

# Mesoporous resin nanobowls with optimized donor–acceptor conjugation for highly efficient photocatalytic hydrogen peroxide production

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## ABSTRACT

Design of metal-free photocatalysts with customized chemical structure and nano-architecture is promising for photocatalytic hydrogen peroxide (H<sub>2</sub>O<sub>2</sub>) production. Herein, for the first time, mesoporous resorcinol–formaldehyde (MRF) nanobowls with optimized benzenoid–quinoid donor–acceptor (D–A) couples have been synthesized via an assembly–hydrothermal–etching process as high-performance photocatalysts for H<sub>2</sub>O<sub>2</sub> production in a sacrificial agent-free system. At the hydrothermal temperature of ~ 250 °C, MRF-250 exhibits optimized structural features including a large surface area, suitable D–A couple ratio, enhanced light absorption, charge–hole separation and mass transfer. Thus, MRF-250 shows an unexpected H<sub>2</sub>O<sub>2</sub> yield of 19.4 mM·g<sup>-1</sup>·h<sup>-1</sup> in pure water, outperforming other RF samples prepared under different conditions and superior to most reported metal-free photocatalysts without the aid of sacrificial agents. Our work paves the way towards the elaborate design of highly effective metal-free photocatalysts for H<sub>2</sub>O<sub>2</sub> production.

## KEYWORDS

donor–acceptor couples, mesoporous, resin, photocatalysts, hydrogen peroxide

## 1 Introduction

Hydrogen peroxide (H<sub>2</sub>O<sub>2</sub>) is a valuable chemical with rapidly increasing demand in various important applications including organic synthesis, pulp and paper industry, environmental remediation and fuel cells [1]. The huge consumption of H<sub>2</sub>O<sub>2</sub> (predicted to be 6.0 million tons by 2024) [2] requires efficient and low-cost production technology. Currently, anthraquinone oxidation is the predominant process for H<sub>2</sub>O<sub>2</sub> synthesis, which involves multi-step organic reactions, large-scale infrastructure, high energy input and substantial waste generated [3, 4]. As one alternative route, direct synthesis from H<sub>2</sub> and O<sub>2</sub> in the presence of catalysts is more facile but exhibits a low selectivity and poor safety [5–8]. Therefore, developing efficient, economic and green routes for H<sub>2</sub>O<sub>2</sub> production is of great significance.

Photocatalytic H<sub>2</sub>O<sub>2</sub> production has emerged as a promisingly new approach, which only needs water and O<sub>2</sub> as raw materials, sustainable sunlight as energy supply and semiconductors as catalysts, without generating hazardous by-products. Great efforts have been devoted to designing promising photocatalysts, which is the key in determining the H<sub>2</sub>O<sub>2</sub> production performance. Recent studies have demonstrated that metal-free photocatalysts such as graphitic carbon nitrides [9–12], covalent triazine frameworks [13], polymer-supported carbon dots [14] and graphene oxides [15] are promising photocatalysts for H<sub>2</sub>O<sub>2</sub> production compared to inorganic metal-based photocatalysts [13]. However, metal-free photocatalysts generally

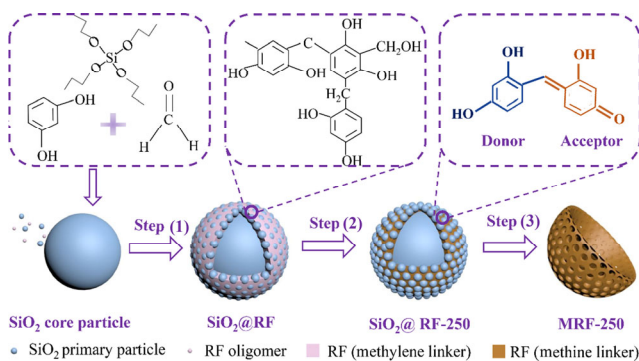
possess wide bandgaps and respond to a limited region of the solar spectrum (< 460 nm) [16–18]. Another challenge is that most of the reported metal-free photocatalysts offer relatively low activity in the absence of organic sacrificial agents (e.g., ethonal, methanol, 2-propanol) [19–21]. Therefore, developing elaborately designed photocatalysts with suitable band gap and high activity in a sacrificial agent-free (e.g., pure water) system is highly desired.

