# **Stress corrosion cracking of X80 pipeline steel exposed to high pH solutions with different concentrations of bicarbonate**

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**Abstract:** Susceptibilities to stress corrosion cracking (SCC) of X80 pipeline steel in high pH solutions with various concentrations of HCO*<sup>−</sup>* <sup>3</sup> at a passive potential of –0.2 V vs. SCE were investigated by slow strain rate tensile (SSRT) test. The SCC mechanism and the effect of HCO*<sup>−</sup>* <sup>3</sup> were discussed with the aid of electrochemical techniques. It is indicated that X80 steel shows enhanced susceptibility to SCC with the concentration of HCO*<sup>−</sup>* <sup>3</sup> increasing from 0.15 to 1.00 mol/L, and the susceptibility can be evaluated in terms of current density at  $-0.2$  V vs. SCE. The SCC behavior is controlled by the dissolution-based mechanism in these circumstances. Increasing the concentration of HCO*<sup>−</sup>* <sup>3</sup> not only increases the risk of rupture of passive films but also promotes the anodic dissolution of crack tips. Besides, little susceptibility to SCC is found in dilute solution containing 0.05 mol/L HCO<sub>3</sub> for X80 steel. This can be attributed to the inhibited repassivation of passive films, manifesting as a more intensive dissolution in the non-crack tip areas than at the crack tips.

**Keywords:** pipeline steel; stress corrosion cracking; bicarbonate; passive films

# **1. Introduction**

Stress corrosion cracking (SCC), as a typical localized corrosion, is one of the most dangerous failure forms occurring in buried pipelines used for high-pressure natural gas transmission, which usually causes sudden leakage and rupture without awareness. This may affect the service safety of pipeline steels [1]. X80 pipeline steel is becoming one of the most widely applied pipe materials because of its high strength and toughness [2]. Although upgrading in steel-grade allows economic benefits and a better performance, this may sacrifice substantial SCC resistance [3].

According to Refs. [1,4], high pH SCC can be attributed primarily to a dissolution-based mechanism, i.e., crack propagation was facilitated by anodic dissolution and repeated rupture of passive films at the crack tips. Many researchers [5-7] believed that the resistance to SCC relied on the properties of passive films formed in concentrated carbonate/bicarbonate solutions. The rupture of passive films usually led to the occurrence of pitting [8-10], which was probably the main cause of initiation of SCC, especially under the application of anodic potentials [11].

Parkins and Zhou [12] found that SCC behavior could be influenced to some extent by the concentration of HCO*<sup>−</sup>* <sup>3</sup> , with the increase of crack growth rate as the concentration of HCO*<sup>−</sup>* <sup>3</sup> increased. Previous work of our research group [13-14] confirmed that the increase in HCO*<sup>−</sup>* 3 concentration deteriorated the corrosion resistance of passive films. However, the relationship between the SCC behavior of X80 pipeline steel and the rupture of passive films assisted by HCO*<sup>−</sup>* <sup>3</sup> in high pH solutions is still unknown. Furthermore, whether the SCC behavior follows the dissolution-based mechanism at passive potential needs verifying.

In light of this, susceptibilities to SCC of X80 pipeline steel in high pH solutions with various concentrations of HCO*<sup>−</sup>* <sup>3</sup> at a passive potential were investigated in this work by slow strain rate tensile (SSRT) test. Based on potentiodynamic polarization curves obtained at quick and slow sweep rates and electrochemical impedance spectroscopy (EIS) measurements, the relationship between the SCC behavior and the HCO*<sup>−</sup>* <sup>3</sup> assisted film rupture was discussed.

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# **2. Experimental**

## **2.1. Specimens and solutions**

Specimens used in this work were made of X80 pipeline steel supplied by Bao Steel Co. Ltd., with the chemical composition (wt%) of 0.036 C, 0.197 Si, 1.771 Mn, 0.012 P, 0.002 S, 0.223 Cr, 0.278 Ni, 0.220 Cu, 0.021 Al, 0.019 Ti, 0.184 Mo, 0.001 V, 0.110 Nb, 0.005 N, and Fe balance. Its yielding strength was 640 MPa and the ultimate tensile strength was 750 MPa. The specimens used in conventional electrochemical measurements were embedded in epoxy resin with the working area of  $1.0 \text{ cm}^2$ . For SSRT test, smooth flat tensile specimens were used with the gauge size of 36 mm in length, 6 mm in width, and 2 mm in thickness, in which the long axis of the specimens was parallel to the circumferential direction of the steel pipe. Prior to the test, all the specimens were ground from 60 grit up to 1000 grit silicon carbide paper, then rinsed with deionized water, and degreased in acetone. Bicarbonate solutions consisting of 0.05 mol/L NaCl and different concentrations of HCO*<sup>−</sup>* <sup>3</sup> (0.05-1.00 mol/L) were used as the testing solution, and the pH value of solution was kept at approximately 8.31.

