



Ultrasonic microwave-assisted extraction coupled with macroporous resin chromatography for the purification of antioxidant phenolics from waste jackfruit (*Artocarpus heterophyllus* Lam.) peels

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Abstract An efficient ultrasonic microwave-assisted extraction (UMAE) coupled with macroporous resin chromatography technique was successfully used for the extraction and purification of antioxidant phenolics from jackfruit by-products (peels). After optimization by single factor experiments and response surface methodology, the optimum extraction conditions for UMAE were: ethanol concentration 63%, solvent-to-solid ratio 34 mL/g, microwave power 160 W and irradiation time 20 min. Under the optimal condition, the phenolics extraction yield was 8.14 mg GAE/g DW. After the purification by macroporous resin AB-8, the purity of antioxidant phenolics from UMAE extracts improved from 13.59 to 49.07%. Furthermore, ABTS radical scavenging activities were also significantly increased from 35.95 ± 2.21 to 162.36 ± 10.26 mg TE/g. HPLC analysis revealed that gallic acid, chlorogenic acid, and catechin were three dominant antioxidant phenolics in jackfruit peels. All of the results demonstrated that waste jackfruit peels could be utilized as a good source of phenolics with strong antioxidant activities in food and pharmaceutical industry.

Keywords Jackfruit peels · Phenolics · Antioxidant · Ultrasonic microwave-assisted extraction · Response surface methodology · Macroporous resin

Introduction

Jackfruit (*Artocarpus heterophyllus*) is the largest fruit in the world, and mainly cultivated in and around tropical areas (Shyamamma et al. 2008). Jackfruit is rich in vitamins and minerals, and offers numerous health benefits (de Faria et al. 2009; Swami et al. 2012). After processing, jackfruit residues, e.g. peel, is usually discarded as a waste and prone to microbial spoilage, which was not only a waste of resource, but also pollution to the environment. Virtually, jackfruit by-products are still rich in beneficial substances with high added value, which may find application as ingredients in the food, feed, cosmetics, and pharmaceutical industries. In recent years, many polyphenolic compounds have exhibited various biological activities, including antioxidant (Balasundram et al. 2006), anti-inflammatory (Hsu et al. 2013) and antimicrobial activities (Alves et al. 2013), and so forth. However, to the best of our knowledge, few information is available about the phenolics from jackfruit by-products (peels).

Extraction of phenolics is one of the most imperative steps for both application and further research and development. Various efficient and advanced extraction methods have been investigated, such as super critical fluid (CO₂) extraction (SCFE), ultrasound-assisted extraction (UAE), and microwave-assisted extraction (MAE). However, these extraction techniques have drawbacks to some extent. For example, despite representing non-organic solvents residing as advantage, SCFE equipment is expensive with a high-energy consumption (Zhang and Liu 2008). Microwave-assisted extraction offers a rapid, clean, safe, and cost-effective method for heating that can cause a thermal effect by polarizing macromolecules, leading to alignment with electromagnetic field poles that may cause the breakage of hydrogen bonds, while its disadvantage is

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inhomogeneous heating (Lou et al. 2012; Liu et al. 2014). Ultrasound-assisted extraction relies on acoustic cavitation, which causes disruption of cell walls of plant materials, resulting in a more extensive release of internal cell compounds and a more homogeneous system (Pongmalai et al. 2015; Fan et al. 2015). Thus, ultrasonic microwave-assisted extraction (UMAE) may be an effective complementary technology for dramatically accelerating the extracting process, improving selectivity and simplifying manipulation (Xiao et al. 2012).

As for the separation and enrichment of phenolics, macroporous resins, with different physicochemical properties including specific surface area, pore diameter and polarity, have been successfully applied for the purification and enrichment of bioactive compounds from natural resources (Feng et al. 2015; Wang et al. 2013).

In the present study, UMAE technique was used as rapid and efficient extraction process for phenolics from jackfruit peels for high yields. Several processing parameters that could potentially influence the extraction efficiency were analyzed and optimized using RSM. Then, macroporous resin chromatography was employed to separate the crude extracts into six fractions with diverse phenolics contents and antioxidant activities. Finally, reverse phase high-performance liquid chromatography (RP-HPLC) method was established for qualitative identification and quantitative analysis of phenolics-enriched fractions.

Materials and methods

Samples

Fresh jackfruit fruits were purchased from local fruit center in Haikou City, Hainan Province of China. It was manually peeled and cut into small pieces (the moisture content for 84.5%), which were dried in a hot air oven at 60 °C for 48 h before being grinded and powdered (60 mesh).

Chemicals

ABTS [2,2'-azino-bis (3-ethylbenzthiazoline-6-sulfonic acid)] and Folin-Ciocalteu reagent were provided by Huadong Chemicals Co. (Hangzhou, China). Trolox, gallic acid, chlorogenic acid, catechin, rutin, quercetin, norartocarpetin and artocarpesin were obtained from Sigma Chemical Co. (St, Louis, MO, USA). Acetonitrile of HPLC grade was purchased from Merck (Darmstadt, Germany). The other chemical reagents were of analytical grade. Macroporous resins including HP20, D101, AB-8, NKA-II and S-8 were purchased from Nankai University Chemical Plant (Tianjin, China).

