From Syngas Fermentation to Chain Elongation: the Role of Key Microorganisms and Multi-omics Analysis

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Received: 17 July 2023 / Accepted: 23 October 2023 / Published online: 11 November 2023 © The Author(s), under exclusive licence to Springer Science+Business Media, LLC, part of Springer Nature 2023

Abstract

Bioproduction of short chain carboxylic acids (SCCAs) and medium chain carboxylic acids (MCCAs) has emerged as an alternative strategy to upgrade low-value organic waste and reduce fossil fuels requirement. Using synthesis gas (syngas) to generate SCCAs and MCCAs by microbial communities would be an option to address part of the current energy challenge. Syngas fermentation offers a pathway for the sustainable synthesis of fuels and chemicals with advantages over catalytic syngas conversion. In the same way, chain elongation is an anaerobic microbial process driven by ethanol, carbohydrates, and SCCAs (e.g., acetate, lactate) to obtain high-value MCCAs (e.g., caproate, valerate). Because these technologies use organic wastes as feedstocks, mixed microbial communities are often considered biocatalysts. However, the management of microbial communities is the biggest bottleneck for efficient and simultaneous production of SCCAs and MCCAs. Understanding and steering these microbiomes is critical to optimize bioprocess performance. Therefore, this review discusses the metabolic pathways of both syngas fermentation and chain elongation, the influence of reactor parameters on the growth and metabolic activity of the key microorganisms is presented. The experimental strategies for simultaneous syngas fermentation and chain elongation processes towards full-scale applications.

Keywords Carboxylic acids · Gas bioconversion · Mixed cultures · Synthesis gas

Introduction

Use of oil and other fossil resources for transportation and service chemicals is deeply engrained today. However, their handling is unsustainable as the nature of fossil fuels relies

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on finite reserves, and herein they have negative environmental impacts, such as the release of carbon dioxide (CO_2) and other pollutants (e.g., sulfur and nitrogen oxides) during combustion [1]. Thus, we need alternative processes to produce energy and chemicals. Examples of cleaner and effective processes are those based on biotechnological applications such as anaerobic digestion, dark fermentation, bioethanol, and biodiesel production. Nonetheless, the transition to a sustainable energy supply is not straightforward and will take considerable time. Thus, short-term solutions can lessen the environmental impact of fossil fuels.

Waste biomass valorization is being developed to produce high-value fuels or chemicals to reduce fossil fuels global consumption. Anaerobic digestion and dark fermentation are well-documented technologies for valorizing biowastes through fermentation of easily degradable carbohydrate-rich substrates, such as corn starch and sugar cane [2]. Alternatively, fermentable sugars can be obtained through acid or



enzymatic hydrolysis of insoluble cellulosic biomass [3]. However, most biomass sources like straw or bagasse contain a great amount of material that cannot be efficiently converted by fermentative microorganisms. A feasible alternative is to gasify the organic biomass and use the synthesis gas (or syngas) as a feedstock to produce ethanol, acetate, and other valuable compounds.

Commonly, in biomass gasification, the lignocellulosic structure of biomass is thermally cracked into carbon monoxide (CO), hydrogen (H₂), and carbon dioxide (CO₂) as the main constituents of syngas and minor amounts of methane (CH₄), water steam, and trace gases [4–6]. The most common process to produce syngas is coal gasification, which uses steam and oxygen (from air) at high temperatures, a process that produces large amounts of CO₂. One more environmentally friendly way to create syngas, called methane dry reforming, involves getting two potent greenhouse gases to react, CH₄ (e.g., from natural gas) and CO₂. But that process is not widely used at industrial scales, partly because it requires temperatures of at least 700 °C to initiate the chemical reaction [7].

Traditionally, the conversion of syngas to organic molecules is executed by the Fischer-Tropsch metal catalysts synthesis. However, this process is highly exothermic, low energy efficient, and presents internal diffusion limitations [8]. Alternatively, syngas fermentation is a potential microbial pathway in which anaerobic microorganisms mediate the biocatalytic conversion of syngas components to various useful biochemicals and biofuels (e.g., H₂, ethanol, acetic acid). Through metabolic pathways, such as Wood-Ljungdahl or carboxydrotrophic acetogenesis, anaerobic bacteria utilize the CO and/or CO₂ as the carbon source and H₂ as the energy source [9]. Microbial communities capable of performing syngas fermentation can adapt to different proportions of the gas mixture and operate at mesophilic temperatures, and overall, this process could be a carbon-neutral process. Bacteria belonging to the genera Clostridium, Acetobacterium, Rhodospirillum, Rubrivivax, and Citrobacter have been widely reported as efficient syngas fermenters [10, 11]. However, inefficient gas-liquid mass transfer of the gases due to their low solubility, the low growth rate of fermenters, and the toxicity of CO are the most common challenges in syngas fermentation [12].

Interestingly, the acetate and ethanol obtained from the syngas fermentation can be further transformed by microorganisms in a process known as microbial chain elongation (CE), obtaining high value biochemicals classified in short chain carboxylic acids (SCCAs, C1 to C4), such as propionate (C3) and butyrate (C4), and medium chain carboxylic acids (MCCAs, C5 to C12), such as valerate (C5) and caproate (C6). Carboxylate CE occurs via cyclical pathways such as the reverse β -oxidation and analogous, for example, the Wood-Ljungdahl pathway coupled to acetyl-CoA reduction [13–15]. Among the microorganisms capable to elongate carboxylates are bacteria of the genera *Clostridium*, *Veillonella*, *Eubacterium*, *Megasphaera*, *Rhodospirillum*, and *Caproiciproducens* [16]. The production of MCCAs by single strain cultures has been intensively investigated with relevant results [15, 17, 18]. Nonetheless, mixed-culture fermentation could be more suitable to produce MCCAs from organic waste due to its resilience. However, the MCCA yields could be negatively affected by the competitive bioreactions existing in mixed-cultures, such as the acetoclastic methanogenesis or propionic production [19]. Therefore, understanding the cooperative and competitive relationships among key functional microorganisms is of great significance to further increase the production rate of MCCAs.

