**ORIGINAL ARTICLE** 



# Enhanced enzymatic hydrolysis of corncob by ultrasound-assisted soaking in aqueous ammonia pretreatment

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## Abstract

Ultrasound-assisted soaking in aqueous ammonia (USAA) pretreatment with 15 wt% aqueous ammonia under low temperature (~60 °C) and short-time (<12 min) low-frequency (20 kHz, 60–650 W) ultrasound has been investigated for enhancement of enzymatic hydrolysis of corncob. Operational parameters of energy density (2.93–17.07 W/mL) and sonication time (0.34–11.66 min) that affect cellulose recovery, delignification, and sugar recovery yield were studied and optimized. The maximum cellulose recovery, delignification and sugar recovery yield determined at the optimum conditions (energy density 10 W/mL, sonication time 11.66 min) were 83.8, 84.7, and 77.6%, respectively. The corncob pretreated using USAA has a lower hemicellulose content (28.9% vs 31.8%), a slightly lower crystallinity index value (42.7% vs 43.7%), and a larger surface cavity diameter (> 36  $\mu$ m vs < 20  $\mu$ m) than that pretreated using soaking in aqueous ammonia (SAA) pretreatment. The USAA pretreatment was proved to be a reliable and effective method for corncob pretreatment.

Keywords Corncob  $\cdot$  Ultrasound  $\cdot$  Enzymatic hydrolysis  $\cdot$  SAA  $\cdot$  USAA

## Introduction

Lignocellulose, a renewable resource alternative to fossil resources, can produce second-generation bioethanol and commodity chemicals simultaneously, and has potential to resolve the food, energy, and environment trilemma (Tilman et al. 2009). Corncob has been recognized as a promising lignocellulosic feedstock for bioethanol production because of its wide distribution, high bulk density, and high collection and transport convenience (Liu et al. 2010). On the basis of these advantages, several energy companies, such as POET, DDCE, and ABENGOA, have chosen corncob as the

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<sup>3</sup> Collaborative Innovation Center of Chemical Science and Engineering (Tianjin), Tianjin 300072, China major raw material for bioethanol production. However, the lignocellulosic material has a supramolecular matrix composed of cellulose, hemicellulose, and lignin, and its noncellulosic element is a recalcitrant block of lignocellulosic biodegradation. To break this block, pretreatment is necessary. For corncob, many pretreatment methods have been evaluated: dilute acid (Wang et al. 2011; Kahar et al. 2010), sulphite (Cheng et al. 2011), oxalic acid (Lee et al. 2009, 2010), formic acid (Huang et al. 2010; Zhang et al. 2010), and soaking in aqueous ammonia (Du et al. 2012, 2013). Among these methods, soaking in aqueous ammonia (SAA) is superior to the others because of its ability to effectively remove lignin and retain major cellulose and hemicellulose fractions (Kim et al. 2008).

However, our previous research (Du et al. 2012, 2013) has found that SAA method has an underdone delignification (57.3–61.8%) and has no destructive effect on the surface of lignocellulosic materials but swelling. Therefore, there is a need for further improvement of this method to obtain higher delignification and more cracked surface; and hence, ultrasound was integrated with SAA methods. Recently, Xu et al. (2017) has studied ultrasound-assisted aqueous ammonia pretreatment (USAA) for intensification of enzyme hydrolysis for corn cob, whereas with dilute aqueous ammonia concentration of 1.0–4.0 wt%, low solid content of 0.5 g



dry basis/25 mL buffer and long ultrasonic time of 1–4 h. In this study, corncob was used as a feedstock, which has a lignin content close to 20%. The ultrasound-assisted soaking in aqueous ammonia (USAA) pretreatment with 15 wt% aqueous ammonia under low temperature (~60 °C) and short-time (<12 min) low-frequency (20 kHz, 60–650 W) ultrasound has been investigated for enhancement of enzymatic hydrolysis of corncob. Furthermore, it is hoped that acoustic cavitation will facilitate subsequent high-solid enzymatic hydrolysis.

## Materials and methods

#### **Materials**

Corncob (glucan, 34.8%; xylan, 30.3%; lignin, 21.6%) was collected from a farm in Tianjin, China. It was washed with distilled water and air-dried to remove the moisture present. The dried corncob was milled and screened to 20–80 mesh. Cellulase (GC220, 160 FPU/mL) derived from *Trichoderma reesei* was provided by Genencor International (Palo Alto, CA, USA).

