

# Polyacrylic Acid-grafted Magnetite Nanoparticles for Remediation of Pb(II)-Contained Water

Xiaoyu Guan, Sunxian Yan, Qi Zeng, Zhou Xu<sup>1</sup>, Yi Chen\*, and Haojun Fan

Key Laboratory of Leather Chemistry and Engineering of Ministry of Education, Sichuan University, Chengdu 610065, P. R. China

<sup>1</sup>Solid-state Fermentation Resource Utilization Key Laboratory of Sichuan Province, Yibin University, Yibin 644007, P. R. China

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**Abstract:** Toxic Pb(II) contaminants in water pose a significant threat to the environment and public health, and thus technologies for Pb(II) remediation are attracting increasing industrial interests. In the present work, polyacrylic acid, offering abundant carboxyl groups capable of coordination with Pb(II) cations, was grafted from the magnetite nanoparticle surface *via* the bridging function of silane coupling agent for remediation of Pb(II)-contained water. Multiple techniques were employed to characterize the structure of the nanocomposite, and the effects of nanoadsorbent dose, pH value, and temperature on Pb(II) removal capability of the nanocomposite were investigated, respectively. Furthermore, adsorption kinetics and isotherms studies were performed for better understanding the mechanism by which Pb(II) cations were adsorbed. Finally, the feasibility of regenerating the exhausted nanoadsorbent by simply changing pH value was explored. According to these results, we intend to offer an efficient, separable, and reusable magnetic nanoadsorbent that may be a potential candidate for remediating Pb(II) contamination in water.

**Keywords:** Polyacrylic acid, Magnetite, Nanocomposite, Adsorption, Pb(II)

## Introduction

Heavy metal ions in industrial wastewater and natural water, due to their toxicity and bioaccumulation through the food chain, pose a significant threat to environment and, thus, human health. Among various heavy metal ions, lead ion (Pb(II)) is believed to be a dominating contaminant, the hazardous effects of which have been documented since ancient Rome. Exposure to water with even a low concentration of Pb(II) can give rise to toxic effects that may suppress cellular activities, and hence arouse a variety of cancers [1-3]. With fast industrialization and modernization all over the world, the perniciousness of Pb(II) to human beings will persist, if not worsen, in the short run. Over the past few decades, significant efforts were directed to explore technologies for Pb(II) removal from aqueous solution, such as ion exchange [4], chemical precipitation [5], membrane-based process [6], and adsorption [7]. Of these effectual technologies, adsorption exhibits both economic and operational feasibility by virtue of its versatile adaptability, cost effectiveness as well as easy regeneration [8,9].

Ever since 1950s, it has been demonstrated that materials that range from approximately 1 to 100 nanometers in at least one dimension have distinct advantages over traditional bulk materials, which has been attracting increasingly extensive attention for both fundamental research and practical applications [10-15]. On the one hand, the extremely small size, and thus high specific surface area of nanoscale materials are propitious for interface-related applications,

such as adsorption or catalysis. On the other hand, the surface chemistry of nanoscale materials proves tunable, yielding nanocomposite manifesting fundamentally new functions or emergent properties unattainable in traditional composites. Recently, magnetite-supported nanomaterials have attracted extensive interests in diverse fields. By decorating the magnetite surface with different functional materials, the resultant nanocomposite can be manipulated conveniently by using an external magnetic field. This so-called “remote control” or “action at a distance” has currently found a broad spectrum of possible applications, including electronics, catalysis, enzyme immobilization, targeted drug delivery, magnetic resonance imaging, and environmental remediation [16-21]. One compelling example is that of magnetite nanoparticles surface-grafted with poly(*N*-acryloyl ciprofloxacin-*co*-acrylic acid), which were reported as a magnetically-recoverable nanocomposite potentially applicable for microbial decontamination of collagen solution [19]. In addition, Feng *et al.* explored the feasibility of using polyhydroquinone-coated magnetite as a recyclable catalyst for degradation of flumequine in aqueous solution [20].

In this study, polyacrylic acid was grafted from vinyl-silane modified magnetite nanoparticle surface *via* free radical polymerization, in an attempt to design a nanoadsorbent potentially applicable for remediating Pb(II)-contained water. Multiple techniques were employed to characterize the structure of the nanoadsorbent, and the effects of nanoadsorbent dose, pH value, and temperature on Pb(II) removal capability of the nanoadsorbent were investigated, respectively. Furthermore, adsorption kinetics and isotherms

\*Corresponding author: chen\_yi\_leon@scu.edu.cn

studies were performed for better understanding the mechanism by which Pb(II) cations were adsorbed. Finally, the feasibility of regenerating the exhausted nanoadsorbent by simply changing pH value was explored. Based on these results, we intend to offer an efficient, separable, and reusable magnetic nanoadsorbent that may be an addition to the ongoing fight against Pb(II) contamination in water.

