



# Surface Modification of Magnetite Using Silica Coating: Spectroscopic, Structural, Morphological Characterization and Interaction with Crystal Violet Dye

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## Abstract

The essential goal of this work is to produce an eco-friendly and economically nano-adsorbent that may separate organic dye, especially, cationic dye, from polluted water prior to making use of this adsorbent in industrial field. This work suggests a way of fabricating magnetite and silica. The proposed approach concerned three steps: the preparation of magnetite ( $\text{Fe}_3\text{O}_4$ ) nanoparticles by co-precipitation method, then of silica using sodium silicate prepared from silica sand, and finally a magnetite coating of silica  $\text{Fe}_3\text{O}_4/\text{SiO}_2$ . The nanocomposites were investigated by X-ray diffraction (XRD), Fourier transform infrared spectroscopy (FTIR) and transmission electron microscopy (TEM). The XRD characterization displayed that silica formed an amorphous phase and that magnetite shaped a spinel phase. To optimize the diverse experimental variables affecting the elimination performance of the CV, the effects of experimental parameters including solution pH, adsorbent dose, contact time, initial dye concentration and temperature were evaluated. Adsorption kinetic disclosed that pseudo-second-order is the best model ( $R^2 > 0.99$ ,  $q_e = 5.68 \text{ mg g}^{-1}$ ). Adsorption isotherm represented that Langmuir is the best model with  $Q_{\text{max}} = 200 \text{ mg g}^{-1}$ . The negative  $\Delta H^\circ$  and  $\Delta G^\circ$  values exhibited the exothermic and spontaneous nature of CV sorption on the nanoparticles, respectively.

**Keywords** Silica sand ·  $\text{Fe}_3\text{O}_4/\text{SiO}_2$  · Cristal violet dye · Characterization · Adsorption

## 1 Introduction

In current years, synthetic dyes have become one of the primary origin of water pollution. These pollutants are dangerous, carcinogenic and harmful to people, animals and plants [1]. Many decolorization techniques have been conducted for water treatment contaminated by the dye. These procedures are chemical, biological, and physical [2]. Physical methods including coagulation, adsorption, and oxidation have

been proven for the purification of dye-containing effluent [3]. Adsorption is a successful physical remedy procedure for wastewater. It enables the removal of the organic pollutants in a cheap, direct, profitable, and straightforward manner, even if these pollutants exist in small quantities [4]. The high-quality technique for getting rid of the dye is adsorption because it is straightforward to use, inexpensive, very powerful and environmentally benign [5, 6]. Numerous materials have been employed and examined, such as activated carbon, polymers, zeolite [7], clay [8] and nanomaterials [9] etc. Currently, magnetite nanoparticles have garnered strong attention for many contaminants, which include dyes due to their biocompatibility, high activity, excellent magnetic features, easy and the economic synthesis process [10]. Nowadays, they are several processes for the magnetite nanoparticles synthesis among them: co-precipitation [11], sol-gel [12], thermal decomposition [2], Hydrothermal [13], microwave irradiation, etc. Among them, co-precipitation is a crucial process, owing to it's a very simple, fast and inexpensive method and having a relatively low temperature in a short process [3–14]. After their fabrication, magnetite particles are unstable in the air; it is oxidized by oxygen of the air and

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agglomerate easily [15] because of the dipolar interactions between them. Therefore, these nanoparticles demand functionalization and surface modification [16] by coating these particles with a layer of a material that is usually diamagnetic on the way to keep away from aggregation. The coating can be used with extra materials, including silica [17], polymers [18], carbon [19], clay [20], zeolite [21], etc. In this research, the magnetic particle ( $\text{Fe}_3\text{O}_4$ ) changed into mixed with  $\text{SiO}_2$  since it has a lot of benefits like the ability of its pure materials and the large capacity of cation exchange. Tunisia is a country with plentiful natural resources. Among them, silica sand. Silica has hydrophobic or hydrophilic properties based on its structure and morphology [22]. This material was employed in several factories and medical field owing to its biocompatibility, easy surface modification because of the abundant silanol groups, stability and its ability to absorb various substances such as water, oil, and radioactive material. In addition, coating procedure offers many advantages, such as simple method, low cost, availability of Tunisia sand, and credible time. To date, the majority of investigations have been synthesized silica coated by magnetite particles using Stöber process [23], which is an important method, as silica is formed in situ through the condensation of a sol–gel precursor as the tetraethyl orthosilicate (TEOS). Furthermore, few studies have been published regarding the fabrication of  $\text{Fe}_3\text{O}_4 @\text{SiO}_2$  nanocomposites by natural material. For example, Taufiq et al. [24] synthesized silica-covered magnetite from natural sand.

The paper aims to synthesize nanomaterial magnetite by coprecipitation method and then coating with silica extracted from natural resource to obtain  $\text{Fe}_3\text{O}_4 @\text{SiO}_2$  nanocomposites. The powders were studied using XRD, FTIR, SEM, TEM, and BET and applied as a magnetic adsorbent in the removal of crystal violet (CV) from aqueous solution. Several parameters such as pH, adsorbent dose, contact time, initial concentration of CV and temperature were investigated on the adsorption process. The kinetics, isotherms and thermodynamic parameters of adsorption were studied.

## 2 Experimental

### 2.1 Materials

The silica sand was sampled from the borj Hfayedh (Nabeul area, Northeast of Tunisia). Iron (III) chloride hexahydrate ( $\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$ ), iron (II) sulfate heptahydrate ( $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$ ), sodium hydroxide, ammonium hydroxide were all purchased from Oxford lab Chem. ( $\text{NH}_3 \cdot \text{H}_2\text{O}$ ), ethanol ( $\text{C}_2\text{H}_5\text{OH}$ ) and were purchased from Sigma Aldrich.

Cristal violet (CV) that also known C.I. 42,555 was purchased from Merck. The molecular weight for CV was  $407.979 \text{ g mol}^{-1}$  with a chemical formula of  $\text{C}_{25}\text{N}_3\text{H}_{30}\text{Cl}$  and purity of 98%. For this purpose,  $1000 \text{ mg L}^{-1}$  of dye was inoculated into deionized water and then a serial dilution was prepared.

