ORIGINAL ARTICLE



Screening of Yeasts for Selection of Potential Strains and Their Utilization for In Situ Microbial Detoxification (ISMD) of Sugarcane Bagasse Hemicellulosic Hydrolysate

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Abstract Many toxic compounds are produced and released in the hemicellulosic hydrolyzates during the acid pretreatment step, which are required for the disruption of the lignocelluloses matrix and sugars release. The conventional methods of detoxification i.e. overliming, activated charcoal, ion exchange or even membrane-based separations have the limitations in removal of these toxic inhibitors in fermentation process. Hence, it is imperative to explore biological methods to overcome the inhibitors by minimizing the filtration steps, sugar loss and chemical additions. In the present study we screened sixty-four strains of yeasts to select potential strains for detoxification of furfural, acetic acid, ferulic acid, 5-hydroxymethyl furfural (5-HMF) as carbon and energy source. Among these strains Pichia occidentalis M1, Y1'a, Y1'b and Y3' showed a significant decrease in the toxic compounds but we selected two best yeast strains i.e. P. occidentalis Y1'a and P. occidentalis M1 for the further experiments with an aim to remove the fermentation inhibitors. The yeasts P. occidentalis Y1'a and P. occidentalis M1 were grown aerobically in sugarcane bagasse hemicellulose hydrolysate under

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submerged cultivation. For each yeast, a 2^2 full factorial design was performed considering the variables—pH (4.0 or 5.0) and agitation rate (100 or 300 rpm), and the percentage removal of HMF, furfural, acetic acid and phenols from hemicellulosic hydrolysates were responsive variables. After 96 h of biological treatment, *P. occidentalis* M1 and *P. occidentalis* Y1'a showed 42.89 and 46.04 % cumulative removal of inhibitors, respectively.

Keywords Microbial detoxification · Sugarcane bagasse · Dilute acid hydrolysis · Inhibitors

Introduction

Lignocellulosic materials are mainly composed of cellulose, hemicellulose and lignin [1, 2]. The carbohydrate fraction of lignocellulosic materials, if harnessed judiciously, can serve as an excellent building block for the production of renewable ethanol and other commodity chemicals via microbial fermentation. Production of fuel ethanol from lignocellulosic biomass so called secondgeneration (2G) ethanol is an important necessity due to the heavy usage of gasoline worldwide and environmental pollution. The 2G ethanol is completely renewable and is able to reduce atmospheric pollution due to the lower release of carbon dioxide, while offering several geo-political benefits [3]. Sugarcane bagasse (SB), a fibrous product after extraction of juice is an excellent carbohydrate source (~ 67 %) for 2G ethanol production [3].

Conventional process of ethanol production from lignocellulose biomass comprises of four major steps: pretreatment (responsible for the disruption of lignocellulosic matrix), enzymatic hydrolysis (leading to depolymerization of cellulose into glucose by the action of cellulolytic enzymes), the fermentation (which is the conversion of sugars to ethanol, generally carried out by yeast); distillation, rectification and dehydration steps (for separation and purification of the final product) [4]. The pretreatment of SB is an inevitable step to increase the accessibility of carbohydrate fraction towards enzymatic action [3]. Dilute acid hydrolysis of lignocellulosics is a fast and effective process but, it has bottlenecks, such as, by-product formation and non-selectivity [5]. Dilute sulfuric acid pretreatment precisely acts on hemicellulose releasing hemicellulosic monomers and releasing some undesired compounds like furans (5-hydroxymethylfurfural and hydroxymethylfurfural), phenolics, weak acids, and others. The dilute acid pretreatment is conducted at high temperature and pressure, and the reaction time takes for seconds or minutes [3]. Sulfuric acid (H₂SO₄) is mostly used catalyst, but other weak acids, such as: hydrochloric acid (HCl) and nitric acid (HNO₃) have also been used for the hemicellulose removal from variety of lignocellulosic materials [6].