## Sonicator

Scientz-IID amplifier (20 kHz, 0–950 W, Scientz Biotechnology Co., Ltd., Ningbo, China) with a  $\Phi$ 6 horn (tip diameter 6 mm, 20 kHz, 60–650 W) was used in this study. The ultrasonic pulse was maintained at 50% (2 s/2 s) and the temperature was controlled using a water bath.

#### Pretreatment of corncob

#### SAA pretreatment

Corncob was treated with 15 wt% aqueous ammonia in a screw-capped bottle at 60 °C for 12 h. Solid-to-liquid (S/L) ratios were 1:6. After pretreatment, the solids (SAA-treated corncob, SAACC) were separated from the liquid by filtration under vacuum and washed with deionized water until the pH reached 7.0. The residue obtained was oven dried until constant weight was observed, and then, it was subjected to enzymatic hydrolysis.

#### **USAA** pretreatment

Corncob was treated with 15 wt% aqueous ammonia and a 20 kHz sonicator in a screw-capped bottle at 60 °C for 12 h. The S/L ratios were 1:6. The horn was inserted approximately 1 cm under the surface of the sample solution. After pretreatment, the solids (USAA treated corncob, USAACC) were separated from the liquid by filtration under vacuum



and washed with deionized water until the pH of the filtrate reached neutral condition. The residue obtained was oven dried until constant weight was observed, and then, it was subjected to enzymatic hydrolysis. The % cellulose recovery in the solid content was calculated using the following equation (Ramadoss and Muthukumar 2014):

% cellulose recovery = 
$$\left(\frac{C_{PT-CC}}{C_{CC}}\right) \times 100,$$
 (1)

where  $C_{\rm CC}$  is the amount of cellulose in native corncob and  $C_{\rm PT-CC}$  is the amount of cellulose in pretreated corncob measured in (g/g).

The % delignification was calculated using the following equation (Ramadoss and Muthukumar 2014):

% delignification = 
$$\left(\frac{L_{CC} - L_{PT-CC}}{L_{CC}}\right) \times 100,$$
 (2)

where  $L_{\text{CC}}$  is the amount of lignin present in native corncob and  $L_{\text{PT-CC}}$  is the amount of lignin in pretreated corncob measured in (g/g).

#### **Response surface methodology**

To achieve high enzymatic digestibility after USAA pretreatment, ultrasonic parameters were optimized by the two factors, three levels central-composite design (CCD). The matrix corresponding to the CCD is presented in Table 1. Thirteen experiments were carried out with two variables and each variable varied at three levels for sugar recovery

Table 1 Two factors, three levels central-composite design (CCD) with experimental responses of sugar recovery yields  $(Y_S, \%)$ 

| Run | Parameters                |           |                                 |           | $Y_{\rm S}(\%)$ |
|-----|---------------------------|-----------|---------------------------------|-----------|-----------------|
|     | A (energy density, W/ mL) |           | <i>B</i> (sonication time, min) |           |                 |
| 8   | 2.93                      | (- 1.414) | 6.00                            | (0)       | 59.09           |
| 9   | 5.00                      | (-1)      | 2.00                            | (-1)      | 60.53           |
| 1   | 15.00                     | (1)       | 2.00                            | (-1)      | 66.66           |
| 7   | 10.00                     | (0)       | 11.66                           | (1.414)   | 77.60           |
| 2   | 10.00                     | (0)       | 6.00                            | (0)       | 73.39           |
| 4   | 10.00                     | (0)       | 6.00                            | (0)       | 73.59           |
| 6   | 10.00                     | (0)       | 6.00                            | (0)       | 73.26           |
| 5   | 10.00                     | (0)       | 0.34                            | (- 1.414) | 58.24           |
| 11  | 10.00                     | (0)       | 6.00                            | (0)       | 73.55           |
| 3   | 17.07                     | (1.414)   | 6.00                            | (0)       | 67.47           |
| 12  | 5.00                      | (-1)      | 10.00                           | (1)       | 64.85           |
| 13  | 10.00                     | (0)       | 6.00                            | (0)       | 73.56           |
| 10  | 15.00                     | (1)       | 10.00                           | (1)       | 69.43           |

yields. The sugar recovery yield ( $Y_S$ ) was calculated according to the following equation (Yoo et al. 2013):

