

# Elevated critical micelle concentration in soil–water system and its implication on PAH removal and surfactant selecting

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**Abstract** Triton X-100 (TX100) and Brij 35 (B35) were used to investigate the elevated critical micelle concentration (CMC) induced by surfactant sorption and its influence on PAH removal in soil washing systems. The surface tension technique was applied to determine the CMC and the apparent CMC ( $CMC_{soil}$ ) in soil–water systems. Surfactant sorption experiments were conducted by the batch equilibration technique. Surfactants sorbed on the soil at concentrations below the  $CMC_{soil}$  were quantified with data from the surface tension experiments for both an aqueous system and a soil–water system. Due to sorption, the  $CMC_{soil}$  values of the two surfactants are 2.75 and 6.31 times their corresponding CMC values in aqueous solutions, respectively. At concentrations below  $CMC_{soil}$ , the loss of B35 (92–99.7 %) was greater than that of TX100 (63–92 %). The PAH removal efficiencies are greatly dependent on the  $CMC_{soil}$  value. At surfactant concentrations below  $CMC_{soil}$ , the PAH removal is very low and

remains almost invariable. Whereas, at concentrations above  $CMC_{soil}$ , the PAH removal increases greatly. B35 inhibited PAH desorption at concentrations below its  $CMC_{soil}$ . For TX100, some degree of PAH desorption enhancement was observed at concentrations below its  $CMC_{soil}$ .  $CMC_{soil}$  is a key parameter while selecting a surfactant for a specific soil washing system, only surfactant concentrations above their  $CMC_{soil}$  should be evaluated.

**Keywords** Surfactant · Soil washing · PAHs · Sorption/Desorption · Apparent critical micelle concentration

## Introduction

Polycyclic aromatic hydrocarbons (PAHs) are ubiquitous pollutants in the environment, and are mainly derived from anthropogenic activities, such as biomass burning, incomplete fossil fuel combustion, oil spills and some industrial processes (Bernardez 2008; Nganje et al. 2012; Wang et al. 2012; Tay and Biney 2013). Among which coal processing is one of the most important sources of PAHs. Soils from many sites such as areas of coal storage, coke oven plants, manufactured gas plants, and areas of coal tar spillage are highly contaminated by PAHs (Paria and Yuet 2006; Viglianti et al. 2006). These contaminated sites pose risks to the human and the environment, especially those located in urban areas that have been abandoned by pollution intensive industries (Sousa 2001). Due to their known or potential genotoxicity and carcinogenicity, remediation of these PAH-contaminated sites has been always a major environmental concern (Woo et al. 2001; Ahn et al. 2008, Guo et al. 2013).

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Many technologies have been used to remediate PAH-contaminated soils such as bioremediation (Hughes et al. 1997), phytoremediation (Huesemann et al. 2009), chemical oxidation (Alderman et al. 2007), photocatalytic degradation (Zhang et al. 2008), and electrokinetic remediation (Reddy et al. 2006). Compared with the forenamed techniques, soil washing provides an effective and relatively low cost alternative for the remediation of PAH-contaminated soil. Due to their hydrophobic nature, PAHs are strongly sorbed to soil. As a consequence, the remediation of PAHs in soil–water systems depends strongly on their desorption rates from the soil surface and the subsequent incorporation of the pollutant into the bulk aqueous phase (Jin et al. 2007; Din et al. 2009). Surfactants have frequently been used to enhance desorption of PAHs from soil and the subsequent transfer into water through solute solubilization into aqueous micelles (Paterson et al. 1999; Yuan and Marshall 2007; Alcantara et al. 2009; Petitgirard et al. 2009). Surfactant-enhanced remediation has been suggested as a promising technology for the remediation of contaminated soils and groundwater (Harwell et al. 1999; Mulligan et al. 2001).