Although ethanol and acetate production from syngas is a feasible process, inducing CE in the same consortium can increase the value of the process. This is because MCCAs have a higher market value than other short-chain compounds. Therefore, this review is focused on key microorganisms to better understand syngas fermentation, CE, and the relationship of both processes. This review aims to (1) review the metabolic pathway of both syngas fermentation and CE; (2) summarize representative microbial communities for both syngas fermentation and CE; (3) analyze the simultaneous syngas fermentation and CE; and (4) discuss the use of advanced molecular tools to better understand both syngas fermentation and CE processes.

Basics of Syngas Fermentation

Syngas Generation

Obtaining syngas from biomass involves a series of thermal and chemical processes to convert the organic matter in biomass into a mixture of H₂ and CO, known as syngas. The primary steps in this process typically include biomass feedstock preparation, drying, pyrolysis, and gasification. First, the biomass feedstock, which can range from wood chips and agricultural residues to municipal solid waste, is collected and prepared by removing impurities and reducing its moisture content [7, 20]. Then, the prepared biomass is subjected to drying to reduce further moisture levels, which is essential for efficient conversion. Next, pyrolysis is employed to heat the biomass in the absence of oxygen, causing it to release volatile components in the form of gases, liquids, and char. Finally, gasification takes place, where the remaining char reacts with a controlled amount of oxygen or steam to generate syngas (containing H₂, CO, and CO₂, principally), which can be utilized for various applications, including power generation, fuel production, and chemical synthesis [21]. The composition and quality of the syngas can be adjusted

by optimizing the gasification process parameters and feedstock selection.

Syngas Fermentation

The main syngas fermenting microorganisms are chemolithoautotrophic bacteria that under strict anaerobic conditions convert carbon-based gas streams to SSCAs (acetate, principally) and alcohols [22]. These microorganisms are divided in two groups based on their metabolism. The first is the acetogenic bacteria, which require H₂ and CO₂ for acetate generation through the Wood-Ljungdahl pathway [23]. The second is carboxydotrophic microorganisms, which utilize the CO to produce CO₂ and H₂ by carboxydotrophic hydrogenesis, or by acetate generation through carboxydotrophic acetogenesis (Fig. 1) [4].

In the Wood-Ljungdahl pathway, microorganisms use CO and/or CO₂ as carbon source and H₂ as energy source, while the carboxydotrophic microorganisms utilize only CO as carbon and energy source. Then, in the acetogenesis stage, the intermediate acetyl-CoA is produced through reduction reactions. Finally, during solventogenesis, products such as ethanol (Eqs. (1) and (2)) or acetate (Eqs. (3) and (4)) are generated [26]. Since ethanol production generates less energy than acetate, microorganisms use solventogenesis as a passive step [6].

$$\begin{array}{l} 6~{\rm CO}+3~{\rm H_2O}\rightarrow{\rm C_2H_5OH}+4~{\rm CO_2}~~(\Delta {\rm G^\circ}=-217.4~{\rm kJ/mol}) \\ (1) \\ 6~{\rm H_2}+2~{\rm CO_2}\rightarrow{\rm C_2H_5OH}+3~{\rm H_2O}~(\Delta {\rm G^\circ}=-97.0~{\rm kJ/mol}) \\ (2) \\ 4~{\rm CO}+2~{\rm H_2O}\rightarrow{\rm CH_3COOH}+2~{\rm CO_2}~(\Delta {\rm G^\circ}=-154.6~{\rm kJ/mol}) \\ (3) \\ 4~{\rm H_2}+2~{\rm CO_2}\rightarrow{\rm CH_3COOH}+2~{\rm H_2O}~(\Delta {\rm G^\circ}=-74.3~{\rm kJ/mol}) \\ (4) \end{array}$$

217.4 tr I/mas

Microorganisms Performing Syngas Fermentation

Acetogenesis is a process conducted by various microorganisms, including bacteria, archaea, and even eukaryotes. Nevertheless, acetogenic bacteria have been documented as the predominant group during syngas fermentation, owing to their ability to adapt their metabolism based on environmental conditions and substrate availability [25]. Overall, the source of acetogenic bacteria can be obtained from mixed cultures or single strain cultures [27–29].

Single Strain Cultures

In single strain cultures syngas fermentation, the medium is sterilized before inoculation with one type of microorganism. The most commonly studied microorganisms in single



Fig. 1 Schematic representation of the principal metabolic pathways for syngas fermentation for acetate (CH₃COOH) production and ethanol. Adapted from Asimakopoulus et al. [24], and Phillips et al. [25]

strain cultures syngas fermentations are bacteria belonging to genera, such as *Clostridium*, *Alkalibaculum*, and *Butyrib*acterium [27]. The obtained products depend on the selected bacteria and experimental conditions; nevertheless, some commonly reported products from single strain culture fermentation include ethanol, butanol, hexanol, acetic acid, butyric acid, and hexanoic acid [25].

In this sense, one of the primary acetogens commonly documented was Clostridium ljungdahlii, an anaerobic strain isolated from an enrichment inoculated with chicken yard waste at an initial pH of 5.0 and incubated at 37 °C under an atmosphere of synthesis gas (CO, H₂, CO₂, CH₄, 73:15:10:2) [30]. This bacterium demonstrates the capacity to convert syngas and/or simple carbohydrates into ethanol through the Wood-Ljungdahl pathway [31].