Inhibitory compounds generated in lignocellulosic bioethanol production are main hurdle faced during the hydrolysis process. One of the main challenges associated with 2G ethanol production is to overcome the cumulative negative effect of cell wall derived inhibitors on the fermenting microorganisms during fermentation reactions [7-11]. Inhibitory compounds like acids, furans and phenolic compounds interferes the fermenting microorganisms and complete process by reducing ethanol yield and productivity during fermentation. These inhibitors negatively affect the performance of microorganisms in the fermentation process [5]. Concentration of these inhibitors produced depends on process conditions and raw materials used for hydrolysis. Furans and phenol monomers produced during hydrolysis of lignin are also major cofactors which inhibit or slow down the hydrolysis process. Generally, furans and phenolic compounds constrain growth and rate of ethanol production. Therefore, it is essential, to remove these inhibitors prior to fermentation in order to obtain the desired ethanol or any other metabolite. Detoxification process can be categorized into physical, chemical and biological methods. Biological methods certainly have unique advantages. Further, to consolidate the detoxification and ethanol or xylitol fermentation so called simultaneous detoxification and fermentation (SDF) is also possible by the appropriate use of microorganisms in a single vessel [11].

This study was aimed to develop a biological detoxification method for sugarcane bagasse hemicellulosic hydrolysates. For this, the yeasts *Pichia occidentalis* Y1'a and *P. occidentalis* M1 [12] were grown in concentrated sugarcane bagasse hemicellulosic hydrolysate. For both the strains of yeast, a 2^2 full factorial design was carried out. The variables, pH (4.0 or 5.0) and agitation rate (100 rpm or 300 rpm), were evaluated and the percentage removal of HMF, furfural, acetic acid and phenols after 96-h of biological treatment were responsive variables.

Materials and Methods

Yeast Screening

Sixty-four strains of yeasts were screened to search for potential strains for detoxification of furfural, acetic acid, ferulic acid, HMF as carbon and energy source. Of these, only two strains of *Picchia occidentalis* were selected for detoxification (ISMD) of sugarcane bagasse hemicellulosic hydrolysate.

The growth medium for yeasts was composed of 6.7 g/l of yeast nitrogen base (YNB), 18.0 g/l agar and with different concentrations of individual (furfural, 0.2820 g/l; 5-HMF, 0.0149 g/l; total phenolics, 3.13 g/l) and combined toxic compounds (furfural, 0.2820 g/l + 5-HMF, 0.0149 g/l + total phenolics, 3.13 g/l). The medium containing the toxic compounds (hydroxymethyl furfural, furfural, acetic acid, ferulic acid and syringaldehyde) was prepared for the screening of the yeasts.

Preparation of Sugarcane Bagasse Hemicellulosic Hydrolysates

The sugarcane bagasse was hydrolyzed in vertical rotary drum reactor of 50 L capacity at 121 °C for 10 min with H_2SO_4 (98 %) at 1:10 solid/liquid ratio (100 mg of H_2SO_4 g⁻¹ dry sugarcane bagasse). The hydrolyzed hemicellulose was recovered after filtration and subsequently concentrated at 70 °C under vacuum to obtain a fivefold increase in the xylose content.

The pH of the hemicellulosic hydrolysate was adjusted with 2 M NaOH according to the values of design experiment. It was filtered and subsequently autoclaved at 110 °C for 15 min. Then, hydrolysate was centrifuged under aseptic conditions at $2600 \times g$ for 20 min to remove the suspended solids, in order to use the hydrolysates for biological detoxification experiments.

Inoculum Preparation

Pichia occidentalis Y1'a (Genbank accession number: KP033405) and *P. occidentalis* M1 (Genbank accession number: KP033404) were obtained from stock strains of Social Insects Study Center, Rio Claro Biosciences Institute, São Paulo State University (UNESP—Universidade Estadual Paulista, Rio Claro, São Paulo State, Brazil). Both the strains were identified according to the standard

methods described by Melo et al. [8]. All the strains were maintained at 5 °C in 2 % Sabouraud Agar Medium. The medium used for inoculum preparation contained 10 g/l of yeast extract, 20 g/l of peptone and 20 g/l of glucose. For inoculum preparation, loopful of cultures were transferred to 250 ml Erlenmeyer flasks containing 100 ml of YPX medium (10.0 g/l yeast extract, 20.0 g/l peptone, 30.0 g/l xylose, pH 6.0). The flasks were incubated at 30 °C, 200 rpm for 24 h. After 24 h of incubation, the cells were recovered by centrifugation $(2000 \times g, 20 \text{ min})$ at room temperature, washed, centrifuged again and suspended in sterile distilled water to obtain an initial concentration of 0.5 g/l. Erlenmeyer flasks (500 ml) each containing 200 ml of medium closed with cotton plugs were incubated in rotary shaker (New Brunswick Scientific, Edison, NJ, USA) at 200 rpm for 24 h at 30 °C.

