



Metabolic Engineering of Central Carbon Metabolism of *Bacillus licheniformis* for Enhanced Production of Poly- γ -glutamic Acid

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Abstract

Poly- γ -glutamic acid (γ -PGA) is an anionic polymer with wide-ranging applications in the areas of medicine, light chemical industry, wastewater treatment, and agriculture. However, the production cost of γ -PGA is high for the requirement of adding the expensive precursor L-glutamic acid during fermentation, which hinders its widespread application. In this study, in order to improve γ -PGA yield, central carbon metabolism was engineered to enhance the carbon flux of tricarboxylic acid (TCA) cycle and glutamic acid synthesis in a γ -PGA production strain *Bacillus licheniformis* WX-02. Firstly, pyruvate dehydrogenase (PdhABCD) and citrate synthase (CitA) were overexpressed to strengthen the flux of pyruvate into TCA cycle, resulting in 34.93% and 11.14% increase of γ -PGA yield in *B. licheniformis* WX-02, respectively. Secondly, the carbon flux to glyoxylate shunt was rewired via varying the expression of isocitrate lyase (AceA), and a 23.24% increase of γ -PGA yield was obtained in AceA down-regulated strain WXP_{baeA}aceBA. Thirdly, deletion of pyruvate formate-lyase gene *pflB* led to a 30.70% increase of γ -PGA yield. Finally, combinatorial metabolic engineering was applied, and γ -PGA titer was enhanced to 12.02 g/L via overexpressing *pdhABCD* and *citA*, repressing *aceA*, and deleting *pflB*, with a 69.30% improvement compared to WX-02. Collectively, metabolic engineering of central carbon metabolism is an effective strategy for enhanced γ -PGA production in *B. licheniformis*, and this research provided a promising strain for industrial production of γ -PGA.

Keywords *Bacillus licheniformis* · Poly- γ -glutamic acid · Central carbon metabolism · Tricarboxylic acid cycle

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Introduction

Poly- γ -glutamic acid (γ -PGA) is a natural anionic polymer with numerous valuable properties, such as water solubility, water holding, biodegradability, edibility, non-immunogenicity, and non-toxicity, and it has a variety of applications in the areas of medicine, light chemical industry, wastewater treatment, and agriculture [1]. However, high cost of γ -PGA impedes its large-scale production, which further affects γ -PGA application promotion [2].

The requirement of adding large quantities of expensive L-glutamate in the fermentation medium is a main cause of high cost of γ -PGA production [3]. Thus, improving synthetic capability of glutamic acid has been suggested to be effective strategy for reducing production cost [4]. Recently, many approaches have been implemented to improve the supply of intracellular glutamic acid for γ -PGA production. For instance, deletion of the glutamate dehydrogenase-encoded genes *rocR* and *gudB* significantly improved γ -PGA biosynthesis, enabling the engineering of *B. amyloliquefaciens* LL3 to produce 4.55 g/L γ -PGA, increased by 38% compared with wild type [5]. Introducing an energy-saving NADPH-dependent glutamate dehydrogenase pathway in *B. amyloliquefaciens* led to a 9% improvement of γ -PGA production [6]. Overexpression of *zwf* (encodes glucose-6-phosphate dehydrogenase) improved NADPH generation and increased synthetic capability of glutamic acid from α -ketoglutaric acid and eventually enhanced γ -PGA production by 35% in *B. licheniformis* WX-02 [4].

