

Prioritizing the Causes of Fire and Explosion in the External Floating Roof Tanks

Parisa Moshashaei · Seyed Shamseddin Alizadeh · Mohammad Asghari Jafarabadi ·
Leila Khazini

Submitted: 17 April 2018 / Accepted: 16 October 2018 / Published online: 2 November 2018
© ASM International 2018

Abstract In the oil industry, many flammable products such as liquid hydrocarbons are usually stored in the atmospheric storage tanks. One type of these suitable tanks is the floating roof tanks. Among the floating roof tanks, external floating roof tanks are mainly used to store large quantities of petroleum products such as crude oil or condensate, gasoline, kerosene. The purpose of this study is prioritizing the causes of fire and explosion in the external floating roof tanks. In this study, firstly, the causes of fire and explosion of the external floating roof tanks were identified and then the obtained variables were scored by the process and safety specialists. In the next step, the causes were weighed and prioritized using the analytic network process method and Super Decisions software. The findings of the study identified 11 main criteria and 71 sub-criteria for fire and explosion of external floating roof tanks. Results revealed that several effective risk factors in

the fire and explosion are natural disasters, static electricity, operational error, faulty firefighting system, maintenance error, piping rupture/leak, equipment/instrument failure, open flames, tank crack/rupture, runaway reactions, and sabotage, respectively. This study will help experts to identify the effective risk factors in fire and explosion in external floating roof tanks and their importance. Therefore, they can prioritize and implement the control measures to prevent fire and explosion incidents in external floating roof tanks.

Keywords Fire · Explosion ·
External floating roof tanks · ANP

Introduction

In recent years with the development of industry, energy demand is increasing, especially fossil fuels, and this issue is becoming much more serious; therefore, the scale of the petrochemical industry becomes greater and greater [1–4]. The petrochemical industry, especially refineries, normally uses large storage tanks. Due to the advantages of presentation and the accurate and full solution for providing appropriate and lockable on-site oil storage, atmospheric storage tanks are commonly used. However, these oil tanks, and in particular floating roof tanks which are commonly used for the storage of large amount of crude oil, are the most vulnerable equipment.

Storage tanks contain significant amounts of flammable and hazardous hydrocarbon fuels and chemicals [5–7]. Thus, the occurrence of a storage tank accident is possible and usually leads to fire and explosions [7–9]. As evident based on industry experience, oil tank fire is enormous and

P. Moshashaei · S. S. Alizadeh (✉)
Department of Occupational Health Engineering, Health Faculty,
Tabriz University of Medical Sciences, Tabriz, Iran
e-mail: ss.alizadeh2013@gmail.com; alizadehsh@tbzmed.ac.ir

P. Moshashaei
e-mail: parisamoshashai@gmail.com

M. A. Jafarabadi
Road Traffic Injury Research Center, Tabriz University of
Medical Sciences, Tabriz, Iran
e-mail: m.asghari862@gmail.com

M. A. Jafarabadi
Department of Statistics and Epidemiology, Health Faculty,
Tabriz University of Medical Sciences, Tabriz, Iran

L. Khazini
Department of Chemical Engineering, Chemical and Petroleum
Engineering Faculty, Tabriz University, Tabriz, Iran
e-mail: khazini@tabrizu.ac.ir

has strong radiation and high flame and it is considered a major challenge both to control and to extinguish [5, 10].

The storage tank type used in storing flammable and combustible liquids depends on the physical characteristics of the product stored and the tank's location [5, 11, 12]. Many flammable products, for example, liquid hydrocarbons at normal temperature and pressure, are usually stored in large tank at atmospheric pressure [13, 14]. These tanks can hold more than 1.5 million barrels of flammable or combustible liquids [12]. Due to this high volume storage of flammable and/or hazardous chemicals, atmospheric storage tank incidents are a major concern [15] with regards to industrial safety such as ignition of a hydrocarbon–air mixture in such tanks which can lead to fire and explosion [16].

Floating roof tanks are a type of atmospheric storage tank [17, 18]. Vertical cylindrical tank, including the floating roof type, is the most commonly used metal storage tank [10]. Floating roof tanks are not intended for all products, but they are mainly used to store large quantities of high-volatility products such as crude oil or gasoline [13, 19, 20].

The purpose of this paper is prioritizing the causes of fire and explosion in the external floating roof tanks using ANP method. We hope that this work will be beneficial to tank operators and engineers.

External Floating Roof Tank

External floating roof tanks (EFRT) have cylindrical steel shells equipped with a roof that floats on the product in an open tank; the roof is open to the atmosphere and rises and falls along with the liquid level [21–24]. As opposed to a fixed roof tank, there is almost no vapor space between floating plate and oil surface and this significantly eliminates breathing losses and reduces evaporation losses of the stored liquid. The external floating roof crude storage tank is the most common storage tank. The floating roof system consists of a deck, fittings, and rim seal system [21, 25]. The rim seal system is between the tank shell and roof that is attached to the deck perimeter and contacts the tank wall to reduce rim evaporation [26–28].

An external floating roof tank is usually used in steel open-top tank larger than 20,000 m³ and mainly used to store large quantities of petroleum products such as crude oil or condensate, gasoline, kerosene [29].

Impact of Major Accidents in the External Floating Roof Tank

Nowadays, explosion and fire accidents are one of the main reasons for high risk of large-scale crude oil depots because crude oil is flammable and combustible. Among the types

of tank, large-scale floating roof tanks are the main type of tanks for storing crude oil.

Results of the study of Chang and Lin presented on 242 accidents of storage tanks that occurred in industrial facilities over 40 years showed that 74% of the accidents occurred in petroleum refineries, oil terminals or storage parks, while fire and explosion account for 85% of the accidents. The most common contents of the tank were crude oil and oil products such as gasoline, fuel oil, and diesel oil. The study also showed that the fires occurred more frequently in the atmospheric external floating roof tank instead of fixed roof tanks [30].

Another study by Persson and Lonnermark identified 480 storage tank fire incidents worldwide between 1951 and 2003. The number of tank fires reported by worldwide media is in the range of 15–20 each year. About one-third (31%) of reported tank fire incidents have been attributed to lightning striking atmospheric external floating roof tanks [31].

