



Synthesis of CuAl-layered double hydroxide/MgO₂ nanocomposite catalyst for the degradation of organic dye under dark condition

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Abstract

Water pollution as a result of releasing organic and inorganic pollutants is the main concern and health risk factor for human beings. To minimize the effect of toxicity from pollutants, enormous method has been applied. In this report, the CuAl-layered double hydroxide/MgO₂ composite catalysts were synthesized via in-situ growth of magnesium peroxide on the layered double hydroxide (LDH) sheet. The preparations of the catalysts were performed with varying the ratio of LDH: MgO₂ which was abbreviated as CuAl-LDH/MgO₂-35, CuAl-LDH/MgO₂-50, and CuAl-LDH/MgO₂-65 for 35:65, 50:50, and 65:35% weight ratios, respectively. The prepared catalysts were characterized and evaluated for methyl orange (MO) dye degradation at room temperature under dark conditions. Among the catalysts, CuAl-LDH/MgO₂-50 showed an excellent Fenton-like reaction under neutral condition at which 97% of MO was degraded in the 100 min reaction. However, CuAl-LDH, MgO₂, CuAl-LDH/MgO₂-35, and CuAl-LDH/MgO₂-65 catalysts degrade only 61, 8, 35, and 69% of MO dye. The highest degradation efficiency for CuAl-LDH/MgO₂-50 could be due to the presence of optimum amount of copper along with the sufficient amount of generated hydrogen peroxide from MgO₂ to run the Fenton-like reaction process. Moreover, the catalyst can also be able to use repeatedly with a minimum loss of activity. In general, the result suggests that CuAl-LDH/MgO₂ composite is an option for the degradation of organic pollutants.

Keywords Fenton-like reaction · Layered double hydroxide · MgO₂ · Catalyst · Organic pollutants

Introduction

Organic pollutants such as phenols, pesticides, dyes, and other organic pollutants are a major threat for living things (Dvininov et al. 2010; Zelekew and Kuo 2017a). Since the developments of industries utilize several chemicals as input, effects related to effluents becomes worse recently (Lu et al. 2019). Particularly, chemicals released from industries and population growth are the main causes of water pollution and have led to an adverse effect on healthy life (Rupa et al.

2019). Therefore, the decontamination of polluted water resources is now the main concern for researchers around the globe (Zelekew et al. 2021). Although several water treatment methods such as filtration (Cardenas et al. 2016), sedimentation (Soltani et al. 2016), and distillation (Mustapha et al. 2020) were used, they have their own drawback in the complete removal of pollutants. Other methods such as adsorption and photocatalytic degradation have been used for wastewater treatment (Garcia-Muñoz et al. 2020; Wan et al. 2018). It is also reported that photocatalysis is an effective and efficient method for the treatment of wastewater (Opoku et al. 2017; Zhang et al. 2019). For this purpose, metal oxide catalysts can be used due to their efficiency, economical, and stability (Zelekew et al. 2017).

Metal oxides such as TiO₂ and ZnO are an important class of materials and are used for wastewater treatment (Ahmad et al. 2020; Marinho et al. 2017). However, they have their own limitations such as high electron and hole recombination rate and large bandgap (Opoku et al. 2017; Aragaw et al. 2020). To enhance the catalytic activities of metal oxide,

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supporting materials to minimize agglomeration effects can be used (Zelekew and Kuo 2017b). In this perspective, layered materials and clays have been used as a support that can help to immobilize metal oxides and reduce agglomeration thereby providing a site for growth (Fei et al. 2019; Hadjitaief et al. 2021). Additionally, the layered double hydroxides (LDHs) which are synthetic anionic clay-like layered materials have been studied to treat pollutants through both adsorption and degradation process owing to their layered and special memorial property than the usually known metal oxides (Lu et al. 2016; Ali et al. 2020; Seftel et al. 2014).

It has been also reported that the Fenton-like advanced oxidation process is a promising technique for the prompting of strong oxidants even in a dark environment (Brillas and Garcia-Segura 2020). Particularly, iron has advantages due to plentiful abundance, low cost, adaptability to the environment, and being low-poisonous. However, the iron-based Fenton reactions required acidic condition, a cause for H_2O_2 transportation difficulties, and lead to lower lifetime in the oxidation reaction (Bokare and Choi 2014; Wu et al. 2019). Thus, many researchers have been engaged in the modification to cure the challenges present in conventional Fenton processes. Among the findings, using non-ferrous-based catalysts and in-situ generation of peroxide have been reported and showed an intensified performance (Asghar et al. 2015; Torres-Pinto et al. 2020). Latterly, metal peroxides exhibited much attention since these materials are economically advisable besides generating sufficient hydrogen peroxide (Wu et al. 2019). Such findings not only broaden Fenton-like activity to a wider pH range but also minimize the loss of catalysts that happened through precipitation. Particularly, Cu-based catalysts in Fenton-like reactions can provide great potential in Fenton reactions in which it can works in the neutral pH conditions unlike iron-based Fenton reactions (Ma et al. 2019).

It is also know that the LDH materials alone are not sufficient in the removal of pollutants due to the relatively lower charge transfer efficiency and the higher photo-generated electron and hole pairs recombination rate (Gao et al. 2021). Hence, combining the LDH with other materials such as oxides (Fei et al. 2019; Zhang et al. 2021), metals (Lestari et al. 2021), MOFs (Soltani et al. 2021), and rGO (Khaatae et al. 2019) are important. In addition to LDH-based materials, peroxides are used in the degradation of pollutants due to their effectiveness with increasing the photogenerated reactive species (El-Shamy 2020a, 2020b). Among peroxides, the ZnO_2 and MgO_2 are reported for the degradation of organic pollutants (Yang et al. 2017; Zeng et al. 2020). For example, the ZnO_2 -based nanocomposite catalyst was used for the photocatalytic degradation of dyes (El-Shamy 2020b). Wu et al. (2019) used MgO_2 nanoparticles to enhanced Fenton-like degradation of organic pollutants. Naim et al. (Al Naim and El-Shamy 2021) also prepared

PVA/ MgO_2 composite catalyst for organic dye removal. However, there is no report on the preparation of CuAl-LDH/ MgO_2 composite catalyst via in-situ growth of MgO_2 on the surface of CuAl-LDH which is used for the degradation of MO dye under dark condition.

