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# Mechanistic evaluation and reaction pathway of UV photo-assisted Fenton-like degradation of progesterone in water and wastewater

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Abstract The mechanisms and reaction pathway of UV photo-assisted Fenton-like degradation of progesterone in water and wastewater were investigated. The reaction followed the pseudo-first-order kinetics for both the dark Fenton-like and UV photo-Fenton-like processes. The reaction kinetics of the UV photo-assisted process improved with the presence of humic acid (HA) in wastewater, due to the formation of Fe(III)-HA complexes which enhanced Fe(II) production by a ligand-to-metal charge transfer. The UV photo-assisted process reduced the amount of ferric required to completely degrade progesterone by 60 % and lowered the activation energy to 42 kJ/mol compared to 104 kJ/mol for the dark Fenton-like process. Complete degradation of progesterone was achieved through a multi-step process involving several intermediate compounds.

Keywords Degradation - Endocrine disruptors - Photo-Fenton - Progesterone - Ultraviolet irradiation

# Introduction

Endocrine disrupting chemicals (EDCs), particularly the steroid hormones, have been detected in wastewater effluent around the world (Ko et al. [2007](#page-8-0); Kueh and Lam [2008;](#page-8-0) Xu et al. [2014\)](#page-9-0). They have generated considerable

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research on the potential global threat these chemicals pose to both human health and the environment. These chemicals, particularly the oestrogens and progestogens, disrupt the natural functioning of the endocrine system. The principal sources of release into the environment are through wastewater treatment plants (WWTPs) (Basile et al. [2011;](#page-8-0) Sin et al. [2011;](#page-9-0) Ifelebuegu [2011\)](#page-8-0). Other sources of EDCs to waterways include agricultural run-offs and steroidal hormones excreted by livestock (Gadd et al. [2010](#page-8-0); Bartelt-Hunt et al. [2012;](#page-8-0) Lim et al. [2013](#page-8-0)). Conventional biological wastewater treatment processes used in the wastewater industry are not adequate to completely eliminate these chemicals, hence the search for more efficient processes (Nakada et al. [2006](#page-9-0); Kraigher et al. [2008](#page-8-0); Balabanic et al. [2012](#page-8-0)).

Various advanced oxidation processes (AOPs) have been applied successfully for the removal or degradation of toxic pollutants for conversion into biodegradable compounds, which can then be treated by conventional biological methods. The efficiency of AOPs is dependent on the generation of reactive free radicals, especially the hydroxyl radicals (Klavarioti et al. [2009\)](#page-8-0). The hydroxyl radical is responsible for the oxidation and mineralisation of organic compounds to water and carbon dioxide (Matilainen and Sillanpaa [2010](#page-8-0); Ifelebuegu et al. [2014](#page-8-0)). Hydroxyl radicals possess strong reactive electrophilic properties that make them effective for destroying organic compounds by reacting non-selectively and rapidly with almost all electron-rich organic compounds (Fan et al. [2012](#page-8-0)).

Fenton oxidation is widely considered and used for the treatment of highly contaminated waters amongst other AOPs in wastewater treatment. It is an advanced oxidation process that generates a highly reactive HO by the combination of Fe<sup>2+</sup> and hydrogen peroxide  $(H_2O_2)$ . The



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concentration.

<span id="page-1-0"></span>organics than the dark reaction process and can take advantage of utilising UV irradiation (Kavitha and Palanivelu [2004;](#page-8-0) Navarro et al. [2011;](#page-9-0) Vilar et al. [2012\)](#page-9-0). The Fenton process is dependent on conditions such as pH, reaction time, temperature, ratio of  $\text{Fe}^{2+}$  to  $\text{H}_2\text{O}_2$ , and iron