Nonionic surfactants can sorb onto soil to some extent, and anionic surfactant will precipitate with divalent cations in soils (e.g.,  $\text{Ca}^{2+}$ ,  $\text{Mg}^{2+}$ ) (Wang and Keller 2009). Understanding the sorption characteristics of the surfactant can greatly assist in designing and optimizing the surfactant-enhanced remediation technologies (Grasso et al. 2001; Zhu and Zhou 2008). In a soil–water system, the surfactant dose required for micelle formation is greater owing to surfactant sorption, which results in a higher measured CMC for soil–water systems compared to the CMC in aqueous solutions. This elevated CMC is referred to the apparent CMC and is denoted by  $\text{CMC}_{\text{soil}}$  in this paper. Former researches have demonstrated that surfactants can significantly enhance PAH desorption only at concentrations above their  $\text{CMC}_{\text{soil}}$  (Grasso et al. 2001; Zhu and Zhou 2008). Sorbed surfactant may account for the majority of added surfactant in surfactant amended remediation applications, and this may result in increased hydrophobic organic compound (HOC) partitioning onto soil until HOC solubilization by micellar phase surfactant successfully competes with increased HOC sorption on surfactant-modified soil (Zhou and Zhu 2008; Laha et al. 2009).

In this study, Triton X-100 (TX100) and Brij 35 (B35) were used to facilitate desorption of PAHs from aged-contaminated soils. The objectives of this research were (1) to investigate the surfactant loss due to sorption, and its influence on PAH removal efficiency; and (2) to evaluate the elevated CMC induced by surfactant sorption and its implication on surfactant selecting for soil washing systems.

## Materials and methods

### Study site and sample collection

The soil used in this study was collected from a former coke oven plant in Beijing, China, which mainly produced coke, coal gas, coke tar and some other coal chemical products. The contamination of this site is about 50 years. Before the start of the 2008 Olympic Games, Beijing coke oven plant was moved out to other city in order to improve the environmental quality. The contaminated land needs to be remediated according to laws before its reuse. 15 sample sites in horizontal direction and three sample sites in vertical direction (from 0 to 2.5 m below the ground surface) were set to get representative soil samples. Oversize materials were removed. Individual samples were mixed for purpose of treatability study for soil washing. The mixed samples were air-dried. Particles that passed through a 2-mm sieve were used for subsequent experiment. Selected physical and chemical properties of the soil samples are listed in Table 1. The initial PAH concentrations are shown in Table 2.

### Chemical reagents

TX100 and B35 were purchased from Amresco. They were selected due to their wide use in soil washing systems. All the surfactants were used as obtained without further purification. 16 US EPA priority PAHs standard mixture consisted of naphthalene (Nap), acenaphthylene (Acy), acenaphthene (Ace), fluorene (Flu), phenanthrene (Phen), anthracene (Ant), fluoranthene (FlA), pyrene (Pyr), benzo[a]anthracene (BaA), chrysene (Chr), benzo[b]fluoranthene (BbF), benzo[k]fluoranthene (BkF), benzo[a]pyrene (BaP), indeno[1,2,3-cd]pyrene (InP), dibenzo[a,h]anthracene (DBA), benzo[g,h,i]perylene (BgP) and deuterated surrogate naphthalene- $\text{d}_8$ , phenanthrene- $\text{d}_{10}$ , chrysene- $\text{d}_{12}$  and Perylene- $\text{d}_{12}$  were obtained from AccuStandard, and internal standard of hexamethylbenzene was obtained from Sigma. Alumina (100–200 mesh), silica gel (80–100 mesh), anhydrous sodium sulfate, diatomite, and copper powder were analytical grade obtained from Beijing Chemical Reagents Company (China). All solvents used for sample processing and analysis (dichloromethane, acetone, hexane and ethanol) were HPLC grade purchased from J.T. Baker. Deionized water was produced by a Milli-Q system (Millipore).

### Surface tension measurements

The surface tension technique was applied to determine the CMC and the  $\text{CMC}_{\text{soil}}$ . The surface tension measurements were carried out with a tensiometer (JWY-200A, Beijing

**Table 1** Selected physiochemical properties of soil samples

Initial water content (%)	pH	TOC (%)	CEC (Cmol kg <sup>-1</sup> )	Soil texture (%)			
				Gravel	Sand	Silt	Clay
3.0	8.0	0.5	9.7	0.03	82.92	12.80	4.25

**Table 2** Initial PAH concentrations in soil

PAH	Average concentration (mg kg <sup>-1</sup> )	Standard deviation
Nap	0.380	0.145
Acy	0.357	0.011
Ace	0.097	0.015
Flu	0.419	0.007
Phe	2.395	0.190
Ant	0.635	0.261
FlA	3.969	0.276
Pyr	3.298	0.035
BaA	2.195	0.174
Chr	2.222	0.232
BbF	3.476	0.008
BkF	2.040	1.303
BaP	1.992	0.094
InP	2.381	0.013
DBA	0.595	0.045
BgP	2.317	0.041
Σ16PAHs	28.769	2.757

Jinshengxin Testing Machine) following the method of Grasso et al. (2001). Triplicate measurements were made for each sample, which was comprised of surfactant solutions and filtered supernatant from a centrifuged soil-aqueous system. The samples were tested in increasing concentrations and the ring was rinsed with deionized water between samples.