In this work, the CuAl-LDH/ MgO_2 catalyst was prepared via in-situ growth of MgO_2 on the surface of CuAl-LDH according to the reported literature (Seftel et al. 2014). The characterization for the resulting catalysts was performed and applied in the MO dye degradation. The catalytic efficiency is expected to be active due to the synergistic effects of the LDH and MgO_2 . Moreover, the presence of sufficient copper content together with generated H_2O_2 from MgO_2 used for facilitating Fenton-like reaction that could also enhances the MO dye the degradation process. The degradation mechanism was also illustrated in which the LDH initially absorbs pollutants through electrostatic attraction followed by an ion exchanging capability. Then, the hydrogen peroxide generated will be interacted with the adsorbed MO pollutant. Finally, the degradation process will occur through the Fenton-like reaction mechanism. Moreover, the stability of the catalyst was also checked, and it was illustrated that the catalyst was highly stable.

Materials and methods

Chemicals and reagents

All chemicals and reagents were used without further purifications. The $Cu(NO_3)_2 \cdot 3H_2O$, $Al(NO_3)_3 \cdot 9H_2O$, NaOH, Na_2CO_3 (99%), isopropanol ($CH_3CHOHCH_3$) 99.5%, ammonium hydroxide (NH_4OH), $MgCl_2 \cdot 6H_2O$, H_2SO_4 , H_2O_2 (30%), methyl orange (MO), ethylene diamine tetra acetic acid disodium salt (Na_2EDTA), and ethanol (C_2H_5OH , 99.9%) were used in the experimental work.

Synthesis of CuAl-LDH catalyst

CuAl LDHs was prepared through co-precipitation method (Zhu et al. 2017). Typically, 15 mmol of $Cu(NO_3)_2 \cdot 3H_2O$ and 7.5 mmol of $Al(NO_3)_3 \cdot 9H_2O$ were dissolved in 100 mL distilled water. The mixture was stirred for 2 h with a molar ratio Cu to Al of 2:1. Under stirring, an aqueous solution of 1.2 M Na_2CO_3 and 0.6 M NaOH were dropped into the salt solution until pH becomes 9. The resulting solution was stirred at room temperature for another 10 h. Finally, the precipitate was separated through filtration and washed with distilled water and ethanol. Finally, the as-synthesized precipitate was dried at 70 °C for 20 h, and CuAl-LDH powder was obtained.

Synthesis of MgO₂

Using the in-situ growth method as reported in the literature (Navik et al. 2017; Lakshmi Prasanna and Vijayaraghavan 2017), 10 mL of H₂O₂ was added to 20 mL of 2 g MgCl₂·6H₂O solution and stirred for 2 h at room temperature. Then, 2 M of NaOH was dropped until the white foam was formed and further stirred for 3 h until the foam broken down. The milky white-colored precipitate was aged for 18 h. The precipitate was washed with distilled water, ethanol, and finally with ammonia solution until pH reaches neutral and dried at 100 °C for 2 h.

Synthesis of CuAl-LDH/MgO₂ composites

In a particular method, 0.35 g CuAl-LDH, 0.5 g CuAl-LDH, and 0.65 g CuAl-LDH were added in different beakers containing distilled water and dispersed at room temperature for 30 min to produce homogeneous suspension (Setegn 2020). Then, 2.36 g, 1.81 g, and 1.26 of MgCl₂·6H₂O were added into the beakers containing 0.35 g CuAl-LDH, 0.5 g CuAl-LDH, and 0.65 g CuAl-LDH suspension. The suspensions were further stirred for 1 h at room temperature. The pH was adjusted to 12 using NaOH for each suspension. Keeping pH constant, 10 mL of H₂O₂ was dropped to each beaker and stirred for another 4 h. The resulted mixtures were aged at room temperature for 16 h. The obtained precipitates were washed with water and ethanol. Finally, the powders were dried at 100 °C for 2 h and used for the degradation of MO dye. The prepared samples for 0.35, 0.5, and 0.65 g of CuAl-LDH with H₂O₂ were abbreviated as CuAl LDH/MgO₂-35, CuAl-LDH/MgO₂-50, and CuAl-LDH/MgO₂-65, respectively, for simplicity.

Characterization of the catalysts

The X-ray photoelectron spectroscopy (XPS) (ESCALAB 250) was used to determine chemical states of the sample. Shimadzu XRD- 7000 was used to analyze the X-ray diffraction (XRD). The field-emission scanning electron microscopy (FESEM, JSM 6500F, JEOL) and transmitted electron microscopy (TEM) (FEG TEM technai G2 F30) instruments were used for surface characterization. The bonding and functional groups of the samples were checked by using FTIR instrument (Ft/IR-6600 type A). The Shimadzu-3600 Plus UV-Vis spectrophotometer was used to check the concentration of the pollutant.

Catalytic activity test

The degradation of MO was determined by using UV-Vis spectrophotometer. In a particular procedure, 50 mL (10 ppm) MO solution was placed in a beaker. Subsequently,

20 mg of the catalyst was added under neutral conditions at room temperature. Under stirring, 5 mL of the solution was taken in every 20 min interval. After centrifuge, the concentration of MO was determined using UV-Vis spectrometer.

Moreover, the stability of the catalyst was also evaluated by running four cycles. Typically, 200 mg of CuAl-LDH/MgO₂-50 catalyst was added into 500 mL of 10 ppm MO solution. After 100 min, the catalyst was allowed to settle for 2 h. Then, the sample was filtered and re-used for the next remaining runs.

Results and discussion

XRD analysis

Figures 1a–e show the XRD patterns of the MgO₂, CuAl-LDH, and CuAl-LDH/MgO₂ (CuAl-LDH/MgO₂-35, CuAl-LDH/MgO₂-50, CuAl-LDH/MgO₂-65) samples, respectively. As we have seen from the XRD result, all the diffraction patterns of CuAl-LDH/MgO₂ resemble the CuAl-LDH peaks. However, the diffraction peaks of CuAl-LDH/MgO₂-35 get minimum due to the lower content of LDH and the dominant phases of MgO₂ available in catalyst. The typical diffraction peaks at 2θ value of 11.73, 23.59, 32.74, 35.47, 40.22, 47.97, and 60.3° correspond to (300), (006),

