

Magnetic separation of metal sulfides/oxides by $Fe₃O₄$ at room temperature and atmospheric pressure

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Abstract The recovery of heterogeneous catalysts can save costs and avoid secondary pollution, but its separation efficiency and recovery cost are limited by conventional separation methods such as precipitation–flocculation, centrifugation and filtration. In this paper, we found that surface-defective metal sulfides/oxides $(WS_2, CuS, ZnS,$ $MoS₂, CdS, TiO₂, MoO₂ and ZnO) commonly used in$ advanced oxidation processes (AOPs) could be magnetically recovered at room temperature and atmospheric pressure by mechanically mixing with $Fe₃O₄$. Zeta potential, Raman, X-ray photoelectron spectroscopy (XPS) and electro-spin resonance (ESR) spectra were measured to explore the mechanism of the magnetic separation phenomenon. The exposed active metal sites on the surface of defective metal sulfides/oxides are beneficial for the formation of chemical bonds, which are combined with electrostatic force to be responsible for the magnetic separation. Moreover, other factors affecting the magnetic separation were also investigated, such as the addition of amount of $Fe₃O₄$, different solvents and particle sizes. Finally, WS_2 was chosen to be applied as a co-catalyst in Fenton reaction, which could be well separated by the magnetic $Fe₃O₄$ to achieve the recycle of catalyst in Fenton reaction. Our research provides a general strategy for the

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M.-Y. Xing e-mail: mingyangxing@ecust.edu.cn recycle of metal sulfides/oxides in the catalytic applications.

Keywords Magnetic separation; Metal sulfides/oxides; Recycle; Fenton reaction

1 Introduction

During the past few decades, catalysts have played an increasingly irreplaceable role in industrial production. They can reduce the activation energy, accelerate the reaction rate or increase the selectivity of chemical reactions [\[1–3](#page-9-0)]. However, the practical application of homogeneous catalysts in liquid-phase reaction is restricted by high costs, difficulties in separation and recovery and formation of metal-complexing [\[4](#page-9-0)]. To overcome these shortcomings of homogeneous catalysts, different methods have been proposed, such as nanofiltration and new separation techniques based on liquid–liquid separation, including ionic liquids, fluorine phases, supercritical solvents and polymeric supports; however, some problems have arisen, which lead to the limitations of costs, efficiency and secondary pollution [[5\]](#page-9-0). Therefore, heterogeneous catalysis is occupying a more important position gradually for the effective and environmentally friendly reactions. Different types of heterogeneous catalysts have been applied in many fields, such as the production of fine chemicals and pharmaceuticals, chemical technology and advanced oxidation processes (AOPs) [\[6–11](#page-9-0)]. Heterogeneous catalysts with relatively recyclable nature will save the cost, reduce the waste and make the reaction environmentally friendly, which is consistent with the strategy of sustainable development.

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As a robust, efficient and rapid tool to separate heterogeneous catalysts, magnetic separation has many advantages compared to those approaches like precipitation– flocculation, filtration or centrifugation. Actually, magnetic separation technology has been widely used in the mining and food processing industries for decades, via using eddy currents, electromagnets and permanent magnets to separate magnetic materials from non-magnetic materials on a wet or dry basis [\[12](#page-9-0)]. As an inherent part of many material handling operations, magnetic technology has undergone tremendous development over the past decades [\[13](#page-9-0)]. Generally, the selection of separation processes is determined by the chemical and physical properties of materials, as well as the time and energy expended. Although traditional separation methods such as centrifugal separation or filtration have been widely used, it may be the best choice for the materials with intrinsic magnetism to be separated by an applied magnetic field, which is of easy operation and convenient [\[14](#page-9-0)[–18](#page-10-0)].