Ultrasonic and microwave assisted extraction

Phenolic compounds from powers of jackfruit (*A. heterophyllus* Lam.) peel were extracted using a domestic oven system (CW-2000, Shanghai Xin-tuo Microwave Instrument Co. Ltd., Shanghai, China). The apparatus was equipped with an open microwave with maximal power of 800 W at a frequency of 2450 MHz, and an ultrasonic transducer with a fixed power of 50 W at a frequency of 40 kHz. For each extraction, the pre-treated jackfruit peel powders (1 g) were weighed accurately and then transferred into the flask and proper volume (assigned according to the experimental design) of aqueous ethanol was added. Subsequently, the flask was transferred into the chamber of the apparatus connected with condensing tubes. Finally, the door of chamber was closed and the program of the parameters (microwave power and extraction time) according to the experiment planning was set for the extraction of phenolic compounds. When the extraction was accomplished, the flask was removed from apparatus and the resulting mixture was filtrated, then the volume of the filtrate and phenolic content in it were measured. Triplicate experiments were done for each design.

Response surface methodology (RSM)

Single-factor-test was employed to determination the preliminary range of the extraction variables including X_1 (ethanol concentration, %), X_2 (microwave power, W), X_3 (irradiation time, min) and X_4 (solvent-to-solid ratio, mL/g). Then, a three-level-four-factor Box–Behnken design (BBD) was conducted to determine the best combination of extraction variables for maximum recovery of total phenolic compounds (TPC) from jackfruit peels. Regression analysis was performed on the basis of the experimental data and fitted to a quadratic polynomial model presented in the following equation:

$$Y = \beta_0 + \sum_{i=1}^4 \beta_i X_i + \sum_{i=1}^4 \beta_{ii} X_i^2 + \sum_{i=1}^3 \sum_{j=i+1}^4 \beta_{ij} X_i X_j \quad (1)$$

where Y is the predicted response (the yield of TPC in mg gallic acid equivalents (GAE)/g dry weight (DW) basis); β_0 , β_i , β_{ii} , β_{ij} are the regression coefficients for intercept, linearity, square and interaction, respectively; X_i and X_j are the independent variables.

Design Expert software (Trial Version 8.0.5, Stat-Ease Inc., Minneapolis, MN, USA) was used to estimate the response of each set of experimental design and optimized conditions. The adequacy of the generated quadratic polynomial model was evaluated by the regression coefficient R^2 as well as the lack of fit using the F test. F value

and p value were used to check the significances of the regression coefficient.

Determination of total phenolics

Total phenolics (TPs) content of the extract from jackfruit peels were determined using Folin–Ciocalteu reagent, according to a procedure described by Altemimi et al. (2015). Briefly, 1.5 mL of properly diluted extract solution were mixed with 2 mL of Folin–Ciocalteu reagent and shaken vigorously. After incubation for 5 min, 2 mL of sodium carbonate solution (10% w/v) was added into the mixture, following by topping up the mixture to 25 mL with distilled water. After standing for 40 min in the dark at room temperature, the absorbance was measured at 760 nm using a UV–Vis spectrophotometer against a reagent blank without the extract. A calibration curve ($A = 0.0729 X + 0.0008$, $R^2 = 0.9985$) was established using standard solution of gallic acid (0–400 $\mu\text{g/mL}$). The results were expressed as mg of gallic acid equivalents (GAE) per gram of powder on dry weight basis.

Total antioxidant capacity assay

The total antioxidant capacity assay of the crude extract or fractions was determined with ABTS method, according to the procedure described by Mocan et al. (Mocan et al. 2014), with slight modifications. $\text{ABTS}^{+\cdot}$ radical solution was generated by mixing 7 mM ABTS solution with 2.45 mM potassium persulfate solution and was kept at room temperature in dark for 12–16 h. Then, the $\text{ABTS}^{+\cdot}$ radical solution was diluted with methanol to a final absorbance of 0.70 ± 0.02 at 734 nm to produce $\text{ABTS}^{+\cdot}$ working solution. 5 μL of samples or blank (distilled water) was rapidly added in corresponding wells of 96-microplate, followed by addition of 200 μL of $\text{ABTS}^{+\cdot}$ working solution to each well. After reaction for 5 min at 25 °C, the absorbance was measured at 734 nm by using the microplate reader. The percentage of ABTS consumption was converted to Trolox equivalents (TE) using a calibration curve with Trolox standard solutions of 10–400 mg/L. The higher the rate of ABTS consumption is, the stronger the antioxidant capacity.