Medium and Detoxification Conditions

The concentrated sugarcane bagasse hemicellulosic hydrolysate was supplemented with 6.7 g/l of YNB (Sigma-Aldrich, USA). Fifty milliliter of medium was taken in Erlenmeyer flasks (125 ml capacity), and inoculated with 0.5 g/l of cells. The biological detoxification was conducted at different agitation at 30 °C for 96 h on rotary shaker (New Brunswick Scientific—Edison, NJ, USA). Assays were performed in triplicates. Aliquots of 50 ml samples were taken at times 0, 24, 48, 72 and 96 h for the quantification of D-glucose, D-xylose, D-arabinose, HMF, furfural, phenols and acetic acid, and pH and cell growth determination.

Analytical Methods

The concentrations of glucose, xylose, arabinose and acetic acid were determined by HPLC with a refraction index detector (Waters 410; Milford, MA, USA). The samples were diluted in a ratio of 1:10 and filtered through a Sep Pak C18 filter. Subsequently, samples were injected into the chromatograph, using the following conditions: column BIO-RAD Aminex HPX-87H $(7.8 \times 300 \text{ mm})$ (Bio-Rad, Hecules, CA, USA), a temperature of 45 °C, eluent: 0.005 M sulfuric acid, flow 0.6 ml/min in a sample volume of 20 µL. Furfural and 5-HMF was also determined by HPLC with UV detector (Waters 2487/USA). The samples were filtered through Schleicher and Schuell membrane, 0.45 µm and subsequently injected into the chromatograph using the following conditions: column Eclipse XDB-C18 5 µm $(4.6 \times 150 \text{ mm})$, a temperature of 25 °C, eluent: acetonitrile and water at a ratio of 1:8 with 1 % acetic acid and phosphoric acid, flow 0.9 ml/min, sample volume of 25 µl. Total concentration of phenolics was determined by method described by Gouveia et al. [13]. Cell growth was determined
 Table 1 Composition of sugarcane bagasse hemicellulosic hydrolysates after acid hydrolysis and concentrated fivefold by vacuum evaporation

Compounds	Hemicellulose hydrolysates before concentration (g/l)	Hemicellulose hydrolyzates After concentration (g/l)
Xylose	14.19	69.65
Glucose	1.52	7.32
Arabinose	1.43	7.08
Acetic acid	0.85	3.15
Furfural	0.2820	0.1680
5-HMF	0.0149	0.0378
Phenolics	3.13	8.87
pH	0.99	0.24

by measuring absorbance at 600 nm using a Bioespectro SP-220 spectrophotometer. Cell concentration was calculated based on the relationship of optical density and cell dry weight through a calibration curve. Statistical analysis of the experiments was performed using Statistica 8.

Results

Preparation of Sugarcane Bagasse Hemicellulosic Hydrolysates

After hydrolysis, hemicellulose hydrolysate was concentrated by vacuum concentration process to increase the concentration of sugar in hydrolysate. Table 1 shows the composition of hemicellulose hydrolysates before and after the vacuum concentration process. Xylose was the major



Fig. 1 Yeasts growth tested in positive control (glucose as carbon source), after 21 days of incubation at 25 $^{\circ}{\rm C}$

