

# A pyrazine based metal-organic framework for selective removal of copper from strongly acidic solutions

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## HIGHLIGHTS

- pz-UiO-66 was synthesized facilely by a solvothermal method.
- Efficient capture of copper from highly acidic solution was achieved by pz-UiO-66.
- pz-UiO-66 exhibited excellent selectivity and capacity for copper capture.
- Pyrazine-N in pz-UiO-66 was shown to be the dominant adsorption site.

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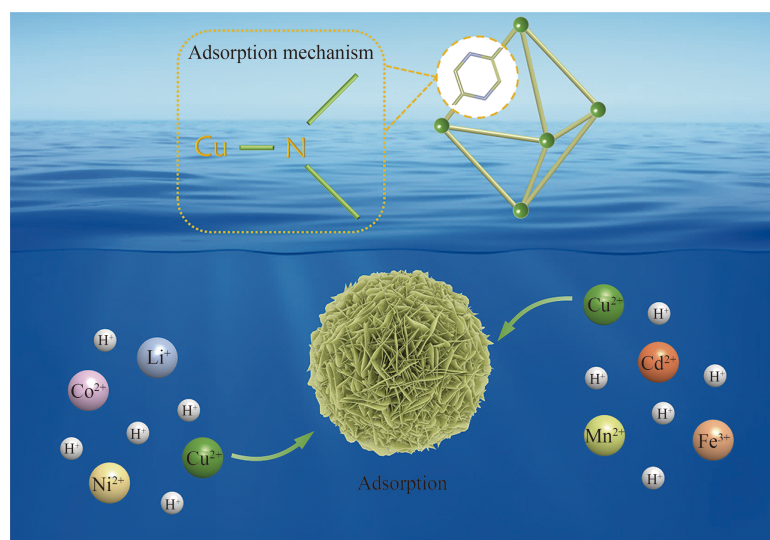
Metal-organic frameworks

Copper removal

Strong acidity

High selectivity

## GRAPHIC ABSTRACT



## ABSTRACT

The selective capture of copper from strongly acidic solutions is of vital importance from the perspective of sustainable development and environmental protection. Metal organic frameworks (MOFs) have attracted the interest of many scholars for adsorption due to their fascinating physicochemical characteristics, including adjustable structure, strong stability and porosity. Herein, pz-UiO-66 containing a pyrazine structure is successfully synthesized for the efficient separation of copper from strongly acidic conditions. Selective copper removal at low pH values is accomplished by using this material that is not available in previously reported metal-organic frameworks. Furthermore, the material exhibits excellent adsorption capacity, with a theoretical maximum copper uptake of 247 mg/g. As proven by XPS and FT-IR analysis, the coordination of pyrazine nitrogen atoms with copper ions is the dominant adsorption mechanism of copper by pz-UiO-66. This work provides an opportunity for efficient and selective copper removal under strongly acidic conditions, and promises extensive application prospects for the removal of copper in the treatment for acid metallurgical wastewater.

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## 1 Introduction

Copper, as a basic mineral element for human health, performs a critical role in enzyme synthesis and bone

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development (Awual, 2019). However, the existence of excess copper is also related to many illnesses, such as cancer, Parkinsonian syndrome and Wilson's disease (Brady et al., 2014; Lee et al., 2016). Moreover, the World Health Organization (WHO) and Environmental Protection Agency (EPA) specify the upper limit concentrations of copper in drinking water of separately 2.0 and 1.3 mg/L (Fitzgerald, 1998). Given the ubiquity of copper in various industries and the negligence of copper-containing wastewater treatment in many industrial countries (Awual, 2019; Bui et al., 2020), maintaining a low concentration of copper ions in water has become the focus of global environmental governance. Therefore, seeking efficient technologies to remove copper from industrial wastewater is urgent. It is noteworthy that research on the selective separation of copper is also limited in the field of acid metallurgical wastewater treatment and urgently needs to be improved. For example, the selective removal of copper from the anodic solution of nickel electrolysis before electrodeposition and the selective separation of copper from acid mine drainages have posed major challenges with respect to metallurgical industry wastewater and a more efficient approach is desired (Chen et al., 2013b; Park et al., 2019).

Various approaches have been applied to separate heavy metals from water media, including but not limited to ion exchange, chemical precipitation and electrochemical methods (Lin et al., 2017; Cao et al., 2019; Shao et al., 2020). Compared with other advanced technologies, adsorption has been proven to be a facile and high-efficiency approach for treating heavy metal ions due to the characteristics of its wide range of application, flexibility in operation, low energy consumption and low maintenance costs (Ai et al., 2016; Peng et al., 2018; Yao et al., 2022). Common adsorbent materials that are effective in removing copper include chelating resins (Chen et al., 2010; Chen et al., 2013a; Kuz'min and Kuz'min, 2014), carbon-based adsorbents (Demiral and Güngör, 2016), porous aromatic frameworks and metal-organic frameworks (MOFs) (Lee et al., 2016; Zhang et al., 2016). Several chelating resins have been investigated for removing copper, such as CEAD (Chen et al., 2013a), D001-PEI and Purolite S930 (Chen et al., 2010; Kuz'min and Kuz'min, 2014), however, all of them exhibit low adsorption capacities. A porous aromatic framework functionalized with thioether, PAF-1-SMe, was demonstrated to be selective and efficient in the extraction of copper from aqueous media as well as biological fluids, but it was specifically designed as a diagnostic tool to detect Wilson's disease (Lee et al., 2016). ZIF-8 was proven to be effective in capturing copper, with a reported uptake of 800 mg/g, establishing it as an effective copper adsorbent, although it was unstable in acidic solutions (Zhang et al., 2016). In general, most of the copper ion trapping materials investigated to date tend to suffer from certain defects,

such as poor selectivity, insufficient capacity, or limited application at low pH; moreover, the synthesis of these materials usually uses expensive reagents that preclude large-scale production. To meet these challenges, one adsorbent with a high adsorption capacity, high selectivity to target ions, stability in strongly acidic solution and relatively fast adsorption kinetics is needed.

MOFs are new porous crystalline materials composed of metal centers connected by organic linkers. They have rich chemical properties and show promising application prospects in adsorption. Compared with traditional inorganic porous materials such as carbon nanotubes and silica, a significant drawback of MOFs is their lower stability. However, zirconium-based MOFs have drawn much attention owing to their outstanding stability compared with other common MOFs, in which strong Zr-O bonds impart remarkable chemical stability, mechanical stability as well as thermal stability (Cavka et al., 2008; Daliran et al., 2020; Zhang et al., 2021). These characteristics give Zr-MOFs excellent application prospects. Therefore, Zr-MOFs were chosen as an ideal candidate material to efficiently adsorb copper from aqueous solution under strongly acidic conditions. In addition, in strongly acidic solution, an extremely high hydrogen ion concentration will affect the ionization state of functional groups on the material, such as carboxyl groups and amino groups, thus affecting the adsorption capacity of the adsorbent. Pyrazine has two nitrogen donor atoms and is a weak base with a pKa value of 0.65. Even in strongly acidic solutions, the protonation of one nitrogen atom greatly reduces the electron cloud density of the other nitrogen atom, making it difficult to be protonated (Miniyar et al., 2013) and thus maintaining its coordination function with metal ions. Consequently, pyrazine nitrogen is used as the functional adsorption site in this study, which enables the functional groups on the material to remain effective at high hydrogen ion concentrations. In general, we take advantage of the highly oxygenophilic capability of Zr<sup>4+</sup> and the stability of Zr-O, and consider the electron-withdrawing effect of pyrazine nitrogen atoms to design a material that can remain stable in strongly acidic solution and whose functional groups are not affected by protonation.