In the LASTFIRE incident review sponsored by 16 oil industry companies in 2012, it was reported that 52 of the 62 initial fire events within the scope of the survey were lightning-ignited rim seal fires in external floating roof tank [32–34]. In another study conducted by the LASTFIRE project in 1997, it was found that rim seal fires in external floating roof tank are the most common scenario [34].

In a review of tank incidents conducted by Thyer et al. [15], 64 single-tank fires were identified between 1919 and 2004, with the causes being attributed to many factors that most of them are sinking floating roof in floating roof tank. American Petroleum Institute (API) collected 22 full-surface fire accidents among the 81 large-scale floating roof tank fire accidents from 1951 to 1995, and this accounted for 27% and the diameter of those collected tanks was among 30.5–100 m [35].

Causes of Fire and Explosion in the External Floating Roof Tanks

Effective direct and indirect causes of fire and explosion in oil tankers were obtained as a result from a library research and data collection of accidents records and documents of oil tankers through validated articles, LASTFIRE project, API report, Fire magazines, NFPA Special Data Information Package, and output of methods of risk assessment conducted on tanks such as HAZOP, FMEA, FTA, and Internet. To assign the causes to the floating roof tanks, a few visits to tanks were performed. Causes obtained due to the views of several process engineering, safety, and fire were finalized. Lastly, the 11 criteria and 71 sub-criteria obtained in accordance with Table 1 were classified.

Prioritizing the Causes Using ANP Method

ANP Method

The analytic network process is a method proposed by Saaty [36]. Analytic network process (ANP) is a novel tool for multi-criteria decision-making (MCDM) but can also be applied in academic research to prioritize factors or criteria [37]. ANP is a generalization of the analytic hierarchy process (AHP), by considering the dependence between the elements of the hierarchy [38]. Many decision problems cannot be structured hierarchically because they involve the interaction and dependence of higher-level elements in a hierarchy on lower-level elements. Therefore, ANP is represented by a network, rather than a hierarchy. Although most of the studies implemented in the context of supply chain risks have employed AHP, it should be acknowledged that risk is a complicated factor and its clusters and sub-factors have implicit effects on each other [39].

The advantage of using the ANP in a supply chain is to designate the impact of risks on each other, so that each of the risks can interact with other clusters (i.e., risks) and their sub-factors. Moreover, sub-factors of each risk can influence other factors. The ANP method needs to apply a pairwise comparison matrix. This complicated and sensitive pairwise comparison would be completed by a skilled expert team [40].

In the literature, ANP has been applied in many complicated decision-making problems. The ANP has its own advantages and has produced ideal results in various fields. In the field of oil and gas products, Jafarnezhad et al. [41] proposed ANP for priority of technology transfer methods in oil drilling industry. Valipour et al. [42] developed and tested a comprehensive model for risk assessment of gas refinery EPC projects using the ANP technique. Moradi et al. [43] proposed the risk analysis of oil projects using fuzzy ANP technique.

In this paper, ANP was used to prioritize the causes. Thereafter, all factors affecting fire and explosions of external floating roof tanks were collected and approved. In the next step, checklist composed of criteria and sub-criteria affecting fire and explosion of external floating roof tanks was taken from the previous step. Then, checklist was sent to 30 process and safety experts familiar with the tankers in the oil refinery and they did pairwise comparison between variables in the checklist.

In the first stage, the main criteria are regarding independence, together with the pairwise comparison. In the second stage, sub-criteria for each main criterion were pairwise comparison. For pairwise comparison criteria and sub-criteria, comparison scale of nine levels presented by Saaty was used (Table 2).

To find the matrix priority and compute the consistency ratio (CR), we applied the Expert Choice software.

Steps for applying the ANP methodology are mentioned below [39]:

Step 1: Analyze the problem and determine the main goal.

Step 2: Determine the criteria and sub-criteria that affect the main goal.

Step 3: Determine alternatives for the problem.

Step 4: Determine the interactions between criteria, sub-criteria, and alternatives with respect to the main goal.

Step 5: Construct a super-matrix according to the network and then construct a weighted super-matrix and limit super-matrix. In a super-matrix, each element is represented by one row and one respective column. If the column sum of any column in the composed super-matrix is greater than 1, that column will be normalized. Such a super-matrix is known as weighted super-matrix. The weighted super-matrix is then raised to a significantly large power in order to have converged or stable values. The values of this limit matrix are the desired priorities of the elements with respect to the goal.

Step 6: Prioritize the alternatives and choose the best alternative with the highest priority.

The use of ANP method to solve practical problems is complex; hence, we must use special calculation software. The Super Decisions software will be used to prioritize the causes in this paper.

Super Decisions Software

Super Decisions software is decision-making software which works based on two multi-criteria decision-making methods.

The ANP is implemented in the Super Decisions software and has been applied to various decision problems. It is a coupling of two parts. The first consists of a control hierarchy or network of criteria and sub-criteria that control the interactions in the system under study. The second is a network of influences among the elements and clusters. Applications may be simple, consisting of a single network, or complex, and consisting of the main network and two or more layers of sub-networks. Each network and sub-network is created in its own window [44].

Steps to build an ANP hierarchical decision model using the Super Decisions software as shown below.

