Enhancement of catalytic activity of Au/TiO*2* by thermal and plasma treatment

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Abstract^{*−*A} significant enhancement in the catalytic activity of Au/TiO₂ in CO oxidation and preferential oxidation reaction by creating the active sites on the catalyst surface by thermal treatment as well as by producing small gold particles by plasma treatment has been studied. Au/TiO₂ catalyst (Au (1 wt%) supported on TiO₂) was prepared by conventional deposition-precipitation method with NaOH (DP NaOH) followed by washing, drying and calcination in air at 400 °C for 4 h. Thermal treatment of Au/TiO₂ was carried out at 550 °C under 0.05 mTorr. A small amount of Au/TiO₂ catalyst was taken from the untreated and thermally treated Au/TiO₂ and both kinds of catalysts were treated with plasma sputtering at room temperature. The activity of the catalysts has been examined in the reaction of CO oxidation and preferential oxidation (PROX) at 25-250 °C. Thermally treated $Au/TiO₂$ showed better catalytic activity as compared to the untreated catalyst. There is also an additional enhancement in the catalytic activity due to plasma sputtering on the both kinds of catalysts. Thermally treated Au/TiO₂ followed by plasma sputtering Au/TiO₂ showed higher conversion rates for CO oxidation reaction compared with untreated, thermally treated and plasma sputtered Au/TiO₂ catalysts. It may be concluded that the enhancement of catalytic activity of thermally treated Au/TiO₂ followed by plasma sputtering is owing to the generation of active sites such as oxygen vacancies/defects in TiO₂ support using thermal treatment as well as by producing small gold particles using plasma treatment.

Key words: Catalytic Activity, Au/TiO₂ Catalyst, CO Oxidation, Thermal and Plasma Treatment

INTRODUCTION

Since the discovery in the late 1980s that gold is catalytically active when it is dispersed as small particles on an oxide support, the preparation of gold-based catalysts has been widely studied [1-5]. They are active in many reactions of both industrial and environmental importance. The most remarkable catalytic properties of supported gold have been obtained for the reaction of CO oxidation at ambient temperature [3-6]. The catalytic activity strongly depends on the dimensions of gold particles and is the highest in the range of 1-3 nm [7-11], the material used as support, the synthesis method, parameters of the preparation (contact time, pH, temperature (T)) and the catalyst activation procedure [7,9,12,13].

Titanium oxide has attracted a great deal of research interest among the commercially employed catalysts over the past 30 years. Additional research interest has arisen for $TiO₂$ as a support for metal catalysts, particularly since Haruta et al. demonstrated that Au acts as a catalyst for low-temperature CO oxidation when dispersed as nanoclusters on a $TiO₂$ support [14]. It has been proven that the catalytic activity of Au/TiO₂ catalyst is mainly affected by two factors [15,16], the particle size of Au and the interaction between Au and TiO₂, in which the latter is more important than the former. Many researchers [16-20] are of the opinion that Au is the active site for CO adsorption and $TiO₂$ is the active site for $O₂$ adsorption, and the strong interaction between Au and $TiO₂$ can accelerate a spillover

of the reaction species between Au and $TiO₂$, resulting in an increase in the catalytic activity.

Most of the highly active catalysts reported to date are prepared using precipitation methods, either co-precipitation or deposition-precipitation. It has been proposed that new adsorption sites are created at the interface, and some synergism between gold nanoparticles and support is responsible for the high activity [18,21]. Furthermore, it has been speculated that surface defects may alter the electronic configuration of Au nanoparticles to enable catalytic reactions [22]. However, only negligible research has been conducted so far to increase the activity of gold catalysts by creation of oxygen vacancies/ defect sites. In view of fulfilling this research deficiency, we have selected to study the effect of oxygen vacancies/defect sites in gold catalysts for CO oxidation and preferential oxidation reactions. The goal of this work was to prepare Au/TiO₂ catalysts to study their catalytic performance and stability as a function of time in the CO oxidation reaction and PROX reaction. In this study, we have reported that nano-crystalline gold catalysts for CO oxidation and PROX reactions at low temperatures may be promoted by the creation of oxygen vacancies/defects on the support surface due to thermal treatment as well as by producing small gold particles using plasma treatment.

EXPERIMENTAL

1. Synthesis of $Au/TiO₂$ Catalysts

The Au/TiO₂ catalyst with nominal gold loading of 1 wt\% supported on TiO₂ was prepared by deposition-precipitation (DP) under

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complete control of all parameters: temperature, pH, and stirrer speed using solid $HAuCl₄·3H₂O$ (Acros) as gold precursor and Titania complete control of all parameters: temperature, pH, and stirrer speed using solid $HAuCl_4$ ^{-3H₂O (Acros) as gold precursor and Titania (Degussa P25) was used as support (45 m² g⁻¹, nonporous, purity} >99.5%). The gold precursor solution was neutralized slowly with vigorous stirring to pH 7 at 70 °C with a NaOH solution and mixed with a TiO₂ suspension that was kept at 35 °C. The resulting mixture was maintained at pH 7 at 35 °C for two hours. The mixture was filtered, and the solid was washed twice with room temperature deionized water and then once with 70 °C water. The solid was suction filtered and dried at room temperature.