Fenton-like oxidation is an AOP that is based on ferric  $(Fe^{3+})$  and H<sub>2</sub>O<sub>2</sub>, in which H<sub>2</sub>O<sub>2</sub> plays the role of an oxidative agent, and ferric ion plays that of a catalytic agent (Tamimi et al. [2008\)](#page-9-0). This is usually carried out at an acidic pH level (pH 3) to prevent the occurrence of iron hydroxide precipitation, for the degradation of organic compounds (Mohapatra et al. [2011\)](#page-9-0). The reaction between  $Fe<sup>3+</sup>$  and H<sub>2</sub>O<sub>2</sub> leads first to the formation of Fe<sup>2+</sup> and hydroperoxide radical (Eq. 1), and the Fenton reaction between the formed Fe<sup>2+</sup> and H<sub>2</sub>O<sub>2</sub> gives rise to the generation of hydroxyl radicals (Eq. 2) responsible for the mineralisation of organic compounds in aqueous solutions.  $\text{Fe}^{3+} + \text{H}_2\text{O}_2 \rightarrow \text{Fe}^{2+} + \text{HO}_2 + \text{H}^+$  (1)  $\text{Fe}^{2+} + \text{H}_2\text{O}_2 \rightarrow \text{Fe}^{3+} + \text{OH} + \text{OH}^-$  (2) The Fenton process has been shown to be a good option for the removal of micro-contaminants from water systems (Klavarioti et al. [2009](#page-8-0); Ifelebuegu and Ezenwa [2011](#page-8-0); Rivera-Utrilla et al. [2013\)](#page-9-0). Although the impact and treatment of oestrogens are well documented in the literature, a limited study has been conducted on the removal and treatment of progesterone (Fayad et al. [2013](#page-8-0); Liu et al. [2009;](#page-8-0) Ifelebuegu and Onwugbuta [2016\)](#page-8-0)—the most important and only naturally occurring progestogen. The aim of this paper is to determine the mechanisms of photo-Fenton-like degradation of progesterone (Fig. 1) in water and wastewater and to propose a degradation pathway. This study was carried between 2014 and 2015

## Materials

Progesterone (99 %) was purchased from Sigma-Aldrich UK. Analytical grade ferric nitrate  $(Fe(NO<sub>3</sub>)<sub>3</sub>·9H<sub>2</sub>O)$ , 30 % hydrogen peroxide  $(H_2O_2)$ , sodium hydroxide (NaOH), hydrochloric acid (HCl), potassium permanganate  $(KMnO<sub>4</sub>)$ , and methanol  $(CH<sub>3</sub>OH)$  was obtained from Fisher Scientific UK. Milli-Q water was obtained from a water purification system (Millipore, USA), resistivity  $\geq 8$   $\Omega$ M. Unless otherwise stated, all samples were prepared in deionised water obtained from a water purification system. Wastewater effluent was obtained from an activated sludge plant in Coventry, UK.

## Fenton-like oxidation treatment

Non-photocatalytic experiments were undertaken to establish their isolated influence on the degradation of progesterone. A 150 mL of 2 mg/L progesterone solution in milli-Q water was transferred into a 250 mL batch reactor. The solution was adjusted to pH 3 using 1 M HCl to prevent iron precipitate formation (Mohapatra et al. [2013](#page-9-0)). To determine the optimum iron concentration, various ferric concentrations (4, 7.5, 15, 30, 75 and 85 mg/L as Fe) were prepared. A molar ratio of  $1:10$  of Fe: $H<sub>2</sub>O<sub>2</sub>$  was used as it is said to be effective for Fenton oxidation (Mert et al. [2010](#page-8-0); Nakrst et al. [2010](#page-9-0)). Details of the analytical procedures have been previously reported by Ifelebuegu and Ezenwa ([2011\)](#page-8-0). The thermodynamic evaluation was carried out at varying temperatures of 20, 25, 30 and  $35 \pm 2$  °C.

# Photo-Fenton-like oxidation treatment

The photo-Fenton-like oxidation was carried out under the same experimental conditions as the Fenton-like oxidation.



at Coventry University, UK.



The only difference was the introduction of a UV lamp set at a wavelength of 254 nm  $(E = 6 \text{ J/cm}^2)$ , which was placed at a distance of 10.5 cm from the surface of the reactor. The photo-Fenton-like experiments were conducted as described by Yaping and Jiangyong [\(2008](#page-9-0)) at temperature of  $25 \pm 2$  °C. The experiments were also repeated using wastewater to evaluate the effects of natural organics on the degradation kinetics.