#### **2.2. Experimental methods**

Susceptibilities to SCC of X80 pipeline steel were evaluated using the SSRT method. The strain rate was controlled at  $1 \times 10^{-6}$  s<sup>-1</sup>. During the test, a passive potential of  $-0.2$  V vs. SCE was adopted, which was obtained from the potentiodynamic polarization curves at slow sweep rate. In order to characterize the susceptibility qualitatively, reduction-in-area loss  $(I_{\psi})$  and fracture strength loss  $(I_{\sigma})$  were introduced to describe the toughness and strength deterioration, respectively, and were defined as

$$
I_{\psi} = \frac{\psi_0 - \psi_E}{\psi_0} \times 100\% \tag{1}
$$

$$
I_{\sigma} = \frac{\sigma_0 - \sigma_E}{\sigma_0} \times 100\%
$$
 (2)

where  $\psi_{\rm E}$ ,  $\psi_0$ ,  $\sigma_{\rm E}$ , and  $\sigma_0$  were corresponding to the reduction-in-area and fracture strength in solution and in air, respectively [15]. The fracture morphologies of the cross-side and surfaces of tensile specimens after the SSRT test were observed by scanning electron microscopy (SEM).

Electrochemical experiments were performed with PARSTAT 2273, using a conventional three-electrode cell system, in which a saturated calomel electrode (SCE) was used as the reference electrode and a platinum sheet as the counter electrode. All the potentials quoted in this work were referred to SCE. Prior to the test, all the electrodes were immersed in solutions until the open circuit potential (OCP) was stable. Potentiodynamic polarization curves were acquired by scanning from  $-1.5$  to 1.5 V vs. SCE at a slow sweep rate of 1 mV/s and a quick sweep rate of 100

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mV/s. EIS measurements were carried out at passive potential (if any) of  $-0.2$  V vs. SCE, with the AC amplitude of the sinusoidal perturbation of 10 mV vs. SCE and the measurement frequency from 100 kHz to 10 mHz.

# **3. Results**

#### **3.1. SSRT results**

The stress-strain curves of X80 pipeline steel in the solutions with different concentrations of HCO*<sup>−</sup>* <sup>3</sup> at –0.2 V vs. SCE were shown in Fig. 1. Compared with the curve obtained in air, X80 steel in bicarbonate solutions displayed susceptibility to SCC. With the increase of HCO<sub>3</sub><sup>-</sup> concentration, the susceptibility enhanced with the reduction in toughness and strength, which was manifested with the elevated values of  $I_{\psi}$  and  $I_{\sigma}$  in Fig. 2. Among these results, it was noticed that when the concentration of HCO*<sup>−</sup>* <sup>3</sup> was relatively low (0.05 mol/L), X80 steel showed lower  $I_{\psi}$  and  $I_{\sigma}$ , and the fracture elongation of the specimen was almost as the same as that in air (Fig. 1), which indicated that the



**Fig. 1. Stress-strain curves of X80 steel in air and in the solutions with different concentrations of HCO***−* **<sup>3</sup> at –0.2 V vs. SCE.**



**Fig. 2. Effect of HCO***−* **<sup>3</sup> concentration on susceptibility to SCC reflected by reduction-in-area loss and fracture strength loss.**

steel appeared little susceptibility to SCC in such a dilute bicarbonate solution. These results were further confirmed by the observation of fracture morphologies below.

#### **3.2. Fractographic observation**

In the solution containing 0.05 mol/L HCO*<sup>−</sup>* <sup>3</sup> , the steel showed little susceptibility to SCC. A densely distributed dimple feature can be found on the fracture surface  $(Fig. 3(a))$ , and there were no visible secondary cracks on the lateral surface. Moreover, the fracture surface and lateral surface were both corroded seriously due to the combined effect of a lower amount of HCO*<sup>−</sup>* <sup>3</sup> and a moderate amount of Cl*−*. Considerable large and shallow pits were found on the specimen surface, and some of them were in nested type, i.e., newly formed pits evolved at the bottom of old pits (Fig. 3(b)).