From the same genus, C. autoethanogenum also can transform syngas into ethanol and acetate. For example, Xu et al. [32] conducted batch experiments to investigate the bioconversion of CO and syngas by C. autoethanogenum. Their study reported a maximum ethanol concentration of 75 mM when 100% CO was used as the substrate. In contrast, when biomass-generated syngas was employed (with a composition of 36.2% CO, 23.0% H₂, 15.4% CO₂, and 11.3% N₂), the ethanol production was only 5.4 mM. This lower ethanol yield may be attributed to the presence of O_2 and C_2H_2 . Other strains that can metabolize CO to ethanol, butanol, or even hexanol are Butyribacterium *methylotrophicum* and *Clostridium* carboxidivorans [25]. Overall, in single culture strains, the productivity of the culture depends on the type of microorganism, gas mixture, medium composition, and fermentation conditions (reactor type, temperature, pH, pressure) [27]. However, most of the metabolites produced by single strain cultures contain only two carbons, and they are characterized by low cellular density, limited substrate utilization, susceptibility to contamination, lack of robustness, high operational costs, and strict growth conditions [6].

Mixed Cultures

The inoculum for mixed cultures can originate from wastewater anaerobic sludge or similar [22, 33]. Compared with single strain cultures, mixed cultures are robust systems, capable of metabolizing different syngas mixtures, and more tolerant to environmental stress and changes [4, 6, 26, 34]. Table 1 includes studies of mixed cultures for syngas fermentation. Considering that H₂ and CO₂ present low water solubility (Henry's constants of 7.7×10^{-6} and 3.4×10^{-4} mol/m³ Pa, respectively), mass transfer represents the main bottleneck in syngas fermentation [40]. Additionally, autotrophic bacteria are slow growers with duplication times of 15 to 21 h in the case of H₂/CO₂/CO fermentation by *Clostridium* genus [20]. However, using biofilms for syngas fermentation overcomes the problems mentioned before. For instance, the fixed biomass decouples the hydraulic retention time from the cellular retention time, allowing slow-growing bacteria to develop [24]. Moreover, using a biofilm attached to a hollow fiber membrane enhances the delivery of syngas to the microbiome, and thus improves fermentation performance [6, 40].

In 2018, Liu et al. [41] investigated the effects of pH and temperature on the conversion efficiency, product, and microbial community composition during batch syngas

Inoculum source	Reactor configuration	Principal microorganisms reported	Substrate	Main products	Reference
Mesophilic anaerobic digester	Hollow-fiber membrane biofilm reactor	Clostridium, Thermoan- aerobacterium	H ₂ , 60% CO, 40%	Acetate, 70 mM Butyrate, 14.7 mM Caproate, 7.7 mM Caprylate, 4.3 mM	[35]
Mesophilic methane production reactor	Hollow-fiber membrane biofilm reactor	Clostridium ljungdahlii, Clostridium kluyveri	H ₂ , 60% CO ₂ , 40%	Acetate, 123.2 mM Butyrate, 20.4 mM Caproate, 8.6 mM Caprylate, 3.5 mM	[36]
Wastewater activated sludge	Continuous stirred tank reactor	Clostridia, Desulfitispora	H ₂ , 40% CO ₂ , 20% CO, 40% Wastewater activated sludge	Acetate, 70.4 mM Propionate, 3.7 mM Iso-valerate, 175 mM	[37]
Acetogens enriched sludge	Suspended biomass batch reactor	Clostridium, Eubacte- rium, Methylophilus, Nannocystis	CO ₂ , 1.6 mM Glucose, 5.6 mM	Acetate, 5.5 mM Ethanol, 14 mM	[38]
Enriched brewery sludge	Suspended biomass batch reactor	Acetobacterium, Desul- fovibrio	H ₂ , 80% CO ₂ , 20%	Acetate, 76.1 mM	[34]
Wastewater treatment anaerobic sludge	Batch reactor coupled to microbial electrosyn- thesis	Actinomycetales, Xanthomonadaceae, Tissierellaceae	H ₂ , 15% CO, 15% CO ₂ , 50% N ₂ , 20%	Acetate, 262 mM	[9]
Anaerobic granular sludge	Continuously gas-fed stirred tank bioreactor	Not reported	CO, 100%	Acetate, 103.2 mM Butyrate, 13.6 mM Caproate, 3.4 mM	[39]

Tab

fermentation. The study reached acetate and ethanol concentrations up to 56.6 mM and 67.4 mM, both at pH 9 under mesophilic conditions with a high relative abundance of the genera Clostridium and Acetobacterium, and reporting other several acetogens. Alternatively, the use of acetogensenriched sludge as inoculum improved the substrate utilization rate and acetate percentage in SCCAs [33]. In such batch experiments, the acetate yield increased by 1.77 times with CO_2 sparge in the headspace of the reactor; also, the genera Clostridium, Eubacterium, Methylophilus, and Nannocystis were detected in the culture. Moreover, the addition of sulfate in syngas mixed cultures was explored in batch experiments. In presence of 0.9 g sulfate/L, the maximum acetate concentration achieved was 75 mM at a H₂ feeding of 21.4 mM/d. In such study, Acetobacterium and Desulfovibrio were the dominant microorganisms in the consortia, suggesting co-metabolism between acetogens and sulfate-reducing bacteria [34]. Although mixed cultures have shown promising results, the product yield and specificity compared to single strain cultures remain relatively low [27]. Therefore, it is imperative to dedicate research efforts to selecting, managing, and controlling of mixed cultures to improve syngas fermentation.