Semiconductor polymers composed of electron donor (D) and acceptor (A) units play a crucial role in photovoltaic applications due to their highly tunable highest occupied/lowest unoccupied molecular orbital (HOMO/LUMO) energy levels and band gap by using different D–A combinations with distinct charge transfer interactions [22–24]. Very recently, the superior performance of D–A coupled polymer in photocatalytic H<sub>2</sub>O<sub>2</sub> production was firstly demonstrated by Hirai and co-workers. Resorcinol–formaldehyde (RF) resins with benzenoid–quinoid D–A resorcinol couples with low-bandgaps and broad light absorption ranges (up to 700 nm) were designed, which exhibited a peak H<sub>2</sub>O<sub>2</sub> yield of 2.8 mM·g<sup>-1</sup>·h<sup>-1</sup> in a pure water system [25]. The optimized D/A ratio was demonstrated to be ~ 1, owing to the extended  $\pi$ -delocalization of D–A couple compared to single D or A. However, the solid and non-porous structure of RF resin spheres is adverse to the utilization of interior active sites, mass transfer and electron–hole pair separation during photocatalysis. Apart from the compositional design, architectural engineering towards delicate nanostructures is also highly important for enhancing photocatalytic performance, but rarely

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used in reported D–A coupled polymer photocatalysts [23]. It is expected that design of photocatalysts with highly active D–A couples (e.g., benzenoid–quinoid D–A couples) and a mesoporous structure and with large surface areas and accessible mesopores will increase the exposure of active sites, enhance charge separation and accelerate mass transfer [26], and thus the H<sub>2</sub>O<sub>2</sub> production performance will be improved.

Herein, for the first time, bowl-like mesoporous RF (MRF) nanoparticles with the D–A couple were prepared as a photocatalyst for H<sub>2</sub>O<sub>2</sub> production in water. The synthesis process of MRF materials is illustrated in Scheme 1. Using resorcinol, formaldehyde and tetrapropyl orthosilicate (TPOS) as precursors, SiO<sub>2</sub> core particles, SiO<sub>2</sub> primary particles and RF oligomers were firstly assembled [27]. The SiO<sub>2</sub> primary particles and RF oligomers co-condense onto SiO<sub>2</sub> core particles, forming SiO<sub>2</sub>@RF composite spheres in step (1). Through further hydrothermal treatment at different temperatures (*T*) such as 250 °C (the optimized temperature), benzenoid–quinoid D–A couples are generated in the RF framework, resulting in SiO<sub>2</sub>@RF-250 in step (2). Finally, MRF-250 is yielded in step (3), during which the D–A coupled structure with well retained mesoporous structure is produced after silica removal. The resultant MRF-250 exhibits a uniform nanobowl morphology with a large surface area of 101.0 m<sup>2</sup>·g<sup>-1</sup>, a mesopore size of ~ 10 nm, an optimized A/D molar ratio of 0.9:1, enhanced light absorption, charge separation and mass transfer. Combining all these merits, MRF-250 delivers an excellent photocatalytic H<sub>2</sub>O<sub>2</sub> yield of 19.4 mM·g<sup>-1</sup>·h<sup>-1</sup>, outperforming other counterparts prepared under different conditions and even superior to most reported metal-free photocatalysts.



## 2 Experimental

### 2.1 Chemicals

TPOS was purchased from Tokyo Chemical Industry UK Ltd. 30% H<sub>2</sub>O<sub>2</sub> aqueous solution, acetone and hydrofluoric acid (HF) were obtained from Sinopharm Chemical Regent Co., Ltd. Resorcinol (Adamas), formaldehyde (Adamas), ethanol (Adamas), and ammonium hydroxide (NH<sub>3</sub>·H<sub>2</sub>O) (Adamas) were used as received without further purification. Milli-Q water was used in all experiments.

### 2.2 Methods

#### 2.2.1 Synthesis of SiO<sub>2</sub>@RF precursor

The SiO<sub>2</sub>@RF composite was synthesized according to our reported work [27]. Typically, TPOS (3.5 mL) was added to the solution containing ethanol (70 mL), H<sub>2</sub>O (10 mL), and NH<sub>3</sub>·H<sub>2</sub>O (3 mL, 25 wt.%) under stirring at room temperature. After 15 min, resorcinol (0.4 g) and formaldehyde (0.56 mL,

37 wt.%) were added to the solution with reaction for 24 h, generating the SiO<sub>2</sub>@RF precursor solution for further use.

#### 2.2.2 Synthesis of RF bowls

The SiO<sub>2</sub>@RF precursor solution was transferred to a Teflon-lined stainless-steel autoclave and left in an oven for hydrothermal treatment at different temperatures for 24 h. The formed solid was washed thoroughly with acetone and dried in vacuum at room temperature for 12 h, named as SiO<sub>2</sub>@RF-*T* (*T* represents the hydrothermal temperature, *T* = 150, 200, 250, and 270 °C). After removal of silica by HF, products with different D/A ratios were fabricated (denoted as MRF-*T*). For comparison, SiO<sub>2</sub>@RF composite without hydrothermal treatment was also etched by HF, resulting in MRF. A solid RF sample was fabricated using the similar process of MRF-250, except without adding TPOS (named as SRF-250).