### 2.2 Synthesis of $\text{Fe}_3\text{O}_4$ and $\text{Fe}_3\text{O}_4 @\text{SiO}_2$

$\text{Fe}_3\text{O}_4$  sample was synthesized via way of means of coprecipitation method. In this regard 0.8 g of  $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$  and 0.9 g of  $\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$  were dissolved in distilled water (200 mL) and ethanol (40 mL) at  $25^\circ\text{C}$  under the condition of vigorous stirring. After resting for 30 minutes, ammonium hydroxide (15 mL) was added dropwise into the solution as precipitating agent and solution color tends to change from brown to black. The acquired magnetite was amassed using a magnet, rinsed with distilled water to eliminate the surplus of ammonia and then dried in an oven at  $60^\circ\text{C}$  for 8 h.  $\text{Fe}_3\text{O}_4 @\text{SiO}_2$  was prepared by the two step procedure (Fig. 1). Firstly, the used sand was washed and dried at  $60^\circ\text{C}$ . Then it was completely mixed with 100 mL of sulfuric acid (2.5 M) for 48 h. The acid-treated sand was washed to eliminate the traces of the acid. After drying at  $105^\circ\text{C}$  for 24 h, the obtained sample was crushed and sieved at  $100 \mu\text{m}$ . Then, sand and sodium carbonate  $\text{Na}_2\text{CO}_3$  ( $200 \mu\text{m}$ ) were completely



**Fig. 1** Synthesis of  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4 @\text{SiO}_2$

blended with a molar ratio  $\text{SiO}_2/\text{Na}_2\text{O} = 1$  in high temperature ( $1060^\circ\text{C}$ ) to get the sodium silicate powder  $\text{Na}_2\text{SiO}_3$ . In the second step, 1.3 g of  $\text{Na}_2\text{SiO}_3$  and 0.3 g of  $\text{Fe}_3\text{O}_4$  have been dissolved in 100 mL of distilled water at  $80^\circ\text{C}$  for 15 min and the pH 6 of the solution was adjusted using HCl (2 M). Then, the mixture was stirred at  $80^\circ\text{C}$  for 3 h. The nanocomposites obtained ( $\text{Fe}_3\text{O}_4@ \text{SiO}_2$ ) were separated through way of a magnet washed with water and dried at  $60^\circ\text{C}$  for 8 h (Fig. 1).

### 2.3 Characterization

X-Ray diffraction analyses were performed using Bruker diffractometer model D8 advance under conditions of  $\text{CuK}\alpha$  radiation ( $\lambda = 1.5406 \text{ \AA}$ ). The system was operated at 40 kV and 30 mA. Diffraction patterns were recorded in the  $2\theta$  range of  $10^\circ$ – $70^\circ$ .

FTIR spectra were recorded in the region  $4000 \text{ cm}^{-1}$ – $400 \text{ cm}^{-1}$  (1 mg of the sample was prepared using KBr) with a perkin Elmer FTIR2000 infrared Fourier transform spectrometer.

The morphology of the materials was studied by scanning electron microscopy (SEM) microscope with a FEI Quanta 650.

The structural characteristics of the materials were studied by the means of TEM using the TECHNAI 20-Philips instrument (G20, 200 kV) equipped with an energy dispersive X-ray spectroscopy (EDX). The powders were ultrasonically dispersed in ethanol.

The nitrogen adsorption-desorption analysis at 77 K was determined by Micromeritics ASAP 2020 instrument. The Brunauer-Emmett-Teller (BET) and Barrett-Joyner (BJH) methods were used to determine the specific surface area (SSA) and the porosity.

The zeta potential measurement was determined by Malvern ZetaSizer Nano-SZ at different  $\text{pH}_5$  from 2 to 12. So, 1 mg of sample was suspended in 20 ml of 1 mM NaCl and shaken for 24 h. The point of zero charge ( $\text{pH}_{\text{PCZ}}$ ) of the sample was found by plotting the zeta potential (mV) versus the pH.

### 2.4 Adsorption Test of CV on $\text{Fe}_3\text{O}_4@ \text{SiO}_2$

Adsorption test was executed in a batch system with varying different parameters such as pH (2–10), adsorbent dose (0.001–0.1 g), contact time (5–180 min), initial concentration of the dye ( $10$ – $500 \text{ mg L}^{-1}$ ) and temperature ( $25$ – $55^\circ\text{C}$ ). All experiments of adsorption were done on a 200 rpm stirrer until the system reached equilibrium. For this purpose, 0.05 g of  $\text{Fe}_3\text{O}_4@ \text{SiO}_2$  was added about 30 ml of CV ( $10 \text{ mg L}^{-1}$ ) at room temperature. The nanocomposites were separated by an external magnet and the residual CV concentration was measured by Agilent Cary6

UV-vis spectrophotometer of 590 nm. The CV adsorption rate (R) and the adsorption capacity ( $q_e$ ) were calculated consistent with the subsequent equations (Eq. 1) (Eq. 2):

$$R(\%) = \frac{(C_0 - C_e)}{C_0} \times 100 \quad (1)$$

$$q_e = \frac{(C_0 - C_e)V}{M} \quad (2)$$

Where  $C_0$  and  $C_e$  are the initial CV concentration and CV final concentration in  $\text{mg L}^{-1}$ , respectively.  $q_e$  is the CV uptake in  $\text{mg g}^{-1}$  adsorbent,  $V$  is the volume of CV in mL and  $M$  is the quantity of nanocomposite in g.

## 3 Results and Discussion

### 3.1 Adsorbents Characterization

#### 3.1.1 XRD Analysis

X-ray diffraction patterns of the  $\text{Fe}_3\text{O}_4$  nanoparticles and  $\text{Fe}_3\text{O}_4@ \text{SiO}_2$  nanocomposites were presented in Fig. 2. For  $\text{Fe}_3\text{O}_4$ , diffraction peaks detected at  $30.22^\circ$ ,  $35.65^\circ$ ,  $43.23^\circ$ ,  $53.42^\circ$ ,  $57.42^\circ$ ,  $62.79^\circ$  and  $71.41^\circ$  corresponding to the (220), (311), (400), (422), (511), (440), (531) planes, respectively designated that  $\text{Fe}_3\text{O}_4$  is cubic spinel structure [25, 26]. After silica coating on the magnetite surface, a broad peak observed for  $\text{Fe}_3\text{O}_4@ \text{SiO}_2$  at  $2\theta$  of  $23^\circ$ , was assigned to amorphous silica [27]. The particle size may be determined by the following Debye–Scherrer equation (Eq. 3) [28]:

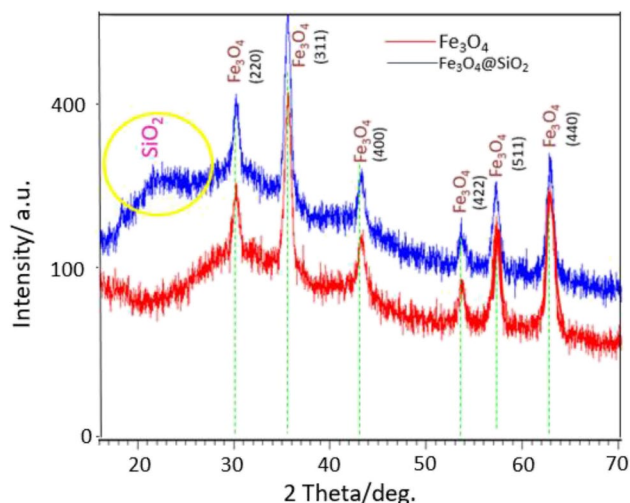
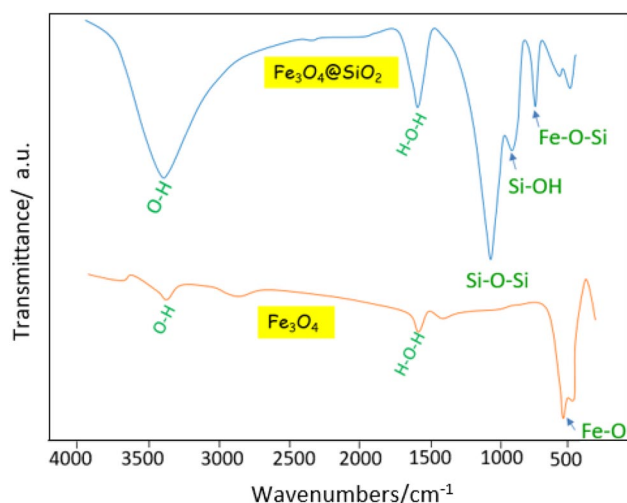