Sorption of surfactants on the soil

Surfactant sorption experiments were conducted in duplicate by the batch equilibration technique. Surfactant solutions were prepared in 0.02 % sodium azide using deionized water. 30-mL surfactant solution was added to 3.0 g of soil sample in 50-mL Teflon centrifuge tubes. The tubes were equilibrated on a reciprocating shaker at 150 rpm and 30 °C for 48 h. Then the soil suspensions were centrifuged at 10,000 rpm for 15 min. A 20 mL aliquot of supernatant was removed to measure the surface tension. Surfactants sorbed on the soil at a concentration lower than the CMC<sub>soil</sub> were quantified from the surface tension experiments described above for both an aqueous system and a soil–water system.

PAH desorption with surfactants

Polycyclic aromatic hydrocarbon desorption experiments were carried out in duplicate by the batch equilibration technique. Surfactant solutions were prepared in 0.02 % sodium azide using deionized water. 30-mL surfactant solution was added to 3.0 g of contaminated soil in 50-mL Teflon centrifuge tubes. The tubes were equilibrated on a reciprocating shaker at 150 rpm and 30 °C for 48 h. Then the soil suspensions were centrifuged at 10,000 rpm for 15 min. A 20-mL aliquot of supernatant was removed to extract PAHs for analysis.

PAH extraction and analysis

Polycyclic aromatic hydrocarbons in the original soil samples were extracted with acetone and dichloromethane mixture (1:1, v:v) using an Accelerated Solvent Extractor (ASE 300, Dionex Corp.). 1.0 g of dried, homogenized soil sample was mixed with diatomite and activated copper powder, then filled into the stainless steel extraction cells. Prior to extraction, the soil was spiked with 1-mL (4 mg L<sup>-1</sup>) deuterated recovery surrogate standards of naphthalene-d<sub>8</sub>, phenanthrene-d<sub>10</sub>, Chrysene-d<sub>12</sub>, Perylene-d<sub>12</sub>. The extracts were concentrated to nearly dryness by rotary evaporation and changed solvent to hexane for further chromatographic separation.

A 20-mL aliquot of surfactant solution containing dissolved PAH compounds was extracted with 3 × 20 mL hexane. Ethanol was added to break the hexane-surfactant emulsion. Deuterated PAH surrogate standards naphthalene-d<sub>8</sub>, phenanthrene-d<sub>10</sub>, chrysene-d<sub>12</sub> and Perylene-d<sub>12</sub> were added to monitor the procedures of cleanup and analysis.

Polycyclic aromatic hydrocarbons in concentrated hexane extract were separated using a 2:1 silica gel/Alumina glass chromatography column (1.0 × 30 cm) with 1-g anhydrous sodium sulfate overlaying the Alumina to remove small quantities of water (Guo et al. 2013). First, 15 mL of hexane was used to remove the aliphatic hydrocarbons, the eluate was discarded. Then PAHs were eluted with 70-mL hexane/dichloromethane (7:3, v:v), the eluate was collected in a 100-mL pear-shaped flask. The sample volume was reduced via rotary evaporation, exchanged into hexane, and concentrated to 1 mL with a

gentle purified N<sub>2</sub> stream. Prior to transfer to GC–MS vials, known quantities of internal standard (hexamethylbenzene) were added.