#### Instrumental analysis

Analytical determination of progesterone concentration was carried out on a Hewlett-Packard Series 1050 HPLC system (HP UK) equipped with a UV detector wavelength set at 254 nm). A UV lamp with BDH dual wavelength of 365/254 nm was used as the source of UV radiation; the lamp was set to 254 nm for the photo-Fenton-like experiments. The separation was done on a Thermo ODS Hypersil  $C_{18}$  column (150  $\times$  4.6 mm, 5 µm) (ThermoFisher UK) fitted with a guard column. The mobile phases methanol and water (80:20) ran in an isocratic mode with a flowrate of 1.2 mL/min and a total runtime of eight minutes (Ifelebuegu et al. [2010\)](#page-8-0). The analysis and identification of byproducts were carried out through an LC–MS/MS (Applied Biosystems, Carlsbad, CA, USA) as previously described elsewhere (Kanda and Churchley [2008;](#page-8-0) Ifelebuegu [2011](#page-8-0)). The humic matter was measured by TOC-V CSH total organic carbon analyser. Wastewater characteristics were analysed according to established methods (APHA [2012](#page-8-0)).

# Results and discussion

## Effect of ferric concentration

The effect of initial ferric concentration on the removal of progesterone in Milli-Q water was studied at pH 3 (Ifelebuegu and Ezenwa [2011;](#page-8-0) Li and Zhang [2014\)](#page-8-0). Various concentrations of Fe(III) were used at 60 min of treatment time and a temperature of  $25^{\circ}$  ± 2 °C. The effects of Fe(III) concentration (4–85 mg/L as Fe) on the degradation of progesterone are shown in Fig. 2a, b. The results obtained indicate that an increase in ferric concentration resulted in an increased percentage conversion of progesterone. Increasing concentrations of ferric is usually beneficial in the decomposition of  $H_2O_2$  and this enhanced progesterone degradation until excess ferric (above 75 mg/L), did not further improve the degradation process but started to act as hydroxyl radical scavenger. All further experiments were conducted at a ferric concentration of 30 mg/L. This trend is consistent with previous studies by Babuponnusami and Muthukumar ([2012](#page-8-0)) and Li et al. ([2012\)](#page-8-0). They observed that the increase in iron concentration yielded



Fig. 2 Progesterone removal at varying concentrations of Ferric (using 1:10 ferric to H<sub>2</sub>O<sub>2</sub> molar ratio), pH 3 at 25  $\pm$  2 °C and initial progesterone concentration of 2 mg/L. a Fenton-like, b Photo-Fentonlike)

greater degradation of contaminants. This could be as a result of the increased formation of  $Fe(III)$ – $H_2O_2$  complexes, resulting in increased ferrous ion and hydroxyl radical formation, consequently accelerating degradation. The total degradation of 2 mg/L of progesterone was achieved by the Fenton-like process at a maximum ferric concentration of 75 mg/L as Fe, while complete degradation was achieved for the photo-assisted reaction process at a maximum ferric concentration of 30 mg/L as Fe. The amount of ferric concentration required for complete degradation is reduced by more than 50 % with the photoassisted reaction. This can be attributed to the increased production of hydroxyl radicals under photo-irradiation, caused by the continuous recycling of Fe(II), as its formation from the reduction of Fe(III) is enhanced by the irradiation process (Zepp et al. [1992](#page-9-0)). Additionally, in the photo-Fenton-like degradation process,  $H_2O_2$  is dissociated under irradiation to produce hydroxyl radical, as the emission wavelength of the UV (254 nm) light used is within the range of the absorbance spectrum of  $H_2O_2$ .



#### <span id="page-3-0"></span>Reaction time and kinetics

The efficiency of the photo-Fenton process has been reported to depend on the rate of formation and scavenging of hydroxyl radicals, which vary according to the type of organic substrate and the irradiation time (Elmolla and Chaudhuri [2009](#page-8-0); Alalm et al. [2015](#page-8-0)). Figure 3 shows the effect of time on the degradation of progesterone at pH 3 and ferric concentration of 30 mg/L. It was observed that the degradation of progesterone took place in two stages: the first where it was rapidly degraded and a second where degradation rate slowed. This initial rapid removal could be as a result of ferrous ions reacting very quickly with  $H_2O_2$  to generate large numbers of hydroxyl radicals, which then rapidly react with progesterone in the initial stage. The slower second stage reaction could be as a result of the slow regeneration of Fe(II) from Fe(III) with increases in reaction time. A similar result was obtained by Zhang and Wang  $(2011)$  $(2011)$ , who found the optimum reaction time of 30 min for the Fenton treatment with a batch reactor for treatment of landfill leachates. This result also compares favourably with a previous study conducted by Frontistis et al. ([2011\)](#page-8-0), who observed an 80 % removal of  $17\beta$ -estradiol (E2) from wastewater from a WWTP in China after 20 min of irradiation time when compared to the Fenton oxidation, which achieved a 35 % removal of E2 after 20 min.