Fig. 2 XRD patterns of  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4@ \text{SiO}_2$





**Fig. 3** FTIR spectra of  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4@\text{SiO}_2$

$$D = K\lambda/\beta\cos\theta \quad (3)$$

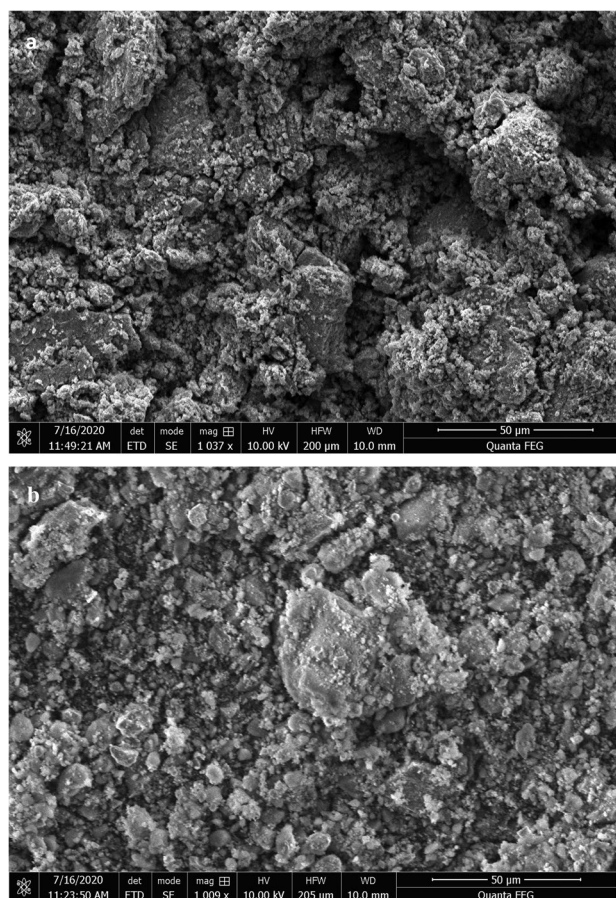
With  $D$  is the average diameter,  $K$  is Sherrer constant,  $\lambda$  is ray wavelength (0.15406 nm),  $\beta$ , the peak width of half-maximum, and  $\theta$ , the Bragg peak angle. The  $\text{Fe}_3\text{O}_4$  size was about 34.68 nm.

### 3.1.2 FTIR Analysis

The FTIR spectra of  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4@\text{SiO}_2$  were executed to confirm the existing of silica shell (Fig. 3). The band at  $3464\text{ cm}^{-1}$  implied the existence of hydroxyl groups. Moreover, the band at  $1641\text{ cm}^{-1}$  is assigned to H-O-H bending mode [29]. The strong band at  $584\text{ cm}^{-1}$  characterizing the Fe-O bonds confirm the spinel type structure of pure  $\text{Fe}_3\text{O}_4$  nanoparticles [17]. In comparison with the curve of pure  $\text{Fe}_3\text{O}_4$ , the peaks at approximately  $1091\text{ cm}^{-1}$ ,  $799\text{ cm}^{-1}$  and  $460\text{ cm}^{-1}$  were ascribed to the symmetric and asymmetric stretching vibrations of Si-O-Si respectively. The peak at  $960\text{ cm}^{-1}$  associated to Si-OH bond vibrations [29], which indicated the  $\text{Fe}_3\text{O}_4$  was successful coated by  $\text{SiO}_2$ . This result has a good consent with the previous research [30].

### 3.1.3 SEM Analysis

SEM analysis was used to examine the morphology of the prepared samples, as seen in Fig. 4. Due to their small size and magnetism, the magnetic  $\text{Fe}_3\text{O}_4$  nanoparticles in Fig. 4a exhibit an irregular crystalline shape, and surface morphology examination shows that they were agglomerated from several fine particles. When the  $\text{Fe}_3\text{O}_4$  nanoparticules were covered with the  $\text{SiO}_2$  layer, Fig. 4b demonstrates that the surface of the  $\text{Fe}_3\text{O}_4@\text{SiO}_2$  nanocomposites was smoother and the agglomeration decreases than that of the  $\text{Fe}_3\text{O}_4$  nanoparticles.



