



Removal of heavy metals from acid mine drainage by native natural clay minerals, batch and continuous studies

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Abstract

Acid mine drainage (AMD) properties are high acidity, high concentration of sulfate and containing a wide range of heavy metal ions. This study was performed to remove the copper, zinc and nickel from AMD by four native natural clay minerals including bentonite, two types of volcanic ash soil (VAS-I, VAS-II) and red soil using both batch and continuous techniques. The characteristics of adsorbents were investigated by X-ray fluorescence and X-ray diffraction analysis. In batch technique, clay minerals adsorbents were used in different dosages. However, in continuous technique one natural clay mineral (volcanic ash soil) was used. Results showed that the order of capacity of adsorption by four types of minerals was: bentonite > red earth > VAS-I > VAS-II. The adsorption affinity order of the metal ions by all sorbents was Ni > Cu > Zn. In continuous technique, the critical concentration ($C/C_0=0.1$) of copper, zinc and nickel in the flow rate 0.8 mL/min was 350, 160 and 170 min, respectively. Therefore, fixed-bed column experiments showed that volcanic ash soils have the characteristics of simplicity of operation, little sludge production, suitability for low concentrations, flexibility and excellence for continuous and batch operations.

Keywords Adsorption · Heavy metal removal · Natural clay minerals · Acid mine drainage

Introduction

Acid mine drainage (AMD) is one of the major problems in the present world, which is produced by the mining activities (Idaszkin et al. 2017; Jones and Cetin 2017). AMD is created as a result of geochemical reaction; when sulfide minerals are exposed to the atmosphere, they are generated by the process of oxidation (Rios et al. 2008; Sánchez-Andrea et al. 2014). The main characteristics of AMD are high acidity, high concentration of sulfate and containing a wide range of heavy metal ions such as Cu^{2+} , Ni^{2+} , Zn^{2+} , Cd^{2+} and Pb^{2+} (Liao et al. 2017; McCauley et al. 2009). If it is discharged

into the environment without neutralization and removal of hazardous heavy metals, due to these heavy metals not biodegradable and accumulating in living organisms, they can cause a serious adverse effect on human health and ecological resources (Cui et al. 2012; Eslami et al. 2018b; Măicăneanu et al. 2013; Rakotonimaro et al. 2017).

There are several methods for the removal of heavy metals from acid mine drainage such as chemical precipitation, oxidation, hydrolysis, reverse osmosis, solvent extraction, ion exchange, neutralization, electrochemical remediation, adsorption and biosorption (Eslami et al. 2018a; Kalhor et al. 2018; Mohan and Chander 2006; Tolonen et al. 2014). Adsorption is a popular and highly effective method for the removal of heavy metals from wastewaters and AMD (Motsi et al. 2009; Rafati et al. 2018a; Zhang 2011). The advantages of adsorption method include simplicity of operation, access to the adsorbent materials, not requiring any chemical substances and little sludge production (Božić et al. 2013; Eren et al. 2009; Khosravi et al. 2018; Malamis and Katsou 2013). Adsorption of heavy metals has been developed by various types of low-cost, natural and effective adsorbents, such as fly ash, tree bark, tea leaves, natural zeolite and clay minerals (Bachale et al. 2016; De Gisi et al. 2016; Rafati et al.

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2018b). Natural clay and clay minerals such as bentonite and red soils have a small particle size and porous structure with a high specific surface area, which have high efficiency for adsorption and cation exchange capacity (Rafati et al. 2016; Uddin 2017). Natural clay minerals due to their low-cost and high availability are used for numerous adsorption researches (Anirudhan et al. 2012; Anna et al. 2015; Melichová and Hromada 2013; Vieira et al. 2010b). Recently, natural mineral clays were investigated for the removal of copper Cu (II) (Zacaroni et al. 2015), arsenic (V) (Bentahar et al. 2016), cadmium (II), lead (II) and chromium (VI) ions from the aqueous environment (Khan and Singh 2010).

Therefore, this study was performed to remove the copper, zinc and nickel from AMD of copper mining (Rafsanjan, Iran) by natural clay minerals adsorbents including bentonite, two types of volcanic ash soils (VAS-I, VAS-II) and red earth in batch and continuous experiments.

Materials and methods

Preparation of adsorbents

In this study, we used four natural clay minerals including bentonite, two types of volcanic ash soil (VAS-I, VAS-II) and red earth that were collected from Kerman province which is located in the southeast part of Iran. First, they were crushed using a jaw crusher (Pulverisette, Fritsch, Germany) and then sieved, and a particle size less than 50 mesh was selected for tests. Chemical and mineralogical composition of NNB is identified by X-ray fluorescence (XRF) and X-ray diffraction (XRD) (Philips PW1730, The Netherlands) analysis. The cation exchange capacity (CEC) of NNB was measured by methylene blue index, according to the ASTM C 837-81 (Calabria et al. 2013).