pretreatment were characterized by an S-4800 field emission SEM (Hitachi High-Technologies Co., Japan) at an accel-

$$Y_{S}(\%) = \frac{\left\{ \left[ R_{glucan}(g) \times D_{glucan}(\%) \right] + \left[ R_{xylan}(g) \times D_{xylan}(\%) \right] \right\} \times S.R.}{\left[ C_{glucan} + C_{xylan} \right](g)} \times 100, \tag{3}$$

where  $R_{glucan}$  ( $R_{xylan}$ ) is the glucan (xylan) remaining after USAA pretreatment measured in (g),  $D_{glucan}$  ( $D_{xylan}$ ) is the enzymatic digestibility of glucan (xylan) measured in (%), and  $C_{glucan}$  ( $C_{xylan}$ ) is the glucan (xylan) content in untreated corncob measured in (g). A second-order polynomial model fitted for the sugar recovery yield (Y) was shown in the following equation (Yoo et al. 2013):

$$Y_{S} = \alpha_{0} + \alpha_{1}A + \alpha_{2}B + \alpha_{11}A^{2} + \alpha_{22}B^{2} + \alpha_{12}AB,$$
(4)

where *A* and *B* are the coded independent variables, and  $\alpha_0$ ,  $\alpha_1$ ,  $\alpha_2$ ,  $\alpha_{11}$ ,  $\alpha_{22}$ , and  $\alpha_{12}$  are regression coefficients for the intercept, linear, quadratic, and interaction effects, respectively. The statistical analysis of the data was performed using Design-Expert software (version 8.0.5b, Stat-Ease, Inc., Minneapolis, USA).

## **Enzymatic hydrolysis**

The enzymatic hydrolysis test was performed to evaluate the pretreatment effectiveness. 1 g of untreated or pretreated corncob sample was added to an Erlenmeyer flask containing 10 mL of 50 mM citric acid-NaOH buffer with a pH value of 4.8, 0.065 mL of GC220 (30 FPU/g glucan), which was then incubated in a shaking water bath at 50 °C and 120 rpm for 24 h. The initial glucan concentration was 10% (w/v) based on 100 mL of total liquid and solid. After enzymatic hydrolysis, the hydrolysates were immediately boiled for 10 min to denature the enzymes and then filtered. The supernatants were taken for fermentable sugar analysis using HPLC.

The glucan and xylan digestibilities were calculated as follows (Yoo et al. 2013):

$$D_{glucan} = \frac{Total \ release \ glucose(g) \times 0.9}{Initial \ glucan \ loading(g)} \times 100$$
(5)

(0.9 is the conversion factors of glucose to equivalent glucan)

$$D_{xylan} = \frac{Total \ release \ xylose(g) \times 0.88}{Initial \ xylan \ loading(g)} \times 100 \tag{6}$$

(0.88 is the conversion factors of xylose to equivalent xylan).

## **Analytical methods**

Carbohydrates and lignin contents in the corncob samples were determined according to the NREL procedures LAP 002. The morphologies of corncob samples before and after eration voltage of 5 kV. Before SEM imaging, the samples were platinum sputter coated without critical point drying. X-ray diffraction (XRD) patterns of corncob samples were measured by an X'Pert Pro X-ray diffractometer (PANalytical Ltd., Holland) with a CoK $\alpha$  radiation of 1.789 Å (30 kV, 30 mA) and a scan rate of 12° min<sup>-1</sup> from  $2\theta$ = 3 – 50 deg. The crystallinity index (CrI) defined as the percentage of crystalline material in corncob was calculated using the Segal method as follows (Wu et al. 2017):

$$CrI = \frac{I_{002} - I_{\rm am}}{I_{002}} \times 100,\tag{7}$$

where  $I_{002}$  is the peak intensity with respect to the (002) lattice plane and  $I_{am}$  is the peak intensity with regard to amorphous zone diffraction intensity of  $2\theta \approx 18.8^{\circ}$ .

## **Results and discussion**

## **Composition of corncob**

The composition of raw corncob was found to be  $34.7 \pm 0.3\%$  cellulose,  $31.3 \pm 0.2\%$  hemicellulose,  $19.0 \pm 0.1\%$  lignin,  $1.3 \pm 0.3\%$  ash, and  $13.7 \pm 0.3\%$  others (extractable non-carbohydrates). The hemicellulose part was found to consist of 92% xylan and 8% arabinan and the lignin part was found to consist of 89% Klason lignin and 11% acid soluble lignin. Carbohydrates present in corncob accounted for about 66% of the dried material and this indicates the suitability of corncob as a very promising substrate.

