ORIGINAL PAPER



# Better Pectin Yield From Passion Fruit Peel (*Passiflora edulis f. flavicarpa*): From Shaker or Ultrasound? A Comparison

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Received: 17 September 2015/Accepted: 6 June 2016/Published online: 21 November 2016 © Springer Science+Business Media Dordrecht 2016

Abstract Extractions of pectin from passion fruit peel (Passiflora edulis f. flavicarpa) were carried out using a shaker and an ultrasound device. A rotational central composite design was applied for each device used. Citric acid concentration and extraction time were the factors investigated. Increased citric acid increased pectin yield obtained with both the shaker and the ultrasound. Increase extraction time had a negative effect on the yield in shaker and it had a positive effect on the yield in ultrasound. Pectin yield obtained with both devices were fitted to second-order polynomial models. The coefficients of determination  $(R^2)$  were higher than 0.90 and the cross-validated  $R^2$  (Q<sup>2</sup>) were higher than 0.92. Higher yield (about 55 %) was obtained using 0.75 M citric acid concentration and sample submitted to ultrasound for 90 min. This was 81 % higher than the highest obtained from using the shaker. Diet gels containing calcium can be produced from the pectin extracted by ultrasound.

Keywords Fruit processing · Waste · Fiber · Empirical model

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#### Introduction

Passion fruit peel is a waste, which contains pectin [25, 27] and it has been receiving increasing attention in research for the development of new food products [6]. Pectin is mainly used in the food processing industry as a gel and thickening agent [4].

The esterification degree (ED), expressed as a percentage of the esterified carboxyl groups, is an important means to classify pectin, and has a major influence on the gel properties of pectin [35]. Depending on the ED, pectin is commercially divided into two groups: high-ester pectin, with ED higher than 50 %, and low-ester pectin, with ED lower than 50 % [29]. Pectin with an ED >50 needs sugar (such as sucrose) and acid (pH 2.0–3.5) to form gels, whereas pectin with an ED <50 needs calcium ions to form gels within a larger pH range (2.0–7.0) whether sugar is present or not [35].

The techniques most frequently used for extraction of pectin are: (1) acid extraction by stirring and heating, (2) heat refluxing extraction and (3) microwave heating extraction [4]. Different acids can be used in the acid extraction by stirring and heating. Nitric, hydrochloric and sulfuric acids are the most used [35]. This generally results in degradation of the arabinan side-chains and therefore in a loss of feruloyl groups, which are the key factors in cross-linking pectin [22]. Furthermore, the use of these strong acids leads to corrosion of equipment and has deleterious effects on the environment [27]. Therefore, organic acids are generally used to reduce the adverse effects of mineral acids.

Studies indicate that citric acid is a natural and safe food additive, and is also advantageous from an economic and environmental point of view [3]. The extraction of pectin from fruit peel using citric acid has been studied recently using passion fruit peel [10, 13, 25] and other vegetable matrices, such as mango peel [7], cacao pod husks [30], sugar beet pulp [12] and banana peel [21].

The use of an ultrasound device for extraction has increased recently, as it is seen to be efficient. This device uses low energy and consumes less solvent [15, 20, 34]. Ultrasound processing is widely used in the food industry due to its capability to induce chemical and physical changes in food components [1, 5, 24]. The increase of emulsifying capacity, the release and diffusion of cell material, and enhanced foaming are some of the improvements in food processing using sonication [28].

In this study, response surface methodology (RSM) was employed to study the extraction of pectin from passion fruit peel using two devices (shaker and ultrasound) to understand the combined effects of variables (citric acid concentration and extraction time) on pectin yield.

## **Materials and Methods**

#### Yellow Passion Fruit Peel

Yellow Passion fruit (*Passiflora edulis f. flavicarpa* L.) was obtained from the local market in Igarassu, Pernambuco state, Brazil. The fruit was washed, cut and the pulp and seeds were removed. The peels were washed in tap water to remove the adhering pulp and soluble sugars. The passion fruit peels with mesocarp were dried in a hot air oven (NT514) at 55 °C overnight. The raw material was milled to an average particle size of 20 Mesh, using a commercial mill (Marconi). The fruit peel powder was packaged in a polyethylene bag and stored at -20 °C in a freezer. All the chemicals used in the study were of analytical grade and purchased from Sigma-Aldrich Chemicals, Brazil.

