008.478](http://dx.doi.org/10.2166/wst.2008.478)
- Kadam AM, Nemade PD, Oza GH, Shankar HS (2009) Treatment of municipal wastewater using laterite-based constructed soil filter. Ecol Eng 35:1051–1061. doi[:10.1016/j.ecoleng.2009.03.008](http://dx.doi.org/10.1016/j.ecoleng.2009.03.008)
- Prasad KSH, Kumar, T., 2012. Decentralized waste water treatment by vermifiltration using river bed material. In: 7th International conference on sustainable built environment, 14–16 December 2012, Kandi, Sri Lanka
- Kumar T, Bhargava R, Prasad KSH, Pruthi V (2015) Evaluation of vermifiltration process using natural ingredients for effective wastewater treatment. Ecol Eng 75:370–377. doi:[10.1016/j.](http://dx.doi.org/10.1016/j.ecoleng.2014.11.044) [ecoleng.2014.11.044](http://dx.doi.org/10.1016/j.ecoleng.2014.11.044)
- Li YS, Robin P, Cluzeau D, Bouche´ M, Qiu JP, Laplanche A, Hassouna M, Morand P, Dappelo C, Callarec J (2008) Vermifiltration as a stage in reuse of swine wastewater: monitoring methodology on an experimental farm. Ecol Eng 32:301–309. doi[:10.1016/j.ecoleng.2007.11.010](http://dx.doi.org/10.1016/j.ecoleng.2007.11.010)
- Li Y-S, Xiao Y-Q, Qiu J-P, Dai Y-Q, Robin P (2009) Continuous village sewage treatment by vermifiltration and activated sludge process. Water Sci Technol 60(11):3001
- Liu J, Lu Z, Yang J, Xing M, Yu F, Guo M (2012) Effect of earthworms on the performance and microbial communities of excess sludge treatment process in vermifilter. Bioresour Technol 117:214–221. doi:[10.1016/j.biortech.2012.04.096](http://dx.doi.org/10.1016/j.biortech.2012.04.096)
- Lourenço N, Nunes LM (2017) Optimization of a vermifiltration process for treating urban wastewater. Ecol Eng 100:138–146. doi[:10.1016/j.ecoleng.2016.11.074](http://dx.doi.org/10.1016/j.ecoleng.2016.11.074)
- Malek TEUA, Ismali SA, Ibrahim MH (2012) Vermifiltration of palm oil effluent (POME). In: UMT 11th international annual symposium on sustainability science and management, Terengganu
- Roy D, Hassan K, Boopathy R (2010) Effect of carbon to nitrogen (C:N) ratio on nitrogen removal from shrimp production waste water using sequencing batch reactor. J Ind Microbiol Biotechnol 37:1105–1110. doi:[10.1007/s10295-010-0869-4](http://dx.doi.org/10.1007/s10295-010-0869-4)
- Sinha RK (2010) Vermiculture technology: reviving the dreams of Sir Charles Darwin for scientific use of earthworms in sustainable development programs. Technol Invest 1:155–172. doi[:10.4236/](http://dx.doi.org/10.4236/ti.2010.13019) [ti.2010.13019](http://dx.doi.org/10.4236/ti.2010.13019)

- Sinha RK, Bharambe G, Chaudhari U (2008) Sewage treatment by vermifiltration with synchronous treatment of sludge by earthworms: a low-cost sustainable technology over conventional systems with potential for decentralization. Environmentalist 28:409–420. doi:[10.1007/s10669-008-9162-8](http://dx.doi.org/10.1007/s10669-008-9162-8)
- Taylor M, Clarke W, Greenfield P (2003) The treatment of domestic wastewater using small-scale vermicompost filter beds. Ecol Eng 21:197–203. doi:[10.1016/j.ecoleng.2003.12.003](http://dx.doi.org/10.1016/j.ecoleng.2003.12.003)
- Tchobanoglous G, Burton FL, Stensel HD (2003) Wastewater engineering: treatment and reuse, 4th edn. McGraw-Hill, New York
- Toffey WE (2008) Biofiltration Basics: Biofilter Design, Operational Overview 54–58
- Tomar P, Suthar S (2011) Urban wastewater treatment using vermibiofiltration system. Desalination 282:95–103. doi:[10.1016/j.](http://dx.doi.org/10.1016/j.desal.2011.09.007) [desal.2011.09.007](http://dx.doi.org/10.1016/j.desal.2011.09.007)
- United States Environmental Protection Agency (2004) Onsite wastewater treatment systems manual. Office of Water and Office of Research and Development, Washington
- Wang S, Yang J, Lou S-J (2010) Wastewater treatment performance of a vermifilter enhancement by a converter slag–coal cinder filter. Ecol Eng 36:489–494. doi:[10.1016/j.ecoleng.2009.11.018](http://dx.doi.org/10.1016/j.ecoleng.2009.11.018)
- World Health Organization (2006) Guidelines for the safe use of wastewater, excreta and greywater. Wastewater use in agriculture 2, Genève, pp 222
- Xing M, Yang J, Lu Z (2005) Microorganism-earthworm integrated biological treatment process—a sewage treatment option for rural settlements. ICID 21st European regional conference, Frankfurt
- Xing M, Li X, Yang J (2010) Treatment performance of small-scale vermifilter for domestic wastewater and its relationship to earthworm growth, reproduction and enzymatic activity. Afr J Biotechnol 9:7513–7520. doi[:10.5897/AJB10.811](http://dx.doi.org/10.5897/AJB10.811)
- Yang F, Wang L, Wang G, Du P, Zhang Y (2015) Organic matter and nitrogen distribution, and functional groups of filter at earthworm packing bed in vermifiltration. Pol J Environ Stud 24(1):375–380
- Zhang J, Huang X, Liu C, Shi H, Hu H (2005) Nitrogen removal enhanced by intermittent operation in a subsurface wastewater infiltration system. Ecol Eng 25:419–428. doi[:10.1016/j.ecoleng.](http://dx.doi.org/10.1016/j.ecoleng.2005.06.011) [2005.06.011](http://dx.doi.org/10.1016/j.ecoleng.2005.06.011)