Metabolic engineering refers to rewiring metabolism of cells for efficiently producing desired products [7]. It is crucial in the construction of strains for the production of platform chemicals, biomaterials, and pharmaceuticals from renewable resources [8]. The central carbon metabolism, including glycolysis (Embden-Meyerhof (EMP) pathway), the pentose phosphate pathway (PPP), and tricarboxylic acid cycle (TCA cycle), plays a critical role in precursor synthesis, energy metabolism, and cofactor balance [1]. Metabolic engineering of carbon metabolic pathways is of great significance for improving the production of many products. Double-deletion mutants of phosphofructokinase ($\Delta pfkA1\Delta pfkA3$) in the EM pathway markedly increased chloramphenicol production by increasing the carbon flux in PP pathway in *Streptomyces avermitilis* [9]. Directing more carbon flux through oxPP pathway efficiently enhanced provision of acetyl-CoA and NADPH and improved 3-hydroxypropionic acid production by more than 24-fold in *Saccharomyces cerevisiae* [7]. The fumaric acid yield was effectively improved by engineering glucose uptake system and manipulation of precursor and by-product pathways in *Escherichia coli* [10]. Systematically engineering of TCA cycle and glyoxylate cycle resulted in high production of 4-hydroxybutyric acid in *E. coli* [11]. Moreover, GlcNAc titer was increased by 1.59-fold through rewiring central carbon metabolism in *B. subtilis* [12]. In the previous research of our group, strengthening TCA cycle efficiently improved the supplies of intracellular amino acids for bacitracin synthesis in *B. licheniformis* DW2 [13]. Glutamic acid involved in γ -PGA synthesis is mainly generated from α -ketoglutaric acid from TCA cycle [14]. Addition of citric acid accelerated the conversion of α -ketoglutaric acid to glutamic acid and eventually improved γ -PGA production [15]. Therefore, metabolic engineering of central carbon metabolic pathways to strengthen the supply of citric acid and glutamic acid is suggested as an efficient strategy to improve γ -PGA production.

B. licheniformis WX-02 is a well-established producer that can synthesize γ -PGA from glucose [16]. However, the γ -PGA productivity was much lower in the medium without glutamic acid addition [4, 17–19], which impedes its production and application. In this study, central carbon metabolism was optimized for efficient production of γ -PGA in *B.*

licheniformis WX-02. Specifically, TCA cycle, glyoxylate shunt and competing pathway were genetically modified to improve γ -PGA yield (Fig. 1). The results of this research suggest that metabolic engineering of central carbon metabolism is an effective strategy for improving the production of glutamate-relevant metabolites.

Materials and Methods

Strains, Plasmids, and Culture Conditions

The strains and plasmids used in this study were listed in Supplementary Table 1. *B. licheniformis* and *E. coli* were cultivated at 37 °C in Lysogeny-broth (LB) broth (1% tryptone, 0.5% yeast extract, 1% NaCl, and pH 7.2). The seed culture of *B. licheniformis* was prepared in a 250 mL flask containing 50 mL LB medium and incubated at 37 °C in a rotary shaker (240 rpm), until OD₆₀₀ reached 4.6~5.0. The seed culture (1.50 mL) was transferred into 250 mL flask containing 50 mL γ -PGA production medium (g/L: glucose 60, sodium nitrate 10, sodium citrate 10, NH₄Cl 8, CaCl₂ 1, K₂HPO₄·3H₂O 1, MgSO₄·7H₂O 1, ZnSO₄·7H₂O 1, and MnSO₄·H₂O 0.15) and shaken at 37 °C and 240 rpm for 36 h. All fermentation experiments were performed in three replicates. The antibiotic kanamycin was added into medium at the final concentration of 20 mg/L, when necessary.