### **Pectin Extraction**

The extraction procedure was based on the methodology reported by Kliemann et al. [9]. A dry mass of passion fruit peel flour (5 g) was subjected to extraction and 250 mL of citric acid was added. The citric acid concentrations and extraction times were according to the experimental design (Table 1). The suspensions were then incubated in a shaker

 Table 1
 Factors and levels used in the rotational central composite design

Factors	Levels				
	-1.41	-1	0	1	+1.41
CA (Citric acid—M)	0.15	0.25	0.5	0.75	0.85
ET (Extraction time-min)	18	30	60	90	105

at 50 °C and 150 rpm (New Brunswick Scientific C25 KC) or using an ultrasound without temperature control and without stirring (UltraSonic Cleaner-UNIQUE). For both processes, the same conditions of time and concentration of citric acid were applied. After extraction, the suspension was filtered using filter qualitative paper of 12.5 cm diameter and the filtrate was cooled down to  $4 \pm 1$  °C for 60 min. The filtrate was coagulated using an equal volume of 96 % (V/V) ethanol and left for 1 h. The coagulated pectin was separated by filtration through a nylon cloth, washed first with 70 % (v/v) acidic ethanol (0.5 % HCl), then with 70 % (V/V) ethanol to neutralize the pH and finally with 96 % (V/V) ethanol. After this process, the resulting material was dried overnight at 55 °C in an airforced oven. Pectin yield (Y) was expressed as the ratio of the amount of extracted pectin (M in grams) obtained after extraction to the initial amount of passion fruit peel powder (5 g) used for extraction (Eq. 1).

$$\mathbf{Y} = \left(\frac{\mathbf{M}}{5}\right) \times 100\tag{1}$$

## **Experimental Design**

In this study, rotational central composite designs with two factors (citric acid concentration and extraction time) were carried out for passion fruit peel flour pectin extraction process using a shaker and an ultrasound device. The extraction time and citric acid concentration varied according to Table 1.

The experimental ranges for the factors were determined according to the results obtained by Kliemann et al. [9]. The whole design consisted of 10 experimental points, two replicates at the central point of the design, which were used to estimate a pure error sum of squares. All the experiments were randomly carried out in order to minimize the effect of unexplained variability due to systematic errors. The experimental design and data analysis were performed using Statistica software 7.0, for both devices (shaker and ultrasound). The response variables were fitted to two quadratic polynomial models, the general form of which was as follows:

$$\hat{\mathbf{y}} = \mathbf{b}_0 + \mathbf{b}_1 \mathbf{X}_1 + \mathbf{b}_2 \mathbf{X}_2 + \mathbf{b}_{11} \mathbf{X}_1^2 + \mathbf{b}_{22} \mathbf{X}_2^2 + \mathbf{b}_{12} \mathbf{X}_1 \mathbf{X}_2 \qquad (2)$$

where  $\hat{y}$  is the pectin yield simulated by Eq. (2); X<sub>1</sub> and X<sub>2</sub> are the factors; b<sub>0</sub> is the model intercept coefficient; b<sub>1</sub>, b<sub>2</sub>, b<sub>11</sub>, b<sub>22</sub> and b<sub>12</sub> are interaction coefficients of linear, quadratic and the second-order terms, respectively [19].