Sample extracts were analyzed for 16 US EPA priority PAHs using a ThermoQuest Trace 2000 GC/MS (Finigan). The PAHs were separated using a DB-5MS 30 m × 0.25 mm fused silica column (J&W) in selected ion mode. GC/MS operating conditions were as follows: the injection port, interface line, and ion source temperature were maintained at 280 °C. Column temperature was programmed at 80 °C (hold for 3 min), increased to 250 °C at the rate of 10 °C min<sup>-1</sup> (hold for 3 min), then increased at 5 °C min<sup>-1</sup> to 290 °C (hold for 7 min). Helium was the carrier gas at a flow of 1.0 mL min<sup>-1</sup> and a linear velocity of 24.6 cm s<sup>-1</sup>. 1 µL volume of each sample was injected manually in the splitless mode. The ionization was carried out in the electron impact mode at 70 eV. Identifications of 16 US EPA priority PAHs were based on the retention time and ion *m/z* ratio of an authentic PAH mixed standard. Concentrations of individual compound were estimated from their areas under the chromatographic peaks using the internal standard peaks as instrument references.

#### Quality control

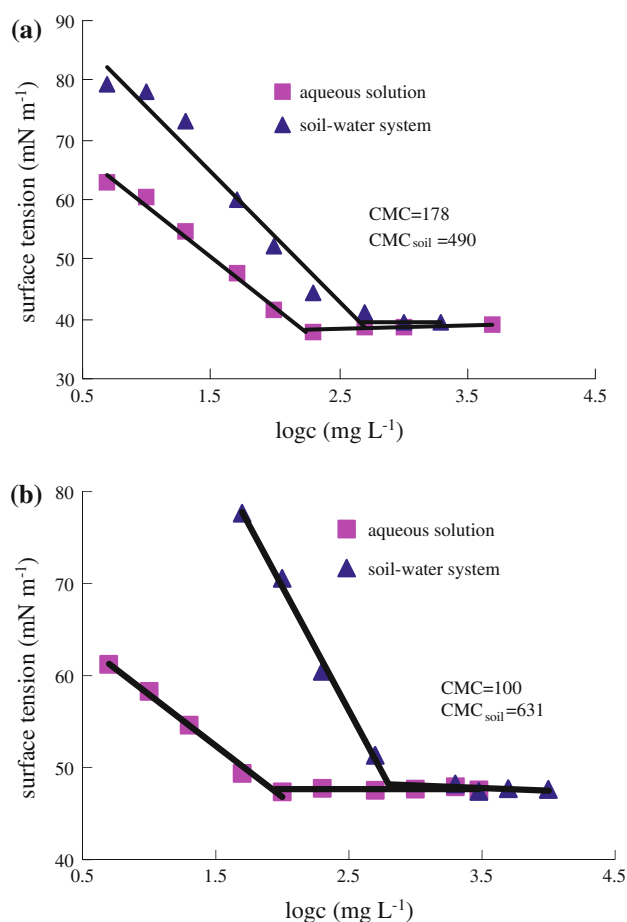
All experiments were carried out in duplicate. Two blank samples were included in every batch of samples. No PAH was detected in blank samples. Recoveries of the four deuterated surrogates added to the soil samples were 55 ± 8 % for naphthalene-d<sub>8</sub>, 74 ± 6 % for phenanthrene-d<sub>10</sub>, 69 ± 7 % for Chrysene-d<sub>12</sub>, and 90 ± 12 % for Perylene-d<sub>12</sub>. Recoveries of the four deuterated surrogates added to the soil washing effluents were 75–92 %. All the values reported in this paper were not corrected to achieve 100 % recovery.

## Results and discussion

#### The apparent CMC of surfactants in soil–water systems

Understanding the surfactants behavior in soil–water systems is important for the design of soil washing projects. Surfactant loss due to sorption may significantly increase the surfactant doses required for ex-situ soil washing (Vreysen and Maes 2005). Furthermore, surfactant adsorption will increase the organic carbon content of the soil, favoring the adsorption of HOCs (Lee et al. 2004; Rodriguez-Cruz et al. 2005). Since the surfactants can only effectively desorb HOCs at concentrations above their CMC<sub>soil</sub> in soil–water systems, the measurement of CMC<sub>soil</sub> can provide scientific basis for a proper surfactant dose.