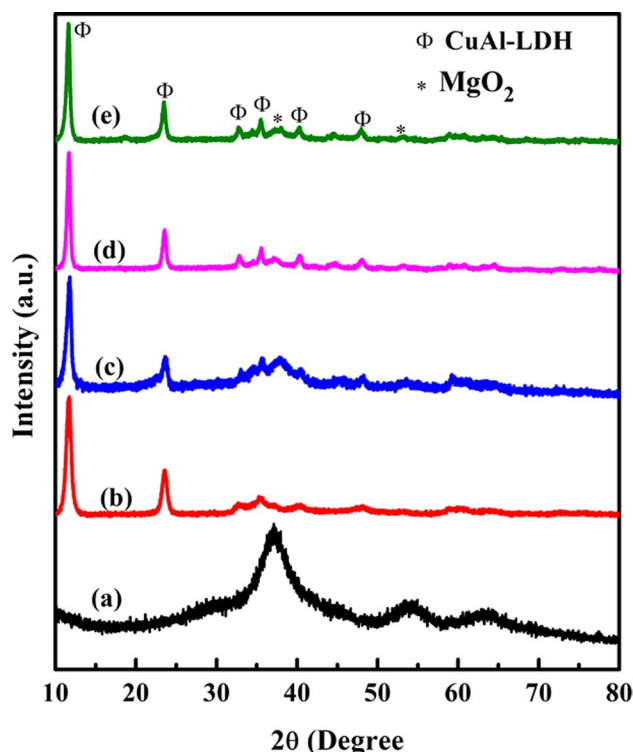


Fig. 1 XRD patterns of **a** MgO₂, **b** CuAl-LDH, **c** CuAl-LDH/MgO₂-35, **d** CuAl-LDH/MgO₂-50, and **e** CuAl-LDH/MgO₂-65

(009), (012), (015), (018), and (110) planes of hydrotalcite-like materials, respectively, (JCPDS card 37-630) (Kameda et al. 2015). The XRD patterns show the formation of the layered double hydroxide which is represented as $\text{Cu}_6\text{Al}_2(\text{OH})_{16}\text{CO}_3 \cdot 4\text{H}_2\text{O}$. Moreover, the peaks at 11.73° correspond to carbonate (CO_3^{2-}) intercalated in the LDH which is resulted from Na_2CO_3 . As it is indicated from Fig. 1a and in all composites, three broad peaks were also obtained at 37.2 , 53.4 , and 63.4° corresponding to (200), (220), and (311) planes of MgO_2 , respectively, (JCPDS No.76-1363) (Wu et al. 2019). The MgO_2 sample was pure, and other extra peaks from MgO and $\text{Mg}(\text{OH})_2$ were not observed which is also similar to a reported literature (Wu et al. 2019). The MgO_2 peaks were broader and show smaller crystalline size. The lower crystalline size of magnesium peroxide

leads to better dispersion upon forming a composite with the layered double hydroxide. In general, LDHs provide a site to grow magnesium peroxide along with inhibiting irregular growth of MgO_2 with better dispersion.

XPS analysis

The chemical oxidation state and surface compositions of CuAl-LDH/MgO_2 were confirmed by XPS as shown in Fig. 2. The XPS peaks for $\text{Cu } 2p_{3/2}$ at 935.88 eV and $\text{Cu } 2p_{1/2}$ at 956.01 eV demonstrate for $\text{Cu}(\text{OH})_2$ (Peng et al. 2018). While the XPS peaks for $\text{Cu } 2p_{3/2}$ at 933.91 eV and $\text{Cu } 2p_{1/2}$ at 955.11 eV indicate for Cu^{2+} in the CuO (Zhao et al. 2019). The peak at 77.11 eV binding energy corresponds to the A–O bond (Lu et al. 2017). Moreover, the