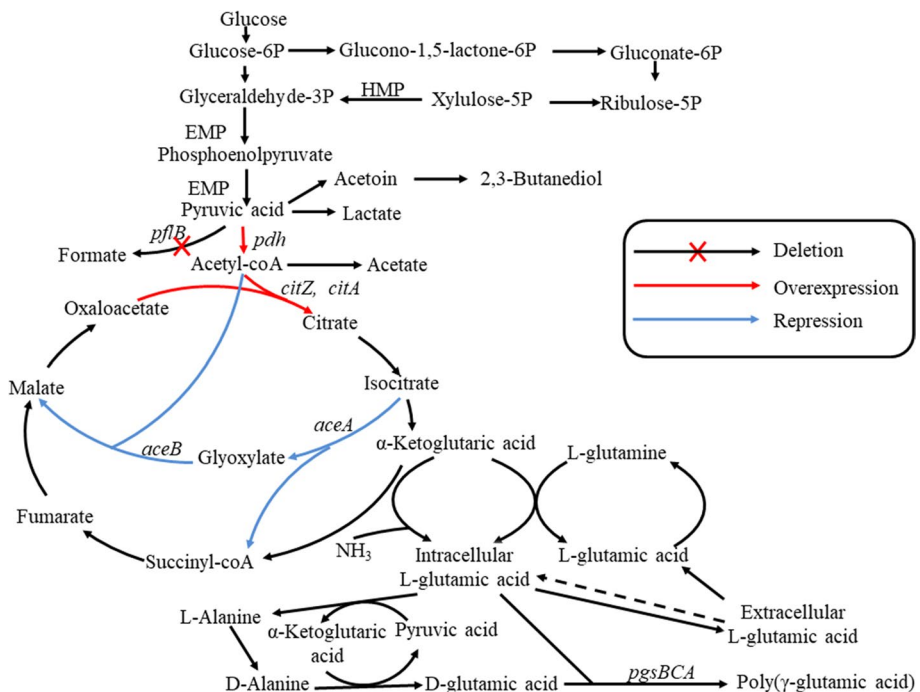


Fig. 1 The schematic diagram of metabolic engineering of central carbon metabolic pathways for efficient production of γ -PGA in *B. licheniformis*. Abbreviations: EMP, glycolysis; HMP, pentose phosphate pathway; *pdh*, encoding pyruvate dehydrogenase; *citZ* and *citA*, encoding citrate synthase; *aceA*, encoding isocitrate lyase; *aceB*, encoding malate synthase; *pflB*, encoding pyruvate formate-lyase

Substitution of Promoter in *B. licheniformis*

Substitution of the original promoters of *pdhABCD*, *citA*, and *aceBA* were performed according to the previously described method [3]. The procedure for replacing the native promoter of *pdhABCD* operon by P43 promoter served as an example. Briefly, the P43 promoter was amplified from *B. subtilis* 168, and homology arms of P_{pdh} were amplified from chromosomal DNA of *B. licheniformis* WX-02. These fragments were purified and ligated by Splicing Overlapping Extension PCR (SOE-PCR). And the fused fragment was inserted into T2(2)-Ori vector, generating promoter replacement plasmid, named T₂-P43*pdh*. Then, T₂-P43*pdh* was transformed into WX-02 by high-osmolality electroporation. The positive colonies were cultured in LB medium containing kanamycin (20 mg/L) at 45°C for 8 h to obtain the single-crossover recombinants. The double-crossover recombinants were screened after serial subculture of single-cross recombinants in LB medium at 37°C. The kanamycin-sensitive colonies resulting from double-crossover event were selected and confirmed by DNA sequence.

Gene Deletion in *B. licheniformis*

To delete pyruvate formate-lyase gene *pflB*, homology arms of *pflB* were amplified from *B. licheniformis* WX-02 genome, respectively. The resulting fragments were ligated by SOE-PCR, and inserted into T2(2)-Ori, resulting in gene knockout plasmid T₂-*pflB*. Furthermore, *pflB* gene knockout mutant was obtained via homologous double crossover, similar with that of promoter replacement [20].

Determination of Biomass, γ -PGA, and Glucose

The cell biomass was detected by measuring dry cell weight. The γ -PGA concentration was measured by high-performance liquid chromatography (HPLC) according to the method described in previous research [16]. The concentration of residual glucose was measured using a SBA-40C biosensor analyzer (Institute of Biology, Shandong Province Academy of Sciences, P.R. China).

Determination of Enzymatic Activities

Crude extracts of *B. licheniformis* for measuring the activities of pyruvate dehydrogenase, citrate synthase, and isocitrate lyase were prepared as follows: cells were harvested by centrifugation (4°C, 8000×g, 5 min) at mid-exponential phase, and cell pellet was washed once with 20 mL buffer (50 mmol/L Tris-HCl, pH 7.4, containing 10 mmol/L β -mercaptoethanol) and resuspended with the same buffer. The suspensions were disrupted by sonication (150 W, 20 kHz, pulse: 1 s on; 2 s off; total: 15 min), and supernatant was collected for enzyme activity analysis. Activity of pyruvate dehydrogenase was determined spectrophotometrically through monitoring the reduction of 2, 6-dichlorophenolindophenol (2, 6-DCPIP) at 600 nm [21]. The citrate synthase (CS) activity was assayed via 5,5-dithiobios-(2-nitrobenzoic acid) (DTNB) method [22]. The

isocitrate lyase activity was detected based on the formation of glyoxylic acid phenylhydrazine from glyoxylate and phenylhydrazine at 324 nm [23].

Statistical Analyses

All samples were analyzed in three replicates. The data were presented as the mean value \pm the standard deviation for each sample.