Static adsorption/desorption tests for screening of resins

In the static adsorption/desorption experiments, each of pretreated hydrated adsorbents (equal to 1 g of dry resins) was put into a conical flask (100 mL) with stopper, followed by the addition of 40 mL of crude extract solutions to each flask. Then, the flasks were continually shaken (120 rpm) in a thermostatic oscillator (TOPT-1102, Xi'an Toption

Instrument Co., Ltd., China) at 30 °C for 24 h. After adsorption equilibrium, the resins were washed with distilled water twice and then desorbed with 30 mL of 90% (v/v) ethanol solution. The total phenolics content of supernatants before and after desorption was determined.

The adsorption capacity, adsorption ratio and desorption ratio of different resins were calculated according to following equation:

$$Q_e = \frac{(C_0 - C_e)V_a}{W} \quad (2)$$

$$E = \frac{(C_0 - C_e)}{C_0} \times 100 \quad (3)$$

$$D = \frac{C_d V_d}{(C_0 - C_e)V_a} \times 100 \quad (4)$$

where Q_e is the adsorption capacity (mg/g dry resin); C_0 and C_e are the initial and equilibrium concentrations of phenolics in the solutions, respectively (mg/mL); V_a is the volume of phenolics solution (mL) and W is the weight of the dry resin used (g); E and D is the adsorption ratio (%) and desorption ratio (%), respectively; C_d is the concentration of phenolics in the desorption solution (mg/mL); V_d is the volume of the desorption solution (mL).

Purification of phenolics by resin column

Purification experiments were carried out on a glass column (300 mm \times 25 mm i.d.) packed with the selected resin. The bed volume (BV) of the wet-packed resin was 120 mL. 1 g of jackfruit peels extract was dissolved in 20 mL of distilled water and carefully applied to the column. After adsorption equilibrium, the column was firstly washed with distilled water to remove water soluble impurities such as sugar, protein, pigment and other water-soluble molecules, and then sequentially eluted with 3 BV of 10%, 30%, 50%, 70% and 90% (v/v) ethanol solution at a constant flow rate of 2 mL/min. Each fraction was collected, evaporated in vacuum, and then freeze-dried. The fractions were weighed and stored at -18 °C until the evaluation of their total phenolics content and antioxidant capacity was performed.

HPLC–DAD analysis

The HPLC analysis of the sample obtained under optimal conditions was performed on an Agilent 1260 Series HPLC System equipped with a quaternary pump, a diode array detector (DAD) and a autosampler (Agilent, Palo Alto, CA, USA). Chromatographic separation was accomplished with a AichromBond C18 analysis column (250 \times 4.6 mm, 5 μm , Agilent, Palo Alto, CA, USA). The mobile phase was composed of acetonitrile (A) and 0.1% formic acid

aqueous solution (B) with a detecting wavelength at 280 nm. The mobile phase gradient was programmed as follows: 0–5 min, 8% A; 5–15 min, 8–35% A; 15–20 min, 35–42% A; 20–25 min, 42–55% A; 25–35 min, 55–60% A; 35–40 min, 60–8% A. The flow rate was set to 1 mL/min and the injection volume was 5 μ L. The phenolic compounds present in the samples were tentatively identified by comparing their retention times with those of the reference standards, while the quantitative determination was performed with the external standard method.

Results and discussion

Single factor experiment

Effect of ethanol concentration

In order to evaluate the effect of ethanol concentration on phenolics extraction yield, extraction process was carried out at various ethanol concentration (30–70%) and the results were shown in Fig. 1. The yield of phenolics increased first and then reduced with the further increase of ethanol concentration, and reached the maximum (6.68 mg GAE/g) at 60% ethanol aqueous solution. It was reported that water is acted as the plant swelling agent, while ethanol is believed to disrupt the bonding between the target components and plant matrices (Liu et al. 2013). Water and low ethanol concentration can easily pass through the cell membranes, but a high ethanol concentration can cause protein denaturation, preventing the dissolution of phenolics and then resulting in the decrease of mass transfer (Dahmoune et al. 2015). Hence, the ethanol concentration of 60% was suitable for the extraction of phenolics.

Effect of solvent-to-solid ratio

The ratio of solvent to solid also played a potentially important parameter for efficient extractions. If the ratio of solvent to solid was too small, phenolics in plant tissue cannot be completely dissolved out and released into the extraction medium. Conversely, if the ratio of solvent to solid is too high, it will cause high process cost (Zou et al. 2011). In this study, the effect of ratio of solvent to solid on extraction yield of phenolics from jackfruit peels was investigated, and the results were listed in Fig. 1. It could be founded that the extraction yield of phenolics continued to increase evidently with the increase of ratio of solvent to solid, and reached to a maximum value at 30 mL/g. However, as the ratio exceeded 30 mL/g, the extraction yields were almost constant regardless of increase of ratio of solvent to solid. Considering the saving of solvent and