### 2.3 Characterization

Powder X-ray powder diffraction (XRD) patterns were recorded by using a Bruker D8 Advanced X-ray diffractometer with Cu K $\alpha$  radiation ( $\lambda$  = 0.154 nm). Fourier transform infrared spectroscopy (FTIR) spectra were recorded on a Thermal-Nicolet iS50 spectrometer. Diffuse reflectance ultraviolet–visible (UV–vis) absorption spectroscopy was performed on a UV–vis spectrophotometer (Lambda950) with BaSO<sub>4</sub> as a reference material. UV–vis spectra were obtained by using a UV–vis spectrophotometer (BioTek Synergy H1 Hybrid Multi-Mode Monochromator). Transmission electron microscopy (TEM) images were collected on a JEM-2100F (JEOL, Japan) with an acceleration voltage of 200 kV. Scanning electron microscope (SEM) images were obtained using a Zeiss Gemini 450 field emission SEM. The solid-state nuclear magnetic resonances (NMR) spectra of <sup>13</sup>C were collected on a Bruker BioSpin Avance III HD 400 high performance digital NMR spectrometer from Switzerland. Electron spin resonance (ESR) spectra were recorded on a Bruker A300 ESR spectrometer. Thermogravimetric analysis (TGA) was conducted on a Mettler-Toledo TGA/SDTA851e equipment.

### 2.4 Calculation of D/A molar ratio

The mole ratios of the quinoid and benzenoid units in the resins were calculated from the deconvoluted peak areas in <sup>13</sup>C-NMR spectrum, by using the following two equations

$$\text{Quinoid (\%)} = \frac{[\text{quinone C=O carbon (b)} \times 6 \times 100]}{[\text{all aromatic carbons (b, c, d, f, g, h)}]} \times 100 \quad (1)$$

$$\text{Benzenoid\%} = 100\% - \text{quinoid\%} \quad (2)$$

### 2.5 Photogeneration of H<sub>2</sub>O<sub>2</sub>

To measure the reductive conversion of O<sub>2</sub> into H<sub>2</sub>O<sub>2</sub>, 50 mg of photocatalyst was dispersed in 30 mL of deionized water by sonification for 5 min. After O<sub>2</sub> bubbling for 1 h, the photoreaction was initiated by irradiation of a 300 W xenon lamp ( $\lambda$  > 420 nm). At given time intervals, a certain suspension was collected and filtrated with a millipore filter (0.45  $\mu$ m) to remove the photocatalyst. The H<sub>2</sub>O<sub>2</sub> concentration was determined by iodometry [28]. Typically, 100  $\mu$ L of reaction solution was added to 2 mL mixture solution of 0.05 M potassium hydrogen phthalate (C<sub>8</sub>H<sub>5</sub>KO<sub>4</sub>) and 0.2 M potassium iodide (KI) with reaction for 30 min. Under acidic condition, the H<sub>2</sub>O<sub>2</sub> molecules would react with I<sup>-</sup> to generate I<sup>3-</sup>. The amount of I<sup>3-</sup> was measured by a UV spectrophotometer

at 350 nm, which was further used to quantify the generated  $\text{H}_2\text{O}_2$ .

### 2.5.1 Solar energy to $\text{H}_2\text{O}_2$ conversion efficiency

To determine the solar energy to  $\text{H}_2\text{O}_2$  conversion efficiency, the  $\text{H}_2\text{O}_2$  production by photocatalysis was conducted following the same procedure mentioned above except using  $5 \text{ mg}\cdot\text{mL}^{-1}$  photocatalyst and AM1.5G simulated sunlight ( $\lambda > 420 \text{ nm}$ ). The light intensity was determined with a radiometer (Perfect Light, PL-MW2000). The total input power was determined to be 0.432 W. The solar-to-chemical conversion (SCC) is calculated from the following equation

$$\text{SCC} (\%) = \frac{[\Delta G \text{ for } \text{H}_2\text{O}_2 \text{ generation (J} \cdot \text{mol}^{-1})][\text{H}_2\text{O}_2 \text{ (mol)}]}{[\text{total input power (W)}][\text{reaction time (s)}]} \times 100 \quad (3)$$

### 2.5.2 Apparent quantum yield (AQY)

The AQY was measured at selected light lengths including 365, 450, 550, and 600 nm. The total input powers were determined to be 0.123, 0.146, 0.196, and 0.225 W, respectively. AQY was calculated using the following equation

$$\text{AQY} (\%) = \frac{[\text{the number of evolved } \text{H}_2\text{O}_2 \text{ molecules} \times 2]}{\text{photon number}} \times 100 \quad (4)$$

## 2.6 Photoelectrochemical test

The photocurrent test was carried out on a Chenhua CHI 760E electrochemical workstation with a standard three-electrode cell system in 0.1 M  $\text{Na}_2\text{SO}_4$  electrolyte using Ag/AgCl electrode, Pt wire and catalyst/indium-doped tin oxide (ITO) as the reference, counter and working electrodes, respectively. The working electrode was prepared as follows: 5 mg of the sample was uniformly dispersed in 30  $\mu\text{L}$  of 10% nafion solution to produce a slurry. Then, the slurry was coated onto an ITO glass (effective area: 1  $\text{cm}^2$ ) and dried at 60  $^\circ\text{C}$  for 12 h. For transient photocurrent test, a 300 W xenon lamp (PLS-SXE300D/300 DUV, Perfect Light) equipped with a 420 nm cutoff filter was utilized as the light source. Electrochemical impedance spectroscopy (EIS) was recorded in the frequency range of 1,000 kHz–0.01 Hz under irradiation.

