

Pressure transient analysis for a fractured well in a stress-sensitive tight multi-medium oil reservoir

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Abstract Tight multi-medium oil reservoirs are the main source of hydrocarbon resources around the world. Acid fracturing is the most effective technology to improve productivity in such reservoirs. As carbonates are primarily composed of dolomite and calcite, which are easily dissolved by hydrochloric acid, high-permeability region will be formed near the well along with the main artificial fracture when acid fracturing is implemented in tight multi-medium oil reservoirs. In this study, a comprehensive composite linear flow model was developed to simulate the transient pressure behavior of an acid fracturing vertical well in a naturally fractured vuggy carbonate reservoir. By utilizing Pedrosa's substitution, perturbation, Laplace transformation and Stehfest numerical inversion technology, the pressure behavior results were obtained in real time domain. Furthermore, the result of this model was validated by comparing with those of previous literature. Additionally, the influences of some prevailing parameters on the type curves were analyzed. Moreover, the proposed model was applied to an acid fracturing well to evaluate the effectiveness of acid fracturing measures, to demonstrate the practicability of the proposed model.

Keywords tight multi-medium oil reservoir, acid fracturing, stress-sensitive permeability, composite linear flow

1 Introduction

Tight multi-medium oil reservoirs are widely distributed around the world, and numerous studies have been conducted on this type of reservoirs (Kossack and Gurpinar, 2001; Kang et al., 2006; Wang et al., 2018a; Xing et al., 2018; Xu et al., 2019). In the last few decades,

many scholars noticed the distinctive pore structure and fluid flow mechanism in carbonate reservoirs, where matrix, natural fractures and vugs coexist in naturally fractured vuggy reservoirs. This renders it complicated and intractable to characterize reservoirs accurately. Generally, matrix and vuggy pores act as storage spaces for hydrocarbon fluids, whereas fractures are usually considered as a pathway for fluid flow. Furthermore, vuggy pores can be subdivided as connected and disconnected with natural fractures. This means that fluid in the vug can flow into fracture directly or indirectly via the bridge of matrix.

Due to complex pore types, it is challenging to model fluid flow through tight multi-medium oil reservoirs. After decades of researches, scholars have put forward some effective methods to tackle this problem. Abdassah and Ershaghi (1986) first proposed triple-porosity/single-permeability model. In their model, and unsteady-state interporosity flow between fracture and other systems was considered in their model. Later, Liu et al. (2003) proposed a tri-continuum medium concept considering pseudo-steady interporosity flow. Wu et al. (2006 and 2007) developed an analytical method for transient flow analysis in tight multi-medium oil reservoirs, taking the flow between vug and matrix into consideration. Camacho-Velázquez et al. (2002) established a triple-porosity/dual-permeability model to consider primary flow not only through fracture system to wellbore, but also vugs system to wellbore. Subsequently, Fuentes-Cruz et al. (2004) extended the model to partially penetrated well. Yao et al. (2010) established the discrete fracture-vug network model and provided to describe fluid flow in the fractured-vuggy porous media. Wu et al (2019) applied the discrete fracture-vug model proposed by Yao et al. (2010) to model macrovugs, while microfractures and microvugs are modeled with the triple-continuum concept. Guo et al. (2012) established a test analysis model of a horizontal well, and triple porosity and dual permeability flow

behavior were analyzed. Their results showed that type curves were dominated by external boundary conditions as well as the permeability ration of fracture system to the sum of fracture and matrix systems.

In order to reduce flow resistance meanwhile extract hydrocarbon resources in carbonate formations effectively, acid fracturing has been the predominant technology (Abass et al., 2006). Thus, it is significant and attractive to understand the flow behavior of acid fracturing wells in tight multi-medium oil reservoirs. Generally speaking, carbonate minerals are composed of dolomite and calcite which are easy to be dissolved by hydrochloric acid. Therefore, acid fracturing can not only act as “hydraulic fracturing”, but also act as acidification to create different types of wormholes (Fredd, 2000; Dora, 2008; Liu et al., 2013). As for the pressure dynamics analysis for acid fracturing wells in tight multi-medium oil reservoirs, great efforts have been made in the last several years. Wang et al. (2014) developed a theoretical wormhole seepage model for the first time. In this model, wormholes are simplified as multi-branched fractures with an infinite conductivity. Later, a semi-analytical model that derives from the previous one to investigate the pressure behavior for finite conductivity multi-branched fractures in fractured-vuggy reservoirs in detail was also suggested by Wang et al. (2018b). Wang and Yi (2017) studied the flow behavior of a well with a finite-conductivity fracture in a tight multi-medium oil reservoir. In their study, the vugs were are conceptualized as spherical shapes and seven flow regimes were are observed. Recently, Wang et al. (2018b) investigated the flow behavior of acid fracturing wells in a composite fractured-vuggy carbonate reservoirs. Lei et al. (2018) presented an analytical solution considering the heterogeneity of the pore networks in acidized region by the utility of the fractal geometry theory.

It is reported that some tight multi-medium oil reservoirs may exhibit strong stress-sensitive characteristic, which has a significant effect on transient pressure behavior (Zhang et al., 2017; Yang et al., 2017). Yet, the aforementioned researches haven't taken this factor into consideration. Moreover, all of their wok were based on the assumption that the fracture is completely penetrated in the vertical direction. Unfortunately, to be our best knowledge, fracture may be partially penetrated in actual acid fracturing implementations. With regard to partially penetrating fractured well, many researchers (Raghavan et al., 1978; Rodriguez et al., 1984; Igbokoyi and Tiab, 2008; Zhang et al., 2015; Yuan et al., 2018) developed point/slab source functions and numerical methods to deal with it respectively. However, numerical methods are complex and time-consuming. Compared with numerical simulation, composite linear flow model can solve the problem of single vertically fractured well or multi-stage fractured horizontal well conveniently. Simultaneously, it also avoids the time-consuming process in numerical simulation and the complexity of Green function methods

(Brown et al., 2009; Stalgorova and Matter, 2012; Tao et al., 2018; Zeng et al., 2018; Zeng et al., 2017).

In this study, we investigate an acid fracturing vertical well in a rectangular fractured-vuggy carbonate reservoir, and the acidized region is also rectangular. Besides, the artificial fracture can be either fully or partially penetrated. The Pedrosa's perturbation (Pedrosa, 1986) is utilized to linearize the non-linear equations caused by stress-sensitive permeability. The physical model and relevant assumptions would be elaborated in Section 2. In Section 3, the mathematical model is established and the corresponding solution is given by Laplace transformation and Stehfest inversion technology (Stehfest, 1970). The model verification and parameters sensitivity analysis are presented in Section 4. Finally, some remarkable conclusions are drawn in Section 5.

2 Physical model

As shown in Fig. 1, a single fractured vertical well is located in the center of a tight multi-medium oil reservoir. The reservoir is modeled as triple-porosity medium while the main artificial fracture is modeled as single-porosity medium. As for the triple-porosity medium, natural fractures act as the main pathways, while vug and matrix provide the storage space. The inter-porosity flow is assumed to be in pseudo-steady state, and the process is shown in Fig. 2. The main artificial fracture formed by acid fracturing is symmetric and it partially penetrates the formation in both vertical and horizontal directions. There is an acidized region with lots of wormholes near the main artificial fracture. Slightly compressible fluid with constant viscosity is produced at a fixed rate through the well. For the sake of simplification, some of other tenable assumptions are elaborated as following:

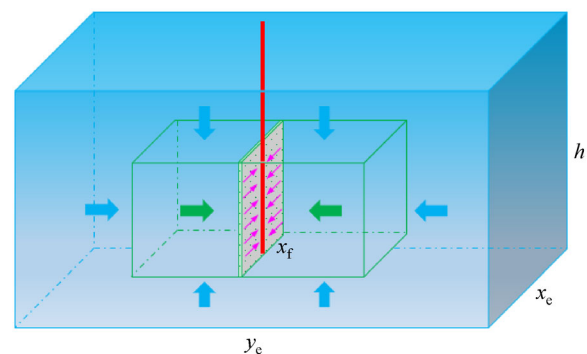


Fig. 1 Schematic of an acid fracturing well in a fractured-vuggy carbonate reservoir.

1) The reservoir is horizontal with uniform thickness of h , and the reservoir pressure is p_i at the beginning time of production and the gradient is uniformly distributed;

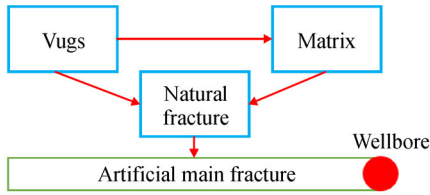


Fig. 2 Physical modelling sketch map of tight multi-medium.

- 2) The upper and bottom boundaries of reservoir are impermeable, and external boundary is also closed;
- 3) Main artificial fracture and natural fractures in regions 1 to 6 possess stress-sensitive permeability and it can be described as the following formula:

$$k_f = k_{fi} e^{-\alpha(p_i - p_f)}, \quad (1)$$

where k_f denotes fracture permeability at current pressure; k_{fi} denotes fracture permeability at initial pressure; α refers to permeability modulus; p_i and p_f refer to initial pressure and fracture pressure.

4) The continuity conditions of pressure and flux at the interfaces are used to connect the adjacent flow regions.

5) Isothermal and Darcy flow process is assumed while the gravity and capillary pressure are ignored.

3 Mathematical model and solution

Based on the aforementioned assumption that the hydraulic fracture is symmetrical both in horizontal and vertical direction, one-quarter of the rectangular carbonate reservoir is implemented to simplify the problem. The system is divided into seven regions as shown in Fig. 3, and the shape of each region presents approximately rectangular.

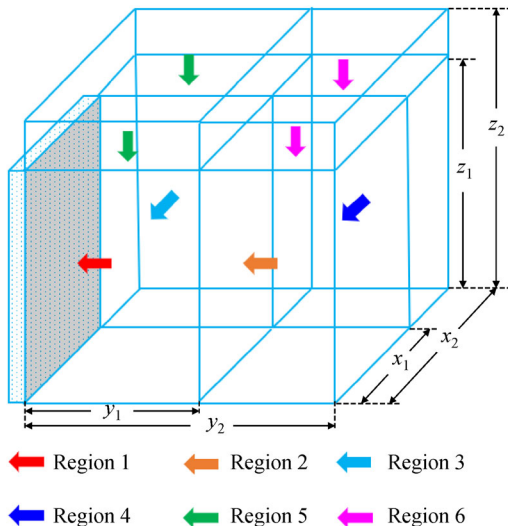


Fig. 3 Physical modeling sketch map of tight multi-medium.

