#### **ORIGINAL ARTICLE**



# β-Glucosidase production by *Trichoderma reesei* and *Thermoascus aurantiacus* by solid state cultivation and application of enzymatic cocktail for saccharification of sugarcane bagasse

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#### Abstract

For degradation of sugarcane bagasse (SCB), several enzymes are needed but  $\beta$ -glucosidase is rate limiting in cellulose hydrolysis. Since different microorganisms synthetize characteristic pool of enzymes, mixing extracts produced by different species may increase hydrolytic efficiency due to synergism between enzymes in cocktails. This paper reports the study of  $\beta$ -glucosidase production in solid state cultivation (SSC) of two filamentous fungi, thermophilic *Thermoascus aurantiacus* and mesophilic *Trichoderma reesei*, and application of the enzymatic extracts on non-pretreated SCB saccharification. Enzyme extract obtained from the thermophilic fungus presented higher  $\beta$ -glucosidase and FPU activities (1.8 U/mL and 10 FPU/mL) than the one from mesophilic (0.2 U/mL and 6 FPU/mL). Optimal SCB hydrolysis was achieved when applying enzymatic cocktail composed of equal volumes of both fungal extracts (3.6 FPU/g<sub>SCB</sub>, filter paper units per gram SCB, 2.25 FPU/g<sub>SCB</sub> provided by extract from *T. aurantiacus* and 1.35 FPU/g<sub>SCB</sub> from *T. reesei*) at 65 °C. The hydrolysis yield applying the enzyme cocktail, 124 mg total reducing sugars (TRS) per g<sub>SCB</sub>, was higher than any yield achieved when using the enzyme extracts separately (105 mg<sub>TRS</sub>/g<sub>SCB</sub> using 12.5 FPU per g<sub>SCB</sub> from *T. aurantiacus* at 65 °C; 79 mg<sub>TRS</sub>/g<sub>SCB</sub> using 7.5 FPU per g<sub>SCB</sub> from *T. reesei* at 45 °C). Therefore, the use of the cocktail (3.6 FPU/g<sub>SCB</sub>) at 65 °C released 18 and 57% more TRS respectively than when extracts from *T. aurantiacus* or from *T. reesei* were applied alone, respectively, even reducing enzyme load (FPU) by 70%, corroborating the synergistic effect when both extracts are used together.

Keywords Biofuels · Fermentation biotechnology · Fungal growth · Enzymes · Hydrolysis

#### Highlights

- Fungal biomass was well estimated based on total protein content by the Kjeldahl method;
- β-Glucosidase activity production was strongly and directly associated with fungal growth;
- Enzymes in cocktail have a synergistic effect on the hydrolysis of sugarcane bagasse.

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Thermophilic fungus yielded more β-glucosidase than the mesophilic one, in a shorter time;

# 1 Introduction

Global concern about depletion of fossil fuel deposits and greenhouse gas effects demands research on renewable energy alternatives. Hence, large-scale production of clean fuels, such as bioethanol, is attracting worldwide interest. Assessments for 2030 estimate potential production of lignocellulosic or second generation ethanol (E2G) enough to provide 10<sup>19</sup> J of energy or 10.5% of current transport fuel demand, using 25% of global forestry and agricultural residues for biofuel production [1].

In Brazil, sugarcane bagasse (SCB) is an abundant agroindustrial by-product for conversion to E2G, since it is a potential source of fermentable sugars [2]. During the 2017/ 2018 season, nearly 641 million tons of sugarcane (*Saccharum officinarum*) were harvested in Brazil [3], generating around 160 million tons of SCB. However, production of E2G from SCB is limited by the recalcitrance of this biomass. The most eco-friendly alternative to produce biofuels is via an enzymatic route, which requires cellulolytic and hemicellulolytic enzymes to depolymerize the biomass into fermentable sugars. Nevertheless, the high cost of commercial enzymes is a key economic factor in E2G production via an enzymatic route [4].

Some strategies are being applied that aim to reduce the effective cost of cellulases, such as the use of cheap raw materials for its production or the use of the enzymes in their crude form, without purification [5]. In this context, studies on obtaining cellulases and hemicellulases and optimizing production processes are very important.

Solid state cultivation (SSC) is a bioprocess that provides high concentrations of enzymes. SSC offers environmentally friendly and economical technology with simple process operations, thereby lowering capital and operational costs. However, SSC still requires further studies for it to become a viable industrial process, comprising selection of microorganisms and substrates [6, 7].

Filamentous fungi yield high activities of cellulolytic and hemicellulolytic enzymes by SSC because this bioprocess mimics the natural habitat of those microorganisms that release high levels of enzymes to an extracellular solid medium [6]. Utilization of agro-industrial by-products as substrates is another great advantage of SSC due to the low cost of these substrates [7].

Nevertheless, direct quantification of biomass in SSC systems is not feasible due to the impossibility of separating the various components of the cultivated media (substrate, microorganism, enzymes, and others), particularly for filamentous fungi, since their hyphae strongly bind to the particle surface and may penetrate far inside the particles. Hence, indirect methods of estimating biomass must be used in SSC. Some of them are based on quantification of specific constituents of microbial cells (e.g., chitin, ergosterol, nucleic acids, and proteins) and of biological activity (e.g., ATP production, enzyme activity, nutrient consumption, and respiration gases) [8]. The Kjeldahl method, based on estimation of total nitrogen, can be used for indirect estimative of fungal growth kinetics in SSC [9].

