

The Effect of Sb Addition on Sn-Based Alloys for High-Temperature Lead-Free Solders: an Investigation of the Ag-Sb-Sn System

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Today there is renewed interest in alloys belonging to the Sb-Sn-X (X = Cu, Ag, Bi) ternary systems and their phase equilibria, phase transformations, and thermodynamic properties because of their possible use as high-temperature lead-free solders in the electronics industry. The integral mixing enthalpy of Ag-Sb-Sn liquid alloys has been measured along five different sections ($\text{Ag}_{0.25}\text{Sn}_{0.75}$, $\text{Ag}_{0.50}\text{Sn}_{0.50}$, $\text{Sb}_{0.30}\text{Sn}_{0.70}$, $\text{Sb}_{0.50}\text{Sn}_{0.50}$, and $\text{Sb}_{0.70}\text{Sn}_{0.30}$) at 530°C, 600°C, and 630°C, using a high-temperature Calvet calorimeter by dropping pure elements (Ag or Sb) in the binary alloy liquid bath. The ternary extrapolation models of Muggianu and Toop were used to calculate the integral enthalpy of mixing and to compare measured and extrapolated values. Selected ternary alloys have been prepared for thermal investigation by using a differential scanning calorimeter at different heating/cooling rates in order to clarify the temperature of the invariant reactions and the crystallization path.

Key words: Ag-Sb-Sn system, enthalpy of mixing, lead-free solder, calorimetry

INTRODUCTION

In recent years, the electronics industry has been involved in the development of a new generation of solder interconnects to replace Pb-Sn with Pb-free solder alloys. This is due to legal, environmental, and technological factors which call for alternative lead-free soldering materials. Among the huge number of systems proposed, many of the most promising lead-free alloys are tin-based systems.¹ Sn-Ag-Cu system solders are currently being considered to be the choice for replacing 63 wt.%Sn-37 wt.%Pb eutectic alloy, whose melting point is 183°C. However, high-temperature Pb-Sn solder with 90 wt.% to 95 wt.% Pb (melting temperature around 280°C), which are used for flip-chip joints,

also need to be replaced, and Ag-Sb-Sn alloys can be one of the promising series of high-temperature lead-free solders. As well as an appropriate melting range, Ag-Sb-Sn alloys also show good thermofatigue resistance.² Commercial solders based on the Ag-Sb-Sn system are currently available, e.g., CASTIN (0.8Cu-0.5Sb-2.5Ag-96.2Sn, wt.%) and J-alloy (Sn-25Ag-10Sb, wt.%). Knowledge of the thermodynamic properties of a solder system is important for understanding the soldering process as well as the final reliability of the joints. However, literature data for the Ag-Sb-Sn system are scarce. The aim of the current work is to measure the mixing enthalpy of Ag-Sb-Sn liquid alloys and to clarify the phase relations in the Ag-Sb-Sn system on the basis of some key selected alloy compositions.

LITERATURE REVIEW

Some thermodynamic data are available in the literature for the Ag-Sb-Sn ternary system and its

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constituent binary systems. The thermochemical data concerning the mixing enthalpy of liquid alloys obtained by calorimetric measurements as well as the phase diagram literature data about the ternary system are reviewed here. Some available information on activity is also reported.

Ag-Sb System

Calorimetric measurements were performed by Kawakami,³ who obtained the Ag-Sb mixing enthalpies at 1050°C in the $0.18 < x_{\text{Sb}} < 0.79$ composition range, and by Ehrlich⁴ at 975°C for the $0.075 < x_{\text{Sb}} < 0.90$ composition range. These results were reported by Hultgren.⁵ Castanet⁶ carried out experiments for the whole composition range at 677°C, 827°C, and 1027°C and observed a strong temperature dependence of the enthalpy of mixing. Predel and Emam⁷ studied calorimetrically the thermodynamic properties of the liquid alloys at 1000°C over the entire composition range. Electromotive force (EMF) measurements were carried out by Vechorv,⁸ Nozaki,⁹ and Okajima and Sakao¹⁰ at different temperatures, and vapor pressure measurements were carried out by Hino.¹¹

Ag-Sn System

Kleppa¹² measured the mixing enthalpy of Ag-Sn alloys in the composition range $0.64 < x_{\text{Sn}} < 0.99$ at 450°C using a dissolution calorimeter with a liquid tin bath. Direct reaction calorimetry has been employed by different scientists to measure the mixing enthalpy for the Ag-Sn system: Wittig and Gehring¹³ in the composition range $0.072 < x_{\text{Sn}} < 0.931$ at 975°C, Castanet¹⁴ in the range $0.05 < x_{\text{Sn}} < 0.95$ at 1000°C, and Rakotomavo¹⁵ in the range $0.02 < x_{\text{Sn}} < 0.934$ at 1100°C. Recently, Flandorfer¹⁶ carried out calorimetric measurements at five temperatures in the interval of 500°C to 1250°C, mainly in the Sn-rich side, and at 1250°C for the Ag-rich side. The data published up to 1973 have been assessed by Hultgren.⁵