	Strain	Species	Substrate where	Rest	ılts										
			strain was obtained	Ace acid	tic	Syrir	ıgaldehyde	Ferulic acid		Furfural		5-hydroxymet	hylfurfural	Com of comp	ounds
				1 g/L	5 g/L	0.2 g/L	0.7 g/L	$\frac{8 \times 10^{-2} 0}{\text{g/L}}$	L 3	1.8×10^{-3} g/L	1.6×10^{-2} g/L	4.0×10^{-3} g/L	$\begin{array}{l} 2.0 \times \ 10^{-2} \\ \mathrm{g/L} \end{array}$	1 ^a	2 ^b
1	PBM 63	Candida metapsilosis ATCC 96144	Atta laevigata	+	I	I	I			I	I	I	I	+	I
7	PBM 52	Candida guilliermondii TJY14a	Atta laevigata	+	I	I	Ι			I	I	I	I	+	Ι
б	TO 100	Aureobasidium pullulans	Acromyrmex balzani	Ι	Ι	Ι	Ι	I		I	I	I	I	Ι	Ι
4	TO 182	Aureobasidium sp.	Acromyrmex balzani	Ι	Ι	Ι	Ι			1	Ι	Ι	Ι	Ι	I
S	TO 178	Aureobasidium pullulans	Acromyrmex balzani	Ι	Ι	Ι	Ι			I	Ι	Ι	Ι	Ι	I
9	TO 047	Cryptococcus laurentii	Acromyrmex balzani	+	Ι	Ι	I			1	I	Ι	Ι	Ι	Ι
٢	PBM 44	Pichia caribbica	Atta laevigata	+	Ι	Ι	I			1	I	Ι	I	+	I
8	PBM 64	Candida parapsilopsis	Atta laevigata	+	Ι	Ι	Ι			I	Ι	Ι	Ι	+	I
6	PBM 30	Pichia burtonii	Atta laevigata	+	Ι	Ι	I			1	I	Ι	Ι	+	Ι
10	BR3- 3BY	Candida silvae	Vriesia sp.	+	I	I	I	1		I	I	I	I	+	I
11	TO 050	Rhodosporidium toruloides	Acromyrmex balzani	+	Ι	Ι	Ι	+		I	I	Ι	I	+	I
12	TO 049	Sporisorium elionuri	Acromyrmex balzani	I	I	I	I	+		1	I	Ι	Ι	+	I
13	TO 217	Trichosporon mycotoxinivorans	Acromyrmex balzani	I	I	I	I	+		I	I	I	I	I	I
14	TO 023	Cryptococcus laurentii	Acromyrmex balzani	+	I	I	I			1	I	Ι	I	Ι	I
15	TO 018	Rhodotorula mucilaginosa	Acromyrmex balzani	+	I	I	Ι	+		1	Ι	Ι	Ι	Ι	I
16	SIA 24.1	Sporobolomyces japonicus	Fallen vegetation litter	Ι	I	I	I	I		I	I	I	Ι	I	I
17	TO 057	Sporisorium elionuri	Acromyrmex balzani	Ι	Ι	Ι	Ι	+		I	I	I	I	Ι	Ι
18	BR6-2AI	Candida shehatae	Bromeliad water	I	Ι	Ι	Ι			I	I	I	Ι	Ι	Ι
19	54	Trichosporon chiarellii	Myrmicocrypta sp.	Ι	Ι	Ι	Ι			I	Ι	Ι	Ι	Ι	I
20	CG8- 8BY	Candida shehatae	Mushroom	I	I	I	I	1		I	I	I	I	I	I
21	PT1- 1BASP	Candida shehatae	Euterpe sp.	T	T	I	I			I	I	I	I	T	I
22	BR6- 2AY	Candida shehatae	Bromeliad water	I	I	I	Ι			I	I	I	I	I	Ι
23	N8a	Meyerozyma guilliermondii	I	+	Ι	I	Ι	I		I	I	I	I	+	Ι
24	N12a2	Trichosporon asahii	Ι	I	I	I	I	1		1	I	I	I	Ι	I
25	N4ap2	Trichosporon asahii	I	Ι	Ι	I	I	I		1	I	I	I	Ι	I