3.1 Flow in regions without acidification (Region 2 + Region 3 + Region 4 + Region 5 + Region 6)

Region 6

In Region 6, considering the effect of stress sensitivity, the governing equations in dimensionless form can be written as

$$e^{-\alpha_D p_{6D}} \left[\frac{\partial^2 p_{6fD}}{\partial z_D^2} - \alpha_D \left(\frac{\partial p_{6fD}}{\partial z_D} \right)^2 \right] = \frac{1}{\eta_{6D}} \left[\omega_{6f} \frac{\partial p_{6fD}}{\partial t_D} + \omega_{6m} \frac{\partial p_{6mD}}{\partial t_D} + \omega_{6v} \frac{\partial p_{6vD}}{\partial t_D} \right], \quad (2)$$

$$\omega_{6m} \frac{1}{\eta_{6D}} \frac{\partial p_{6mD}}{\partial t_D} + \lambda_{6fm} (p_{6mD} - p_{6fD}) - \lambda_{6vm} (p_{6vD} - p_{6mD}) = 0, \quad (3)$$

$$\omega_{6v} \frac{1}{\eta_{6D}} \frac{\partial p_{6mD}}{\partial t_D} + \lambda_{6fv} (p_{6vD} - p_{6fD}) - \lambda_{6vm} (p_{6vD} - p_{6mD}) = 0, \quad (4)$$

where, α is permeability modulus, MPa^{-1} ; ω is storativity ratio, dimensionless; η is diffusivity coefficient, MPa^{-1} ; λ is interporosity flow coefficient, dimensionless; f is natural fracture property; m is matrix property; v is vug property; p is reservoir pressure, MPa ; t is time; e is Euler number; D is dimensionless.

Dimensionless parameters in Eqs. (2)–(4) are defined in Appendix A.

The initial condition is

$$p_{6fD} = p_{6mD} = p_{6vD} = 0. \quad (5)$$

The outer boundary condition (no-flow) is

$$\left. \frac{\partial p_{6D}}{\partial z_D} \right|_{z_D=z_{2D}} = 0, \quad (6)$$

where z is distance.

Based on pressure continuity, the inner boundary condition is given as

$$p_{6D}|_{z_D=z_{1D}} = p_{2D}|_{z_D=z_{1D}} = p_{4D}|_{z_D=z_{1D}}. \quad (7)$$

With Pedrosa-substitution (Pedrosa, 1986), perturbation and Laplace transformation methods (detailed derivations are in Appendix B), we can obtain

$$\begin{aligned} \left. \frac{\partial \tilde{\xi}_{6D}}{\partial z_D} \right|_{z_{1D}} &= \tilde{\xi}_{2D}(z_{1D}) \sqrt{\frac{sg_6(s)}{\eta_{6D}}} \tanh \left[\sqrt{\frac{sg_6(s)}{\eta_{6D}}} (z_{1D} - z_{2D}) \right] \\ &= \tilde{\xi}_{4D}(z_{1D}) \sqrt{\frac{sg_6(s)}{\eta_{6D}}} \tanh \left[\sqrt{\frac{sg_6(s)}{\eta_{6D}}} (z_{1D} - z_{2D}) \right]. \end{aligned} \quad (8)$$

where s is dimensionless time variable in Laplace domain, dimensionless; ξ is a variable after Pedrosa's substitution; \sim is laplace transform; h is formation height, m.

Region 5

Analogously, the governing equations of Region 5 in dimensionless form can be written as

$$e^{-\alpha_D p_{5D}} \left[\frac{\partial^2 p_{5D}}{\partial z_D^2} - \alpha_D \left(\frac{\partial p_{5D}}{\partial z_D} \right)^2 \right] = \frac{1}{\eta_{5D}} \left[\omega_{5f} \frac{\partial p_{5D}}{\partial t_D} + \omega_{5m} \frac{\partial p_{5mD}}{\partial t_D} + \omega_{5v} \frac{\partial p_{5vD}}{\partial t_D} \right], \quad (9)$$

$$\omega_{5m} \frac{1}{\eta_{5D}} \frac{\partial p_{5mD}}{\partial t_D} + \lambda_{5fm} (p_{5mD} - p_{5fD}) - \lambda_{5vm} (p_{5vD} - p_{5mD}) = 0, \quad (10)$$

$$\omega_{5v} \frac{1}{\eta_{5D}} \frac{\partial p_{5vD}}{\partial t_D} + \lambda_{5fv} (p_{5vD} - p_{5fD}) - \lambda_{5vm} (p_{5vD} - p_{5mD}) = 0. \quad (11)$$

The initial condition is

$$p_{5fD} = p_{5mD} = p_{5vD} = 0. \quad (12)$$

The outer boundary condition (no-flow) is

$$\left. \frac{\partial p_{5fD}}{\partial z_D} \right|_{z_D=z_{2D}} = 0. \quad (13)$$

Based on pressure continuity, the inner boundary condition is given as

$$p_{5fD} \Big|_{z_D=z_{1D}} = p_{1fD} \Big|_{z_D=z_{1D}} = p_{3fD} \Big|_{z_D=z_{1D}}. \quad (14)$$

After eliminating the nonlinearity by applying the Pedrosa substitution, the solution of Region 5 can be obtained as following:

$$\begin{aligned} \left. \frac{\partial \tilde{\xi}_{5D}}{\partial z_D} \right|_{z_{1D}} &= \tilde{\xi}_{1D}(z_{1D}) \sqrt{\frac{sg_5(s)}{\eta_{5D}}} \tanh \left[\sqrt{\frac{sg_5(s)}{\eta_{5D}}} (z_{1D} - z_{2D}) \right] \\ &= \tilde{\xi}_{3D}(z_{1D}) \sqrt{\frac{sg_5(s)}{\eta_{5D}}} \tanh \left[\sqrt{\frac{sg_5(s)}{\eta_{5D}}} (z_{1D} - z_{2D}) \right]. \end{aligned} \quad (15)$$

Region 4

In Region 4, the flow is in x and z directions, and the governing equations considering the effect of stress sensitivity in dimensionless form can be written as

$$e^{-\alpha_D p_{4D}} \left[\frac{\partial^2 p_{4D}}{\partial x_D^2} + \frac{\partial^2 p_{4D}}{\partial z_D^2} - \alpha_D \left(\frac{\partial p_{4D}}{\partial x_D} \right)^2 - \alpha_D \left(\frac{\partial p_{4D}}{\partial z_D} \right)^2 \right]$$

$$= \frac{1}{\eta_{4D}} \left[\omega_{4f} \frac{\partial p_{4fD}}{\partial t_D} + \omega_{4m} \frac{\partial p_{4mD}}{\partial t_D} + \omega_{4v} \frac{\partial p_{4vD}}{\partial t_D} \right], \quad (16)$$

$$\omega_{4m} \frac{1}{\eta_{4D}} \frac{\partial p_{4mD}}{\partial t_D} + \lambda_{4fm} (p_{4mD} - p_{4fD}) - \lambda_{4vm} (p_{4vD} - p_{4mD}) = 0, \quad (17)$$

$$\omega_{4v} \frac{1}{\eta_{4D}} \frac{\partial p_{4vD}}{\partial t_D} + \lambda_{4fv} (p_{4vD} - p_{4fD}) - \lambda_{4vm} (p_{4vD} - p_{4mD}) = 0. \quad (18)$$

The no-flow outer boundary in x direction is

$$\left. \frac{\partial p_{4fD}}{\partial x_D} \right|_{x_{2D}} = 0. \quad (19)$$

The pressure continuity condition between Region 4 and Region 2 on the interface is

$$p_{4fD} \Big|_{x_D=x_{1D}} = p_{2fD} \Big|_{x_D=x_{1D}}. \quad (20)$$

Based on the definite conditions, the solution of Region 4 can be written as

$$\left. \frac{\partial \tilde{\xi}_{4D}}{\partial x_D} \right|_{x_{1D}} = \tilde{\xi}_{2D}(x_{1D}) \sqrt{\alpha_4} \tanh[\sqrt{\alpha_4}(x_{1D} - x_{2D})]. \quad (21)$$

Region 3

In Region 3, the flow is in x and z directions, and the governing equations considering the effect of stress sensitivity in dimensionless form can be written as

$$\begin{aligned} e^{-\alpha_D p_{3D}} \left[\frac{\partial^2 p_{3D}}{\partial x_D^2} + \frac{\partial^2 p_{3D}}{\partial z_D^2} - \alpha_D \left(\frac{\partial p_{3D}}{\partial x_D} \right)^2 - \alpha_D \left(\frac{\partial p_{3D}}{\partial z_D} \right)^2 \right] \\ = \frac{1}{\eta_{3D}} \left[\omega_{3f} \frac{\partial p_{3fD}}{\partial t_D} + \omega_{3m} \frac{\partial p_{3mD}}{\partial t_D} + \omega_{3v} \frac{\partial p_{3vD}}{\partial t_D} \right], \end{aligned} \quad (22)$$

$$\omega_{3m} \frac{1}{\eta_{3D}} \frac{\partial p_{3mD}}{\partial t_D} + \lambda_{3fm} (p_{3mD} - p_{3fD}) - \lambda_{3vm} (p_{3vD} - p_{3mD}) = 0, \quad (23)$$

$$\omega_{3v} \frac{1}{\eta_{3D}} \frac{\partial p_{3vD}}{\partial t_D} + \lambda_{3fv} (p_{3vD} - p_{3fD}) - \lambda_{3vm} (p_{3vD} - p_{3mD}) = 0. \quad (24)$$

The no-flow outer boundary in x direction is

$$\left. \frac{\partial p_{3fD}}{\partial x_D} \right|_{x_{2D}} = 0. \quad (25)$$

The pressure continuity condition between Region 3 and Region 1 on the interface is

$$p_{3fD}|_{x_D=x_{1D}} = p_{1fD}|_{x_D=x_{1D}}. \quad (26)$$

Based on the definite conditions, the solution of Region 3 can be written as

$$\left. \frac{\partial \tilde{\xi}_{3D}}{\partial x_D} \right|_{x_{1D}} = \tilde{\xi}_{1D}(x_{1D})\sqrt{\alpha_3}\tan h[\sqrt{\alpha_3}(x_{1D}-x_{2D})]. \quad (27)$$

Region 2

In Region 2, the flow is in x , y and z directions, and the governing equations considering the effect of stress sensitivity in dimensionless form can be written as

$$e^{-\alpha_D p_{2fD}} \left[\frac{\partial^2 p_{2fD}}{\partial y_D^2} + \frac{\partial^2 p_{2fD}}{\partial x_D^2} + \frac{\partial^2 p_{2fD}}{\partial z_D^2} - \alpha_D \left(\frac{\partial p_{2fD}}{\partial y_D} \right)^2 - \alpha_D \left(\frac{\partial p_{2fD}}{\partial x_D} \right)^2 - \alpha_D \left(\frac{\partial p_{2fD}}{\partial z_D} \right)^2 \right] = \frac{1}{\eta_{2D}} \left[\omega_{2f} \frac{\partial p_{2fD}}{\partial t_D} + \omega_{2m} \frac{\partial p_{2mD}}{\partial t_D} + \omega_{2v} \frac{\partial p_{2vD}}{\partial t_D} \right], \quad (28)$$

$$\omega_{2m} \frac{1}{\eta_{2D}} \frac{\partial p_{2mD}}{\partial t_D} + \lambda_{2fm}(p_{2mD} - p_{2fD}) - \lambda_{2vm}(p_{2vD} - p_{2mD}) = 0, \quad (29)$$

$$\omega_{2v} \frac{1}{\eta_{2D}} \frac{\partial p_{2mD}}{\partial t_D} + \lambda_{2fv}(p_{2vD} - p_{2fD}) - \lambda_{2vm}(p_{2vD} - p_{2mD}) = 0. \quad (30)$$

The no-flow outer boundary in y direction is

$$\left. \frac{\partial p_{2fD}}{\partial y_D} \right|_{y_{2D}} = 0. \quad (31)$$