The half amount of prepared Au/TiO₂ catalyst was followed by thermal treatment at 550 °C under 0.05 mTorr for 4 hr. The two catalysts (without and with thermal treatment) were treated with plasma sputtering at room temperature in 26 mTorr Ar for 20 min. In this study, catalysts of Au/TiO₂ (without thermal treatment), Au/TiO₂ (thermally treated), $Au/TiO₂$ (plasma treatment), and Au/TiO , (thermally treated followed by plasma treatment) are referred as AuTi-1, AuTi-2, AuTi-3 and AuTi-4 respectively.

2. Catalysts Characterization

The structure and surface composition of the different catalysts (AuTi-1, AuTi-2, AuTi-3 and AuTi-4) were obtained by different techniques. X-ray diffraction (XRD) measurements were performed on a Bruker D8 advance diffractometer by using $\text{CuK}\alpha$ radiation (within the 2θ range going from 10 to 85) to evaluate the catalyst structure. The size and particle distribution of the Au nanoparticles were derived from transmission electron microscopy (TEM) images. TEM examination of $Au/TiO₂$ catalysts was performed with a Hitachi HF-2000 TEM with a field emission gun at 200 keV. The Raman spectra were recorded on a Renishaw MicroRaman Invia spectrometer, equipped with an argon laser source. The laser excitation line was 514 nm, and the power was of 25 mW. The catalysts were further characterized by inductively coupled plasma atomic emission spectroscopy (ICP-AES) measurements, and thermal plasma deposition (TPD).

3. Activity Measurements

The catalytic activity tests were carried out in a conventional flow reactor system. The products were analyzed by a Varian 3400 gas chromatograph (GC) equipped with a thermal conductivity detector (TCD), flame ionization detector (FID) and a carbosphere column. 0.05 g of Au/TiO₂ was used in each activity test, and the gas compositions were 1 vol% CO with air balance with a gas hourly space 0.05 g of $Au/TiO₂$ was used in e
positions were 1 vol% CO with velocity (GHSV) of 120,000 h^{−1} velocity (GHSV) of $120,000$ h⁻¹ for the oxidation of CO, and 50% blog given that H₂ was used in each delivery lest, and the gas be positions were 1 vol% CO with air balance with a gas hourly sp velocity (GHSV) of 120,000 h⁻¹ for the oxidation of CO, and 5 H₂, 1% O₂, 1% CO and 4 H₂, 1% O₂, 1% CO and 48% N₂ with a GHSV of 120,000 h⁻¹ for the preferential oxidation (PROX) of CO. After CO oxidation, the catalyst bed was purged with Ar for approximately 15 min at 195 K to remove CO and $O₂$ before warming up to room temperature for subsequent H₂ pulse reduction. This step is critical because it has been noted previously that as-prepared $Au/TiO₂$ catalyst can be rapidly reduced by the reaction mixture at room temperature.

RESULTS AND DISCUSSION

1. Catalysts Surface Properties

In the following, we present and discuss results on the structure and surface composition of the various catalysts (AuTi-1, AuTi-2, AuTi-3 and AuTi-4). XRD powder patterns of all catalysts were recorded on a Bruker D8 Advance diffractometer by using $CuK\alpha$

Fig. 1. X-ray diffraction patterns of the studied $Au/TiO₂$ catalysts.

radiation (within the 2θ range going from 10 to 85). XRD patterns of all catalysts show the formation of anatase as the main crystalline $TiO₂$ phase for the entire catalysts as shown in Fig. 1. It seems that the incorporation of Au restricts the transformation of the $TiO₂$ anatase phase to the rutile $TiO₂$ crystalline phase [23]. Normally,

Fig. 2. CO oxidation at 25, 50, 100, 150, 200, 250 °C over $Au/TiO₂$ catalysts. AuTi-1 (■), AuTi-2 (●), AuTi-3 (▲), AuTi-4 $(\blacktriangledown).$

Fig. 3. CO selectivity at 25, 50, 100, 150, 200, 250 °C over Au/TiO_2 catalysts for PROX reaction. AuTi-1 (\blacksquare), AuTi-2 (\spadesuit), AuTi-3 (\blacktriangle), AuTi-4 (∇).

the rutile phase starts to grow at 450 °C in sol gel materials, which means that Au doping favors the retention of the anatase phase on these sol gel materials. In Fig. 1, there are main peaks of anatasetype $TiO₂$, but peaks for gold did not appear in Au/TiO₂. There may be two reasons for the disappearance of Au: one is good dispersion of Au in TiO₂ [24] and the other one may be due the amorphous behavior of Au [23].