Table 1 Causes of fire and explosion in the external floating roof tanks

<i>Tank crack/rupture</i>		<i>Sabotage</i>
<i>Maintenance error</i>		Terrorist attacks and military operations
Sparks from welding	Poor soldering	Arson
Lack of considering the safety in repairs of body and roof tanks	Shell distortion	Theft
Cutting torch (using cutting torch on a tank that contained flammable materials and had not been cleaned)	Poor fabrication	Auto-ignition
Sparks resulting from maintenance and during tank cleaning	Corrosion	Use candles or wicks
Non-explosion-proof motor and tools used	High-pressure liquid from downstream vessels backup subsidence	Electrical equipment (mobile)
	Microbiological sulfate-reducing bacteria	Oils and other flammable materials
		Using chemicals
<i>Operational error</i>	<i>Piping rupture/leak</i>	<i>Open flames</i>
Overflow	Low temperature (cracked walls and leaking)	Adjoining land fire
Lack of timely and accurate measurement the tank products level	Heat stress (caused water vapor or the tilting roof)	Hot particles
Open the drain valve randomly	Flammable liquid leak from a gasket	Flammable vapors flare around tanks
Rubbing off deposits on the tank floor with old and unsafe methods	Leaking on the tank roof	
Depth measuring with metal device (electric create streaming)		
No hot work permit		
Hot work on an empty tank		
Worker smoking (like throwing cigarette butts)		
Operators sampling (a problem in reservoir sample section)		
Oil leakage caused by operator error		
High inlet temperature (in the presence of water in the bottom of the tank, causing the reaction and possible explosion)		
SOP not followed		
<i>Equipment/instrument failure</i>	<i>Static electricity</i>	<i>Natural disasters</i>
Relief valves failure accidentally opened	Lack of insulation of all metal components such as ladders and access routes	Lightning
Frozen valve	Rubber seal cutting	Earthquake
Failure or absence of liquid level indicators	Burden of overcapacity	Wind (storm)
Failure or absence of high-pressure indicators	Wrong connection	Heavy rain

Table 1 continued

Floating roof sunk	Firing caused by current short
Vent valve not open due to corrosion	Carelessness in the handling and use of electrical devices
Discharge valve rupture	Short circuit when pumping petroleum products to the tank (spark caused by the liquid level in the tank)
Leakage through the fractured meter	Risk of electric charge density in the reservoir wall
Failure vacuum breaker	Improper sampling procedure
	Static discharge and sinking of the floating roof
	Fluid transfer
	<i>Faulty firefighting system</i>
<i>Runaway reactions</i>	Infrastructure wear and tear and firefighting equipment (e.g., fixed foam system failure)
Volatile heating reactions (Iron sulfide reacting even though water is present)	
Reaction between hot oil and water emulsion and create a ignited vapor cloud	Inadequate training of staff
High vapor pressure	Incompetent foam and powder to firefighting
	Lack of coordination with urban firefighting equipment
	The lack of cooling tanks monitoring (cooling system and water spray)
	Do not operate an early warning tools and beginning of fire extinguishers

Creation of Clusters and Making Connections Between Them

First, we created priority among the main criteria. To do this, 11 main criteria as nodes within a cluster were created and the connections between them linked them with each other. The main criteria model is shown in Fig. 1. Similarly, node and cluster and internal communication among them were created individually for each sub-criterion.

Criteria and Sub-criteria Pairwise Comparisons

One of the major strengths of the ANP is the use of pairwise comparisons to derive accurate ratio-scale priorities, as opposed to the use of traditional approaches of “assigning weights” which can also be difficult to justify. There are four pairwise comparison assessment modes. We have chosen questionnaire mode to carry out pairwise comparisons.

Formation of Super-Matrix

The priorities derived from the pairwise comparisons are entered in the unweighted super-matrix. In a hierarchical model like this, the weighted super-matrix is the same as the unweighted super-matrix because the clusters are not weighted. Raising the weighted super-matrix to powers yields the limit matrix from which the final answers are extracted. The final priorities for the alternatives are in the column of the goal. Limit matrix for main criteria is shown in Fig. 2. Similarly, the super-matrix tables for each of the sub-criteria were formed.

Synthesis and Sensitivity

The results for the alternatives are obtained with the synthesis command. The Normals column presents the results in the form of priorities. This is the usual way to report results. The Ideals column is obtained from the Normals column by dividing each of its entries by the largest value in the column. The Raw column is read directly from the limit super-matrix. In hierarchical model such as this, the Raw and the Normals columns are the same. These results showed that natural disasters have the highest priority in the causes of fire and explosion in the external floating roof tanks.

The “Ideal” column shows that the results are divided by the largest value so that the more important choice has a priority of 1.0. The others are in the same proportion as in “Normals” and are interpreted this way: Static electricity

with 72.8% is important from operational error and that with 61.4% is important from faulty fire safety system.

Sensitivity analysis is used to analyze how the priorities of the alternative solutions change as we vary the priority of one or more decision-making factors (criteria). Sensitivity rate is desirable to have a value of less than 0.1.

The results of synthesis and sensitivity rate for main criteria are shown in Figs. 3 and 4. Also, the final weight for main criteria and sub-criteria is listed in Table 3.

Important Findings and Discussion

By the weight of the various risk factors, we can conclude that several big risk factors (causes) in fire and explosion in the external floating roof tanks are natural disasters, static electricity, operational error, faulty firefighting system, maintenance error, piping rupture/leak, equipment/instrument failure, open flames, tank crack/rupture, runaway reactions, and sabotage, respectively (Results of Table 3). In the following, criteria and sub-criteria in order of priority are discussed.

Natural Disasters

As indicated in Table 3, natural disasters are allocated the highest rank in the cause of fire and explosion. The oil industry can be adversely affected by natural disasters such as lightning, earthquakes, tornados. Natural events are identified as the principal cause of the accidents in atmospheric storage tanks [45]. Among natural disasters, lightning sub-criteria had the highest priorities, although lightning is by far the most frequent source of ignition in oil tanks with regards to the occurrence of fires within floating roof storage tanks [16]. According to previous findings, lightning accounts for about 61% of all accidents in storage and processing operations [45].

Static Electricity

The second rank of fire and explosion cause in tanks is static electricity. In the storage tanks, static electricity is generated during the filling of the product which can develop a static charge between the tank shell and liquid surface [46]. In atmospheric storage tanks, static electricity may be produced in some ways, such as the attendance of debris which may float and thus be isolated from the floor and become charged as the liquid is static [47].

On the other hand, static discharge and sinking of floating roof sub-criteria had the highest rating. In the LASTFIRE survey (2012), static electricity has been assumed as the source of ignition that has occurred when foam has been placed onto tanks upon discovery that the

Table 2 Scale of relative importance (according to Saaty [39])

Intensity of importance	Definition
1	Equal importance
2	Weak
3	Moderate importance
4	Moderate plus
5	Strong importance
6	Strong plus
7	Very strong or demonstrated importance
8	Very, very strong
9	Extreme importance

roof has sunk or partly sunk [48]. LASTFIRE survey (2012) described that the static discharge may occur if the electrical bonding between the shell and roof of the tank or the earthing of the tank is insufficient [48]. External floating roof tanks require bonding shunts between the wall and the floating roof tank. Although these shunts are used for lightning protection, they also provide protection from electrostatic charges caused by the product's movement [46].