Herein, a Zr-MOF containing a pyrazine structure (pz-UiO-66) was successfully synthesized based on soft and hard acid-base (HSAB) theory and used for the removal of Cu<sup>2+</sup> from strongly acidic wastewater. The successful synthesis of pz-UiO-66 was verified by XRD and FT-IR characterizations and the physical properties and morphology were explored by BET and SEM characterizations. Subsequently, the adsorption performance of pz-UiO-66 for Cu<sup>2+</sup> under strongly acidic conditions and the adsorption selectivity for Cu<sup>2+</sup> were investigated. Additionally, the mechanism of Cu<sup>2+</sup> adsorption by pz-UiO-66 was further explored by XPS analysis.

## 2 Materials and methods

### 2.1 Chemicals

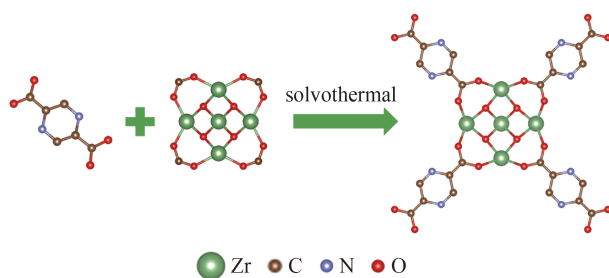
Pyrazine-2,5-dicarboxylic acid ( $H_2PzDC$ , 98 %), benzene-1,4-dicarboxylic acid ( $H_2BDC$ ) and zirconium tetrachloride ( $ZrCl_4$ , 99.5 %) were supplied by J&K Scientific. Anhydrous ethanol ( $CH_3CH_2O$ ,  $\geq 99.7$  %) and  $N, N'$ -dimethylformamide (DMF, 99.5 %) were from Xilong Chemical. Cupric chloride ( $CuCl_2 \cdot 2H_2O$ ), lithium chloride (LiCl), nickel (II) chloride hexahydrate ( $NiCl_2 \cdot 6H_2O$ ), manganese chloride ( $MnCl_2$ ), cobalt (II) chloride hexahydrate ( $CoCl_2 \cdot 6H_2O$ ), cadmium dichloride ( $CdCl_2 \cdot 2.5H_2O$ ) and iron chloride hexahydrate ( $FeCl_3 \cdot 6H_2O$ ) were provided by Silong Chemical and Sinopharm Chemical Reagent. Each metal ion solution was prepared with deionized water which was purified through a Milli-Q water system (Bedford, USA).

### 2.2 Preparation of pz-UiO-66

The synthesis process of pz-UiO-66 is performed in Scheme 1.  $ZrCl_4$  (0.233 g) and  $H_2PzDC$  (0.168 g) were dissolved in  $N, N'$ -dimethylformamide (DMF) (50 mL) and mixed under ultrasound until the mixture was clear. The obtained mixture was then poured into a 100 mL solvent bottle and placed in a 120 °C oven for 24 h. After cooling for a period of time, the crystallization product was filtered, followed by washing several times with DMF to remove the unreacted reagent, washed with ethanol several times to exchange DMF to ethanol, and dried at 60 °C. UiO-66 was prepared by replacing  $H_2PzDC$  with equal molar amounts of  $H_2BDC$ .

### 2.3 Characterization

The morphology characterization of the material was obtained through scanning electron microscopy (SEM) using a Nova Nano SEM450. The crystal structure of the adsorbent was measured based on X-ray diffraction (XRD) using a Bruker AXS with  $Cu K\alpha$  radiation, and recorded in the  $2\theta$  range from 5° to 60° at a scanning speed of 6°/min. Fourier transform infrared (FT-IR) spectrum of the adsorbents were collected at room



**Scheme 1** Schematic diagram of preparation process of pz-UiO-66.

temperature under dry conditions using a Bruker Vertex 70 FTIR (Ettlingen, Germany) spectrophotometer in the 400–4000  $cm^{-1}$  region. The Brunner-Emmett-Teller (BET) surface areas and porosity of the adsorbents were performed using nitrogen adsorption and desorption at 77 K by a F-Sorb 3400 after evacuation at 100 °C for 12 h. X-ray photoelectron spectroscopy (XPS) was taken using a Kratos AXIS ULTRA DLD spectrometer to determine the elemental composition on the sample surface and explore the mechanism of adsorption. Thermogravimetric analysis (TGA) was conducted on the TGA Q600 SDT (New Castle, USA) in a nitrogen atmosphere, with the temperature ranging from 50 °C to 800 °C at a ramping rate of 6 °C/min. Atomic absorption spectrometry (AAS) was applied to determine metal ion concentrations using ContrAA 700 flame atomic absorption spectrophotometer from Analytik Jena, Germany.

### 2.4 Effect of pH on adsorption

To investigate the effect of pH on the copper capture process, solutions comprised of 200 mg/L of  $Cu^{2+}$  were prepared with various pH values (1, 2, 3, 4). In the experiment, 20 mg pz-UiO-66 was added into conical flask containing 50 mL of metal ion solution, and the pH of water media was altered to the desired value by adding dilute sodium hydroxide or hydrochloric acid. Subsequently, the flask containing the solution to be adsorbed was placed in a shaker and reacted at a temperature of 298 K for 12 h at a speed of 180 r/min. After shaking, the solution was treated through a membrane filter of 0.22  $\mu m$ , and the copper ions in the filtered solution were quantified by AAS. The adsorption performance ( $Q_e$ ) for  $Cu^{2+}$  was estimated by Eq. (1):

$$Q_e = \frac{V(C_0 - C_e)}{m}, \quad (1)$$

where  $Q_e$  (mg/L) represents the quantity of adsorbed  $Cu^{2+}$ ,  $C_0$  and  $C_e$  (mg/L) are the original and balanced concentration of  $Cu^{2+}$ , separately,  $m$  (mg) is the weight of adsorbents,  $V$  (mL) is the volume of treated water media.

### 2.5 Selectivity experiment

The co-existed ion ( $Ni^{2+}$ ,  $Co^{2+}$ ,  $Mn^{2+}$ ,  $Li^+$ ,  $Fe^{3+}$ ,  $Cd^{2+}$ ) were carried out to explore the selectivity of pz-UiO-66 toward  $Cu^{2+}$ . The specific adsorption capacity of pz-UiO-66 for  $Cu^{2+}$  in a binary system comprised of  $Cu^{2+}$  and a coexisting ion was investigated firstly. Then, the selectivity of pz-UiO-66 was further analyzed in a multivariate system containing the seven ions mentioned above. All the ion concentrations were 5 mmol/L and the pH of solution was 1. Typically, 20 mg pz-UiO-66 and 50 mL of the above solution were mixed in a conical flask. After 12 h of continuous mixing, the solution was treated through a membrane filter of 0.22  $\mu m$ , and the concentration of  $Cu^{2+}$  in the filtered solutions was determined by AAS.