2. Effects of Thermal and Plasma Treatment on CO Oxidation Activity

Fig. 2 shows the catalytic activity of $Au/TiO₂$ catalysts for CO oxidation prepared by DP method. The catalysts were evaluated for the low temperature oxidation of CO using 1 vol% CO with air balance and total flow rate was 120,000 h⁻¹. AuTi-3 and AuTi-4 balance and total flow rate was 120,000 h⁻¹. AuTi-3 and AuTi-4 catalysts showed higher catalytic activity as compared to AuTi-1 and AuTi-2 catalysts up to 100° C, but all the catalysts showed 100% CO conversion with the increase of temperature up to 150 °C. Thermally treated Au/TiO , followed by plasma sputtering Au/TiO , catalyst has also demonstrated an additional enhancement of catalytic activity.

Fig. 3 shows that all the catalysts showed 100% selectivity at room temperature, but it is gradually decreased with the increase of temperature. The simulation gas contained 50% H_2 , 1% O_2 , 1% CO and 48% The flow rate was fixed at 120,000 h−1
48% N₂, and the flow rate was fixed at 120,000 h^{−1} 48% N_2 , and the flow rate was fixed at 120,000 h⁻¹ in all experiments. The reduction of the selectivity with the increase of temperature is expected for two main reasons. First, when the temperature increases, H₂ adsorption on catalyst is favored compared to that of CO [25]; second, the amount of oxygen in order to oxidize the CO is insufficient due to its consumption by $H₂$ oxidation at higher temperatures.

3. Effects of Thermal and Plasma Treatment on PROX Reaction

Fig. 4 shows the catalytic activity for PROX reaction using same catalysts. The activity also increased for the PROX reaction after oxygen vacancies/defect generation. The order of activity was the same as in case of CO oxidation below 100 °C, but the difference in the activity between catalysts was small. Above 100 °C, the effi-

Fig. 4. CO Oxidation at 25, 50, 100, 150, 200, 250 °C over Au/TiO₂ catalysts in PROX reaction. AuTi-1 (■), AuTi-2 (●), AuTi- 3 (\blacktriangle), AuTi-4 (∇).

ciency order of the catalysts in the PROX reaction is different from that in the CO oxidation reaction. However, it is clear for all the catalysts that in the presence of $H₂$, the conversion of CO reaches a maximum at 100 °C followed by an abrupt decrease, which is attributable to the same reasons responsible for the reduction in selectivity with the increase of temperature.

4. Effects of Plasma Treatment on the $Au/TiO₂$ Catalysts

It is well-known that the particle size of Au has a significant impact on the catalytic activity in supported gold catalysts [26]. To investigate the particle size of Au prepared by DP method, TEM observations were performed as shown in Fig. 5(a)-(d). The number of gold particles increased for AuTi-3 and AuTi-4 as compared to AuTi-1 and AuTi-2, although the same amount of gold was deposited during the preparation of catalysts.

The average size and size distribution of each catalyst were manually calculated from TEM images (Fig. 5(a)-(d)). According to the size distribution histogram, shown in Fig. 6(a)-(d), the average size of the gold particles (manually calculated) was 2.85 nm for the AuTi-4 catalyst, which was much smaller compared to the catalyst AuTi-1 (4.46 nm). To calculate the size distribution, we kept a margin of ± 1 to remove the human error.

The results obtained from ICP-AES (OPTIMA 4300 DV (Perkin-Elmer, USA), Power: 1300 W Amount of catalyst=0.2 g) confirmed that the Au particles increased for AuTi-3 and AuTi-4 as compared to AuTi-1 and AuTi-2 (see Table 1). This implies that the creation of oxygen vacancies/defects on the support surface leads to a greater number of Au particles deposited on the $TiO₂$ surface since a single oxygen vacancy can bind three Au atoms on average [27]. Lopez et al. reported that the adhesion energy of gold particles on a defectfree $TiO₂$ surface is negligibly small and defects are required to obtain stable gold particles for gold deposition on rutile-TiO₂ (110) surface, which they have proved using DFT calculations [28]. They proposed that oxygen vacancies contribute towards the interface energy and determine the size and shape of the gold particles along with the number of active sites. In case of plasma sputtering treatment, it was reported that catalytic active species could be distrib-

uted more uniformly when compared to the catalyst prepared without plasma treatment [29]. It can be seen in Fig. 7 that there may be two main possibilities by sputtering plasma: one is that after sputtering plasma, the gold particles can be pressed and increase the contact area, and the second reason is that plasma sputtering can break down the Au particles into small particles; due to that reason, plasma treatment can increase the active sites.