**Fig. 4** SEM images of (a)  $\text{Fe}_3\text{O}_4$  and (b)  $\text{Fe}_3\text{O}_4@\text{SiO}_2$

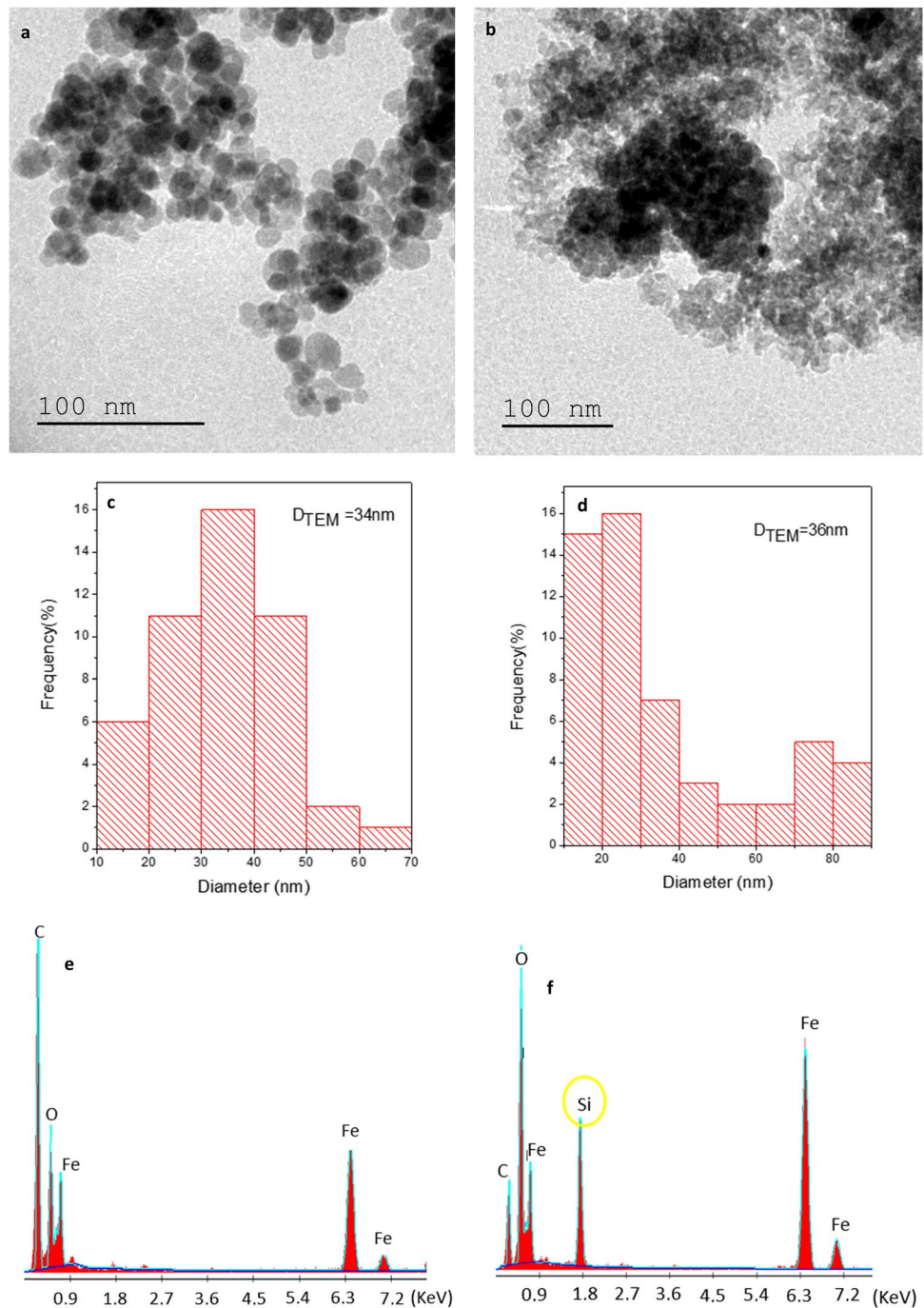
### 3.1.4 TEM Analysis

TEM analysis, size distribution and EDX spectral profile  $\text{Fe}_3\text{O}_4$  and the  $\text{Fe}_3\text{O}_4@\text{SiO}_2$  were observed in Fig. 5. TEM image of magnetite displays that particles are well dispersed with spherical forms (Fig. 5a) with  $\sim 34$  nm diameter (Fig. 5c), which the same with size is obtained from XRD. Figure 5b reveals the TEM image of  $\text{Fe}_3\text{O}_4@\text{SiO}_2$ . The size of this nanomaterial turned out to be approximately 36 nm for  $\text{Fe}_3\text{O}_4@\text{SiO}_2$  (Fig. 5d). Moreover, (Fig. 5e-f) represents the EDX spectra of  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4@\text{SiO}_2$ . As can be seen, the nanocomposites contain elements of silicium (Si), iron (Fe) and oxygen (O). Si band was determined in Fig. 5f after coating of magnetite with silica. In the elemental analysis, the basic composition of % Si, % Fe and O were defined.

### 3.1.5 Zeta Potential Analysis

The zeta potential evaluation of the  $\text{Fe}_3\text{O}_4@\text{SiO}_2$  was assessed in the pH range of 2 to 12 and its result is displayed in Fig. 6. According to the results, the pHzpc

**Fig. 5** TEM images of (a)  $\text{Fe}_3\text{O}_4$  and (b)  $\text{Fe}_3\text{O}_4@\text{SiO}_2$ , and size distribution histogram of (c)  $\text{Fe}_3\text{O}_4$  and (d)  $\text{Fe}_3\text{O}_4@\text{SiO}_2$  obtained from the TEM micrograph, and EDX of (e)  $\text{Fe}_3\text{O}_4$  and (f)  $\text{Fe}_3\text{O}_4@\text{SiO}_2$

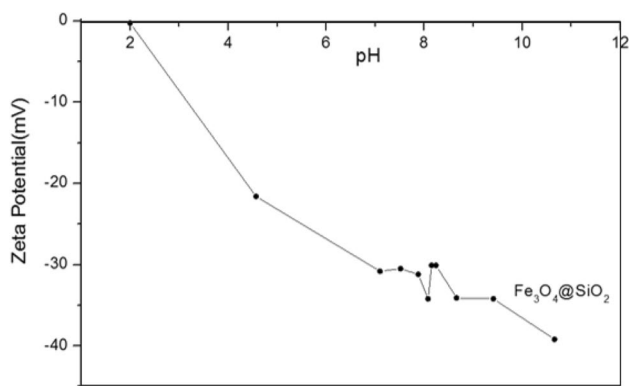


values had been acquired between 0 to  $-38.7$  mV and the isoelectric point of the  $\text{Fe}_3\text{O}_4@\text{SiO}_2$  was found to be approximately 2. This suggests that the  $\text{Fe}_3\text{O}_4@\text{SiO}_2$  surface is negatively charged at pH above 2 that is favorable for the cationic CV adsorption. At very higher pH, there is electrostatic attraction between cationic CV and hydroxyl ions. Furthermore, at acidic pH, there is electrostatic repulsion between cationic CV and positively charged  $\text{Fe}_3\text{O}_4@\text{SiO}_2$  surface along with the existence of

hydrogen ions, which reduces the elimination performance at mentioned pH conditions.

### 3.1.6 Nitrogen Adsorption-Desorption Properties

The  $\text{N}_2$  adsorption-desorption isotherms of  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4@\text{SiO}_2$  were discovered in Fig. 7a. The isotherms indicate type IV with an H3-type hysteresis loop, designate of the mesoporous structure of nanoparticles in keeping with the



**Fig. 6** Zeta potential analysis of  $\text{Fe}_3\text{O}_4@\text{SiO}_2$

IUPAC classification. The specific surface area of  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4@\text{SiO}_2$  were 81 and  $133\text{m}^2/\text{g}$ , respectively. The increase in the specific surface area of  $\text{Fe}_3\text{O}_4@\text{SiO}_2$  indicated that the existence of silica on the surface of  $\text{Fe}_3\text{O}_4$ , which favors the adsorption of dyes. The pore-size distribution measured by the BJH method of the prepared  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4@\text{SiO}_2$  as shown in Fig. 7b. The pore size distribution of  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4@\text{SiO}_2$  were 11.6 and 13 nm, respectively, designates a mesopore distribution. The pore size diameter of  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4@\text{SiO}_2$  were 9.6 and 11.3 nm, respectively, indicating the mesoporous structure. The pore volumes of  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4@\text{SiO}_2$  were 0.238 and  $0.537\text{cm}^3/\text{g}$ , respectively.