The pressure continuity condition between Region 2 and Region 1 on the interface is

$$p_{2fD}(y_{1D}) = p_{1fD}(y_{1D}), \quad (32)$$

$$\left. \frac{\partial \tilde{\xi}_{2fD}}{\partial y_D} \right|_{y_{1D}} = \tilde{\xi}_{1fD}(y_{1D})\sqrt{\alpha_2}\tan h[\sqrt{\alpha_2}(y_{1D}-y_{2D})]. \quad (33)$$

3.2 Flow in acidized region (Region 1)

In Region 1, the flow is also in x , y and z directions, and the governing equations considering the effect of stress sensitivity in dimensionless form can be written as

$$e^{-\alpha_D p_{6fD}} \left[\frac{\partial^2 p_{6fD}}{\partial y_D^2} + \frac{\partial^2 p_{6fD}}{\partial x_D^2} + \frac{\partial^2 p_{6fD}}{\partial z_D^2} - \alpha_D \left(\frac{\partial p_{6fD}}{\partial y_D} \right)^2 \right.$$

$$\left. + -\alpha_D \left(\frac{\partial p_{6fD}}{\partial x_D} \right)^2 - \alpha_D \left(\frac{\partial p_{6fD}}{\partial z_D} \right)^2 \right] = \frac{1}{\eta_{6D}} \left[\omega_{6f} \frac{\partial p_{6fD}}{\partial t_D} + \omega_{6m} \frac{\partial p_{6mD}}{\partial t_D} + \omega_{6v} \frac{\partial p_{6vD}}{\partial t_D} \right]. \quad (34)$$

The solution of region 1 can be obtained as

$$\left. \frac{\partial \tilde{\xi}_{1D}}{\partial y_D} \right|_{\frac{w_D}{2}} = -\beta_2 \tilde{\xi}_{FD} \left(\frac{w_D}{2} \right), \quad (35)$$

where

$$\beta_2 = \frac{\sqrt{\alpha_1} \exp \left[-\sqrt{\alpha_1} \frac{w_D}{2} \right] - \beta_1 \exp \left[\sqrt{\alpha_1} \frac{w_D}{2} \right]}{\exp \left[-\sqrt{\alpha_1} \frac{w_D}{2} \right] + \beta_1 \exp \left[\sqrt{\alpha_1} \frac{w_D}{2} \right]}, \quad (36)$$

$$\beta_1 = \exp \left[-\sqrt{\alpha_1} 2y_{1D} \right]$$

$$\frac{\left(k_{1f,h} \sqrt{\alpha_1} + k_{2f,h} \sqrt{\alpha_2} \tan h \left[\sqrt{\alpha_2} (y_{1D} - y_{2D}) \right] \right)}{\left(k_{1f,h} \sqrt{\alpha_1} - k_{2f,h} \sqrt{\alpha_2} \tan h \left[\sqrt{\alpha_2} (y_{1D} - y_{2D}) \right] \right)}, \quad (37)$$

where w is wellbore property; β is intermediate variable; FD is dimensionless fracture conductivity.

3.3 Flow in artificial main fracture

In the main artificial fracture, the single-porosity model is applied. Thus, the diffusivity equation can be written as

$$\frac{\partial^2 p_{FD}}{\partial x_D^2} + \frac{\partial p_{FD}}{\partial y_D} = \frac{1}{\eta_{FD}} \frac{\partial p_{FD}}{\partial t_D}. \quad (38)$$

The boundary conditions in x direction are

$$\left. \frac{\partial p_{FD}}{\partial x_D} \right|_{x_{1D}} = 0, \quad (39)$$

$$\left. \frac{\partial p_{FD}}{\partial x_D} \right|_{x_{1D}} = 0 \left. \frac{\partial p_{FD}}{\partial x_D} \right|_0 = \frac{\pi}{F_{CD}}, \quad (40)$$

where F_{CD} is dimensionless artificial fracture conductivity, dimensionless.

Therefore, the pressure solution for fracture region is

$$\tilde{\xi}_{FD} = \frac{\pi \cosh \left[\sqrt{\alpha_F} (x_D - x_{1D}) \right]}{s F_{CD} \sqrt{\alpha_F} \sinh \left[\sqrt{\alpha_F} (x_{1D}) \right]}. \quad (41)$$

Set $x_D=0$, we can obtain the final solution for well bottom-hole pressure in Laplace domain as following

$$\tilde{\xi}_{wD} = \frac{\pi}{s F_{CD} \sqrt{\alpha_F} \tan h \left[\sqrt{\alpha_F} (x_{1D}) \right]}. \quad (42)$$

According to the Duhamel and superposition theory, the dimensionless well bottomhole pressure responses incorporating wellbore storage and skin effect in Laplace domain can be written as follows:

$$\tilde{\xi}_{wD}(s, C_D, S_c) = \frac{S_c + s\tilde{\xi}_{wD}}{s + C_D s^2 (s\tilde{\xi}_{wD} + S_c)}, \quad (43)$$

where C_D denotes dimensionless wellbore storage coefficient; S_c denotes skin factor.

Finally, the well bottomhole pressure can be obtained by the following equation:

$$p_{wD} = -\frac{1}{\alpha_D} \ln(1 - \alpha_D \tilde{\xi}_{wD}). \quad (44)$$

4 Results and discussion

4.1 Model verification

In order to verify the proposed model, the results obtained by this model and by trilinear flow model in the reference (Brown et al., 2009) are compared with. Let $g(s)$ equal to 1, y_{1D} equal to y_{2D} and z_{1D} equal to z_{2D} to make the two models the same. In addition, skin factor is not considered in this case. Some other relevant parameters are presented in Table 1.

Figure 4 presents a log/log plot of dimensionless pressure and pressure derivatives vs. dimensionless time solved by the two model. As we can see, the results obtained by this model shows good agreement with the trilinear flow model, which demonstrates the accuracy of this model.

Table 1 Basic dimensionless parameters for model validation

Parameters	Value
Dimensionless acidized main fracture half-length, x_{1D}	1
Dimensionless acidized main fracture half-width, w_D	0.000001
Dimensionless acidized main fracture conductivity, F_{CD}	1.2
Dimensionless acidized region half-width, y_{1D}	10
Dimensionless acidized region half-height, z_{1D}	10
Dimensionless reservoir half-length, x_{2D}	8
Dimensionless reservoir half-width, y_{2D}	10
Dimensionless reservoir half-height, z_{2D}	10
Dimensionless wellbore storage coefficient, C_D	0.1

4.2 Flow regimes recognition

In order to obtain the transient pressure type curves, a series of parameters are set as listed in Table 2, and the corresponding type curves are shown in Fig. 5. There are

Table 2 Basic dimensionless parameters for flow regimes recognition

Parameters	Value
Dimensionless acidized main fracture half-length, x_{1D}	1
Dimensionless acidized main fracture half-width, w_D	0.000001
Dimensionless acidized main fracture conductivity, F_{CD}	0.8
Dimensionless acidized region half-width, y_{1D}	1
Dimensionless acidized region half-height, z_{1D}	8
Dimensionless reservoir half-length, x_{2D}	8
Dimensionless reservoir half-width, y_{2D}	10
Dimensionless reservoir half-height, z_{2D}	10
Dimensionless wellbore storage coefficient, C_D	0.1

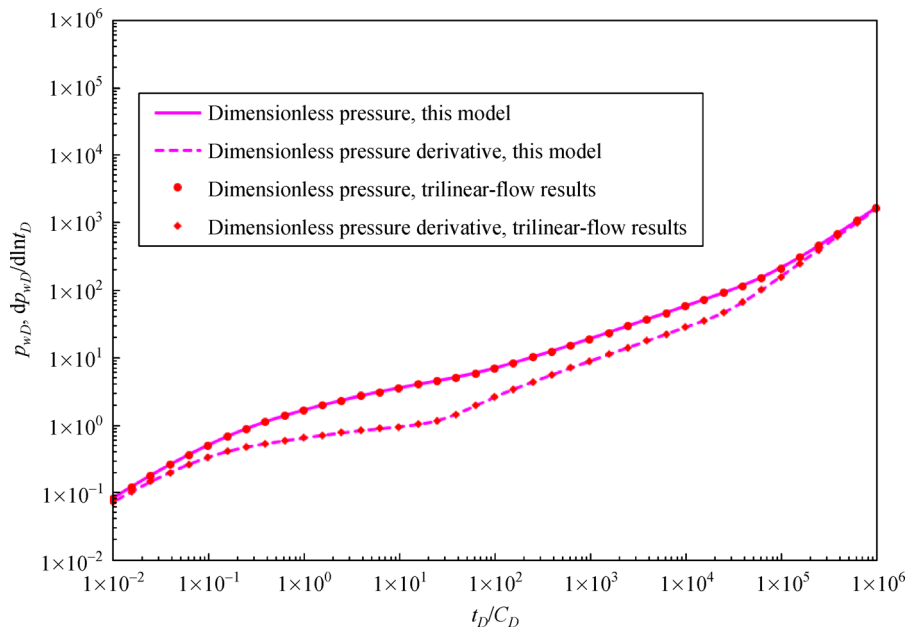


Fig. 4 Comparison of the results between this model and trilinear-flow method.

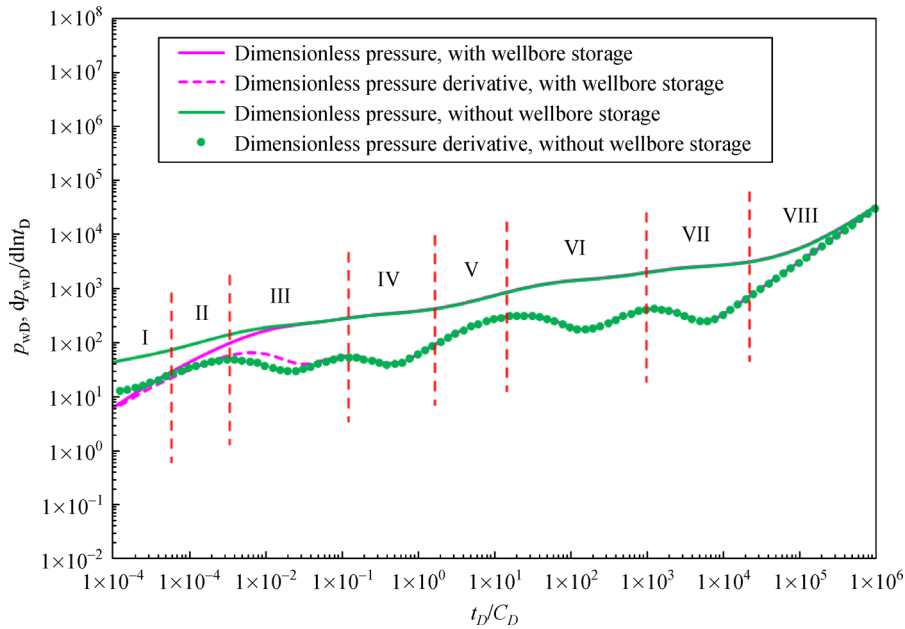


Fig. 5 Pressure type curves of an acid fracturing well in a tight multi-medium oil reservoir.

eight flow regimes can be observed as following respectively from Fig. 5.