Magnetite ($Fe₃O₄$) is a ferrimagnetic mineral with a spinel structure containing ferric and ferrous ions occupying octahedral and tetrahedral coordination sites, respectively, whose oxygen atoms are arranged into cubes to enclose the lattice. The ferrimagnetic property of magnetite is determined by the spin arrangement in ferrous ions antiparallel to that in ferric ions, and the interactions of iron ions in different coordination sites lead to incomplete cancelation of spin moments and a strong magnetization [\[19](#page-10-0)]. Definitely, there are plenty types of magnetic materials, such as maghemite (γ -Fe₂O₃) and other ferrites $(MFe₂O₄, M = Co, Mn, etc.)$ [\[20](#page-10-0)], but the magnetism of them is much lower than that of magnetite. In addition, other magnetic metals, pure zero-valent iron (ZVI) nanoparticles, are always easy to be oxidized [[21,](#page-10-0) [22](#page-10-0)]. Thereby, magnetite is the best choice to participate in magnetic separation as a support, co-catalyst or catalyst in catalytic applications.

The magnetic separation technology is applied in many fields, with the main purpose of separating non-magnetic and magnetic materials. In detail, non-magnetic materials do not interact with target magnetic materials and thus remain in the solution after magnetic materials get separated by an applied magnetic field [\[23](#page-10-0), [24](#page-10-0)]. At present, only those heterogeneous catalysts who have magnetism can be recycled by an external magnetic field, so many magnetic heterogeneous catalysts have been prepared for magnetic recycled purpose. Hajian et al. [\[25](#page-10-0)] prepared Fe3O4@MCM-41-Im@MnPor catalyst with tetraphenylporphyrinatomanganese(III) chloride immobilized onto imidazole functionalized MCM-41 and magnetic nanoparticle core. The prepared catalyst can be easily recovered through the application of an external magnet. The separation of the as-prepared heterogeneous catalyst was achieved by simple magnetic decantation without obvious mass loss, so that it could be reused for the next catalysis application. Ma et al. [[26\]](#page-10-0) fabricated series of magnetic $Fe₃O₄/TiO₂$ composites through simple sol-gel strategy. $Fe₃O₄/TiO₂$ composites exhibited excellent magnetic recycle property because the surface of magnetic $Fe₃O₄$ was coated with spherical $TiO₂$ nanoparticles. However, the preparation of magnetic materials is complex, and there will be other pollution produced during the preparation, increasing the cost and time.

Here, we found that some commercial metal sulfides/ oxides exposed with surface defects and commonly used in AOPs could be magnetic separated with $Fe₃O₄$ with an applied magnetic field. We systematically summarized the recoverable degrees of these metal sulfides/oxides with $Fe₃O₄$ added in the solution, and the mechanism of magnetic separation was explored through zeta potential, Raman, X-ray photoelectron spectroscopy (XPS) analysis and electro-spin resonance (ESR) spectra. The interactions between metal sulfides/oxides and $Fe₃O₄$, such as the electrostatic force or chemical bonds, were considered to be the dominating causes when they were mixed mechanically and separated with an external magnetic field. This method is considered to be more convenient, simple and lower cost than centrifugation, filtration and preparation of magnetic materials. Therefore, magnetic separation has great potential application in the field of heterogeneous catalysts recovery, even some of which are non-magnetic. For instance, this method was successfully applied to WS_2 -Fenton reaction to recycle WS_2 after the reaction.

2 Experimental

2.1 Chemicals and reagents

All the chemicals, including tungsten (IV) sulfide (Alfa Aesar (China) Chemical Co., Ltd., 99.8%), cupric sulfide (Shanghai Macklin Biochemical Co., Ltd., analytical reagent (AR), 99.0%), zinc sulfide (Shanghai Aladdin Bio-Chem Technology Co., Ltd., 99.99%, 3.3–4.3 μm), molybdenum (IV) sulfide (Alfa Aesar (China) Chemical Co., Ltd., 99%; Shanghai Aladdin Bio-Chem Technology Co., Ltd., 99.5%, $\lt 2 \mu m$), cadmium sulfide (Shanghai Macklin Biochemical Co., Ltd., AR, 98%), titanium (IV) oxide (Shanghai Aladdin Bio-Chem Technology Co., Ltd., 99.8%, anatase), molybdenum (IV) oxide (Shanghai Energy Chemical Co., Ltd., 99%), zinc oxide (Shanghai Lingfeng Chemical Reagent Co., Ltd., $> 99\%$), triiron tetraoxide (Beijing HWRK Chem Co., Ltd., 1 µm, 99.9%), sodium hydroxide (Shanghai Titan Scientific Co. Ltd., AR, \geq 96.0%), sulfuric acid (Shanghai Titan Scientific Co. Ltd., CP, 95.0%–98.0%), ferrous sulfate heptahydrate