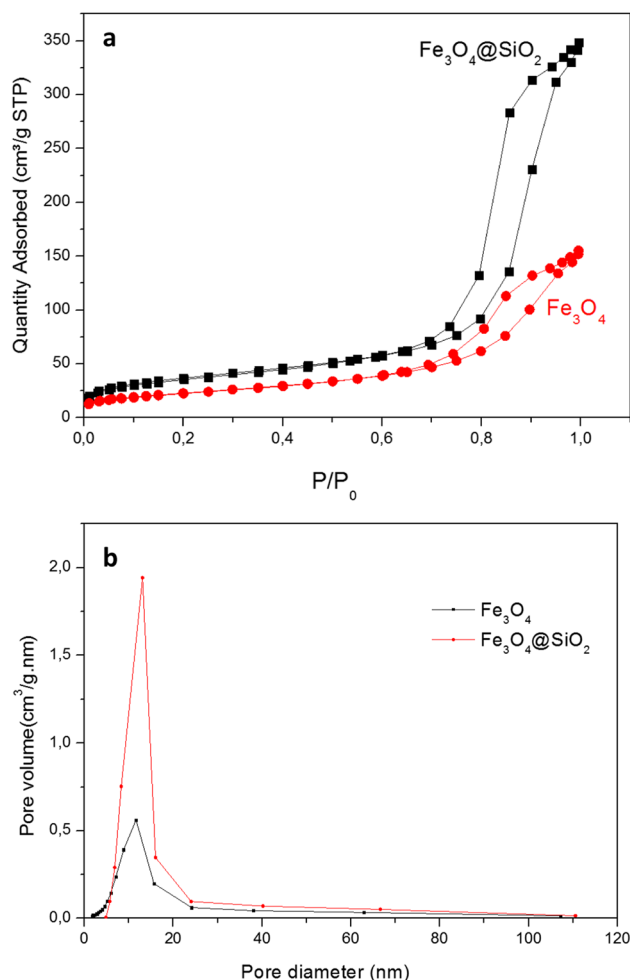
## 3.2 Elimination of CV under Varied Conditions

### 3.2.1 Effect of pH

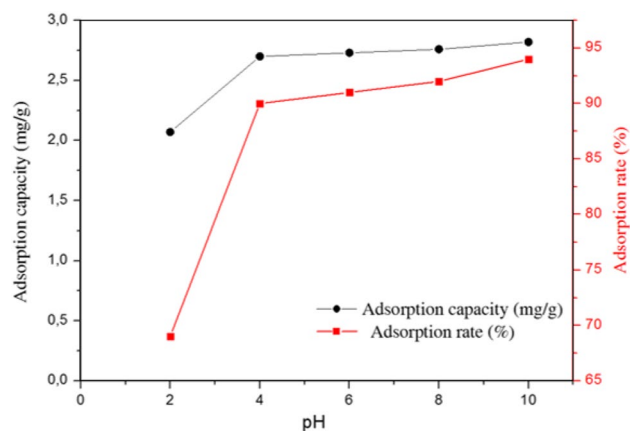
The pH is the main parameter in the uptake of CV on the  $\text{Fe}_3\text{O}_4@\text{SiO}_2$  nanocomposites. The results exhibited that the both adsorption capacity and CV adsorption rate improved by pH increase from 2 to 10 at a fixed initial dye concentration of  $10\text{mg}/\text{L}^{-1}$  and the adsorbent dose of 0.1 g and contact time of 180 min (Fig. 8). At acidic pH, the nanocomposites  $\text{Fe}_3\text{O}_4@\text{SiO}_2$  and CV molecules were protonated and electrostatic repulsion interaction between protonated CV and positively charged  $\text{Fe}_3\text{O}_4@\text{SiO}_2$  active sites lead to CV removal rate decrease [31]. The optimum pH value was fixed at pH 10. The same outcome was reported by Subhan et al. [32].

### 3.2.2 Effect of Adsorbent Dosage

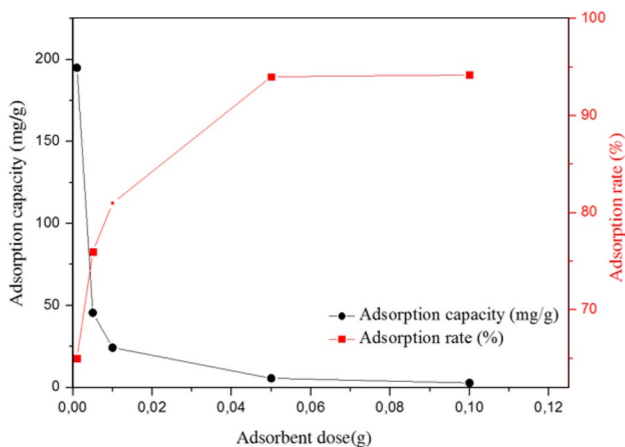
The impact of adsorbent dose of adsorption capacity and CV adsorption rate was studied in the range of 0.005 g to 0.1 g for in initial concentration  $10\text{mg}/\text{L}^{-1}$  and pH 10 and contact time 180 min. The results exhibited in Fig. 9. The adsorption capacity decreases from 195 to  $2.82\text{mg}/\text{g}^{-1}$  with



**Fig. 7** (a) Nitrogen adsorption-desorption isotherms and (b) BJH pore size distribution curves of  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4@\text{SiO}_2$



**Fig. 8** Effect of pH on adsorption capacity and adsorption rate of CV on  $\text{Fe}_3\text{O}_4@\text{SiO}_2$  ( $C_i = 10\text{mg}/\text{L}^{-1}$ ,  $V = 30\text{ml}$ , Time = 180 min,  $T = 298\text{K}$ , Adsorbent dose = 0.1 g)

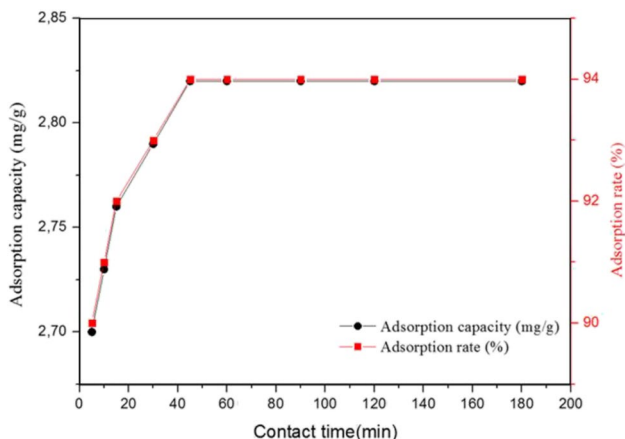


**Fig. 9** Effect of adsorbent dose on adsorption capacity and adsorption rate of CV dye on  $\text{Fe}_3\text{O}_4@\text{SiO}_2$  ( $C_i=10 \text{ mg L}^{-1}$ ,  $V=30 \text{ ml}$ , Time = 180 min,  $T=298 \text{ K}$ ,  $\text{pH}=10$ )