For an evaluation of the kinetics of both oxidation processes for the degradation of progesterone in wastewater, the pseudo-first-order and pseudo-second-order kinetics were used to fit the experimental data. The expressions guiding the reaction kinetics are those of Lagergren pseudo-first-order and pseudo-second-order



Fig. 3 Fenton-like and Photo-Fenton-like oxidation: effect of reaction time and corresponding % removal of progesterone in water. pH 3 at  $25 \pm 2$  °C, initial progesterone concentration of 2 mg/L and ferric concentration of 30 mg/L



kinetic models. The pseudo-first-order kinetic model is expressed in Eq. 3. The reaction rate constant was determined from the equation below:

$$
C = C_0 e^{-kt} \tag{3}
$$

where  $C_0$  is the initial concentration of the progesterone, k the rate constant and  $t$  the time in minutes. Representing the equation in an integral form, it becomes

$$
\ln \frac{C}{C_0} = -kt. \tag{4}
$$

The pseudo-second-order kinetics model is expressed as shown below:

$$
C = \frac{C_0}{1} + k_2 t.
$$
 (5)

Representing the Equation in an integral form, it becomes

$$
\frac{1}{C} - \frac{1}{C_0} = k_2 t.
$$
\n(6)

A graph of  $\ln C/C_0$  against different time intervals showing pseudo-first-order reaction and a graph of  $\frac{1}{C} - \frac{1}{C_0}$ against different time intervals depicting a pseudo-secondorder reaction were plotted to determine the kinetic model which best suits the degradation of progesterone in Milli-Q water (Table 1). The values of the apparent rate constants were calculated by linear regression and the summaries are presented in Table [2](#page-4-0) with their corresponding correlation coefficients.

Previous studies on the advanced oxidation of oestrogenic steroid hormones reported that the reaction followed second-order kinetics (Deborde et al. [2004](#page-8-0); Ifelebuegu and Ezenwa [2011\)](#page-8-0). In this work, both the Fenton-like and photo-Fenton-like oxidation of progesterone showed a better fit to the pseudo-first-order kinetic model compared to the second-order kinetic model by the correlation coefficient, suggesting that the degradation rate may be dependent on the initial concentrations of progesterone.

Table 1 Wastewater effluent characteristics

Parametes	Average (mg/L)		
<b>COD</b>	65.5		
SS	15.2		
<b>BOD</b>	10.51		
<b>DOC</b>	11.2		
Humic matter	18.4		
Phosphate	0.6		
Nitrate	8.5		

<span id="page-4-0"></span>Table 2 Fenton-like and photo-Fenton-like oxidation: rate constants and correlation coefficient values obtained from the pseudo-first-order and pseudo-second-order kinetic models at  $25^{\circ}$ C for Milli-O water

Water type	Reaction type	Reaction kinetics			
		Pseudo-first-order kinetic model		Pseudo-second-order kinetic model	
		$k(10^{-3} \text{ min}^{-1})$		$k_2$ (m <sup>-1</sup> s <sup>-1</sup> )	$R^2$
Milli-O water	Fenton-like	$15 \pm 2$	0.937	$21 \pm 5$	0.928
	Photo-Fenton-like	$44 \pm 6$	0.982	$22 + 2$	0.929

Table 3 Fenton-like and photo-Fenton-like oxidation: rate constants and correlation coefficient values obtained from the pseudo-first-order and pseudo-second-order kinetic models at 25 °C for wastewater effluent