Materials

All chemical reagents used in this study were obtained from Merck Company (Germany) with analytical grade. Acid mine drainage (AMD) was collected from the Sarcheshmeh copper mine located in Rafsanjan, Iran. The chemical characteristics of acid drainage are given in Table 1.

Experiment procedure

This study was carried out at room temperature using both continuous and batch techniques in a laboratory scale. In batch technique, four natural clay minerals were used including bentonite, two types of volcanic ash soil (VAS-I, VAS-II) and red earth in different doses (20, 30, 40 and 60 mg/l), and solutions volume (50 ml) was mixed in 300-ml flat-bottom Erlenmeyer flasks and then shaken for 300 min with

Table 1 Chemical characteristics of acid drainage

Composition	Concentration (mg/l)
Cu	80
Zn	13
Ni	1
pH	4.6
EC(mmhos/cm)	1795

a speed of 150 rpm on a rotary shaker. The suspensions were filtered using a filter paper (0.45 μ m), and then, metal ion concentration in filtrate was determined. Atomic absorption spectrometry (AAS) was used to measure the concentration of metals (Varian AA-975 and AA-1275 models). In this study, the following conditions were constant in all experiments: temperature (27 ± 1 °C), particle size (≤ 50 mesh), solution volume (50 ml) and rate of shaking (150 rpm). The percent of metal ions removal by adsorbents was calculated by the following equation (Eq. 1):

$$\%MS = \frac{C_0 - C_e}{C_0} \times 100 \quad (1)$$

Mass balance equation is used to calculate the capacity of the adsorbents:

$$q_e = \frac{C_0 - C_e}{m} \times V \quad (2)$$

where q_e is the amount of metal ions absorbed on adsorbents (mg/g); C_0 and C_e are the initial and equilibrium concentration (mg/L) of metal ions, respectively; V is the volume of AMD (L); and m is mass of adsorbent (g).

The column studies were carried out by one adsorbent (volcanic ash soli). Column experiments were performed in a glass column with a height of 40 cm which was packed to a height of 15 and 26 cm and internal diameter of 2.5 and 1.5 cm. The tests were conducted in two flow rates (0.8 and 1.4 ml/min and particle size selected in the range 10–20 μ m).

Results and discussion

Adsorbents characteristics

Chemical composition and CEC and mineralogical composition of clay minerals are given in Tables 2 and 3, respectively. Chemical composition analysis by XRF showed that the main compounds in the adsorbents were silica (SiO₂) and alumina (Al₂O₃). Based on the main elements of this mineral clays (Si and Al), therefore, they are in the smectite clay group (Pereira de Araujo et al. 2013). Smectite group

Table 2 Chemical analysis and cation exchange capacity of dried clay minerals adsorbents

Composition	wt%			
	Bentonite	VAS-I	VAS-II	Red soil
SiO ₂	64	58	58.5	58
Al ₂ O ₃	6.5	10	10.5	15.2
Fe ₂ O ₃	3.6	3.6	3.1	3.1
CaO	2.2	2.2	3.4	4.9
MgO	3	1.8	1.6	0.8
Na ₂ O	2.2	5.3	4.5	–
K ₂ O	0.5	1.4	1.8	0.1
LOI	10.7	5.3	6.7	10.7
CEC	94.6	377.4	174.6	114.4

LOI loss of ignition

Table 3 Mineralogical composition of clay minerals adsorbents by XRD analysis

Adsorbents	Mineral	Chemical formula
Bentonite	Quartz	SiO ₂
	Illite	K _{0.5} (Al,Mg) ₃ (Si,Al) ₄ O ₁₀ (OH) ₂
	Montmorillonite	K _{0.5} Al ₂ (Si,Al) ₄ O ₁₀ (OH) ₂ ·H ₂ O
VAS-I	Quartz	SiO ₂
	Bentonite	K(Fe,Mg)AlSi ₃ O ₁₀ (OH) ₂
	Plagioclases	(Ca,Na)(Si,Al) ₄ O ₈
VAS-II	Quartz	SiO ₂
	Plagioclases	(Ca,Na)(Si,Al) ₄ O ₈
	Illite	K _{0.5} (Al,Mg) ₃ (Si,Al) ₄ O ₁₀ (OH) ₂
Red soil	Quartz	SiO ₂
	Plagioclases	(Ca,Na)(Si,Al) ₄ O ₈
	Kaolinite	Al ₂ Si ₂ O ₅ (OH) ₄
	Hematite	Fe ₂ O ₃
	Calcite	CaCO ₃

compared with other clays have high cation exchange capacity, high specific surface area and suitable adsorption efficiency (Uddin 2017). CEC of mineral clays adsorbents has a high cation exchange capacity to adsorb cationic heavy metal such as copper, zinc and nickel (Zhu et al. 2016).