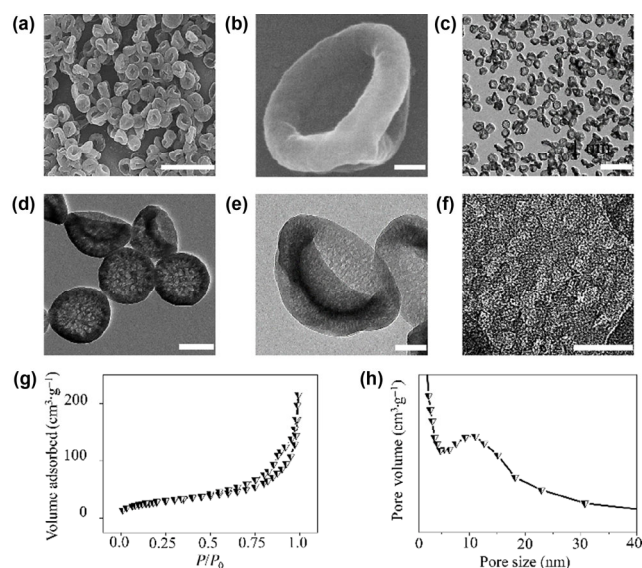
## 3 Results and discussion

SEM and TEM were employed to investigate the morphologies of samples obtained at different stages.  $\text{SiO}_2@\text{RF}$  shows a uniform spherical morphology with an average diameter of  $\sim 400 \text{ nm}$  and a solid structure (Figs. S1(a)–S1(c) in the Electronic Supplementary Material (ESM)). After hydrothermal treatment at 250  $^\circ\text{C}$ , the diameter of  $\text{SiO}_2@\text{RF}-250$  (Figs. S1(d)–S1(f) in the ESM) slightly increases to 450 nm. Silica nano-spikes with higher contrast are observed to be embedded in the RF matrix with a lower contrast on the outer region. The slightly increased particle size of  $\text{SiO}_2@\text{RF}-250$  compared to  $\text{SiO}_2@\text{RF}$  may be ascribed to the further growth of residual RF precursors (Fig. S2 in the ESM) during hydrothermal process. After removal of RF from  $\text{SiO}_2@\text{RF}-250$  by calcination in air, the resultant  $\text{SiO}_2$  nanoparticle (denoted as  $\text{SiO}_2-250$ ) exhibits a core-shell structure with solid core of an average diameter of  $\sim 350 \text{ nm}$  and a radial porous shell of a thickness of  $\sim 50 \text{ nm}$  (Figs. S3(a) and S3(b) in the ESM). The diameter of the  $\text{SiO}_2$  spikes on the shell is measured to be  $\sim 10 \text{ nm}$  (Fig. S3(c) in the ESM). The above results are consistent with the core-shell structure of  $\text{SiO}_2@\text{RF}-250$  shown in Scheme 1.

Removing  $\text{SiO}_2$  from  $\text{SiO}_2@\text{RF}-250$  composite finally results in the formation of MRF-250. The total removal of silica is confirmed by TGA curve of MRF-250, in which 100% of weight loss is observed at  $\sim 600 \text{ }^\circ\text{C}$  due to the complete decomposition of RF resin (Fig. S4 in the ESM). The SEM image (Fig. 1(a)) shows highly dispersed nanoparticles with a distinctive bowl-like morphology and average diameter of  $\sim 400 \text{ nm}$ . In the enlarged SEM image of a typical particle (Fig. 1(b)), deformed shell and relatively smooth surface are observed. TEM images in Figs. 1(c) and 1(d) further demonstrate the uniform nanobowl structure of MRF-250, in agreement with the SEM observations. The relatively lower contrast in the center region than outer shell further indicates the concaved structure [29]. At higher magnifications (Figs. 1(e) and 1(f)), large amount of mesopores with diameter of  $\sim 10 \text{ nm}$  are clearly found, which are distributed through the whole skeleton of MRF-250.

The mesoporous structure is further evidenced by the  $\text{N}_2$  adsorption–desorption isotherm (Fig. 1(g)), in which a typical type IV hysteresis loop is exhibited in high relative pressure regions ( $P/P_0$  of 0.75–1.0), suggesting the existence of abundant mesopores. The Brunauer–Emmett–Teller (BET) surface area and pore volume are measured to be  $101.0 \text{ m}^2\cdot\text{g}^{-1}$  and  $0.33 \text{ cm}^3\cdot\text{g}^{-1}$ . The pore diameter distribution curve calculated from the adsorption branch by Barrett–Joyner–Halenda (BJH) model shows that the mesopore size centers at  $\sim 10 \text{ nm}$  (Fig. 1(f)), in accordance with the TEM results. The mesopore size also matches with the size of shell  $\text{SiO}_2$  particle in  $\text{SiO}_2-250$ , further supporting the formation mechanism of MRF-250 shown in Scheme 1.