#### **Esterification Degree**

Esterification degree (ED), number of esterified carboxyl groups per the total number of carboxyl group (Eq. 3), was

determined by potentiometric titration, as described by Bochek et al. [2].

$$ED = \frac{K_e}{K_t} \times 100 \tag{3}$$

A dry portion of the extracted pectin (0.2 g) was placed in an Erlenmeyer for titration and wet with ethanol. Distilled water heated at 40 °C (20 mL) was added and the mixture was stirred for 2 h. The resulting solution was titrated with 0.1 N NaOH. The number of free carboxyl groups ( $K_f$ ) was calculated using Eq. (4).

$$K_n = \frac{N_{NaOH} V_{NaOH} \times 0.045}{a} \times 100$$
(4)

where n = f (free) or e (esterified); a = portion of pectin with absorbed water (g);  $N_{NaOH} = concentration of NaOH$ (N);  $V_{NaOH} = volume$  (mL) of NaOH spent for titration.

To determinate the number of esterified carboxyl groups (Ke), a 0.1 N NaOH solution (10 mL) was added to a neutralized polygalacturonic acid sample after determination of the free carboxyl groups. The number of the esterified carboxyl groups was calculated from the volume of 0.1 NaOH solution spent for titration (Eq. 4).

## **Results and Discussion**

The values of responses (yield of pectin) under different experimental combinations are given in Table 2. Depending on the experimental conditions, a high yield pectin (more than 40 %) could be achieved. The pH remained between 1.5 and 2.2 for all citric acid concentrations. Low pH stimulated a hydrolysis of protopectin, which is a compound formed by the combination of cellulose with

 Table 2
 Pectin yields obtained in shaker and ultrasound according to rotational central composite design

Run	Factors		Responses		
	CA (M)	ET (min)	$Y_s(\%)$	$Y_u(\%)$	
1	0.25	30	14.48	15.44	
2	0.75	30	30.22	32.80	
3	0.25	90	13.55	22.11	
4	0.75	90	17.63	54.69	
5*	0.50	60	14.76	26.94	
6*	0.50	60	15.35	26.25	
7	0.15	60	9.88	12.91	
8	0.85	60	19.00	40.53	
9	0.50	18	21.40	24.35	
10	0.50	105	15.43	36.14	

\* Experiments at the center point

t were carried out in replicate to estimate the experimental error

pectin molecules [8]. Therefore, pH can be considered as one of the more crucial parameters affecting the yield of extracted pectin [13].

Regardless of the acid concentration (experiments 1, 2) and 9), the relative standard deviation of yield obtained with both devices was less than 10 %, when the extraction time was less or equal to 30 min. This indicates that there was no significant variation in the yield of experiments 1, 2 and 9, for each combination of concentration and time. For these three experiments, the highest yield (about 30 %) was found when 0.75 M and 30 min were used (experiment 2). On the other hand, when the concentrations varied from 0.15 to 0.5 M, the relative standard deviation was higher than 10 % (between 18 and 41 %), for 60 or 90 min (experiments 3, 5, 6 and 7). Given these conditions, the highest yields were obtained with ultrasound. Finally, for extraction time higher or equal to 90 min and concentrations higher or equal to 0.5 M (experiments 4, 8 and 10), the relative standard deviation was higher than 50 %, indicating an even higher difference between the devices used.

Differences in performance of these two devices, can be related to the type of energy used in the extraction process. The increase yield of pectin was observed for extractions conducted under ultrasound and this effect may be due to the changes occurring in plant tissues, for example, a rupture of the parenchymal cells of the plant material [17]. However, this was only observed when the extraction time was higher than 30 min.

Studies have shown that the application of ultrasound can help the extraction of pectin from different vegetable raw materials in addition to the passion fruit. Among these are included grapefruit [32, 34], tomato waste [4], grape pomace [18], sisal waste [15], and pomegranate peel [20].