	Strain	Species	Substrate where	Resu	lts										
			strain was obtained	Aceti acid	с	Syring	aldehyde	Ferulic acio	_	Furfural		5-hydroxyme	thylfurfural	Comb of comp	ination
				1 g/L	5 g/L	0.2 g/L	0.7 g/L	8×10^{-2} g/L	0.4 g/L	$\frac{1.8}{\text{g/L}} \times 10^{-3}$	1.6×10^{-2} g/L	4.0×10^{-3} g/L	2.0×10^{-2} g/L	1 ^a	2 ^b
26	PI-II5	Aureobasidium pullulans	Polybia ignobilis	I	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	I
27	PI-II63	Aureobasidium pullulans	Polybia ignobilis	Ι	Ι	Ι	I	Ι	+	Ι	Ι	Ι	I	Ι	Ι
28	32	Aureobasidium pullulans	Polybia ignobilis	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι
29	MP2- 2CB	Pseudozyma hubeiensis	I	I	I	I	I	I	+	I	I	I	+	+	I
30	PBM 39	Meira Arqovae CBS 110053	Atta laevigata	+	I	I	Ι	I	I	I	I	I	I	+	I
31	A1 M- A12	Pichia caribbica	Atta sp.	+	I	I	I	I	I	I	I	I	I	+	I
32	PBM 3	Aureobasidium pullulans	Atta laevigata	I	T	Ι	Ι	Ι	Ι	I	Ι	Ι	Ι	Ι	I
33	FB1- 1DASP	Candida sp.	Campanulaceae	I	I	I	Ι	I	I	I	I	I	I	I	I
34	H10- 10AY	IN	Hedychium coronarium koening	I	I	I	I	I	I	I	I	I	I	I	I
35	HFLS- 5BASP	Candida tenuis	Hedychium coronarium koenig	I	I	I	I	I	I	I	I	I	I	I	I
36	TO 011	Cryptococcus mangaliensis	Acromyrmex balzani	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι
37	TO 23	Cryptococcus laurentii	Acromyrmex balzani	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι
38	A1M-A7	Exophiala sp.	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	I	Ι	Ι
39	FB8	NI	I	+	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	+	Ι
40	Lj-3	Issatchenkia occidentalis CCTCC M 206097	Wastewater and sludge	+	+	I	I	+	I	I	I	I	I	+	I
41	S-7	Issatchenkia orientalis CCTCC M 206098	Wastewater and sludge	+	I	I	I	I	I	I	I	I	I	+	+
42	LΜ	Lecythophora sp.	Polybia ignob ilis	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι
43	B22a2	Candida azyma	Polybia ignob ilis	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	I	Ι	Ι
44	S11	Saccharomycopsis crataegensis	Polybia ignob ilis	+	I	I	I	+	I	I	I	I	I	+	I
45	Mel 28	Pichia caribbica	Polybia ignob ilis	+	Ι	Ι	Ι	+	Ι	Ι	Ι	Ι	Ι	+	I
46	YS4	Candida kofuensis	Polybia ignob ilis	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι
47	W13a1b	Pichia guilliermondii	Polybia ignob ilis	Ι	Ι	Ι	Ι	Ι	Ι	Ι	I	Ι	Ι	+	Ι
48	Mel 10	Aureobasidium pullulans	Polybia ignob ilis	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι