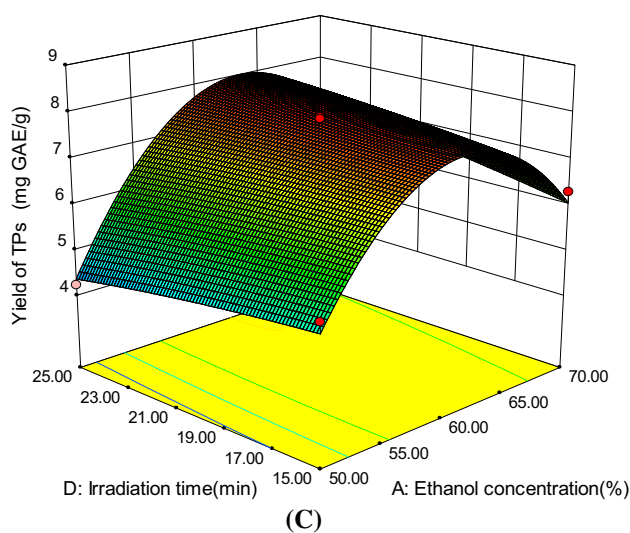
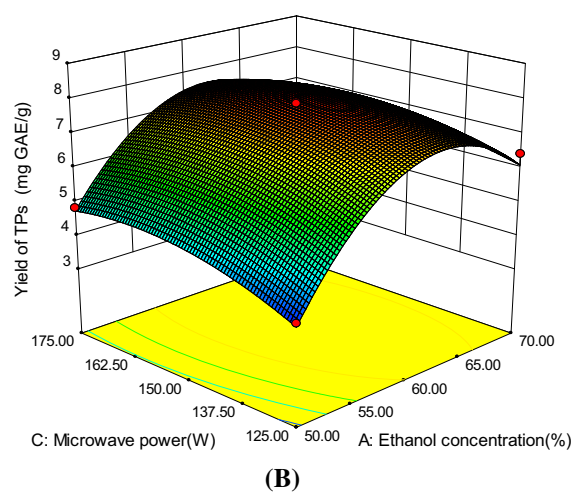
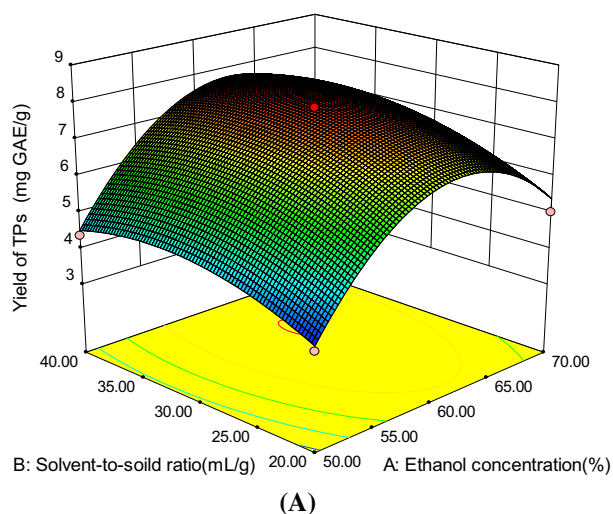


Fig. 1 Response surface plots (a–f) showing the interaction effects of ethanol concentration (X_1), solvent/solid (X_2), microwave power (X_3), and irradiation time (X_4) on the extraction yield of phenolics from jackfruit peels