To further illustrate the selectivity of pz-UiO-66 for  $\text{Cu}^{2+}$ , the experimental results from batch adsorption tests were used to calculate the distribution coefficient ( $K_d$ ) for  $\text{Cu}^{2+}$  uptake using the Eq. (2) below:

$$K_d = 1000 \times \frac{(C_0 - C_e)V}{C_e m}, \quad (2)$$

where  $C_0$  and  $C_e$  (mg/L) are separately the original and balanced concentration of  $\text{Cu}^{2+}$ .

## 2.6 Adsorption tests

The following tests, including adsorption kinetics and isothermal thermodynamics, were conducted at a pH of 1.

The adsorption kinetics of  $\text{Cu}^{2+}$  were examined at 25 °C by adding 200 mg of pz-UiO-66 into a 500 mL water sample with an initial  $\text{Cu}^{2+}$  concentrations of 200 mg/L and the solution were stirred at a constant rate. Equal amounts of the mixed solution were collected at predetermined intervals to confirm the concentration of remaining  $\text{Cu}^{2+}$  ions. The adsorption kinetic data were examined with the pseudo-first-order model (3) and pseudo-second-order model (4, 5) and the models were expressed as below:

$$\ln(Q_e - Q_t) = \ln Q_m - k_1 t, \quad (3)$$

$$\frac{t}{Q_t} = \frac{l}{k_2 Q_m^2} + \frac{t}{Q_m}, \quad (4)$$

$$h_0 = k_2 Q_e^2, \quad (5)$$

where  $Q_t$  (mg/g) is the quantity of adsorbate at  $t$  (min),  $Q_e$  (mg/g) is the copper uptake at equilibrium, and  $k_1$  ( $\text{min}^{-1}$ ), and  $k_2$  ( $\text{g}/(\text{mg} \cdot \text{min})$ ) and  $h_0$  ( $\text{mg}/(\text{g} \cdot \text{min})$ ) are the corresponding rate constants for the pseudo-first-order and second-order models.

Adsorption isotherm experiments were performed by oscillating a mixture containing 20 mg pz-UiO-66 and 50 mL aqueous  $\text{Cu}^{2+}$  solution with initial concentrations of  $\text{Cu}^{2+}$  ranging from 1 to 400 mg/L with a speed of 180 r/min for 12 h to achieve sorption equilibrium at 25 °C. The isothermal test data were processed with the Langmuir (6) and Freundlich (7) models:

$$Q_e = \frac{K_L Q_m C_e}{1 + K_L C_e}, \quad (6)$$

$$Q_e = K_F C_e^{1/n}, \quad (7)$$

where  $C_e$  (mg/L) and  $Q_e$  (mg/g) separately correspond to the concentration of  $\text{Cu}^{2+}$  solution and the amount of adsorbed copper at equilibrium,  $Q_m$  (mg/g) represents the theoretical maximum adsorption capacity,  $K_L$  (L/mg) represents Langmuir constant,  $K_F$  ( $(\text{mg}/\text{g})/(\text{mg}/\text{L})^{1/n}$ ) and  $n$  are ascribed to Freundlich constant.

For the adsorption thermodynamic experiment, 20 mg pz-UiO-66 was added to a conical flask containing 50 mL  $\text{Cu}^{2+}$  solution at a concentration of 200 mg/L and then

agitated in a shaker at 298 K, 308 K and 318 K. The thermodynamic parameters confirmed by the following Eqs. (8) and (9), namely, the standard Gibbs energy change ( $\Delta G^0$ ), enthalpy change ( $\Delta H^0$ ), and entropy change ( $\Delta S^0$ ), can provide insight into the energetic changes associated with the adsorption.

$$\ln K_d = \frac{\Delta S^0}{R} - \frac{\Delta H^0}{RT}, \quad (8)$$

$$\Delta G^0 = -RT \ln K_d, \quad (9)$$

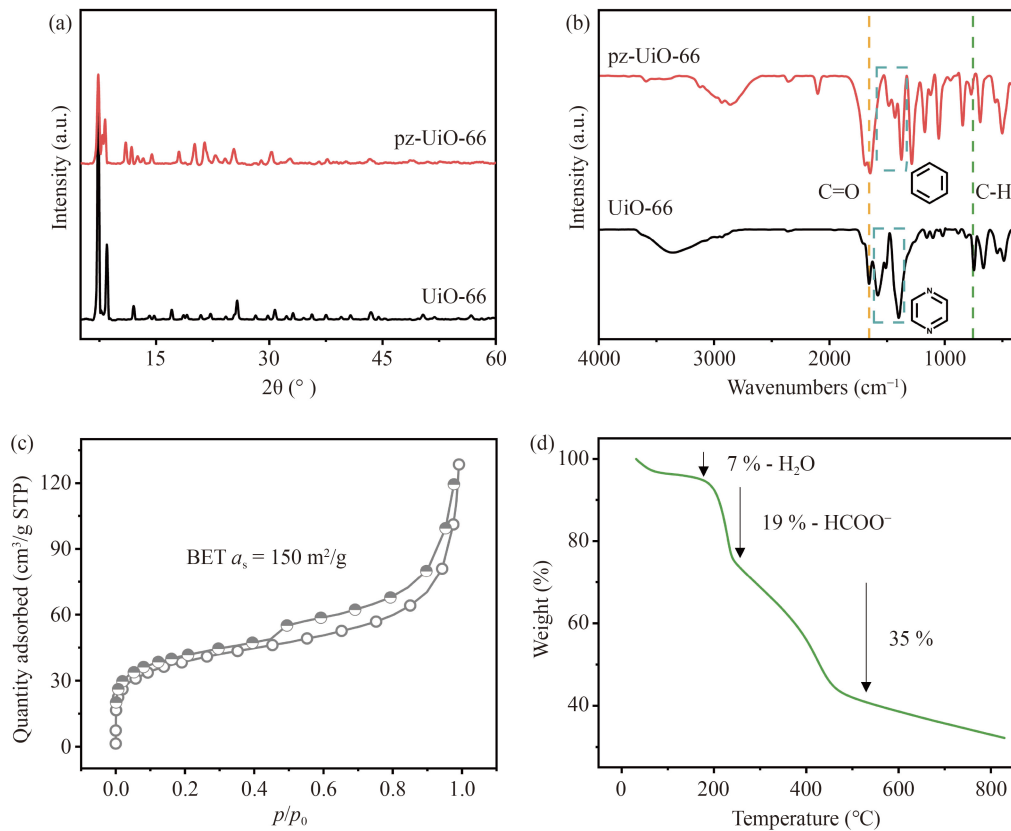
where  $K_d$  (mL/g) is the distribution coefficient of the adsorbates,  $T$  (K) represents the temperature, and  $R$  is the gas constant, respectively.