Table 2 continued

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	Strain	Species	Substrate where	Resul	ts										
			strain was obtained	Aceti acid	5	Syring:	aldehyde	Ferulic acid		Furfural		5-hydroxymet	hylfurfural	Comb of comp	ounds ounds
				1 g/L	5 g/L	0.2 g/L	0.7 g/L	8×10^{-2} g/L	0.4 g/L	1.8×10^{-3} g/L	1.6×10^{-2} g/L	4.0×10^{-3} g/L	$2.0 imes 10^{-2}$ g/L	1^{a}	2^{b}
49	MI	Issatchenkia occidentalis	Syzygium jambolanum	+	+	I	I	I	I	I	I	I	I	+	+
50	Yl'a	Issatchenkia occidentalis	Syzygium j amb olanum	+	+	I	I	I	I	I	I	I	I	+	+
51	Yl'b	Issatchenkia occidentalis	Syzygium jambolanum	+	+	I	I	I	I	I	I	I	I	+	+
52	Y3′	Issatchenkia occidentalis	Syzygium jambolanum	+	+	I	I	I	I	I	I	I	I	+	+
53	JP26/06a	Issatchenkia terricola	Syzygium jambolanum	+	I	I	I	I	I	I	I	I	I	+	I
54	W14	Pichia guilliermondii	Polybia ignobilis	+	Ι	Ι	Ι	I	Ι	Ι	Ι	Ι	Ι	+	Ι
55	BD149	<i>Cryptococcus</i> sp. (in description)	Electrical wiring of lamp post	I	Ι	I	I	I	I	I	I	I	I	+	I
56	A2-1	<i>Cryptococcus</i> sp. (in description)	Electrical wiring of lamp post	+	I	I	I	I	I	I	I	I	I	+	I
57	A2-4	<i>Cryptococcus</i> sp. (in description)	Electrical wiring of lamp post	I	I	I	I	I	I	I	I	Ι	I	I	I
58	TO 622	IN	Acromyrmex balzani	+	Ι	Ι	I	+	+	I	I	I	I	I	Ι
59	TO 623	NI	Acromyrmex balzani	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	I
60	TO 621	NI	Acromyrmex balzani	+	Ι	Ι	Ι	+	Ι	Ι	Ι	Ι	Ι	+	Ι
61	TO 443	NI	Acromyrmex balzani	+	Ι	Ι	I	Ι	Ι	Ι	I	Ι	I	Ι	I
62	TO 440	IN	Acromyrmex balzani	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι
63	TO 753	IN	Acromyrmex balzani	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι	Ι
64	CBS 5813	IN	1	I	I	I	I	I	I	I	I	I	I	I	I
^a Cí	mbination	1: Acetic acid (1 g/L) + Syri	ngaldehyde (0.2 g/L) +	feruli	c acid	(8×1)	.0 ⁻² g/L) -	+ furfural (1	$.8 \times 1$	0^{-3} g/L) + HI	MF (4.0×10^{-1})	⁻³ g/L)			
ŭ	mbination	2: Acetic acid (5 g/L) + Syri	ngaldehyde (0.7 g/L) +	feruli	c acid	(0.40	g/L) + fur	fural (1.6 \times	$10^{-2} \xi$	y(L) + HMF (2)	$2.0 \times 10^{-2} \text{ g/L}$	(
2 +	licroorganis	sm growth in presenting the se	elected compound M	icroor	ganist	n no gr	owth unde	or the selected	d com	punoc					
Stra	ns 40—Lj-	-3 Issatchenkia occidentalis CO	CTCC M 206097 e 41–	I 7-2-	ssatch	enkia o	rientalis C	DCTCC M 20	86090	were used as p	ositive control	[22]			

constituent in the hydrolysate (14.19 g/l) showing the maximum depolymerisation of hemicellulosic fraction from sugarcane bagasse. Also, glucose has been released from the hemicellulose or/and cellulose fractions. However, most of the cellulose remained in substrate and is not hydrolyzed by dilute acid hydrolysis. Fermentation inhibitors i.e. acetic acid, furfural, 5-HMF were also produced in hydrolysate. The non-concentrated acid hydrolysate also contained furfural (0.2820 g/l), 5-HMF (0.0149 g/l) and



Fig. 2 Yeast strains M1 Yl'a, Yl'b, and Y3' and Pichia occidentalis S-7, CCTCC M2006098 used as standard growth observed in the combination with higher concentrations of the toxic compounds tested

total phenolics (3.13 g/l). The vacuum evaporated acid hydrolysate represents almost fivefold increase of each component present in native hydrolysate except acetic acid, furfural and total phenolics.

Screening of Yeast for Detoxification

We have screened sixty-four yeast strains for their potential to use as detoxification of compounds present in hemicellulose hydrolysates (Fig. 1; Table 2). Among these, P. occidentalis M1, Y1'a, Y1'b and Y3' showed a significant decrease in the combination of toxic compounds acetic acid, syring aldehyde, ferulic acid, furfural and HMF in synthetic culture medium (Fig. 2). Out of these tested strains, we selected two yeast strains i.e. P. occidentalis M1 and Y1'a for further experiments with an aim to remove the fermentation inhibitors from sugarcane bagasse hemicellulosic hydrolysates. A 2² full factorial design with three repetitions in central point was carried out considering two process variables-pH and agitation. Cumulative inhibitors removal (%) refers to the difference between the initial and final concentrations of 5-HMF, furfural, phenols and acetic acid concentrations from hemicellulose hydrolysates after vacuum concentration process. Tables 3 and 4 show the initial and final concentrations in g/l of toxic compounds present in hemicellulosic hydrolyzate before and after the biological treatment step employing the strains of Picchia occidentalis M1 and Y1'a all experiments.