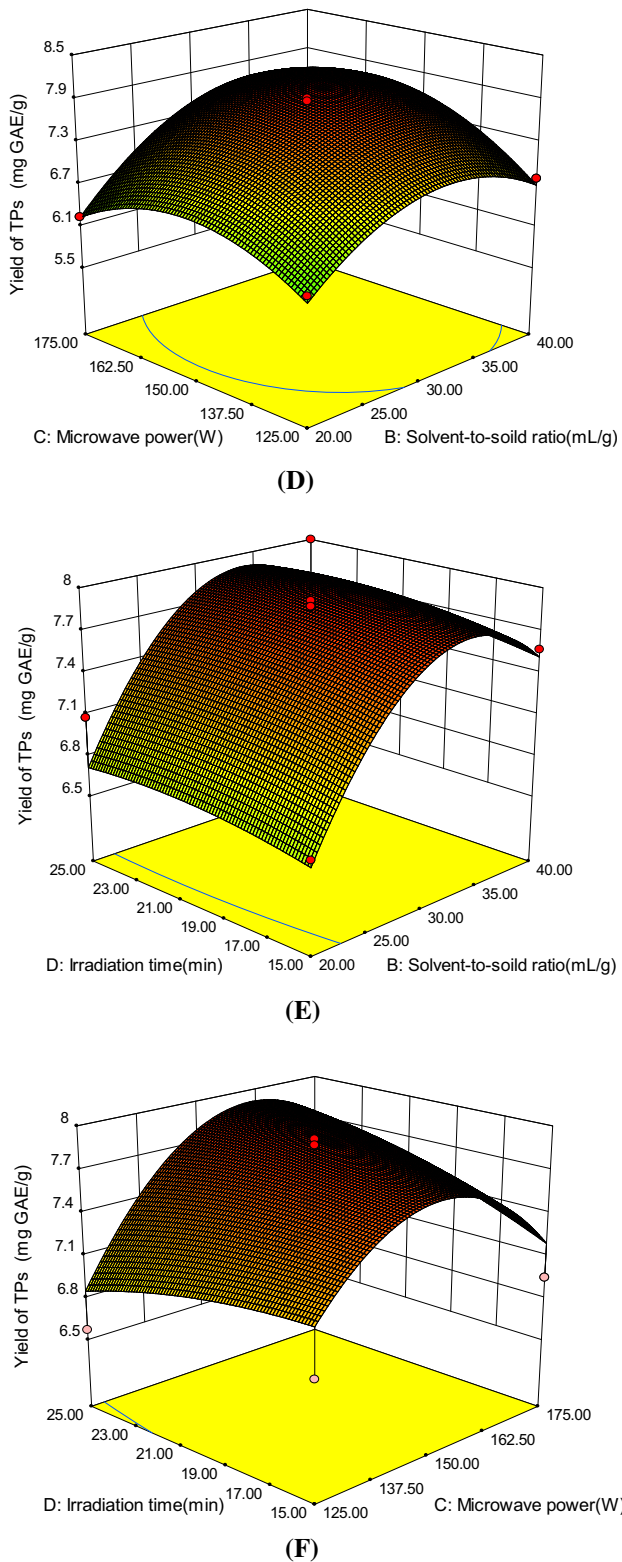


Fig. 1 continued

easy operation, the ratio of 30 mL/g was used as the following optimized experiments.

Effect of microwave power

The effects of microwave power on the yield of phenolics from jackfruit peel were investigated at levels ranging from 50 to 200 W. As shown in Fig. 1, the yield of phenolics increased with the increase of microwave power at the beginning of extraction, and reached the maximum (7.30 mg GAE/g) at 150 W. It could be due to the fact that microwave absorption causes fast internal heating, thus generating significantly high internal pressures in plant material. This causes the cell walls to swell and burst, thus promoting the release and dissolution of target components into the solvent (Lu et al. 2011). However, an evident decrease in the extraction yield of phenolics was observed beyond 150 W. This might be attributed to the thermal degradation of the phytochemicals at higher microwave output power levels. The findings were similar with the research results reported by Ahmad and Langrish (2012). Therefore, microwave power level 150 W was selected for further RSM optimization.

Effect of irradiation time

Generally speaking, by increasing the irradiation time, the quantity of target compounds extracted is increased, although there a risk of degradation of extracted active compounds. In the present study, the yield of phenolics was investigated at various irradiation times (5–25 min). As shown in Fig. 1, the first increase of irradiation time within 5–15 min resulted in a significant increase of phenolics yield, and then the further increase of irradiation time led to the decrease of phenolics yield beyond 15 min. The findings indicated that prolonging irradiation time was not in favor of the yield of phenolics, possibly due to the chemical structural destruction and the decomposition of active compounds in longer exposure periods (Sun et al. 2011). As a result, 15 min was an appropriate irradiation time for further UMAE experiments.

Optimization of UMAE by RSM

Statistical analysis and the model fitting

BBD with four factors and three levels were employed to optimize the mutual effect of four independent variables (ethanol concentration, solvent-to-solid ratio, microwave power and irradiation time) on the extraction yield of phenolics. Table 1 showed the design matrix and the extraction yields of phenolics. By applying multiple regression analysis on the experimental data, the response variable and the independent variables could be related using the following second-order equation:

Table 1 Box–Behnken design with the experimental result for ultrasonic microwave-assisted extraction (UMAE) method

Run	Ethanol X_1 (%)	Solvent/solid X_2 (mL/g)	Microwave power X_3 (W)	Irradiation time X_4 (min)	Yield (mg GAE/g)
1	– 1 (50)	0 (30)	1 (175)	0 (15)	4.84
2	– 1	0	0 (150)	1 (20)	4.23
3	0 (60)	0	1	– 1 (10)	6.95
4	0	– 1 (20)	– 1 (125)	0	6.25
5	0	1 (40)	– 1	0	6.79
6	0	0	0	0	7.79
7	1 (70)	0	1	0	6.36
8	0	0	– 1	1	6.57
9	– 1	0	0	– 1	5.33
10	0	0	1	1	7.54
11	1	1	0	0	6.12
12	1	0	0	1	6.88
13	0	– 1	0	– 1	6.66
14	0	1	0	1	8.01
15	0	1	1	0	7.54
16	0	1	0	– 1	7.57
17	– 1	1	0	0	4.37
18	0	0	0	0	7.91
19	0	0	– 1	– 1	6.83
20	0	– 1	1	0	6.24
21	0	0	0	0	7.87
22	0	– 1	0	1	7.08
23	0	0	0	0	7.73
24	– 1	0	– 1	0	3.88
25	– 1	– 1	0	0	3.64
26	1	0	0	– 1	6.3
27	0	0	0	0	7.87
28	1	– 1	0	0	5.03
29	1	0	– 1	0	6.43

$$\begin{aligned}
 Y = & 7.83 + 0.90X_1 + 0.46X_2 + 0.23X_3 + 0.056X_4 \\
 & + 0.090X_1X_2 - 0.26X_1X_3 + 0.42X_1X_4 + 0.19X_2X_3 \\
 & + 5.0 \times 5.0^{-3}X_2X_4 + 0.21X_3X_4 - 2.13X_1^2 \\
 & - 0.65X_2^2 - 0.53X_3^2 - 0.067X_4^2
 \end{aligned}
 \tag{5}$$

