# Electrochemical preparation of the Fe–Ni36 Invar alloy from a mixed oxides precursor in molten carbonates

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**Abstract:** The Fe–Ni36 alloy was prepared via the one-step electrolysis of a mixed oxides precursor in a molten Na<sub>2</sub>CO<sub>3</sub>–K<sub>2</sub>CO<sub>3</sub> eutectic melt at 750°C, where porous Fe<sub>2</sub>O<sub>3</sub>–NiO pellets served as the cathode and the Ni10Cu11Fe alloy was an inert anode. During the electrolysis, NiO was preferentially electro-reduced to Ni, then Fe<sub>2</sub>O<sub>3</sub> was reduced and simultaneously alloyed with nickel to form the Fe–Ni36 alloy. Different cell voltages were applied to optimize the electrolytic conditions, and a relatively low energy consumption of 2.48 kW·h·kg<sup>-1</sup> for production of FeNi36 alloy was achieved under 1.9 V with a high current efficiency of 94.6%. The particle size of the alloy was found to be much smaller than that of the individual metal. This process provides a low-carbon technology for preparing the Fe–Ni36 alloy via molten carbonates electrolysis.

Keywords: molten carbonates; cyclic voltammetry; electro-reduction; inert anode; Invar36 alloy

# 1. Introduction

Iron and Ni alloys possessing excellent mechanical properties and low cost are one of the most widely used structure materials. For example, near room temperature, Fe-Ni alloys with 30wt%-40wt% Ni have coefficients of thermal expansion (CTEs) lower than those of pure Fe (CTE =  $12 \times 10^{-6}$  $^{\circ}C^{-1}$ ) and Ni (CTE =  $13 \times 10^{-6} \circ C^{-1}$ ). In particular, the Fe–Ni alloys with 36wt% Ni exhibit the lowest CTE (approximately  $1 \times 10^{-6} \,^{\circ}\text{C}^{-1}$ ) among all Fe–Ni alloys [1–3]. The Fe-Ni36 alloy and those of similar composition are denoted "Invar alloys." The Invar alloys are widely used in various applications, such as optical and laser measuring systems, bimetallic strips, shadow masks, precision instruments, large molds for aerospace, and storage vessels for liquefied natural gas [1,3], because of their high temperature strength and oxidation and corrosion resistance. Currently, the preparation of Ni-Fe alloys involves multiple steps, including a carbothermic reduction route for preparing Fe and Ni and an alloying process in which Ni and Fe are mixed at a high temperature [4].

Eletro-deoxidation of solid oxides in molten salts, also called the FFC Cambridge Process, is a straightforward way to prepare metals and/or alloys [5–7]. A variety of alloys have been successfully prepared from their corresponding

oxides or oxide mixtures, i.e., TiFeNi [8], TiNi [9–10], TbFe<sub>2</sub> [11], LaNi<sub>5</sub> [12], TbNi<sub>5</sub> [13], and NiAl [14]. Inspired by the FFC Cambridge process, researchers substituted molten hydroxides [15] and carbonates [16] for molten halide to prepare other noble metals, such as Fe, Co, and Ni [16–18]. The merit of replacing molten halide (e.g., CaCl<sub>2</sub>) is the opportunity to use a cost-effective inert anode. The drawback of using molten hydroxide and carbonate is the relatively narrow electrochemical window limiting the preparation of reactive metals [19–20].

A homemade Ni10Cu11Fe inter-anode can serve as a long-lasting oxygen-evolution anode to electrochemically split Fe<sub>2</sub>O<sub>3</sub>, NiO, and Co<sub>3</sub>O<sub>4</sub> into Fe, Ni, Co, and oxygen [16–18]. Thermodynamically, Ni and other metals having similar electronegativity can be reduced to their corresponding metals/alloys in molten Na<sub>2</sub>CO<sub>3</sub>–K<sub>2</sub>CO<sub>3</sub>. To test the durability of the long-lasting inert anode, the oxidation behavior of the Ni10Cu11Fe inter-anode was investigated, revealing that a three-layer structure oxide scale plays a central role in maintaining the functionality of the inert anode [21–22]. To date, no paper has reported the preparation of ferro-alloys in molten carbonate, and the possibility of the alloying process still needs to be confirmed. Since the wide application of Febased alloys, a molten carbonate with a low-cost inert anode could pave an environmentally friendly way to preparing



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value-added alloys in one step.