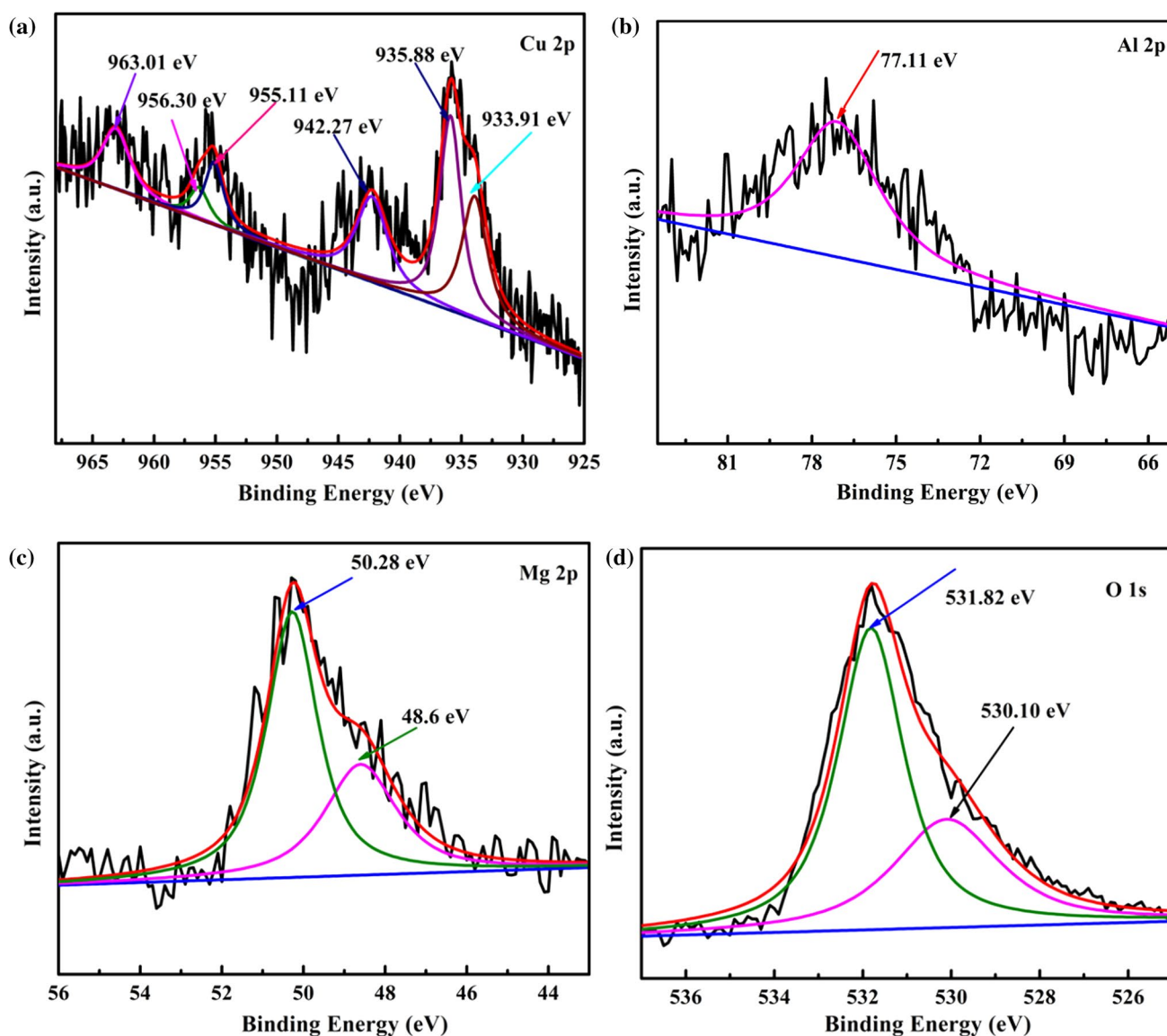


Fig. 2 XPS spectra of **a** Cu 2p, **b** Al 2p, **c** Mg 2p, and **d** O 1s for CuAl-LDH/MgO₂-50

binding energies at 50.28 and 48.6 eV indicate the existence of Mg–O and Mg–OH in the sample, respectively (Zeng et al. 2020). The O1s spectrum with binding energy at 531.82 and 530.10 eV is attributed to the lattice oxygen bonded with metals in the composite catalyst (Zeng et al. 2020; Dupin et al. 2000; Almoisheer et al. 2019).

SEM analysis

Figure 3a, b indicates the lower and the higher resolution SEM images of LDH/MgO₂-50 sample, respectively. The sheet-like morphology was observed (Fig. 3a, b). Moreover, the presence of clustered particles growth of MgO₂ was not observed clearly. This is because the MgO₂ particles were immobilized in the presence of CuAl-LDH support. Moreover, the EDS analysis was also used to check the presence of elements like Cu, Al, O, and Mg, in the CuAl-LDH/MgO₂-50 sample as shown in Fig. 3c.

TEM analysis

Figure 4a, d indicates the lower, medium, and higher resolution TEM, and HRTEM images of the CuAl-LDH/MgO₂-50 sample, respectively. The TEM images in Fig. 4a–c exhibit the sheet-like morphology which is similar to SEM images. The resulting nanosheets exhibit the formation of layer structures of CuAl-LDH. Moreover, the TEM also verifies that there was fewer agglomerated porous sheet-like structure for CuAl-LDHs. Additionally, the smaller dot-like particles were shown on the surface of nanosheets. The smaller dot-like morphologies could be MgO₂ nanoparticles. The HRTEM in Fig. 4d also indicates that the CuAl-LDH/MgO₂-50 sample is crystalline.

FTIR analysis

The Fourier transform infrared spectroscopy (FTIR) analysis was also performed as shown in Fig. 5. Figure 5a, b indicates the FTIR spectrum of CuAl-LDH and CuAl-LDH/MgO₂-50

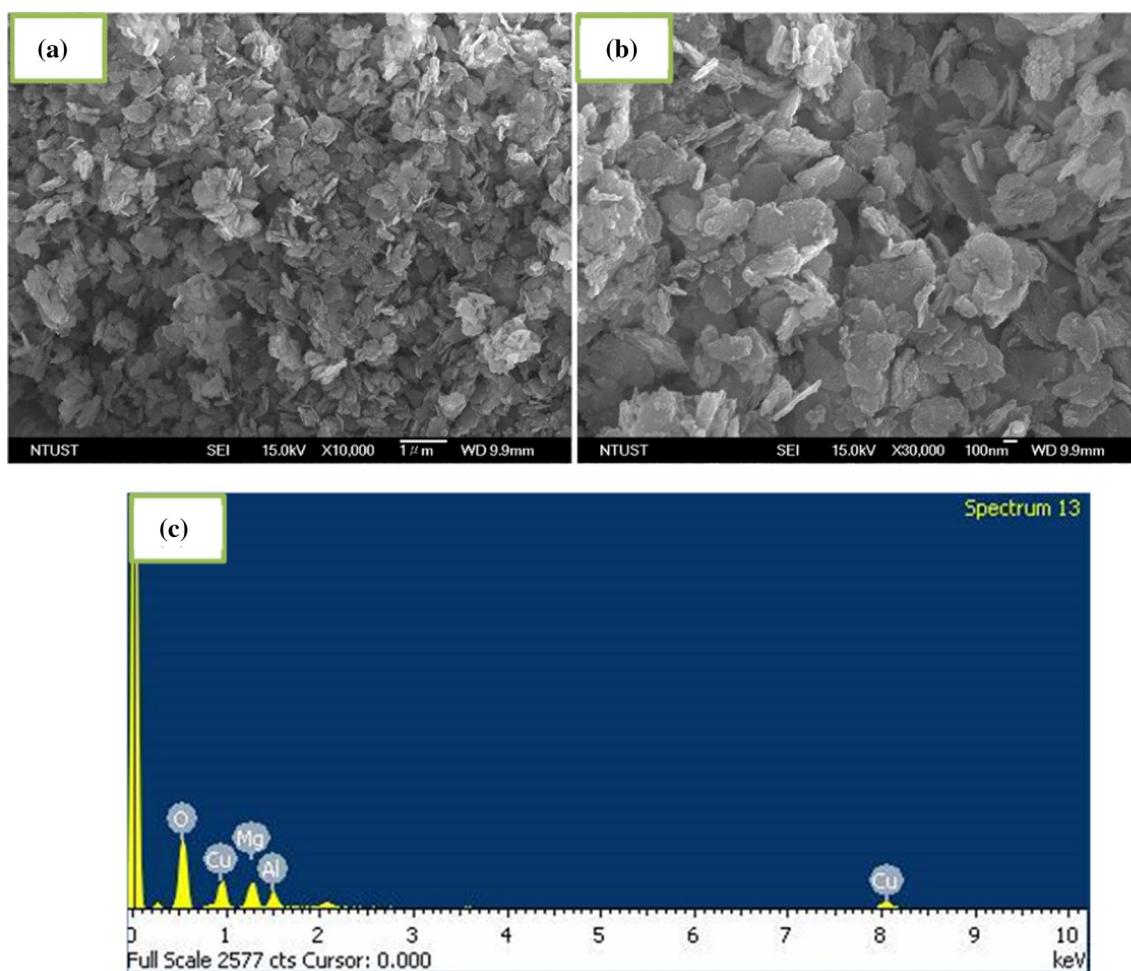


Fig. 3 SEM images of **a–b** the lower and the higher resolution, **c** EDS analysis of CuAl-LDH/MgO₂-50 sample