The measured CMC and CMC<sub>soil</sub> are shown in Fig. 1. The results are the average of triplicate measurements. In general, the surface tension curve has two linear segments for each dose of surfactant. The breakpoint between the two segments indicates the value of CMC in a soil–water system (Chu et al. 2005). The sorption of surfactants is a function of physicochemical and mineralogical properties of soils and the characteristics of surfactants themselves (Rodriguez-Cruz et al. 2005). In this research, the CMC<sub>soil</sub> values of TX100 and B35 are 2.75 and 6.31 times their corresponding CMC values in aqueous solutions, respectively. This is comparable to the results of some other researchers. For example, Chu and Chan (2003) found that the apparent CMC of B35 in a soil–water system is 6.25 times its CMC value in aqueous solution at a soil/water ratio of 1:6. In our research, the CMC<sub>soil</sub> of B35 is 6.31 times their CMC value in aqueous solution at a soil/water ratio of 1:10. Grasso et al. (2001) found that the apparent CMC values of Alfonic 1412-7 in soil–water systems are one to two orders of magnitude of their CMC in aqueous solution at a soil/water ratio of 1:1–1:10.



**Fig. 1** Surface tension and CMC of surfactants in aqueous and soil–water system. **a** TX100, **b** B35

Loss of surfactants resulted from sorption

The sorption of surfactant to the soil is mainly caused by surfactant monomers. Since the monomer concentration in solution is a constant at surfactant doses above  $CMC_{soil}$ , the surfactant sorption should remain unchangeable (Chu et al. 2006; Muherei et al. 2009). Therefore, the surfactant sorption achieves its maximum value at a concentration equals to  $CMC_{soil}$ . At concentrations below the CMC, there exists a linear relationship between the surfactant concentration and the surface tension; therefore, the surfactant sorption can be obtained through surface tension data (Zheng and Obbard 2002; Chu and Chan 2003; Chu et al. 2005; Muherei et al. 2009). The surfactant loss due to sorption can be estimated by the following relationship

$$Q_e = (C_{soil} - C_a) \left( \frac{V_a}{W_{soil}} \right) \quad (1)$$

where  $Q_e$  is the surfactant loss due to sorption to the soil ( $mg\ kg^{-1}$ );  $C_{soil}$  is the bulk surfactant dose in the soil/ aqueous system that produces a surface tension value of  $\sigma$  in the supernatant ( $mg\ L^{-1}$ );  $C_a$  is the corresponding surfactant concentration required to produce the same surface tension value of  $\sigma$  in the absence of soil ( $mg\ L^{-1}$ );  $V_a$  is the volume of aqueous solution (L); and  $W_{soil}$  is the mass of soil (kg).

Freundlich isotherms were used to fit the sorption data of nonionic surfactants at concentrations below  $CMC_{soil}$ :

$$C_S = K_F C_e^n \quad (2)$$

where  $C_S$  is the amount of adsorbed surfactant ( $mg\ kg^{-1}$ ),  $K_F$  is a measure of sorption capacity,  $C_e$  is the equilibrium concentration of surfactant in solution ( $mg\ L^{-1}$ ), and  $n$  is the constant which indicates the curvature of the isotherm.

The Freundlich isotherm fitting results and the surfactant loss data are shown in Table 3. The sorption of TX100 and B35 onto soils is nonlinear, and can fit well with Freundlich isotherm. At concentrations below  $CMC_{soil}$ , most of the surfactants were lost due to sorption. The loss of B35 was greater than that of TX100 with more than 92 % of the surfactant sorbed onto soil at concentrations below its  $CMC_{soil}$ .

**Table 3** Freundlich sorption constants and surfactants loss due to sorption at concentrations below  $CMC_{soil}$

Surfactant	$K_F$	$n$	$R^2$	$PL^a$ (%)	$Q_{max}^b$ ( $mg\ kg^{-1}$ )
TX100	93.99	0.63	0.9431	63–92	3120
B35	761.36	0.54	0.9132	92–99.7	5310