## 3 Results and discussion

### 3.1 Characterization

The crystalline structure of pz-UiO-66 was characterized using powder X-ray diffraction (XRD). As displayed in Fig. 1(a), the as-synthesized material was highly crystalline and possessed the same structure as UiO-66, while slight peak broadening suggested lower crystallinity than the UiO-66 sample. The morphology and size of the prepared material were imaged through scanning electron microscopy (SEM), as depicted in Fig. S1. It could be observed in Fig. S1(c) that the pz-UiO-66 consisted of flower-like microspheres with rod-like petals and an average diameter of  $\approx 4.5 \mu\text{m}$ . In addition, the uniform distribution of elements on the surface of the material was revealed by EDS analysis (Fig. S2). Fig. 1(b) showed that the FT-IR peaks of the MOF were mainly ascribed to the vibration of the ligand. In UiO-66, the peaks near  $1650 \text{ cm}^{-1}$  were caused by the stretching vibrations of C=O in carboxylic acid groups. The absorption bands at  $1581 \text{ cm}^{-1}$ ,  $1500 \text{ cm}^{-1}$  and  $1402 \text{ cm}^{-1}$  belonged to the vibration absorption of the benzene ring skeleton and the peaks observed at  $757 \text{ cm}^{-1}$  were due to aromatic C-H bending vibrations. The peaks evolved at  $1650 \text{ cm}^{-1}$  and  $750 \text{ cm}^{-1}$  in pz-UiO-66 were consistent with those of UiO-66, and were related to the stretching vibrations of C=O bonds and aromatic C-H bonds, respectively. In addition, the peaks presented at  $1487 \text{ cm}^{-1}$ ,  $1433 \text{ cm}^{-1}$  and  $1381 \text{ cm}^{-1}$  belonged to the stretching vibration absorption of the pyrazine ring skeleton, evidencing that pz-UiO-66 was successfully prepared.

Nitrogen adsorption-desorption isotherms was performed at 77 K to gain insight into the textural properties of pz-UiO-66. As depicted in Fig. 1(c), the isotherms of pz-UiO-66 conformed to the type II isotherm, indicating that pz-UiO-66 had a typical microporous structure. The BET specific surface area of pz-UiO-66 was  $150 \text{ m}^2/\text{g}$ , and the pore volume was  $0.1943 \text{ cm}^3/\text{g}$ . Moreover, the corresponding pore size was  $0.4875 \text{ nm}$ , and the size of the micropores allows the diffusion of copper ions within the



**Fig. 1** XRD patterns (a) and FT-IR spectrum (b) of UiO-66 and pz-UiO-66,  $\text{N}_2$  sorption isotherms (c) and TGA profiles (d) of pz-UiO-66.

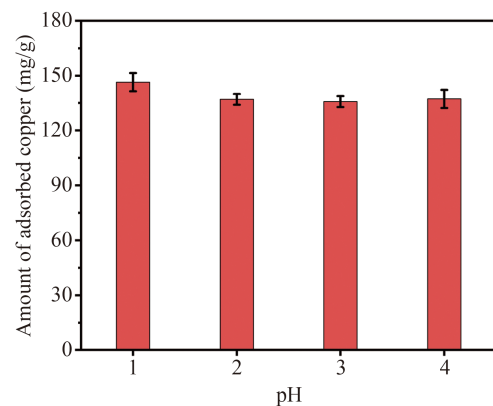
material, bringing functional sites into contact with metal ions (Wang et al., 2019).

To assess the thermal behavior and structural integrity of pz-UiO-66, TGA-DSC curves were collected under a  $\text{N}_2$  atmosphere and presented in Fig. 1(d). The initial loss of less than 10 % occurred at approximately 323 K, which was most likely ascribed to the loss of uncoordinated water. The next step of decomposition is then performed at 200  $^\circ\text{C}$ , likely due to ligand degradation. The final loss could be ascribed to the decomposition of the sample and the last temperature could be considered the upper limit of sample stability, indicating that pz-UiO-66 exhibited good thermal stability.

### 3.2 Effect of pH on adsorption

The pH value of the solution has a significant influence on the adsorption process of copper, because the acidity affects the ionization state of the adsorbent functional groups (Marcus, 1988; Xie et al., 2018). Therefore, the effect of pH on copper capture by pz-UiO-66 was studied. Since copper ions started to precipitate when the pH value was greater than 4.4, in order to prevent copper ions from forming hydroxide precipitates and affecting the adsorption process, the initial solution pH was selected in a suitable range from 1 to 4; within this range, Cu (II)

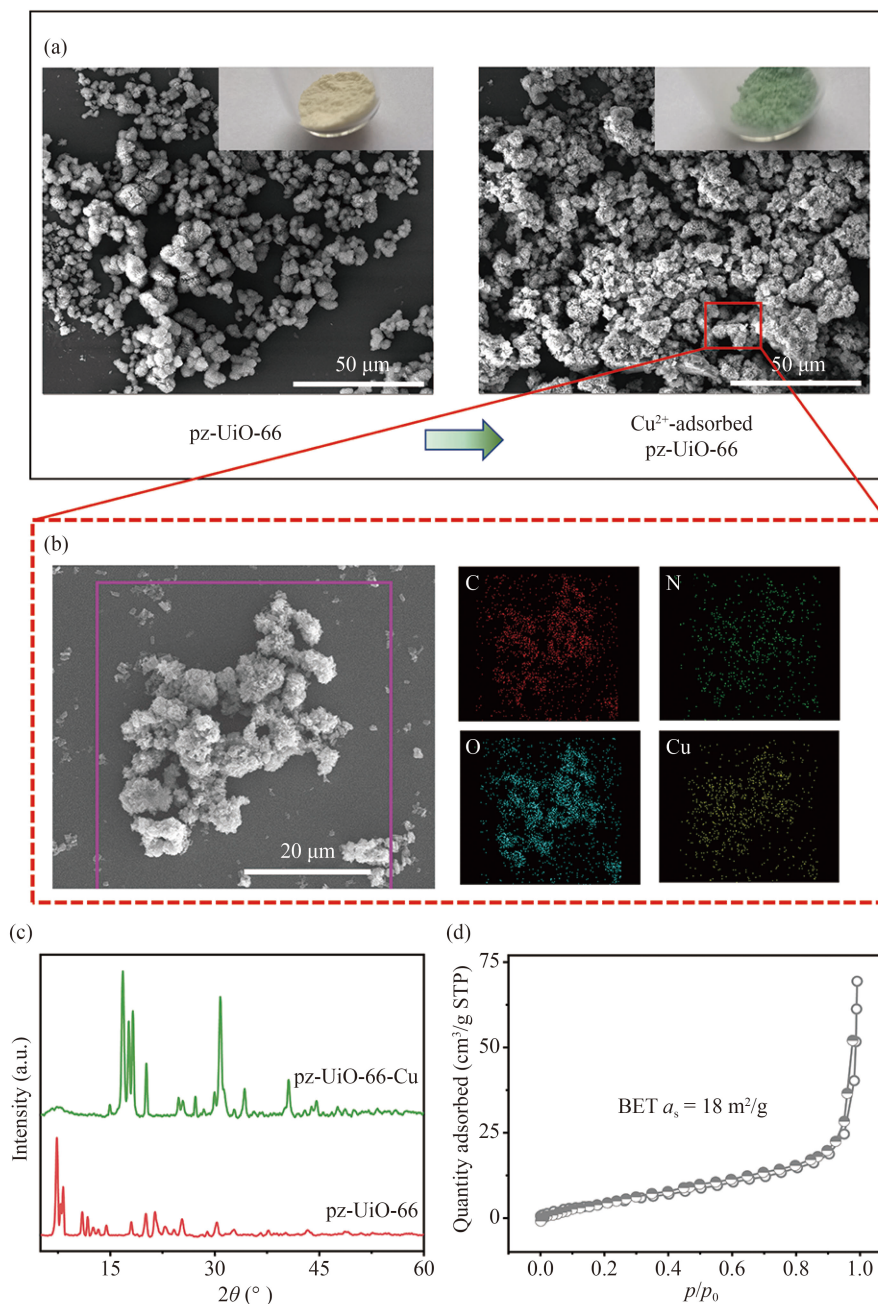
exists in the form of  $\text{Cu}^{2+}$  in aqueous solution (Fig. S4). According to Fig. 2, the adsorption performance of pz-UiO-66 to  $\text{Cu}^{2+}$  was basically the same at pH 1–4, indicating that pz-UiO-66 possessed a strong independence for pH. It was worth noting that the adsorption capacity remained stable even at a strongly acidic pH of 1, which was attributed to the low pKa value of pyrazine in acidic solution, and the pyrazine nitrogen remained deprotonated, thus enabling pz-UiO-66 to adsorb  $\text{Cu}^{2+}$  ions in strongly acidic solutions.