The role of enzymatic cocktails in performing the hydrolysis of cellulose and hemicellulose has called attention. The efficiency with which cellulose is hydrolyzed by enzymes depends on many factors, such as characteristics of the substrate and nature of the enzymatic systems. Recent research has focused on the optimization of the enzymatic profile employed in the process by using enzymatic cocktails as one of the factors to improve both the yield and the rate of enzymatic hydrolysis [10].

The utilization of abundantly available lignocellulosic biomass requires an efficient cellulolytic enzyme system. It is known that the complete degradation of complex molecules such as cellulose requires several enzymes acting together. The action of cellulolytic enzymes depends on at least three hydrolases: endoglucanase, exoglucanase, and  $\beta$ -glucosidase, with the last being essential to avoid an inhibitory effect of cellobiose [10]. Considering that different microorganisms synthetize a characteristic pool of enzymes even when cultivated using the same substrate and under the same conditions, the formulation of enzymatic cocktails obtained by mixing extracts produced by different microorganisms is an alternative to increase the efficiency of the enzymatic hydrolysis, since different enzymes can act synergistically [11].

Based on our previous results and on the literature, two species of fungi are expected to present good potential for producing high levels of cellulases and hemicellulases, the thermophilic *T. aurantiacus* and the mesophilic *T. reesei* [12]. *T. aurantiacus* is a good producer of endoglucanase and endoxylanase, but produces low exoglucanase activity [12]. This thermophilic fungus is also a good source of  $\beta$ -glucosidases [13]. *T. reesei* is recognized for its ability to produce several extracellular enzyme systems involved in the hydrolysis of polysaccharides, but it has a deficiency in  $\beta$ -glucosidases [10]. Thus, an increase in hydrolysis efficiency can be expected by looking for synergism between enzymes from both these fungi.

In the current study, we produced cellulases from both fungi on SSC using agro-industrial by-products as substrates, focusing on the maximization of  $\beta$ -glucosidase production and its relation with growth kinetics. As these fungi present different adaptive and physiological responses (secreted enzymatic activity), we have also studied different compositions of solid medium, based on enzyme production and on specific growth rates. The enzyme extracts and an enzymatic cocktail were applied for the hydrolysis of SCB in order to test the expected synergistic effect.

## 2 Materials and methods

## 2.1 Microorganisms and substrates

The thermophilic fungus *T. aurantiacus* CBMAI756 and the mesophilic *T. reesei* QM9414 were used. They belong to the collection of the Laboratory of Biochemistry and Applied Microbiology of the Institute of Biosciences, Letters and Exact Sciences (IBILCE) of the São Paulo State University (UNESP). They were grown in Dextrose-Sabouraud-Agar (DSA), *T. aurantiacus* at 45 °C for 48 h and *T. reesei* at 28 °C for 168 h.

The culture media for the SSC experiments contained sugarcane bagasse (SCB) and wheat bran (WB). SCB was kindly provided by Usina Vale (Onda Verde-SP, Brazil) and was ground in a knife mill and sieved. The fraction used was that which passed through a sieve with 3-mm openings but was retained by one with 1.44 mm openings. This fraction was washed with tap water to remove dirt and remaining sugar and dried to constant weight in a convective oven at 60 °C. It was then placed in plastic bags and stored at 5 °C. The wheat bran (Cerealista Alvorada, São José do Rio Preto-SP, Brazil) was purchased from a local retailer and was not handled prior to use.

#### 2.2 SSC experiments for β-glucosidase production

SSC experiments were done in plastic bags 12 cm  $\times$  20 cm with a circular opening 3.6 cm in diameter closed with a cotton wool plug, in order to allow gas exchange and avoid contamination. Each plastic bags received 5 g of substrate (dry weight). The sets of plastic bags and substrates were sterilized in an autoclave at 121 °C for 20 min. For inoculation, spores were suspended with nutrient solution enriched with mineral salts [14]. The spore concentration was fixed at 10<sup>7</sup> spores/mL, using a hemocytometer, and 1 mL was added to each bag. The moisture content of the substrate was adjusted by adding nutrient solution to the solid media. *T. aurantiacus* was cultivated at 50 °C for 120 h; *T. reesei* at 28 °C for 168 h.

Some plastic bags were destined for  $\beta$ -glucosidase activity quantification along and at the end of cultivation, as well as some bags were used for indirect measurements of fungal biomass. Each plastic bag was an independent sample. Three identical bags (triplicates) were used for each quantification.

Minitab 15.0 (Minitab Inc., State College, USA) was used for experimental design and statistical analysis, in which the response was the  $\beta$ -glucosidase activity. The chosen experimental design for solid state cultivation was a full-factorial design with random blocks and two factors with three levels for each factor. The factors were (i) moisture content of the substrate, with levels 70, 75, and 80% (wet basis) and (ii) composition of the substrate, with levels SCB:WB 1:1, 3:1, and 9:1 w/w. The fungi were treated as blocks of the design. ANOVA analysis and means comparisons using the Tukey test were performed in order to

find the conditions that provided the highest  $\beta$ -glucosidase activities. All statistical significance levels were 95%.

#### 2.3 Enzymatic activity quantification

For samples destined for enzymatic activity quantification (along and at the end of cultivation), distilled water was added to the fermented material (20 mL/g of initial dry substrate) after 120 h for *T. aurantiacus* and after 168 h for *T. reesei*, followed by agitation at 100 rpm for 30 min at room temperature and centrifugation at  $10^4g$  for 15 min at 5 °C. The supernatant was denoted as enzymatic raw extract.