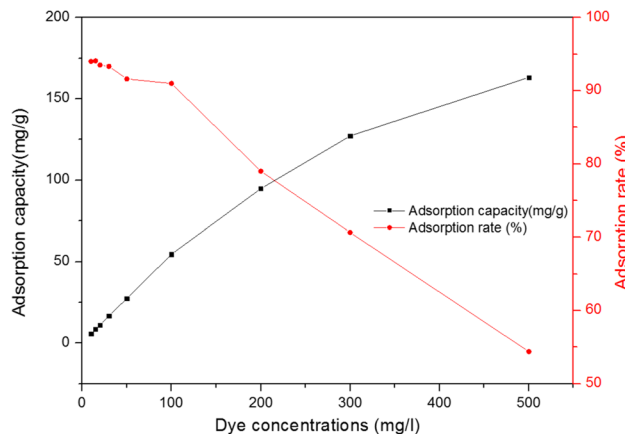
increasing adsorbent dose from 0.005 to 0.1 g that attributed to the availability of adsorption sites. However, the removal efficiency increases from 65 to 94% with increasing adsorbent dose as a consequence the higher number of active sites [9]. The nanosorbent dose was fixed at 0.05 g.

### 3.2.3 Influence of Contact Time

The time between pollutant and solid is a significant factor in wastewater purification; therefore, we also verified the decontamination period of the nanoadsorbent, as it is feasible to observe from Fig. 10. We discovered that the adsorption rate of CV increases rapidly over time. Based at the time study, 80.8% of CV dye was removed within 5 min. This trend in dye uptake is the result of the strong electrostatic



**Fig. 10** Effect of contact time on adsorption capacity and adsorption rate of CV dye on  $\text{Fe}_3\text{O}_4@\text{SiO}_2$  ( $C_i=10 \text{ mg L}^{-1}$ ,  $V=30 \text{ ml}$ ,  $T=298 \text{ K}$ ,  $\text{pH}=10$ , adsorbent dose =0.1 g)

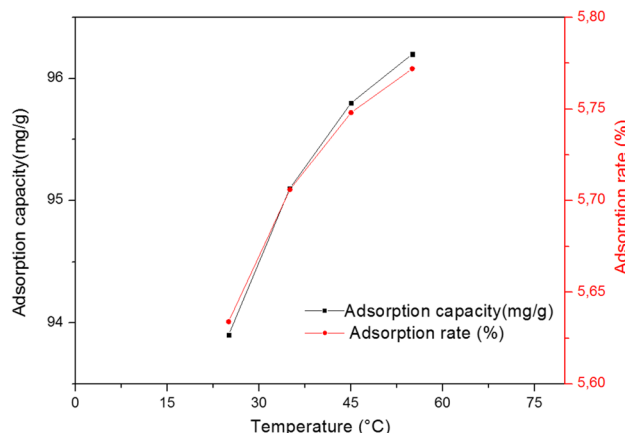


**Fig. 11** Effect of initial dye concentration on adsorption capacity and adsorption rate of CV dye on  $\text{Fe}_3\text{O}_4@\text{SiO}_2$  (adsorbent dose =0.05 g,  $V=30 \text{ ml}$ , Time = 60 min,  $T=298 \text{ K}$ ,  $\text{pH}=10$ )

interactions between CV and predominant silanol groups present on the outer surface of silica. Sorption equilibrium was attained in 60 min. At this time, the adsorbent surface becomes saturated. The test was pursued further for 120 minutes, but no significant increment was found in dye adsorption after 60 min shaking time. Therefore, remaining experiments were determined at 60 min.

### 3.2.4 Influence of Initial Dye Concentration

The influence of initial dye concentration of the adsorption of CV by  $\text{Fe}_3\text{O}_4@\text{SiO}_2$  nanocomposites was carried at the range of 10 to 500  $\text{mg L}^{-1}$  at fixed adsorbent dose 0.05 g, pH 10, contact time 60 min and room temperature. The adsorption capacity and CV adsorption rate was presented in Fig. 11. According to Fig. 11, the adsorption capacity was increased from



**Fig. 12** Effect of temperature on adsorption capacity and adsorption rate of CV dye on  $\text{Fe}_3\text{O}_4@\text{SiO}_2$  ( $C_i=10 \text{ mg L}^{-1}$ , adsorbent dose =0.05 g,  $V=30 \text{ ml}$ , Time = 60 min,  $\text{pH}=10$ )



**Table 1** Estimated parameters of the kinetic models for the CV dye adsorption onto Fe<sub>3</sub>O<sub>4</sub>@SiO<sub>2</sub>

Pseudo-first order			Pseudo-second order			
k <sub>1</sub> (min <sup>-1</sup> )	q (mg g <sup>-1</sup> )	R <sup>2</sup>	q <sub>exp</sub> (mg g <sup>-1</sup> )	k <sub>2</sub> (gmg <sup>-1</sup> min <sup>-1</sup> )	q (mgg <sup>-1</sup> )	R <sup>2</sup>
0.05	0.51	0.875	5.64	0.607	5.68	0.99

5.64 to 163.2 mg g<sup>-1</sup> with increasing initial dye concentration 10–500 mg L<sup>-1</sup>, respectively. The increase in the concentration of CV improves the interaction between the CV molecules and the surface of Fe<sub>3</sub>O<sub>4</sub>@SiO<sub>2</sub> nanocomposites. Although, The CV adsorption rate decreased from 94 to 54.4% with an increase in the CV concentration 10–500 mg l<sup>-1</sup> because the active sites was saturated in the adsorbent surface [33].

### 3.2.5 Influence of Temperature

The effect of temperature of the adsorption of CV by the Fe<sub>3</sub>O<sub>4</sub>@SiO<sub>2</sub> nanocomposites was performed at several temperatures including 25, 35, 45, 55 °C for an initial concentration of 10 mg L<sup>-1</sup> and pH of 10 and the adsorbent dose of 0.05 g and contact time of 60 min. The obtained results showed in Fig. 12. The adsorption capacity and CV adsorption rate increased from 5.63 to 5.77 mg g<sup>-1</sup> and 93.9 to 96.2%, respectively when temperature increased from 25 to 55 °C. This indicates that the adsorption of CV by Fe<sub>3</sub>O<sub>4</sub>@SiO<sub>2</sub> nanocomposites was an endothermic process [34], which confirmed by the positive ΔH° parameter on thermodynamic adsorption. The increase in the temperature reaction induces to changes in the size of the pores, the kinetic energy of CV molecules and the increase in diffusion rates [35].