Equation (2) was fitted to the experimental data. The predicted response Y for the yield of pectin could be obtained by the following regression models for the shaker (Eq. 5) and the ultrasound (Eq. 6) devices.

$$\hat{y} = 15.06 + 4.09X_1 + 0.33x_1^2 - 2.74X_2 + 2.32x_2^2 - 2.92X_1X_2$$
(5)

$$\hat{y} = 26.60 + 11.12X_1 + 0.82x_1^2 + 5.65X_2 + 2.33x_2^2 + 3.81X_1X_2$$
(6)

The coefficients of determination ( $\mathbb{R}^2$ ) of the models for both devices were 0.9195 (shaker) and 0.9749 (ultrasound), which further indicated that the models were able to represent the real relationships among the selected variables. The cross-validated  $\mathbb{R}^2$  ( $\mathbb{Q}^2$ ) were 0.9206 and 0.9601, for shaker and ultrasound, respectively. This parameter describes the goodness of prediction, showing how well new experiments can be predicted using this mathematical model.  $R^2$  and  $Q^2$  values higher than 0.75 and 0.60, respectively, indicate that the model is acceptable [14].

Response surface of the pectin yield as a function of independent variables (citric acid concentration and extraction time) is shown in Fig. 1 for the shaker. Increase citric acid concentration increased the yield. On the other hand, increased extraction time decreased the yield and this effect is shown in the model as the linear coefficient of  $x_2$ , since it was negative. These effects were significant according to the *t* test (95 % confidence) calculated using Statistica.

The response surface of the pectin yield obtained in ultrasound is shown in Fig. 2. Increase citric acid concentration or extraction time increased the yield. All the effects of variables on the yield were significant according to a *t* test (95 % confidence). The higher yield pectin (54.69 %) was found in ultrasound, when using 0.75 M citric acid, for 90 min at 27 °C. This was higher than yields reported in the literature for extraction of pectin from passion fruit peel. Kulkarni and Vijayanand [10] found yield (14.8 %) when using hydrochloric acid and hot water (60–100 °C). Liew et al. [13] found that the pectin yield ranged from 2.25 to 14.60 %, using shaking with water at 70 °C, for 75 min and with citric acid.

Heating extraction has disadvantages for pectin extraction, since it can lead to the degradation of pectin [34]. In the present work, the highest temperature in the shaker in relation to that used in ultrasound may have contributed to a lower yield, when the extraction time was increased. In ultrasound extraction, increased temperature can increase pectin yield due to increased solubility. However, the increase of pectin yield can decrease when the temperature is higher than 80 °C [16, 26].



Fig. 1 Response surface for the dependence of yield on citric acid concentration and extraction time during pectin extraction from passion fruit using shaker



Fig. 2 Response surface for the dependence of yield on citric acid concentration and extraction time during pectin extraction from passion fruit using ultrasound

The ED ranged from 18 % (0.75 M citric acid and 90 min) to 30 % (0.15 M citric acid and 60 min), when the ultrasound device was used. Extracted pectin was only good for the preparation of Ca<sup>2+</sup> mediated low-ester pectin gels. ED vary with fruit peels, extraction parameters and extractors used [13]. Low-ester pectin forms gels in a higher pH range than high-ester pectin, without requiring the presence of sugar [33], therefore, may be used as a gelling agent in low sugar products, such as low-calorie jams and jellies, confectionery jelly products, and other foods applications [31]. In general, pectin extracted from vegetables exhibits methoxyl content between 10 and 12 % [23]. The extraction of pectin yellow passion fruit peel with hot water or oxalate acidified with nitric acid resulted in pectin with ED <50 % [36, 37].

## Conclusion

Extraction of pectin from passion fruit peel was investigated by RSM. The surfaces response disclosed the relationships between citric acid concentration and extraction time. This generated pectin yields for shaker and ultrasound study. Using these surfaces, a satisfactory condition of 0.75 M citric acid concentration, regardless of the equipment used and extraction time of 30 or 90 min for shaker (30.2 %) or ultrasound (54.7 %), respectively, were established. The extraction of pectin from yellow passion fruit using ultrasound and citric acid results in acceptable pectin that can be used to form dietetic gels containing calcium. Acknowledgments The authors acknowledge the financial support from Conselho Nacional de Desenvolvimento Científico e Tecnológico, Brasilia DF, Brazil (CNPq). The English text of this paper was revised by Sidney Pratt, Canadian, MAT (The Johns Hopkins University), RSAdip - TESL (Cambridge University).

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