Basics of Production of Short and Medium Chain Organic Acids

In the anaerobic digestion processes, mixed microbial communities can turn organic matter into H_2 , CO_2 , and SCCAs. The SCCAs are carboxylates of 1 to 4 carbon atoms (C1–C4) with relativity low market value. Moreover, the SCCAs are completely miscible in the liquid phase of fermentation, making the extraction processes expensive and complex [42]. SCCAs have also been used as a substrate for methane generation in the same fermenter of anaerobic digestion; nevertheless, methane has low added value [43].

Recently, CE has emerged as a technology capable of extending SCCAs carbon structure to MCCAs under anaerobic conditions [44]. Furthermore, CE is an efficient fermentation with MCCAs selectivity above 80%. MCCAs are less soluble than their precursors because they contained from 5 to 12 carbon atoms in their structure. Thus, MCCAs high-energy content and simpler extraction make them costeffective bioproducts that are employed in fragrances, rubbers, pharmaceuticals, food additives, and antimicrobials [45, 46]. Additionally, among MCCAs generated by CE, caproate (C6) presents a higher efficiency of conversion and an economic value of 2000 to 3000 USD/ton [47].

Two circular reactions are responsible for the microbial CE: the fatty acid biosynthesis and the reverse β -oxidation pathway (Fig. 2). The reverse β -oxidation is the most widely studied pathway for CE, where the overall process adds an



Fig. 2 Schematic representation of the reverse β -oxidation (RBO) pathway and fatty acid biosynthesis (FAB) pathway for chain elongation. Adapted from Wu et al. [48] and Wang et al. [49]

acetyl-CoA molecule to a SCCA electron acceptor as shown in Fig. 2. The first required environmental condition is the presence of energy-rich reduced compounds (e.g., ethanol, methanol, lactate, H₂) that oxidizes to acetyl-CoA by NAD⁺ and the reduction of ferredoxin by NADH [50]. Furthermore, and before the fatty acid biosynthesis pathway starts, the acetyl-CoA converts to malonyl-ACP by spending 1 ATP molecule and forming malonyl-ACP. Once the fatty acid biosynthesis cycle begins, the process is like the reverse β -oxidation and is catalyzed by a series of analogous reductases (Fig. 2).

In both cases, SCCAs are reduced by an electron donor, commonly ethanol or even H_2 , and two carbons are added to the SCCAs per cycle [48]. For instance, acetate (C2) elongates to butyrate (C4) and then to caproate (C6), while propionate (C3) elongates to valerate (C5) and to heptoic acid (C7) [13]. Generally, a high H_2 partial pressure or a reductive environment is required to prevent oxidation of the generated MCCAs [43]. The additional step before fatty acid biosynthesis is longer and less efficient than the reverse β -oxidation pathway [48]. However, CE carried out by a mixed microbial community made fatty acid biosynthesis more active than reverse β -oxidation [48].

Microorganisms Performing Chain Elongation

CE can occur by single strain cultures, co-culture, or mixed culture, where wild-type strains from the genera *Clostrid-ium*, *Caproiciproducens*, *Megasphaera*, *Eubacterium*, and *Ruminococcaceae* have been isolated and characterized [49]. Specifically, *Clostridium kluyveri* is the most accepted model microorganism that carries out CE from ethanol and acetate through the reverse β -oxidation pathway [51]. Furthermore, *Eubacterium pyruvativorans* is an analogous model whose metabolic strategy resembles C. *kluyveri* [52].

Single Strain Cultures

San-Valero et al. [53] reported the influence of electron acceptors on caproate production by *C. kluyveri*, obtaining a significant increase in caproate concentration when adding a mixture of acetate/butyrate and ethanol as the electron donor. Similarly, a high concentration of caproate (C6) has been achieved by the strain CPB6 of the family *Ruminococcaceae* with lactate as an electron donor [54]. In pure anaerobic culture, *Megasphaera elsdenii* produced a mixture of carboxylates from C2 to C6, using carbohydrates as substrate and lactate or butyrate as electron acceptors. Additionally, it has been reported that *M. elsdenii* can produce until C7-C8 MCCAs in presence of fructose and C2-C4 SCCAs [55]. Strains for the genus *Caproiciproducens* have been isolated from mixed cultures of CE and can convert

different types of saccharides to acetate, butyrate, caproate, and H_2/CO_2 [56, 57].

Strain Co-cultures

Strain co-cultures are designed to take advantage of the interactions between two strains without other microorganisms that could negatively impact the performance of the process. In 2016, Diender et al. [58] reported the establishment of C. autoethanogenum and C. kluyveri co-culture, capable of converting CO and syngas to a mixture of butyrate (8.5 mM/d) and caproate (2.6 mM/d) and their respective alcohols [58]. In the same study, the addition of acetate stimulated the production rates. Similarly, Fernández-Blanco et al. [15] studied the optimal operational conditions and the MCCAs and alcohols resulting from a co-culture of C. aceticum and C. kluyveri in fed syngas bioreactors with ethanol as an exogenous electron agent. This work showed maximum concentrations of butyrate and caproate of 80 and 70.6 mM, respectively, while considerable amounts of butanol were produced from the SCCAs reduction by C. aceticum.

Mixed Cultures

Mixed culture fermentation offers an advantage in CE because its high microbial diversity improves the process stability and resilience under changing conditions. Also, the process does not require sterile conditions, making it suitable for organic waste or gas utilization as substrates [51]. Table 2 comprises the main reports related to CE by mixed cultures.