Fig. 4 a–c the lower, medium, and higher resolution of TEM and **d** HRTEM images of the CuAl-LDH/MgO₂-50 sample

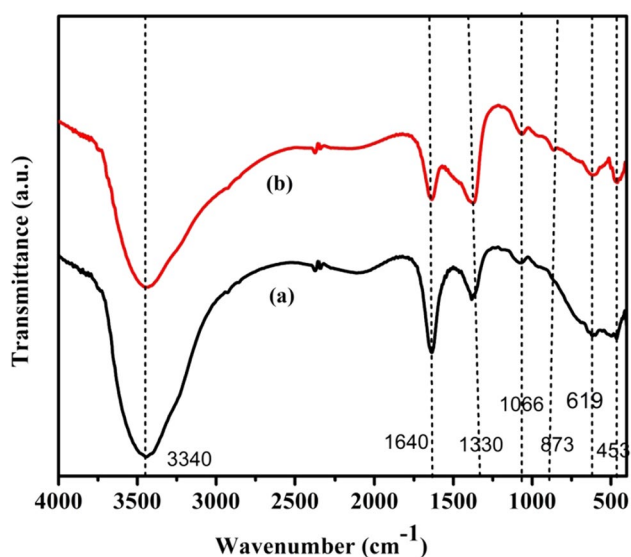
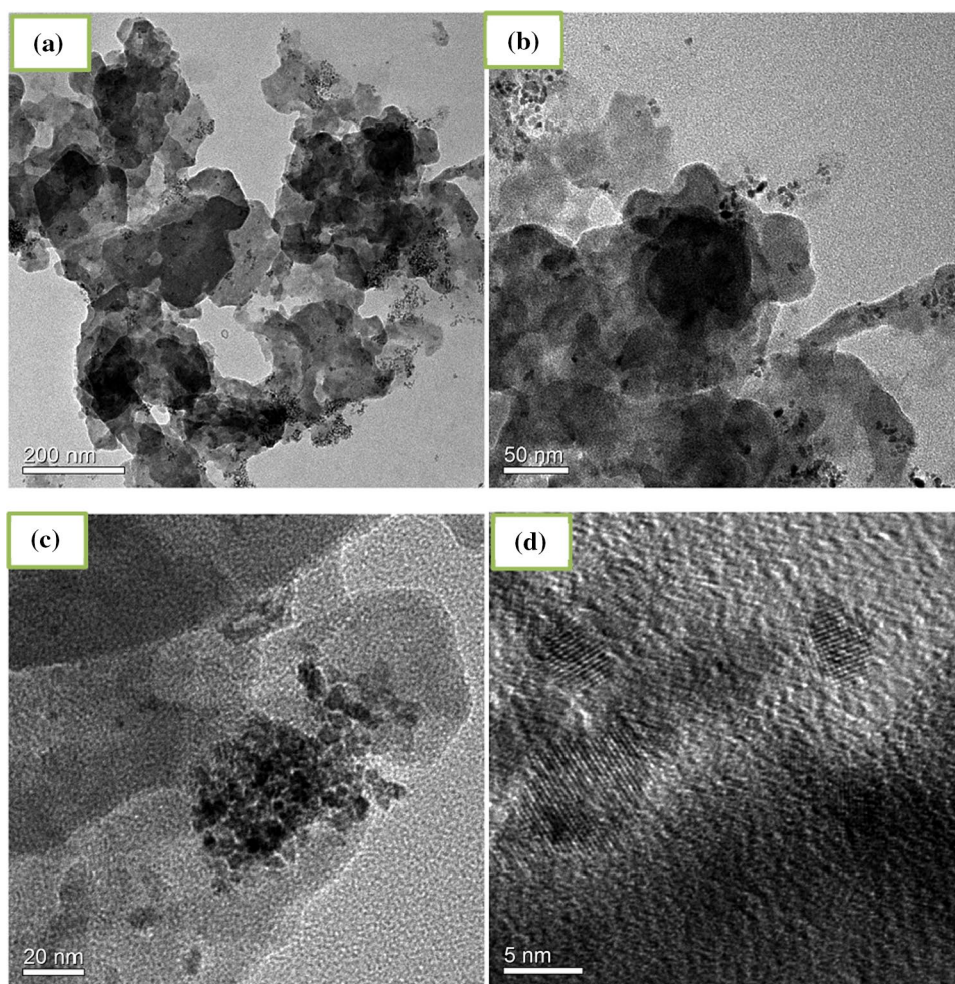


Fig. 5 FTIR spectra of **a** CuAl-LDH, **b** CuAl-LDH/MgO₂-50 samples

samples, respectively. The peak at 3340 and 1640 cm^{-1} attributed to the OH-stretching and the bending modes for the interlayer water and hydroxyls, respectively (Li et al. 2017; Rives et al. 2001). The peak at 1330 cm^{-1} is showed the vibration mode of CO_3^{2-} (Klopprogge et al. 2002). The vibration modes of the carbonate anions were also illustrated at 1066 and 873 cm^{-1} absorption peaks (Li et al. 2017). The 619 and 453 cm^{-1} peaks observed in the sample could be due to lattice vibration of metal oxygen bonding (Rives et al. 2001). In the CuAl-LDH/MgO₂-50 samples (b), the OH stretching is relatively week while CO_3^{2-} vibrations are stronger than its vibration in the LDH sample (a). This is because of the carbonate ion intercalation during MgO₂ deposition onto the LDH.