The carboxymethylcellulase (CMCase) and filter paper (FPU) activities were determined following IUPAC procedures [15]. To determine CMCase, 0.1 mL of appropriately diluted enzyme (to ensure the initial activity rate) was incubated with 0.9 mL of a suspension containing 4% of carboxymethylcellulose (Sigma-Aldrich, St. Louis, USA). In the case of FPU activity determination, the substrate was 50 mg  $(1 \times 6 \text{ cm strip})$  of Whatman no. 1 filter paper. Carboxymethylcellulase (CMC) were dissolved in 0.1 M acetate buffer, pH 5.0. For filter paper, 0.9 mL buffer and 0.1 mL enzyme extract were used as well. After incubation at 60 °C for 10 min for CMCase and for 60 min for FPU, the amount of total reducing sugars (TRS) released were determined by 3,5-dinitrosalicylic acid (DNS) [16], as further detailed below. Controls were prepared with the enzyme extract being added after the boiling step of the referred methodology, in order to discount TRS possibly present in enzyme extracts prior to the reaction. One unit of enzyme activity (U) was defined as that amount which released 1 µmol of glucose per minute under the reaction conditions, by using glucose standard curves at 540 nm.

β-Glucosidase activity was quantified according to Leite et al. [17] at 45 °C for *T. reesei* and 65 °C for *T. aurantiacus*. The reaction mixture was 50 µL of the enzymatic extract, 250 µL of 100 mM sodium acetate buffer pH 5.0, and 250 µL of 4 mM4-nitrophenyl β-D-glucopyranoside (PNPG, Sigma). After 10 min, the reaction was stopped by the addition of 2 mL of 2 M sodium carbonate. One unit of enzymatic activity was the quantity of enzyme needed to release 1 µmol of *p*-nitrophenol per minute of reaction. A standard curve of *p*-nitrophenol at 410 nm was used.

#### 2.4 Indirect measurement for biomass estimative

According to the Kjeldahl method, indirect measurement of biomass content in the fermented material along cultivation was based on total nitrogen [9]. The total nitrogen content of the fermented material was quantified by Kjeldahl method and then the total protein content was calculated by multiplying the nitrogen content by 6.25. The fungal protein content was obtained by subtracting the total protein content at given time interval from time zero (i.e., immediately after inoculation).

The logistic model of microbial growth was fitted to the estimated data of biomass concentration based on total protein content. Non-linear least square method optimized by Levenberg-Marquardt algorithm was used by the software Origin 6.0 (Microcal Software Inc., Northampton, USA). According to Viccini et al. [18], this model best represents growth in many SSC systems, being given by:

$$\frac{\mathrm{d} X}{\mathrm{d} t} = \mu X \left( 1 - \frac{X}{X_{\mathrm{m}}} \right) \tag{1}$$

where X is the actual biomass concentration;  $X_m$  is the maximum biomass concentration;  $\mu$  is the maximum specific growth rate constant; t is time. In the current paper, X is expressed as mg of estimated fungal biomass per gram of fermented material.

The integrated form of Eq. (1), which was used in the fitting procedure, is:

$$X = \frac{Xm}{1 + \left(\frac{Xm}{X0} - 1\right)e^{-\mu t}}$$
(2)

where  $X_0$  is the initial biomass in the system (for t = 0). The parameters estimated from the experimental data were  $X_{\rm m}$ ,  $X_0$ , and  $\mu$ .

## 2.5 Hydrolysis of SCB

For hydrolysis, SCB fibers were milled to a particle size of 0.84 mm. Saccharification assays were performed with 0.2 g SCB in a thermostatic bath with orbital agitation. Minitab 15.0 (Minitab Inc., State College, USA) was used for generating and further analyzing a Box-Behnken experimental design, with 3 factors (total volume of enzyme, temperature of hydrolysis, and composition of the enzymes cocktail) with 3 levels for each factor (comprising 15 assays, 12 conditions and 3 tests on central point). For all assays, the final volume of the reaction was completed with 10 mL sodium acetate buffer 0.2 mol  $L^{-1}$  at pH 5.0.

The response of the hydrolysis tests was the quantity of total reducing sugars (TRS) released during the reaction. At the central point of experimental design, experiments varying the time of saccharification were also performed by taking independent samples every 4 h up to 24 h, in order to give the kinetics of saccharification under those conditions. Hydrolysis kinetic assays were also performed using 0.2 g SCB and applying 5 mL of the enzymatic extracts produced by *T. aurantiacus* and *T. reesei* at 55 °C, individually and combined (enzyme cocktail), to verify the synergistic effect. The experiments were performed under the same conditions

described above, in order to give the kinetics of saccharification for the enzyme extracts alone and for the cocktail.

The release of TRS was determined according to Miller [16], using glucose as standard. The reaction was performed by adding 1.0 mL of the filtered sample and 1.0 mL of DNS reagent to the test tube and boiling for 10 min. During boiling, the DNS (3,5-dinitrosalicylic acid) reagent, when reacting with reducing sugars present in the medium, changes its initially yellow coloration to brown tones. The color intensity is directly proportional to the concentration of sugars in the medium. The coloring reaction is interrupted when the samples are transferred to an ice bath. 8.0 mL of distilled water was added, after which the absorbance was read at 540 nm. A calibration curve using glucose as a standard was plotted and the results were expressed as mg of reducing sugars/g of sugarcane bagasse.