The activity of Ag in liquid alloys has been determined by Yamaji¹⁷ and Okajima¹⁰ by an EMF method. The activity of Sn in liquid Ag-Sn alloys has been extensively measured at different temperatures by Frantik,¹⁸ Yanko,¹⁹ Nozaki,⁹ Laurie,²⁰ Elliot,²¹ Chowdhury,²² Kubaschewski,²³ Yamaji,¹⁷ Okajima,¹⁰ Fahri,²⁴ Seetharaman,²⁵ Iwase,²⁶ and Kameda.²⁷

Sb-Sn System

The mixing enthalpy of liquid Sb-Sn alloys has been measured by Kawakami,³ Witting and Gehring,²⁸ Yasawa,²⁹ Sommer,³⁰ and Azzaoui³¹ at various temperatures. Dissolution enthalpy of solid Sb in liquid Sn at 450°C was measured by Kleppa³² by Sn solution calorimetry. EMF measurement has been carried out and the chemical potential of the liquid phase was determined by Frantik and McDonald,³³ Yanko,³⁴ Hao,³⁵ Itho,³⁶ and Vassiliev.^{37,38}

Ag-Sb-Sn System

Gather³⁹ measured the mixing enthalpy of the Ag-Sb-Sn ternary system along four sections at 951°C and one section at 980°C using a heat flow calorimeter. Onderka⁴⁰ performed electrochemical studies of the thermodynamic properties of ternary Ag-Sb-Sn alloys by an EMF method along three cross-sections with a constant Ag/Sb ratio equal to 1/3, 1/1, and 3/1. The Sn compositions were from 10 at.% up to 80 at.% Sn at 10 at.% intervals, and the measurements were carried out in the temperature range from 973 K to 1223 K.

Literature data relating to the invariant reactions detected in the Ag-Sb-Sn system are summarized in Table I, together with the experimental results determined in this work. Table II summarizes the binary invariant reactions relevant to the Ag-Sb-Sn ternary system.

Masson and Kirkpatrick² as well as Chen⁴² determined the liquidus surface and the invariant reactions of the Ag-Sb-Sn system using differential thermal analysis (DTA) combined with metallographic analysis. Cheng and Lee⁴³ determined the Ag-Sb-Sn isothermal section at room temperature in the Ag-rich corner by x-ray diffraction (XRD) and metallographic analyses. The isothermal sections at 220°C and 250°C were reported, respectively, by Oberndorff⁴⁴ and Chen⁴²; Lin⁴⁵ investigated the isothermal sections at 400°C and 150°C and Zheng⁴⁶ reported the room temperature isothermal section. Oh⁴⁷ critically assessed all available experimental data and achieved a satisfactory representation of the literature data. However, no experimental information was available for the invariant reaction for which a temperature value of 329°C, higher than p_6 (321°C), was calculated, and a P-type equilibrium was suggested. Schmid-Fetzer⁴⁸ reviewed the literature relating to this system and proposed the solidification diagram, mainly on the basis of the work of Oh. However, he pointed out that the invariant reaction $P_1: L + \beta + \epsilon \leftrightarrow \text{Sn}_3\text{Sb}_2$ reported by Oh⁴⁷ is not correct, since the composition of Sn_3Sb_2 is not located in the tie-triangle formed by the other three phases. Therefore, Schmid-Fetzer modified the invariant reaction to U-type ($U_2: L + \beta \leftrightarrow \epsilon + \text{Sn}_3\text{Sb}_2$). Recently, Chen⁴² performed differential scanning calorimetry (DSC) analysis using a scanning rate of 10°C/min and proposed a temperature of 314°C for this reaction. Moreover, in a previous paper,⁴⁹ the same authors stated that the Sn_3Sb_2 phase is stable down to room temperature, while during a critical reinvestigation on Sb-Sn performed by us,⁵⁰ we proved the decomposition of this phase, in agreement with Predel's version.⁵¹ The more recent assessment of the Ag-Sb-Sn system made by Gierlotka⁵² was based on Chen's experimental results,^{42,49} and therefore the phase relations should be revised.