In 2015, Weimer et al. [66] employed a ruminal mixed culture that was bioaugmented with a rumen-derived strain of C. kluyveri for cellulosic biomass fermentation. In presence of ethanol as an electron donor, the major generated MCCAs included valerate (C5) and caproate (C6) over a 48-72-h time period in batch reactors, with a caproate concentration of 52.5 mM. In the same way, Leng et al. [62] used a mixed microbial community in a semi-continuous reactor fed with a stoichiometric ratio of 4:3:1 of glycerolethanol-acetate for CE. The study reached a caproate production of 2.95 mM C/d where the fermentation and CE were mainly facilitated by a microbial community of Eubacterium limosum, C. kluyveri, and Massilibacterium senega*lese* [62]. For the full conversion of butyrate from food waste fermentation, the liquid phase of a mixed culture reactor was recycled as previously reported [44]. This work reported the enhanced production by 4.1 times of MCCAs by elongating butyrate to caproate and valerate to heptanoate, with a high abundance of the strain Clostridium sensu stricto 12.

Mixed cultures can include syngas fermenting bacteria, which use CO_2 and CO as a carbon source and H_2 as an electron donor for acetate generation. Then, the acetate is

Table 2 Studies for chain elongation c	arried out by mixed microbial commun	uities			
Inoculum source	Reactor configuration	Principal microorganisms reported	Substrate	Main products	Reference
Mesophilic methane production reactor	Hollow-fiber membrane biofilm reactor	Clostridium ljungdahlii, Clostridium kluyveri	H ₂ , 60% CO, 40%	Acetate, 123.2 mM Butyrate, 20.4 mM Caproate, 8.6 mM Caprylate, 3.5 mM	[36]
Wastewater treatment anaerobic sludge	Up-flow blanket filter reactor	Clostridium, Bacteroides, Alkaliphi- lus, Petrotoga, Bacillus, Parabac- teroides	Ethanol, 60 mM Acetate, 20 mM	Butyrate, 80 mM Caproate, 26.5 mM	[51]
Wastewater treatment anaerobic sludge	Suspended biomass batch reactor	Not reported	Ethanol, acetate, 300 mM total carbon	Caproate, 25.8 mM	[59]
Pond sediments + wastewater treat- ment anaerobic sludge	Biofilm bioelectrochemical reactor	Not reported	CO ₂ , 100%	Acetate, 163.1 mM/d Butyrate, 36.31 mM/d Caproate, 7.74 mM/d	[09]
Acclimatized anaerobic sludge	Suspended biomass batch reactor	Clostridium sensu stricto 12, Protein- iphilum	Sewage sludge, 8% TS	Caproate, 43.4 mM	[61]
Wastewater treatment anaerobic sludge	Suspended biomass batch reactor	Clostridium, Oscillibacter, Lepto- linea, Exilispira	Ethanol, synthetic alkaline fermenta- tion liquor	Caproate, 7.7 mM Heptanoate, 3.2 mM Caprylate, 10 mM	[48]
Sewage treatment anaerobic sludge	Suspended biomass batch reactor	Eubacterium limosum, Clostridium kluyveri, Massilibacterium senega- lense	Glycerol, ethanol, acetate, 4:3:1 ratio	Caproate, 2.9 mM/d	[62]
Sheep rumen + thermophilic anaero- bic sludge	Anaerobic sequencing batch reactor	Caproiciproducens, Ruminococcus, Oscilibacter, Methanobacterium	Corn beer	Caproate, 200 mM C Caprylate, 420 mM C	[63]
Lab-scale chain elongation bioreactor	Suspended biomass batch reactor	Clostridium sensu stricto 12, Capro- iciproducens, Oscillibacter	Lactate, 30 g/L Acetate, 6 g/L	Caproate, 37 mM Butyrate, 5.6 mM	[64]
Wasted activated sludge	Membrane biofilm reactor	Acetobacterium, Bacteroidales, Rhodocyclaceae, Alcaligenaceae, Thermoanaerobacteriales, Erysip- elotrichaceae	NaHCO ₃ , 64 mM H ₂ , 1.15 atm	Acetate, 1.6 mM Ethanol, 2.1 mM Propionate, 1.3 mM Butyrate, 3.5 mM Caproate, 2.5 mM Caproate, 1.7 mM	[40]
Primary sludge + waste activated sludge	Suspended biomass batch reactor	Caproiciproducens, Clostridium sensu stricto 1, Clostridium sensu stricto 7, Clostridium sensu stricto 12, Pseudoramibacter, Oscillibac- ter, Dechloromonas	Mixed wastewater sludge, ethanol	Caproate, 4.3 mM Heptanoate, 3.8 mM Caprylate, 7.4 mM	[65]

mM millimolar, mM C millimolar of total carbon

used as an electron acceptor by the CE microorganisms [49]. The first study that demonstrated the in situ production of MCCAs from H₂ and CO₂ in a hollow-fiber membrane biofilm reactor by mixed microbial culture achieved a caproate production rate of 31.4 mM C/d [36]. In the same report, the microbial community of the biofilm was dominated by C. *ljungdahlii* and *C. kluyveri*. Furthermore, Jourdin et al. [60] showed a biofilm-driven production of acetate, butyrate, and caproate from CO₂ and carbon-felt electrodes as the electron donor, with a caproate productivity of 8.2 mM/d. Recently, a membrane biofilm reactor with an inorganic carbon source and H₂ fed through hollow membranes was employed and achieved up to C8 MCCAs production (28.1 mM C/m²d). The biofilm microbial community presented the wellknown acetogen Acetobacterium and phylotypes related to CE microorganisms such as *Bacteroidales*, *Rhodocyclaceae*, Alcaligenaceae, Thermoanaerobacteriales, and Erysipelotrichaceae [40].