Operational Error

Good operating procedures are the main point in the safe operation of a process industry. Operating procedures are integral to the general management of process safety, as both a source and a safeguard against operational error.

One of the most important operational sub-criteria is standard operating procedure (SOP). SOPs are used for the safe and effective operation of industrial plants, including oil and gas facilities [49]. Sometimes instead of the term SOP, terms such as protocols, instructions, worksheets, and laboratory operating procedures may also be used. But SOPs are frequently developed late in the project after the design is completed and construction is well underway. SOPs may be used for little other than operator training. Being used this way, SOPs have little impact on either the design or the operation of the facility (Fig. 5) [50].

Faulty Firefighting System

A fixed or a semi-fixed firefighting system is one practical method to protect flammable liquid storage tanks against fire. If these systems are incorrectly installed, they may cause damage to the owner's property and forced outage risks will increase, while operator's personnel safety will decrease. A firefighting system can be used for fire prevention, control, or direct extinguishing of any flammable

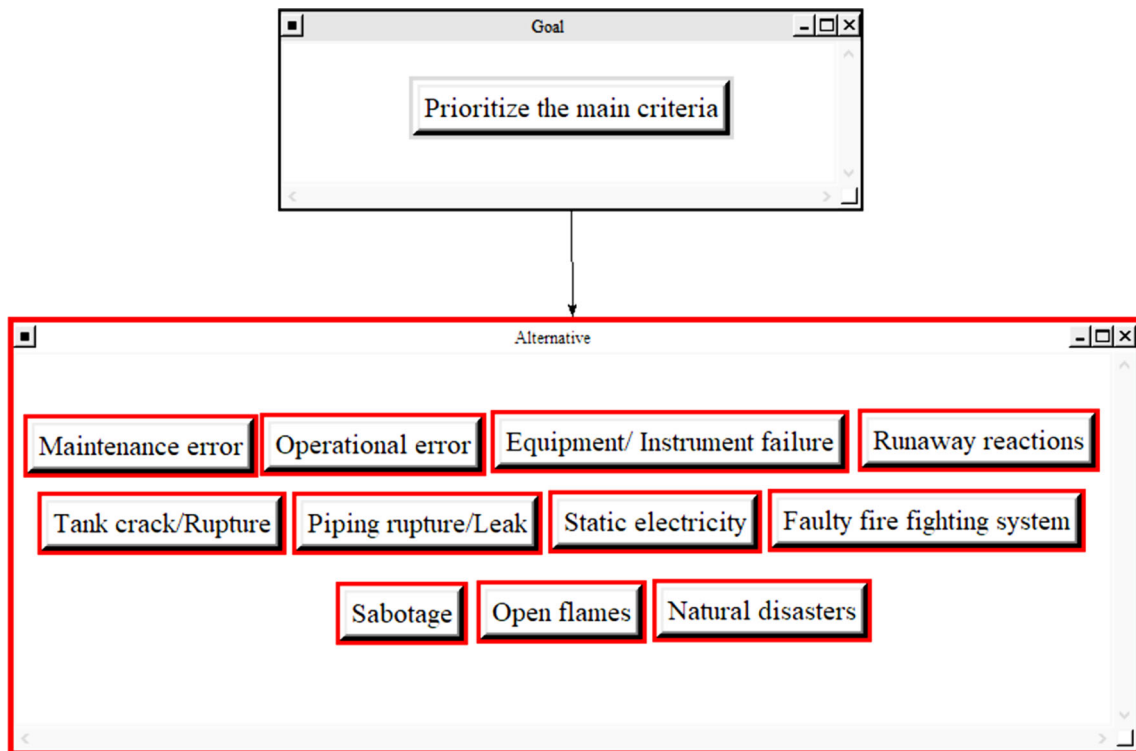


Fig. 1 Main criteria model

Final priorities for the Alternatives

Cluster Node Labels		Alternative							Goal
		Open flames	Operational error	Piping rupture/Leak	Runaway reactions	Sabotage	Static electricity	Tank crack/Rupture	Prioritize the main criteria
Alternative	Equipment/ Instrument failure	0.000000	0.000000	0.000000	0.000000	0.000000	0.000000	0.000000	0.055567
	Faulty fire fighting system	0.000000	0.000000	0.000000	0.000000	0.000000	0.000000	0.000000	0.107883
	Maintenance error	0.000000	0.000000	0.000000	0.000000	0.000000	0.000000	0.000000	0.095287
	Natural disasters	0.000000	0.000000	0.000000	0.000000	0.000000	0.000000	0.000000	0.223927
	Open flames	0.000000	0.000000	0.000000	0.000000	0.000000	0.000000	0.000000	0.048643
	Operational error	0.000000	0.000000	0.000000	0.000000	0.000000	0.000000	0.000000	0.137523
	Piping rupture/Leak	0.000000	0.000000	0.000000	0.000000	0.000000	0.000000	0.000000	0.064179
	Runaway reactions	0.000000	0.000000	0.000000	0.000000	0.000000	0.000000	0.000000	0.034045

Fig. 2 Limit matrix for main criteria

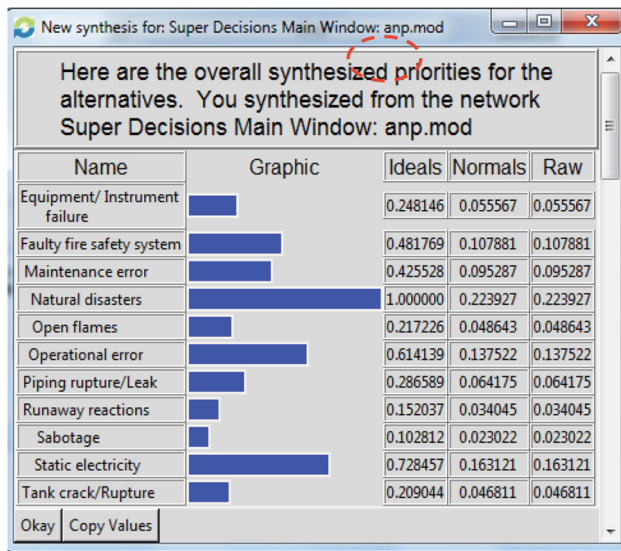


Fig. 3 Main criteria synthesis

liquid fire within the tank. Presently, in floating roof tanks, fixed foam system is used for extinguishing rim seal fires [51]. Fire system infrastructure failure is one of the most important weaknesses in firefighting. When engineered, installed, and maintained correctly, these systems will offer many years of reliable service [52].