According to Pareto diagram, agitation (X2) showed significant reduction of inhibitors (90 %). However, pH

Table 3 Initial and final concentrations of toxic compounds in hemicellulose hydrolyzate treated biologically by Picchia occidentalis M1 (g/L)

Exp.	Concentration	HMF (g/L)	Furfural (g/L)	Acetic acid (g/L)	Total phenols (g/L)	Total concentration (g/L) ^a	Removed amount of toxic compounds (%) ^b
1	Initial	0.0364	0.1402	1.3	6.373	7.85	19.43
	Final	0.0297	0.1256	0.91	5.26	6.325	
2	Initial	0.0324	0.0153	1.47	6.04	7.557	22.87
	Final	0.002	0.0043	1.2	4.623	5.829	
3	Initial	0.0371	0.1135	1.12	6.51	7.781	36.29
	Final	0.0005	0.0065	0	4.95	4.957	
4	Initial	0.032	0.0925	1.42	6.41	7.954	42.89
	Final	0.0017	0.0007	0	4.54	4.542	
5	Initial	0.0341	0.1359	2.06	5.31	7.538	39.52
	Final	0.002	0.007	0	4.55	4.559	
6	Initial	0.0341	0.1284	2.04	5.356	7.562	39.98
	Final	0.002	0.007	0	4.53	4.539	
7	Initial	0.0335	0.1229	2.09	5.27	7.521	39.01
	Final	0.002	0.005	0	4.58	4.587	

^a "Total concentration" (g/L) refers to the sum of the concentrations of HMF, furfural, acetic acid and total phenols

^b "Removed amount of toxic compounds" (%) refers to the difference between initial concentration and final total concentration (g/L)

Table 4 Initial and final concentrations of toxic compounds in hemicellulose hydrolyzate treated biologically by Picchia occidentalis Y1'a (g/L)

Exp.	Concentration	HMF (g/L)	Furfural (g/L)	Acetic acid (g/L)	Total phenols (g/L)	Total concentration (g/L) ^a	Removed amount of toxic compounds (%) ^b
1	Initial	0.037	0.1443	1.02	6.495	7.696	17.69
	Final	0.035	0.0293	0.92	5.35	6.334	
2	Initial	0.0322	0.0575	1.57	6.02	7.679	20.5
	Final	0.0018	0.0035	1.33	4.77	6.105	
3	Initial	0.037	0.1283	2.13	6.52	8.815	46.04
	Final	0.0009	0.0051	0	4.75	4.755	
4	Initial	0.0317	0.1002	1.43	5.9	7.462	38.97
	Final	0.0015	0.002	0	4.55	4.553	
5	Initial	0.034	0.1394	2.02	5.69	7.882	43.08
	Final	0.0016	0.005	0	4.48	4.486	
6	Initial	0.0347	0.1415	2.04	5.63	7.842	42.79
	Final	0.0016	0.0049	0	4.48	4.486	
7	Initial	0.034	0.1374	1.9	5.7	7.769	42.41
	Final	0.0015	0.0031	0	4.47	4.474	

^a "Total concentration" (g/L) refers to the sum of the concentrations of HMF, furfural, acetic acid and total phenols

^b "Removed amount of toxic compounds" (%) refers to the difference between initial concentration and final total concentration (g/L)

(X1) and the interaction factor (X1 and X2) showed no significant removal of inhibitors for both strains of *P. occidentalis.* The agitation variable (X2) acted positively in the removal of toxic compounds (Fig. 3). Experiment 4 (pH 5.0, 300 rpm) demonstrated the most significant cumulative removal (42.89 %) of toxic compounds by *P. occidentalis* M1 (Table 5) allowing the removal of 94.77 % of 0.032 g/l 5-HMF, 99.19 % of 0.0925 g/l furfural, 29.17 % of 6.41 g/l phenolics and 100 % of 1.42 g/l acetic acid. On the other hand, experiment 3 (pH 4.0 and 300 rpm) showed the most significant cumulative removal (42.89 %) of toxic compounds by *P. occidentalis* Y1'a (46.04 %), i.e. 97.68 % of 0.037 g/l HMF, 96.06 % of 0.128 g/l furfural, 27.15 % of 6.52 g/l phenol and 100 % of 2.13 g/l acetic acid.