Nitrogen adsorption–desorption isotherm

The BET analysis of the CuAl-LDH/MgO₂-50 sample indicated in Fig. 6. As it is illustrated in Fig. 6a, the isotherm plot of the CuAl-LDH/MgO₂-50 sample is coincident with the type IV in which it has mesoporous characteristics

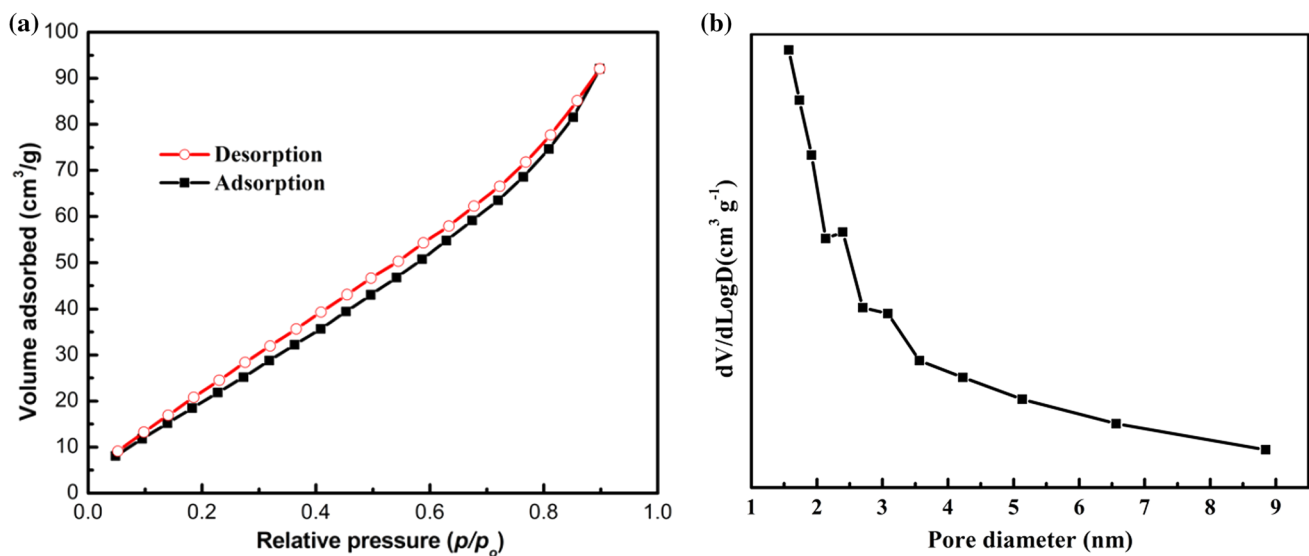


Fig. 6 **a** Nitrogen adsorption and desorption isotherm and **b** the pore size distribution curve of CuAl-LDH/MgO₂-50

(Rouquerol et al. 2013). Moreover, the hysteresis loop demonstrates irregular pore size distribution. The loop can be also defined as H3-type and the pore channels are mainly mesopores (Triantafyllidis et al. 2010). Being H3-type also implying that there is a number of slit shaped pore channels resulted from aggregate or packing of platelet shaped particles of the LDH (Li et al. 2017; Zhi et al. 2010). Figure 6b shows the pore size distribution of the CuAl-LDH/MgO₂-50 sample. From the BET analysis, the total surface area (110.69 m²/g), pores volume (0.128 cm³ g⁻¹), and average pore size distribution (1.569 nm) of the sample were also illustrated. The higher surface area of the sample could help to enhance the catalytic activities of CuAl-LDH/MgO₂-50 sample.

Catalytic activity

All the experiments were performed at room temperature under dark condition. The catalytic performance of CuAl-LDH, MgO₂, and CuAl-LDH/MgO₂ composites were measured using UV–visible spectroscopy. The UV–Vis absorption spectra of the MgO₂, CuAl-LDH, CuAl-LDH/MgO₂-35, CuAl-LDH/MgO₂-50, and CuAl-LDH/MgO₂-65 samples are shown in Fig. 7a–e at different interval of times. As it is indicated in Fig. 7a, there was no degradation performance with MgO₂ sample only. MgO₂ cannot generate peroxides to produce active species without other reagents (Lakshmi Prasanna and Vijayaraghavan 2017). Moreover, the CuAl-LDH sample as shown in Fig. 7(b) also had no significant degradation efficiency after it is reached at maximum adsorption capacity within 20 min. On the other hand, the composite form of MgO₂ and CuAl-LDH lead to both adsorption and degradation outcome as shown in Fig. 7c–e

Among the composites, CuAl-LDH/MgO₂-35 (Fig. 7c) shows a minimum performance. It is due to the minimum amount of copper to produce hydroxyl radicals in the composite catalyst. Among the composites, maximum activity was obtained by CuAl-LDH/MgO₂-50 (Fig. 7d) which had the optimum amount of both CuAl-LDH and MgO₂ in the catalyst system. Further increasing of the CuAl-LDH also deactivates the catalytic activities in which the minimum amount of MgO₂ that can be used to generate active species is available.

The degradation efficiency of the CuAl-LDH/MgO₂-50 composite sample was the highest as shown in Fig. 7d. This particular composition suggests that both copper and MgO₂ are the main components for the generation of optimal active oxygen species. On the other hand, CuAl-LDH/MgO₂-65 composite also showed good performance next to CuAl-LDH/MgO₂-50 composite. The resulting performance could be due to the higher copper content. Initially CuAl-LDH/MgO₂-65 performs well, but as time increases, it doesn't work like CuAl-LDH/MgO₂-50. The reason may be the lowest peroxide generation due to the lower amount of MgO₂ in the LDH/MgO₂-65 composition catalyst. The CuAl-LDH/MgO₂-50 shows an excellent Fenton-like reaction under the neutral condition at which 97% of MO dye was degraded within 100 min. However, CuAl-LDH, MgO₂, CuAl-LDH/MgO₂-35, and CuAl-LDH/MgO₂-65 catalysts degrade only 61, 8, 35, and 69% of MO dye. Generally, the optimum amount of H₂O₂ generated from MgO₂ in aqueous media and the higher content of copper that can able to generate more ROS thereby facilitated the degradation of MO dye. The LDHs also enhance the adsorption of the dye and facilitates for the interaction between the dye and the reactive oxygen species on the surface of the catalyst.