Herein, we report the preparation of the Fe–Ni36 alloy via one-step electrolysis of a mixed oxides precursor in molten carbonates. The reduction process of the Fe<sub>2</sub>O<sub>3</sub>–NiO mixture in molten Na<sub>2</sub>CO<sub>3</sub>–K<sub>2</sub>CO<sub>3</sub> and the optimized electrolytic condition, current efficiency, and energy consumption were studied using cyclic voltammetry and constant cell voltage electrolysis.

## 2. Experimental

#### 2.1. Materials and chemicals

Fe<sub>2</sub>O<sub>3</sub> and NiO powders (Fe : Ni mass ratio of 64:36; analytical purity; Sinopharm Chemical Regent Co. Ltd., China) were ball-mixed for 12 h, and the mixed oxides were mixed with 20wt% NH<sub>4</sub>HCO<sub>3</sub> manually and made into pellets by die-pressing at a pressure of 6 MPa. Afterward, the oxide pellets were sintered in a muffle furnace at 800°C for 2 h to ensure a reasonable mechanical strength. The NH<sub>4</sub>HCO<sub>3</sub> was added to increase the porosity of the pellets through the decomposition of NH<sub>4</sub>HCO<sub>3</sub> at a high temperature. Then, the sintered pellets were attached to an iron wire (2 mm in diameter) working as a cathode. A Ni10Cu11Fe alloy rod (20 mm in diameter) was applied as an anode, and the detailed preparation process was reported in our previous work [18]. A 500 g eutectic Na<sub>2</sub>CO<sub>3</sub>-K<sub>2</sub>CO<sub>3</sub> mixture (59:41 in molar ratio; analytical purity; Sinopharm Chemical Regent Co. Ltd., China) was placed in an alumina crucible in a closed-end, sealed steel reactor. Before the electrolysis, the mixed salts were heated to 850°C to melt the electrolyte, and then the temperature was lowered to 750°C for electrochemical measurements. Pre-electrolysis was conducted under a constant cell voltage of 1.8 V with a Ni10Cu11Fe inert anode and a nickel sheet cathode for 2 h to remove the residual water and, if any, other impurities from the salts. All experiments were performed under an argon flow (>99.999%; Wuhan Iron and Steel Group Corp., China).

#### 2.2. Cyclic voltammetry

A three-electrode setup was applied to conduct cyclic voltammetry (CV) measurements controlled by a CHI1140a electrochemical workstation (Shanghai Chenhua Instrument Co. Ltd., China) to investigate the reduction mechanisms of NiO and Fe<sub>2</sub>O<sub>3</sub>. A nickel wire (1 mm in diameter, 5–6 mm in length, immersed in the melt) and an oxide coated nickel or iron wire were used as the working electrodes. The reference electrode was a silver wire dipped in a Ag<sub>2</sub>SO<sub>4</sub> (2mol%) eutectic melt (Li<sub>2</sub>CO<sub>3</sub> : Na<sub>2</sub>CO<sub>3</sub> : K<sub>2</sub>CO<sub>3</sub> molar ratio = 43.5:25:31.5) in a one-end closed mullite tube, and a Ni10Cu11Fe alloy rod was used as the counter electrode. The oxide coated nickel or iron wire was fabricated by repeatedly dipping a nickel wire (1 mm in diameter) into an oxide- or mixed-oxide-ethanol suspension (3 g of oxides in 5 mL of

ethanol under sonication), then the ethanol was dried, giving an oxide powder coated metal wire working electrode. Unless otherwise specified, all potentials were collected with respect to the reference electrode.