## Effect of natural organic matter on reaction kinetics

The effect of dissolved organics on the degradation of progesterone was also investigated by using effluent wastewater from a local WWTP (Table [1\)](#page-3-0). The experiments were conducted at temperature of  $25 \pm 2$  °C and pH 3. It can be seen from Table 3 that there was no significant changes in the first and second-order rate constants for the dark Fenton-like process in Milli-Q water  $(k = 0.015 \text{ min}^{-1}, k_2 = 21 \text{ M}^{-1} \text{s}^{-1})$  compared to wastewater  $(k = 0.012 \text{ min}^{-1}, k_2 = 25 \text{ M}^{-1} \text{s}^{-1})$ , while the rate constants for the photo-assisted process increased at a more significant rate  $(k = 0.044 \text{ min}^{-1}, k_2 = 22 \text{ M}^{-1} \text{s}^{-1}$  for Milli-Q water and  $k = 0.098 \text{ min}^{-1}$ ,  $k_2 = 119 \text{ M}^{-1} \text{s}^{-1}$  for wastewater). This suggests that the presence of dissolved organics enhanced the photo-assisted degradation of progesterone. This can be attributed to the presence of humic acid (HA) in the wastewater effluent. Previous studies have reported significant enhancement of the degradation of phenolic moieties in the presence of HA (He et al. [2010](#page-8-0); Jiang et al. [2010](#page-8-0)). Leech et al. ([2009\)](#page-8-0) also reported an enhanced degradation of oestrogens during irradiation due to the organic radical formation from the interaction of humic acid, sunlight, and oxygen. We postulate that the improved photo-Fenton degradation of progesterone in the presence of humic acid is due to Fe(III)-HA complex formation, which under irradiation encourages the formation of Fe(II) by ligand-to-metal charge transfer (Ou et al. [2009](#page-9-0)).

## Effects of temperature on reaction kinetics

The effects of temperature on the degradation rates of progesterone by Fenton-like and photo-Fenton-like degradation were investigated at varying temperatures (20, 25, 30 and 35 °C), pH 3 and ferric concentration of 30 mg/ L. This is represented in Fig. [4](#page-5-0). The observed increase in degradation rate with temperature can be attributed to the fact that at higher temperatures, the generation of hydroxyl radicals are enhanced (Khamaruddin et al. [2011;](#page-8-0) Aygun et al. [2012](#page-8-0)), increasing the degradation rate constant and hence accelerating progesterone degradation.

The significant activation energies of the degradation of progesterone were determined from the Arrhenius equation expressed as:

$$
k = A_0 e^{-\frac{E_a}{RT}} \tag{7}
$$

where k is the rate constant for the reaction,  $A_0$  is the Arrhenius factor,  $E_a$  is the activation energy for the reaction,  $T$  is the solution temperature, and  $R$  is the gas constant  $(8.314 \text{ J/(mol K)})$ . A plot of ln k against  $1/T$  was used to evaluate the activation energy  $(E_a)$ .

## Fenton–like oxidation

 $E_a$  and  $A_0$  for the reaction were evaluated from the slope and intercept of the Arrhenius plot of  $ln(k)$  against  $1/T$ , which had a good linear relationship ( $R^2 = 0.9593$ ). The value of the activation energy,  $E_a$ , obtained from the Arrhenius plot shown in Fig. [5a](#page-5-0), b was found to be 103.6 kJ/mol and  $A_0 = 4.27 \times 10^{16}$  min<sup>-1</sup>, which indicates the rate of collision of molecules.

The value of the activation energy  $E_a$  obtained from the Arrhenius plot shows that the reaction rate of Fenton oxidation of progesterone in wastewater is very sensitive to temperature change and also that it is hard for the reaction to occur (degradation of progesterone), as the activation



<span id="page-5-0"></span>

Fig. 4 Degradation rates of progesterone at varying temperatures, pH 3, initial progesterone concentration of 2 mg/L and ferric concentration of 30 mg/L

energy value was observed to be high. This is in support of the findings of Chen and Zhu ([2007\)](#page-8-0), who stated that the values of activation energy of thermal reactions are usually between 60 and 250 kJ/mol. Also, the high activation energy can be attributed to the presence of the carbon– carbon double bond that exists in progesterone molecules (Cendejas-Santana et al. [2002](#page-8-0)), as progesterone is known to belong to the ketone and oxygenated functional with a carbon–carbon bond possessing energies around 376.81 kJ/mol (Nicotra [2009](#page-9-0)). So, for degradation of progesterone to occur, these bonds have to be broken, resulting in high activation energy.