## Experimental

### Materials

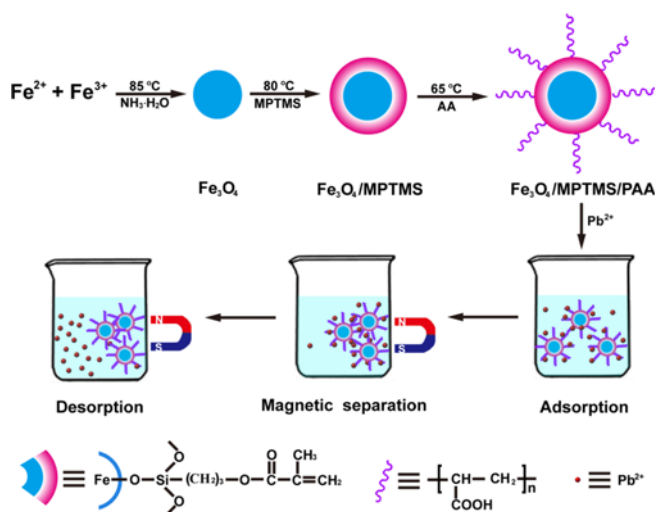
Ferric chloride ( $\text{FeCl}_3$ , reagent grade, purity  $\geq 98.0\%$ ), ferrous chloride dihydrate ( $\text{FeCl}_2 \cdot 2\text{H}_2\text{O}$ , ACS reagent, purity  $\geq 99.5\%$ ), ammonium hydroxide solution ( $\text{NH}_3 \cdot \text{H}_2\text{O}$ , ACS reagent, 25.0-30.0%  $\text{NH}_3$  basis), and anhydrous ethanol ( $\text{CH}_3\text{CH}_2\text{OH}$ , reagent grade, purity  $\geq 99.5\%$ ) were purchased from Cheng Jie Chemical Engineering Co. Ltd. (Shanghai, China). Methacryloxy propyl trimethoxyl silane (MPTMS, deposition grade, purity  $\geq 99\%$ ) and toluene ( $\text{C}_7\text{H}_8$ , analytical grade, purity  $\geq 99.5\%$ ) were available from Sigma-Aldrich (Shanghai, China). Furthermore, *N,N*-dimethyl formamide (DMF, analytical grade, purity  $\geq 99.5\%$ ), anhydrous acrylic acid (AA, recrystallized from chloroform before use, purity  $\geq 99.5\%$ ), azobisisobutyronitrile (AIBN, recrystallized from methanol before use, purity  $\geq 99\%$ ), sodium hydroxide (NaOH, reagent grade, purity  $\geq 98.0\%$ ), nitric acid ( $\text{HNO}_3$ , reagent grade, purity  $\geq 98.0\%$ ), and lead nitrate ( $\text{Pb}(\text{NO}_3)_2$ , analytical grade, purity  $\geq 99.5\%$ ) were obtained from Kelong Chemical Engineering Co. Ltd. (Chengdu, China).

### Preparation of $\text{Fe}_3\text{O}_4$ Nanoparticles

$\text{Fe}_3\text{O}_4$  nanoparticles were synthesized according to a slightly modified version of a previously published protocol [22]. Briefly,  $\text{FeCl}_3$  (2.8 g) and  $\text{FeCl}_2 \cdot 2\text{H}_2\text{O}$  (1.6 g) were dissolved in nitrogen-purged ultrapure water ( $18.2 \text{ M}\Omega \cdot \text{cm}$  at  $25^\circ\text{C}$ ) to yield a mixture, where the molar ratio of  $\text{Fe}^{3+}$  and  $\text{Fe}^{2+}$  cations approximated to 1.75:1. Then,  $\text{NH}_3$  aqueous solution (25.0-30.0%  $\text{NH}_3$  basis) was added dropwise until the pH value reached 10. After incubated at  $85^\circ\text{C}$  for 30 min, the black  $\text{Fe}_3\text{O}_4$  precipitations were magnetically separated and washed with anhydrous ethanol for five times. Finally, the product was dried in a vacuum oven at  $60^\circ\text{C}$  until a constant weight.

### Vinyl-silane Modification of $\text{Fe}_3\text{O}_4$ Nanoparticles

To facilitate polyacrylic acid (PAA) grafting from the magnetite nanoparticle surface, the magnetite nanoparticles prepared above were modified by vinyl-terminated silane coupling agent first. Typically, 2 g  $\text{Fe}_3\text{O}_4$  and 250 ml toluene were added into a three-necked flask equipped with a flowing nitrogen atmosphere and a mechanical stirrer. After mechanical stirring at ambient temperature for 30 min, 4 ml MPTMS was added in batches and then the temperature was



**Scheme 1.** Synthesis of  $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$  nanocomposite and its application for Pb(II) removal from aqueous solution.

elevated up to  $80^\circ\text{C}$  for incubation. After 10 h, the engineered magnetite nanoparticles, referred to as  $\text{Fe}_3\text{O}_4/\text{MPTMS}$ , were isolated from the solution by using a magnet, washed five times with anhydrous ethanol, and dried at  $70^\circ\text{C}$ .

### Synthesis of $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$ Nanoparticles

PAA-functionalization of  $\text{Fe}_3\text{O}_4/\text{MPTMS}$  nanoparticles was carried out according to the following procedure. In brief, 1 g  $\text{Fe}_3\text{O}_4/\text{MPTMS}$ , 150 ml DMF, 2 ml AA, and 0.02 g AIBN were added into a 250 ml three-necked flask. Free radical polymerization was then carried out at  $65^\circ\text{C}$  under an atmosphere of nitrogen. After 8 h, the reaction was quenched by cooling the system to room temperature. The magnetic nanocomposite obtained, referred to as  $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$ , was separated with a magnet and washed repeatedly with ultrapure water to remove any excess AA, PAA from self-polymerization and/or AIBN. The synthesis procedure and the structure of the product are illustrated in Scheme 1.

### Structural Characterization of $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$ Nanoparticles

SEM images were taken on a JEOL JSM-7500F (Japan) field emission scanning electron microscope operated at an accelerating voltage of 5.0 kV. TEM specimens were observed on a JEOL JEM-2010 transmission electron microscope (Japan) at an accelerating voltage of 200 kV. Brunauer-Emmitt-Teller (BET) specific surface area was measured by low-temperature nitrogen adsorption/desorption experiments, conducted on a Micromeritics ASAP 2020 Accelerated Specific Surface Area and Porosimetry Analyzer (United States). X-ray photoelectron spectra (XPS) measurement was conducted on a Kratos XSAM800 system (Britain) with  $\text{Al-K}\alpha$  radiation (1486.6 eV) in the constant analyzer energy mode. During data acquisition, all the binding energies were

calibrated based on the hydrocarbon C1s peak set at 284.6 eV. Total organic carbon (TOC) content was measured by using an Apollo 9000 TOC/TN auto analysis system (Tekmar-Dohrmann, United States). XRD patterns were collected on a Philips X'Pert pro MPD diffractometer equipped with a copper anode producing X-rays with a wavelength of 1.5406 Å in the range of  $2\theta=10-80^\circ$ . A model No. 735 vibrating sample magnetometer (VSM, NanJing, China) with a magnetic field of  $\pm 10$  kOe was employed to determine the magnetization of the magnetic nanoparticles.