Maintenance Error

Maintenance is a key activity to reduce the risk of major accidents. On the other hand, maintenance may have a negative effect on barrier performance if the execution is incorrect, insufficient, delayed, or excessive. Also, it can be the cause of an incident, for example, by operating equipment wrongly [53].

Based on the results, one of the most dangerous factors which create a risk of fire among maintenance error is welding. According to the LASTFIRE incident survey (1997) result, two rim seal fires were recorded due to hot work on tanks. In these cases, heat from welding caused flammable vapors to be emitted from hydrocarbon deposits [34]. In August 2008, a fire occurred in a crude oil atmospheric storage tank with a capacity of 80,000 m³ in Ra's Lanuf; the cause of the fire was attributed to hot work [54].

Piping Rupture/Leak

A leak or rupture of the tank or pipe can be caused by the brittle failure of tank walls, welds, or connected pipework due to the use of inadequate materials, combined with loading such as wind, earthquake, or impact that can release some or all of their contents. In the event of a leak or rupture, these materials may be ignited and cause a fire

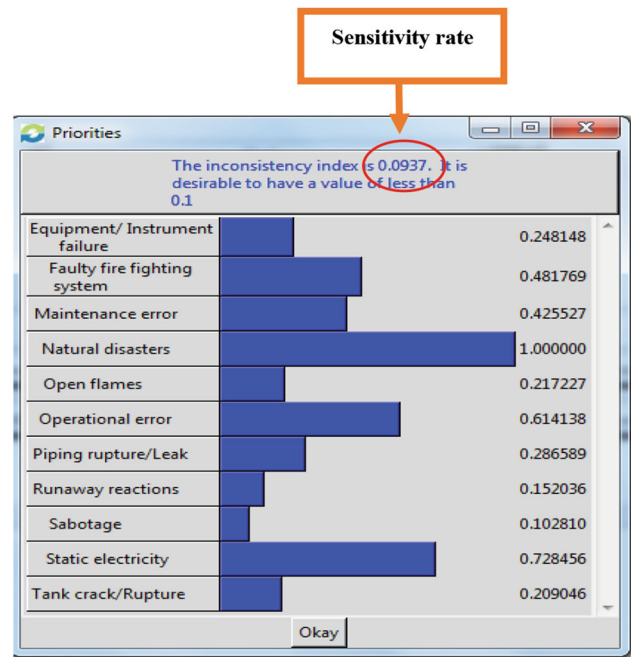


Fig. 4 Main criteria sensitivity rate

that could result in injury or possibly fatality [55]. The uncertainty in values for atmospheric storage tanks could be represented by a range of at least a factor of 10 either higher or lower. Estimates of leak frequencies for large pressure piping for both the overall leak frequencies and the rupture frequencies range over four orders of magnitude. The LASTFIRE data are considered the most reliable source for releases from floating roof tanks.

Leaking on the tank roof sub-criteria achieved the highest probability of fire and explosion in external floating roof tank. Water on the roof is usually drained from a flexible hose or other special drain line system that runs from a drain sump on the roof through the stored liquid to a drain valve on the shell at the base of the tank. A hose often develops leaks and drains both water and product, while other drain lines do not leak [56].

Equipment/Instrument Failure

Equipment failure could have a massive negative effect on employee safety and loss of production in the oil industry. Further, in the oil refinery, reliability and safety go hand-in-hand due to their growing recognition. Equipment that is improperly maintained, malfunctioning, or operating outside its design limits exposes employees to risk [57].

The most common failure on the floating roof is due to the sinking of the floating roof. The floating roof is overtopped by the liquid inside the tank and the roof sink or maybe the tank will ignite due to the spark generated during the unstable movement of the roof [16]. If

Table 3 Weight prioritization main criteria and sub-criteria for fire and explosion in the external floating roof tanks

Ranking	Main criterion	Weight obtained (%)	Ranking	Sub-criteria	Weight obtained (%)	Sensitivity rate
1	Natural disasters	100	1	Lightning	100	0.089
			2	Heavy rain	52.9	
			3	Earthquake	26.6	
			4	Wind (storm)	14.5	
2	Static electricity	72.8	1	Static discharge and sinking of the floating roof	100	0.092
			2	Rubber seal cutting	98.6	
			3	Lack of insulation of all metal components such as ladders and access routes	70.7	
			4	Short circuit when pumping petroleum products to the tank	58.1	
			5	Burden of overcapacity	46.7	
			6	Firing caused by current short	45.2	
			7	Risk of electric charge density in the reservoir wall	31.9	
			8	Improper sampling procedure	31.0	
			9	Wrong connection	28.6	
			10	Fluid transfer	23.9	
			11	Carelessness in the handling and use of electrical devices	20.7	
3	Operational error	61.4	1	SOP not followed	100	0.095
			2	No hot work permit	83.3	
			3	Hot work on an empty tank	80.6	
			4	Overfill	72.2	
			5	Rubbing off deposits on the tank floor with old and unsafe methods	64.4	
			6	Depth measuring with metal device (electric create streaming)	59.9	
			7	Oil leakage caused by operator error	51.1	
			8	Worker smoking (like throwing cigarette butts)	46.2	
			9	Lack of timely and accurate measurement of the tank products level	40.2	
			10	Open the drain valve randomly	31.2	
			11	Operators sampling (a problem in reservoir sample section)	26.1	
			12	High inlet temperature	21.1	
4	Faulty firefighting system	48.1	1	Infrastructure wear and tear and firefighting equipment (e.g., fixed foam system failure)	100	0.097
			2	Do not operate an early warning tools and beginning of fire extinguishers	92.8	
			3	Incompetent foam and powder to firefighting	78.2	
			4	Inadequate training of staff	61.6	
			5	Lack of coordination with urban firefighting equipment	53.6	
			6	Lack of cooling tanks monitoring (cooling system and water spray)	32.8	