When the concentration of HCO*<sup>−</sup>* <sup>3</sup> increased to 0.15 mol/L, the fractograph exhibited quasi-cleavage morphology with reduced dimples  $(Fig. 3(c))$ , and the pits were enlarged to coalesce with the adjacent ones on the lateral surface (Fig. 3(d)). With a further increase in HCO<sub>3</sub><sup>-</sup> concentration, dimples continually faded and cleavage planes became more and more remarkable, showing gradually lifted brittleness (Figs. 3(e) and  $(g)$ ). The formation of cleavage planes might be attributed to the rapid propagation of cracks along the slip steps until the specimen fractured. Meanwhile, the already coalesced pits grew even larger. Secondary cracks initiated at the bottom of these pits, and propagated until they were linked with the cracks emerged in the adjacent pits  $(Figs. 3(f)$  and  $(h)$ ), showing a more enhanced susceptibility to SCC. Therefore, pitting probably played an important role in cracking of the steel in concentrated bicarbonate solutions.

## **4. Discussion**

### **4.1. SCC mechanism of X80 steel**

Potentiodynamic polarization curves measured at 1 and 100 mV/s are shown in Fig. 4. Parkins [16] pointed out that potentiodynamic polarization curves at different potential sweep rates could be used to evaluate the susceptibility to SCC of pipeline steel in some certain electrolyte environment. Scanning at a quick sweep rate would extremely eliminate the influence of the formation of passive films, guaranteeing a barely fresh metal surface exposed to the electrolyte, where intensive anodic dissolution took place, so it could reflect the electrochemical characteristic of crack tips. At the slow sweep rate for polarization, the metal surface could be sufficiently passivated, which manifested the electrochemical characteristic of non-crack tip areas.

Assuming that the SCC behavior was controlled by the anodic dissolution mechanism, it should depend on the discrepancy between corrosion rates of crack tips and noncrack tips as well as the propagation rate of crack tips [17].

The former could be represented by  $i_q/i_s - 1$ , and the latter could be assessed by  $i_q$ .  $i_q$  and  $i_s$  referred to the current densities at –0.2 V vs. SCE obtained from the polarization curves at quick and slow sweep rates, respectively. Thus,  $i_q \cdot (i_q/i_s - 1)$  was used to estimate the susceptibility to SCC of X80 steel in different bicarbonate solutions. The calculated results of  $i_q \cdot (i_q/i_s - 1)$  are shown in Fig. 5. The curve of  $i_q \cdot (i_q/i_s - 1)$  varied with a same tendency as those of  $I_{\psi}$  and  $I_{\sigma}$ . This indicated that the higher concentration of HCO*<sup>−</sup>* <sup>3</sup> the solution contained, the higher susceptibility to SCC the steel would show. It should be noticed that the value of  $i_q \cdot (i_q/i_s - 1)$  obtained in the solution containing 0.05 mol/L HCO<sub>3</sub> was negative, i.e.,  $i_s > i_q$ . Theoretically, cracking could not be initiated when the dissolution rate of non-crack tip areas was greater than that of crack tips [18]. Thus, it provided an explanation from the electrochemical kinetics aspect for the phenomenon that X80 steel exposed to dilute bicarbonate solution represented little susceptibility to SCC.

In order to estimate the reasonableness of  $i_q \cdot (i_q/i_s-$ 1), the criterion of susceptibility to SCC based on electrochemical measurements [15] was introduced, which had the following form:

$$
I_{\text{SCC}} = k_{\text{a}} \cdot i_{\text{q}} \cdot \left(\frac{i_{\text{q}}}{i_{\text{s}}} - 1\right) + I_{\text{a}},\tag{3}
$$

where  $k_a$  and  $I_a$  were constants in relation to the material/electrolyte system. By applying the results of  $I_{\psi}$  and  $I_{\sigma}$ , the values of  $k_{\rm a}$  and  $I_{\rm a}$  were estimated and the formulations used for solutions containing 0.15-1.00 mol/L HCO*<sup>−</sup>* 3 are given as follows:

$$
I_{\text{SCC}} = \begin{cases} 1.56 \cdot i_{\mathbf{q}} \cdot \left(\frac{i_{\mathbf{q}}}{i_{\mathbf{s}}} - 1\right) + 6.8\%, & \text{for } I_{\psi} \\ 0.044 \cdot i_{\mathbf{q}} \cdot \left(\frac{i_{\mathbf{q}}}{i_{\mathbf{s}}} - 1\right) + 11.9\%, & \text{for } I_{\sigma} \end{cases}
$$
(4)

The results had a good agreement with the measured results as shown in Fig. 6. It indicated that it was reasonable to use  $i_q \cdot (i_q/i_s - 1)$  to evaluate the susceptibility to SCC of X80 steel at passive potential in relatively concentrated bicarbonate solutions. It also proved that the SCC behavior was controlled by the dissolution-based mechanism in these circumstances.