**Fig. 2** Effect of pH on the adsorption of copper ions.

The adsorption process of copper on pz-UiO-66 was observed in Fig. 3(a), and the pz-UiO-66 underwent a color change at the room temperature. It could be seen that the color of pz-UiO-66 changed from off-white to green within the first 10 min during the copper adsorption process. The SEM image of pz-UiO-66 after adsorbing  $\text{Cu}^{2+}$  revealed that it retained a flower-like microsphere structure following 24 h of exposure to  $\text{Cu}^{2+}$ , while the microsphere surface became rougher due to the change of the more thickened petals (Fig. S1(f)). Furthermore, the

elemental mapping images of pz-UiO-66 after capture of  $\text{Cu}^{2+}$  showed an even distribution of copper element on the surface of the adsorbent, manifesting that  $\text{Cu}^{2+}$  was successfully adsorbed on the material (Fig. 3(b)), and the EDS analysis results showed that the content of copper on pz-UiO-66 was slightly lower than the theoretical content, which might be attributed to the blockage of surface pores due to adsorption, resulting in more copper ions being unable to contact the adsorption site. In addition, the PXRD characterization revealed that pz-UiO-66 trans-



**Fig. 3** Transformation of pz-UiO-66 after adsorption: (a) SEM images and optical properties of pz-UiO-66 and pz-UiO-66-Cu, (b) Extended scanning electron microscopy image and energy-dispersive X-ray spectroscopy analysis of pz-UiO-66-Cu, (c) PXRD data for pz-UiO-66 and pz-UiO-66-Cu, (d) N<sub>2</sub> sorption isotherms of pz-UiO-66-Cu.

mitted into a new crystal state after  $\text{Cu}^{2+}$  uptake, which might be due to the formation of new species (Fig. 3(c)). The  $\text{N}_2$  adsorption-desorption isotherm of pz-UiO-66-Cu suggested that the BET surface area of the adsorbed material dropped sharply, which further proved the above speculation (Fig. 3(d)).

### 3.3 Selective adsorption

Given the complexity of actual water environments, the coexistence of metal ions might significantly influence the  $\text{Cu}^{2+}$  uptake efficacy. To validate the application potential of pz-UiO-66, selective adsorption of pz-UiO-66 was performed in solutions composed of  $\text{Cu}^{2+}$ ,  $\text{Li}^+$ ,  $\text{Ni}^{2+}$ ,  $\text{Co}^{2+}$ ,  $\text{Fe}^{3+}$ ,  $\text{Mn}^{2+}$ , and  $\text{Cd}^{2+}$  ions. Notably, as illustrated in Fig. 4, the absorption of  $\text{Cu}^{2+}$  by pz-UiO-66 was much greater than that of other metal ions, or even did not adsorb other metal ions at all, which indicated that most of the binding sites on pz-UiO-66 were preferentially occupied by  $\text{Cu}^{2+}$  ions.

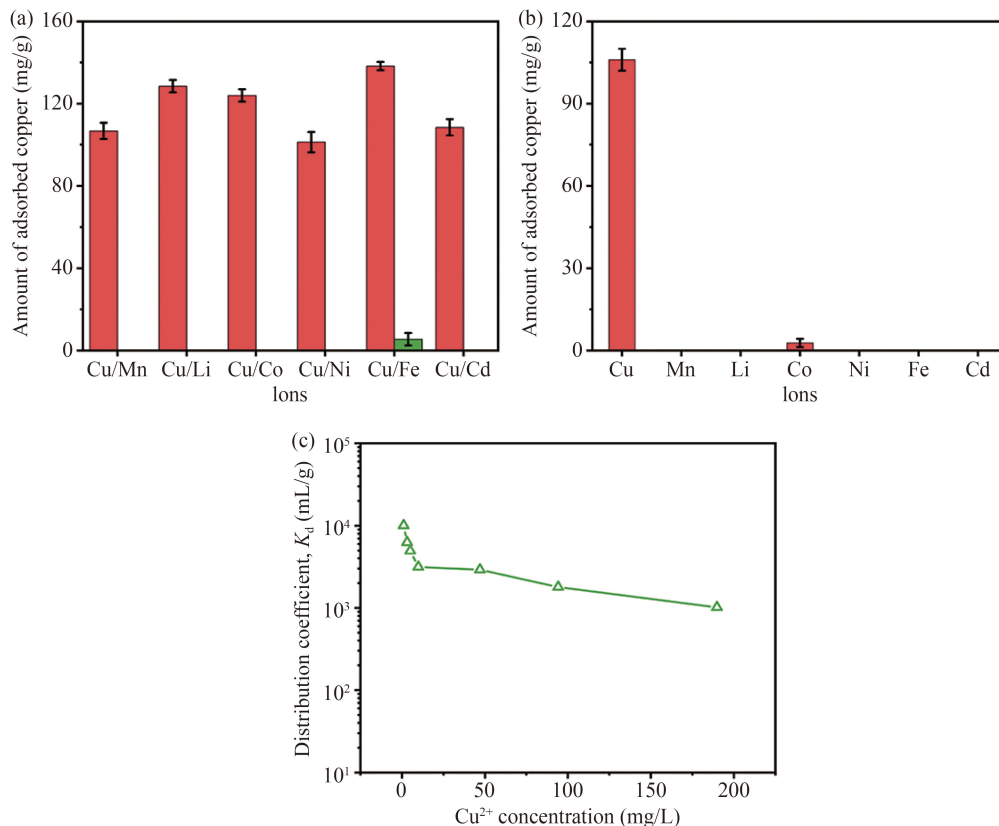
Subsequently, the copper distribution coefficient ( $K_d$ , mL/g) was calculated to further quantitatively assess the selectivity of pz-UiO-66 (Fig. 4(c)). In general,  $K_d$  represents the effectiveness of a sorbent in separating the target species and the selectivity of the sorbent for the species, in which  $K_d > 5000$  is regarded as good and  $K_d$

$\geq 10^4$  is considered excellent. Notably, pz-UiO-66 exhibited  $K_d$  values as high as  $10^4$  at various concentrations of  $\text{Cu}^{2+}$ , indicating that pz-UiO-66 exhibited excellent selectivity for  $\text{Cu}^{2+}$  in strongly acidic solution, which would be beneficial to practical engineering applications.

