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A parametric study using Box‑Behnken design for melanoidin removal via Cu‑impregnated activated carbon prepared from waste leaves biomass

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Abstract

Distillery industry is amidst the top source of surface water pollution owing to its very high content of recalcitrant organics, inorganics, and persistent turbidity contents. Melanoidins are the chief dark brown-colored complex contaminant existing in the distillery generated effluent with a very high organic load. The present investigation examined the melanoidin elimination from a model wastewater system utilizing Cu-impregnated activated carbon derived from waste leaves of *Mangifera indica*. With the initial surface characterization utilizing SEM equipped with EDX and FTIR, the Box-Behnken design of experiments was engaged for determining the infuence of diferent factors for the melanoidin removal from the aqueous system. Adsorbent dose, initial melanoidin concentration, and contact time have imposed the maximum efect on to the melanoidin removal (73%) using the synthesized activated carbon, clearly showing its ability for the melanoidin removal from the aqueous contaminated system.

Keywords Activated carbon · Melanoidin removal · Response surface methodology · FTIR

Introduction

Melanoidins, a heterogeneous polymer (high molecular weight), formed during the last stage of Millard reaction due to the reaction between reducing sugars carbonyl group and amino acids peptide or amino group (Diaz-Morales et al. [2020](#page-7-0)). During cooking, thermal treatment or preservation non-enzymatic browning alteration occurs in food and provides organoleptic characteristics in processed food. Thus, they are brown-colored, polymeric complex with chemical oxygen demand and are present in various food such as cocoa beans, beer, sweet wine, coffee, honey, bakery products (Alves et al. [2020](#page-6-0); Goulas et al. [2018](#page-7-1)). These industries generate large amount of wastewater mainly characterized by brown color with high chemical oxygen demand (COD),

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biological oxygen demand (BOD), dissolved organic nitrogen, phenolics, total dissolved solid, phosphates, and sulfates (Kumari et al. [2020](#page-7-2); Goswami et al. [2018a](#page-7-3), [2019](#page-7-4)). They are also known to have antioxidant, antimicrobial, cytotoxic, and anti-hypertensive activities (Kushwaha et al. [2022;](#page-7-5) Hussain et al. [2021](#page-7-6); Liakos and Lazaridis [2016\)](#page-7-7). Also, metal ions interact with melanoidin and form stable complexes which further contributes in environmental pollution (Chandra et al. [2008;](#page-7-8) Gautam et al. [2021\)](#page-7-9). Furthermore, it reduces the alkalinity and manganese availability in soil, thereby, impeding the seed propagation which leads to abridged crop yield (Gupta et al. [2020;](#page-7-10) Lata et al. [2021;](#page-7-11) Bajgai et al. [2022](#page-6-1)). In water, it lessens the sunlight dissemination causing less oxygen level and ultimately death of aquatic life (Sathe et al. [2021](#page-8-0), [2020;](#page-8-1) Devi et al. [2021\)](#page-7-12).

Earlier, several conventional technologies (biological and chemical) have been implemented for the elimination of melanoidin from aqueous wastewater (Borah et al. [2021;](#page-6-2) Liakos and Lazaridis [2016\)](#page-7-7). These methods are efective in melanoidin removal but are time-consuming, require a large area, generate perilous by-products, and a large amount of sludge; thus, not suitable for treating such effluents (Gupt et al. [2020,](#page-7-13) [2021](#page-7-14); Kushwaha et al. [2016;](#page-7-15) Goswami et al. [2022](#page-7-16)). To assuage the limitations of conventional technologies, physico-chemical

methods utilizing various adsorbents particularly bioadsorbents (activated carbon, biochar, and coal-fred fy ash) are efective techniques (Goswami et al. [2020,](#page-7-17) [2017;](#page-7-18) Kumar et al. [2019;](#page-7-19) Bind et al. [2019](#page-6-3)). Bioadsorption is a simple, easy, costefective, squat energy requirement, eco-friendly, and constancy in employing a wide range of adsorbents due to their specificity toward the pollutant (Yadav et al. [2021a,](#page-8-2) [b;](#page-8-3) Singh et al. [2019;](#page-8-4) Kushwaha et al. [2020,](#page-7-20) [2017a](#page-7-21)).