Thus, the cracking procedure of X80 steel in bicarbonate solutions can be expressed by Figs.  $7(a)-(d)$ . First, applied stress promoted the dislocation emission. With the accumulation of dislocations, slip bands  $1$  and  $2$  in Fig.  $7(a)$ set in motion successively and the dislocation slip steps became more and more obvious, which led to the rupture of passive films. Dislocations were then pushed toward the slip steps and piled up there  $(Fig. 7(b))$ . When these local sites were directly exposed to the aggressive electrolytes, pitting was initiated by selective dissolution of these sites because of the relatively higher electrochemical activity



**Fig. 3. Morphologies of fracture surfaces and lateral surfaces in the solutions with different concentrations of HCO***−* **<sup>3</sup> : (a) fracture surface and (b) lateral surface in 0.05 mol/L bicarbonate solution; (c) fracture surface and** (d) lateral surface in  $0.15 \text{ mol/L}$  bicarbonate solution; (e) fracture surface and (f) lateral surface in  $0.50 \text{ mol/L}$ **bicarbonate solution; and (g) fracture surface and (h) lateral surface in 1.00 mol/L bicarbonate solution.**



**Fig. 4. Polarization curves of X80 steel in the solutions with different concentrations of HCO***−* **<sup>3</sup> measured at sweep rates of 1 mV/s (a) and 100 mV/s (b).**



**Fig. 5.** Relationship between  $i_q \cdot (i_q/i_s - 1)$  and  $HCO_3^$ **concentration.**



**Fig. 6. Comparison between measured and calculated**  $I_{\psi}$  and  $I_{\sigma}$  using Eq. (4).



**Fig. 7. Schematic diagrams showing the SCC process of X80 steel exposed to solutions containing Cl***−* **and different concentrations of HCO***−* **<sup>3</sup> : (a) the steel with passive films in original state; (b) film rupture combined with the formation of slip steps and dislocation pileups; (c) initiation of pitting; (d) generation of defect points in passive films and cracking along cleavage planes in concentrated bicarbonate solutions; (e) development of pitting in dilute bicarbonate solution.**

and lattice distortion [19]. Dislocation pileups further advanced to the bottom of these pits under the stress triaxiality (Fig. 7(c)), and the atoms at these stress concentrated points would be dissolved preferentially to form microcracks. Finally, HCO*<sup>−</sup>* <sup>3</sup> promoted the dissolution of crack tips and the propagation of cracks along cleavage planes (Fig. 7(d)). Therefore, cleavage cracks were inclined to initiate in pits formed along the dislocation slip steps as shown in Figs.  $3(f)$  and  $(h)$ .

# **4.2. Effect of HCO***−* **<sup>3</sup> on the rupture of passive films and SCC behavior**

In high pH solutions, the properties of passive films formed on the steel surface is essential to the occurrence of SCC based on the anodic dissolution mechanism [20]. Nyquist plots in Fig. 8 show that the capacitance arc corresponding to the electric double layer at high frequency decreased rapidly with the increase of HCO*<sup>−</sup>* <sup>3</sup> concentration, and the one referred to the passive films at low frequency shrank into diffusion impedance. Fig. 9 shows the equivalent electric circuit, where  $R<sub>s</sub>$  is the resistance of the electrolyte,  $C_{d1}$  and  $R_{ct}$  correspond to the electric double layer capacitance and charge transfer resistance, respectively, and  $W$  is the Warburg impedance. By using the equivalent electric circuit in Fig. 9, the fitting values of  $R_{\rm ct}$ are shown in Fig. 10.  $R_{\rm ct}$  decreased with an increase in HCO*<sup>−</sup>* <sup>3</sup> concentration, indicating that the inhibiting effect of passive films on the diffusion of aggressive electrolytes was deteriorated by excessive HCO*<sup>−</sup>* 3 .