Results

Channeling Carbon Flux into TCA Cycle to Enhance γ -PGA Production

Acting as the precursor for γ -PGA synthesis, glutamic acid supply serves as the critical role in γ -PGA production. Glutamic acid is generated from α -ketoglutaric acid, an important intermediate metabolite in TCA cycle. However, TCA cycle is repressed in the presence of excess glucose, and a large proportion of by-products (such as lactate, acetoin, and 2, 3-butanediol) are converted from silted pyruvate [24], all of which hinder γ -PGA synthesis.

Pyruvate dehydrogenase (PDH), encoded by *pdhABCD* operon, is an important enzyme that mediates glycolysis pathway to TCA cycle. Previously, overexpression of PDH could strengthen acetyl-coenzyme A (CoA) supply and TCA cycle flux [25]. Here, in order to channel more glycolytic flux into TCA cycle, the origin promoter of *pdhABCD* operon was replaced by a stronger promoter (P43) in *B. licheniformis* WX-02, according to the procedure described in the section of “Substitution of promoter in *B. licheniformis*”, resulting in recombinant strain WXP43*pdh*. In addition, strains WXP_{*bacA*}*pdh* and WXP_{*srf*}*pdh* were constructed according to the same method, respectively. As showed in Fig. 2a, PDH activities of WXP43*pdh*, WXP_{*bacA*}*pdh*, and WXP_{*srf*}*pdh* were increased by 4.58%, 3.09%, and 8.04%, respectively, compared with that of control strain WX-02. Consistently, γ -PGA yields of WXP43*pdh*, WXP_{*bacA*}*pdh*, and WXP_{*srf*}*pdh* were enhanced to 7.44 g/L, 7.38 g/L, and 9.58 g/L, which were 4.79%, 3.94%, and 34.93% higher than that of WX-02 (7.10 g L⁻¹) (Fig. 2b), respectively.

CS catalyzes the first step of TCA cycle and is generally regarded as the rate-limiting enzyme in TCA cycle. Overexpression of CS redirected more carbon flux towards TCA cycle, which further benefited γ -PGA production [26]. In *B. licheniformis* WX-02, two genes *citZ* (encodes CS-II) and *citA* (encodes CS-I) encode CS [27]. Previous studies revealed that CS-II is inhibited by reduced nicotinamide adenine dinucleotide (NADH), and CS-I is insensitive to NADH [28]. In this study, the native promoter of *citA* in WX-02 was replaced with promoters P43, P_{*bacA*}, and P_{*srf*}, resulting in the mutants WXP43*citA*, WXP_{*bacA*}*citA*, and WXP_{*srf*}*citA*, respectively. As shown in Fig. 2c, CS activities in WXP_{*srf*}*citA* and WXP43*citA* were increased by 87.78% and 22.49%, respectively. And CS activity in WXP_{*bacA*}*citA* was decreased by 26.54% (Fig. 2c). The mutants WXP_{*srf*}*citA* and WXP43*citA* produced 7.89 g/L and 7.76 g/L γ -PGA, which were 11.14% and 9.26% higher than that of WX-02, respectively (Fig. 2d), while the mutant WXP_{*bacA*}*citA* produced 6.91 g/L γ -PGA, decreased by 2.70% compared to that of WX-02 (Fig. 2d).