Recently, the use of activated carbon (AC) for removal of perilous contaminants has gained attention because of their assorted form with diverse ostensible properties attained via surface modifcations (physical and chemical) such as pore size and volume, functional groups, surface area, and high reactivity (Singh et al. [2022](#page-8-5); Goswami et al. [2019;](#page-7-4) Hoarau et al. [2018](#page-7-22)). Additionally, the properties of AC are governed by the type of raw material used, precursor, temperature, method used, and activating agent (Goswami et al. [2021](#page-7-23)). The adsorption of contaminants (micropollutants, heavy metals, phosphates, and nitrates) was carried via precursors prepared aboriginal from oil palm, peanut shells, mango kernels, date stones, endocarp, etc. (Kumari et al. [2020](#page-7-2); Kushwaha et al. [2021a](#page-7-24), [b](#page-7-25); Kumar et al. [2021](#page-7-26)). Further, some recent literature reported the Fe ions doping to increase the sorption ability/affinity toward the melanoidin elimination along with its revival as a biosorbent (Shah et al. [2015\)](#page-8-6). The surface modifcations are carried out using diferent oxidizing agents trailed by doping with Fe/Cu precursor.

Therefore, the present investigation deals with the gaps in the literature stated above by concurrently probing the removal of melanoidins by exploring copper-impregnated AC derived from *Mangifera indica* forae leaves. Earlier, we have examined three diferent kinds of AC prepared from leaf waste (Rizvi et al. [2020\)](#page-8-7). Here, the efficacy of copperimpregnated AC for melanoidin removal was assessed. Furthermore, the copper-impregnated AC loaded with melanoidin after the adsorption process was evaluated by using scanning electron microscopy (SEM) equipped with energydispersive spectroscopy (EDX) for detecting the change in morphology, and Fourier transform infrared spectroscopy (FTIR) analyses were employed to detect the melanoidin binding functional groups present on the AC surface that were responsible for its removal. Nevertheless, the present investigation deals with melanoidins but can also be considered a prototypical system for other pollutant elimination by adsorption.

Materials and methods

Chemicals

Glucose was procured from HiMedia (Mumbai, India) with > 98% purity. Analytical grade chemicals for preparing

the melanoidin stock solution were obtained from HiMedia (Mumbai, India). MilliQ water was utilized throughout the experiments. A copper metal stock solution of 0.5 mol/L concentration was prepared from $Cu(NO₃)$ ₂ and was diluted accordingly using MilliQ water (Hu et al. [2017](#page-7-27)).

Stock preparation

The stock solution of melanoidin was made as described by Rafgh and Soleymani ([2020\)](#page-8-8) with slight modifcations. Briefly, in 100 mL MilliQ water, glycine, glucose, and NaHCO₃ were mixed and heated at 80 \degree C for 8 h and kept aside to cool. The working solution of melanoidin was prepared by diluting appropriate amount of melanoidin solution in MilliQ water (Yaylayan and Kaminsky [1998](#page-8-9)).

Synthesis of copper‑impregnated activated carbon

The waste leaves of *M. indica* were cumulated nearby from Kanpur, Uttar Pradesh, India. All three types of leaves were converted to AC by following Rizvi et al. ([2020](#page-8-7)). In brief, initially, leaves were laved and dried in an oven at 105 ℃ for 24 h. The samples were grounded, sieved, and stored in a desiccator to avoid surplus moistness. The homogenized samples were amalgamated with HCl (1:2) and kept for 12 h (overnight) for digestion and subsequently, washed and dehydrated at 105 °C for 8 h, and kept at 600 °C for 90 min in a muffle furnace for carbonization.