### Pb(II) Adsorption and Desorption Experiment

Aqueous Pb(II) stock solution with different concentrations were prepared by dissolving a predetermined quantity of  $\text{Pb}(\text{NO}_3)_2$  in ultrapure water. Batch Pb(II) adsorption studies were carried out by mixing a predetermined amount of  $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$  with a certain volume (25 ml) of Pb(II) aqueous solution held in a 100-ml Erlenmeyer flask. The mixture was subject to ultrasonic oscillation for 2 min, and then shaken at 200 rpm in a thermostatic orbit incubator to reach equilibrium. The impact of nanoadsorbent dose, pH value, and temperature on Pb(II) removal capacity of  $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$  were investigated, respectively. After a predetermined adsorption time, the nanoparticles were separated temporarily by using a magnet, and 1 ml of the residual solution was withdrawn by a syringe. In order to measure the residual concentration of Pb(II) by inductively coupled plasma-optical emission spectroscopy (ICP-OES, Optima 2100 DV, Perkin-Elmer Instruments, United States), the solution withdrawn was subject to traditional acid digestion first. Briefly, the withdrawn solution (1 ml) was introduced into a 100-ml Erlenmeyer flask containing 30 ml of ultrapure water and 2 ml of concentrated  $\text{HNO}_3$ , and then digested on a fuming cupboard at  $100^\circ\text{C}$  until the volume of the solution decreased to approximately 10 ml. After that, 2 ml of  $\text{H}_2\text{SO}_4$  aqueous solution (50 % v/v) was added and the digestion process continued for another 1 min. Finally, the digested solution was transferred into a 50-ml volumetric flask, diluted with ultrapure water to volume, and then filtered through a 0.2  $\mu\text{m}$  cellulose acetate filter before ICP-OES measurement. Detailed experimental condition for Pb(II) adsorption experiment mentioned above were tabulated in Table S1. The amount of Pb(II) adsorbed per unit nanoadsorbent mass at time  $t$  ( $q_t$ ) was calculated according to the following equation:

$$q_t = \frac{C_0 \times V_0 - C_t \times V_t}{m} \quad (1)$$

where  $C_0$  (mg/l) and  $V_0$  (l) are the initial concentration and volume (25 ml) of the Pb(II) solution,  $C_t$  (mg/l) and  $V_t$  (l) refer to the residual concentration and volume of the Pb(II) solution at time  $t$ , and  $m$  (g) represents the nanoadsorbent dose. In addition, the Pb(II) removal percentage at equilibrium was quantified by equation (2):

$$\% \text{ Removal} = \frac{C_0 - C_e}{C_0} \times 100 \quad (2)$$

where  $C_0$  (mg/l) and  $C_e$  (mg/l) stand for the initial and equilibrium concentration of the Pb(II) solution, respectively.

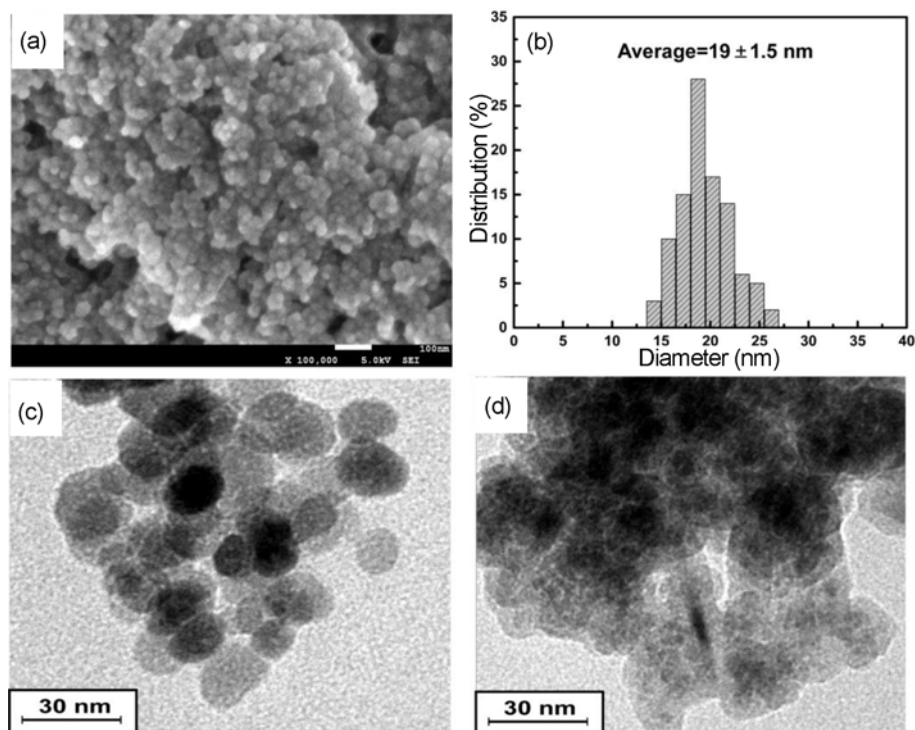
To investigate the reusability of  $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$ , the exhausted nanoadsorbent was regenerated by using a 0.1 M  $\text{HNO}_3$  solution as the desorbent. Desorption of Pb(II) was carried out by mechanically stirring the exhausted nanoadsorbent in the  $\text{HNO}_3$  solution for 45 min at  $50^\circ\text{C}$ , and then the regenerated nanoadsorbent was washed thoroughly with ultrapure water until neutral. Subsequently, the regenerated nanoadsorbent was employed for Pb(II) removal from aqueous solution again, according to the methods described above. This desorption-adsorption procedure was repeated for five coherent recycles.