#### 2.3. Two-electrode constant cell voltage electrolysis

Two-electrode constant cell voltage electrolysis was conducted to prepare the Fe-Ni36 alloy from the pre-sintered Fe<sub>2</sub>O<sub>3</sub>-NiO mixture pellets. The sintered Fe<sub>2</sub>O<sub>3</sub>-NiO pellets  $(\sim 0.6 \text{ g})$  were wrapped with a nickel foam and then attached to an iron wire (2 mm in diameter) working as the cathode in conjunction with a Ni10Cu11Fe inert anode. Constant electrolysis was applied between the cathode and anode in a potential range from 1.0 to 2.2 V, and the electrolysis was controlled using a DC power system (Shenzhen Neware Electronic Ltd., China). After electrolysis, the obtained products were washed in distilled water to remove the residual molten salt, followed by vacuum-drying and conservation in ethanol. The electrolytic samples were characterized using scanning electron microscopy (SEM, FEI Sirion field emission), X-ray diffraction spectroscopy (XRD, Shimadzu X-ray 6000 with Cu K<sub>a1</sub> radiation at  $\lambda = 0.15405$  nm), and energy-dispersive X-ray spectroscopy (EDX, EDAX GENESIS 7000).

#### 3. Results and discussion

#### 3.1. CV measurements

Cyclic voltammetry was conducted to investigate the reduction mechanisms of NiO and Fe<sub>2</sub>O<sub>3</sub> in the Na<sub>2</sub>CO<sub>3</sub>–K<sub>2</sub>CO<sub>3</sub> eutectic melt. As shown in Fig. 1, only one reduction peak was present for the NiO coated nickel working electrode, indicating a one-step reduction process for NiO. For the Fe<sub>2</sub>O<sub>3</sub> coated iron working electrode, two reduction peaks were observed for Fe<sub>2</sub>O<sub>3</sub> reduction, which are related to electrochemical intercalation of Na<sup>+</sup> into Fe<sub>2</sub>O<sub>3</sub> to form NaFe<sub>2</sub>O<sub>3</sub> and NaFeO<sub>2</sub> (reactions (1) and (2)) and electro-reduction of NaFeO<sub>2</sub> to iron metal (reaction (3)) [23]. The reduction peak of NiO began at -1.34 V (peak a3 in Fig. 1, reaction (4)), which was close to the first reduction peak of Fe<sub>2</sub>O<sub>3</sub> (peak a1 in Fig. 1, -1.40 V), suggesting that NiO can be more easily electro-reduced to metal than Fe<sub>2</sub>O<sub>3</sub>.

$$Fe_2O_3 + Na^+ + e = NaFe_2O_3$$
<sup>(1)</sup>

 $2NaFe_2O_3 + Na^+ + e = 3NaFeO_2 + Fe$ (2)

$$NaFeO_2 + 3e = Fe + Na^+ + 2O^2$$
 (3)

$$NiO + 2e = Ni + O^{2^{-1}}$$
(4)

#### 3.2. Two-electrode constant cell voltage electrolysis

As shown in Fig. 2, NiO reacted with  $Fe_2O_3$  to form  $NiFe_2O_4$  at a high temperature of 800°C, and the excess amount of  $Fe_2O_3$  still maintained the original form.

Constant cell voltage electrolysis was used to reduce the



Fig. 1. Cyclic voltammograms of oxides coated electrodes at 750°C with a scan rate of 100 mV/s.



Fig. 2. XRD patterns of  $Fe_2O_3$ , NiO, and the mixed oxides of  $Fe_2O_3$  and NiO (NiO&Fe\_2O\_3) after sintering at 800°C for 2 h.