Quantification of glucose, xylose, and cellobiose was carried out using a Dionex, ICS-5000 high-performance anionexchange chromatography—with pulsed amperometric detection (HPAEC-PAD) (Thermo Scientific, Waltham, USA) with a CarboPac® PA-1 anion-exchange column with compartments at 25 °C and 30 °C, diluents prepared with ultrapure deionized water 18 M $\Omega$  and degassed with N<sub>2</sub>, with a flow of 1 mL min<sup>-1</sup> with solvent A (ultrapure water) and B (500 mmol L<sup>-1</sup> NaOH). Isocratic elution was used for column cleaning from 0 to 12 min with 95.2% A, from 12 to 16 min 100% B was used and from 16 to 30 min 95.2% of A was used to end the process [19]. The results were analyzed and quantified based on standard curves of glucose, xylose, and cellobiose (Sigma-Aldrich, St Louis, USA).

# **3** Results and discussion

# 3.1 $\beta$ -Glucosidase activities and effect of the substrate composition and moisture content

Due to the different metabolisms of each microorganism and the variation in fermentative media, each fungus responded differently to medium stimuli, as a result of their different adaptation. For the thermophilic fungus, the minimum  $\beta$ glucosidase activity (6.8 U/gss) was obtained with SCB:WB 1:1 w/w and 80% moisture content, while the maximum (16.8 U/gss) was found with SCB:WB 9:1 independent of moisture content (Table 1). Statistical analysis based on main effects plots suggested that  $\beta$ -glucosidase activity is significantly affected only by substrate composition. However, ANOVA analysis pointed out statistically significant interaction effects among substrate composition and moisture content in all treatments.

Selection of a proper substrate is another key aspect of SSC. Porous media act both as physical support and as a source of nutrients. However, in addition to supplying

**Table 1**  $\beta$ -Glucosidase activities of the enzymatic extracts obtained from cultivation of thermophilic fungus *T. aurantiacus* CBMAI 756 and of mesophilic fungus *T. reesei* QM9414 on three combinations of substrate composition and moisture content

 $\beta\text{-Glucosidase}$  activities (average value of triplicates)  $\pm$  standard deviations (U/gss)

Thermoascus aurantiacus								
MC	SCB:WB							
(%)	1:1	3:1	9:1	← Average				
70	8.0 (± 1.2)	7.9 (± 1.2)	16.8 (± 0.8)	$10.9 \ (\pm 5.1)^{a}$				
75	$7.0 (\pm 1.0)$	8.9 (± 2.6)	15.9 (± 0.2)	$10.6 (\pm 4.7)^{a}$				
80	6.8 (± 1.0)	12.6 (± 1.1)	15.0 (± 1.2)	$11.5 \ (\pm 4.2)^a$				
Average ↑	$7.3 (\pm 0.6)^{\rm B}$	$9.8 (\pm 2.5)^{B}$	$15.9 (\pm 0.9)^{\rm A}$					
Trichoderma reesei								
MC	SCB:WB							
(%)	1:1	3:1	9:1	$\leftarrow$ Average				
70	$5.0 (\pm 0.1)$	3.8 (± 0.2)	$3.9 (\pm 0.5)$	$4.2 (\pm 0.7)^{b}$				
75	$5.0 (\pm 0.7)$	$4.3 (\pm 0.3)$	$4.2 (\pm 0.3)$	$4.5 \ (\pm 0.4)^{ab}$				
80	$5.4 (\pm 0.3)$	$4.6 (\pm 0.3)$	4.3 (± 0.3)	$4.8 \ (\pm 0.6)^{a}$				
Average ↑	$5.1 \ (\pm \ 0.2)^{\rm A}$	$4.2~(\pm~0.4)^{\rm B}$	$4.1 (\pm 0.2)^{\rm B}$					

Significance level  $\alpha = 0.05$ . Different capital letters at same row indicate significant difference by Tukey test (p < 0.05) due to effect of composition, for average value of activity for each moisture content (MC, % w.b.); different lowercase letters at same column indicate significant difference by Tukey test (p < 0.05) due to effect of MC, for average value of activity for each composition; equal capital letters at same row and equal lowercase letters at same column indicate no significant difference by Tukey test (p < 0.05) due to effects of composition difference by Tukey test (p < 0.05) due to effects of composition difference by Tukey test (p < 0.05) due to effects of composition (for average on MC) and of MC (for average on composition), respectively

nutrients, the appropriate substrate is one that is also capable of inducing the production of the specific target enzyme [6]. Also, it is important to remember that an ideal porous matrix for SSC bioreactors should both fulfill the nutritional microbial needs and provide adequate physical structure for air percolation to guarantee efficient transfer of the respiratory gases and facilitate metabolic heat removal [20].

For the mesophilic fungus *T. reesei*, Table 1 shows minimum  $\beta$ -glucosidase activity (3.8 U/gss) for SCB:WB 3:1 w/w and 70% moisture content, while maximum activity (5.4 U/ gss) was obtained with SCB:WB 1:1 w/w and 80% moisture content. Statistical analysis based on main effects plots suggested that, for *T. reesei*,  $\beta$ -glucosidase activity is significantly affected by both the substrate composition and the moisture content.

Grajek [21] evaluated  $\beta$ -glucosidase activity from the cultivation of *T. aurantiacus* on sugar beet pulp and the author found results similar to the ones in the current paper. Pinto [22] also obtained highest  $\beta$ -glucosidase activity (4.4 U/gss) in the solid cultivation of *T. reesei* on SCB:WB 1:1 w/w with 80% moisture content, although this was quantified after 216 h of cultivation. Casciatori et al. [20] have studied filter paper activity (FPU) of a crude extract produced by same strain of *T. reesei* QM9414 cultivated in SCB:WB 1:1, 3:1, and 9:1 w/w and moisture contents 70, 75, and 80%. The authors found better results for SCB:WB 9:1 and 70% moisture content and attributed such a result to the structural properties of the porous media. These results, when compared to ours, show that the fermentation conditions influence the production of the target enzyme.