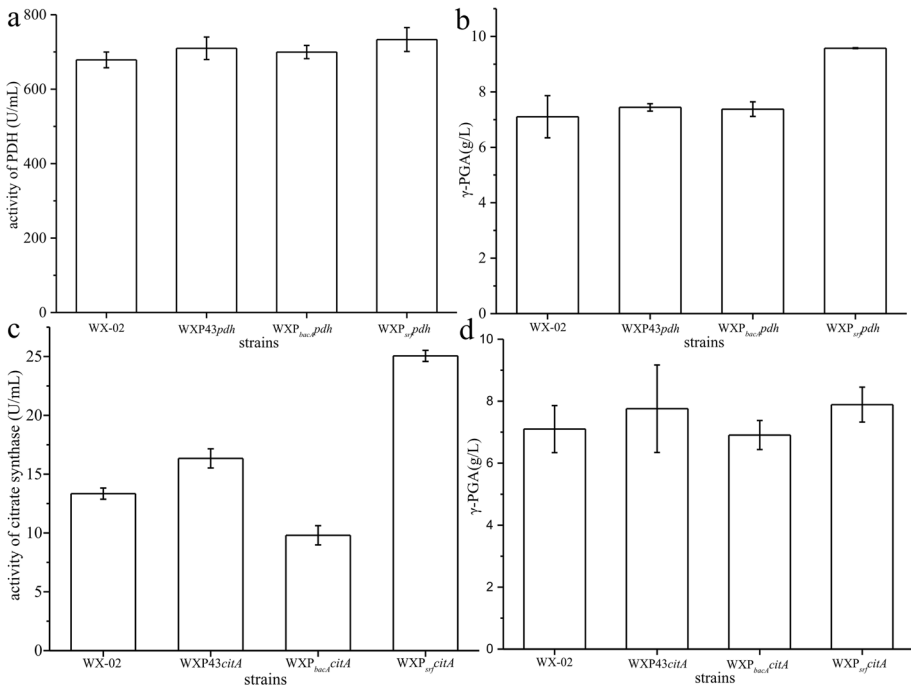


Fig. 2 Channeling carbon flux into tricarboxylic acid (TCA) cycle to enhance γ -PGA production. **a** Specific PDH activity in different *B. licheniformis* strains (WX-02, WXP43pdh, WXP_{bacA}pdh, and WXP_{srf}pdh). **b** The effect of overexpression of *pdh* on γ -PGA production. **c** Specific CS activity in different *B. licheniformis* strains (WX-02, WXP43citA, WXP_{bacA}citA, and WXP_{srf}citA). **d** The effect of overexpression of *aceA* on γ -PGA production

Effects of Glyoxylate Shunt on γ -PGA Production

The glyoxylate shunt is a bypass of TCA cycle. And it is indispensable for glutamate overproduction in *Corynebacterium glutamicum*, since it supplies the key metabolites as well as energy during cell growth phase [29]. However, high flux of glyoxylate shunt might lead to a shortage of α -ketoglutarate, which is not conducive to glutamic acid production [30]. To optimize the carbon flux of glyoxylate cycle, the activities of enzymes involved in glyoxylate shunt were adjusted by replacing the native promoter of *aceBA* with promoter P43, P_{bacA}, or P_{srf} resulting in mutant strains WXP43*aceBA*, WXP_{bacA}*aceBA*, and WXP_{srf}*aceBA*, respectively. As shown in Fig. 3a, the activities of isocitrate lyase in WXP43*aceBA* (2.05 U/mL) and WXP_{srf}*aceBA* (3.42 U/mL) were increased by 93.40% and 222.64% than that in WX-02 (1.06 U/mL), respectively. However, the activity of isocitrate lyase in WXP_{bacA}*aceBA* (0.62 U/mL) was decreased by 41.51% (Fig. 3a). The productions of γ -PGA by mutants WXP43*aceBA* (6.94 g/L) and WXP_{srf}*aceBA* (7.10 g/L) exhibited no significant difference from WX-02 (Fig. 3b), while WXP_{bacA}*aceBA* showed 23.24% increase in γ -PGA yield (8.65 g/L) (Fig. 3b). Collectively, these results indicated that reducing flux of glyoxylate pathway was beneficial for γ -PGA production.

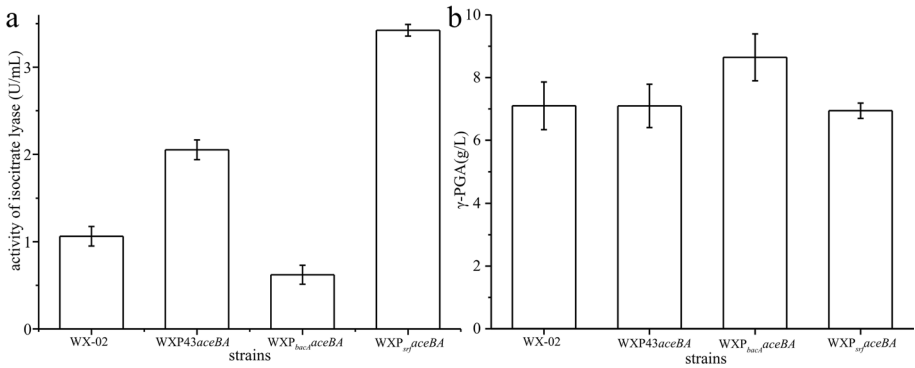


Fig. 3 Effects of varied AceA expression on γ -PGA production. **a** Specific AceA activity. **b** γ -PGA production