(Shanghai Aladdin Bio-Chem Technology Co., Ltd., 99.95%), hydrogen peroxide (Shanghai Experiment Reagent Co., Ltd., 30%), cyclohexane (Shanghai Titan Scientific Co. Ltd., AR, \geq 99.5%), 2-propanol (Shanghai Titan Scientific Co. Ltd., $AR \geq 99.7\%$), ethanol (Shanghai Titan Scientific Co. Ltd., $AR \geq 99.7\%$), were used without further purification. Deionized water (DI-water) was produced by OKP-S040 Standard ultrapure water system and applied in all the following experiments.

2.2 Experimental procedures

The magnetic separation experiments were performed in glass vials, the quality of which were weighed and recorded in advance. The fixed amount of the metal sulfide/oxide and $Fe₃O₄$ were mixed into 10 ml solvent while only the metal sulfide/oxide was added as a control experiment. The solution pH was adjusted and recorded. Subsequently, a magnet was placed on the side of glass vials for the magnetic separation test, and the magnetic separation time was taken down. A few seconds later, with the magnet attracting, the solvent and the part that could not be magnetic separated were emptied, and the residues were washed by the solvent once and then dried for 48 h in a vacuum drying chamber. Finally, the total masses of glass vials were weighed so that the mass of the metal sulfide/ oxide separated by the magnetic field could be calculated.

The degradation experiments were performed in plastic cups with a magnetic stirring to keep the solution homogeneous during the reaction. The predesigned initial pH of RhB solution was adjusted to 4.0 first with sodium hydroxide and sulfuric acid, which was considered to be the best pH in Fenton reaction. Then, the fixed amount of WS_2 and $FeSO_4 \cdot 7H_2O$ were added into 100 ml reaction solution with desired concentration of RhB. Finally, quantitative H_2O_2 was added to initiate the oxidation. Samples were taken out at regular intervals, centrifuged and analyzed immediately. After the reaction, $Fe₃O₄$ was added into the solution. Then, $Fe₃O₄$ and $WS₂$ were magnetic separated by an external magnetic field.

2.3 Analytic methods

The pH values of the solution were detected with a pH meter (INESA PHS-3C). Raman spectra of metal sulfides/ oxides were measured by using a Renishaw inVia spectrometer using Ar^+ laser of 532 nm at room temperature. The XPS of metal sulfides/oxides was conducted at a condition of Al Ka irradiation by THERMO ESCALAB 250 Xi. Zeta potentials of metal sulfides/oxides and size distributions of $MoS₂$ from different manufacturers were investigated by a Zetasizer (Malvern, ZEN3600). ESR spectrometer (Bruker, 100G-18 KG/EMX-8/2.7) was used to detect the types of defects in metal sulfides/oxides at room temperature. The concentration of RhB was measured with a ultraviolet–visible (UV–Vis) spectrophotometer (SHIMADZU UV-2450).

3 Results and discussion

3.1 Magnetic separation of different metal sulfides/ oxides with $Fe₃O₄$ in aqueous solution

All the metal sulfides/oxides (WS_2 , CuS, ZnS, MoS₂, CdS, $TiO₂$, MoO₂ and ZnO) used in the experiments are nonmagnetic. As shown in Fig. [1,](#page-3-0) no magnetic separation of any metal sulfide/oxide was observed without $Fe₃O₄$ added in aqueous solution. However, when $Fe₃O₄$ was added, the metal sulfides/oxides were separated to different degrees quickly. For instance, with $Fe₃O₄$ present, $WS₂$, CdS and CuS were magnetically separated thoroughly, making the aqueous solution clarified; $MoS₂$ (Alfa), $MoO₂$ and ZnO seemed partial separation with some residues left; ZnS, $TiO₂$ and $MoS₂$ (Aladdin) had poor magnetic separation, resulting in turbid solutions that show no significant change compared to the solutions before magnetic separation.