Davies and Burstein [21] pointed out that HCO*<sup>−</sup>* 3 could accelerate the dissolution of the steels whether in



**Fig. 8. EIS plots of X80 steel in the solutions with different concentrations of HCO***−* **<sup>3</sup> at –0.2 V vs. SCE.**



**Fig. 9. Equivalent electric circuit.**



**Fig. 10.** Relationship between  $R_{\rm ct}$  and  $\rm{HCO}_{3}^-$  concen**tration.**

the active or in passive potential region due to the formation of soluble composite ion  $\text{Fe}(\text{CO}_3)_2^{2-}$ :

$$
FeCO_3 + HCO_3^- \to Fe(CO_3)_2^{2-} + H^+. \tag{5}
$$

The initially formed passive films were dissolved by excessive  $\text{HCO}_3^-$  in accordance with Eq. (5). As a result, the transformation of the passive films from  $FeCO<sub>3</sub>$  to more stable phase  $Fe<sub>3</sub>O<sub>4</sub>$  and  $Fe<sub>2</sub>O<sub>3</sub>$  at  $-0.2$  V vs. SCE was suppressed. Subsequently, pores and other type of defects in the passive films increased [22]. These defects made the absorption points and penetration path formed for the aggressive ions (Cl*<sup>−</sup>* and HCO*<sup>−</sup>* <sup>3</sup> ), which facilitated the rupture of passive films, as well as the occurrence of pitting and cracking at these locations [23] as shown in Fig. 7(d). Moreover, the increase of HCO*<sup>−</sup>* <sup>3</sup> concentration could promote the anodic dissolution of crack tips [12], which is represented with the rapid increase of  $i_q \cdot (i_q/i_s - 1)$  as shown in Fig. 5. That is why higher concentrations of HCO*<sup>−</sup>* <sup>3</sup> contributed to a higher susceptibility to SCC of X80 steel.

However, X80 steel showed little susceptibility to SCC in dilute bicarbonate solution (0.05 mol/L HCO*<sup>−</sup>* <sup>3</sup> ). The initiation of SCC can be seen as a competition procedure between the rupture and the repassivation of passive films, in which only moderate repassivation rate is beneficial to cracking [24]. In this work, the steel could not be passivated in this dilute solution as shown in Fig. 4(a), and the value of  $i_q \cdot (i_q/i_s - 1)$  was below zero (Fig. 5), i.e.,  $i_s$ was greater than  $i_q$  at  $-0.2$  V vs. SCE, so the formation of passive films at crack tips and in non-crack tip areas were both inhibited, and the non-crack tip areas experienced relatively more intensive dissolution than the crack tips. It can be concluded that the repassivation of passive films significantly fell behind the rupture in this circumstance. Therefore, microcracks, once emerged, would not propagate but instantly go blunt and transform into pits because of intensive dissolution at the sidewalls of the cracks. After that, new microcracks initiated and developed into new pits at the bottom of the original pits. Consequently, only the development of pitting was observed as shown in Fig. 3(b). The schematic diagram related to this process is shown in Fig. 7(e). Therefore, the tendency to SCC caused by the dissolution-based mechanism was negligible in dilute bicarbonate solution.

## **5. Conclusions**

(1) It is proven that the SCC behavior of X80 steel at –0.2 V vs. SCE in concentrated bicarbonate solutions containing 0.15-1.00 mol/L HCO*<sup>−</sup>* <sup>3</sup> is controlled by the dissolution-based mechanism, and the susceptibility to SCC can be evaluated by using  $i_q \cdot (i_q/i_s - 1)$ . The increase in HCO*<sup>−</sup>* <sup>3</sup> concentration results in the enhanced susceptibility to SCC. Cleavage cracks are inclined to initiate in pits formed along the dislocation slip steps.

(2) The rupture of passive films is promoted by excessive HCO*<sup>−</sup>* <sup>3</sup> , which also facilitates the occurrence of pitting and cracking. Increasing the HCO*<sup>−</sup>* <sup>3</sup> concentration not only increases the number of defects in passive films due to the formation of the soluble composite ion  $\text{Fe(CO}_3)_2^{2-}$  but also promotes the anodic dissolution of crack tips.

(3) X80 steel only shows the development of pitting at –0.2 V vs. SCE in dilute bicarbonate solution with 0.05 mol/L HCO<sub>3</sub><sup>2</sup>, and the tendency to SCC caused by anodic dissolution can be negligible. This should be attributed to the inhibited repassivation process, manifesting as the more intensive dissolution in the non-crack tip areas than at the crack tips.

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