Regime I: bilinear flow in artificial fracture and in the acidized region (Region 1). The pressure derivative curve’s slope is 1/4 in the regime;

Regime II: first linear flow in the acidized region. The pressure derivative curve shows a straight line with a slope of 1/2;

Regime III: interporosity flow from vug system to natural fracture system in acidized region;

Regime IV: interporosity flow from matrix system to natural fracture system and from vug system to matrix system in acidized region;

Regime V: second linear flow from un-acidized region to acidized region. The pressure derivative curve shows a straight line with a slope of 1/2;

Regime VI: interporosity flow from vug system to natural fracture system in un-acidized region;

Regime VII: interporosity flow from matrix system to natural fracture system and from vug system to matrix system in un-acidized region;

Region VIII: pseudo-steady flow (boundary-dominated flow).

4.3 Parameters analysis

4.3.1 Effect of fracture conductivity

Figure 6 shows the effect of fracture conductivity on dimensionless pressure and pressure derivative. It can be seen that fracture conductivity mainly influences the type curves at the early stage. The greater the fracture

conductivity is, the smaller the dimensionless pressure is. It means that lower flow resistance in the artificial main fracture. It can also be seen that the bilinear flow stage disappears when fracture conductivity equals to 10, and the “concaves” in the third and fourth flow regimes have an apparent “dip”, which indicates that fracture conductivity has a significant influence on the pressure behavior of acidized region.

4.3.2 Effect of permeability modulus

Figure 7 illustrates the effect of permeability modulus on transient pressure behavior. As shown in the picture, stress permeability has an apparent impact on the type curves in the late time period. The greater the permeability modulus is, the faster the permeability decreases and it leads to larger pressure consumption at the same production. As the permeability modulus increases from 0.00009 to 0.00019, the boundary dominated flow shifts to an early time.

4.3.3 Effect of the coefficient of interporosity flow between matrix and vug system

Figure 8 depicts the effect of coefficient of cross-flow from vug to fracture on transient pressure behavior. As is known, the coefficient of interporosity flow from vug to fracture in acidized region represents permeability ratio of the vug system in the fracture system. Therefore, a large value of λ_{fv1} denotes a high permeability of vug and leads to an early occurrence of first interporosity flow stage. As Fig. 8 shows, the first interporosity flow stage advances with the increase of the parameter λ_{fv1} . It can also be seen

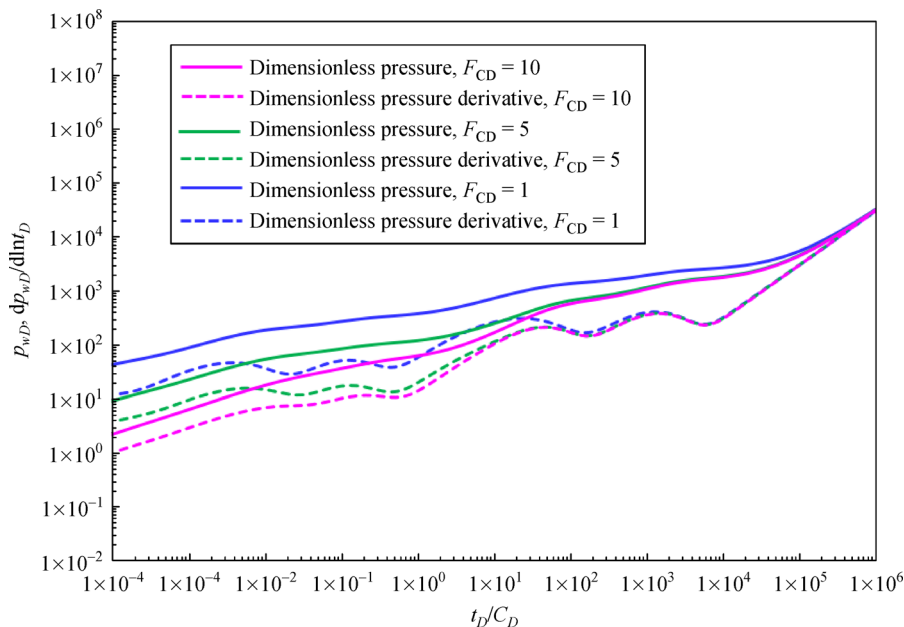


Fig. 6 The effect of fracture conductivity on transient pressure behavior.

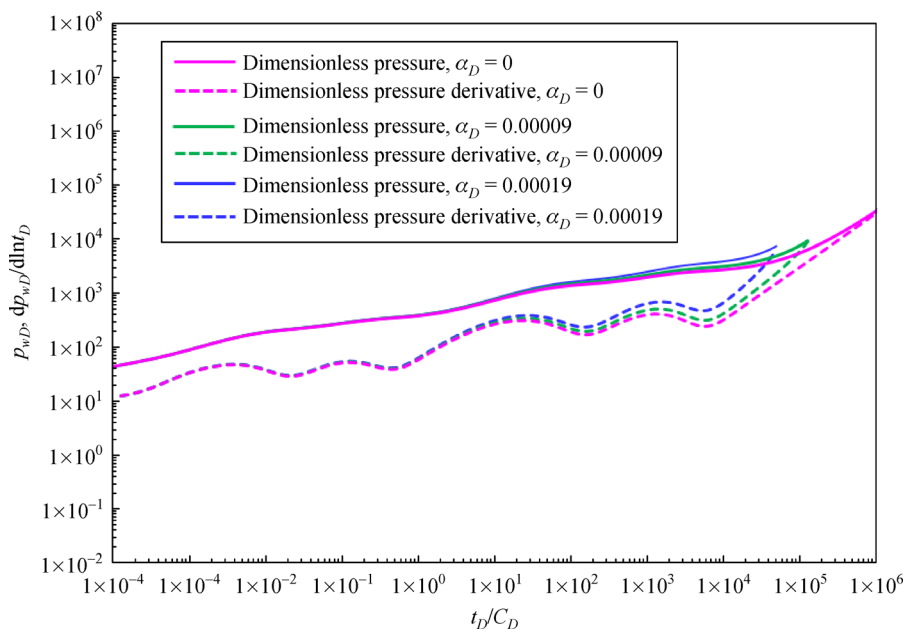


Fig. 7 The effect of permeability modulus on transient pressure behavior.

that a bigger will pose a smaller pressure depletion because dimensionless pressure curve descends as parameter λ_{f1} increases from 0.1 to 1.

4.3.4 Effect of storativity ratio of natural fracture in acidized region

Figure 9 shows the effect of storage ratio of natural fracture system in Region 1 on the flow regimes. The natural

fracture storativity ratio refers to the ratio of the fluid storing volume in natural fracture system to the total capacity of fluid storing in the reservoir. Furthermore, it reflects the fracture growth level as well, so it can be called fracture intensity as well. Similar to the coefficient of interporosity flow from vug to fracture, storativity ratio of natural fracture in acidized region mainly takes effect during the first interporosity flow stage as well. The smaller the parameter ω_{f1} is, the lower the first V-segment becomes.

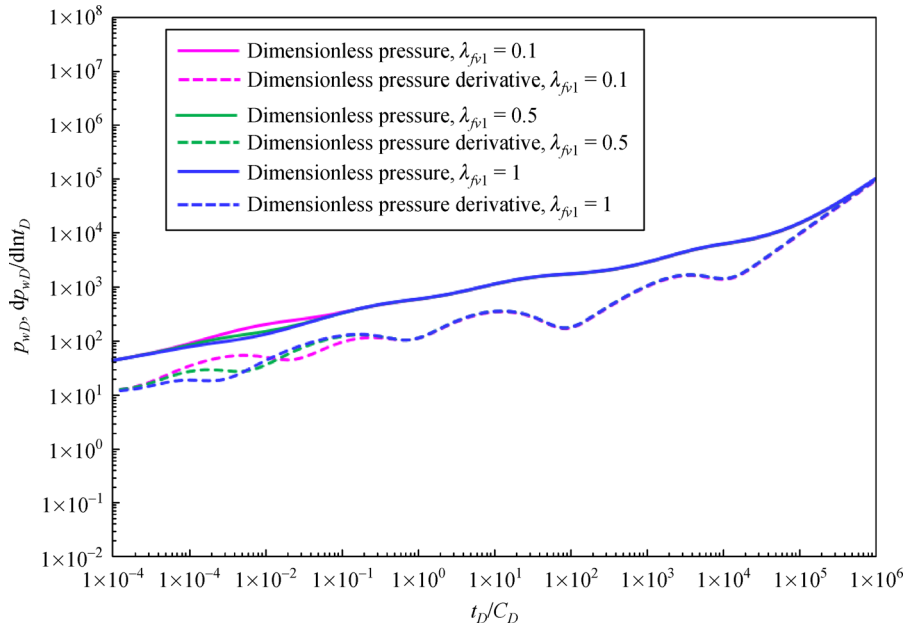


Fig. 8 The effect of interporosity flow coefficient on transient pressure behavior.

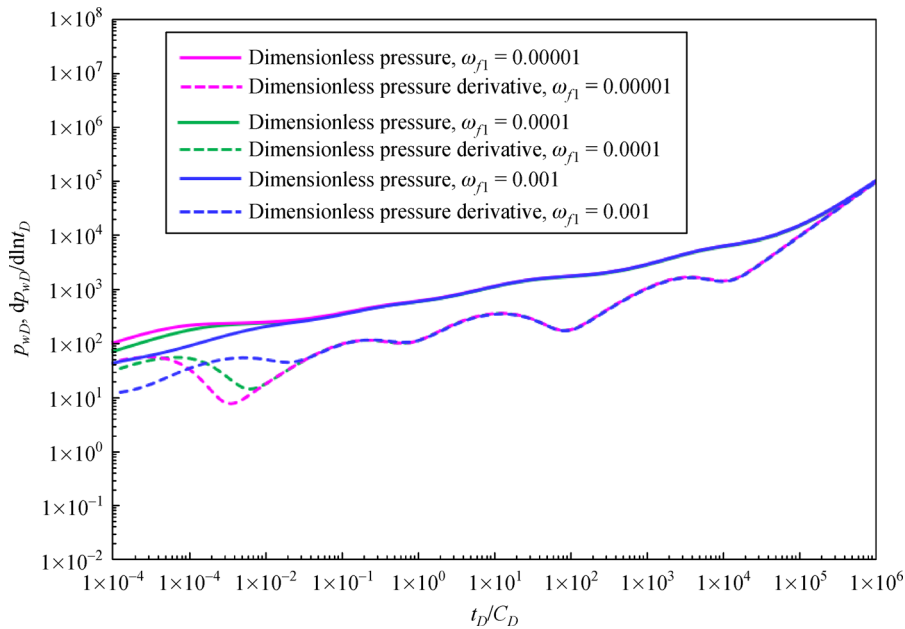


Fig. 9 The effect of storativity ratio on transient pressure behavior.

4.3.5 Effect of width of acidized region

To investigate the width of acidized region separately, the length of acidized region is considered as a constant. Figure 10 indicates the effect of the width of acidized region on the transient pressure behavior. As shown in Fig. 10, the interporosity flow in acidized region happens later with the increasing of the width of acidized region, while the interporosity flow in unacidized region happens earlier. Meanwhile, the larger the size of acidized region is,

the lower the dimensionless pressure curve falls, and the fact implies that engineer should try to enlarge the volume of acidized region to reduce the flow obstacle and improve well productivity.