Table 3 continued

Ranking	Main criterion	Weight obtained (%)	Ranking	Sub-criteria	Weight obtained (%)	Sensitivity rate
5	Maintenance error	42.5	1	Sparks from welding	100	0.096
			2	Lack of considering the safety in repairs of body and roof tanks	42.5	
			3	Non-explosion-proof motor	28.5	
			4	Sparks resulting from maintenance and during tank cleaning	14.5	
			5	Cutting torch	11.4	
6	Piping rupture/leak	28.6	1	Leaking on the tank roof	100	0.053
			2	Low temperature (cracked walls and leaking)	48.3	
			3	Heat stress (caused water vapor or the tilting roof)	34.2	
			4	Flammable liquid leak from a gasket	16.7	
7	Equipment/instrument failure	24.8	1	Floating roof sunk	100	
			2	Failure or absence of liquid level indicators	92.7	
			3	Vent valve not open due to corrosion	91.9	
			4	Frozen valve	75.3	
			5	Relief valves failure accidentally opened	70.1	
			6	Failure or absence of high-pressure indicators	65.1	
			7	Discharge valve rupture	54.9	
			8	Leakage through the fractured meter	41.1	
			9	Failure vacuum breaker	33.4	
8	Open flames	21.7	1	Adjoining land fire	100	0.051
			2	Flammable vapors flare around tanks	41.9	
			3	Hot particles	26.4	
9	Tank crack/rupture	20.9	1	Shell distortion	100	0.093
			2	Poor fabrication	73.4	
			3	Corrosion	51.7	
			4	Microbiological sulfate-reducing bacteria	37.3	
			5	Poor soldering	36.7	
			6	High-pressure liquid from downstream vessels backup subsidence	35.5	
10	Runaway reactions	15.2	1	Volatile heating reactions (despite the iron sulfide in the presence of water will start to burn)	100	0.070
			2	Reaction between hot oil and water emulsion and create a ignited vapor cloud	43.6	
			3	High vapor pressure	19.1	

Table 3 continued

Ranking	Main criterion	Weight obtained (%)	Ranking	Sub-criteria	Weight obtained (%)	Sensitivity rate
11	Sabotage	10.2	1	Use candles or wicks	100	0.092
			2	Using chemicals	93.6	
			3	Arson	76.6	
			4	Auto-ignition	69.6	
			5	Oils and other flammable materials	62.8	
			6	Electrical equipment (mobile)	49.9	
			7	Terrorist attacks and military operations	45.1	
			8	Theft	27.3	

the floating roofs are inadequately designed or wrong approaches were applied to the design, the roof will fail and the pontoon will be buckled and damaged. On January 25, 2014, the floating roof sank into the stabilized condensate tank 5E-220-TB002A at Mellitah complex due to the heavy fire water/foam [58].

Open Flames

Open flames can be considered as an external source of heat in the tanks fire and explosion. The most important open flames sub-criteria in the floating roof tank fire were ground fires or adjoining land fire, flammable vapors flare around tanks, and hot particles, respectively. In the incident at a Baton Rouge, Louisiana refinery fire was caused by the ground fires or explosion close by [31].

Tank Crack/Rupture

Most storage tank damage is attributable to age deterioration, corrosion, and seismic motions. Cracks usually occur at the bottom or the welding edges. A 1970 crack at the bottom of a crude oil storage tank at a Kaohsiung, Taiwan refinery, was attributed to the slow subsidence of the foundation [59]. Cracks in the floating roof tank top always occur only on the edge of the oil tank top which is just the weakest area [60, 61].

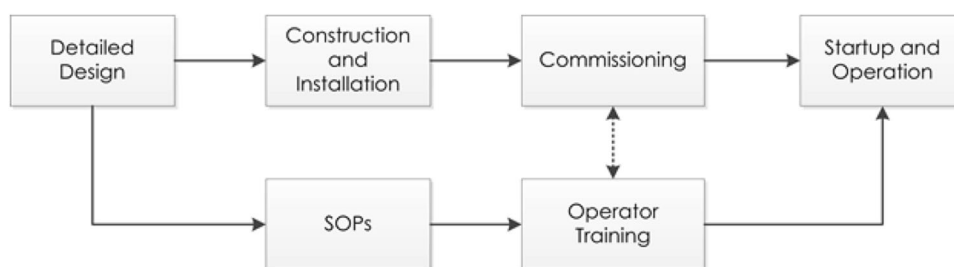
To prevent the shell distortion that was the first priority of the sub-criteria, Greenwood [62] suggested that an average tilt of possibly more than 0.5% of the best-fit rigid-settlement tilt plane could be experienced before the distortion (i.e., out-of-roundness) at the top ring girder of a floating roof tank and would cause binding between the roof and the shell [63]. Also in the floating roof tanks, mechanical seals are unsuitable for distorted tank shells or where shell coatings have been applied. Liquid seals are suitable for all tanks, but particularly where tank shell distortion is present.

Runaway Reactions

A runaway reaction is a chemical reaction over which control has been lost. It continues to accelerate in reaction speed until it runs out of reactants [64]. Exothermic runaway reactions may occur when impurities or foreign materials are present in the storage tanks.

According to the results, runaway reaction is less important in the development of external floating roof tanks fire. Many of the runaway chemical reactions occurred in reaction tanks that failed or even exploded by means of thermal runaway. The temperature of the reaction increased rapidly resulting in increased pressure as liquids evaporated, and the tank failed because of the increased

Fig. 5 Wrong set-up of the SOP



pressure. Other incidents occurred because of inadvertent mixing of incompatible materials or chemicals that exploded because of instability [65]. As seen, volatile heating reactions had to be rated first among other sub-criteria.