mixed oxide precursor. Fig. 3 shows the XRD patterns of the electrolytic products under cell voltages from 1.0 to 2.2 V for 11 h. Under 1.5 V, the major diffraction peaks of NiO, Fe<sub>2</sub>O<sub>3</sub>, and NiFe<sub>2</sub>O<sub>4</sub> disappeared, suggesting that reduction occurred. The theoretical decomposition voltage for NiO at 750°C is 0.76 V, and it can be electro-reduced at a low cell voltage of 0.9 V [18]. The three new main diffraction peaks located at  $44.5^{\circ}$ ,  $51.8^{\circ}$ , and  $76.4^{\circ}$  should ascribe to the freshly formed Ni, while other peaks located at 21.3° 29.6°, 33.5°, and 36.9° should be attributed to the intermediate compounds NaFe<sub>2</sub>O<sub>3</sub> and NaFeO<sub>2</sub> [23]. When the cell voltage increased to 1.8 V, only the three main diffraction peaks were detected, indicating that the intermediate compounds were electro-reduced completely. Note that no Fe was observed under different cell voltages, suggesting that the reduction of iron compounds and generation of Ni-Fex alloys occurred simultaneously (Ni and the Fe-Ni36 alloy have identical characteristic diffraction peaks). This finding means that the reduction of Fe on the preformed Ni directly resulted in formation of Ni-Fe alloys. As the Ni-Fe solid solution formed, the main diffraction peaks negatively shifted to 43.9°, 51.2°, and 75.3°, respectively.



Fig. 3. XRD patterns of the electrolytic products obtained from the indicated constant cell voltages electrolysis experiments at 750°C in a Na<sub>2</sub>CO<sub>3</sub>–K<sub>2</sub>CO<sub>3</sub> eutectic melt.

The SEM images of the electrolytic products obtained under different cell voltages are shown in Fig. 4. Under a cell voltage lower than 1.5 V (Figs. 4(a)–4(c)), the particles were uniform and the SEM images of the samples were similar. When the cell voltage was increased to 1.7-1.8 V (Figs. 4(d)–4(e)), coral-like metal structures began to appear [23]. As the cell voltage increased from 1.9 to 2.2 V (Figs. 4(f)–4(i)), a uniform coral-like structure was observed, suggesting that the mixed oxides had been completely reduced to alloys. Therefore, a cell voltage of 1.9 V was selected for investigating the reduction process of the mixed oxides in detail.

The XRD patterns of samples obtained under 1.9 V for different electrolysis durations are shown in Fig. 5. Before electrolysis, the pellet consisted of NiFe<sub>2</sub>O<sub>4</sub> and Fe<sub>2</sub>O<sub>3</sub>. After 0.5 h, weak diffraction peaks of nickel metal were detected, and their intensity increased with increasing electrolysis time from 0.5 to 4 h. After 4 h, the diffraction peaks of NiFe<sub>2</sub>O<sub>4</sub> disappeared, and the major diffractions peaks came from the Fe–Ni alloy. After electrolysis for 11 h, the oxides were fully reduced to form the Fe–Ni36 alloy. Notably, the main diffraction peaks also negatively shifted with a prolonged electrolysis time, which suggested that iron was progressively reduced and combined with Ni to form a Ni–Fe solid solution.

The SEM images of the mixed oxides precursor and the electrolytic products obtained under 1.9 V with different electrolysis times are shown in Fig. 6. Before electrolysis, the mixed oxides were irregular particles (Fig. 6(a)), and no obvious change was observed (Figs. 6(b) and 6(c)) after 1 h. After electrolyzed for 2 h (Fig. 6(d)), aggregation occurred between the particles. Larger granules were observed after 4 h (Fig. 6(e)), suggesting that nickel metal was obtained. After 6 h, a coral-like morphology was observed (Fig. 6(g)), and the remaining fine particles became fewer. After 11 h (Figs. 6(h))



Fig. 4. SEM images of the obtained products of NiO–Fe<sub>2</sub>O<sub>3</sub> mixed oxides pellets after electrolysis under constant cell voltages of (a) 1.0 V, (b) 1.3 V, (c) 1.5 V, (d) 1.7 V, (e) 1.8 V, (f) 1.9 V, (g) 2.0 V, (h) 2.1 V, and (i) 2.2 V at 750°C in a Na<sub>2</sub>CO<sub>3</sub>–K<sub>2</sub>CO<sub>3</sub> eutectic melt for 11 h.