The effect of hydrothermal temperature on the structure of MRF-T was then carefully investigated ( $T = 150, 200, \text{ and } 270 \text{ }^\circ\text{C}$ ). MRF was also synthesized by directly removing silica from  $\text{SiO}_2@\text{RF}$ . As shown in Fig. S5 in the ESM, all the RF samples possess bowl-like morphology with more deformation at increasing hydrothermal temperature, which may be ascribed to the higher degree of polymerization and shrinkage at higher temperature. The  $\text{N}_2$  isotherms of MRF, MRF-150 and MRF-200 show type I hysteresis loop, different from MRF-250 (Fig. S6(a) in the ESM). Meanwhile, no obvious peaks are found in the range of mesopores pore size distribution curves (Fig. S6(b) in the ESM). This may be ascribed to that the RF framework obtained at a relatively lower hydrothermal temperature is not

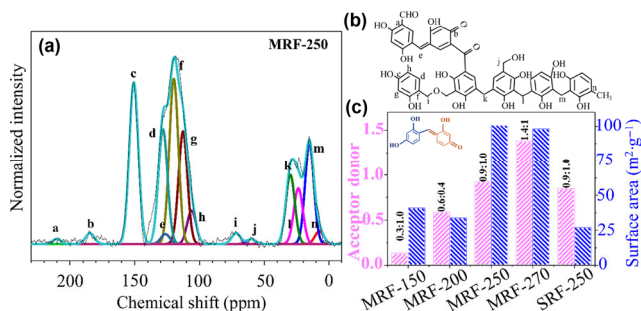


**Figure 1** (a) and (b) SEM images, (c)–(f) TEM images, (g)  $\text{N}_2$  sorption isotherms and (h) pore size distribution curves of MRF-250. Scale bars are (a) and (c) 1  $\mu\text{m}$ , (d) 200 nm, (b) and (e) 100 nm, and (f) 50 nm, respectively.

rigid enough to maintain the mesoporous structure during silica removing, thus resulting in extremely low BET surface area and pore volume (Table S1 in the ESM). At a higher hydrothermal temperature, MRF-270 possesses a similar mesoporous structure to MRF-250 with slightly lower surface area and pore volume. In addition, SRF-250 is also prepared by using the similar synthesis protocol of MRF except without adding TPOS (Fig. S7 in the ESM). Through hydrothermal treatment at 250 °C, SRF-250 is obtained, showing a solid and dense structure with a low surface area of 27 m<sup>2</sup>·g<sup>-1</sup> and a pore volume of 0.06 cm<sup>3</sup>·g<sup>-1</sup>.

The various carbon structures in RF resins were investigated by solid-state <sup>13</sup>C NMR technique. The NMR spectrum of MRF-250 is presented in Fig. 2(a), which can be fitted into 14 carbon components (a–n in Fig. 2(b)), and assigned to aromatics, linkers and residual groups in RF resins [25]. Specifically, the peaks at 182 ppm (b in Fig. 2(a)) and 126 ppm (e in Fig. 2(a)) are assigned to the quinone C=O carbon [30] of the quinoid units (A) and the corresponding methine linker carbon [31] with almost the same peak areas. This observation indicates the formation of quinoid units  $\pi$ -conjugated with benzenoid units via methine linkers according to a previous report [25]. Furthermore, the D/A molar ratios in different RF samples are calculated by integration of the a–n components in the spectra for the respective resins (Fig. S8 in the ESM). As summarized in Fig. 2(c), the A/D ratio increases from 0.3:1.0 to 1.4:1 by increasing the hydrothermal temperature from 150 to 270 °C. At the same hydrothermal temperature, the A/D ratio of SRF-250 is almost same with MRF-250 (~ 0.9:1.0), close to the optimized D/A coupling ratio of 1.

The chemical structures of different RF materials were further studied by FTIR (Fig. S9 in the ESM). The spectrum of MRF exhibits bands at 1,615, 1,450, and 1,303 cm<sup>-1</sup>, are assigned to C=C group of aromatic ring, C–H group of methylene linker, and C–H group of aromatic ring, consistent with the reported RF material synthesized at room temperature [32]. With increasing the hydrothermal temperature to 250 and 270 °C, a new peak of quinone group is observed at 1,650 cm<sup>-1</sup> in the spectra of MRF-250, 270 and SRF-250. Meanwhile, the band intensities of aromatic ring (C=C) and methylene linker (C–H) groups increase, indicating the formation of methine linkers according to the previous reports [25, 33].