4.3.6 Effect of reservoir size

Figure 11 displays the effect of the reservoir size on the transient pressure behavior. As is shown in the figure, the dimensionless pressure decreases especially in the late time

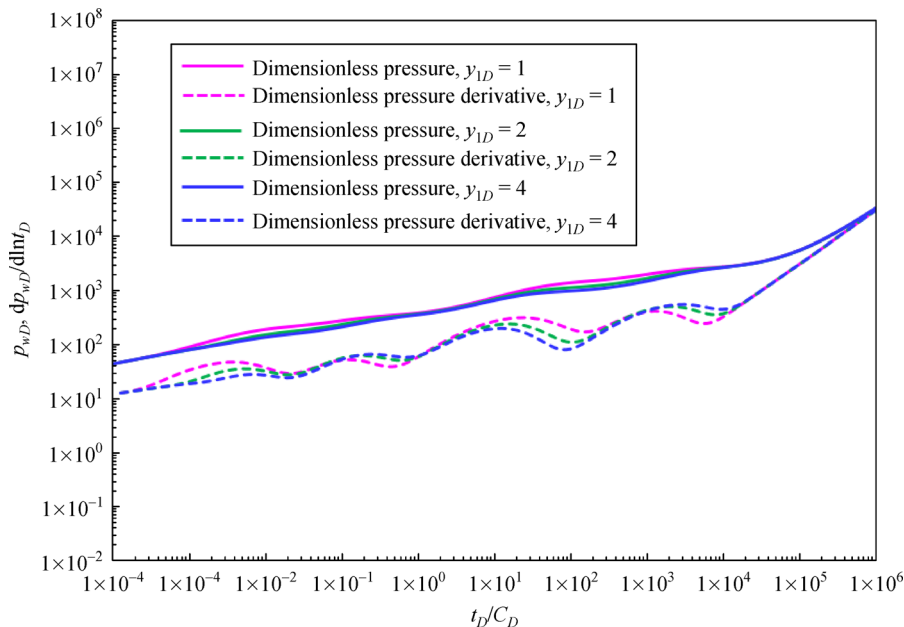


Fig. 10 The effect of acidized region width on transient pressure behavior.

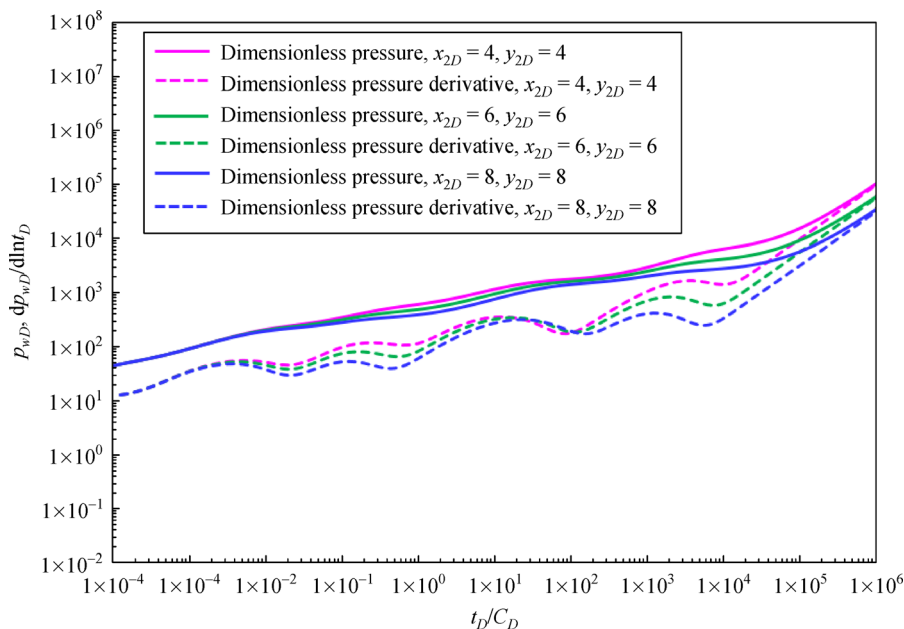


Fig. 11 The effect of reservoir size on transient pressure behavior.

with the increase of reservoir size. It is mainly because that larger reservoir size can provide more fluid to slow down the pressure depletion when well produces at the same rate. Thus, a smaller reservoir size leads to an early boundary-dominant flow.

4.4 Real case application

This section provides an application of the presented

model. Well A is located in Tarim oil field in northwest China. The effective height of well A is 28m. Figure 12 presents the buildup data fitting with the proposed model through an algorithm of auto history matching. As presented in Fig. 12, the model is able to match the real testing data perfectly. The interpretation parameters are shown in Table 3. As we can see in Fig. 12, the permeability of Region 1 is 325 mD, which demonstrates that the acidized fracturing makes an effective work.

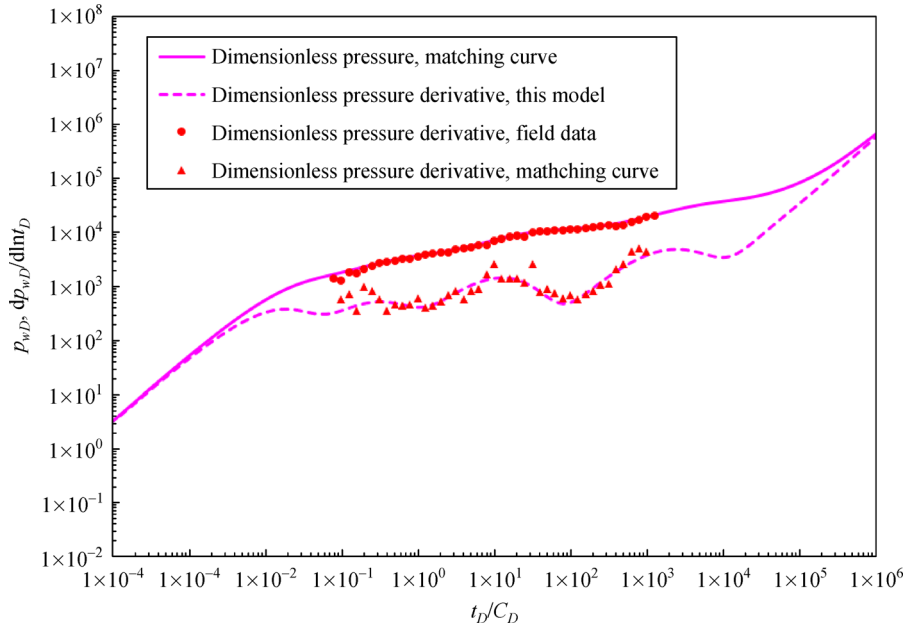


Fig. 12 The effect of reservoir size on transient pressure behavior.

Table 3 The interpretation results of pressure-curve fitting

Parameters	Interpretation Results
Half artificial fracture length, x_1 (m)	31
Artificial fracture permeability, k_F ($10^{-3} \mu\text{m}^2$)	2928
Natural fracture permeability in acidized region, k_{f1} ($10^{-3} \mu\text{m}^2$)	325
Matrix permeability in acidized region, k_{m1} ($10^{-3} \mu\text{m}^2$)	7.3
Natural fracture permeability in un-acidized region, $k_{f2}=k_{f3}=k_{f4}=k_{f5}=k_{f6}$ ($10^{-3} \mu\text{m}^2$)	86
Matrix permeability in un-acidized region, $K_{m2}=k_{m3}=k_{m4}=k_{m5}=k_{m6}$ ($10^{-3} \mu\text{m}^2$)	7.3
Interporosity flow coefficient between vug and fracture in acidized region, λ_{fv1}	0.1
Interporosity flow coefficient between matrix and fracture in acidized region, λ_{fm1}	0.001
Interporosity flow coefficient between vug and matrix in acidized region, λ_{mv1}	0.001
Storativity ratio of natural fracture, ω_{f1}	0.001
Storativity ratio of matrix, ω_{m1}	0.994
Storativity ratio of vugs, ω_{v1}	0.005
Dimensionless wellbore storage coefficient, C_D	0.0013
Skin factor, S_c	0

5 Conclusions

In this paper, an efficient alternative for the analysis of acid fracturing well in carbonate oil reservoir is developed. Acidized regions in acid fracturing carbonate reservoir are

considered as the same as SRV concept in hydraulic fracturing tight and shale reservoir. The fracture, matrix and vug are conceptualized as multiple-continuum medium and the composite linear model is used to solve the problem. The stress-sensitive permeability and partially penetrated fracture are both taken into consideration. Based on the investigation of this paper, the following conclusions can be drawn.

1) As for an acidized fracturing well in a carbonate oil reservoir, the flow regimes can be subdivided into the following stages, e.g., bilinear flow stage; linear flow stage; cross flow in acidized region; second linear flow from un-acidized region to acidized region; cross flow in un-acidized region; boundary-dominant flow.

2) Parameters sensitivity analysis demonstrates that fracture conductivity mainly influences the type curves in the early stage while permeability modulus influences the late stage; storativity ratio and interporosity flow mainly influences the cross flow stage; large acidized region size can reduce the pressure loss and enhance well productivity.

3) The presented solution combining with the algorithm of auto history matching can be used to obtain reservoir parameters and evaluate the effectiveness of acid fracturing measures.

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Appendix A. Dimensionless definitions

To simplify the equations and the corresponding solutions, some associated dimensionless variables are defined as

follows:

Dimensionless pressure:

$$p_D = \frac{2\pi k_{\text{ref}} h (p_i - p)}{q\mu B}. \quad (\text{A1})$$

Dimensionless time:

$$t_D = \frac{\eta_{\text{ref}} t}{L_{\text{ref}}^2}, \quad (\text{A2})$$

where k_{ref} , η_{ref} , and L_{ref} are reference permeability, diffusivity and length respectively. Besides, the expression of η_{ref} is given as

$$\eta_{\text{ref}} = \frac{k_{\text{ref}}}{[(\varphi c_t)_f + (\varphi c_t)_m + (\varphi c_t)_v]_{\text{ref}} \mu}, \quad (\text{A3})$$

where φ is porosity, fraction; c_t is compressibility, MPa^{-1} ; μ is fluid viscosity, $10^{-3} \text{ Pa}\cdot\text{s}$.

Dimensionless distances:

$$\begin{aligned} x_{1D} &= \frac{x_f}{L_{\text{ref}}}, x_{2D} = \frac{x_2}{L_{\text{ref}}}, y_{1D} = \frac{y_1}{L_{\text{ref}}}, \\ y_{2D} &= \frac{y_2}{L_{\text{ref}}}, z_{1D} = \frac{z_1}{L_{\text{ref}}}, z_{2D} = \frac{z_2}{L_{\text{ref}}}. \end{aligned} \quad (\text{A4})$$

Dimensionless permeability modulus:

$$\alpha_D = \alpha \frac{q\mu B}{2\pi k_{\text{ref}} h}. \quad (\text{A5})$$

where r is wellbore radius, m; h is formation height, m.