#### Pretreatment

Corncob was pretreated with two different methods and the composition data obtained are presented in Table 2. SAA pretreatment method produced 73.6 g dry weight per 100 g corncob and showed 96.3% cellulose recovery. The hemicellulose and lignin elimination ratio obtained was 25.2 and 68.2%, respectively. USAA pretreatment showed a yield of 72.3 g dry weight per 100 g corncob. The cellulose recovery obtained was 83.8%, whereas hemicellulose and lignin removal were 33.2 and 84.7%, respectively (Fig. 1). The hemicellulose and lignin content in native corncob was 31.3 and 19.0%, respectively, and after the USAA pretreatment, the amount was reduced to 28.9 and 4.03%, respectively. This is due to the synergistic effect of ammonia and hydroxyl



 Table 2
 Chemical composition

 of CC before and after
 pretreatment

| Constituents (wt%)         | Native CC (%) <sup>a</sup> | SAA-treated CC <sup>a</sup> | USAA-treated CC  |  |
|----------------------------|----------------------------|-----------------------------|------------------|--|
| S.R. <sup>b</sup>          | 100                        | 73.6                        | 72.3             |  |
| Cellulose                  | $34.7 \pm 0.3\%$           | $45.4 \pm 0.1\%$            | $40.2 \pm 0.2\%$ |  |
| Hemicellulose <sup>c</sup> | $31.3 \pm 0.2\%$           | $31.8 \pm 0.3\%$            | $28.9 \pm 0.3\%$ |  |
| Lignin <sup>d</sup>        | $19.0 \pm 0.1\%$           | $8.2 \pm 0.2\%$             | $4.03 \pm 0.1\%$ |  |
| Ash                        | $1.3 \pm 0.3\%$            | $1.1 \pm 0.1\%$             | $0.9 \pm 0.1\%$  |  |
| Others                     | $13.7 \pm 0.3\%$           | NA                          | NA               |  |

Data in the table are based on the oven-dry untreated biomass. Values are expressed as mean and standard deviation

<sup>a</sup>The data are from our previous work (Du et al. 2013)

<sup>b</sup>S.R. stands for solid remaining (wt%) after pretreatment

<sup>c</sup>Xylan and arabinan

<sup>d</sup>Klason lignin and acid soluble lignin



**Fig. 1** Performance analysis of different pretreatment methods: SAA pretreatment (15 wt%, 12 h, 6:1 mL/g, 60 °C) and USAA pretreatment (15 wt%, 12 h, 6:1 mL/g, 60 °C, 10 W/mL, 8 min)

radicals formed during the cavitation which enhanced the depolymerization of lignin and cleavage of lignin–hemicellulose linkages (Ramadoss and Muthukumar 2014). Hence, the dry weight of USAA pretreated corncob was decreased. The USAA pretreatment gave 31.8% more removal of hemicellulose and 24.1% more removal of lignin compared to SAA pretreatment, respectively.

#### RSM study

The RSM experiments were used to optimize the USAA pretreatment conditions and performed with S/L ratio of 1:6 and 15 wt% aqueous ammonia. The sugar recovery yield ( $Y_S$ ) was calculated and used due to its combination of carbohydrate remaining and enzymatic digestibility (see Eqs. (3)–(6)) (Yoo et al. 2013). The responses of sugar recovery yield were subjected to ANOVA analysis. The



second-order polynomial equation, describing the sugar recovery yield  $(Y_S)$  as a simultaneous function of energy density and sonication time of USAA pretreatment, is shown below:

$$Y_S = 73.47 + 2.82A + 4.31B - 5.15A^2 - 2.83B^2 - 0.39AB.$$
(8)

Values of p for A, B,  $A^2$ , and  $B^2$  less than 0.05 indicated that these coefficients can significantly affect sugar recovery yield, and for AB greater than 0.1000 indicated that this coefficient cannot significantly affect sugar recovery yield. The F value of 11.63 implies the model is significant. The determination coefficient ( $R^2 = 0.9991$ ) indicated that 99.91% of the variability in the response could be explained by the model. The 3D response surface for sugar recovery yield is shown in Fig. 2. The optimization of energy density and sonication time of USAA treatments to achieve maximum sugar recovery yield was carried out in the range of experimental runs using the Design-Expert software. The maximum sugar recovery yield and optimal conditions were also determined as 77.6% with 10 W/mL energy density, 11.66 min sonication time, 15 wt% NH4OH, 1:6 S/L ratio, and 60 °C reaction temperature.