## Results and Discussion

### Structure of $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$

Figure 1(a) presented the SEM image of native  $\text{Fe}_3\text{O}_4$  nanoparticles. Clearly, they were roughly spherical in geometry with similar particle size, and piled up together after drying. The statistical size distribution of these  $\text{Fe}_3\text{O}_4$  nanoparticles, which was obtained by cropping the SEM image *via* Image *J* software developed by National Institutes of Health (United States), was exhibited in Figure 1(b). The diameter of these native  $\text{Fe}_3\text{O}_4$  nanoparticles averaged  $19 \pm 1.5$  nm, ranging from 13 to 26 nm. Furthermore, according to low-temperature nitrogen adsorption isotherm, these  $\text{Fe}_3\text{O}_4$  nanoparticles possessed a specific surface area of  $55.6 \pm 1.1$   $\text{m}^2/\text{g}$ . After surface grafting of PAA, the specific surface area of the nanocomposite decreased to  $45.9 \pm 0.8$   $\text{m}^2/\text{g}$ . In spite of such decrease, the specific surface area of the nanocomposite was still so large that facilitated more Pb(II) adsorption and, thus, removal from aqueous solution. Figure 1(c) and (d) represented the TEM images of  $\text{Fe}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$  nanoparticles, respectively. In the case of  $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$ , it was clear that the  $\text{Fe}_3\text{O}_4$  nanoparticles, manifesting as dark contrast, were wrapped by a layer of light contrast. This observation indicated that a layer of polymer was successfully grafted from the  $\text{Fe}_3\text{O}_4$  surface, yielding a typical core-shell structure as designed.

Whether PAA was successfully grafted from the engineered  $\text{Fe}_3\text{O}_4$  nanoparticles as designed was further qualitatively verified by analyzing the XPS spectra of  $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$  demonstrated in Figure 2. As could be seen in Figure 2(a), four elements, including Fe, Si, C, O, were detected in the XPS survey spectrum of  $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$  nanocomposite. The high resolution XPS spectra of these four elements were further illustrated in Figure 2(b)-(e), respectively. In Figure 2(b), the photoelectron peak at 725.1 eV corresponded to the binding energy of Fe  $2p_{1/2}$  in the  $\text{Fe}_3\text{O}_4$  core, while the peak at 711.9 eV was attributed to Fe  $2p_{3/2}$



**Figure 1.** (a) SEM image, (b) size distribution of native  $\text{Fe}_3\text{O}_4$  nanoparticles; TEM images of (c)  $\text{Fe}_3\text{O}_4$  and (d)  $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$  nanoparticles.

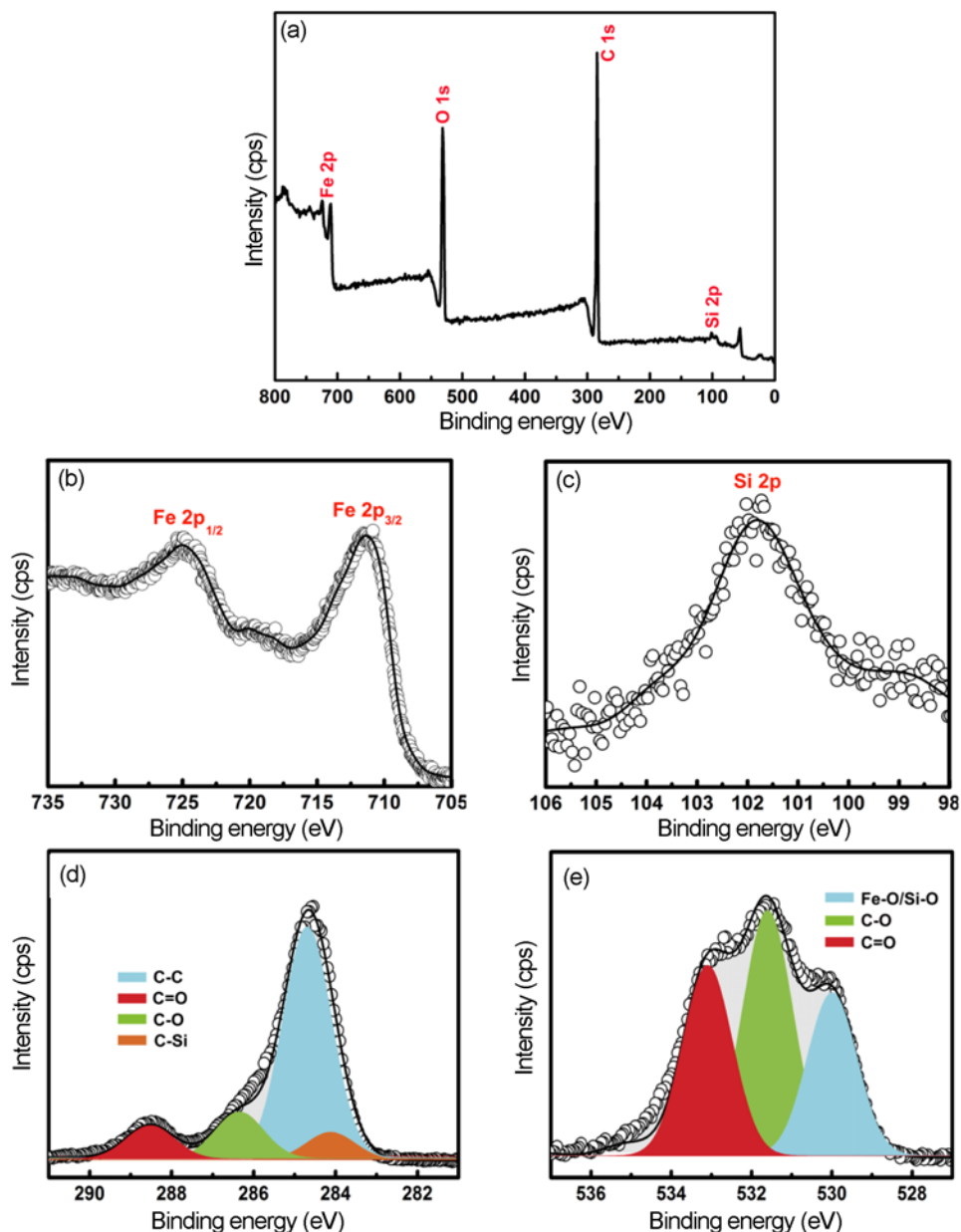
[19]. In addition, another XPS signal with relatively low intensity was found at 101.9 eV, corresponding to Si 2p component. This signal could only be ascribed to MPTMS derivative. The high resolution C 1s and O 1s core-level spectra, both deconvoluted into four Gaussian components, were plotted in Figure 2(d) and (e), respectively. The C=O (288.6 eV/533.1 eV) and C-O (286.6 eV/531.4 eV) components could be assigned either to the ester from MPTMS or to those carboxyls from polyacrylic acid. In addition, the C-Si (284.1 eV) and Si-O (530.0 eV) components could only be ascribed to MPTMS derivative, while the Fe-O (530.0 eV) component stemmed from the  $\text{Fe}_3\text{O}_4$  nanoparticle core. Furthermore, according to the theoretical carbon content (50.0 % (w/w)) in acrylic acid, as well as the total organic carbon (TOC) values in  $\text{Fe}_3\text{O}_4/\text{MPTMS}$  ( $168 \pm 2$  mg/g) and  $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$  ( $232 \pm 5$  mg/g), it could be calculated that the  $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$  nanocomposite roughly contained  $12.8 \pm 0.3$  % (w/w) of polyacrylic acid as the functional shell.