Statistical testing of the developed model was performed in the form of analysis of variance (ANOVA) by software of Design-Expert 8.0.5. The ANOVA for the experiment results are listed in Table 2. High F value ($F = 34.55$) with a very low p value ($p < 0.0001$) suggested that the developed model was statistically significant, demonstrating that the extraction yield of TPs could be well predicted within the variable range employed with the model. Significance of the fitted model was also judged by lack-of-fit (Ji et al. 2012). As shown in Table 2, F value ($F = 24.45$) and

p value ($p = 0.0537$) of the lack of fit implied that it was not significant relative to the pure error, which further confirmed that the fitted model adequately represented the experimental results under any combination of values of the variables during UMAE. The value of the determination coefficient (R^2) evaluated from the second-order regression model was 0.9719, while the value of adjusted R-square (R_{adj}^2) was 0.9437, indicating a good degree of correlation between the actual and predicted values (Firatligil-Durmus and Evranuz 2010). At the same time, the relatively low value of coefficient of variation (C.V. = 4.76%) demonstrated a high degree of precision and good reliability of the experimental results. It is widely accepted that a model should be considered reasonably reproducible if the C.V. value is lower than 10% (Karabegović et al. 2013). All these results above suggested that

Table 2 Analysis of variance for the fitted quadratic polynomial equation of extraction of phenolics

Source	Sum of squares	df	Mean square	F value	p value
Model	45.34	14	3.24	34.55	< 0.0001**
X ₁	9.77	1	9.77	104.29	< 0.0001**
X ₂	2.52	1	2.52	26.90	0.0001**
X ₃	0.62	1	0.62	6.58	0.0225*
X ₄	0.037	1	0.037	0.40	0.5377
X ₁ X ₂	0.032	1	0.032	0.35	0.5659
X ₁ X ₃	0.27	1	0.27	2.83	0.1147
X ₁ X ₄	0.71	1	0.71	7.53	0.0158*
X ₂ X ₃	0.14	1	0.14	1.54	0.2349
X ₂ X ₄	0.0001	1	0.0001	0.0011	0.9744
X ₃ X ₄	0.18	1	0.18	1.93	0.1868
X ₁ ²	29.54	1	29.54	315.20	< 0.0001**
X ₂ ²	2.72	1	2.72	29.05	< 0.0001**
X ₃ ²	1.84	1	1.84	19.65	0.0006**
X ₄ ²	0.029	1	0.029	0.31	0.5884
Residual	1.31	14	0.094		
Lack of Fit	1.29	10	0.13	24.45	0.0537
Pure Error	0.021	4	0.0053		
Cor. Total	46.65	28			

$R^2 = 0.9719, R_{adj}^2 = 0.9437, C.V. = 4.76\%$

* $p < 0.05$; ** $p < 0.01$

the fitted model could work well for the prediction of TPC extract from jackfruit peels.

The *F* and *p* values are used as a tool to confirm the significance of each coefficient. The smaller the *p* value, the more significant the corresponding coefficient (Wu et al. 2015). According to the *p* and *F* values (Table 3), the linear coefficients (*X*₁, *X*₂ and *X*₃), quadratic term coefficients (*X*₁², *X*₂² and *X*₃²) and cross product coefficients (*X*₁*X*₄) were significant, with very small *p* value (*p* < 0.05). Meanwhile, the ethanol concentration was the most significant factor affecting the extraction yield of phenolics.

Optimization of extracting parameters and validation of the model

According to regression model, the optimum conditons were ethanol concentration 62.93%, solvent-to-solid ratio 34.39 mL/g, microwave power 160.49 W and irradiation time 20 min. Under above conditions, the model predicted

a maximum response of 8.21 mg GAE/g DW. Considering the actual operability, the optimized condition was modified as following: ethanol concentration 63%, solvent-to-solid ratio of 34 mL/g, microwave power of 160 W and irradiation time 20 min. To validate the suitability of the model equation, a verification experiment was carried out. In the verification experiment, the average yield of phenolics was 8.14 mg GAE/g DW (n = 3), which was no significant difference from the predicted value within the 95% confidence interval. This good correlation confirmed that the response model was adequate for reflecting the expected optimization.