Furthermore, detailed magnetic recovery rates of different metal sulfates/oxides are shown in Fig. [2a](#page-4-0), which were consistent with the experimental phenomena in Fig. [1.](#page-3-0) Among all metal sulfides/oxides, WS_2 reached the highest magnetic recovery rate (99.0%), while CuS and CdS also performed relatively good magnetic recovery rates of 87.5% and 90.5%, respectively. The recycling rates of other metal sulfides/oxides became decreasing. Specifically, the recovery rates of $MoS₂ (Alfa)$, $Moo₂$ and ZnO were 85.2%, 79.6% and 80.1%, respectively, while ZnS, $TiO₂$ and $MoS₂$ (Aladdin) only obtained the magnetic recovery rates of 69.5%, 46.8% and 43.0%, respectively. There is no doubt that $Fe₃O₄$ is magnetic and can be attracted with a magnetic field [\[27](#page-10-0), [28\]](#page-10-0), but the reason why non-magnetic metal sulfides/oxides together with $Fe₃O₄$ could also be separated by a magnetic field needs to be further investigated. Some kinds of interactions should be present between metal sulfides/ oxides and $Fe₃O₄$ after mechanical mixing so that metal sulfides/oxides would follow $Fe₃O₄$ to be separated together while an applied magnetic field was attracting. Moreover, metal sulfides/oxides weakly interacting with $Fe₃O₄$ would have a relatively poor magnetic separation degree while strong interactions between them would result in a through separation from the solution.

3.2 Role of electrostatic force in magnetic separation

In view of the above-mentioned phenomena in Fig. [2](#page-4-0), the electrostatic force between metal sulfides/oxides and $Fe₃O₄$

Fig. 1 Magnetic separations of different metal sulfides/oxides with Fe₃O₄ (left of each picture) and without Fe₃O₄ (right of each picture): a WS₂, **b** CuS, c CdS, d ZnS, e MoS₂ (Aladdin), f MoS₂ (Alfa), g TiO₂, h ZnO and i MoO₂

is the first reason worth considering, because they were just mechanically blended [\[29](#page-10-0)]. Therefore, zeta potential tests were taken to determine the charged states of different particle surfaces. Considering that WS_2 had the best magnetic separation rate and $TiO₂$ had comparatively low magnetic separation rate, they were chosen to participate in zeta potential tests. The main purpose was to explore the isoelectric points of them. As shown in Fig. [2](#page-4-0)b, the zeta potential of $Fe₃O₄$ was -34.7 mV at pH = 10.84, 6.59 mV at $pH = 5.00$ and 4.46 mV at $pH = 1.86$, respectively; the zeta potential of WS_2 was -30.3 mV at $pH = 3.23$ and $- 16.3$ mV at $pH = 1.25$, respectively; the zeta potential of TiO₂ was -22.7 mV at pH = 11.77, 0.42 mV at $pH = 9.92$ and 17.4 mV at $pH = 6.10$, respectively. Therefore, the isoelectric points of $Fe₃O₄$, $WS₂$ and $TiO₂$ could be speculated as follows: at pH between 5.00 and 10.84 for $Fe₃O₄$, lower than 1.25 for $WS₂$ and near neutral for $TiO₂$ [\[30](#page-10-0)].

As shown in Fig. [2c](#page-4-0), the pH of WS_2/Fe_3O_4 mixture was 3.24, at which the surfaces of WS_2 and $Fe₃O₄$ were charged negatively and positively, respectively, and they were magnetically separated in 3 s (Fig. [2](#page-4-0)f). When the solution pH was adjusted to 11.30, both of their surfaces became

negative. The magnetic separation time became a bit longer, but they could still be magnetically separated in 5 s (Fig. [2g](#page-4-0)), implying that there should be another kind of interaction between WS_2 and $Fe₃O₄$ for the magnetic sep-aration. As shown in Fig. [2d](#page-4-0), as for $TiO₂/Fe₃O₄$ mixture, the initial pH was 4.20, at which the surfaces of $TiO₂$ and $Fe₃O₄$ both were charged positively that may account for their poor magnetic separation rate (46.8%) (Fig. [2](#page-4-0)h). Although there was no significant variation of the magnetic separation degrees after the pH adjusted to 8.00, at which the surface of $TiO₂$ became positive but the surface of $Fe₃O₄$ remained negative, the recovery of TiO₂ had slight improvement, reaching 49.5% in Fig. [2i](#page-4-0).