The crystalline structure and magnetic properties of  $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$  nanocomposite were verified by XRD patterns and magnetic hysteresis loops, respectively. Figure 3(a) illustrated the XRD patterns of native  $\text{Fe}_3\text{O}_4$ ,  $\text{Fe}_3\text{O}_4/\text{MPTMS}$ , and  $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$  nanoparticles, respectively. In these three samples, the diffraction peaks observed could be indexed to the crystal planes of magnetic  $\text{Fe}_3\text{O}_4$  nanoparticles. The peak positions and relative intensities were in good agreement with standard JCPDS data (75-0449),

revealing the spinel structure of the co-precipitated  $\text{Fe}_3\text{O}_4$  core [23,24]. In addition, a broad amorphous halo in the  $2\theta$  range from  $20.0^\circ$  to  $30.0^\circ$  appeared in both  $\text{Fe}_3\text{O}_4/\text{MPTMS}$  and  $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$  nanoparticles, indicating the presence of MPTMS derivative and the PAA shell, which differed in morphology from the core. Figure 3(b) showed the magnetic hysteresis loops of  $\text{Fe}_3\text{O}_4$  nanoparticles before and after surface modification. The hysteresis loops demonstrated the superparamagnetism of all three samples, because there was almost no coercivity once the magnetic field was removed. In addition, the saturated magnetization of native  $\text{Fe}_3\text{O}_4$ ,  $\text{Fe}_3\text{O}_4/\text{MPTMS}$ , and  $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$  nanoparticles was found to be 78.1, 40.8, and 18.9 emu/g, respectively. The decrease in saturation magnetization could be credited to decreased magnetite component after surface decoration [25,23]. In spite of such decrease, the magnetization of  $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$  nanocomposite was still strong enough for them to be separated from aqueous solution by the aid of an external magnetic field. As shown in the inset of Figure 3(b), the  $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$  nanocomposite could be magnetically recovered from aqueous solution within only 10 min, and as a result, the solution experienced a significant color change from black to transparent.

#### **Pb(II) Removal Capability of $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$**

The influence of nanoadsorbent dose on Pb(II) removal by  $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$  was presented in Figure 4(a). According

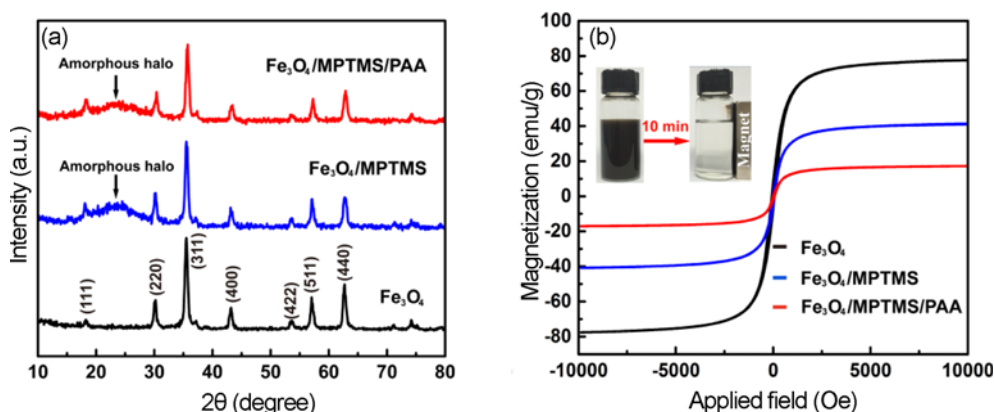


**Figure 2.** (a) XPS survey spectrum and high resolution XPS spectra of (b) Fe 2p, (c) Si 2p, (d) C 1s, (e) O 1s for Fe<sub>3</sub>O<sub>4</sub>/MPTMS/PAA nanocomposite. The experimental spectra were deconvoluted into Gaussian components after Shirley background subtraction using CasaXPS software.