Sabotage

The last criterion effective in external floating roof tank explosion fire is sabotage. In 1972, four external floating roof tanks containing 500,000 barrels were sabotaged in Trieste, Italy. During this incident, foam lines are widely burned and damaged and bomb attack destroyed two tanks [31]. Fire damaged six more tanks. Pit fires spread to roof seals; roof sank and boilover occurred. The use of candles or wicks achieved the highest degree from the perspective of experts in fire and explosion.

Conclusion

In this paper, prioritizing the causes of fire and explosion in the external floating roof tanks was put forward. The relationship between the 11 main criteria and 71 sub-criteria effective in the fire and explosions was evaluated. Weighting and prioritization of criteria and sub-criteria were performed by ANP method and Super Decisions software. This study will help to identify the importance of each of the effective risk factors in fire and explosion in external floating roof tanks. That way, we can prioritize and implement control measures to prevent any risk factors in fire and explosion.

Acknowledgment The authors are grateful to Health Faculty of Tabriz University of Medical Sciences for funding this work under the master's thesis (Project Reference: 5/D/35901). The authors are also grateful to experts of safety and process of refineries in Tabriz, Tehran, and to those who helped us collect the data.

References

1. F. Centeno, E.E.C. Rodrigues, Reduced-scale study of liquid fuel storage tank fire using fire dynamics simulator. *Therm. Eng.* **14**(1), 40–46 (2015)
2. X. Fu et al., Application of compressed air foam system in extinguishing oil tank fire and middle layer effect. *Procedia Eng.* **45**, 669–673 (2012)
3. K.R. Marianayagam, *Numerical Simulation Study on Parameters related to Athabasca Bitumen Recovery with SAGD. Earth Sciences and Petroleum Engineering* (Institutt for petroleumsteknologi og anvendt geofysikk, Norwegian University of Science and Technology, Trondheim, 2012), p. 57
4. H. Zhao, J.S. Liu, The feasibility study of extinguishing oil tank fire by using compressed air foam system. *Procedia Eng.* **135**(1), 61–66 (2016)
5. E. Akyuz, Quantification of human error probability towards the gas inerting process on-board crude oil tankers. *Saf. Sci.* **80**, 77–86 (2015)
6. Z. Nivolianitou, et al., A methodology for the hazard assessment in large hydrocarbon fuel tanks. *Chem. Eng. Trans.* **26**, 171–176 (2012)
7. W. Wen-hea, X. Zhi-shenga, S. Bao-jiang, Numerical simulation of fire thermal radiation field for large crude oil tank exposed to pool fire. *Procedia Eng.* **52**, 395–400 (2013)
8. S. Lin, P. Yi, Y. Shuangchun, The cause of fire and preventive measures in oil depot. *Int. J. Eng. Res. Dev.* **4**(11), 55–57 (2012)
9. F. Zhang, H. Jiang, C. Zhang, Study of charging nitrogen to external floating roof tank to prevent rim-seal fires from lightning. *Procedia Eng.* **71**, 124–129 (2014)
10. J. Guan et al., Experiment study of oil tank fire characteristics dependent on the opening of tank top. *Procedia Eng.* **62**, 932–939 (2013)
11. C.D. Argyropoulos et al., Modelling pollutants dispersion and plume rise from large hydrocarbon tank fires in neutrally stratified atmosphere. *Atmos. Environ.* **44**, 803–813 (2010)
12. C.H. Shelley, storage tank fires: is your department prepared? *Fire Eng.* **161**(11), 63 (2008)
13. T. Ennis, Pressure relief considerations for low-pressure (atmospheric) storage tanks. *Symp. Ser.* **151**, 1–13 (2006)
14. J. Taveau, Explosion of fixed roof atmospheric storage tanks, part 1: background and review of case histories. *Process Saf. Prog.* **30**(4), 381–392 (2011)
15. A.M. Thyer, et al., A review of catastrophic failures of bulk liquid storage tanks. *Loss Prev. Bull.* **1**(205), 3–11 (2009)