Based on above experimental results, we could draw the conclusion that the electrostatic force was one of the factors affecting the magnetic separation, not only the magnetic separation time, but also the recovery rate; however, it was not the dominant force to influence non-magnetic substances magnetic separated with $Fe₃O₄$ by an applied magnetic field.

Fig. 2 a Magnetic recovery rate of different metal sulfides/oxides with Fe₃O₄; b zeta potential of Fe₃O₄, WS₂ and TiO₂ at different pH; c variation of magnetic separation time of WS₂ and Fe₃O₄ at different pH; d variation of magnetic separation rate at different pH; e Raman spectrum of Fe₃O₄; variation of magnetic separation time of WS₂ and Fe₃O₄ at pH f 3.24 and g 11.30; variation of magnetic separation time of WS_2 and $Fe₃O₄$ at pH **h** 4.20 and **i** 8.00

3.3 Formation of chemical bonds in magnetic separation

In order to explore whether chemical bonds were established or not between metal sulfides/oxides and $Fe₃O₄$ after mechanical mixing, Raman, XPS and ESR spectra were employed in this case. With the same reasons as mentioned above, WS_2 and TiO_2 were chosen for primary detailed characterizations and discussions. Figures 2e and [3](#page-5-0) show Raman spectra of magnetite and different metal sulfides/ oxides before and after mixing and magnetic separation with $Fe₃O₄$. As shown in Fig. 2e, the strongest magnetite band (A_{1g} mode) of Fe₃O₄ Raman spectrum was observed at 665 cm^{-1} . The other three magnetite phonon frequencies generated much smaller bands at 189 (T_{2g}), 346 (E_g) and 497 (T_{2g}) cm⁻¹, respectively, which were consistent with the previous report $[31]$ $[31]$. Figure [3](#page-5-0)a exhibits the Raman spectra of WS_2 with the characteristic peak at 475 cm⁻¹ [\[32](#page-10-0)], and it was worth noting that the weak contribution appearing at 669 cm^{-1} of the mixture was referred to the

 A_{1g} mode of Fe₃O₄ that was not observed on the Raman spectrum of the pure WS_2 . Moreover, the A_{1g} mode of Fe₃O₄ was blueshifted by 4 cm⁻¹ compared to that of the pure $Fe₃O₄$, proving that the electron clouds on the surface of $Fe₃O₄$ transferred to $WS₂$, building the connection between $Fe₃O₄$ and $WS₂$. The Raman spectra of pure anatase and anatase/Fe₃O₄ mixture are shown in Fig. [3b](#page-5-0). The black line represents the five characteristic peaks corresponding to the Raman modes of TiO₂: E_g (144 cm^{-1}) , E_g (198 cm^{-1}) , B_{1g} (396 cm^{-1}) , B_{1g}/A_{1g} (518 cm^{-1}) and E_{g} (638 cm⁻¹), respectively [[33\]](#page-10-0) (A_{1g} and B_{1g} are the brookite Raman peaks). Both the frequencies of B_{1g} mode and A_{1g} mode were close to 518 cm⁻¹. After the mechanical mixing and magnetic separation with $Fe₃O₄$, all the peaks of $TiO₂$ became wider because the Raman peak positions of TiO₂ and Fe₃O₄ were close. Moreover, the E_g mode and A_{1g} mode of Fe₃O₄ were observed. The results evidenced that $TiO₂$ could also be magnetically separated, but the inferior separation was still confused. As for other metal sulfides/oxides (Fig. [3](#page-5-0)c–i), the A_{1g} modes of Fe₃O₄

Fig. 3 Raman spectra of a WS₂, b TiO₂, c CdS, d CuS, e ZnS, f MoS₂ (Aladdin), g MoS₂ (Alfa), h ZnO, i MoO₂ before and after mixing and separated with $Fe₃O₄$

were also observed in their Raman spectra, which varied in strength and position. For instance, the A_{1g} modes in CuS and CdS Raman spectra both occurred at 663 cm⁻¹ (Fig. 3c, d), with 2 cm⁻¹ lower than that of pure Fe₃O₄, implying that the electron clouds transferred from CuS and CdS to $Fe₃O₄$.