EXPERIMENTAL PROCEDURES

The starting materials were Ag (Johnson-Matthey Ltd., 99.99%), Sn (Newmet koch, 99.999%),

Table I. Invariant reactions detected in the Ag-Sb-Sn ternary system

| Type of Reaction | Invariant Reaction | Temperature (°C) | | Reference |
|------------------|--|------------------|------------|-----------|
| | | Experimental | Calculated | |
| U ₁ | L + (Sb) ↔ ε + β | | 375 | 47 |
| P ₁ | L + β + ε ↔ Sn ₃ Sb ₂ | | 329 | |
| U ₂ | L + Sn ₃ Sb ₂ ↔ ε + (Sn) | | 232 | |
| U ₁ | L + (Sb) ↔ ε + β | 379 | | 42 |
| U ₂ | L + β ↔ ε + Sn ₃ Sb ₂ | 314 | | |
| U ₃ | L + Sn ₃ Sb ₂ ↔ ε + (Sn) | 233 | | |
| U ₁ | L + (Sb) ↔ ε + β | 375 | | This work |
| U ₂ | L + β ↔ ε + Sn ₃ Sb ₂ | 308 | | |
| U ₃ | L + Sn ₃ Sb ₂ ↔ ε + (Sn) | 229 | | |

Table II. Binary invariant reactions relevant to the Ag-Sb-Sn ternary system

| Binary System | Type of Reaction | Invariant Reaction | T (°C) | Reference |
|---------------|------------------|--|--------|-----------|
| Ag-Sb | p ₂ | L + (Ag) ↔ ζ | 702.5 | 41 |
| | p ₃ | L + ζ ↔ ε | 558 | |
| | e ₁ | L ↔ ε + (Sb) | 485 | |
| Ag-Sn | p ₁ | L + (Ag) ↔ ζ | 724 | 41 |
| | p ₄ | L + ζ ↔ ε | 480 | |
| | e ₃ | L ↔ ε + (Sn) | 221 | |
| Sb-Sn | p ₅ | L + (Sb) ↔ β | 421 | 50 |
| | p ₆ | L + β ↔ Sn ₃ Sb ₂ | 321 | |
| | p ₇ | L + Sn ₃ Sb ₂ ↔ (Sn) | 244 | |
| | e ₂ | Sn ₃ Sb ₂ ↔ β + (Sn) | 243 | |

and Sb (Newmet koch, 99.999%). Ag pieces were cleaned with diluted HCl and then heated in a quartz tube under vacuum at 700°C for 30 min to remove impurities from the surface; the surfaces of Sn pieces were mechanically cleaned.

The experiments were performed using a high-temperature Calvet-type calorimeter whose details have been described elsewhere.⁵³ In addition to the previous setup, the Calvet calorimeter was equipped with an automatic sample introducer, which is located in a gas-tight cylinder block and consists of a stepper motor which turns around two discs carrying 15 small crucibles each. Up to 30 samples can therefore be added to the bath in the course of one measurement. The stepper motor was controlled by homemade software (CALMAA) developed in the LabView[®] environment, which was also used for signal acquisition. The furnace was controlled by an automatic device in order to maintain the temperature of the apparatus constant in a range of ±0.5 K. The error range of the integral mixing enthalpies measured in this work was estimated as ±150 J mol⁻¹ (see the “[Experimental Results and Discussion](#)” section).

The liquid bath of binary alloy (Ag-Sn or Sb-Sn) was prepared by placing weighed pure metals in a graphite crucible which had been inserted into the calorimetric cell maintained at the selected

working temperature; the equilibrium state and a stable baseline were obtained after 6 h. Pieces of the pure metal (Ag or Sb) were dropped into the bath from room temperature. After each series, five pieces of NIST (National Institute of Standards and Technology, Gaithersburg, MD) standard Al₂O₃ were dropped in order to perform calibration. The solvent bath contained around 1.5 g of material, and an interval of 70 min was employed for each drop to ensure complete dissolution. At the beginning of every measurement, the reaction cell as well as the automatic dropping unit were repeatedly flushed with high-purity Ar, and an Ar flow (around 2 L/h) was applied throughout the entire measurement.

The calorimetric experiments were performed along five composition sections of the Ag-Sb-Sn system with a total number of 18 measurements. The starting compositions of the liquid bath were Ag_{0.25}Sn_{0.75}, Ag_{0.50}Sn_{0.50}, Sb_{0.30}Sn_{0.70}, Sb_{0.50}Sn_{0.50}, and Sb_{0.70}Sn_{0.30}, and the third element was added as the dropped element. The five sections are indicated as sections A–E below. The experiments were performed at three different temperatures: 530°C, 600°C, and 630°C.

The total mass of the samples together with that of the crucibles was checked before and after the measurements; weight loss was found to be negligible.