#### Morphologies of corncob

The morphological changes induced by pretreatment were imaged by SEM to obtain insight into the principle of different pretreatment method, and the results are shown in Fig. 3. The image of CC shows that it has a relatively smooth and continuous surface, while those of the pretreated corncob samples exhibit an ablated and collapsed surface containing large quantities of cellular structures, indicating that both two pretreatment methods (SAA and USAA) have modified the structure of corncob to some degree. The broken surface and cellular structures can be attributed to the collective effect of  $NH_4OH$  and







Fig. 3 SEM images of CC (a), SAACC (b), USAACC-6 (c), USAACC-8 (d), and USAACC-10 (e)

ultrasound. Kim et al. (2008) previously reported that ammonia could effectively remove lignin from biomass and swell the substrate. At the same time, the SAA at low temperature (~ 60 °C) has been proved which can effectively retain the hemicellulose in the solids (Rollin et al. 2011). As Wu et al. (2017) and Su et al. (2017) pointed out, ultrasonication as well as the resulting shear forces, shock waves, and microjets can split the interior and surface of corncob. Moreover, cavitation as well as the consequent highly reactive hydroxyl radicals can attack the lignocellulosic cell wall constituents at close proximity, resulting in collapse of the lignocellulose matrix, interrupt of cellulose chains, and modification of lignin network. It can be seen that cavity diameter  $(36.1-42.0 \ \mu\text{m})$  of the outer surface of the USAA pretreated corncob samples were dramatically







**Fig.4** X-ray crystallography of CC (a), SAACC (b), USAACC-6 (c), USAACC-8 (d), and USAACC-10 (e)

amplified, indicating that the ultrasonication intensified the swelling effect of SAA pretreatment.

## **Crystallinity of corncob**

Crystallinity of lignocellulosic substrate has been recognized as one of the major properties determining hydrolysis rate (Bansal et al. 2010; Shirkavand et al. 2016). In general, the amorphous fraction of lignocellulosic substrate is related to hemicellulose and lignin, and cellulose is almost considered crystalline. In this work, the effect of pretreatment on the cellulose crystallinity of corncob was investigated through XRD analysis, and the results are shown in Fig. 4. The major diffraction peak corresponding to the cellulose crystalline plane (002) was obtained for  $2\theta$  ranging between 21.8° and 27.5°, and the smaller peak corresponding to the amorphous zone (101) was obtained for  $2\theta = 18.8^{\circ}$ . It can be observed that the pretreated corncob samples have higher (002) plane. According to the Segal method, the calculated crystallinity index values are 34.6, 43.7, 42.7, 42.3, and 42.1% for corncob, SAACC, USAACC-6, USAACC-8, and USAACC-10, respectively. It can be seen that the SAA and USAA pretreatment distinctly increases the crystallinity index of corncob. Based on the above composition and SEM analyses, it can be concluded that the change in the crystallinity index is largely due to the increase of cellulose content (Chundawat et al. 2011). USAACC-6, USAACC-8, and USAACC-10 have a slightly lower crystallinity index value than SAACC, indicating that the ultrasound-assisted soaking in aqueous ammonia pretreatment may have a better efficiency in decreasing the crystallinity of corncob.

Conclusions

In this study, corncob was pretreated using USAA method for the fermentable sugar production. The maximum cellulose recovery (83.8%), delignification (84.7%), and sugar recovery yield (77.6%) were obtained at the optimum conditions of energy density 10 W/mL and sonication time 11.66 min. The composition analysis shows that the USAA pretreatment could selectively remove lignin and hemicellulose without degrading cellulose. XRD analysis confirmed the slightly reduction in cellulose crystallinity by USAA and SEM analysis confirmed the dramatic amplification of surface cavity diameter, which is beneficial to fermentable sugar production. The results of this study concluded that USAA was a reliable and effective method for corncob pretreatment.

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## **Compliance with ethical standards**

**Conflict of interests** The authors declare that they have no conflict of interests.

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