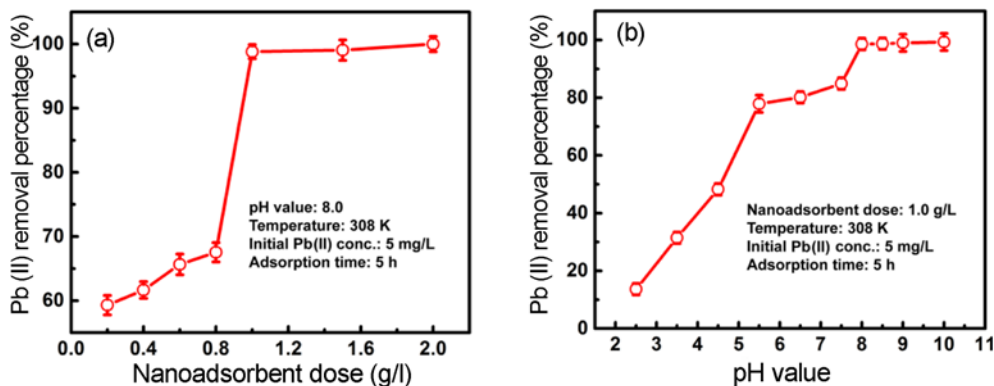
to these data, it was found that the nanoadsorbent dose affected Pb(II) uptake significantly. Increasing the nanoadsorbent dose from 0.2 g/l up to 1.0 g/l gave rise to a sharp increase in the Pb(II) removal percentage from 59.3±1.2 % to 97.5±0.8 %. This observation could be assigned to increased adsorption sites available. However, when the nanoadsorbent dose further increased from 1.0 g/l, the Pb(II) removal percentage levelled off, indicating an equilibrium had been established between the adsorbed Pb(II) and those dissociative in the solution. Based on these results, a nanoadsorbent dose of

1.0 g/l was selected for subsequent experiments.

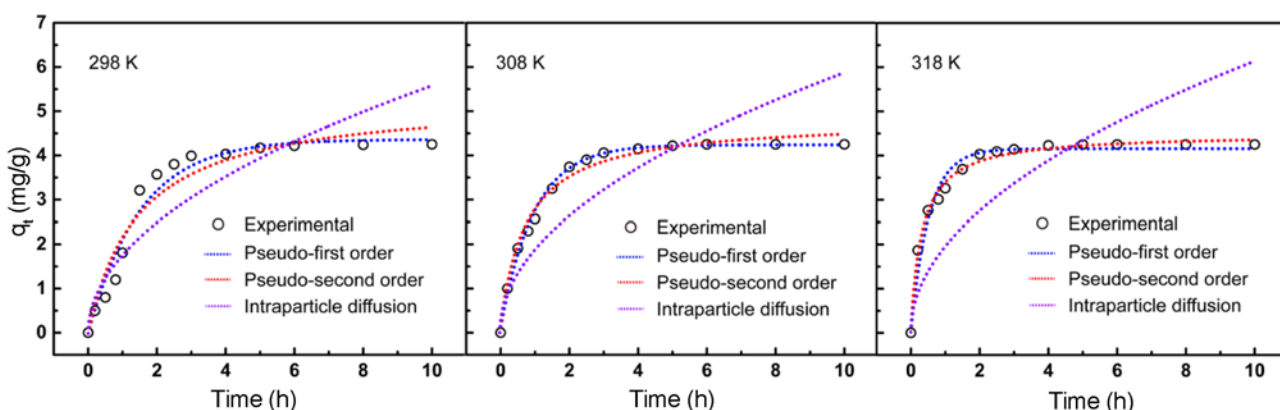
The pH value that governed the dissociation degree of carboxyl groups and the hydrolysis of Pb(II) was another important factor affecting Pb(II) removal capability of the nanoadsorbent. Since Pb(II) cations (initial Pb(II) concentration= 5 mg/l,  $T=308$  K) was inclined to precipitate as Pb(OH)<sub>2</sub> once the pH value exceeded 10 [26], the pH of interests herein was restricted to a range of 2.5-10. As could be seen in Figure 4(b), the Pb(II) removal percentage was only about 16 % when the pH value was 2.5. This phenomenon could



**Figure 3.** (a) XRD patterns and (b) room-temperature magnetic hysteresis loops of native Fe<sub>3</sub>O<sub>4</sub>, Fe<sub>3</sub>O<sub>4</sub>/MPTMS, and Fe<sub>3</sub>O<sub>4</sub>/MPTMS/PAA nanoparticles. The inset in (b) displays the appearance of 2.0 mg/ml Fe<sub>3</sub>O<sub>4</sub>/MPTMS/PAA nanocomposite dispersed in an aqueous solution of 0.1 M NaOH with a pH value of 8.0, and their fast response to an externally applied magnetic field.



**Figure 4.** Effect of (a) nanoadsorbent dose and (b) pH value on Pb(II) removal percentage from aqueous solution using Fe<sub>3</sub>O<sub>4</sub>/MPTMS/PAA nanoadsorbent.



**Figure 5.** Kinetics of Pb(II) adsorption on Fe<sub>3</sub>O<sub>4</sub>/MPTMS/PAA nanoadsorbent at three different temperatures (Initial Pb(II) concentration=5 mg/l; pH value=8.0; nanoadsorbent dose=1.0 g/l).

be ascribed to the fact that those carboxyl groups in PAA were predominantly undissociated, and thus uncoordinated with metal ions at such low pH value. As the pH value increased from 2.5 up to 8.0, the Pb(II) removal percentage

increased significantly to approximately 97.9±1.1%. On the one hand, this phenomenon could be attributed to increased dissociation degree of carboxyl groups in the PAA shell with increasing pH value. On the other hand, Pb(II) in aqueous

solution would gradually hydrolyze to form soluble hydroxide complexes, such as  $\text{Pb}(\text{OH})^+$ , when the pH value increased up to 8.0. According to modern coordination chemistry, the presence of hydroxide ligands usually made dissociated carboxyls easily accessible to the metal center [27], which facilitated adsorption of Pb(II) cations. However, with the dissociation degree of carboxyl groups and the hydrolysis of Pb(II) approaching maximum at a pH value of 8.0, the Pb(II) removal percentage levelled off as the pH value increased thereafter. To guarantee as much Pb(II) could be removed as possible by  $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$  nanoadsorbent, therefore, the pH value of the Pb(II) solution was set at 8.0 for all further experiments.