XPS measurements were performed to further study the composition and surface chemical environment of metal sulfides/oxides. Figure [4](#page-6-0)a, d, g shows the survey XPS spectra of WS_2 , CuS and TiO₂, respectively, before and after the mechanical mixing and magnetic separation with Fe₃O₄. W 4f and S 2p core levels of WS_2 are exhibited in Fig. [4](#page-6-0)b, c, respectively. The W 4f core level spectrum contained a doublet located at 33.3 and 35.5 eV, corresponding to W (IV) $4f_{7/2}$ and W (IV) $4f_{5/2}$, respectively. The peaks at 36.3 and 38.9 eV were specified as W (VI) $4f_{7/2}$ and W (VI) $4f_{5/2}$, respectively. The core level spectrum of S 2p had two peaks at 163.0 and 164.2 eV, assigned to the doublet of S $2p_{3/2}$ and S $2p_{1/2}$ states, respectively. The oxidation of surface sulfur atoms may account for the peak appeared at 169.8 eV [[34–36\]](#page-10-0). After the mechanical mixing and magnetic separation with Fe3O4, all the peaks of W 4f and S 2p were shifted to lower binding energy, declining by 0.3–0.5 eV, respectively, proving that the density of the electron clouds around tungsten atoms and sulfur atoms increased so that their ability to bind with electrons decreased. Furthermore, the peak area ratio of W(IV)/W(VI) increased, further verifying the results obtained from Raman spectra of WS_2 : the formation of W(IV)-O-Fe between $Fe₃O₄$ and WS₂ was established, leading to the transformation of electrons from $Fe₃O₄$ to WS₂. Figure [4e](#page-6-0) shows the high-resolution XPS spectra of Cu 2p peak of CuS. The peaks at 932.0 and 951.9 eV were assigned to Cu $2p_{3/2}$ and Cu $2p_{1/2}$ of Cu–S bond, while the peaks located at 934.6 and 954.3 eV were attributed to Cu $2p_{3/2}$ and Cu $2p_{1/2}$ of Cu–O bond, suggesting the surface oxidation of CuS. The other two peaks at 943.4 and 963.0 eV were the satellite peaks. Figure [4f](#page-6-0) shows the high-resolution XPS spectra of S 2p for CuS, which could be fitted to three types of S. The two peaks at 162.1 and 163.1 eV were assigned to S–S bond of S $2p_{3/2}$ and S $2p_{1/2}$, respectively, and the sulfide of Cu–S may

Fig. 4 XPS spectra of WS₂: a survey spectrum, high-resolution spectra of b W 4f and c S 2p; XPS spectra of CuS: d survey spectrum, highresolution spectra of **e** Cu 2p and **f** S 2p; XPS spectra of TiO₂: **g** survey spectrum, high-resolution spectra of **h** Ti 2p and **i** O 1s

account for the peak at 161.0 eV, and the peaks at 168.9 and 170.1 eV were all attributed to the oxidized sulfur species of SO_r [\[37–39](#page-10-0)]. After the mechanical mingling and magnetic separation with $Fe₃O₄$, all the peaks of Cu 2p and S 2p had slight but diverse changes. The Cu–S and S–S bonds, including Cu $2p_{3/2}$, Cu $2p_{1/2}$, S $2p_{3/2}$ and S $2p_{1/2}$, shifted to high binding energy, increasing by 0.1–0.2 eV; however, the oxidation peaks of CuS XPS spectrum became lower, declining by 0.2–0.5 eV. This phenomenon proved that the $Cu(II)-O-Fe$ bond was formed and electrons transferred from Cu–S bonds to $Fe₃O₄$, corresponding to the Raman result. Figure 4h, i shows the high-resolution XPS spectra of Ti 2p and O 1s. The two peaks of Ti 2p at 458.6 and 464.4 eV were ascribed to Ti $2p_{3/2}$ and Ti $2p_{1/2}$, respectively. Besides, the O 1s peaks could be fitted into three peaks and the binding energy at 529.9, 531.4 and 532.4 eV were referred as the lattice oxygen (Ti–O), the chemisorbed surface oxygen (Ti–O) and hydroxyl (–OH),

respectively [[40\]](#page-10-0). After the mechanical mixing and magnetic separation with $Fe₃O₄$, all the peaks of Ti 2p and O 1s were shifted to higher binding energy, increasing by 0.1–0.2 eV. Considering that the magnetic separation of TiO₂ with Fe₃O₄ was poor, partial TiO₂ still gets magnetically separated successfully, which was not surprising. The electrons transferred from TiO₂ to Fe₃O₄, opposite to that of WS_2 , which may be difficult to bond toughly to $Fe₃O₄$.