Discussions

Xylose and arabinose are the monomeric pentose sugars from hydrolysis of the hemicellulose fraction [9, 14]. Also, glucose produced in hydrolysate is from hemicellulose or/ and cellulose fractions [15]. Acetic acid is derived from the hydrolysis of the acetyl groups linked to the monomers of this polymer [9]. Xylose sugar has the highest concentration in the hemicellulosic hydrolysates due to the considerable amount of xylan present in hemicellulose [15, 16]. After vacuum evaporation of hydrolysate, acetic acid, furfural and total phenolic compounds might have evaporated or eliminated during the filtration of concentrated hydrolysates, therefore did not show the fivefold increase in concentarion. The pH of the concentrated hydrolysate was slightly decreased. These results are in well accordance with the studies of Martiniano et al. [17] and Milessi et al. [18].

Vacuum concentration process is essential to increase the concentration of sugars in the lignocellulosic hydrolysates [19]. The concentration of xylose, glucose and arabinose increased in accordance with the concentration factor employed (fivefold). However, acetic acid, 5-HMF, furfural and phenolics concentrations did not show the same behavior. The concentration of acetic acid was increased, but not according to concentration factor used, which may be related, in part, to the volatility of it. Phenolics and 5-HMF concentrations showed the same behavior, suggesting a partial volatilization and/or degradation of 5-HMF [20]. Also, Furfural concentration might be reduced due to its volatile nature. Our results showed resemblance with the report of Parajó et al. [19] and Carvalho et al. [20]. Detoxification results of hdrolysates by four strains i.e. P. occidentalis M1, Y1'a, Y1'b and Y3' corroborates with the work of Fonesca et al. [21].

Hou-Rui et al. [22] also, used *P. occidentalis* CCTCC M 206097 to remove fermentation inhibitors from sugarcane bagasse hemicellulosic hydrolysates and confirmed that this strain was able to remove 100 % of 2.0 g/l acetic acid and 0.02 g/l furfural. Likewise, Fonseca et al. [21] employed the same yeast strain *P. occidentalis* CCTCC M



Fig. 3 Pareto diagram representing the estimated effects of the variables and their interactions to a confidence level of 90 % (p = 0.1) for removal of toxic compounds by *Pichia occidentalis* strains M1 (**a**) and Y1'a (**b**)

Table 5 Experimental matrix of full factorial 2^2 design of experiments with the variables' values and the cumulative inhibitors removal (%) in each experiment by *Pichia occidentalis* M1 and *P. occidentalis* Y1'a

Experiment	Real le	evels	Cumulative inhil	bitors removal (%)
	X ₁ (pH)	X ₂ (rpm)	P. occidentalis M1	<i>P. occidentalis</i> Y1'a
1	4.0	100	19.43	17.69
2	5.0	100	22.87	20.50
3	4.0	300	36.29	46.04
4	5.0	300	42.89	38.97
5	4.5	200	39.52	43.08
6	4.5	200	39.98	42.79
7	4.5	200	39.01	42.41

206097 and reported 6.1 % removal of 3.3 g/l acetic acid, 100 % of 0.02 g/l of HMF and 100 % of 0.16 g/l furfural, after 72 h of biological detoxification. These results showed that *P. occidentalis* is a promising candidate for the in situ removal of toxic compounds from hemicellulosic hydrolysate. It is important to note that 5-HMF and furfural removal are not only related to the type of yeast used in the process, but also the kind of lignocelullosic material used to obtain the hemicellulosic hydrolysates. The different hemicellulosic hydrolysates provide different percentages removal by *P. occidentalis* [21].

This study demonstrates the potential of the yeasts for removal of inhibitors under the experimental conditions, pH (4.0 or 5.0) and agitation rate (100 rpm or 300 rpm), employing microbial detoxification approach. *P. occidentalis* M1 and *P. occidentalis* Y1'a exhibited the significant cumulative removal of inhibitors by 42.89 and 46.04 %, respectively. The major advantage of inhibitors removal by biological treatment is the cost-effectiveness and the minimization of filtration steps. Whereas, other detoxification methods required substantial investments. Also, biological treatment is an eco-friendly, economically-viable and can be used for the industrial applications.

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Compliance with Ethical Standards

Conflict of interest The authors also declare that they have no conflict of interest in the publication.

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