Fig. 5. XRD patterns of the obtained products of NiO and  $Fe_2O_3$  mixed oxides pellets after electrolysis under a constant cell voltage of 1.9 V over the indicated electrolysis times at 750°C in a  $Na_2CO_3$ - $K_2CO_3$  eutectic melt.

and 6(i)), the particles continually grew and linked with each other, indicating that the mixed oxides were fully electro-reduced to Fe–Ni36.

Fig. 7 displays the SEM images of the electro-reduced nickel, iron, and Fe-Ni36 alloy obtained in molten carbonates (Na<sub>2</sub>CO<sub>3</sub>-K<sub>2</sub>CO<sub>3</sub>) at 750°C. The particle sizes of the electrolytic products were larger than those of their corresponding oxide precursors. For NiO, the morphology of the electrolytic nickel metal normally exhibited nodular particles with a particle size of  $5-10 \mu m$  (Fig. 7(a)). The electrolytic Fe exhibited an interconnected coral-like morphology with a particle size range of  $5-10 \,\mu\text{m}$  (Fig. 7(b)). For the mixed oxides of NiO-Fe<sub>2</sub>O<sub>3</sub>, the electrolytic alloy had a similar morphology with the coral-like sponge iron (Fig. 7(c)), but its particle size range was  $1-2 \mu m$ , which was smaller than that of iron. According to the phase diagram of Fe-Ni, Ni and Fe form a solid solution at 750°C, revealing that the electrolytic product was the Fe-Ni36 alloy and not the separated Ni and Fe. Interestingly, the Ni-Fe alloy particles were obviously smaller than the individual metal particles at the same temperature, which should be closely related to the formation process of the Ni-Fe alloy. As discussed above, NiO is preferentially reduced to the Ni cation during the electrochemical reduction of the mixed oxides. Nearby iron oxides are reduced and the fresh Fe atoms diffuse to the Ni cation to form a Ni-Fe solution. The mobility of the Ni-Fe cation is posY.P. Dou et al., Electrochemical preparation of the Fe-Ni36 Invar alloy from a mixed oxides precursor in molten ...



Fig. 6. SEM images of the obtained products of NiO and Fe<sub>2</sub>O<sub>3</sub> mixed oxides after electrolysis under constant cell voltages of 1.9 V with different electrolysis times of (a) 0 h, (b) 0.5 h, (c) 1 h, (d) 2 h, (e) 4 h, (f) 6 h, (g) 8 h, and (h, i) 11 h at 750°C in a Na<sub>2</sub>CO<sub>3</sub>–K<sub>2</sub>CO<sub>3</sub> eutectic melt.



Fig. 7. SEM images of the electro-reduced (a) nickel, (b) iron, and (c) Fe–Ni36 alloy prepared at 750°C in a Na<sub>2</sub>CO<sub>3</sub>–K<sub>2</sub>CO<sub>3</sub> eutectic melt.

sibly lower than that of the Ni or Fe cation. On the other hand, the reduction of the iron oxide intermediate compound is more sluggish, so it might become a diffusion barrier for the preferentially reduced Ni and Ni–Fe.

Fig. 8 shows the digital photos of NiO–Fe<sub>2</sub>O<sub>3</sub> mixed oxide pellets before (left) and after (right) electrolyzed under 1.9 V for 11 h at 750°C in a Na<sub>2</sub>CO<sub>3</sub>–K<sub>2</sub>CO<sub>3</sub> eutectic melt. The electrolytic product had metallic luster and good conductivity, and the size of the original pellet apparently shrank after 11 h of electrolysis because of the removal of oxygen.

The element distributions of Fe and Ni were characterized by an EDX element mapping analysis (Fig. 9). The Fe and Ni



Fig. 8. Digital photos of mixed NiO and Fe<sub>2</sub>O<sub>3</sub> pellets before (left) and after (right) electrolysis at 750°C with a cell voltage of 1.9 V in a Na<sub>2</sub>CO<sub>3</sub>-K<sub>2</sub>CO<sub>3</sub> eutectic melt for 11 h.