Selection of macroporous adsorption resin

Static adsorption and desorption tests were investigated in order to select appropriate macroporous resins. The macroporous adsorption resins exhibit higher adsorption capacity not only because of their similar polarity with the

Table 3 Adsorption capacities and desorption ratio of phenolics on macroporous resins

Grade	Adsorption capacity (mg g ⁻¹)	Asorption ratio (%)	Desorption ratio (%)
HP20	34.23 ± 2.01	43.29 ± 2.34	91.81 ± 4.21
D101	33.03 ± 1.26	38.07 ± 2.70	90.56 ± 3.34
AB-8	41.67 ± 1.83	54.90 ± 1.98	94.20 ± 4.52
NKA-II	29.07 ± 1.26	45.09 ± 1.71	87.23 ± 3.26
S-8	44.37 ± 2.58	58.68 ± 3.06	37.66 ± 1.61

target compounds, but also because of their higher surface area and larger average pore diameter (Lin et al. 2012). Furthermore, phenolics possessing hydrogen groups and benzene rings, could be adsorbed by weak-polar or polar resins with appropriate surface area and average pore diameter. Therefore, five sorts of commonly used commercial macroporous resins, varying from non-polarity to polarity, were tested to acquire the most suitable resin for adsorbing and separating phenolics from jackfruit peels. The adsorption capacities and desorption ratios of the resins are depicted in Table 3. Results demonstrated that among five resins, AB-8 and S-8 exhibited considerably high adsorption capacities (41.67 and 44.37 mg TP g⁻¹ resin, respectively) and adsorption ratios (54.90% and 58.68%, respectively). But as far as desorption ratio, it was very low for S-8 (37.66%) which was likely attributed to its strong polarity and adsorbability, which inevitably led to difficult desorption of phenolics, while it was comparatively high for AB-8 (94.20%). The polarity differences between AB-8 and S-8 is due to the result of different polar groups on their structural surfaces, which results in their distinctly different desorption abilities (He and Xia 2008). AB-8 exhibited moderate polarity compared with S-8. As a result, AB-8 resin possessed a relatively higher adsorption selectivity for phenolics in the complex extract solution as well as higher desorption ratio. Thus, AB-8 resin was selected as an appropriate macroporous resin for the enrichment and separation of phenolics.

Purification of phenolics by resin column

The purification of phenolics was performed by the adsorption of resin and desorption of aqueous ethanol. As shown in Table 4, the majority of the phenolics adsorbed by AB-8 resin were obtained when desorption agents of 30% and 50% ethanol solution were used. The total phenolics accounted for over 40.51% and 57.22% in the 30% and 50% ethanol fractions, respectively. In addition, the

substances with excellent antioxidant ability were also found in the 30% and 50% ethanol fractions obtained from AB-8 resin column, especially in 50% ethanol fraction. The ABTS⁺ radical scavenging capacity of the 30% and 50% ethanol fractions were 3.06–4.52 times higher than that of original crude extract. The results demonstrated that the total phenolics content in jackfruit peels extract had a significant correlation with its antioxidant capacity. Consequently, AB-8 could be used as effective macroporous resin for the purification of antioxidant phenolics from waste jackfruit peels. The phenolic-enriched fractions, namely 30% and 50% ethanol fractions, were combined, concentrated and freeze-dried for further HPLC–DAD analysis.

HPLC–DAD analysis

Due to the fact that phenolics usually exist in complex plant matrices together with a large variety of other phytochemicals, the direct analysis of phenolics from complex extracts is a challenging task. Thus, the macroporous resin chromatography, with high adsorption capacity, good stability and easy regeneration, was used for purification of phenolics from original crude extracts of jackfruit peels. As shown in Fig. 2, Gallic acid, chlorogenic acid, catechin were identified in the extract of jackfruit peels by comparing the retention times with authentic standards. The amount of individual phenolics (expressed as mg g⁻¹ of dried plant) were as follows: 0.68 ± 0.01 Gallic acid, 2.53 ± 0.04 chlorogenic acid, 0.56 ± 0.01 catechin in jackfruit peels. The results revealed that chlorogenic acid was the dominant phenolic compound in jackfruit peels. Chlorogenic acid has been documented to effectively scavenge free radicals and improve antioxidant defenses in humans and animals (Sun et al. 2015), and might be mainly responsible for the antioxidant activity of enriched phenolic extract from jackfruit peels.

Table 4 Results of the gradient elution of phenolics by AB-8 resin column

Macroporous resin	Ethanol concentration (%)	Mass of dried mass (mg)	Content of phenolics (%)	ABTS (mg TE/g)
AB-8	Water fraction	401.2 ± 14.1	4.21 ± 0.62	10.14 ± 0.65
	10	60.5 ± 7.2	9.33 ± 0.45	20.26 ± 1.12
	30	92.1 ± 8.3	57.22 ± 3.54	162.36 ± 10.26
	50	87.7 ± 6.2	40.51 ± 2.67	109.94 ± 7.23
	70	69.4 ± 5.6	7.34 ± 0.41	17.42 ± 1.22
	90	17.6 ± 1.3	5.42 ± 0.35	9.76 ± 0.89
	Recovery yield (%)	72.8	85.93	
Original crude extract			13.59 ± 0.68	35.95 ± 2.21