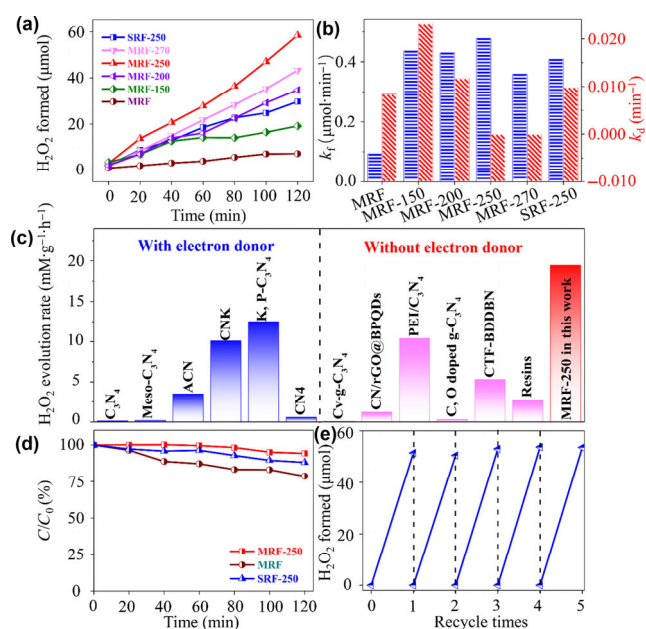


**Figure 2** (a) Solid-state <sup>13</sup>C-NMR spectrum for MRF-250. The assignments of the respective carbon components: aldehyde –CHO (210 ppm: a), quinone C=O (182 ppm: b), resorcinol C–OH (153 ppm: c), non-substituted resorcinol C at the meta position (130 ppm: d), methine linker –C= (126 ppm: e), substituted resorcinol C (117 ppm: f), non-substituted resorcinol C at the para and ortho positions (110 ppm: g, 105 ppm: h), methylene ether linker –C–O–C– (70 ppm: i), methylol C–OH (55 ppm: j), methylene linker –C– substituted to 4,4',-2,4',- and 2,2'-positions of resorcinols (30 ppm: k, 20 ppm: l, 10 ppm: m), and methyl –CH<sub>3</sub> (5 ppm: n). (b) The possible chemical structure of MRF-250. (c) The A/D ratio and BET surface areas of MRF-150, MRF-200, MRF-250, MRF-270 and SRF-250. The mole fractions of the quinoid and benzenoid units in the resins were determined from <sup>13</sup>C-NMR spectrum.

The XRD patterns of different RF resins are shown in Fig. S10 in the ESM. All resins exhibit broad diffraction at  $2\theta = \sim 20^\circ$ , originated from the  $\pi$ -stacking interaction between D–A couples. It can be also found that this diffraction shifts to higher degrees for the resins prepared at higher hydrothermal temperatures, implying a narrowed distance between the aromatic planes with stronger  $\pi$ -stacking [25]. Together with the NMR and FTIR results, the formation of D–A coupled MRF-250 with a D/A coupling ratio close to 1 is demonstrated.

The photocatalytic activities of synthesized catalysts for H<sub>2</sub>O<sub>2</sub> production are evaluated under visible-light irradiation without using sacrificing electron donors (Fig. 3(a)). The time-dependent change in the amounts of generated H<sub>2</sub>O<sub>2</sub> is shown in Fig. 3(a). MRF exhibits poor activity with H<sub>2</sub>O<sub>2</sub> production of 7.2  $\mu$ mol after reaction for 120 min. Through hydrothermal treatment, the H<sub>2</sub>O<sub>2</sub> production amount gradually increases from 19.2 to 58.4  $\mu$ mol with temperature increasing from 150 to 250 °C. When the temperature is further raised to 270 °C, less H<sub>2</sub>O<sub>2</sub> amount of 43.3  $\mu$ mol is generated. Therefore, the optimized H<sub>2</sub>O<sub>2</sub> production activity is achieved by MRF-250, also superior to SRF-250 that produces 29.7  $\mu$ mol of H<sub>2</sub>O<sub>2</sub> in 120 min, indicating the positive contribution of both D–A couples and mesopores during photocatalysis. Notably, MRF-250 delivers a H<sub>2</sub>O<sub>2</sub> production rate of 19.4 mM·g<sup>-1</sup>·h<sup>-1</sup>, which is higher than most reported sacrificing electron donor-free systems, even comparable to the best catalysts using sacrificial agents (Fig. 3(c) and Table S2 in the ESM) [12, 13, 19, 20, 25, 34–40]. By prolonging the reaction time to 24 h, the H<sub>2</sub>O<sub>2</sub> generation amount of MRF-250 increases to 169.2  $\mu$ mol (Fig. S11 in the ESM), higher than that of SRF-250 (106.2  $\mu$ mol), indicating the sustainable production of H<sub>2</sub>O<sub>2</sub>.