Dimensionless diffusivity:

$$\eta_{jD} = \frac{\eta_{ji}}{\eta_{\text{ref}}}, j = F, 1, 2, 3, 4, 5, 6. \quad (\text{A6})$$

The storativity ratios of fracture, matrix and vug are respectively listed as following:

$$\omega_f = \frac{(\varphi c_t)_f}{(\varphi c_t)_f + (\varphi c_t)_m + (\varphi c_t)_c}, \quad (\text{A7})$$

$$\omega_m = \frac{(\varphi c_t)_m}{(\varphi c_t)_f + (\varphi c_t)_m + (\varphi c_t)_c}, \quad (\text{A8})$$

$$\omega_c = \frac{(\varphi c_t)_c}{(\varphi c_t)_f + (\varphi c_t)_m + (\varphi c_t)_c}. \quad (\text{A9})$$

The interporosity coefficients of vug to fracture, matrix to fracture and vug to matrix are defined as following respectively:

$$\lambda_{fv} = \sigma_{fv} \frac{k_v}{k_{fi}} L_{\text{ref}}^2, \quad (\text{A10})$$

$$\lambda_{fm} = \sigma_{fm} \frac{k_m}{k_{fi}} L_{\text{ref}}^2, \quad (\text{A11})$$

$$\lambda_{vm} = \sigma_{vm} \frac{k_v}{k_m} L_{\text{ref}}^2, \quad (\text{A12})$$

where σ is shape factor, m^{-2} .

Dimensionless fracture conductivity:

$$F_{CD} = \frac{k_F w}{k_1 L_{\text{ref}}} = \frac{k_F w_D}{k_1}. \quad (\text{A13})$$

Appendix B. Derivation of the Mathematical Model

Region 6

Region 6 is the unstimulated region due to partial penetration in vertical direction, and we assume that the flow in this section is a 1D linear flow in z direction. Thus, the diffusivity equations in natural fracture, matrix and vug are respectively given as

$$\begin{aligned} &e^{-\alpha(p_i - p_{6f})} \left[\frac{\partial^2 p_{6f}}{\partial z^2} + \alpha \left(\frac{\partial p_{6f}}{\partial z} \right)^2 \right] \\ &= \frac{(\varphi c_t)_{6f} \mu}{k_{6fi}} \frac{\partial p_{6f}}{\partial t} + \frac{(\varphi c_t)_{6m} \mu}{k_{6fi}} \frac{\partial p_{6m}}{\partial t} + \frac{(\varphi c_t)_{6v} \mu}{k_{6fi}} \frac{\partial p_{6v}}{\partial t}, \end{aligned} \quad (\text{B1})$$

$$(\varphi c_t)_{6m} \frac{\partial p_{6m}}{\partial t} + \sigma_{6fm} \frac{k_{6m}}{\mu} (p_{6m} - p_{6f}) - \sigma_{6vm} \frac{k_{6v}}{\mu} (p_{6v} - p_{6m}) = 0, \quad (\text{B2})$$

$$(\varphi c_t)_{6v} \frac{\partial p_{6v}}{\partial t} + \sigma_{6fv} \frac{k_{6v}}{\mu} (p_{6v} - p_{6f}) + \sigma_{6vm} \frac{k_{6v}}{\mu} (p_{6v} - p_{6m}) = 0. \quad (\text{B3})$$

Based on the dimensionless definitions in Appendix A, Eqs. (B1) to (B3) can be converted into dimensionless form as following:

$$\begin{aligned} &e^{-\alpha_D p_{6fD}} \left[\frac{\partial^2 p_{6fD}}{\partial z_D^2} - \alpha_D \left(\frac{\partial p_{6fD}}{\partial z_D} \right)^2 \right] \\ &= \frac{1}{\eta_{6D}} \left[\omega_{6f} \frac{\partial p_{6fD}}{\partial t_D} + \omega_{6m} \frac{\partial p_{6mD}}{\partial t_D} + \omega_{6v} \frac{\partial p_{6vD}}{\partial t_D} \right], \end{aligned} \quad (\text{B4})$$

$$\omega_{6m} \frac{1}{\eta_{6D}} \frac{\partial p_{6m}}{\partial t_D} + \lambda_{6fm} (p_{6m} - p_{6f}) - \lambda_{6vm} (p_{6v} - p_{6m}) = 0, \quad (\text{B5})$$

$$\omega_{6v} \frac{1}{\eta_{6D}} \frac{\partial p_{6m}}{\partial t_D} + \lambda_{6fv} (p_{6v} - p_{6f}) - \lambda_{6vm} (p_{6v} - p_{6m}) = 0. \quad (\text{B6})$$

Since Eq. (B4) is strongly nonlinear due to the consideration of pressure-dependent permeability, we introduce Pedrosa's substitution to eliminate the non-linearity [] (Pedrosa, 1986):

$$p_{6D} = -\frac{1}{\alpha_D} \ln(1 - \alpha_D \zeta_{6D}). \tag{B7}$$

Thus, Eq. (B4) can be converted into

$$\begin{aligned} \frac{\partial^2 \zeta_{6D}}{\partial z_D^2} &= \frac{\omega_{6f}}{\eta_{6D}} \frac{1}{1 - \alpha_D \zeta_{6D}} \frac{\partial \zeta_{6D}}{\partial t_D} + \frac{\omega_{6m}}{\eta_{6D}} \frac{\partial p_{6mD}}{\partial t_D} \\ &+ \frac{\omega_{6v}}{\eta_{6D}} \frac{\partial p_{6vD}}{\partial t_D}. \end{aligned} \tag{B8}$$

A perturbation in α_D is conducted:

$$\frac{1}{1 - \alpha_D \zeta_{6D}} = 1 + \alpha_D \zeta_{6D} + (\alpha_D \zeta_{6D})^2 + (\alpha_D \zeta_{6D})^3 + \dots, \tag{B9}$$

$$-\frac{1}{\alpha_D} \ln(1 - \alpha_D \zeta_{6D}) = \zeta_{6D} + \frac{1}{2} \alpha_D \zeta_{6D}^2 + \frac{1}{3} \alpha_D^2 \zeta_{6D}^3 \dots \tag{B10}$$

For small α_D , the higher-order terms in the series become smaller successively and the zero-order perturbation solution cansatisfies the accuracy requirement. Thus, Eqs. (B4)–(B6) can be rewritten as

$$\frac{\partial^2 \zeta_{6D}}{\partial z_D^2} = \frac{\omega_{6f}}{\eta_{6D}} \frac{\partial \zeta_{6D}}{\partial t_D} + \frac{\omega_{6m}}{\eta_{6D}} \frac{\partial p_{6mD}}{\partial t_D} + \frac{\omega_{6v}}{\eta_{6D}} \frac{\partial p_{6vD}}{\partial t_D}, \tag{B11}$$

$$\omega_{6m} \frac{1}{\eta_{6D}} \frac{\partial p_{6m}}{\partial t_D} + \lambda_{6fm}(p_{6m} - \zeta_{6f}) - \lambda_{6vm}(p_{6v} - p_{6m}) = 0, \tag{B12}$$

$$\omega_{6v} \frac{1}{\eta_{6D}} \frac{\partial p_{6v}}{\partial t_D} + \lambda_{6fv}(p_{6v} - \zeta_{6f}) + \lambda_{6vm}(p_{6v} - p_{6m}) = 0. \tag{B13}$$

The initial and boundary conditions can be transformed into

$$\zeta_{6D}|_{t_D=0} = 0, \tag{B14}$$

$$\left. \frac{\partial \zeta_{6D}}{\partial z_D} \right|_{z_D=z_{2D}} = 0, \tag{B15}$$

$$\zeta_{6D}|_{z_D=z_{1D}} = \zeta_{2D}|_{z_D=z_{1D}} = \zeta_{4D}|_{z_D=z_{1D}}. \tag{B16}$$

Subsequently, we apply the Laplace transformation of t_D to convert Eqs. (B11)–(B13) into Laplace domain. The Laplace transformation with respect to t_D is defined as following:

$$\tilde{\zeta}_{6D}(z_D, s) = \int_0^{+\infty} e^{-st_D} \zeta_{6D}(z_D, t_D) dt_D. \tag{B17}$$

Eqs. (B11)–(B13) can be written as

$$\frac{\partial^2 \tilde{\zeta}_{6D}}{\partial z_D^2} = s \frac{\omega_{6f}}{\eta_{6D}} \tilde{\zeta}_{6D} + s \frac{\omega_{6m}}{\eta_{6D}} \tilde{p}_{6mD} + s \frac{\omega_{6v}}{\eta_{6D}} \tilde{p}_{6vD}, \tag{B18}$$

$$s \frac{\omega_{6m}}{\eta_{6D}} \tilde{p}_{6m} + \lambda_{6fm}(\tilde{p}_{6m} - \tilde{\zeta}_{6f}) - \lambda_{6vm}(\tilde{p}_{6v} - \tilde{p}_{6m}) = 0, \tag{B19}$$

$$s \frac{\omega_{6v}}{\eta_{6D}} \tilde{p}_{6v} + \lambda_{6fv}(\tilde{p}_{6v} - \tilde{\zeta}_{6f}) + \lambda_{6vm}(\tilde{p}_{6v} - \tilde{p}_{6m}) = 0. \tag{B20}$$

Substituting the matrix and vuginterporosity flow Eqs. (B19) and (B20), we can obtain

$$\frac{\partial^2 \tilde{\zeta}_{6D}}{\partial z_D^2} = \frac{s}{\eta_{6D}} g_6(s) \tilde{\zeta}_{6D}, \tag{B21}$$

$$g_6(s) = \omega_{6f} + \frac{(\lambda_{6fv} + \lambda_{6fm}) \frac{s}{\eta_{6D}} + \frac{1 - \omega_{6f}}{\omega_{6v} \omega_{6m}} [\lambda_{6fv} \lambda_{6fm} + (\lambda_{6fv} + \lambda_{6fm}) \lambda_{6vm}]}{\left(\frac{s}{\eta_{6D}}\right)^2 + \left[\frac{\lambda_{6fv}}{\omega_{6v}} + \frac{\lambda_{6fm}}{\omega_{6m}} + \left(\frac{1}{\omega_{6v}} + \frac{1}{\omega_{6m}}\right) \lambda_{6vm}\right] \frac{s}{\eta_{6D}} + \frac{\lambda_{6fv} \lambda_{6fm} + (\lambda_{6fv} + \lambda_{6fm}) \lambda_{6vm}}{\omega_{6v} \omega_{6m}}}. \tag{B22}$$

The boundary conditions in Laplace domain are

$$\left. \frac{\partial \tilde{\zeta}_{6D}}{\partial z_D} \right|_{z_D=z_{2D}} = 0, \tag{B23}$$

$$\tilde{\zeta}_{6D}|_{z_D=z_{1D}} = \tilde{\zeta}_{2D}|_{z_D=z_{1D}} = \tilde{\zeta}_{4D}|_{z_D=z_{1D}}. \tag{B24}$$

Combining boundary conditions of Eqs. (B23) and (B24), we can obtain the pressure solutions for Region 6 as

following:

$$\tilde{\zeta}_{6D} = \tilde{\zeta}_{2D}(z_{1D}) \frac{\cosh \left[\sqrt{\frac{sg_6(s)}{\eta_{6D}}} (z_D - z_{2D}) \right]}{\cosh \left[\sqrt{\frac{sg_6(s)}{\eta_{6D}}} (z_{1D} - z_{2D}) \right]}, \tag{B25}$$

$$\tilde{\zeta}_{6D} = \tilde{\zeta}_{4D}(z_{1D}) \frac{\cosh \left[\sqrt{\frac{sg_6(s)}{\eta_{6D}}}(z_D - z_{2D}) \right]}{\cosh \left[\sqrt{\frac{sg_6(s)}{\eta_{6D}}}(z_{1D} - z_{2D}) \right]}. \tag{B26}$$