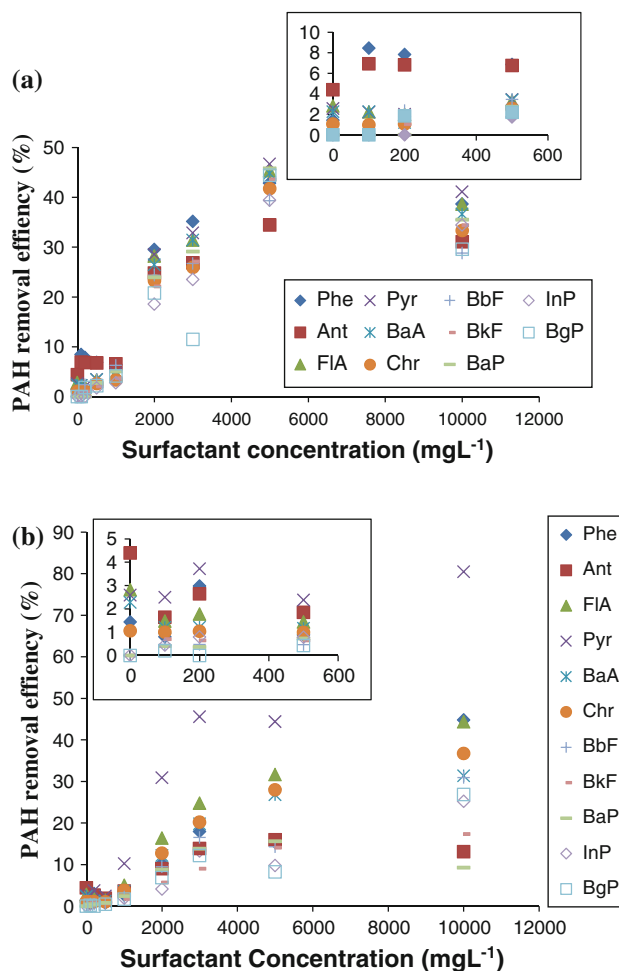
<sup>a</sup> The percentage of surfactant loss due to sorption

<sup>b</sup> The maximal surfactant loss due to sorption

Implications of  $CMC_{soil}$  on PAH removal efficiencies and surfactant selecting

Surfactant-enhanced desorption of PAHs in soils from a former coke oven plant were conducted using TX100 and B35. The removal efficiency was defined as the fraction of PAHs removed from the soils. Figure 2 presents PAH removal efficiency as a function of surfactant concentrations.

As shown in Fig. 2, depending on the surfactant concentrations below or above their  $CMC_{soil}$ , the PAH removal by surfactants presented different patterns. At concentrations below their  $CMC_{soil}$ , due to severe surfactant loss (Table 3), only a small quantity of surfactant molecules were left to exist in the form of monomers. Earlier studies have demonstrated that surfactant monomers have a weak or no HOC desorption enhancement abilities (Chu and Chan 2003). Therefore, the PAH removal is very low and remains almost invariable. Whereas, at concentrations above their  $CMC_{soil}$ , surfactant micelles begin to form in the solution and the PAH removal began to increase greatly.



**Fig. 2** PAH removal efficiency as a function of surfactant concentration. **a** TX100, **b** B35

For B35, at concentrations below its  $CMC_{soil}$ , the PAH removal efficiencies were even less than that in the absence of surfactant. This is similar to the results of some other researchers who have demonstrated that the addition of nonionic surfactants at concentrations below CMC may enhance the retardation of HOCs (Sun et al. 1995; Park and Bielefeldt 2003; Zhou and Zhu 2005). For TX100 which has lesser sorption loss, removal efficiencies less than that in the absence of surfactant were observed only at low surfactant concentrations of 100 and 200 mg L<sup>-1</sup> for some PAHs (FIA, Pyr and BaA).

A desorption efficiency coefficient,  $E$ , can be defined according to that of Wang and Keller (2008):

$$E = \frac{D_s}{D_w}$$

where  $D_s$  and  $D_w$  are the fractions of PAHs desorbed from the soils in the presence ( $D_s$ ) and absence ( $D_w$ ) of surfactant. An  $E > 1$  indicates enhanced PAH desorption, while  $E < 1$  represents an inhibited PAH desorption.