As already stated, the use of two fungi with different thermal behaviors aimed at comparing which system (fungus and temperature) enables reaching higher  $\beta$ -glucosidase activities [23]. Enzymatic extracts obtained from the cultivation of T. aurantiacus presented β-glucosidase activities approximately 3 times higher than the activities of the extracts obtained from T. reesei, reiterating that the thermophilic fungus is able to release enzymes which are more thermostable and have higher activities [23, 24]. Grajek [21, 25, 26] determined optimal temperature and pH for cellulase activities of enzymatic extracts obtained from several thermophilic fungi isolated from wood chip piles. T. aurantiacus (Miehe) produced the extracts with highest cellulases activities cultivated on solid media, reiterating the good adaptation of this thermophilic fungus to SSC [21, 22], which is in agreement with the results in the present study.

# 3.2 Correlation between β-glucosidase activities and fungal growth kinetics

Figure 1a shows that, for *T. aurantiacus* cultivated under the previously determined, best conditions, during the phase of fast increase in biomass (exponential phase), there was a simultaneous increase in  $\beta$ -glucosidase activity. When the stationary phase of growth was reached,  $\beta$ -glucosidase activity also became almost constant, which means that enzyme activity production is associated with fungal growth. Logistic equation (Eq. 2), with substitution of X by P and of  $\mu$  by k (here defined as a specific kinetics constant of β-glucosidase production), also fitted well ( $r^2 = 0.95$ ) to the experimental data of β-glucosidase activities over time. This reiterates the similarity between the curves of fungal growth and of enzyme activity kinetics, addressing the enzyme is a growth-associated product. Moreover, the fitted equation may be combined with SSC models and the fitting parameters values  $P_{\text{max}} = 14.1 \text{ U/}$ gss,  $P_0 = 0.23$  U/gss, and k = 0.080 h<sup>-1</sup> can be useful for simulations and predictions of  $\beta$ -glucosidase yields when this cultivation is held at a pilot-scale, for instance.

Many authors reported linear relations between extracellular enzymes and microbial growth in SSC systems. For instance, Palma [27] correlated growth kinetics (estimates based on *N*-acetyl-glucosamine content) and kinetics of xylanase production of *T. aurantiacus*; the author observed association between biomass formation and enzyme production during



**Fig. 1** Fungal growth and  $\beta$ -glucosidase production. **a** *Thermoascus aurantiacus*. **b** *Trichoderma reesei (triangle,*  $\beta$ -glucosidase activity; *broken lines*, fitting of logistic eq. to  $\beta$ -glucosidase; *square*, biomass estimated by protein content (mg); *horizontal line*, fitting of logistic eq. to biomass)

the exponential phase, with enzymatic activity increasing with the increase of biomass, similar to that observed in the current paper. Kalogeris et al. [28] have also reported good correlation between *T. aurantiacus* growth on WB and production of cellulases and xylanase.

Similarly, for *T. reesei* cultivated on the best previously determined substrate composition and moisture content, Fig. 1b also shows simultaneous increases of fungal biomass and  $\beta$ glucosidase activities at early stages of the cultivation. However, in the later stages, fungal biomass reached a constant value before  $\beta$ -glucosidase activities became constant. The logistic equation adapted to  $\beta$ -glucosidase production also fitted well ( $r^2 = 0.97$ ) to the experimental data of  $\beta$ -glucosidase activities over time of cultivation of *T. reesei*, with fitting parameters  $P_{\text{max}} = 0.74$  U/gss,  $P_0 = 0.016$  U/gss, and k = 0.040 h<sup>-1</sup>. In this case, the enzyme was non-growth-associated, but it was continuously produced independently of the stage of growth. Studies on correlation between enzymatic activity and microbial growth are another interesting alternative for evaluating metabolic activity in SSC systems and it enables predicting process yields, mainly when enzymes are the interesting product [29].

Smits et al. [29] reported xylanase production was growthassociated under cultivation of *T. reesei* on WB, agreeing with the findings of the current paper, which supports an interpretation that the type of substrate, moisture, and microorganism can affect the hydrolytic enzyme production. On the above, monitoring fungal growth kinetics in SSC can indicate the stages of production of interesting metabolites from the cultivation, and with this, determine the right time to stop the growth, resulting in cost reduction. Moreover, kinetics parameters of fungal growth and of enzyme production are reliable for application in further modeling and simulation studies aimed at the design and operation of SSC bioreactors.

# 3.3 Saccharification of SCB by applying the raw enzymatic extracts

Prior to the application of the cellulolytic enzymes produced by *T. aurantiacus* CBMAI756 and *T. reesei* QM9414 on SCB saccharification, CMCase, FPU [15] and  $\beta$ -glucosidase [17] activities were determined (Table 2). It is possible to observe that enzymatic activities obtained for the extract produced by the mesophilic fungus were much lower than those obtained for the one produced by the thermophilic fungus under the best cultivation conditions, which is in agreement with De Cassia Pereira et al. [27].

Leite et al. [17], when evaluating the production of  $\beta$ glucosidases by SSC employing the thermophilic fungus *T. aurantiacus* and the mesophilic fungus *Aureobasidium pullulans* on different substrates, had also reported that the thermophilic microorganism provided greater activities in comparison with the mesophilic fungus. The results also confirm that *T. aurantiacus* is well suited to the solid culture process and it is recognized for secreting high levels of cellulolytic enzymes into the medium [12].