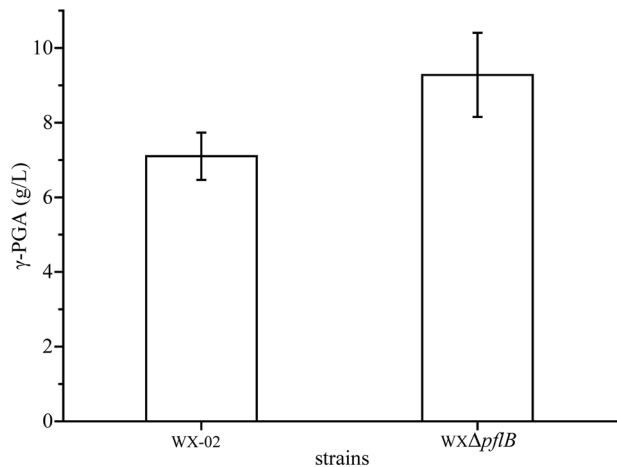
Minimization of Carbon Loss by Deleting *pflB*

The formation of γ -PGA could increase the viscosity of fermentation broth and decrease oxygen transfer efficiency [17]. Under micro-aerobic condition, most pyruvate is resolved to formate and acetyl-CoA through pyruvate formate-lyase (PFL) [31]. In silico analysis of genome sequence showed that *B. licheniformis* WX-02 possesses gene *pflB* that encodes PFL [27]. In this research, the *pflB* gene was deleted to block the metabolic flux from pyruvate to formate and acetyl-CoA, obtaining mutant strain $WX\Delta pflB$. As shown in Fig. 4, $WX\Delta pflB$ produced 9.28 g/L γ -PGA, 30.70% higher than that of WX-02.

Combinatorial Metabolic Engineering for Enhanced Production of γ -PGA

To further improve γ -PGA production, combinatorial metabolic engineering was applied to overlay the above priority strategies. Firstly, origin promoter of gene *citA* was replaced with promoter P_{srfI} in $WXP_{srfI}pdh$, generating strain WX-PA. The γ -PGA yield of WX-PA

Fig. 4 γ -PGA production of *B. licheniformis* strains WX-02 and $WX\Delta pflB$



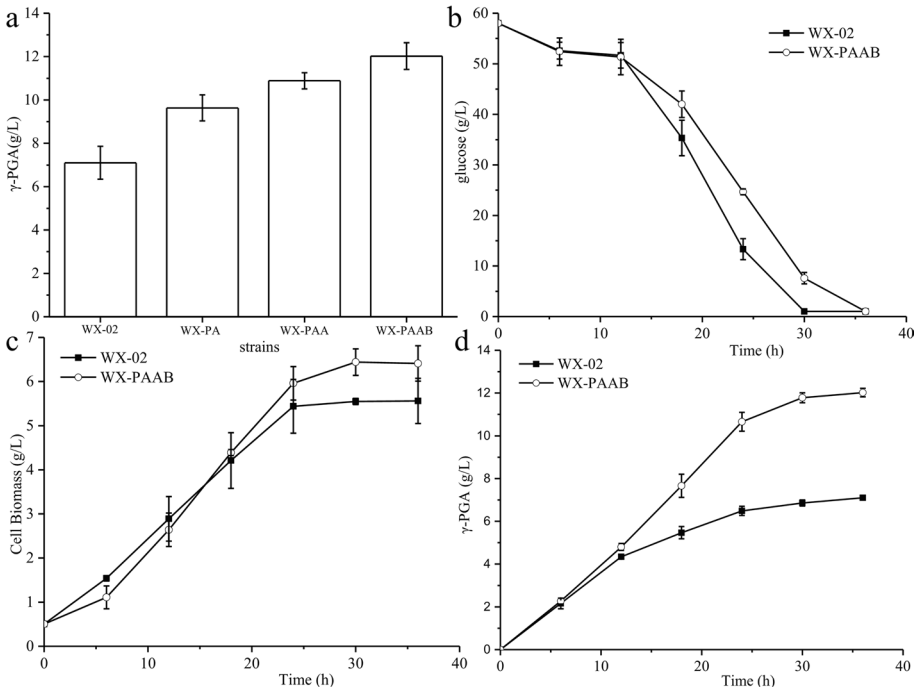


Fig. 5 Combining the beneficial manipulations to improve γ -PGA production. **a** Comparison of γ -PGA fermentation between WX-02 and mutant strains. **b–d** Fermentation process curves of WX-02 and WX-PAAB during γ -PGA production: **b** glucose concentration, **c** cell biomass, **d** γ -PGA yield