## Photo-Fenton-like oxidation

In the photo-Fenton-like oxidation process, an activation energy  $E_a$  value of 42.01 kJ/mol ( $R^2 = 0.9436$ ) was obtained from the slope of the plot and a pre-exponential factor value of 2.41  $\times$  10<sup>9</sup> min<sup>-1</sup> from the y-intercept of the plot. The low activation energy obtained in the photo-Fenton process (a 60 % reduction compared to the





Fig. 5 a Fenton-like and b photo-Fenton-like oxidation: Arrhenius plot at all studied temperatures for the removal of progesterone in water



Fig. 6 Progesterone and DOC profile for UV photo-Fenton-like oxidation in wastewater effluent pH 6.8 at  $25 \pm 2$  °C and initial progesterone concentration of 2 mg/L, ferric concentration of 30 mg/L

<span id="page-6-0"></span>



Table 5 Predominant transformation by-products of progesterone identified during the UV photo-assisted Fenton-like degradation of progesterone in Milli-Q water after 30 min of reaction time

Compound	Structure	$RT$ (min)	Molecular weight	m/z % abundance
4-Hydroxyl butanoic acid C <sub>4</sub> H <sub>8</sub> O <sub>3</sub>		6.60	104	260 (100),
				$346(25)$ ,
	HO. ЮH			256 (14)
Acetaldehyde $C_2H_4O$		5.20	44	265 (100),
	$H_3C$ Н			242 (45)
Oxalic acid $C_2H_2O_4$	O	5.30	90	284 (100),
	OH. HO $\Omega$			365(48)
Methanoic acid $CH2O2$	O	5.80	46	284 (100),
	OH H.			254 (45)

activation energy of the dark Fenton-like process) could be as a result of the presence of the recycled  $\text{Fe}^{2+}$  catalyst and the photo-catalytic effects of the UV irradiation, which speed up the reaction by lowering the transition state. Lower activation energy will result in larger rate constants as presented in Table [3](#page-4-0), because the rate of a reaction is directly complementary to the rate constant  $k$ .

# Mineralisation and degradation by-products

Figure [6](#page-5-0) shows the change in the concentration of progesterone during the photo-Fenton degradation process and the corresponding changes in DOC. The values demonstrate the presence of degradation by-products of progesterone oxidation. The double bonds in the progesterone molecule between





Fig. 7 Proposed reaction pathway

C4 and C5, the hydroxyl group on C12 and double bond oxygen on C3 (Fig. [1](#page-1-0)a, b), are the likely points of hydroxyl radical attack. Hydroxyl radicals are known to transform olefinic moieties by electrophilic attack at these double bonds (Lee and von Gunten [2010;](#page-8-0) Yang et al. [2012](#page-9-0)). The proposed pathway is, therefore, a  $2 + 2$  addition to the olefinic bonds by the organometallic complex formed (Yang et al. [2012](#page-9-0)). There is also the possibility of hydroxyl radical addition to the olefinic bond forming cyclic esters (Yang et al. [2012](#page-9-0)). The increased BOD/COD ratios also suggest increased biodegradability of the post-photo-Fenton-like oxidation effluent, suggesting the transformation of the by-products through ring rupturing reactions into simpler molecules like carboxylic acids and acetaldehydes (Zhao et al. [2008](#page-9-0)). Tables [4](#page-6-0) and [5](#page-6-0) indicate the identified predominant by-products. It can be concluded that there was a multi-step degradation of the progesterone involving several intermediate transformation by-products that went through further degradation and ring rupture to form simpler organic molecules, carbon dioxide, and water. This is supported in Fig. [6](#page-5-0) by the gradual drop in the DOC after 30 min of degradation time. Figure 7, therefore, proposes a possible pathway for the UV photo-assisted degradation of progesterone.

# Conclusion

The mechanism and reaction pathway of UV photo-assisted Fenton-like degradation of progesterone in water and wastewater were investigated in this study. There was a 60 % reduction in the ferric requirement by the photo-assisted Fenton-like process compared to the dark Fenton process. The kinetic data obtained fitted the pseudo-firstorder model for both processes. The activation energy for the Fenton-like degradation of 104 kJ/mol was significantly reduced to 42 kJ/mol with the UV photo-assisted process due to the photocatalytic effect. The presence of humic acid in wastewater effluent enhanced the UV photoassisted degradation process through the formation of Fe(III)-HA complexes, which produced Fe(II) by ligand-tometal charge transfer. The overall degradation of progesterone was a step change with initial oestrogen-like byproducts and eventual ring rupture, resulting in a complete transformation to simpler organics, carbon dioxide, and water.

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