The results of enzymatic activities CMCase (140.7 U/gss), FPU (10.1 U/gss), and  $\beta$ -glucosidase (35.7 U/gss) obtained in this study for *T. aurantiacus* are promising when compared with other works in the literature that used fungi of the same

 
 Table 2
 Enzymatic activities of extracts obtained from SSC of Thermoascus aurantiacus CBMAI756 and Trichoderma reesei QM9414

Fungus	Enzymatic a	(gss)	
	CMCase	FPU	β- Glucosidase
Thermoascus aurantiacus Trichoderma reesei	140.7 73.7	10.1 5.8	35.7 4.1

genus to produce enzymes on different substrates, in which CMCases and  $\beta$ -glucosidase activities ranged from 53.2 to 1709.0 U/gss and 8.9 to 105.0 U/gss, respectively [17, 28, 30].

Similarly, the results of activities obtained for the extract produced by the fungus *T. reesei* by solid cultivation, CMCase (73.7 U/gss), FPU (5.8 U/gss) and  $\beta$ -glucosidase (4.1 U/gss), are comparable to others found in the literature, considering that the results of the present study were similar to those reported by several authors for enzyme production, using fungi of the same genus on solid substrates, in which CMCase, FPU and  $\beta$ -glucosidase activities varied from 5.7 to 55.7 U/gss; 4.0 to 7.7 U/gss and 5.0 to 11.2 U/gss, respectively [31, 32].

Agreeing with our results, *T. reesei* is recognized for its remarkable ability to secrete a pool of saccharifying enzymes, although it has a deficiency in the production of  $\beta$ -glucosidases [10]. This deficiency in the expression of the  $\beta$ -glucosidase enzyme by the fungus *T. reesei* results in the accumulation of cellobiose, which inhibits the action of cellobiohydrolases and endoglucanases, decreasing the rate of hydrolysis [33]. Therefore, for the effective application in enzymatic saccharification of SCB, supplementation of the enzyme extract produced by *T. reesei* with  $\beta$ -glucosidase is necessary, in order to increase the conversion efficiency of cellulose to glucose [10].

Yields of total reducing sugars (TRS) released in the saccharification of SCB by applying the raw enzymatic extracts for 24 h, expressed as mg of TRS per gram of SCB, are presented in Table 3. It is possible to observe that the best result (approximately 124 mg TRS/g SCB) was obtained when applying 9 mL of the enzymes cocktail composed by equal parts of extracts from the cultivation of *T. aurantiacus* and *T. reesei* at 65 °C. This dosage is equivalent to an enzyme load of 3.6 FPU/g<sub>SCB</sub>, 2.25 FPU/g<sub>SCB</sub> provided by extract from *T. aurantiacus* and 1.35 FPU/ $g_{SCB}$  by extract from *T. reesei*.

Perrone et al. [19] performed hydrolysis using the commercial enzyme Prozyn® (São Paulo, Brazil), with a cellulase dosage of 32 FPU per gram of bagasse (dry basis) in sugarcane bagasse without pretreatment, and obtained 15 mg/g glucose, which corresponds to a glucose yield of 3%. Moretti et al. [34] performed hydrolysis by applying enzymes produced by the fungus *Myceliophthora thermophila* M.7.7. by solid culture and also the commercial enzyme Celluclast 1.5 L (Novozymes®) in untreated sugarcane bagasse (control). The authors reported that 17.9 mg/g and 27.5 mg/g, respectively, were obtained, corresponding to yields of 3 and 3.1%. Therefore, the results obtained in the present work are promising when compared to those reported in the literature for enzymatic hydrolysis of untreated sugarcane bagasse.

Statistical analysis of the Box-Behnken design pointed out a significant influence of the quadratic term of volume of enzymes. One may also observe that when the enzymatic extract produced from the cultivation of *T. aurantiacus* is applied (*T. aurantiacus/T. reesei* 1:0 v/v), TRS increase as temperature increases, since the enzymes from this thermophilic fungus do not act well at 45 °C, reducing the efficiency of the hydrolysis. On the other hand, when the enzymatic extract produced from the cultivation of *T. reesei* is applied (*T. aurantiacus/T. reesei* 0:1 v/v), TRS decrease as temperature increases, due to the start of thermal denaturation of the enzymes from the mesophilic strain at 65 °C. Such observations are reflected by a near-significant (p = 0.097) effect of interaction between hydrolysis temperature and composition of the enzymes cocktail.

Cellulase preparations from *T. reesei* usually have to be supplemented with  $\beta$ -glucosidase from other sources for

Table 3TRS released fromenzymatic hydrolysis of SCB(Box-Behnken experimentaldesign)

Test	Volume of enzyme extract (mL)	T (°C)	Composition <i>Thermoascus aurantiacus/</i> <i>Trichoderma reesei</i> (v/v)	TRS released (mg/g SCB)
1	1 (-1)	45 (-1)	1:1 (0)	39.77
2	9 (+1)	45 (-1)	1:1 (0)	27.78
3	1 (-1)	65 (+1)	1:1 (0)	47.62
4	9 (+1)	65 (+1)	1:1 (0)	123.66
5	1 (-1)	55 (0)	0:1 (-1)	26.76
6	9 (+1)	55 (0)	0:1 (-1)	32.76
7	1 (-1)	55 (0)	1:0 (+ 1)	38.92
8	9 (+1)	55 (0)	1:0 (+ 1)	32.60
9	5 (0)	45 (-1)	0:1 (-1)	78.70
10	5 (0)	65 (+1)	0:1 (-1)	28.38
11	5 (0)	45 (-1)	1:0 (+ 1)	64.96
12	5 (0)	65 (+1)	1:0 (+ 1)	105.21
13	5 (0)	55 (0)	1:1 (0)	82.11
14	5 (0)	55 (0)	1:1 (0)	82.21
15	5 (0)	55 (0)	1:1 (0)	85.57

cellulose saccharification on an industrial scale [35]. In this context, tests with *T. aurantiacus/T. reesei* 1:1 v/v at 65 °C may have released more TRS due to the synergistic effect between exo and endoglucanases from *T. reesei* and  $\beta$ -glucosidase from *T. aurantiacus*, since the extract from the thermophilic fungus presents high  $\beta$ -glucosidase activity at 65 °C, resulting in a near-significant effect of quadratic term of composition of the cocktail (p = 0.137).