Batch study

Effects of adsorbent dose on removal efficiency of bentonite, VAS-I, VAS-II and red earth are shown in Figs. 1, 2, 3 and 4, respectively. With increasing amount of adsorbents, increases removal of copper, nickel and zinc ions from AMD. Moreover, increasing amount of adsorbents results in increased available site in solution. Therefore, the adsorption of surface area increased for metal ions uptake (Karapinar and Donat 2009). In addition to the

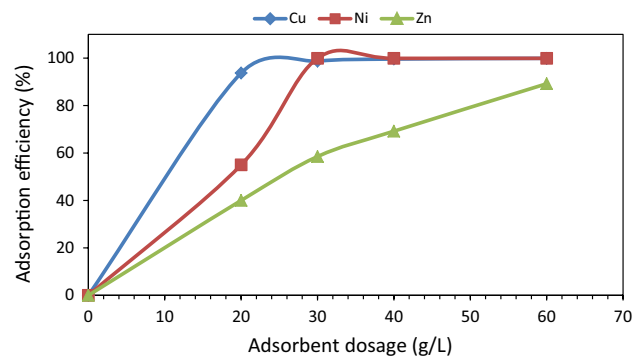


Fig. 1 Adsorption of heavy metals (copper, nickel and zinc) on bentonite

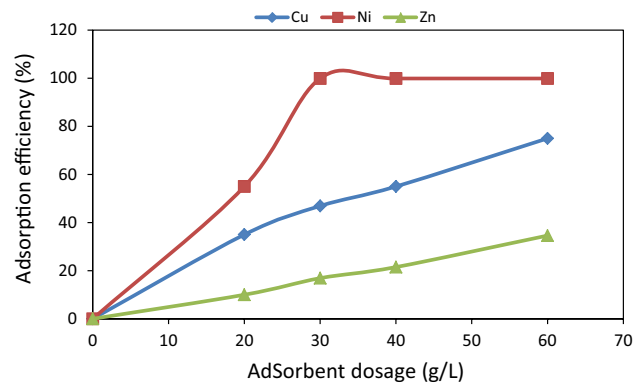


Fig. 2 Adsorption of heavy metals (copper, nickel and zinc) on VAS-I

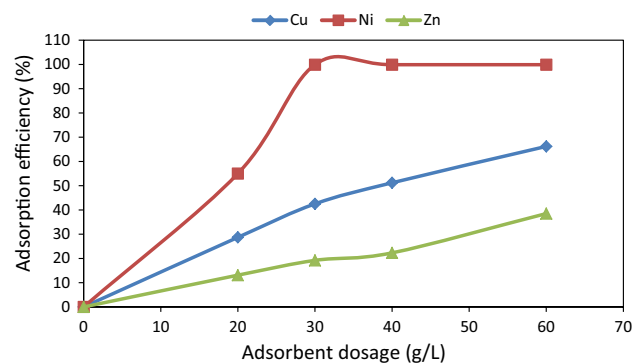


Fig. 3 Adsorption of heavy metals (copper, nickel and zinc) on VAS-II

removal of metal ions, neutralization process is occurred. Several investigators have confirmed these results (Jiang et al. 2006; Sen and Gomez 2011). Results showed that the order of capacity of adsorption by four types of minerals was: bentonite > red earth > volcanic ash soils. Type of natural clay mineral has a significant effect on the removal of heavy metal ions from water and wastewater (Malamis and Katsou 2013). In most cases, in addition

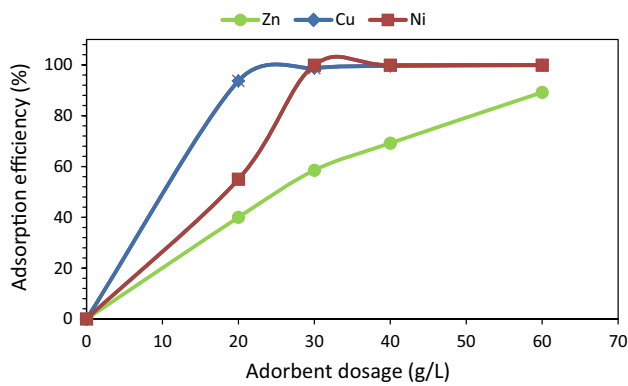


Fig. 4 Adsorption of heavy metals (copper, nickel and zinc) on red soil

to the ability of clay mineral for absorbent of metal ions, must be considers other characteristics of them. The most important properties are cost, efficiency, simplicity of operation, access to the adsorbent, the availability of materials, little sludge production, suitability for low concentrations, flexibility and excellence for continuous and batch operations (Božić et al. 2013; Eren et al. 2009; Vieira et al. 2010a). Sometimes can be increase the adsorption capacity by the chemical and thermal modification methods (Malamis and Katsou 2013). The results showed that red earth and bentonite have high capability for removing copper, zinc and nickel from AMD. The removal efficiency of copper, zinc and nickel by bentonite at dose 60 g/l was 99.9%, 89.2% and 99.9%, respectively. The adsorption affinity order of the metal ions by all sorbents was $Ni > Cu > Zn$. Many studies show which mineral type has deferment of capacity for the removal of heavy metal ions from aqueous solution (Malamis and Katsou 2013).