reached 9.63 g/L, increased by 35.63% compared with that of WX-02 (Fig. 5a). Then, strain WX-PAA was constructed by replacing origin promoter of *aceBA* operon with promoter P_{bacA} based on strain WX-PA. The WX-PAA strain showed a 53.24% improvement in γ -PGA production (Fig. 5a). Finally, *pfkB* gene was deleted, resulting in final strain WX-PAAB. As shown in Fig. 5b, the glucose consumption of WX-PAAB (36 h) was slower than that of WX-02 (30 h). The maximum cell biomass of WX-PAAB (6.44 g/L) was enhanced by 16.04% compared with that of WX-02 (Fig. 5c). The γ -PGA titer of WX-PAAB increased with the increasing fermentation time, and the maximum titer reached 12.02 g/L at 36 h, increased by 69% compared with that of WX-02 (Fig. 5d). The γ -PGA yield and productivity reached 1.71 g/g cell and 0.33 g/L/h, respectively, significantly higher than those of WX-02 (1.27 g/g cell and 0.20 g/L/h, respectively).

Discussion

γ -PGA is a natural polymer with wide-ranging applications. Currently, microbial synthesis of γ -PGA with *Bacillus* species relies on supplementation of expensive precursor L-glutamic acid, which sharply increases overall cost [2]. Central carbon metabolism is crucial for cell growth and product synthesis. In this study, we improved γ -PGA production via overexpression of pyruvate dehydrogenase and citrate synthase, weakening the glyoxylic acid cycle, and disrupting the conversion of pyruvate to formate and acetyl-CoA in *B.*

licheniformis WX-02. Our results confirmed that metabolic engineering of central carbon metabolism is an effective strategy for enhanced production of γ -PGA in *B. licheniformis*.

Glucose is an efficient carbon source for γ -PGA production [1]. It is degraded to pyruvate via EMP pathway. Pyruvate is converted to citrate that is subsequently metabolized to α -ketoglutaric acid through TCA cycle. Then α -ketoglutaric acid is converted to glutamic acid, the precursor for the synthesis of γ -PGA (Fig. 1). Therefore, γ -PGA production can possibly be improved by enhancing the TCA cycle and glutamate synthesis. In general, *Bacillus* species have a strong overflow metabolic pathway from glucose, owing to the lower activity of TCA cycle and respiratory chain relative to the glucose uptake rate [32]. The TCA cycle is repressed by CcpA-dependent catabolite repression mechanism in the presence of excess glucose [24]. Moreover, the expression of enzymes encoded by *alsSD* involved in acetoin production is activated by CcpA [33]. Acetoin can be reduced to 2, 3-butanediol by 2, 3-BD dehydrogenase (BDH) with oxidation of NADH to NAD⁺ [34]. In addition, the high viscosity of γ -PGA hinders the oxygen supply, which prevents the oxidation of NADH via respiratory chain and increases the pool of NADH availability for 2, 3-butanediol generation [17, 35, 36]. Therefore, a large proportion of glucose is metabolized to pyruvate and subsequently converted to acetoin and 2, 3-butanediol that are excreted to the outside of cell as by-products during γ -PGA fermentation, when using glucose as carbon source in *B. licheniformis* [36, 37]. Reducing the production of acetoin and 2, 3-butanediol was suggested to be beneficial for γ -PGA production [3, 38, 39]. However, deletion of gene *alsS* (encoded acetolactate synthase) resulted in poor cell growth [40], which was unfavorable for γ -PGA production. Pyruvate is converted to acetyl-CoA under the catalysis of PDH. Overexpression of PDH improved acetyl-CoA supply for TCA cycle [25, 26, 41], which may be beneficial for γ -PGA synthesis. In this study, substitution of the native promoter of *pdhABCD* operon with stronger promoters (P₄₃, P_{bacA}, and P_{srj}) successfully enhanced PDH activity (Fig. 2a) and increased the γ -PGA yield by 4.79%, 3.94%, and 34.93%, respectively (Fig. 2b).