The excellent selective adsorption of copper ions could be explained through hard-soft-acid-base (HSAB) theory and the stability of transition metal complexes. Pyrazine nitrogen as a borderline Lewis base, tends to form coordination bonds with borderline Lewis acids ( $\text{Cu}^{2+}$ ,  $\text{Ni}^{2+}$ ,  $\text{Co}^{2+}$ ), rather than hard acids ( $\text{Mn}^{2+}$ ,  $\text{Li}^+$ ,  $\text{Fe}^{3+}$ ) or soft acids ( $\text{Cd}^{2+}$ ) (Xu et al., 2020). In addition, the specific adsorption of  $\text{Cu}^{2+}$  among transition metals ( $\text{Cu}^{2+}$ ,  $\text{Ni}^{2+}$ ,  $\text{Co}^{2+}$ ) by pz-UiO-66 could be explained by the stability of transition metal complexes. Considering that copper complexes have higher stability than nickel and cobalt complexes, pyrazine nitrogen adsorption sites might preferentially coordinate with  $\text{Cu}^{2+}$  during solution adsorption (Irving and Williams, 1953). Further adsorption mechanisms are discussed in Section 3.6.

### 3.4 Adsorption isotherms

To further assess the adsorption performance of pz-UiO-66 for  $\text{Cu}^{2+}$ , the isothermal adsorption experiments were



**Fig. 4** Adsorption capacity of pz-UiO-66 for  $\text{Cu}^{2+}$  with coexisting  $\text{Mn}^{2+}$ ,  $\text{Li}^+$ ,  $\text{Co}^{2+}$ ,  $\text{Ni}^{2+}$ ,  $\text{Fe}^{3+}$  and  $\text{Cd}^{2+}$  in binary systems (a) and in a mixed solution composed of seven metal ions (b), distribution coefficients (c) of pz-UiO-66 with respect to  $\text{Cu}^{2+}$  concentration.

carried out over a wide range of copper concentrations, and the results are displayed in Fig. 5(a). The adsorption property of pz-UiO-66 for  $\text{Cu}^{2+}$  augmented as the initial concentration of  $\text{Cu}^{2+}$  rose, and reached a saturated uptake value of 147.5 mg/g at adsorption equilibrium. To better evaluate the adsorption performance of  $\text{Cu}^{2+}$  on pz-UiO-66, the Langmuir and Freundlich models were used to analyze the isotherm adsorption data at 25 °C (Yu et al., 2019), and the relevant parameters were tabulated in Table S3. The Langmuir model was more suitable to express the copper capture process ascribed to its better correlation coefficient, suggesting that the adsorption on pz-UiO-66 was likely monolayer coverage. The fitting data indicated that the expected adsorption capacity of  $\text{Cu}^{2+}$  on pz-UiO-66 was 247 mg/g, slightly exceeding the actual capacity.

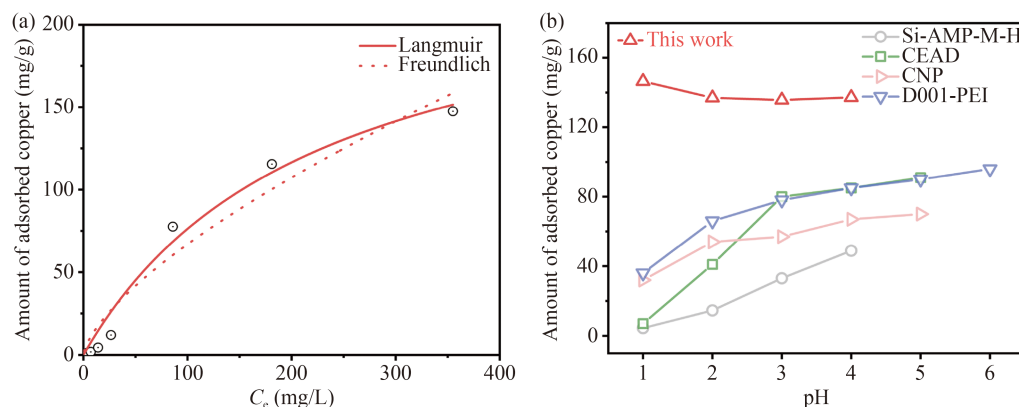
According to HSAB theory, N-functionalized adsorbents usually exhibit a certain adsorption capacity for  $\text{Cu}^{2+}$ , which is accomplished mainly through the formation of coordination bonds between nitrogen atoms and  $\text{Cu}^{2+}$  ions. Herein, the adsorption isotherms of most N-containing adsorbents for  $\text{Cu}^{2+}$  were analyzed. As shown in Fig. 5(b) and Table S4, most N-functionalized adsorbents, such as CEAD, D001-PEI and PLLA nanofibers, showed a maximum copper uptake of less than 2 mmol/g at pH 4-6, and almost no adsorption at pH values less than 2, which was owing to protonation of nitrogen atoms as the concentration of hydrogen ions increases, and the functional groups on the adsorbent could not capture  $\text{Cu}^{2+}$  under strongly acidic conditions. Although some pyridine-functionalized adsorbents exhibited a certain ability to remove  $\text{Cu}^{2+}$  at a pH of 1 or 2, the adsorption capacity of the adsorbents was still less than 0.5 mmol/g. The pz-UiO-66 in this work far outperformed most comparable reported adsorbents, exhibiting superior absorption performance in capturing  $\text{Cu}^{2+}$ . It had a fairly high adsorption capacity and was able to adapt to solutions with low pH values, which was quietly critical for the application of adsorbents for acid

metallurgical wastewater treatment.