Therefore, the flux between Region 6 and 2, and Region 6 and 4 is proportional to

$$\left. \frac{\partial \tilde{\zeta}_{6D}}{\partial z_D} \right|_{z_{1D}} = \tilde{\zeta}_{2D}(z_{1D}) \sqrt{\frac{sg_6(s)}{\eta_{6D}}} \tanh \left[\sqrt{\frac{sg_6(s)}{\eta_{6D}}}(z_{1D} - z_{2D}) \right], \tag{B27}$$

$$\left. \frac{\partial \tilde{\zeta}_{6D}}{\partial z_D} \right|_{z_{1D}} = \tilde{\zeta}_{4D}(z_{1D}) \sqrt{\frac{sg_6(s)}{\eta_{6D}}} \tanh \left[\sqrt{\frac{sg_6(s)}{\eta_{6D}}}(z_{1D} - z_{2D}) \right]. \tag{B28}$$

Region 5

Analogously, the diffusivity equation and boundary conditions in Region 5 in Laplace domain are

$$\frac{\partial^2 \tilde{\zeta}_{5D}}{\partial z_D^2} = \frac{s}{\eta_{5D}} g_5(s) \tilde{\zeta}_{5D}, \tag{B29}$$

where

$$\zeta_{5D} = \frac{1}{\alpha_D} (1 - e^{\alpha_D p_{5D}}), \tag{B30}$$

$$g_5(s) = \omega_{5f} + \frac{(\lambda_{5fv} + \lambda_{5fm}) \frac{s}{\eta_{5D}} + \frac{1 - \omega_{5f}}{\omega_{5v} \omega_{5m}} [\lambda_{5fv} \lambda_{5fm} + (\lambda_{5fv} + \lambda_{5fm}) \lambda_{5vm}]}{\left(\frac{s}{\eta_{5D}} \right)^2 + \left[\frac{\lambda_{5fv}}{\omega_{5v}} + \frac{\lambda_{5fm}}{\omega_{5m}} + \left(\frac{1}{\omega_{5v}} + \frac{1}{\omega_{5m}} \right) \lambda_{5vm} \right] \frac{s}{\eta_{5D}} + \frac{\lambda_{5fv} \lambda_{5fm} + (\lambda_{5fv} + \lambda_{5fm}) \lambda_{5vm}}{\omega_{5v} \omega_{5m}}}. \tag{B31}$$

The boundary conditions in Laplace domain are

$$\left. \frac{\partial \tilde{\zeta}_{5D}}{\partial z_D} \right|_{z_D = z_{2D}} = 0, \tag{B32}$$

$$\left. \frac{\partial \tilde{\zeta}_{5D}}{\partial z_D} \right|_{z_{1D}} = \tilde{\zeta}_{3D}(z_{1D}) \sqrt{\frac{sg_5(s)}{\eta_{5D}}} \tanh \left[\sqrt{\frac{sg_5(s)}{\eta_{5D}}}(z_{1D} - z_{2D}) \right]. \tag{B35}$$

$$\tilde{\zeta}_{5D}|_{z_D = z_{1D}} = \tilde{\zeta}_{1D}|_{z_D = z_{1D}} = \tilde{\zeta}_{3D}|_{z_D = z_{1D}}. \tag{B33}$$

The flux between Region 5 and Region 1, and Region 5 and Region 3 is proportional to

$$\left. \frac{\partial \tilde{\zeta}_{5D}}{\partial z_D} \right|_{z_{1D}} = \tilde{\zeta}_{1D}(z_{1D}) \sqrt{\frac{sg_5(s)}{\eta_{5D}}} \tanh \left[\sqrt{\frac{sg_5(s)}{\eta_{5D}}}(z_{1D} - z_{2D}) \right], \tag{B34}$$

Region 4

In Region 4, the diffusivity equation in Laplace domain is

$$\frac{\partial^2 \tilde{\zeta}_{4D}}{\partial x_D^2} + \frac{\partial^2 \tilde{\zeta}_{4D}}{\partial z_D^2} - \frac{sg_4(s)}{\eta_{4D}} \tilde{\zeta}_{4D} = 0, \tag{B36}$$

where

$$\zeta_{4D} = \frac{1}{\alpha_D} (1 - e^{\alpha_D p_{4D}}), \tag{B37}$$

$$g_4(s) = \omega_{4f} + \frac{(\lambda_{4fv} + \lambda_{4fm}) \frac{s}{\eta_{4D}} + \frac{1 - \omega_{4f}}{\omega_{4v} \omega_{4m}} [\lambda_{4fv} \lambda_{4fm} + (\lambda_{4fv} + \lambda_{4fm}) \lambda_{4vm}]}{\left(\frac{s}{\eta_{4D}} \right)^2 + \left[\frac{\lambda_{4fv}}{\omega_{4v}} + \frac{\lambda_{4fm}}{\omega_{4m}} + \left(\frac{1}{\omega_{4v}} + \frac{1}{\omega_{4m}} \right) \lambda_{4vm} \right] \frac{s}{\eta_{4D}} + \frac{\lambda_{4fv} \lambda_{4fm} + (\lambda_{4fv} + \lambda_{4fm}) \lambda_{4vm}}{\omega_{4v} \omega_{4m}}}. \tag{B38}$$

To convert Eq. (B36) into a 1D form, we integrate each of its term from 0 to z_{1D} with respect to z_D . Assuming that the pressure in Region 4 does not depend on z_D , and combining the flux continuity condition between Region 6 and Region 4, Eq. (B36) can be rewritten as

$$\frac{\partial^2 \tilde{\zeta}_{4D}}{\partial x_D^2} + \frac{k_{6f,v}}{k_{4f,v} z_{1D}} \left. \frac{\partial \tilde{\zeta}_{6D}}{\partial z_D} \right|_{z_{1D}} - \frac{sg_4(s)}{\eta_{4D}} \tilde{\zeta}_{4D} = 0. \tag{B39}$$

Substituting Eq. (B28) into (B39), we can obtain

$$\frac{\partial^2 \tilde{\zeta}_{4D}}{\partial x_D^2} - \alpha_4 \tilde{\zeta}_{4D} = 0, \tag{B40}$$

where

$$\alpha_4 = \frac{sg_4(s)}{\eta_{4D}} - \frac{k_{6f,v}}{k_{4f,v} z_{1D}} \sqrt{\frac{sg_6(s)}{\eta_{6D}}} \tanh \left[\sqrt{\frac{sg_6(s)}{\eta_{6D}}}(z_{1D} - z_{2D}) \right]. \tag{B41}$$

The boundary conditions in Laplace domain are

$$\left. \frac{\partial \tilde{\xi}_{4D}}{\partial x_D} \right|_{x_{2D}} = 0, \tag{B42}$$

$$\tilde{\xi}_{4D}|_{x_D=x_{1D}} = \tilde{\xi}_{2D}|_{x_D=x_{1D}}. \tag{B43}$$

The flux between Region 4 and 2 is proportional to

$$\left. \frac{\partial \tilde{\xi}_{4D}}{\partial x_D} \right|_{x_{1D}} = \tilde{\xi}_{2D}(x_{1D})\sqrt{\alpha_4}\tanh[\sqrt{\alpha_4}(x_{1D}-x_{2D})]. \tag{B44}$$

$$g_3(s) = \omega_{3f} + \frac{(\lambda_{3fv} + \lambda_{3fm})\frac{s}{\eta_{3D}} + \frac{1-\omega_{3f}}{\omega_{3v}\omega_{3m}}[\lambda_{3fv}\lambda_{3fm} + (\lambda_{3fv} + \lambda_{3fm})\lambda_{3vm}]}{\left(\frac{s}{\eta_{3D}}\right)^2 + \left[\frac{\lambda_{3fv}}{\omega_{3v}} + \frac{\lambda_{3fm}}{\omega_{3m}} + \left(\frac{1}{\omega_{3v}} + \frac{1}{\omega_{3m}}\right)\lambda_{3vm}\right]\frac{s}{\eta_{3D}} + \frac{\lambda_{3fv}\lambda_{3fm} + (\lambda_{3fv} + \lambda_{3fm})\lambda_{3vm}}{\omega_{3v}\omega_{3m}}}. \tag{B47}$$

To convert Eq. (B45) into a 1D form, we integrate each of its term from 0 to z_{1D} with respect to z_D . Assuming that pressure in Region 3 does not depend on z_D , and using the flux continuity condition between Region 5 and Region 3, Eq. (B45) can be rewritten as

$$\frac{\partial^2 \tilde{\xi}_{3D}}{\partial x_D^2} + \frac{k_{5f,v}}{k_{3f,v}z_{1D}} \left. \frac{\partial \tilde{\xi}_{5D}}{\partial z_D} \right|_{z_{1D}} - \frac{sg_3(s)}{\eta_{3D}} \tilde{\xi}_{3D} = 0. \tag{B48}$$

Substituting Eq. (B35) into Eq. (B48), we can obtain

$$\frac{\partial^2 \tilde{p}_{3D}}{\partial x_D^2} - \alpha_3 \tilde{p}_{3D} = 0. \tag{B49}$$

where

$$\alpha_3 = \frac{sg_3(s)}{\eta_{3D}} - \frac{k_{5f,v}}{k_{3f,v}z_{1D}} \sqrt{\frac{sg_5(s)}{\eta_{3D}}} \tanh \left[\sqrt{\frac{sg_5(s)}{\eta_{3D}}}(z_{1D}-z_{2D}) \right]. \tag{B50}$$

The boundary conditions in Laplace domain are

$$g_2(s) = \omega_{2f} + \frac{(\lambda_{2fv} + \lambda_{2fm})\frac{s}{\eta_{2D}} + \frac{1-\omega_{2f}}{\omega_{2v}\omega_{2m}}[\lambda_{2fv}\lambda_{2fm} + (\lambda_{2fv} + \lambda_{2fm})\lambda_{4vm}]}{\left(\frac{s}{\eta_{2D}}\right)^2 + \left[\frac{\lambda_{2fv}}{\omega_{2v}} + \frac{\lambda_{2fm}}{\omega_{2m}} + \left(\frac{1}{\omega_{2v}} + \frac{1}{\omega_{2m}}\right)\lambda_{2vm}\right]\frac{s}{\eta_{2D}} + \frac{\lambda_{2fv}\lambda_{2fm} + (\lambda_{2fv} + \lambda_{2fm})\lambda_{2vm}}{\omega_{2v}\omega_{2m}}}. \tag{B56}$$

To convert Eq. (B54) into a 1D form, we integrate each of its term from 0 to z_{1D} with respect to z_D , and from 0 to x_{1D} with respect to x_D . Assuming that the pressure in Region 2 does not depend on x_D and z_D , and combining the flux continuity condition between Region 2 and 4, and Region 2 and 6, Eq. (B54) can be rewritten as

$$\frac{\partial^2 \tilde{\xi}_{2D}}{\partial y_D^2} + \frac{k_{4f,v}}{k_{2f,v}x_{1D}} \left. \frac{\partial \tilde{\xi}_{4D}}{\partial x_D} \right|_{x_{1D}} + \frac{k_{6f,v}}{k_{2f,v}z_{1D}} \left. \frac{\partial \tilde{\xi}_{2D}}{\partial z_D} \right|_{z_{1D}}$$