Syngas Fermentation to Chain Elongation: Perspectives from the Microbial Ecology of Mixed Communities

Syngas fermentation and CE presents a promising platform for biotechnological CO_2 and CO fixation and fermentation of rich-organic substrates, respectively. Therefore, the synergy of combining syngas fermentation and CE has been a topic in previous studies [5, 13]. The first approach is a twostage process (Fig. 3A), where syngas fermentation is the first stage and the second stage is a CE reactor fed with the effluent from the first reactor, preferably with high acetate and ethanol concentrations. The first reactor depends on carboxydotrophic and acetogenic bacteria, and the second reactor requires bacteria able to use ethanol and acetate. CE studies have used this strategy in which a single strain is used for the syngas fermentation stage (e.g., *C. carboxidivorans, C. ljungdahlii, C. autoethanogenum*), and *C. kluyveri* or a mixed culture is employed for the CE stage [67, 68].

Another approach consisted in the simultaneous combination of both processes when only syngas is fed (Fig. 3B). For example, Diender et al. [58] used a stable co-culture of C. autoethanogenum and C. kluyveri in culture bottles to convert syngas and CO ultimately to SCCAs and MCCAs. A similar synergy between a co-culture of C. aceticum and C. kluyveri was reported in a continuous bubbling reactor, where up to 79.4 mM butyrate and 68.9 mM caproate were obtained from a syngas mixture with 30% CO, 5% CO₂, 15% H₂, and 50% N₂ [15]. Interestingly and up to date, C. carboxidivorans and E. limosum are the only two strains reported to be able to produce caproate from syngas, and C. carboxidivorans is the only known strain able to synthetize hexanol from syngas [69]. When C. carboxidivorans was not detected in syngas-fed microbiota, it was supposed that caproate and/or caprylate production arose via a multispecies synergy with conventional CE intermediated by acetate (or butyrate) and ethanol from the Wood-Ljungdahl pathway [2].

Besides the above mentioned "syngas aided anaerobic fermentation," the use of organic electron donors such as



Fig. 3 Different strategies of syngas aided chain elongation (CE). A Two-stage process, **B** simultaneous syngas fermentation and CE, **C** syngas fermentation and CE aided to anaerobic digestion, and **D**

dark fermentation aided to simultaneous syngas fermentation and CE. Short (SCCAs) and medium chain (MCCAs) carboxylic acids

acetate, lactate, or ethanol can enable the production of MCCAs through microbial CE in anaerobic fermentation. For instance, the addition of 0.5 g/L of acetate improved the bioconversion of CO to ethanol and acetate in batch cultures of C. autoethanogenum [32]. However, and from a sustainable point of view, utilization of rich carbohydrates biomass is preferable to obtain such electron donors (Fig. 3C). One anaerobic fermentation option is the lactic acid fermentation. In this process, lactic acid bacteria in situ convert carbohydrates to lactate as electron donors that are subsequently consumed during CE. Simultaneously, utilizing H₂, CO₂, and occasionally CO in fermentation systems can facilitate the production of MCCAs through the generation of acetate, an electron acceptor in CE, and the generation of ethanol, serving as an electron donor for CE. Generally, the use of mixed cultures has reported productivities and concentrations of MCCAs comparable with those of single strain cultures of CE species and in a broader range of pH [5]. For example, Nzeteu et al. [70] suggested that a lactate-based CE community had synergy with hydrogenotrophic activity to produce about 130% more caproate (until 89.5 mM) in comparison with the H₂-free fermentation (35.2 mM). A similar synergy was recently reported by Wu et al. [71], where comparing with non-H₂-supplemented test, the lactatecarbon-flow used for MCCAs production was enhanced by 28.4% after H₂ supply, obtaining maximum caproate production of 47.3 mM.

The strategy depicted in Fig. 3D allows the incorporation of dark fermentation to CE. Dark fermentation is the anaerobic conversion of carbohydrate-rich organic matter into some SCCAs (e.g., acetate, butyrate, lactate), alcohols, H₂, and CO₂, principally [72]. Continuous dark fermentation reactors have reported suitable gas productivities until 54 L/L-d (55% H₂ and 45% CO₂) and average acetate, butyrate and lactate concentrations of 6, 11, and 10 g/L [73, 74]. The stimulation/presence of acetogens and lactic acid bacteria was one of the main results obtained in such investigations. Nevertheless, the use of biomass with high abundance and activity of acetogens for syngas fermentation has been poorly studied. And the combination of dark fermentation to syngas aided CE has not been reported until now.

Therefore, a foreseen way forward in the field is the development of a sequential system to produce CO_2 , H_2 , SCCAs, and MCCAs. The implementation of such system could consist of two reactors. In the first reactor, the dark fermentation process will be carried out with the production of H_2 , CO_2 , and SCCAs at organic loading rates where acetogenic bacteria are naturally present. In the second reactor, the gas fermentation will be performed using the H_2 and CO_2 produced in the first reactor and the selected and enriched autotrophic biomass from the first reactor as a source of inoculum. This second reactor is expected to produce acetate and ethanol without the fed of an organic substrate, as well as butyrate, valerate, caproate by the CE process.