5. Generation of Oxygen Vacancies/Defects by Thermal Treatment

In our study, it is suggested that additional number of gold particles were distributed on the support surfaces by plasma treatment. Therefore, it can be concluded that the enhancement in the catalytic activity of the thermally treated catalysts is attributable to the creation of oxygen vacancies/defects.

To verify the generation of oxygen vacancies/defects sites by thermal treatment, Raman spectra were taken as shown in Fig. 8. In the Raman spectra, the shifts of peak positions to the lower wave numbers were observed for the anatase TiO₂ bands. This result reveals that bond strength between Ti and O increased by the creation of the oxygen vacancies/defects.

Activation of oxygen at interface of Au and support is proposed to be the crucial factor in the synergism of gold and Titania [30]. Therefore, the increase in the CO oxidation activity after oxygen vacancies/defects generation is expected to result partly from the increase in the amount of O_2 adsorption on the Ti O_2 support as shown in Fig. 9. As the amount of O_2 adsorption increases, the amount of active oxygen adsorbed at room temperature for 1 hr. The temperature increased from 30 °C to 500 °C with temperature increasing

Fig. 6. Size distribution histograms of $Au/TiO₂$ catalysts. (a) AuTi-1, (b) AuTi-2, (c) AuTi-3, (d) AuTi-4.

No.	Au (wt%)
$AuTi-1$	0.94
$AuTi-2$	0.95
$AuTi-3$	0.98
AuTi-4	0.99
Plasma Au	Au Au Au Au (a) TiO ₂ (support)
TiO ₂ (support)	Au (b)
	TiO ₂ (support)

Table 1. ICP-AES results of Au/TiO₂ catalysts

Fig. 7. Plasma effect on Au/TiO₂.

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ratio of 10 °C min⁻¹. Two distinctive adsorption sites exist for all catalysts (see Fig. 9). One is a weakly adsorbed site appearing at 120 °C, and the other is a strongly adsorbed site at about 200 °C, because $O₂$ adsorption energy at the interface is higher than at Au [31]. We assigned peaks at 200 °C to O_2 species desorbed from the interface of Au/TiO₂ catalyst. For the AuTi-1 catalyst, the desorption peak at

Fig. 8. Raman spectra of the studied $Au/TiO₂$ catalysts.

200 °C appeared as a shoulder. But for the defected catalysts, this peak can be seen clearly. The amount of strongly adsorbed oxygen species that desorbed above 200 °C increased for the thermal and/ or plasma treated catalysts. It is thought that oxygen species desorbed at higher temperature participate in the CO oxidation reaction on the Au/TiO₂ catalyst. Therefore, the increase in CO oxidation activity after defects generation can be attributed to the increase of ability to adsorb these active oxygen species on $Au/TiO₂$ catalyst, particularly on the interface of Au and TiO₂. Fig. 9 shows the $O₂$ desorption spectra for the AuTi-1 catalyst, when $O₂$ was adsorbed

Fig. 9. Oxygen TPD spectra of Au/TiO₂ catalysts. AuTi-1, AuTi-2, AuTi-3, AuTi-4.

at 30 °C and 100 °C, respectively. The activity differences between catalysts at 100 °C were smaller compared to at room temperature. AuTi-1 catalyst also showed high activity at that temperature. Therefore, it was thought that if $O₂$ was adsorbed at high temperature, the amount of active oxygen species, which desorbs at high temperature, would increase. The increase of the amount of the desorbed $O₂$ at 200 °C in spite of high adsorption temperature means that these are chemisorbed species. It is expected that this species participate in the CO oxidation reaction more actively. On the other hand, AuTi-3 catalysts showed almost the same result regardless of the $O₂$ adsorption temperature. This means that AuTi-3 catalyst has ability to adsorb these active oxygen species on the interface of $Au/TiO₂$ catalyst even at the room temperature.

CONCLUSIONS

Catalytically active $Au/TiO₂$ catalysts were fabricated by DP method. To gain further insight into the role of the defects and gold/ Titania interface in the low temperature oxidation of CO, we created oxygen vacancy/defects by thermal treatment and small gold particles by plasma treatment. After thermal and plasma treatment, catalysts showed better activity than untreated Au/TiO₂ catalysts. The enhancement in the catalytic activity in CO oxidation and preferential oxidation of CO (PROX) can be attributed to an increase in the number of gold particles by plasma treatment and to created oxygen vacancy/defects by thermal treatment. The catalytic activity of the Au/TiO₂ catalysts showed size dependence where higher catalytic activity occurred on smaller gold nanoparticles. The improvement in the catalytic activity of Au/TiO₂ catalysts may be due to increase in the number of gold particles by plasma treatment deposited on TiO₂ surface and the ability to absorb active oxygen in the low temperature by creating oxygen vacancies/defects by thermal treatment.

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