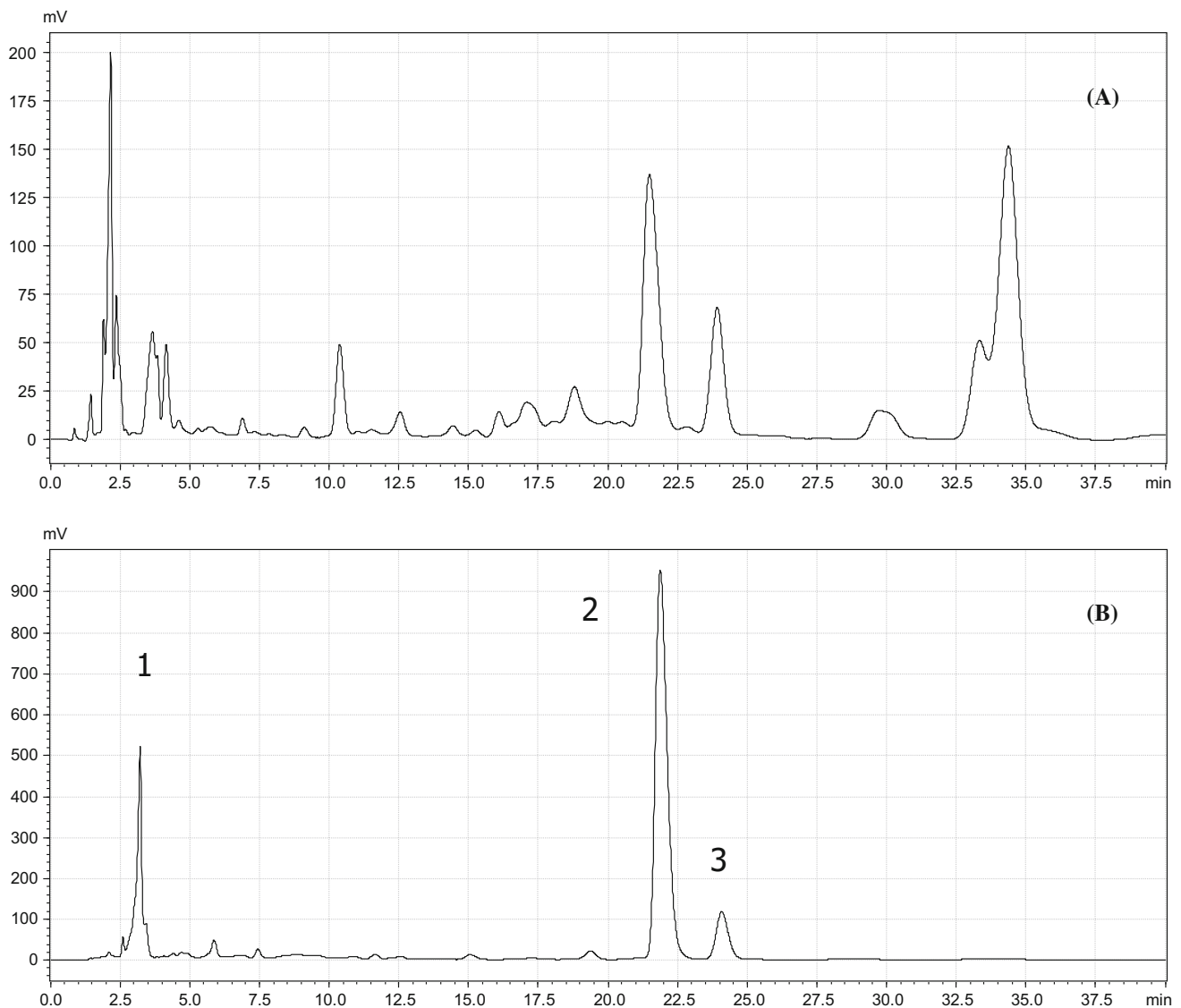


Fig. 2 HPLC chromatography of crude and fractionated extracts (a, the crude extract; b, the purified fraction by AB-8 resin) obtained from jackfruit peels. Peak: (1) Gallic acid, (2) chlorogenic acid, (3) catechin

Conclusion

An efficient extraction and purification technique based on ultrasonic microwave-assisted extraction method combining macroporous resin chromatography was established to obtain phenolics-rich fraction from jackfruit by-products. The final results demonstrated that the optimum extraction conditions for UMAE were: ethanol concentration 63%, solvent-to-solid ratio of 34 mL/g, microwave power of 160 W and irradiation time 20 min. Under the optimal extraction conditions, the phenolics extraction yield was 8.14 mg GAE/g DW. The best macroporous resin for the purification of phenolics was AB-8 resin. After the purification by macroporous resin chromatography, the purity of phenolics in the crude extracts improved from 13.59 to

49.07%. HPLC–DAD analysis revealed that chlorogenic acid was the dominant phenolic compound in jackfruit peels. Furthermore, total phenolics content showed good correlations with antioxidant activities, indicating that waste jackfruit peels could be utilized as a good source of phenolics with strong antioxidant activities for food and pharmaceutical industry. The study provides a new way for utilization of waste jackfruit peels. These results could be helpful in the development of large-scale batch adsorption–desorption system for use in the production of antioxidant phenolics from jackfruit peels.

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