### 3.5 Adsorption kinetics and thermodynamics

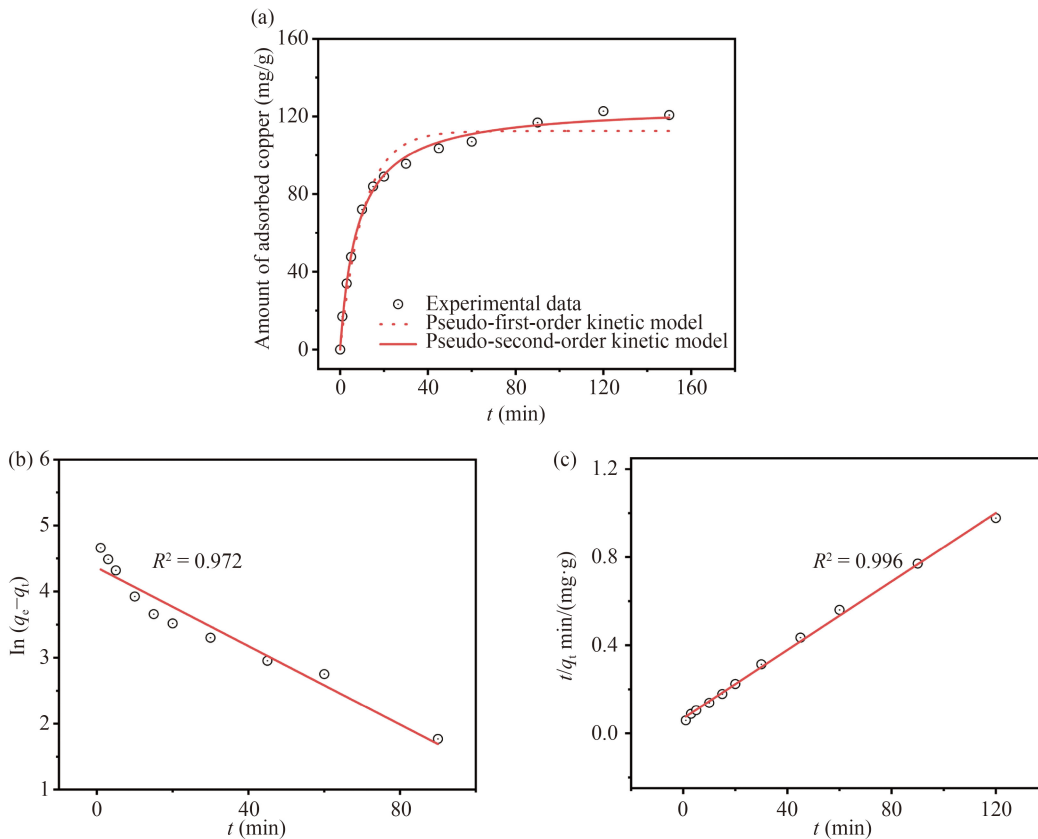
To further explore the adsorption capacity of pz-UiO-66 for  $\text{Cu}^{2+}$ , the adsorption kinetics were performed at a strongly acidic pH of 1. As shown in Fig. 6(a), fast adsorption equilibrium on pz-UiO-66 was achieved within approximately 40 min due to the exposure of more pyrazine nitrogen atoms on the adsorbent surface, and after the rapid adsorption stage, the adsorption rate decreased as the nitrogen atoms used for adsorption tended to become saturated and the final adsorption saturation was achieved within 120 min. To further illustrate the dynamic behavior, pseudo-first- and pseudo-second-order models were applied to describe the kinetics data (Wang et al., 2022), as depicted in Fig. 6, as well as the fitting data listed in Table S5. Both linear fitting curves were displayed in Fig. 6, it was obvious that the pseudo-second-order curve had a better linear fitting compared with the other curve. In addition, from the kinetic parameters, the fitting of the pseudo-first-order model ( $R^2 = 0.972$ ) reflected a lower correlation coefficient than that of the pseudo-second-order model ( $R^2 = 0.996$ ), and the fitting value  $Q_m$  of the pseudo-second-order dynamics equation had a small deviation from the experimental data. This showed that the pseudo-second-order kinetic model was better than the first-order kinetic model for characterizing the copper capture process by pz-UiO-66, suggesting that chemical adsorption showed a dominant function in the adsorption process of  $\text{Cu}^{2+}$  by pz-UiO-66 (Choudhary et al., 2020).

To gain insight into the possible mechanisms involved in the removal process, the thermodynamics of adsorption were investigated. The adsorption data of pz-UiO-66 for copper at different temperatures were presented in Fig. 7 (a). The amount of adsorbed  $\text{Cu}^{2+}$  ions by pz-UiO-66 improved slightly with increasing temperature, as did the

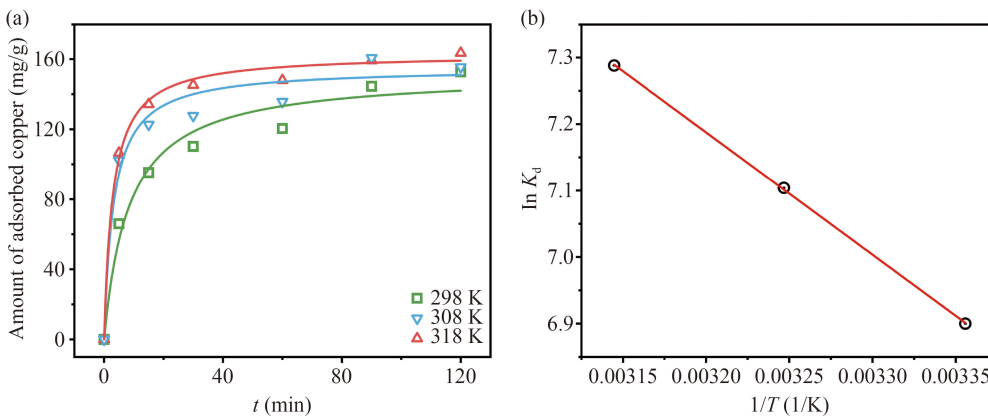


**Fig. 5** Adsorption isotherms (a) for pz-UiO-66 fitted by Langmuir model and Freundlich model and comparative plot (b) of the effect of pH on copper adsorption for pz-UiO-66 and other copper ion sorbents.





**Fig. 6** Adsorption kinetics data and fitting curves (a), pseudo-first order (b) and pseudo-second order (c) plots of pz-UiO-66 for the adsorption of  $\text{Cu}^{2+}$ .



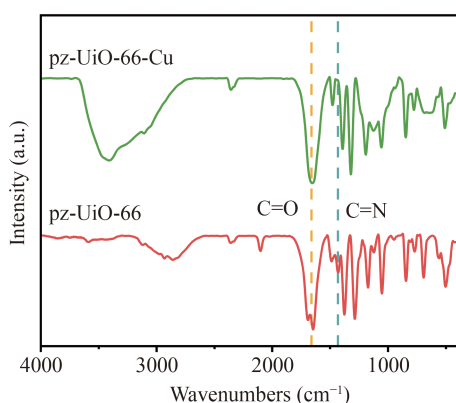
**Fig. 7** Adsorption thermodynamics data (a) and plot of  $\ln K_d$  vs.  $1/T$  (b) for the adsorption of  $\text{Cu}^{2+}$  by pz-UiO-66.

adsorption rate, indicating that the effect of temperature on the adsorption performance was positively correlated. The van't Hoff graph, presented in Fig. 7(b), was plotted as  $\ln K_d$  relative to  $1/T$  to calculate the thermodynamic parameters and the results were summarized in Table. S6. The value of  $\Delta H^\circ$  for  $\text{Cu}^{2+}$  was positive, suggesting that the adsorption of  $\text{Cu}^{2+}$  by pz-UiO-66 was an endothermic process and driven by chemical reactions. The value of  $\Delta S^\circ$  was positive, implying that the randomness at the

interface between the adsorbent and liquid was enhanced during the removal process. The negative value of  $\Delta G^0$  means that the reaction process could be spontaneous, which proved the feasibility of  $\text{Cu}^{2+}$  adsorption. Notably, the absolute value of  $\Delta G^0$  increased as the temperature rose. As previously reported, a more negative  $\Delta G^0$  is more conducive to a positive reaction (Jiang et al., 2019). Consequently, the adsorbent exhibited better adsorption performance for  $\text{Cu}^{2+}$  at 318 K.