Generally, the concentration of H<sub>2</sub>O<sub>2</sub> is determined by the competition between the H<sub>2</sub>O<sub>2</sub> formation ( $k_f$ ) and decomposition ( $k_d$ ) rates over the catalysts, which can be calculated based on the following formula  $[H_2O_2] = (k_f/k_d)(1 - \exp(-k_d t))$  [11]. As shown in Fig. 3(b), MRF-250 exhibits the highest  $k_f$  and lowest  $k_d$  among all samples. In addition, the photocatalytic



**Figure 3** (a) Time-dependent H<sub>2</sub>O<sub>2</sub> photoproduction profiles using various RF photocatalysts. (b) The H<sub>2</sub>O<sub>2</sub> formation rate constant ( $k_f$ , blue) and H<sub>2</sub>O<sub>2</sub> decomposition rate constant ( $k_d$ , red) of various RF photocatalysts. (c) Comparison of H<sub>2</sub>O<sub>2</sub> production rate with reported photocatalysts. (d) The photocatalytic decomposition of H<sub>2</sub>O<sub>2</sub> (0.1 mM) for MRF-250, MRF, and SRF-250 under visible light irradiation. (e) Reusability of MRF-250 for H<sub>2</sub>O<sub>2</sub> production.

decomposition of  $\text{H}_2\text{O}_2$  was also measured [41] by using the 0.1 mM  $\text{H}_2\text{O}_2$  aqueous solution as origin reaction solution. As shown in Fig. 3(d), 10% and 20% of  $\text{H}_2\text{O}_2$  are decomposed after 120 min by SRF-250 and MRF respectively, but only 6% of  $\text{H}_2\text{O}_2$  is decomposed by MRF-250. Therefore, MRF-250 not only promotes the production of  $\text{H}_2\text{O}_2$  but also prevents the subsequent decomposition of  $\text{H}_2\text{O}_2$  under irradiation.

The SCC efficiency of MRF-250 was tested under AM1.5G simulated sunlight ( $\lambda > 420$  nm) according to the previous report [25]. As shown in Fig. S12 in the ESM, the SCC efficiency for  $\text{H}_2\text{O}_2$  generation is 0.84% after 1 h of photoirradiation, then gradually decreases to 0.33% at 5 h of photoirradiation. Further prolonging the reaction time to 8 h results in an SCC efficiency of 0.31% without significant decrease. The sample after reaction for 4 h was collected and characterized by the NMR and FTIR (Figs. S13 and S14 in the ESM). The ketone carbon (in Fig. S13 in the ESM) at 190 ppm is found, but not in the fresh MRF-250, suggesting the resin oxidation may consume the photogenerated holes and promote electron–hole separation for  $\text{O}_2$  reduction into  $\text{H}_2\text{O}_2$  [25]. This is evidenced by the decreased SCC efficiency of reused MRF-250, the value of which is  $\sim 0.32\%$  at 1 h, lower than that of fresh MRF-250 (0.84%, Fig. S15 in the ESM). However, this contribution is expected to decrease when available sites of resin (e.g., methylol and methylene groups) are oxidized, leading to gradually decreased SCC efficiency with prolonged reaction time. The higher SCC efficiency decrease of MRF-250 than reported RF [25] may be ascribed to the high specific surface area of MRF-250 with more surface exposed functional groups that can be oxidized.

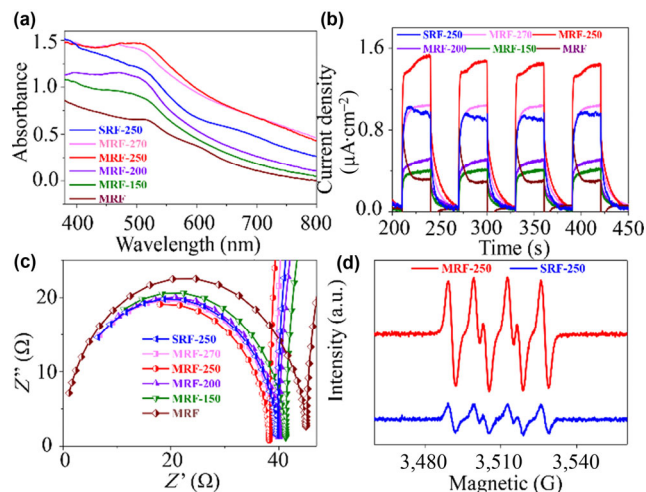
In addition, from the NMR spectrum the peak of quinone group at 182 ppm is observed and the A/D ratio is calculated to be  $\sim 0.88:1$ , similar to that of fresh MRF-250 (0.9:1). In the FTIR spectra of MRF-250 after reaction for 4 h, the peak of quinone group is also observed at  $\sim 1,650$   $\text{cm}^{-1}$ . Therefore, the SCC efficiency change as a function of time should be mainly attributed to the resin self-oxidation, instead of the D–A couple structure.