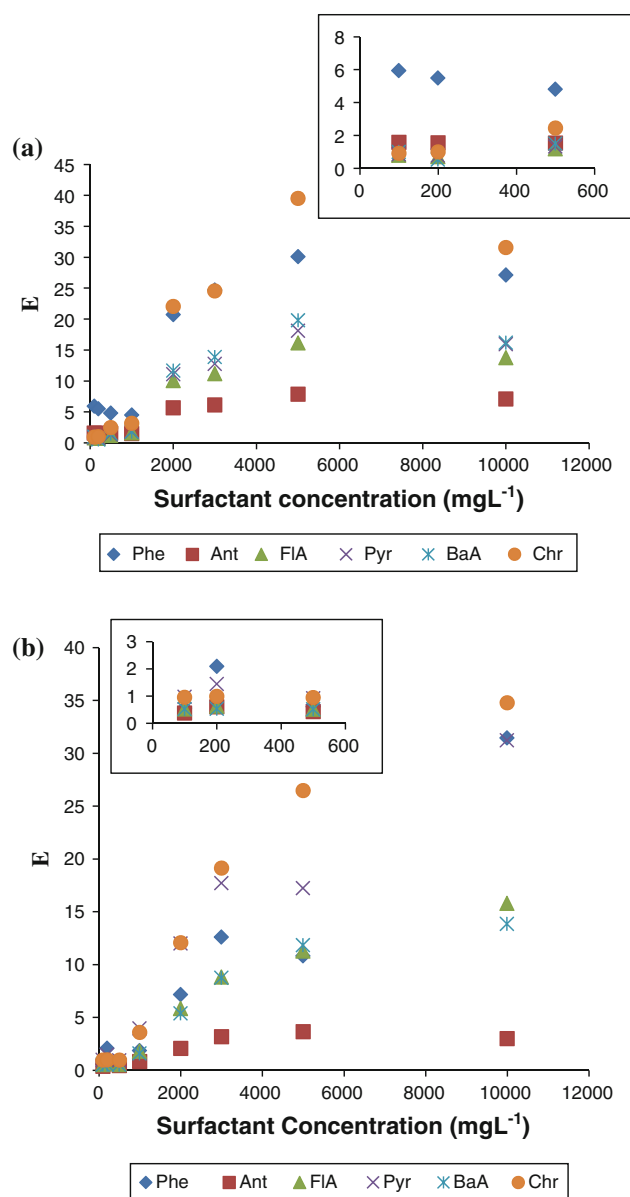
As the heavy molecular PAHs (B(b)F, B(K)F, BaP, DBA and InP) were not detected in the experiment with no surfactant added, the  $E$  value was not obtained for all the PAHs.

Figure 3 shows the  $E$  values. Due to severe surfactant sorption (Table 3), B35 inhibited PAH desorption at concentrations below its  $CMC_{soil}$ . For TX100 which has lesser sorption loss, some degree of PAH desorption enhancement was observed at concentrations below its  $CMC_{soil}$ . It seemed that surface tension reduction mechanism took effect in the PAH removal. Only when PAHs desorbed into water by surface tension reduction exceed those sorption on surfactant-modified soil, can desorption enhancement be observed.

In the design and application of surfactant-enhanced remediation processes for contaminated sites, the selection of surfactant is critical (Grasso et al. 2001). Deshpande et al. (1999) have recommended that both anionic and nonionic surfactants at concentrations below and above their CMC should be evaluated in selecting a surfactant for a given soil-contaminant system. However, according to our research, nonionic surfactant TX100 and BJ35 can greatly enhance PAH desorption only at concentrations well above their  $CMC_{soil}$ . We think  $CMC_{soil}$  is a key parameter while selecting a surfactant for a specific soil washing system. In order to reduce time and money cost, only surfactant concentrations above their  $CMC_{soil}$  should be evaluated in surfactant selecting.

## Conclusions

TX100 and B35 were used to facilitate the desorption of PAHs from soils. The surfactant loss due to sorption and



**Fig. 3** Desorption efficiency coefficient ( $E$ ) as a function of surfactant concentration. **a** TX100, **b** B35

the PAH removal efficiencies by each surfactant is evaluated. Results showed that the  $CMC_{soil}$  values of the two surfactants are 2.75 and 6.31 times their corresponding CMC values in aqueous solutions, respectively. At concentrations below  $CMC_{soil}$ , the loss of B35 (92–99.7 %) was greater than that of TX100 (63–92 %). The PAH removal efficiencies are greatly dependent on the  $CMC_{soil}$  value. At surfactant concentrations below  $CMC_{soil}$ , PAH removal is very low and remains almost invariable. Whereas, at concentrations above their  $CMC_{soil}$ , the PAH removal increases greatly. B35 inhibited PAH desorption at concentrations below its  $CMC_{soil}$ . For TX100, some degree of PAH desorption enhancement was observed at

concentrations below its  $CMC_{soil}$ .  $CMC_{soil}$  is a key parameter while selecting a surfactant for a specific soil washing system, only surfactant concentrations above their  $CMC_{soil}$  should be evaluated.

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