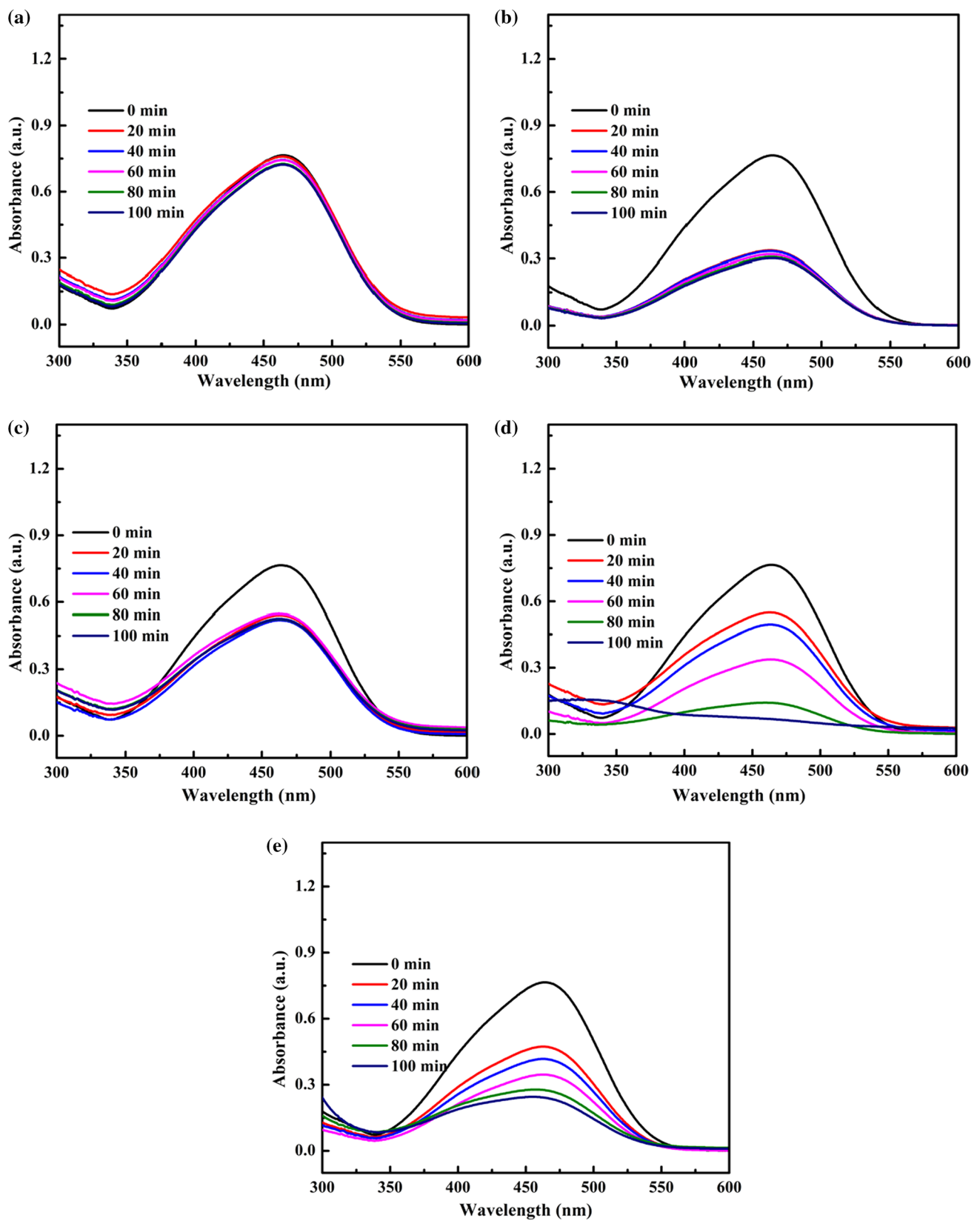


Fig. 7 UV-visible absorption spectra of MO dye with **a** MgO₂, **b** CuAl-LDH, **c** CuAl-LDH/MgO₂-35, **d** CuAl-LDH/MgO₂-50, and **e** CuAl-LDH/MgO₂-65 catalysts

Figure 8b also indicates the degradation kinetics of MO with catalysts at different interval of time fitting with pseudo-first-order reaction and calculated as $-\ln(C_t/C_0) = kt$ (where C_0 is initial concentrations, C_t is the concentration after the irradiated time (in a minute), and k is the rate constant (Youssef et al. 2016; Stupar et al. 2020). The rate constant values for the degradations of MO dye with MgO_2 , CuAl-LDH, CuAl-LDH/ MgO_2 -35, CuAl-LDH/ MgO_2 -50, and CuAl-LDH/ MgO_2 -65 were 0.0005, 0.0071, 0.0031, 0.031, and 0.011 min^{-1} , respectively. As it is observed from data, the rate constant of the CuAl-LDH/ MgO_2 -50 catalyst was highest.

Stability test

The stability of the catalyst was also demonstrated and showed in Fig. 9a. It is reported that the difficulty in transporting hydrogen peroxide upon conducting Fenton reaction has been remained as a common challenge. As it is reported, the CuAl-LDH for MO degradation doesn't show persistent activity after multiple runs (Li et al. 2017). In this particular work, the stability of the as synthesized catalyst was relatively higher and stable. As H_2O_2 generated in-situ way, it shows consistent activity for multiple runs. After 4th cycle, the CuAl-LDH/ MgO_2 -50 catalyst degrades 92.7% of MO dye. Furthermore, the XRD diffraction patterns after

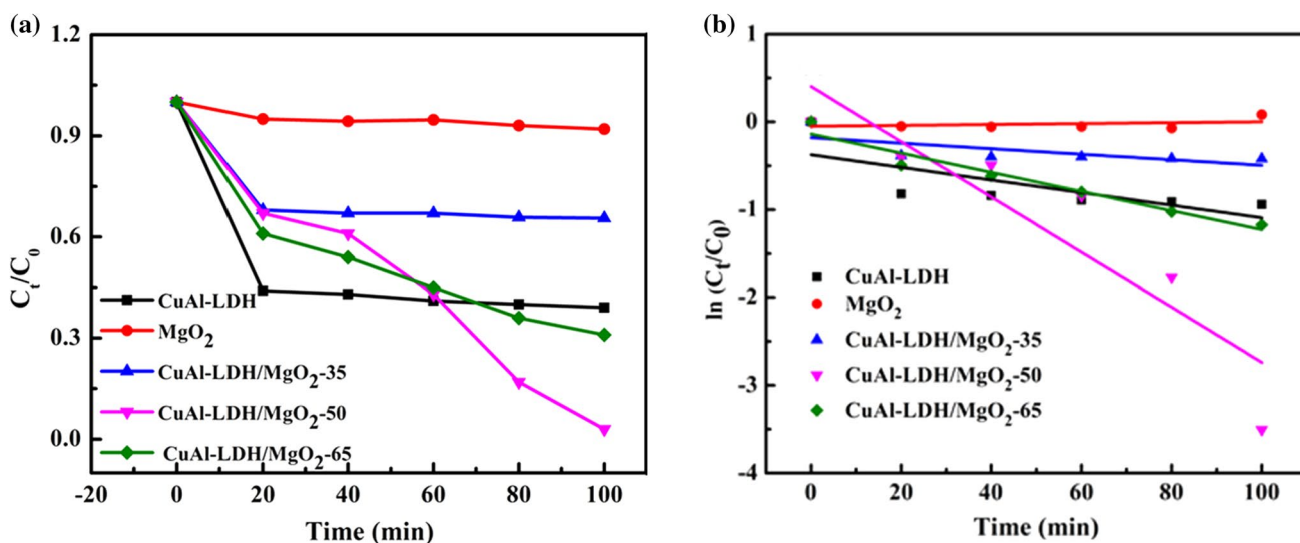


Fig. 8 a The C_t/C_0 photodegradation results and b Pseudo first-order reaction kinetics rates of MO dye with different catalysts