T. reesei is known to produce at least two exoglucanases (CBHI and CBHII), five endoglucanases (EGI, EGII, EGIII, EGIV, and EGV), and two  $\beta$ -glucosidases (BGLI and BGLII) [36]. CBHI and CBHII and EGI and EGII are produced in an approximate proportion of 6:2:1:1 (w/w), i.e., endoglucanases represent only 20% of the cellulase system produced by T. reesei. However, exo and endoglucanases comprise 90% of the system, while  $\beta$ -glucosidases secreted by this fungus represent less than 1% of the cellulolytic extract produced. Once cellobiose-the major product of CBHI and CHBII activity—inhibits the activity of the CBHs and EGs [36] and T. reesei produces  $\beta$ -glucosidases at low levels, cellulase preparations from T. reesei usually have to be supplemented with  $\beta$ -glucosidase from other sources for cellulose saccharification on industrial scale [35, 36]. In this context, tests with T. aurantiacus/T. reesei 1:1 v/v at 65 °C have released more TRS probably due to the synergistic effect between CBHs and EGs from T. reesei and  $\beta$ -glucosidase from T. aurantiacus, since the extract from the thermophilic fungus presented high  $\beta$ -glucosidase activity at this temperature, as also reported by Leite et al. [17] and to a near-significant influence of the quadratic term of composition of the enzymes cocktail (p =0.137). This increase in hydrolysis seen with this enzymatic cocktail could also be partially due to the presence in of oxidative enzymes of the GH61 family, which have recently been shown [37, 38] to play a key role in the cellulosic biomass hydrolysis (not accessed in this work).

By anion-exchange chromatography, it has been possible to evaluate the sugar content of the hydrolysates of SCB using isolated extracts of T. aurantiacus and of T. reesei or by a mixture of them in a cocktail (Fig. 2). Xylose content did not differ significantly between the hydrolysates, while glucose content was significantly higher in the hydrolysate resulting from the application of the cocktail. An increase of approximately 20% in the amount of glucose was achieved if the cocktail is compared with the extract from T. aurantiacus alone, while glucose concentration increases around 100% when the cocktail is compared to the extract from T. reesei alone. Comparing the application of the extract from T. aurantiacus alone with the one from T. reesei alone, as well as the glucose content being 75% higher in the hydrolysate using enzymes of the thermophilic fungus, the cellobiose content (dimers which were not converted into glucose) draws attention. In the hydrolysate using enzymes from T. reesei, the concentration of cellobiose exceeds the glucose



**Fig. 2** Sugar contents (HPAEC-PAD) in hydrolysates of SCB by isolate and mixed extracts, 5 mL of enzyme, 24 h, 55 °C; (*grayscale rectangle*) cellobiose; (*black rectangle*) glucose; (*white rectangle*) xylose. For *T. aurantiacus*, hydrolysis with 12.5 FPU/g<sub>SCB</sub> at 65 °C; for *T. reesei*, 7.5 FPU/g<sub>SCB</sub> at 45 °C; for cocktail, 3.6 FPU/g<sub>SCB</sub> at 65 °C

concentration by around 50%. This is a consequence of the  $\beta$ -glucosidase deficiency of the extract from the mesophilic fungus. Cellobiose is a disaccharide considered a cellulase inhibitor [10], leading to incomplete hydrolysis of the cellulose. As already mentioned, *T. reesei* is reported to be deficient in synthetizing  $\beta$ -glucosidases [10], which are the enzymes responsible for cleaving cellobiose residues into glucose. As that extract contains a small amount of these enzymes, cellobiose accumulates in the reaction medium, impairing the overall efficiency of the enzymatic hydrolysis process.

With the objective of verifying the synergistic effect between the enzymes contained in the pool secreted by each fungus in SSC, at the central point (5 mL, 1:1 and 55 °C), experiments varying time of saccharification were performed by taking independent samples every 4 h over 24 h for determination of the hydrolysis kinetic of SCB. It is observed that TRS released increases over time (Fig. 3a).

For every analysis time, higher efficiency of hydrolysis was obtained when applying the enzymatic cocktail (Fig. 3a). Concerning the individual extracts, the one produced by T. reesei was more efficient than the one produced by T. aurantiacus up to 4 h but then it was overtaken by the extract produced by the thermophilic fungus and even more so by the enzymatic cocktail. This suggests a partial denaturation of some enzymes secreted by the mesophilic fungus is likely over increasing time of exposure at 55 °C. The cocktail of extracts produced by fungi with different thermal preferences and its application at an intermediate temperature achieved a synergistic effect between the enzymes secreted by both fungi, resulting in an improvement in the efficiency of the saccharification of SCB. Concerning the hydrolysis kinetics, similar trends have been reported by Bi et al. [39].