### 3.2.6 Adsorption Kinetics

To explore the rate of CV adsorption by the nonadsorbent, the pseudo-first-order (Eq. 4) [36] and the

pseudo-second-order (Eq. 5) [37] models were adopted to correlate the time-dependent sorption data.

$$\ln(q_{eq} - q_t) = \ln q_{eq} - \frac{k_1}{2.303} t \quad (4)$$

$$\frac{t}{q_t} = \frac{1}{k_2 q_{eq}^2} + \frac{1}{q_{eq}} t \quad (5)$$

With,

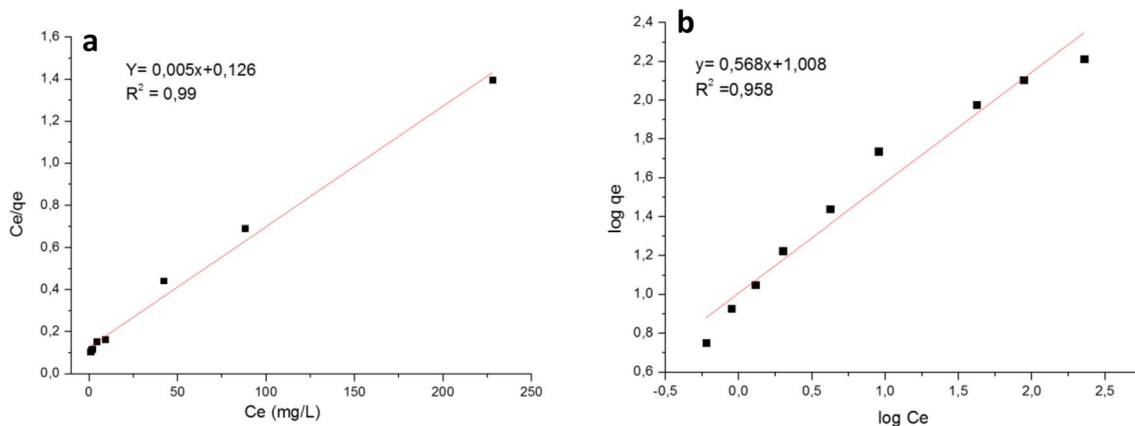
q<sub>eq</sub>: Amount of CV adsorbed at equilibrium (mg/g); q<sub>t</sub>: Amount of CV adsorbed on Fe<sub>3</sub>O<sub>4</sub>@SiO<sub>2</sub> (mg g<sup>-1</sup>) at the instant t; k<sub>1</sub> (min<sup>-1</sup>) and k<sub>2</sub> (g mg<sup>-1</sup> min<sup>-1</sup>): Pseudo-first and Pseudo-second rate constants.

The parameters of these kinetic models have been summarized in Table 1. The highest correlation (R<sup>2</sup>), and good conformity between the q<sub>eq,exp</sub> and q<sub>eq,cal</sub> values exhibited that the uptake of CV onto Fe<sub>3</sub>O<sub>4</sub>@SiO<sub>2</sub> could be well modeled with the pseudo-second-order, which is similar to the outcomes found by some other researchers for dye adsorption.

### 3.2.7 Adsorption Isotherms

The experimental data for CV on the Fe<sub>3</sub>O<sub>4</sub>@SiO<sub>2</sub> were fitted by the Langmuir and Freundlich models. Such models designate the sorption mechanism between CV and nanocomposites. The two models are expressed by (Eq. 6) and (Eq. 7).

*Langmuir model* [38]:



**Fig. 13** Langmuir isotherms (a) and Freundlich isotherm (b) for adsorption of CV on Fe<sub>3</sub>O<sub>4</sub>@SiO<sub>2</sub>



**Table 2** Isotherms parameters for CV adsorption onto Fe<sub>3</sub>O<sub>4</sub>@SiO<sub>2</sub>

Langmuir				Freundlich		
K <sub>L</sub>	R <sup>2</sup>	R <sub>L</sub>	Q <sub>m</sub> (mg g <sup>-1</sup> )	K <sub>F</sub>	n	R <sup>2</sup>
0.0045	0.98	0.818	200	2.76	1.736	0.958

$$q_{eq} = \frac{Q_m K_L C_{eq}}{1 + K_L C_{eq}} \tag{6}$$

$$k_d = \frac{q_{eq}}{C_{eq}} \tag{9}$$

Where C<sub>eq</sub> (mg l<sup>-1</sup>) is the equilibrium concentration of CV, q<sub>eq</sub> (mg g<sup>-1</sup>) is the equilibrium adsorption ability and Q<sub>m</sub> is a quantity of CV fixed per gram of nanosorbent (mg g<sup>-1</sup>). In addition, K<sub>L</sub> is the empirical constant.

*Freundlich model* [39]:

$$q_{eq} = K_F C_{eq}^{1/n} \tag{7}$$

With, K<sub>F</sub> (mg g<sup>-1</sup>)/(Lmg<sup>-1</sup>)<sup>n</sup> is adsorption capacity.

The Langmuir model correlated higher to the investigated procedure in assessment with that of the Freundlich model (Fig. 13) utilizing the experimental outcomes for the uptake equilibrium of CV by nanocomposites (Table 2), therefore, it may be deduced that the adsorption sites are homogeneous. Likewise, Q<sub>m</sub> for nanocomposites is 200 mg g<sup>-1</sup>. The adsorption capacity of Fe<sub>3</sub>O<sub>4</sub>@SiO<sub>2</sub> has been compared with different nanosorbents (Table 3). As can be observed, the Fe<sub>3</sub>O<sub>4</sub>@SiO<sub>2</sub> Q<sub>m</sub> value is more than this other adsorbents.

### 3.2.8 Thermodynamic Study

To understand the thermodynamic performances of CV adsorption onto Fe<sub>3</sub>O<sub>4</sub>@SiO<sub>2</sub>, thermodynamic functions were evaluated. Thermodynamic parameters, i.e., the change in the Gibbs free energy (ΔG°, kJ mol<sup>-1</sup>), the change in enthalpy (ΔH°, kJ mol<sup>-1</sup>), and the change in entropy (ΔS°, J mol<sup>-1</sup> K<sup>-1</sup>), are used to evaluate the thermodynamic feasibility and the nature of the process. The ΔH° (Eq. 8), ΔS° (Eq. 9), and ΔG° (Eq. 10) parameters were determined [44] and are listed in Table 4.

$$\Delta G^\circ = -RT \ln k_d \tag{8}$$

$$\ln k_d = \frac{\Delta S^\circ}{R} - \frac{\Delta H^\circ}{RT} \tag{10}$$

Table 4 exhibits the calculated data. The negative values of ΔG° verify the feasibility and spontaneity of the adsorption of CV dye on Fe<sub>3</sub>O<sub>4</sub>@SiO<sub>2</sub>. Additionally, the value of ΔG° changed from -5.46 to -7.46 kJ mol<sup>-1</sup>, whereas the temperature increased from 298 to 328 K, this suggesting that adsorption is highly spontaneous at higher temperatures.