To better understand the adsorption process, the kinetic profiles of Pb(II) adsorption at three different temperatures were investigated, and the results were shown in Figure 5. It was found that regardless of the temperature, the Pb(II) removal rate was fast during the initial 2 h, followed by the adsorption approaching an equilibrium. The rapid Pb(II) adsorption by  $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$  nanoadsorbent during the first stage was due to more adsorption sites accessible on the surface of the nanoadsorbent. This kinetics feature was beneficial for practice application, which saved the operating time of  $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$  nanoadsorbent. In addition, pseudo-first order, pseudo-second order, and intraparticle diffusion models were employed to fit the experimental data in Figure 5, which shed light on possible adsorption mechanism of Pb(II) by  $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$  nanoadsorbent. The equations for these three models were given in equations (3), (4) and (5), respectively [28]:

$$q_t = q_e \times (1 - e^{-k_1 \times t}) \quad (3)$$

$$q_t = \frac{t}{\frac{1}{k_2 \times q_e^2} + \frac{t}{q_e}} \quad (4)$$

$$q_t = k_3 \times \sqrt{t} \quad (5)$$

where  $q_t$  and  $q_e$  (mg/g) refer to the amount of Pb(II) adsorbed per unit adsorbent mass at time  $t$  (min) and at equilibrium, respectively;  $k_1$  ( $\text{min}^{-1}$ ),  $k_2$  ( $\text{g}/\text{mg} \cdot \text{min}$ ), and  $k_3$  ( $\text{mg}/\text{g} \cdot \text{min}^{1/2}$ ) stand for pseudo-first order, pseudo-second order and intraparticle diffusion rate constants, respectively.

The fitting results by using non-linear regression were present in Table 1. For both pseudo-first order and pseudo-second order models, the average relative errors were relatively low ( $<3.45$ ) and the coefficients of determination approached unity, indicating that these two models described well the kinetics data. In general, pseudo-first order approach is based on the conception that the adsorption rate is dominated by only one process or a mechanism involving a single class of adsorbing sites; pseudo-second order model assumes that the adsorption procedure may be a chemical one involving valence forces by the exchange or sharing of electrons between adsorbate and adsorbent [28,29]. Thus, it could be inferred that the Pb(II) adsorption process by  $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$  nanoadsorbent was a chemical procedure involving valence forces *via* sharing or exchange of electrons, and the adsorption rate was limited by the availability of carboxyl groups only. Besides, it was found that  $k_1$ ,  $k_2$ , as well as  $q_e$  from both pseudo-first order and pseudo-second order models were enhanced with increasing temperature, indicating the endothermic nature of the adsorption procedure.

Adsorption isotherm is often used to describe the relationship between the residual metal ion concentration in solution and the amount of metal adsorbed by solid phase at equilibrium, which reflects the efficiency of the adsorbents [30]. In the present study, Langmuir isotherm and Freundlich isotherm models were employed to fit the experimental equilibrium data obtained. The Langmuir isotherm hypothesizes that the adsorption can only take place at a fixed number of definite localized sites by chemical action [30]. Freundlich isotherm is an empirical isotherm assuming that the amount of adsorbate on the surface of the adsorbent enhances with adsorbate concentration [30]. The equations of these two models were formulated as follows [31]:

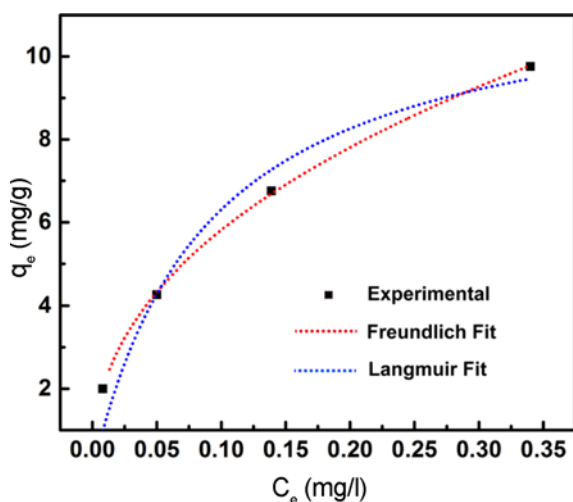
$$q_e = \frac{q_{\max} \times b \times C_e}{1 + b \times C_e} \quad (6)$$

$$q_e = K_F \times C_e^{1/n} \quad (7)$$

where  $q_e$  (mg/g) and  $C_e$  (mg/l) represent the adsorbate concentration in the solid and liquid phase at equilibrium, respectively;  $q_{\max}$  (mg/g) and  $b$  (l/mg) are Langmuir constants that express the theoretical maximum for adsorbate adsorption and the affinity of the adsorbent, respectively;  $K_F$  ( $(\text{L}/\text{g})^{-1/n}$ )

**Table 1.** Fitting results of Pb(II) adsorption on  $\text{Fe}_3\text{O}_4/\text{MPTMS}/\text{PAA}$  nanoadsorbent employing pseudo-first order, pseudo-second order, and intraparticle diffusion kinetic models