The TCA cycle is one of the important metabolic pathways involved in the production of energy. Also, TCA cycle provides precursors for anabolism, such as α -ketoglutaric acid for glutamic acid and oxaloacetate for aspartic acid families [13]. Thus, enhancing TCA cycle was confirmed to be an efficient strategy to improve the supply of ATP and precursors for metabolite production [13, 30, 42]. Overexpression of *citA*, *citB*, and *icd* shifted the carbon flux to α -ketoglutarate, resulting in a slight increase in γ -PGA production in *B. subtilis* [26]. In the present study, the substitution of stronger promoter P_{srj} for the native promoter of NADH-insensitive citrate synthase CitA effectively increased the CS activity and enhanced γ -PGA production (Fig. 2c and d). This result was consistent with the previous research [26].

The glyoxylate shunt is an important anaplerotic pathway of TCA cycle for replenishing key metabolites, such as succinate and oxaloacetate [29]. Engineering the glyoxylate bypass has been used to improve the production of various products. Enhancing glyoxylate shunt has been applied to produce succinate [43], acetyl-CoA-derived chemicals (phloroglucinol and 3-hydroxypropionate) [44], L-threonine [45, 46], and tyrosine [47]. The glyoxylate cycle is crucial for glutamate overproduction in *C. glutamicum* [29]. The relationship between glutamate production and glyoxylate cycle is complicated. High flux of glyoxylate shunt may lead to a shortage of α -ketoglutarate, the precursor of glutamic acid. Conversely, insufficient flux may result in the lack of other key metabolites, such as succinate and oxaloacetate, which impairs cell growth. Appropriate activity of glyoxylate cycle enhanced TCA cycle and provided more α -ketoglutarate for the syntheses of related metabolites in *E. coli* [45, 48]. In this study, the native promoter of *aceBA* was replaced

with different strength promoters P₄₃, P_{bacA}, and P_{srf}. The activity of isocitrate lyase was decreased by 41.51% in WXP_{bacA}*aceBA*, while that in WXP₄₃*aceBA* and WXP_{srf}*aceBA* were increased by 93.40% and 222.64%, respectively. The WXP_{bacA}*aceBA* showed a 23.24% increase in γ -PGA production compared to WX-02. These results indicated that the flux of glyoxylate cycle is high in *B. licheniformis* WX-02, which is detrimental to γ -PGA production. Therefore, glyoxylate shunt flux should be rewired at appropriate level for optimal γ -PGA production.

In conclusion, central carbon metabolism was engineering for efficient production of γ -PGA in *B. licheniformis*. Firstly, the flux of pyruvate to the TCA cycle was enhanced by replacing the native promoter of *pdhABCD* operon with stronger promoter P_{srf}. Secondly, the TCA cycle was strengthened by enhancing the activity of NADH-insensitive citrate synthase CitA through substitution of the origin promoter of *citA*. Subsequently, the carbon flux to glyoxylate shunt was rewired via varying the expression of isocitrate lyase AceA, and γ -PGA yield was increased in AceA down-regulated strain WXP_{bacA}*aceBA*. Furthermore, the pyruvate formate-lyase gene *pflB* was deleted to reduce the carbon loss. Finally, through a combinatorial metabolic engineering approach, the γ -PGA yield of the final strain WX-PAAB reached 12.02 g/L, 69% higher than that of the starting strain WX-02. These results demonstrated that metabolic engineering of central carbon metabolic pathways is an effective strategy for enhanced production of γ -PGA, and this strategy may be widely applicable for the production of other important chemicals.

Supplementary Information The online version contains supplementary material available at <https://doi.org/10.1007/s12010-021-03619-4>.

Author Contribution B Li, D Cai, and S Chen designed the study. B Li carried out the molecular biology studies, construction of engineering strains, and the fermentation studies. B Li, D Cai, and S Chen analyzed the data and wrote the manuscript. All authors read and approved the final manuscript.

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Declarations

Conflict of Interest The authors declare no competing interests.

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