Further, the copper doping was carried out with the defnite amount to the respective selected AC in 50 mL of 0.5 M Cu $(NO_3)_2$ and kept in a shaker (200 rpm) for 2 h at room temperature (Park et al. [2015](#page-8-10)). The pH was adjusted accordingly to 7.0 with NaOH to attain copper-impregnated AC. The excess salts from adsorbents were removed by washing with deionized water. The prepared AC was dried and stored in a desiccator until further analysis.

The adsorbents morphological characterization was accomplished via SEM (Carl Zeiss EVO 50) (Kushwaha et al. [2017b](#page-7-28)). For SEM–EDX analysis AC and copperimpregnated AC were vacuum-dried and mounted on aluminum stubs over double-sided carbon tape followed by double coating with a thin gold layer by sputter coater (Borah et al. [2019](#page-6-4)). The most distinctive characteristic of adsorbent is functional group occurrence, which is important for binding with pollutants primarily characterized by FTIR (Bruker Tensor 27) with fve scans in the range 450–4000 cm−1 (Goswami et al. [2019](#page-7-4)).

Experiment set‑up

The batch experiment was conducted in 250-mL Erlenmeyer fasks with a working volume (100 mL) of the respective adsorbate concentration. Primarily, all the adsorbents were **Fig. 1** Scanning electron microscopy and EDX spectra of the prepared *M. indica* adsorbent. **a** AC and **b** Cu-impregnated AC

studied, opting for its potential fnal dosage for optimization of adsorbate removal studies. The effect of adsorbent on adsorbate adsorption was attained by reaction, 500 mg/L of starting melanoidin concentration with 50 mg/L adsorbent dosage. The suspension was agitated at pH 3 for 2 h. Later, depending on the result, the adsorbent showing maximum removal was selected (*M. indica*) for further studies. The efect of factors afecting melanoidin removal was determined. Similar parameters were followed for the experiment as per our previous experiment (Rizvi et al. [2020\)](#page-8-7): adsorbent dosage (A: 25–100 mg/L); adsorbate amount (B: 100–1000 mg/L); temperature (C: $30-50^{\circ}$ C); and contact time (D: 30–120 min), and iron/adsorbent ratio (E: 20–40%).

The experimental trials were carried out at pH 4. The optimization of parameters was performed using Box-Behnken design via Design Expert (Version 11, USA) depending on the literature accessible so far. Supplementary Table S1 represents the diferent experimental runs for optimizing the removal process. Based on the literature available for all the studies, pH was kept at 4.0 to elude the doped Cu-particles leaching. The percentage melanoidin removal was calculated as stated in equation:

Melanoidin removal (
$$
\%
$$
) = $\frac{C_0 - C_e}{C_0} \times 100$

Fig. 2 FTIR spectra of the activated carbon and Cu-impregnated activated carbon

where C_0 and C_e signify the initial and final melanoidin concentrations, respectively.

Analytical methods

At the end of the adsorption process, the adsorbents were removed by centrifugation at 8000 rpm for 15 min. The supernatant was collected and examined for adsorbate concentration via a UV–visible spectrophotometer (Systronics UV 22,300) (475 nm) (Rafgh and Soleymani [2020\)](#page-8-8). All the experiments were executed in triplicates, and the values are expressed as mean \pm standard deviation.

Results and discussion

Characterization of prepared Cu‑impregnated activated carbon

The micrographs for both of the prepared adsorbents are presented in Fig. [1.](#page-2-0) The micrographs clearly show that the morphologies have maintained the lignocellulosic herald shape. This technique has led to eliminating the non-carbonaceous substances showing the relative homogenous cavities onto the external surfaces. In addition, the SEM–EDX analysis (Fig. [1](#page-2-0)) demonstrates the copper doping onto the prepared AC adsorbent surface, further confrming the extra Cu peak in all the EDX spectra.