It is possible that the simple mechanical mixing will generate chemical bonds, for which defects on the surface of the metal sulfides/oxides may account. Theoretically, as for metal sulfides, the presence of sulfur vacancy makes it easy for oxygen atoms to fill in so that the connection between metal sulfides/oxides and $Fe₃O₄$ is established. Figure [5](#page-7-0) shows the ESR spectra of WS_2 , CuS, TiO₂, MoS₂ (Alfa) and $MoS₂$ (Aladdin), which were measured at room temperature. The results showed that WS_2 , MoS_2 (Aladdin)

Fig. 5 Room temperature ESR spectra of a WS₂, b CuS, c MoS₂ (Aladdin), d MoS₂ (Alfa) and e TiO₂

and $MoS₂$ (Alfa) possessed a resonance signal at around $g = 2.000$ (where g is used to indicate the internal magnetic field generated by the orbital motion of unpaired electrons in the molecule.), specifically, 2.001 (Fig. 5a), 2.004 (Fig. 5c) and 2.000 (Fig. 5d), respectively. Based on recent researches, this signal was the symbol of sulfur vacancy [\[41](#page-10-0), [42](#page-10-0)]. CuS had a similar signal appearing at 2.120 (Fig. 5b), considered that the sulfur vacancy was also existed in CuS $[43]$ $[43]$. As for TiO₂, Fig. 5e shows two main signals at $g = 1.982$ and $g = 2.004$ [[44,](#page-10-0) [45](#page-10-0)]. The weak paramagnetic signal observed at $g = 1.982$ was the characteristic peak of Ti^{3+} , while the strongest paramagnetic signal at $g = 2.004$ indicated the presence of oxygen vacancies. The existence of these defects allowed the production of chemical bonds between metal sulfides and $Fe₃O₄$ by simply mechanically mixing them in deionized water, due to the exposure of active metal sites on the surface of metal sulfides/oxides [[46\]](#page-10-0). As mentioned above, the peak area ratio of W(IV)/W(VI) increased and the W(IV)–O–Fe bond was built. This could be explained that the oxygen atoms of $Fe₃O₄$ filled in the sulfur vacancy as electron donors [\[46](#page-10-0)] gave electrons to W(VI) and reduced partial W(VI) to W(IV). As for CuS, the oxygen atoms of Fe3O4 filled in the sulfur vacancy of CuS; on the one hand, the oxygen atoms were extremely electronegative, so they would attract electrons around it, increasing the binding energy of Cu–S bonds; on the other hand, as electron donors, the increase in the number of Cu–O bonds reduced their binding energy, which verified the generation of Cu(II)-O-Fe bonds. Similarly, the filling of oxygen atoms from $Fe₃O₄$ in the oxygen vacancy of TiO₂ attracted the surrounding electron clouds, thus increasing the binding energy of Ti–O bonds. There must be plenty of Ti^{3+} around the oxygen vacancy and the electrons transferred from Ti^{3+} to the oxygen atoms of Fe₃O₄, resulting in the increase in the binding energy. However, the oxygen vacancy on the surface of commercial $TiO₂$ may be much less than the sulfur vacancy on the surface of metal sulfides, leading to the poor magnetic recovery rate.