The positive value of ΔH°, confirm the endothermic nature of the sorption process and the possibility of physical adsorption [45]. The positive values of ΔH° suggest the enhancement in randomness at the Fe<sub>3</sub>O<sub>4</sub>@SiO<sub>2</sub>/liquid interface with some structural modifications in the solute and material as well as the good affinity of Fe<sub>3</sub>O<sub>4</sub>@SiO<sub>2</sub> for the CV [46].

### 3.2.9 Adsorption Mechanism

The Fe<sub>3</sub>O<sub>4</sub>@SiO<sub>2</sub> surface contains active sites; these sites gave a platform for CV to adsorb on it Fig. 14 depicted a schematic sketch for the sorption mechanism of CV dye molecule onto Fe<sub>3</sub>O<sub>4</sub>@SiO<sub>2</sub> nanoadsorbent. Silica was first used to coat Fe<sub>3</sub>O<sub>4</sub> nanoparticles and then to synthesize Fe<sub>3</sub>O<sub>4</sub>@SiO<sub>2</sub> nanocomposites to ameliorate the surface area and consequently the number of adsorption sites. As mentioned early, after coating, the SSA increases from 81 to 133 m<sup>2</sup>g<sup>-1</sup>. Therefore, the nanocomposites Fe<sub>3</sub>O<sub>4</sub>@SiO<sub>2</sub>, which surface consists of silicium, carbon, oxygen, and iron was finally used as a nanoadsorbent for decolorization of textile waste water. In fact, pH affected the adsorption

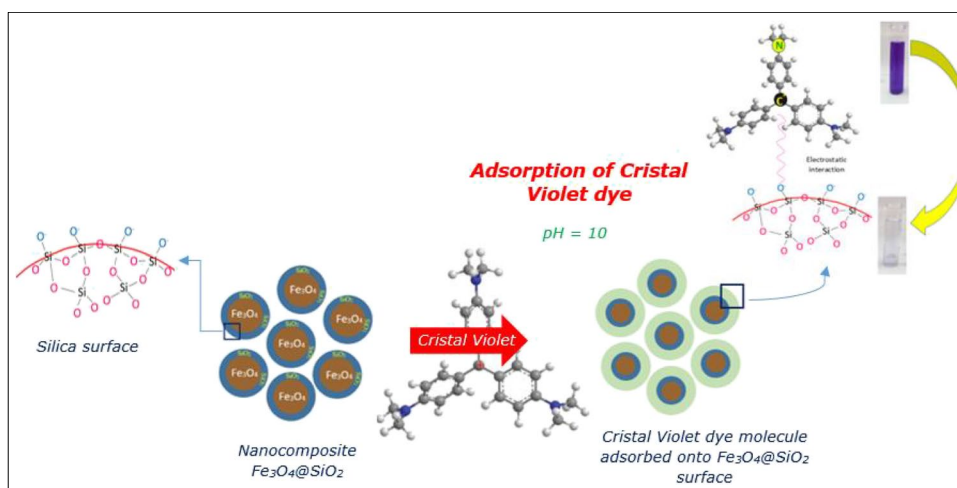
**Table 3** Comparison of maximum monolayer adsorption capacities of CV onto Fe<sub>3</sub>O<sub>4</sub>@SiO<sub>2</sub>

Adsorbents	Q <sub>m</sub> (mg g <sup>-1</sup> )	References
Fe <sub>3</sub> O <sub>4</sub> @ clinoptilolite	44.052	[40]
Magnetite Alginate	37.5	[41]
Fe <sub>3</sub> O <sub>4</sub> /ActivatedCarbon	35.31	[42]
Fe <sub>3</sub> O <sub>4</sub> @chitosan	183.2	[43]
Fe <sub>3</sub> O <sub>4</sub> @SiO <sub>2</sub>	200	This work

**Table 4** Thermodynamic parameters for adsorption of CV onto Fe<sub>3</sub>O<sub>4</sub>@SiO<sub>2</sub>

Temperature (K)	ΔG° (KJ mol <sup>-1</sup> )	ΔH° (J mol <sup>-1</sup> )	ΔS° (J mol <sup>-1</sup> K <sup>-1</sup> )
298	-5.46		
308	-6.17	188.81	25.95
318	-6.91		
328	-7.42		

**Fig. 14** Schematic sketch for the sorption mechanism of CV dye molecule onto  $\text{Fe}_3\text{O}_4@ \text{SiO}_2$  nano-adsorbent



behavior and mechanism. At  $\text{pH} = 10$ , the surface functional groups of  $\text{Fe}_3\text{O}_4@ \text{SiO}_2$  were deprotonated and made it negatively charged. This negative charge resulted in electrostatic interaction with positively charged groups of CV. While decreasing the  $\text{pH}$ , the surface charge density of  $\text{Fe}_3\text{O}_4@ \text{SiO}_2$  increased due to protonation, and electrostatic repulsion between positive CV and  $\text{Fe}_3\text{O}_4@ \text{SiO}_2$  surface lowered the percentage adsorption.

## 4 Conclusions

$\text{Fe}_3\text{O}_4@ \text{SiO}_2$  core–shell nanocomposites were synthesized by siliceous sand using co-precipitation method. Fourier transforms infrared spectra and X-ray diffraction revealed that  $\text{Fe}_3\text{O}_4$  was successfully coated by silica. According to TEM results, the  $\text{Fe}_3\text{O}_4$  was spherical, regular in shape, and the  $\text{SiO}_2$  coating layer was uniform. The size of  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4@ \text{SiO}_2$  were about 34 and 36 nm, respectively. The BET method indicated that the coating of the surface of magnetite by silica increases the surface area of  $\text{Fe}_3\text{O}_4@ \text{SiO}_2$  compared with  $\text{Fe}_3\text{O}_4$ . Moreover, this work primarily aimed at determining the optimal variant of the process to maximize the adsorption rate (R) and the adsorption capacity ( $q_e$ ). The findings displayed that the optimum conditions for the solution  $\text{pH}$ , contact time, sorbent amount and initial dye concentration were 10.0, 60 min, 0.05 g, 10  $\text{mg L}^{-1}$  respectively, were given maximum R of 94% and an at most capacity  $Q_{\text{max}}$  of 200  $\text{mg g}^{-1}$ . Thermodynamic parameters designated that CV adsorption on  $\text{Fe}_3\text{O}_4@ \text{SiO}_2$  was endothermic. In this work, the silica coated magnetite as a low-cost material is highly efficient and well suited for the elimination of dyes and in particular CV.

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**Data Availability** The authors declare that the data supporting the findings of this study are available within the article and its supplementary information are available by request.

## Declarations

**Competing Interests** The authors have non relevant financial or non-financial to disclose.

**Ethical Approval** Not Applicable.

**Consent for Publications** All the authors of the manuscript mutually agree on submission and publication in the journal.

**Consent to Participate All** Authors contributed to the work and revised the manuscript.

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