Fig. 9. Elemental distribution maps of the NiO and Fe<sub>2</sub>O<sub>3</sub> mixed oxides pellet after electrolysis under a cell voltage of 1.9 V for 11 h at 750°C in a Na<sub>2</sub>CO<sub>3</sub>–K<sub>2</sub>CO<sub>3</sub> eutectic melt.

were distributed uniformly, further confirming that they underwent a full alloying process. Therefore, the electrochemical alloying process was realized in the electro-deoxidation process at a relatively low temperature. Note that a small amount of element O was present because of the surface oxidation when the electrolytic pellet was exposed to the air and water.

Current–time plots recorded from the electrochemical reduction of the mixed oxides pellets under different cell voltages are shown in Fig. 10. All curves had several current plateaus before reaching a stable platform, suggesting that the reduction of the oxides pellets involved multiple steps, which agreed with the CV measurements. As with the XRD and CV analyses, the different plateaus should be due to the reduction of NiO, then electrochemical intercalation of Na<sup>+</sup> into iron oxide, and finally the reduction of NaFe<sub>2</sub>O<sub>3</sub> and NaFeO<sub>2</sub> to generate Fe–Ni alloy. A higher cell voltage corresponded to a larger current and shorter reduction time.

The current efficiency and energy consumption of the electrolysis under different cell voltages are summarized in Table 1. Note that the energy used for heating the furnace was not included in the calculation of energy consumption of the electrolysis. The optimized current efficiency and energy consumption were achieved under a cell voltage of 1.9 V, and were 94.62% and 2.48 kW·h·kg<sup>-1</sup> for production of FeNi36



Fig. 10. Current-time plots of NiO and  $Fe_2O_3$  mixed oxides pellets electrolyzed under different cell voltages for 11 h at 750°C in a Na<sub>2</sub>CO<sub>3</sub>-K<sub>2</sub>CO<sub>3</sub> eutectic melt. Inset shows the partial drawing.

alloy, respectively. More importantly, the Ni10Cu11Fe alloy anode can produce oxygen during electrolysis [24]. The alloy anode survived over 800 h without any dimensional change upon consecutive electrolysis experiments in molten carbonates. This result further confirmed the inert nature of the alloy anode, enabling a low-emission electrolysis process in molten carbonates.

Electrolytic conditions	Mass of Fe <sub>2</sub> O <sub>3</sub> and NiO / g	Actual consumed electric quantity / $(mA \cdot h^{-1})$	Current efficiency / %	Energy consumption / $(kW \cdot h \cdot kg^{-1})$
1.9 V, 11 h	1.4251	1286.5	94.62	2.48
2.0 V, 11 h	1.6365	1477.4	91.39	2.70
2.1 V, 11 h	1.6077	1451.4	88.35	2.94
2.2 V, 11 h	1.3806	1246.3	71.62	3.80

Table 1. Current efficiency and energy consumption for electro-reduction of NiO and Fe<sub>2</sub>O<sub>3</sub> mixed oxides pellets under different electrolytic conditions

# 4. Conclusion

The Fe-Ni36 alloy was successfully prepared by electrodeoxidation of Fe<sub>2</sub>O<sub>3</sub>-NiO precursors using a one-step process in molten Na<sub>2</sub>CO<sub>3</sub>-K<sub>2</sub>CO<sub>3</sub> at 750°C. After sintering, the oxide precursor consisted of NiFe<sub>2</sub>O<sub>4</sub> and Fe<sub>2</sub>O<sub>3</sub>. During the electrolysis, Ni was preferentially extracted by electrochemical reduction of NiFe2O4, and then the reduction of iron oxides and formation of Ni-Fe alloy simultaneously occurred. No pure iron phase was observed during the electrolysis. The particle size of the obtained Fe-Ni36 alloy was smaller than those of iron and nickel, and Ni distributed uniformly in the Fe matrix. Under a constant cell voltage of 1.9 V, a current efficiency of 94.6% and an energy consumption of 2.48 kW·h·kg<sup>-1</sup> for production of FeNi36 alloy were achieved. The present study provides an energy-effective and lowemission approach to prepare Fe-Ni36 with the assistance of a low-cost inert anode at an intermediate temperature, and this method can also be used to prepare the other Fe-based alloys.

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