Region 3

Similarly, the governing equation in Region 3 in Laplace domain is

$$\frac{\partial^2 \tilde{\xi}_{3D}}{\partial x_D^2} + \frac{\partial^2 \tilde{\xi}_{3D}}{\partial z_D^2} - \frac{sg_3(s)}{\eta_{3D}} \tilde{\xi}_{3D} = 0, \tag{B45}$$

where

$$\xi_{4D} = \frac{1}{\alpha_D}(1 - e^{\alpha_D p_{4D}}), \tag{B46}$$

$$\left. \frac{\partial \tilde{\xi}_{3D}}{\partial x_D} \right|_{x_{2D}} = 0, \tag{B51}$$

$$\tilde{\xi}_{3D}|_{x_D=x_{1D}} = \tilde{\xi}_{1D}|_{x_D=x_{1D}}. \tag{B52}$$

Flux between Region 3 and Region 1 is proportional to

$$\left. \frac{\partial \tilde{p}_{3D}}{\partial x_D} \right|_{x_{1D}} = \tilde{p}_{1D}(x_{1D})\sqrt{\alpha_3}\tanh[\sqrt{\alpha_3}(x_{1D}-x_{2D})]. \tag{B53}$$

Region 2

In Region 2, the diffusivity equation in Laplace domain is

$$\frac{\partial^2 \tilde{\xi}_{2D}}{\partial y_D^2} + \frac{\partial^2 \tilde{\xi}_{2D}}{\partial x_D^2} + \frac{\partial^2 \tilde{\xi}_{2D}}{\partial z_D^2} - \frac{sg_2(s)}{\eta_{2D}} \tilde{\xi}_{2D} = 0, \tag{B54}$$

where

$$\xi_{4D} = \frac{1}{\alpha_D}(1 - e^{\alpha_D p_{4D}}), \tag{B55}$$

$$-\frac{sg_2(s)}{\eta_{2D}} \tilde{p}_{2D} = 0. \tag{B57}$$

Substituting Eqs. (B27) and (B44) into (B57), we can obtain

$$\frac{\partial^2 \tilde{\xi}_{2D}}{\partial y_D^2} - \alpha_2 \tilde{\xi}_{2D} = 0, \tag{B58}$$

where

$$\alpha_2 = \frac{s}{\eta_{2D}} - \frac{k_4}{k_2 x_{1D}} \sqrt{\alpha_4} \tanh[\sqrt{\alpha_4}(x_{1D} - x_{2D})] - \frac{k_6}{k_2 z_{1D}} \sqrt{\frac{s}{\eta_{6D}}} \tanh\left[\sqrt{\frac{s}{\eta_{6D}}}(z_{1D} - z_{2D})\right]. \tag{B59}$$

The boundary conditions in Laplace domain are

$$\left. \frac{\partial \tilde{\xi}_{2D}}{\partial y_D} \right|_{y_{2D}} = 0, \tag{B60}$$

$$\tilde{\xi}_{2D}(y_{1D}) = \tilde{\xi}_{1D}(y_{1D}). \tag{B61}$$

The flux between Region 2 and 1 is proportional to

$$g_1(s) = \omega_{1f} + \frac{(\lambda_{1fv} + \lambda_{1fm}) \frac{s}{\eta_{1D}} + \frac{1 - \omega_{1f}}{\omega_{1v} \omega_{1m}} [\lambda_{1fv} \lambda_{1fm} + (\lambda_{1fv} + \lambda_{1fm}) \lambda_{1vm}]}{\left(\frac{s}{\eta_{1D}}\right)^2 + \left[\frac{\lambda_{1fv}}{\omega_{1v}} + \frac{\lambda_{1fm}}{\omega_{1m}} + \left(\frac{1}{\omega_{1v}} + \frac{1}{\omega_{1m}}\right) \lambda_{1vm}\right] \frac{s}{\eta_{4D}} + \frac{\lambda_{1fv} \lambda_{1fm} + (\lambda_{1fv} + \lambda_{1fm}) \lambda_{1vm}}{\omega_{1v} \omega_{1m}}}. \tag{B65}$$

To convert Eq. (B63) into a 1D form, we integrate each of its term from 0 to z_{1D} with respect to z_D , and from 0 to x_{1D} with respect to x_D . Assuming that the pressure in Region 1 does not depend on x_D and z_D , and combining the flux continuity condition between Region 1 and 3, and Region 1 and 5, Eq. (B54) can be rewritten as

$$\left. \frac{\partial^2 \tilde{\xi}_{1D}}{\partial y_D^2} + \frac{k_3}{k_1 x_{1D}} \frac{\partial \tilde{\xi}_{3D}}{\partial x_D} \right|_{x_{1D}} + \left. \frac{k_5}{k_1 z_{1D}} \frac{\partial \tilde{\xi}_{5D}}{\partial z_D} \right|_{z_{1D}} - \frac{sg_1(s)}{\eta_{1D}} \tilde{\xi}_{1D} = 0, \tag{B66}$$

$$\frac{\partial^2 \tilde{\xi}_{1D}}{\partial y_D^2} - \alpha_1 \tilde{\xi}_{1D} = 0, \tag{B67}$$

where

$$\alpha_1 = \frac{sg_1(s)}{\eta_{1D}} - \frac{k_3}{k_1 x_{1D}} \sqrt{\alpha_3} \tanh[\sqrt{\alpha_3}(x_{1D} - x_{2D})] - \frac{k_5}{k_1 z_{1D}} \sqrt{\frac{sg_5(s)}{\eta_{5D}}} \tanh\left[\sqrt{\frac{sg_5(s)}{\eta_{5D}}}(z_{1D} - z_{2D})\right]. \tag{B68}$$

Based on the flux continuity condition at the interface of Regions 1 and 2, and the pressure continuity condition at the interface of Region 1 and main artificial fracture, we can obtain

$$\left. \frac{\partial \tilde{\xi}_{1D}}{\partial y_D} \right|_{\frac{w_D}{2}} = -\beta_2 \tilde{\xi}_{FD} \left(\frac{w_D}{2}\right), \tag{B69}$$

$$\left. \frac{\partial \tilde{\xi}_{2D}}{\partial y_D} \right|_{y_{1D}} = \tilde{\xi}_{1D}(y_{1D}) \sqrt{\alpha_2} \tanh[\sqrt{\alpha_2}(y_{1D} - y_{2D})]. \tag{B62}$$

Region 1

In Region 1, the diffusivity equation in Laplace domain is

$$\frac{\partial^2 \tilde{\xi}_{1D}}{\partial y_D^2} + \frac{\partial^2 \tilde{\xi}_{1D}}{\partial x_D^2} + \frac{\partial^2 \tilde{\xi}_{1D}}{\partial z_D^2} - \frac{sg_1(s)}{\eta_{1D}} \tilde{\xi}_{1D} = 0, \tag{B63}$$

where

$$\xi_{1D} = \frac{1}{\alpha_D} (1 - e^{\alpha_D p_{1D}}), \tag{B64}$$

where

$$\beta_2 = \sqrt{\alpha_1} \frac{\exp\left[-\sqrt{\alpha_1} \frac{w_D}{2}\right] - \beta_1 \exp\left[\sqrt{\alpha_1} \frac{w_D}{2}\right]}{\exp\left[-\sqrt{\alpha_1} \frac{w_D}{2}\right] + \beta_1 \exp\left[\sqrt{\alpha_1} \frac{w_D}{2}\right]}, \tag{B70}$$

$$\beta_1 = \exp[-\sqrt{\alpha_1} 2y_{1D}]$$

$$\frac{(k_1 \sqrt{\alpha_1} + k_2 \sqrt{\alpha_2} \tanh[\sqrt{\alpha_2}(y_{1D} - y_{2D})])}{(k_1 \sqrt{\alpha_1} - k_2 \sqrt{\alpha_2} \tanh[\sqrt{\alpha_2}(y_{1D} - y_{2D})])}. \tag{B71}$$

Fracture

The diffusivity equation for main artificial fracture in Laplace domain is

$$\frac{\partial^2 \tilde{\xi}_{FD}}{\partial x_D^2} + \frac{\partial^2 \tilde{\xi}_{FD}}{\partial y_D^2} - \frac{s}{\eta_{FD}} \tilde{\xi}_{FD} = 0, \tag{B72}$$

where

$$\xi_{FD} = \frac{1}{\alpha_D} (1 - e^{\alpha_D p_{FD}}). \tag{B73}$$

To convert Eq. (B63) into a 1D form, we integrate each of its term from 0 to x_{1D} with respect to x_D . Assuming that the pressure in Region 1 does not depend on x_D , and combining the flux continuity condition between fracture and Region 1 Eq. (B54) can be rewritten as

$$\frac{\partial^2 \tilde{\xi}_{FD}}{\partial x_D^2} + \frac{2k_1}{w_D k_F} \left. \frac{\partial \tilde{\xi}_{1D}}{\partial y_D} \right|_{\frac{w_D}{2}} - \frac{s}{\eta_{FD}} \tilde{\xi}_{FD} = 0. \tag{B74}$$

Based on the dimensionless fracture conductivity defined in Eq (A13), we can obtain

$$\frac{\partial^2 \tilde{\zeta}_{FD}}{\partial x_D^2} + \frac{2}{F_{CD}} \frac{\partial \tilde{\zeta}_{1D}}{\partial y_D} \Big|_{\frac{w_D}{2}} - \frac{s}{\eta_{FD}} \tilde{\zeta}_{FD} = 0. \quad (\text{B75})$$

Substituting Eq. (B69) into (B75), we can obtain

$$\frac{\partial^2 \tilde{\zeta}_{FD}}{\partial x_D^2} - \alpha_F \tilde{\zeta}_{FD} = 0, \quad (\text{B76})$$

where

$$\alpha_F = \frac{2\beta_2}{F_{CD}} + \frac{s}{\eta_{FD}}. \quad (\text{B77})$$

The boundary conditions in x direction are

$$\frac{\partial \tilde{\zeta}_{FD}}{\partial x_D} \Big|_{x_{1D}} = 0, \quad (\text{B78})$$

$$\frac{\partial \tilde{\zeta}_{FD}}{\partial x_D} \Big|_0 = -\frac{\pi}{sF_{CD}}. \quad (\text{B79})$$

Therefore, the pressure solution for fracture region is

$$\tilde{\zeta}_{FD} = \frac{\pi \cosh[\sqrt{\alpha_F}(x_D - x_{1D})]}{sF_{CD}\sqrt{\alpha_F} \sinh[\sqrt{\alpha_F}(x_{1D})]}. \quad (\text{B80})$$

Set $x_D=0$, we can obtain the final solution for the well bottom-hole pressure in Laplace domain as following:

$$\tilde{\zeta}_{wD} = \frac{\pi}{sF_{CD}\sqrt{\alpha_F} \tanh[\sqrt{\alpha_F}(x_{1D})]}. \quad (\text{B81})$$

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