FTIR spectra of both the activated carbon and Cu-impreg-nated AC are represented in Fig. [2.](#page-3-0) Primarily, it is affirmed from the FTIR spectra that the surface of AC has numerous oxygenated groups such as -COOH and -OH (Rodrigues et al. 2020). Also, it could well be detected that all the band intensities dropped owing to the doping of copper for almost at all the stretch bands (Rizvi et al. [2020](#page-8-7)). The band in between 635 and 648 cm⁻¹ (i.e., ~ 640 cm⁻¹) resembles the saturated carbon stretching of $-CH_2$ group. The minute peaks $-C=O$ and $-CH_2$ bands were clearly observed at 1265 and 1028 cm−1, respec-tively (Goswami et al. [2017\)](#page-7-18), along with the -C=O asymmet-ric stretches at 1690 cm⁻¹ (Rizvi et al. [2020\)](#page-8-7). Furthermore, in most cases, a wide spectrum is usually observed at 3500 cm^{-1} , confrming the presence of -OH bonds (Bind et al. [2019\)](#page-6-3).

Melanoidin removal

Earlier, we performed the melanoidin adsorption experiments and examined that the AC prepared from *M. indica* leaf wastes had performed better than others in the batch process (Rizvi et al. [2020](#page-8-7)). Hence, the Cu-impregnated AC prepared from *M. indica* was nominated for further experiment.

Experimental design

For performing the optimization experiments, five different parameters were evaluated for the melanoidin removal utilizing Cu-impregnated AC. The parameters mentioned above (in Sect. [Experiment set-up](#page-1-0)) were selected to determine the efect on the removal process. The experiments were carried out in triplicates, and average results were described. Maximum removal of 73.29% was attained at all the central points of the operational parameters (Fig. [3](#page-4-0)). The present removal was on the lower side in comparison with our earlier study performed with the Fe-impregnated AC (Rizvi et al. [2020](#page-8-7)).

In addition, the ANOVA outcome from the experimental process, the quadratic model reported 46.97 of the *F*-value, inferring the signifcance of the model. Moreover, the projected R^2 (0.8963) agrees with the adjusted R^2 (0.9533), describing that all the exploratory and projected values were lying inside the constricted interval (Supplementary Table S2). Most of the model terms were substantial that validate the accuracy and reliability of the optimization process (Supplementary Table S3). Also, the lack of ft analysis was observed to be irrelevant. The linear efects of three parameters, i.e., adsorbent dosage, initial melanoidin concentration, and temperature, were inferred as the major interacting factors having *P* values<0.001. Similarly, adsorbent dosage–adsorbate concentration (AB), adsorbent dosage–contact time (AD), and adsorbate concentration–contact time (BD) were examined to be the most signifcant interrelating parameter depicting the elliptical nature of the contour plot (Fig. [3](#page-4-0)).

It is also important to evaluate the factors that have substantial efects on melanoidin removal. The perturbation plot helps in determining the impact of various factors on

Fig. 3 Response surface plot depicting the efect of various parameters for melanoidin removal via Cu-impregnated activated carbon

the response. Figure [4](#page-5-0)a is plotted for all five factors. Now, the infuence of each factor is plotted at a defnite point, while the other parameters are kept fxed for melanoidin removal. Here, the mid-point of two extreme values of every factor was selected as the reference point (Das et al. [2014](#page-7-29)). Adsorbent dosage, initial melanoidin concentration, and temperature were primarily observed as noteworthy following the center points.

Figure [4b](#page-5-0) depicts the correlation between experimental and projected values. It further confrms the response scattering amidst the data points and the diagonal lines demonstrating the satisfactory agreement between the actual and projected data (Ab Ghani et al. [2017\)](#page-6-5). Further, the Box-Cox plot was employed to examine the *λ*-value, which is generally used to envisage the change in the experimental numerals to enhance the model impact. In accordance with

Fig. 4 Diagnostic plots generated during ANOVA. **a** Relation between the actual and predicted values; **b** perturbation plot of all the process parameters; and **c** Box-Cox plot for melanoidin removal (%) using the prepared activated carbon

Fig. 5 Plausible mechanism of melanoidin removal via adsorption onto copper-impregnated activated carbon

the *λ*-value of 1.62 generated from the plot, a natural log transformation was utilized (Fig. [4](#page-5-0)c).