According to Lopes et al. [40], mixtures of varied enzymes from different sources usually lead to an increase in hydrolysis rate. This was observed in the present work, which showed a 26% increase compared to *T. aurantiacus* and 59% to *T. reesei* when the enzymatic cocktail was applied. Braga et al. [41] supplemented a commercial preparation (Celluclast 1.5 L; Novozymes) with 30% of the crude extract from *Aspergillus oryzae* P21C3, a good producer of xylanase and feruloylesterases, resulting in an enhancement of 36% in the conversion of cellulose from pretreated sugarcane bagasse.

Arias et al. [42] in the enzymatic breakdown of sugarcane bagasse by crude extracts from Trichoderma harzianum, Penicillium funiculosum, and A. niger obtained 42, 66, and 1%, respectively. On the other hand, the optimized cocktail comprising 50% of the crude extract from P. funiculosum, and 35 and 15% of the crude extracts from A. niger and T. harzianum, respectively, showed a hydrolysis yield of sugarcane bagasse of 91%, confirming the synergism of enzymes in the hydrolysis. In another study, an optimized enzymatic cocktail developed to hydrolyze sugarcane bagasse, comprising 80% T. reesei fraction, 10% endoglucanase (recombinant enzyme from Bacillus subtilis), and 10% BGL (from A. niger), converted 72% of cellulose present in hydrothermally pretreated bagasse [43]. The lower conversions achieved in the current work are very likely related to the use of untreated sugarcane bagasse with lower enzymatic loads.

The local derivatives of the experimental curve of TRS as a function of time gave the rate of TRS release (Fig. 3b). From 8 h of hydrolysis on, the rate of reaction decreases and remains almost constant, likely due to both partial thermal denaturation of the enzymes and gradual reduction of substrate concentration.

Kaschuk et al. [5] studied the production of reducing sugars obtained from the enzymatic hydrolysis of sisal pulp, microcrystalline cellulose and filter paper using cellulases from *Aspergillus* sp. CBMAI 1198. The authors reported that for microcrystalline cellulose and sisal pulp, the amounts of reducing sugars produced were close, and a large increase in the production was observed up to 10 h, followed by a deceleration up to 48 h. However, for the enzymatic hydrolysis of the filter paper, higher amounts of reducing sugars were produced from the beginning of the reaction until 23 h, when a deceleration was observed. This deceleration observed has already been reported in other studies, and may be attributed to changes in the substrates or related to the increase in reaction products (glucose and oligosaccharides) that can inhibit the enzyme cellulases in the reaction medium [5].

An exponential decay curve was fitted to the experimental points, resulting in the following Eq. (3):

$$\frac{\mathrm{d}(\mathrm{TRS})}{\mathrm{dt}} = \frac{\mathrm{d}(\mathrm{TRS})}{\mathrm{dt}}\Big|_{0} + \mathrm{A} \,\mathrm{e}^{-\mathrm{t/n}} \qquad \frac{\mathrm{d}(\mathrm{TRS})}{\mathrm{dt}}$$
$$= \frac{\mathrm{d}(\mathrm{TRS})}{\mathrm{dt}}\Big|_{0} + \mathrm{A}\mathrm{e}^{-\mathrm{t/n}} \qquad (3)$$

where  $d(TRS)/dt|_0$  is the initial reaction rate; A is a preexponential factor and 1/n is a constant on the exponential argument.

The parameters for the fitting of exponential decay to the hydrolysis kinetics were:  $d(TRS)/dt|_0 = 1.07$ ; A = 3.85 and n = 5.34 ( $r^2 = 0.86$ ) for *T. aurantiacus;*  $d(TRS)/dt|_0 = -3.87$ ; A = 8.89 and n = 15.76 ( $r^2 = 0.86$ ) for *T. reesei;*  $d(TRS)/dt|_0 = 1.67$ ; A = 5.95 and n = 4.61 ( $r^2 = 0.94$ ) for the enzymatic cocktail.

The parameters of the fitting of exponential decay to hydrolysis kinetics are useful parameters for design and optimization of the hydrolysis operation in terms of its extension to bioreactor use, as well as for simulation of the process.

Based on the saccharification results, applying combined raw enzymatic extracts of *T. aurantiacus* and *T. reesei* for enzymatic hydrolysis of SCB is very interesting in the production of ethanol 2G, since a reasonably acceptable level of TRS is released, which can then be used for yeast fermentation.

# 4 Conclusions

The enzymatic extract produced by T. aurantiacus presents higher β-glucosidase, CMCase and filter paper activities than the one produced by T. reesei, hence it can be said the thermophilic fungus is better suited to the SSC process. Total protein content quantification enabled the estimation of fungal biomass data and fitting the logistic model to describe the growth. For both fungi, comparing kinetics of estimated fungal growth and of  $\beta$ -glucosidase activity, *T. aurantiacus* shows a growth-associated production and T. reesei shows an enzyme production independent of stage. Optimal saccharification of SCB was achieved by using 9 mL of an enzymatic cocktail composed of equal volumes of both fungal extracts, totaling 3.6 FPU/g<sub>SCB</sub>, at 65 °C. Once higher efficiency of hydrolysis was obtained for the application of the enzymatic cocktail with lower enzyme load, a synergy between enzymes from both extracts is addressed. The major contributions of this work are twofold: hydrolytic enzyme production is related to fungal growth, so it can express process kinetics; and a lowcost in-house produced enzymatic cocktail, using a combination of T. reesei and T. aurantiacus enzymes, is effective for lignocellulose saccharification at a high temperature and with low enzyme load.

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## Compliance with ethical standards

**Conflict of interest** The authors declare that they have no conflict of interest.

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