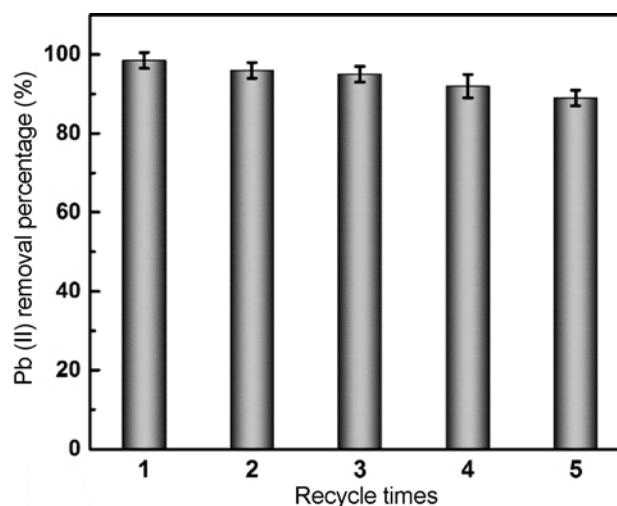
$T$ (K)	Pseudo-first order				Pseudo-second order				Intraparticle diffusion		
	$q_e$ (mg/g)	$k_1$ ( $\text{min}^{-1}$ )	$ARE$ (%)	$R^2$	$q_e$ (mg/g)	$k_2$ ( $\text{g}/\text{mg} \cdot \text{min}$ )	$ARE$ (%)	$R^2$	$k_3$ ( $\text{mg}/\text{g} \cdot \text{min}^{1/2}$ )	$ARE$ (%)	$R^2$
298	4.14	0.66	2.12	0.96	4.48	0.13	3.45	0.93	1.77	8.92	0.78
308	4.24	1.03	0.98	0.99	4.81	0.28	2.79	0.99	1.85	10.11	0.63
318	4.38	1.90	2.00	0.95	5.33	0.69	2.35	0.99	1.93	18.20	0.17



**Figure 6.** Adsorption isotherm of Pb(II) on Fe<sub>3</sub>O<sub>4</sub>/MPTMS/PAA nanoadsorbent (pH value=8.0; adsorption time=5 h; nanoadsorbent dose=1.0 g/l; temperature=308 K).

and  $n$  are Freundlich constants, referring to the adsorption capacity and intensity, respectively. Figure 6 exhibited the experimental equilibrium data, as well as the fitting results using Langmuir and Freundlich isotherm models. The parameters originating from the isotherm models were tabulated in Table 2. Clearly, both Langmuir and Freundlich isotherms provided a good correlation of the experimental equilibrium data since  $R^2 > 0.9$ . From Langmuir model, the theoretical maximum for metal uptake,  $q_{\max}$ , could be obtained even if it could not be experimentally reached. The  $q_{\max}$  value of Fe<sub>3</sub>O<sub>4</sub>/MPTMS/PAA nanoadsorbent for Pb(II) removal was 11.96 mg/g, comparable to other adsorbents that had been previously suggested efficient for Pb(II) removal from water (8.89 mg/g for bituminous coal [32]; 12.15-15.90 mg/g for sawdust [33]). According to the fitting results in Table 2, the  $K_F$  value of Fe<sub>3</sub>O<sub>4</sub>/MPTMS/PAA nanoadsorbent for Pb(II) removal was also comparable to those of other efficient Pb(II) adsorbents (11.49 for activated carbon [34]; 12.44 for sulphurised activated carbon [34]), indicating comparable adsorption capacity for a given adsorbate. In addition, the process of Pb(II) adsorption by Fe<sub>3</sub>O<sub>4</sub>/MPTMS/PAA nanoadsorbent was favorable according to the  $1/n$  value ( $0.1 < 1/n < 0.5$ , favorable;  $1/n > 2$ , unfavorable [35]).

From an economic perspective, it is important to regenerate the exhausted adsorbent for repeated use. As demonstrated in Figure 7, the Pb(II) removal percentage of Fe<sub>3</sub>O<sub>4</sub>/



**Figure 7.** Pb(II) removal percentage of Fe<sub>3</sub>O<sub>4</sub>/MPTMS/PAA in different cycles (Initial Pb(II) concentration=5 mg/l; pH value=8.0; nanoadsorbent dose=1.0 g/l; temperature=308 K; adsorption time=5 h).

MPTMS/PAA nanoadsorbent slightly decreased when the regenerated nanoadsorbent was used repeatedly for Pb(II) removal. This phenomenon was quite normal in the reusability of adsorbents [36,37]. Despite such decrease, the Pb(II) removal percentage of Fe<sub>3</sub>O<sub>4</sub>/MPTMS/PAA nanoadsorbent was still over 90 % in the fifth adsorption-desorption cycles. Therefore, it was concluded that Fe<sub>3</sub>O<sub>4</sub>/MPTMS/PAA nanoadsorbent could be repeatedly used without compromising its adsorption potency significantly, promising its cost effectiveness as a nanoadsorbent for Pb(II)-containing water.

## Conclusion

Polyacrylic acid could be grafted from Fe<sub>3</sub>O<sub>4</sub> nanoparticle surface *via* the bridging function of MPTMS silane coupling agent. The components of the nanocomposite played synergistic roles as a nanoadsorbent for Pb(II) removal from contaminated water. The polyacrylic acid shell was capable of capturing Pb(II) *via* spontaneous, chemical coordination, while the magnetic core enabled fast separation of the exhausted nanoadsorbent from the decontaminated water by using a magnet. Pb(II) adsorption on such magnetite-supported nanoadsorbent was fast and efficient. By chemical desorption, the nanoadsorbent could be regenerated and reused without significantly compromising its original capability. Based on these advantages, the Fe<sub>3</sub>O<sub>4</sub>/MPTMS/PAA nanoadsorbent designed herein could be a potential

**Table 2.** Fitting results of Pb(II) adsorption isotherm on Fe<sub>3</sub>O<sub>4</sub>/MPTMS/PAA nanoadsorbent by Langmuir and Freundlich models

Langmuir isotherm model				Freundlich isotherm model			
$q_{\max}$ (mg/g)	$b$ (l/mg)	ARE (%)	$R^2$	$K_F$ (l/g) <sup>1/n</sup>	1/n	ARE (%)	$R^2$
11.96	11.15	6.78	0.94	15.48	0.42	1.70	0.99



candidate for remediating Pb(II) contamination in water.

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