Overall, the co-feeding strategy of syngas and degradable substrates can brand mixed cultures viable for syngasfermenting reactors. In other words, mixed microbial communities may outclass in syngas-aided CE. The use of mixed microbial communities can further add simplifications to the bioprocess of SCCAs and MCCAs production. It is known from anaerobic digestion and fermentation studies that microbial communities can operate steadily in non-sterile reactors, which can reduce operating and maintaining costs in comparison with single strain cultures [72, 75]. Besides, it is expected that mixed microbial communities can better handle the inhibitors and contaminants typically found in syngas (e.g., sulfur oxides, ethylene, acetylene) that may negatively affect the performance of the syngas fermenters [5]. This characteristic resilience to substrate quality and composition fluctuations has been decisive for the success of anaerobic digestion and wastewater treatment [72]. However, and to the best of our knowledge, studies focused on the robustness of mixed microbial communities with real syngas must be developed.

Omic-Sciences in Syngas Fermentation and Chain Elongation

To date, most studies have employed 16S rRNA gene Illumina sequencing to characterize CE and syngas fermentation microbiomes (Tables 1 and 2), which is a well-established technology but has important biases and limitations. For example, the sequencing data reported in each individual study may be affected by biases such as extraction protocol, primer choice, and sequencing approach. Also, a comprehensive and complete characterization of the microbial community structure can be hindered by the low sequencing depth of 16S rRNA sequencing. Therefore, omics-sciences stand out as excellent tools to complement and acquire information that cannot be obtained from 16S rRNA sequencing analysis. They are designed mostly at the universal detection of genes (metagenomics), mRNA (metatranscriptomics), proteins (metaproteomics), and metabolites (metabolomics) in a specific biologic sample in a non-targeted and non-biased way [76].

The advent of high-throughput sequencing technologies used in metagenomics and metatranscriptomics has made it possible to obtain datasets that are commensurate to the complexity of these microbial communities. Metagenomics is a new approach to study microorganisms obtained from a specific environment by functional gene screening or sequencing analysis. Metagenomics studies focus on microbial diversity, community structure, genetic and evolutionary relationships, and interactions and relationships with the environment [77]. Metatranscriptomic methods can be used to compare a biological response to different conditions or treatments or to assess physiological responses to external stimulation. Whole transcriptome sequencing is the most widely used method for studying RNA functions, exploring and analyzing the gene structure and function, and revealing intrinsic links between gene expression and biological phenomena [78], whereas metaproteomics involves characterization of the protein components present in the environmental microbial community at a specific time. It determines the protein complement that is post-transcriptionally regulated and translated. The community protein complement also includes the proteins that interact within and among a microbial community [79]. Finally, metabolomics is a comprehensive, qualitative, and quantitative study of all the small molecules in an organism. Metabolomic tools are being increasingly used to generate an unbiased global profile of metabolites in samples or to quantify with high sensitivity a small panel of metabolites. Metabolites are the result of the interaction of the system's genome with its environment and are not only the end product of gene expression but also form part of the regulatory system in an integrated manner [78].

In the literature, few metagenomics and metatranscriptomics studies report the microbial ecology of CE and syngas fermentation processes with mixed microbial communities. Agler et al. [80] conducted the first study of metagenomic analysis on mixed cultures to produce MCCAs using raw organic materials (yeast-fermentation beer). The metagenomic analysis suggested that more than 50% of all assigned reads were from *Clostridium* spp. (particularly C. kluyveri), and that these were highly correlated with caproate production. Also, they found that other genera, including Ethanoligenens, Bifidobacterium, and Desulfitobacterium, represented important pools of genes for hydrolysis and ethanol oxidation. Wu et al. [48] through a metagenomic analysis suggested that both the reverse β -oxidation and the fatty acid biosynthesis pathways contributed to the CE process in a system with waste activated sludge and alkaline fermentation liquor as a feedstock. Also, they estimated that the functional enzymes as well as the fatty acid biosynthesis and the reverse β -oxidation pathways were mainly associated with C. kluyveri, C. botulinum, and C. magnum as key species responsible for the CE process. This study also proposed that acetogenesis, via the Wood-Ljungdahl pathway, is another important bioprocess for inorganic carbon fixation. Similarly, Leng et al. [62] studied the co-production of propanediol and caproate in a 2 L mixed-cultured semicontinuous reactor. From the metagenomic analysis, the authors proposed that E. limosum is capable of converting glycerol to propanediol, ethanol and H₂, and redirecting the electron potential of H_2 into acetate via the Wood-Ljungdahl pathway, which is then used for caproate production. *C. kluyveri* worked synergistically with *E. limosum* by consuming ethanol and acetate for caproate production.

Han et al. [51] carried out a metagenomic analysis from a CE reactor inoculated with acclimated biogas microbiome reactor. Using the metagenomic assembly approach, they retrieved 91 draft genomes in total, 3 of which were nearly complete and were assigned to unknown strains of Methanolinea tarda, Bordetella avium, and Planctomycetaceae, which except for the methanogen M. tarda, were likely new-found active participators of CE in the mixed culture. Another relevant result in this investigation was that the microbial structure of the CE reactor was like the inoculum reactor although reactor performances differed. Therefore, a metatranscriptomic analysis was additionally performed. The RNA sequencing results demonstrated that the microbial structure was highly stable while their function was flexible. Additionally, the fatty acid biosynthesis pathway, rather than the reverse β -oxidation pathway for CE, was more active and pivotal [42]. Interestingly, the distribution of microbial abundance in the metagenomic and metatranscriptomic analysis was significantly different. For example, the *Clostridium* relative abundances varied from 0.0 to 6.2; however, the low genetic abundance exhibited much higher relative transcriptomic abundances, while methanogens were not assigned as the transcriptionally active genera. These results reveal that metagenome analysis at the shotgun level also had limitations to identify the reactor microbiome. Additionally, key genes with low abundance but high transcription might be ignored. Therefore, metatranscriptomic analysis is more recommended to identify microorganisms and their functional associations.