Various literature has utilized diferent adsorbents for the melanoidin removal, viz. natural oxides, waste biomaterials, agro-based adsorbents, waste-derived chitin, AC prepared from waste materials, nanosheets, etc. Arimi et al. ([2015\)](#page-6-6) used natural manganese oxides for color and COD removal, where a strong pH dependence was observed. Further, the removal mechanism includes chemical transformation, precipitation, and adsorption. Some researchers had explored the melanoidin removal by graphene oxide nanosheets and reported 18.3 g/g of the adsorption capacity for the actual industrial melanoidincontaminated wastewater (Rafgh and Soleymani [2020\)](#page-8-8). Tsiakiri et al. [\(2020\)](#page-8-11) prepared Baker's yeast cells via immobilizing on to the alumina/silica particles. Around 80 and 100% removal (degradation) were achieved in 48 h for alumina and silica support, respectively. Here, the secretion of laccase and peroxidase activity plays an important role in melanoidin degradation.

Further, Wongcharee and Aravinthan ([2020](#page-8-12)) examined the mesoporous magnetic nanosorbent prepared from *Macadamia* nutshell residues for dissolved organic carbon (DOC) removal. Approximately 68.4% of removal was reported

with the removal phenomena following pseudo-second-order kinetic model and Langmuir isotherm. Susree et al. ([2013\)](#page-8-13) efficiently removed 83.2% of COD using an electrochemical reactor in batch mode with simultaneous enhancement in current density and electrolyte concentration. Additionally, Navgire et al. ([2012](#page-8-14)) synthesized $MoO₃-TiO₂$ nanocrystalline composite material via the sol–gel method. The prepared catalytic material was efficient in degrading melanoidin (molasses) under UV–visible exposure.

Mechanism involved in the treatment process

Figure [5](#page-5-1) depicts the diferent kinds of bonds available on to the surface of the prepared AC, which is plausibly involved in the contaminant removal from the wastewater. Diffusion and attraction are primarily engaged in the physical removal process by adsorption (Rizvi et al. [2020](#page-8-7)). The various bond including hydrogen bonding, *π*–*π* interactions, cationic electrostatic attraction, interparticle difusion, anionic–cationic electrostatic bonding, porefilling, hydrophobic effect, and intersphere complexation, etc., plays an imperious role in melanoidin elimination from wastewater (Goswami et al. [2018b;](#page-7-30) Ab Ghani et al. [2017](#page-6-5); Tan et al., [2015](#page-8-15)). Further, the carboxylic and lactonic groups present on the AC surface can extract the *π*-electrons leading to electron shortage (Liu et al. [2015\)](#page-8-16).

Henceforth, Cu-impregnated AC has shown a substantial amount of melanoidin removal from the contaminated wastewater. The Box-Behnken optimization has further impacted a positive efect on the removal process. All the process parameters have their key role in [melanoidin](#page-3-1) [removal](#page-3-1). Overall, to enhance the removal, we can further explore and optimize various other biowaste materials or industrial waste to make the removal process more efficient.

Conclusions

Overall, the synthesized Cu-impregnated AC was found efficient in treating melanoidin-contaminated wastewater. The utilization of the optimizing tool for the optimization of diferent process parameters has certainly played a crucial role in melanoidin removal. Adsorbent dosage, melanoidin concentration, and contact time have played a substantial role. In addition, the up-scaling to determine the efficiency of the adsorbent and the real wastewater containing melanoidin could be preferred to have a clear insight and performance of the removal process.

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Declarations

Conflict of interest All the authors do not have any confict of interest.

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