3.4 Influence of other factors in magnetic separation

Owing to the typical magnetic separation characteristics, WS_2 and MoS_2 were selected to be typical materials to further explore the influence of other factors in magnetic separation. First, the mass ratio of $Fe₃O₄$ to $WS₂$ was investigated. Not surprisingly, the magnetic separation time decreased with the addition of $Fe₃O₄$ increasing. As shown in Figs. [6](#page-8-0)a–e and [7](#page-8-0)a, when the mass ratio varied from 0.5 to 2.0, the magnetic separation time decreased from 11 to 4 s. Nevertheless, only $Fe₃O₄$ was magnetic, so the increase in addition of $Fe₃O₄$ would inevitably increase the formation number of W(IV)–O–Fe bonds and therefore decrease the magnetic separation time. Moreover, WS_2 could still be separated thoroughly even with low amount of $Fe₃O₄$ due to the observation of clarified solutions (Fig. [6a](#page-8-0)–e). Secondly, the magnetic separation effect of mingling metal sulfides/oxides and $Fe₃O₄$ in organic solvents was also investigated. As shown in Fig. $6f-i$ $6f-i$, WS₂ could not be magnetically separated alone in any solvent, including deionized water, cyclohexane, alcohol and isopropanol; however, when $Fe₃O₄$ was added into the

Fig. 6 Different mass ratios of Fe₃O₄/WS₂ in deionized water: a 0.25, b 0.50, c 1.00, d 1.50 and e 2.00; magnetic separation in different solvents: f deionized water, g cyclohexane, h alcohol and i isopropanol

Fig. 7 a Variation of magnetic separation time with different mass ratios of Fe₃O₄/WS₂; b average size of MoS₂ from different manufacturers; c degradation of RhB in Fenton reaction with conditions of 0.4 mmol L^{-1} H₂O₂, 20 mg L^{-1} FeSO₄·7H₂O, 300 mg L^{-1} WS₂, pH 4.0 (C/C₀: concentration of l-RhB/initial concentration l-RhB); magnetic separation of WS₂ d before and e after adding Fe₃O₄

solution, WS_2 was successfully magnetically separated in deionized water, cyclohexane and alcohol, but failed to be recycled in isopropanol. Furthermore, it was noticed that the complete magnetic separation time of WS_2 and Fe_3O_4 was different in deionized water (3 s), cyclohexane (2 s) and alcohol (65 s). Thirdly, the particle size may be another factor affecting magnetic separation. Figure [7](#page-8-0)b shows the average sizes of $MoS₂$ bought from Aladdin and Alfa, which was 723 and 2752 nm, respectively. One of the possible reasons may be that the larger the particle size of $MoS₂$, the smaller the number of particles per unit mass, and the less the traction force provided by $Fe₃O₄$ was needed. Thus, $MoS₂$ (Alfa) could be magnetically separated better than $MoS₂$ (Aladdin) with the same mass of $Fe₃O₄$.

3.5 Application of magnetic separation in Fenton reaction

The rapid and efficient magnetic separation of metal sulfides/oxides was applied to Fenton reaction with metal sulfides/oxides as co-catalysts [\[46](#page-10-0)]. As shown in Fig. [7](#page-8-0)c, the degradation of RhB was greatly enhanced with WS_2 as a co-catalyst compared with traditional Fenton reaction, from 60.0% to 97.7% in 30 min. After reaction, the solution was turbid for the dispersion of WS_2 (Fig. [7d](#page-8-0)). Then, 5 mg Fe₃O₄ was added into the solution, and a few seconds later, the solution gradually became clear due to the magnetic separation of WS_2 with Fe₃O₄ (Fig. [7](#page-8-0)e). After the recovery of WS₂, Fenton reaction was performed again without any treatment on WS_2 , and only a slight decrease on RhB degradation rate was observed, with 89.9% RhB degraded in 30 min, which was still higher and faster than traditional Fenton reaction. This result demonstrated that magnetic separation was a feasible method to separate metal sulfides/oxides.

4 Conclusion

The low separation efficiency of metal sulfides/oxides was solved by adding $Fe₃O₄$, and the mixture could be magnetic separated with an applied magnetic field. The mechanism was explored. The electrostatic force and the formation of chemical bonds were proved as the two main reasons to explain the magnetic separation phenomenon through mechanically mixing metal sulfides/oxides and $Fe₃O₄$. Different additions of $Fe₃O₄$ and different sizes of metal sulfides/oxides would influence the magnetic separation time and rate, and the magnetic separation could be applied in some organic solvent systems. Furthermore, as a characteristic metal sulfide, WS_2 was used as a co-catalyst in Fenton reaction, which could be magnetically separated

with $Fe₃O₄$ after reaction. We believe this study will provide a new perspective for rapid and highly efficient recovery of heterogeneous catalysts in many fields.

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