Wang et al. [44] carried out a metatranscriptomic study of Clostridium lactatifermentans for CE in batch reactors fed with glucose and lactose. Interestingly, they found that C. lactatifermentans showed robust growth on glucose but more active caproate synthesis on lactate. Comparative transcriptome revealed that the genes involved in the reverse β-oxidation for caproate synthesis and ATPase-dependent ATP generation were upregulated under lactate feeding, while several genes responsible for biomass synthesis were upregulated under glucose feeding. Thus, metatranscriptomics achieves an in-depth understanding of carbon and energy metabolism in single strain and/or mixed cultures for future genetic engineering to optimize microbial cell factory towards MCCAs production. To our knowledge, metaproteomic and metametabolomic analyses have not been used into the analysis of CE and syngas fermentation processes.

Overall, the information obtained via several omics is not only important to understand the ecology and function in microbiomes; nonetheless, will also become crucial to choose the right chain elongator microorganism. Some microbial species or genera may have faster growth rates or higher tolerances for substrates, making them more suitable as "biocatalysts" in a given process/application, or conversely, such features might need to be taken into consideration in the bioprocess design [2].

Research Gaps and Future Perspectives

The biotechnological processes involving syngas fermentation and CE with mixed cultures hold immense potential for biofuel production, chemical synthesis, and waste utilization. Nevertheless, and as highlighted in previous sections and resumed in Fig. 4, several research gaps and challenges in these domains require attention to unlock their full potential. The main research gaps relate on the scarce understanding of the selection and interaction of microorganisms within mixed cultures. Overall, the microbial communities in open or mixed-culture fermentation are inherently more complex than single strain cultures. Despite the identification of single strains, the specific roles of satellite communities within the mixed-culture fermentation system still need clarified. The use of high-throughput sequencing technologies is imperative to gain a deeper insight into the criteria for selecting microbial cultures and to elucidate how various consortia perform under diverse conditions. This understanding is crucial for elucidating their cooperative interactions and the competition among microbial groups for substrates. Similarly, ensuring the stability of mixed cultures over prolonged fermentation periods is of paramount relevance for their industrial applicability. Future research actions should prioritize enhancing these cultures resilience, robustness, and durability while devising strategies for effective recovery from disturbances or upsets.

Reactor and process design for coupling syngas fermentation and CE are critical to advance these biotechnological processes. Effective mass transfer of syngas components and products within the reactor remains challenging. Research should focus on investigating reactor designs that facilitate efficient gas-liquid-solid interactions, optimizing the conversion of syngas into desired products while minimizing waste. Interestingly, current research often needs more integrated reactor systems that can simultaneously support both syngas fermentation and CE processes. Therefore, future research should focus on (i) the design of multi-compartment reactors that can house distinct microbial consortia optimized for syngas fermentation and CE, enabling enhanced process control; (ii) the integration of reactor design with downstream processing techniques, such as product recovery and separation, to create a holistic and efficient production chain; and (iii) the transition from batch to continuous reactor operation to improve productivity and stability. Continuous processes can minimize downtime and enhance product consistency.

Finally, more investigation is needed on utilizing waste streams, such as agricultural residues and industrial byproducts, as supplemental feedstocks for syngas fermentation, and CE, promoting sustainability and circular economy principles. Furthermore, the operational expenses associated with the extraction equipment pose a significant challenge to be addressed in full-scale applications. These costs encompass factors such as the price of the extractant and electricity consumption. Subsequent research efforts may focus on identifying cost-effective extractants and advancing the development of novel membrane materials. This pursuit aims to minimize operational investments and enhance product selectivity.

Fig. 4 Integrating syngas fermentation and chain elongation with mixed cultures: a way for the future



Conclusions

Emerging syngas fermentation and CE process for biofuel production has both environmental and sustainable advantages. In this review, we summarized recent advances when using mixed cultures for syngas fermentation and MCCAs production via CE process. Overall, the use of mixed microbial communities offers advantages over single strain cultures because the microbial diversity in mixed cultures improves the process stability and resilience under changing conditions. However, some negative reactions such as methanogenesis also compete for substrates with the CE.

In addition, the metabolic pathways of syngas fermentation and CE processes has been investigated by various molecular biology technologies. In general, for CE the reverse β -oxidation is widely recognized as the main metabolic pathway, but current studies revealed a new potential CE process, e.g., the fatty acid biosynthesis process. Future studies should aim at improving fatty acid biosynthesis pathway to produce MCCAs. Although the syngas fermentation aimed CE process from organic wastes to obtain caproate and/or long-chain acids is attractive, its physiological understanding is insufficient, and further omics studies are required for stable operation or trouble shooting bioreactors. Therefore, future work should build on the expanding molecular information from mixed cultures and characterization efforts to eventually unravel the flows of substrates and products within microbial community members.

Acknowledgements E. Razo-Flores acknowledges the "Cátedra Rodolfo Quintero-Ramírez" granted by the Universidad Autónoma Metropolitana-Cuajimalpa. P. Núñez-Valenzuela is thankful for the postgraduate scholarship provided by CONAHCYT.

Author Contribution J.J.M.-R.: conceptualization, investigation, data curation, formal analysis, writing-original draft. P.N.-V.: investigation, data curation, formal analysis, writing-original draft. A.O.-V.: conceptualization, writing-review and editing. M.M.-I.: writing-review and editing. S.R.: writing-review and editing. E.R.-F.: conceptualization, writing-review and editing, supervision, funding acquisition.

Funding This investigation was financially supported by SEP-CONA-CYT project A1-S-37174.

Data Availability All data generated or analysed during this study are included in this published article.

Declarations

Competing Interests The authors have no competing interests to declare that are relevant to the content of this article.

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