16. K. Mansour, *Fires in Large Atmospheric Storage Tanks and Their Effect on Adjacent Tank* (Loughborough University, Loughborough, 2012)
17. API, *Evaporative Loss Measurement*. in *Manual of Petroleum Measurement Standards*. Ch. 19, Sec. 2-E., Washington, DC: API (1997)
18. API, *API Standard 650, Welded Steel Tanks for Oil Storage*, tenth edition. Washington (1998)
19. A. Alaska, *Fire Hazard Assessment for Valdez Crude Tank Internal Floating Roofs* (Alyeska Pipeline Service Company, Alaska, 2004)
20. C.B. Ching, J.R. Lockwood, *An Application Of Fire Science To An Industrial Incident Fire Safety Science Digital Archive* (National University of Singapore, India, 1988)
21. K.S. Yeng, *Design, Construction and Operation of the Floating Roof Tank*. Course ENG 4111 and ENG 4112 Research Project (2009)
22. API, *Evaporative Loss From External Floating Roof Tanks* (American Petroleum Institute, Washington, 1989)
23. R. Park, *VOC Emissions From Volatile Organic Liquid Storage Tanks-Background Information For Proposed Standards*, EPA-450/3-81-003a. U. S. Environmental Protection Agency (1984)
24. D.O. Nwabueze, *Liquid hydrocarbon storage tank fires—how prepared is your facility?* Chem. Eng. Trans. **48**, 301–306 (2016)
25. EPA, *Alternative Control Techniques Document: Volatile Organic Liquid Storage in Floating and Fixed Roof Tanks* (U.S. Environmental Protection Agency, Washington, 1994)
26. *Manual Of Petroleum Measurement Standards: Chapter 19: Evaporative Loss Measurement, Evaporative Loss From Floating Roof Tanks*. American Petroleum Institute, Washington, DC (1994)
27. R.L. Ferry, *Estimating Storage Tank Emissions-Changes Are Coming* (TGB Partnership, Hillsborough, 1994)
28. EPA, *Benzene Emissions From Benzene Storage Tanks-Background Information For Proposed Standards*. EPA-450/3-80-034a, U. S. Environmental Protection Agency, Research Triangle Park, NC (1980)
29. TICO, *Storage tank. Turnkey project solution. Internal Floating Roof Tank VS External Floating Roof Tank, Which Is Better?. Concept of external floating roof tank. A complete solution for tanks. Floating Roof Tank. External Floating Roof Tank. BNH. Gas tanks. Tags: Floating Roof Tank. Manufacturer, Exporter, India, Cheap Cost*
30. J.I. Changa, C.C. Lin, *A study of storage tank accidents*. J. Loss Prev. Process Ind. **19**, 51–59 (2006)
31. H. Persson, A. Lönnermark, *Tank Fires: Review of Fire Incidents 1951–2003* (SP Swedish National Testing and Research Institute, Borås, 2004)
32. A.A. Israel, *Lightning protection of floating roof tanks*. Am. J. Eng. Res. AJER **2**(10), 11–21 (2013)
33. API, *Verification of lightning protection requirements for above ground hydrocarbon storage tanks*. API/EI Research Report (2009)
34. LASTFIRE, *Review of Escalation Mechanisms* (Resource Protection International, Buckinghamshire, 1997)
35. API, *Interim Study-Prevention and Suppression of Fires in Large Aboveground Atmospheric Storage Tanks*. API Publication 2021A (1998)
36. T. Saaty, *Fundamentals of the analytic network process*. in *The fifth international symposium on the analytic hierarchy process ISAHP*. August, Kobe, Japan. (12–14), p. 1–14 (1999)
37. W. Eddie, L. Heng, *Application of ANP in process models: an example of strategic partnering*. Build. Environ. **42**, 278–287 (2007)
38. Ş. Gür, M. Hamurcu, T. Eren, *Using analytic network process and goal programming methods for project selection in the public institution*. Les Cahiers MECAS **13**, 36–46 (2016)
39. T. Saaty, *The Analytic Hierarchy Process* (McGraw-Hill, New York, 1980)
40. T. Saaty, *Decision Making with Dependence and Feedback: the Analytic Network Process* (RWS Publications, Pittsburgh, 1996)
41. A. Jafarnezhad, E. Asgharizadeh, G. Asemian, *Priority of technology transfer methods in oil drilling industry by using analysis network process (ANP)*. Int. J. Learn. Dev. **3**(5), 15–25 (2013)
42. A. Valipour et al., *Analytic network process (ANP) to risk assessment of gas refinery EPC projects in Iran*. J. Appl. Sci. Res. **9**(3), 1359–1365 (2013)
43. M. Moradi, A. Fatemi, H. Soltanpanah, *The risk analysis of oil projects using fuzz ANP technique*. Int. Res. J. Manag. Sci. **2**(2), 55–61 (2014)
44. T. Saaty, *The Analytic Hierarchy Process (AHP) for Decision Making and The Analytic Network Process (ANP) for Decision Making with Dependence and Feedback: Super Decisions* (2003)
45. W. Atherton, J. Ash, *Review Of Failures, Causes & Consequences In The Bulk Storage Industry* (2007)
46. D. Sullivan, P. Curran, *Static Ignition Hazards When Handling Petroleum Products* (Fiberglass Tank & Pipe Institute, Houston, 2013), pp. 1–10
47. R. Alaimo, *Handbook of Chemical Health and Safety* (American Chemical Society, Washington, 2001)
48. LASTFIRE, *Review of Escalation Mechanisms* (Resource Protection International, Buckinghamshire, 2012)
49. EPA, *Guidance document for the writing of standard operating procedures Taken from United States Environmental Protection Agency Guidance for Preparing Standard Operating Procedures (SOPs) EPA QA/G-6* (2007)
50. H. Duhon, *SOPs That Operators Will Actually Want To Use: A Guide to Writing Effective SOPs* (Society of Petroleum Engineers, 2015), p. 31
51. L. Xu-qing, L. Quan-zhen, G. Hong, *Study of fire fighting system to extinguish full surface fire of large scale floating roof tanks*. Procedia Eng. **11**, 189–195 (2011)
52. Chemguard, *Fixed or Semi-Fixed Fire Protection Systems for Storage Tanks*. 204 S. 6th Ave • Mansfield, Tx 76063. www.chemguard.com (2005)
53. P. Okoh, S. Haugen, *The influence of maintenance on some selected major accidents*. Chem. Eng. Trans. **31**, 493–498 (2013)
54. K.A. Mansour, *Fires in large atmospheric storage tanks and their effect on adjacent tanks*, pp. 22. Doctoral dissertation (2012)
55. OGP, *Risk assessment data directory storage incident frequencies*. Int. Assoc. Oil Gas Prod. **3**(434), 7–18 (2010)
56. Wikipedia, *External floating roof tank* (2015)
57. CLG, *Creating a Reliability Culture: CASE STUDY*. CLG • 500 Cherrington Parkway. www.clg.com (2010)
58. B.V. M.O.a.G., *Floating Roof sinking Failure report of Condensate Tank 5E-220-TB002A*. Acting Production Eng. Coordinator (2014)
59. C. Lin, *A safety study of oil tank farms*. M.S. thesis. National Kaohsiung First University of Science and Technology, Kaohsiung, Taiwan, ROC (2003)
60. S. Li, *Oil tank fire statistical analysis*. Fire Control Theory Res. **4**, 117 (2004)
61. Y. Yao, *Oil tank fire mode and behavior of the fire*. Nat Gas Oil **27**, 20 (2006)
62. D.A. Greenwood, *Differential settlement tolerance of cylindrical steel tanks for bulk liquid storage. Proceeding of the conference on settlement of structures*. British geotechnical society, Cambridge, England (1974)

63. S. Gazioglu, J. Withiam, Evaluation of a Differentially Settled Tank. Missouri University of Science and Technology (Scholars' Mine) (1984)
64. E2G, Pressure Relief Systems for Runaway Reactions. Engineers at E2G/The Equity Engineering Group, Inc. (2017)
65. PEAC, Runaway Industrial Chemical Reactions (2006)