To evaluate the effect of light condition on the  $\text{H}_2\text{O}_2$  production, the AQY of MRF-250 was measured with four wavelengths (Fig. S16 in the ESM). The AQY reached the peak value of 2.9% at 365 nm and decreased to 2.5%, 1.0% and 0.3% at 450, 550 and 600 nm, respectively, which is in accordance with the absorption spectrum of MRF-250.

The cycling performance of MRF-250 was then determined. As shown in Fig. 3(e), after recycled for five times under the same conditions, MRF-250 shows negligible changes of the catalytic performance with 98% of  $\text{H}_2\text{O}_2$  amount generated compared to the first cycle, indicating its robust activity. In addition, the TEM image of MRF-250 (Fig. S17 in the ESM) after use shows well-retained mesoporous structure and bowl-like morphology.

To gain insight into the enhanced activity of MRF-250, the semiconductive properties were further studied. The UV–vis absorption spectra of different RF photocatalysts are shown in Fig. 4(a). MRF exhibits relatively low absorption in the range of visible light. With the hydrothermal temperature rising, the absorption is enhanced first and then reduced, and reaches the peak at 250 °C due to the optimized D/A ratio (close to 1) in MRF-250, which can extend the  $\pi$ -delocalization and reduce the band gap according to a previous report [25]. Compared to SRF-250 with almost the same D/A ratio, MRF-250 also shows enhanced light absorption. This may be ascribed to that the created mesopores in MRF-250 with high surface area promote the exposure and utilization of D–A couples, thus resulting in the superior light harvesting ability.

To investigate the separation and transfer behaviors of charge



**Figure 4** (a) UV–vis absorption spectra. (b) Transient photocurrent responses and (c) EIS profiles of different RF photocatalysts. (d) ESR signals of  $\text{DMPO}\cdot\text{O}_2^-$  over MRF-250 and SRF-250 under visible light.

carries, transient photocurrent responses and EIS were also tested. Within the light on/off cycles, the generated photocurrent intensity first increases and then decreases when the hydrothermal temperature increases (Fig. 4(b)). Among different MRF samples, MRF-250 delivers the largest photocurrent, which is also  $\sim 2$  times higher than SRF-250, suggesting the highest separation efficiency of electrons and holes. The EIS spectra (Fig. 4(c)) show that MRF-250 presents the smallest semicircle diameter, indicating the lowest charge transfer resistance.

To get insights on the mechanism of photocatalytic  $\text{H}_2\text{O}_2$  production of MRF-250 and SRF-250, the 5,5-dimethyl-pyrroline N-oxide (DMPO) spin-trapping ESR technique was employed for the detection of  $\cdot\text{O}_2^-$ . As shown in Fig. 4(d), characteristic peaks assigned to  $\text{DMPO}\cdot\text{O}_2^-$  are observed, indicating the generation of  $\cdot\text{O}_2^-$  during the photocatalytic reaction. Therefore, the  $\text{H}_2\text{O}_2$  production on MRF-250 is likely through a two-step single-electron reduction mechanism with  $\cdot\text{O}_2^-$  as the intermediate product ( $\text{O}_2 + e^- \rightarrow \cdot\text{O}_2^-$  and  $\cdot\text{O}_2^- + 2\text{H}^+ + e^- \rightarrow \text{H}_2\text{O}_2$ ) [12, 34]. In addition, the signal intensities in the spectrum of MRF-250 are stronger than those of SRF-250, further confirming the enhanced activity of MRF-250.

Based on the aforementioned observations, the excellent photocatalytic performance of MRF-250 may be attributed to following reasons: (1) The optimized ratio of D–A couple (close to 1:1) extends the  $\pi$ -delocalization, enhances the light absorption and produces large amount of charge carries under irradiation; (2) the mesoporous and concaved bowl-like structure accelerates the charge transfer to the surface of catalyst, and promotes the charge separation. Meanwhile, the further reaction with produced  $\text{H}_2\text{O}_2$  is disadvantaged, thus preventing the subsequent decomposition of  $\text{H}_2\text{O}_2$ ; (3) the mesoporous structure with high surface area also increases the exposure of active sites and facilitates the adsorption of reactants and desorption of products, thus accelerating the photocatalytic reaction.

## 4 Conclusion

In summary, we report the synthesis of MRF nanobowls with optimized benzenoid–quinoid donor–acceptor (D–A) couples as efficient photocatalysts through an assembly–hydrothermal-etching process for  $\text{H}_2\text{O}_2$  production in a pure water system. The hydrothermal temperature is optimized to be  $\sim 250$  °C for obtaining MRF-250 with large surface area, suitable D–A couple ratio, enhanced light absorption, charge separation and mass

transfer. Benefiting from these structural advantages, MRF-250 exhibits the highest  $\text{H}_2\text{O}_2$  yield of  $19.4 \text{ mM}\cdot\text{g}^{-1}\cdot\text{h}^{-1}$  among all prepared samples, which is even superior to reported metal-free photocatalysts without the usage of sacrificial agents.

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