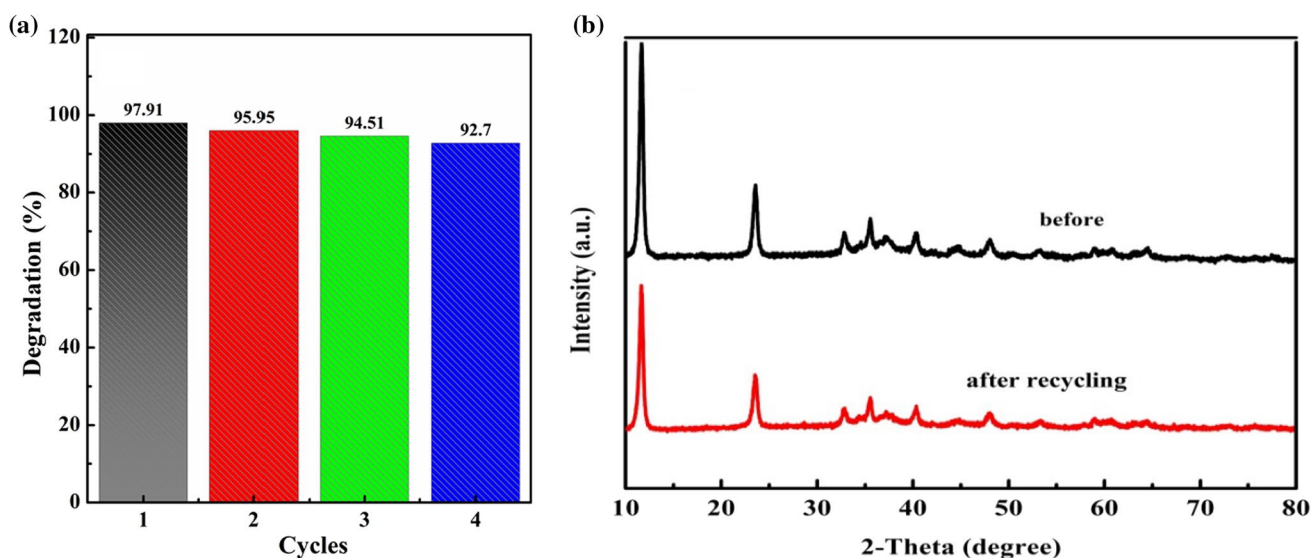


Fig. 9 a Re-usability and b XRD patterns of CuAl-LDH/ MgO_2 -50 catalyst before and after reaction

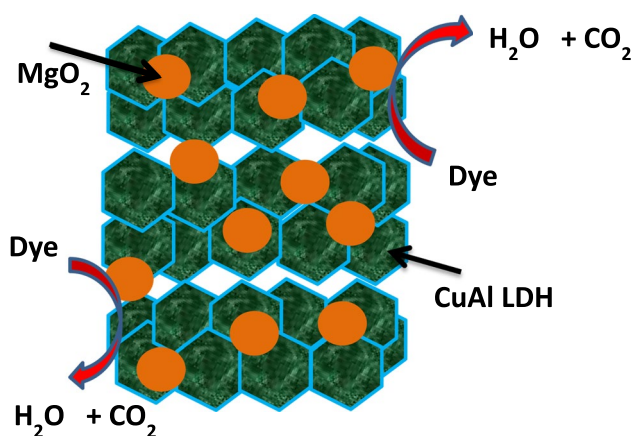


Fig. 10 The degradation mechanism of MO with CuAl-LDH/MgO₂-50 catalyst

reaction resembles the pattern of the composite before a reaction (Fig. 9b). This further pinpoints the better stability owned by the as-synthesised composite.

Degradation mechanism

Recently, using LDH-based composite catalyst in the water treatment attracts a great attention. The catalytic reaction mechanism was also investigated (Peng et al. 2018). Initially, the organic pollutants will be adsorbed by the catalyst through electrostatic attraction. Under aqueous media magnesium peroxide starts to generate hydrogen peroxide while copper from the hydroxalate layer converts the generated peroxide into active oxygen species. Once the active species formed, there will be interaction between the reactive oxygen species and MO. Finally, the MO will be converted to CO₂ and H₂O. The generation of ·OH through Fenton-like reaction is dependent on the content of available reagent and peroxide. Figure 10 shows the degradation mechanism of MO with CuAl-LDH/MgO₂-50 catalyst.

Conclusion

The CuAl-LDH/MgO₂ catalyst was synthesized via in-situ growth of magnesium peroxide on the CuAl-LDH sheet. The catalyst was used for the Fenton-like reaction process. In the reaction process, CuAl-LDH/MgO₂ catalyst had the ability to generate reactive oxygen species under aqueous solution in the dark condition. The CuAl-LDH/MgO₂-50 shows enhanced Fenton-like reaction, and 97% of MO dye was degraded within 100 min. However, CuAl-LDH, MgO₂, CuAl-LDH/MgO₂-35, and CuAl-LDH/MgO₂-65 catalysts degrade only 61, 8, 35, and 69% of MO dye. The LDHs also enhance the adsorption of the dye and facilitates for the

interaction between the dye and the reactive oxygen species on the surface of the catalyst. The catalytic enhancement of the composites could be synergistic effects obtained from the CuAl-LDH and MgO₂. Hence, the optimum amount of H₂O₂ generated from MgO₂ in aqueous media and the higher content of copper that can able to generate more ROS thereby facilitating the degradation of MO dye are the main species.

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Declarations

Conflict of interest The authors declare no competing interest.

Ethical approval The authors declare no any ethical conduct.

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