Also, the pH of the solutions increases with increasing amount of adsorbents. pH is one of the most important factors in adsorption metal ions from aqueous solution (Uddin 2017). pH of solution has significantly effects on the number of H^+ ions, the characteristic of clay minerals and chemistry of metal (Malamis and Katsou 2013). It has also the effect on the process of precipitation and formation of ligands (Saravanan et al. 2013). At low pH, there are a large number of H^+ ions in solution which compete with metal ions for active sites on the adsorbent; consequently, the removal of metals is less (Anirudhan et al. 2012; Jiang et al. 2010). With increasing pH, the number of H^+ ions is reduced and then the competition between H^+ ions and metal ions for adsorption sites decreased. Therefore, uptake of the heavy metals into adsorbents was increased (Eloussaief and Benzina 2010; Jiang et al. 2010; Saravanan et al. 2013).

Continuous study

In fixed-bed column studies, for the determination of dynamic and operation response the behavior of breakthrough curves is important; therefore, in these studies adsorption data are described by using breakthrough curves (Atar et al. 2012). Figures 5 and 6 show the breakthrough curves for ions of copper, zinc and nickel. According to Fig. 5, the critical concentration ($C/C_0 = 0.1$) of copper, zinc and nickel in the flow rate 0.8 ml/min is equal to 350, 160 and 170 min, respectively. In the flow rate 1.4 ml/min, the critical concentration of copper, zinc and nickel was reduced and almost became half of the previous flow rate.

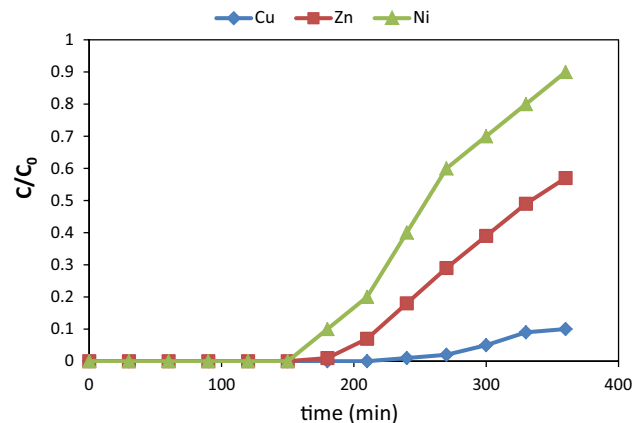


Fig. 5 Breakthrough curve for the adsorption copper, nickel and zinc on VAS-I (flow rate = 0.8 ml/min; $T = 27 \pm 1$ °C)

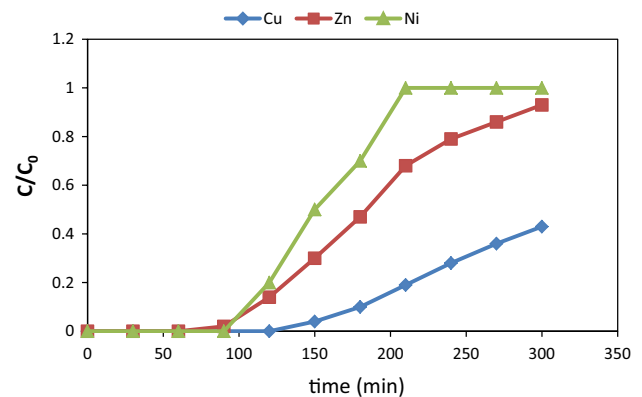


Fig. 6 Breakthrough curve for the adsorption copper, nickel and zinc on VAS-I (flow rate = 1.4 ml/min; $T = 27 \pm 1$ °C)

Conclusion

Results showed that the order of capacity of adsorption by four types of minerals is: bentonite > red earth > volcanic ash soils. The percentage of removal of copper, zinc and nickel by bentonite at dose 60 g/l was 99.9%, 89.2% and 99.9%, respectively. Also, in all tests the pH of final solution increased and neutralization process is occurred. The fixed-bed column tests showed that volcanic ash soils have the characteristics of simplicity of operation, little sludge production, suitability for low concentrations, flexibility and excellence for continuous and batch operations.

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Compliance with ethical standards

Conflict of interest The authors declare that they have no conflict of interest.

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