### 3.6 Adsorption mechanism

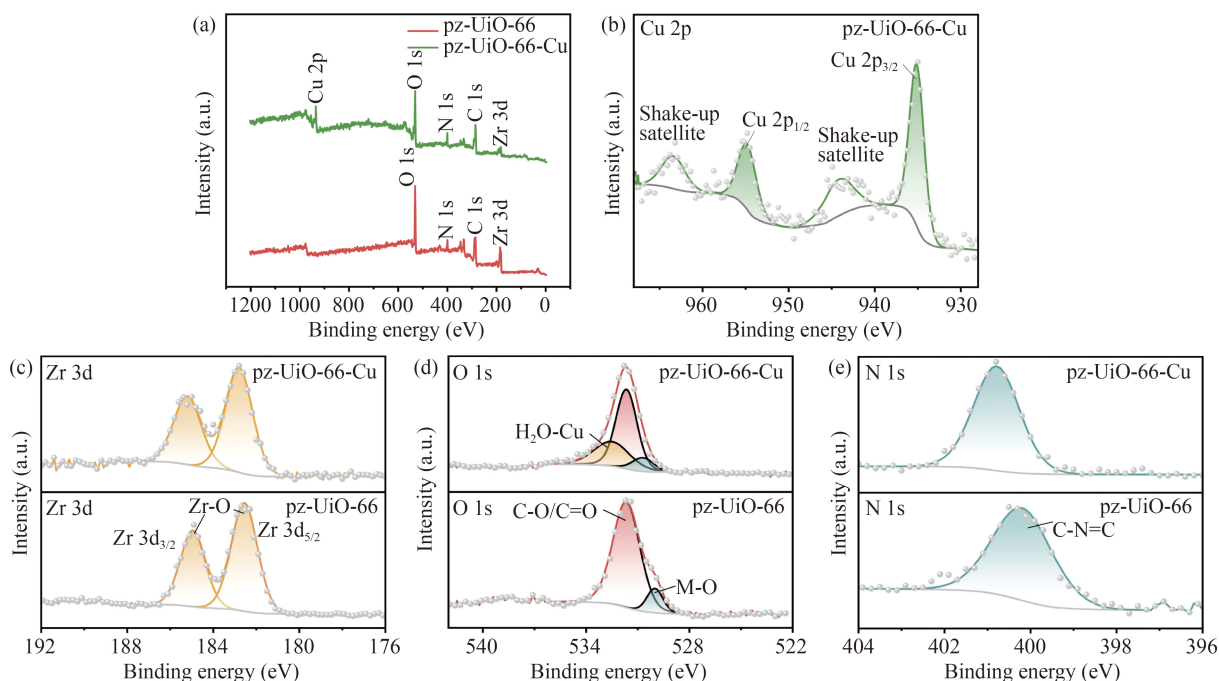
To gain insight into the mechanisms leading to copper ion uptake in pz-UiO-66, FT-IR was applied to analyze the changes in the adsorption sites of pz-UiO-66 before and after the adsorption of copper ions, with the results presented in Fig. 8. It could be observed that the adsorption band at  $2901\text{ cm}^{-1}$  belonged to stretching vibration of C-H on the pyrazine ring and the characteristic peaks near  $1487\text{ cm}^{-1}$ ,  $1430\text{ cm}^{-1}$  and  $1380\text{ cm}^{-1}$  were assigned to the skeletal vibration of pyrazine, all of which were associated with pz-UiO-66. It was noteworthy that the appearance of a new peak at  $3410\text{ cm}^{-1}$  was ascribed to the stretching vibration of O-H after copper adsorption, which may be attributed to water molecules



**Fig. 8** FTIR spectrum of pz-UiO-66 before and after  $\text{Cu}^{2+}$  capture.

(Hosseinpournajjar et al., 2022). Moreover, the stretching vibration peak of pyrazine at  $1432\text{ cm}^{-1}$  was significantly weakened and almost disappeared, which might be because pyrazine in pz-UiO-66 formed coordination bonds with copper, thus successfully adsorbing copper. The results showed that the process of pz-UiO-66 trapping copper ions was mainly through coordination interactions.

X-ray photoelectron spectroscopy (XPS) spectra were analyzed to further reveal the coordination interaction of pz-UiO-66 with copper ions, and the chemical composition of pz-UiO-66 before and after  $\text{Cu}^{2+}$  capture was determined. As displayed in Fig. 9(a), the corresponding regions of Zr 3d, O 1s, C 1s, and N 1s were clearly characterized in the measured scanning spectrum, and the presence of Cu 2p in the spectrogram after adsorption indicated that  $\text{Cu}^{2+}$  was successfully captured by pz-UiO-66, which was consistent with the SEM results. To be specific, the Cu 2p spectrum was analyzed, as presented in Fig. 9(b); the binding energies of 935.1 eV and 954.8 eV could be responsible for Cu  $2p_{3/2}$  and Cu  $2p_{1/2}$ , respectively, and the satellite peaks of 944.2 eV and 963.4 eV could be ascribed to the presence of  $\text{Cu}^{2+}$  species (Feng et al., 2016). The Zr 3d spectra in Fig. 9(c) showed two obvious peaks at 184.95 eV and 182.55 eV during the adsorption process, indicative of Zr  $3d_{3/2}$  and Zr  $3d_{5/2}$ , respectively, but these two peaks shifted to 185.2 eV and 182.8 eV after the adsorption of copper, and spectra of O 1s were shown in Fig. 9(d), giving a shift of M-O (M = metal) from 530 eV to 530.7 eV, manifesting that Zr nodes might also be involved in the adsorption process of



**Fig. 9** XPS characterization of pz-UiO-66 before and after  $\text{Cu}^{2+}$  adsorption: (a) full spectrum, (b) Cu 2p, (c) Zr 3d, (d) O 1s and (e) N 1s.

copper ions. It could be speculated that a small number of defects in pz-UiO-66 itself combine with copper ions to form Zr-O-Cu bonds, leading to the above deviation in binding energy (Ma et al., 2022). In addition, the peak at 532 eV in the O 1s spectrum corresponded to the oxygen of hydroxyl groups in water molecule, which agreed with the conclusion of the infrared analysis. It was reported that the coordination sites with metal ions resulted in a shifting of the binding energy of coordination atoms to higher values, which was attributed to the electron donating/accepting ability of the metal ions (Wang et al., 1997). As depicted in Fig. 9(e), the N spectrum of pz-UiO-66-Cu showed that the N 1s binding energy of pz-UiO-66 on pyrazine nitrogen shifted from 400.2 eV to 400.8 eV after copper adsorption, indicating that this site was of vital importance for copper ion adsorption. According to the above XPS analysis, it could be concluded that pz-UiO-66 combines with  $\text{Cu}^{2+}$  ions by the coordination of pyrazine nitrogen atoms in the material and the interaction of zirconium nodes in the skeleton.

In addition, UiO-66 prepared by the same method was used as a contrast adsorbent to conduct copper adsorption experiments to prove the key role of pyrazine nitrogen atoms. In the experiments, 20 mg of the two adsorbents was separately added to 50 mL  $\text{Cu}^{2+}$  solution with a pH of 1. As shown in Fig. S5, after two h of adsorption, the adsorption capacity of UiO-66 was less than 20 mg/g, accounting for only 1/7 that of pz-UiO-66, which further indicates that the coordination of pyrazine nitrogen atoms is necessary and plays a dominant role in copper capture.

## 4 Conclusions

In summary, a pyrazine structured metal-organic framework was successfully synthesized by a solvothermal method, for the selective capture of copper from highly acidic solutions. pz-UiO-66 achieved effective adsorption and separation selectivity of  $\text{Cu}^{2+}$  at ultralow pH compared with other reported materials, even in mixed solutions of multiple metal ions. Furthermore, the strong Zr-O bonds and pyrazine functional groups enabled the material to maintain structural stability and adsorption capacity in highly acidic solutions. The FTIR and XPS spectra proved that the main adsorption mechanism is the coordination between pyrazine nitrogen atom and copper. Consequently, pz-UiO-66 provides a more feasible and efficient approach for the selective removal of copper from complex metal ion solutions even under highly acidic conditions.

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