Table III. Partial and integral enthalpies of mixing of liquid Ag-Sb-Sn alloys at 530°C (reference state: pure liquid components)

| m_i (g) | x_{Sn} | x_i | Q_i (J) | Q_{mi} (J/mol) | $\Delta_{\text{mix}}H_m$ (J/mol) | $\Delta_{\text{mix}}\bar{H}$ | |
|---|-----------------|--------|-----------|------------------|----------------------------------|------------------------------|---------|
| | | | | | | x_i | (J/mol) |
| Section B (Sb _{0.50} Sn _{0.50}) first run, $i = \text{Ag}$, starting amount: $n_{\text{Sn}} = 6.2076$ mmol, $n_{\text{Sb}} = 6.2062$ mmol | | | | | | | |
| 0.0000 | 0.5000 | 0.0000 | – | – | –1423.78 | 0.0000 | – |
| 0.0173 | 0.4936 | 0.0128 | 5.45 | 34,003 | –1284 | 0.0064 | 9557 |
| 0.0178 | 0.4872 | 0.0255 | 5.30 | 32,093 | –1168 | 0.0191 | 7647 |
| 0.0193 | 0.4804 | 0.0390 | 5.66 | 31,638 | –1052 | 0.0323 | 7192 |
| 0.0194 | 0.4738 | 0.0522 | 5.60 | 31,160 | –946 | 0.0456 | 6714 |
| 0.0196 | 0.4673 | 0.0652 | 5.53 | 30,458 | –850 | 0.0587 | 6012 |
| 0.0223 | 0.4602 | 0.0795 | 6.58 | 31,847 | –724 | 0.0724 | 7401 |
| 0.0258 | 0.4522 | 0.0956 | 7.21 | 30,136 | –612 | 0.0876 | 5690 |
| 0.0261 | 0.4443 | 0.1112 | 7.36 | 30,404 | –498 | 0.1034 | 5958 |
| 0.0265 | 0.4366 | 0.1266 | 6.54 | 26,627 | –452 | 0.1189 | 2181 |
| 0.0272 | 0.4290 | 0.1418 | 7.21 | 28,574 | –372 | 0.1342 | 4128 |
| 0.0273 | 0.4217 | 0.1566 | 7.14 | 28,196 | –301 | 0.1492 | 3750 |
| 0.0300 | 0.4138 | 0.1722 | 7.71 | 27,736 | –235 | 0.1644 | 3291 |
| 0.0319 | 0.4058 | 0.1882 | 8.22 | 27,805 | –165 | 0.1802 | 3359 |
| 0.0323 | 0.3980 | 0.2038 | 8.16 | 27,263 | –108 | 0.1960 | 2818 |
| 0.0368 | 0.3895 | 0.2209 | 8.93 | 26,170 | –69 | 0.2123 | 1724 |
| 0.0391 | 0.3809 | 0.2382 | 9.04 | 24,953 | –56 | 0.2295 | 507 |
| 0.0397 | 0.3724 | 0.2550 | 9.16 | 24,878 | –45 | 0.2466 | 433 |
| 0.0399 | 0.3644 | 0.2712 | 9.04 | 24,447 | –44 | 0.2631 | 1 |
| 0.0402 | 0.3566 | 0.2868 | 9.14 | 24,517 | –42 | 0.2790 | 72 |
| 0.0407 | 0.3490 | 0.3019 | 9.24 | 24,489 | –40 | 0.2944 | 43 |
| 0.0416 | 0.3416 | 0.3168 | 9.16 | 23,746 | –54 | 0.3094 | –699 |
| 0.0427 | 0.3343 | 0.3313 | 9.33 | 23,566 | –71 | 0.3240 | –879 |
| 0.0441 | 0.3271 | 0.3457 | 9.24 | 22,608 | –109 | 0.3385 | –1838 |
| 0.0441 | 0.3202 | 0.3595 | 9.11 | 22,286 | –153 | 0.3526 | –2160 |
| Section B (Sb _{0.50} Sn _{0.50}) second run, $i = \text{Ag}$, starting amount: $n_{\text{Sn}} = 6.195$ mmol, $n_{\text{Sb}} = 6.196$ mmol | | | | | | | |
| 0.0000 | 0.5000 | 0.0000 | – | – | –1423.78 | – | – |
| 0.0355 | 0.4871 | 0.0259 | 10.82 | 32,889 | –1170 | 0.0129 | 8388 |
| 0.0448 | 0.4717 | 0.0567 | 13.18 | 31,741 | –904 | 0.0413 | 7240 |
| 0.0466 | 0.4567 | 0.0867 | 13.40 | 31,017 | –668 | 0.0717 | 6516 |
| 0.0540 | 0.4404 | 0.1192 | 14.84 | 29,649 | –461 | 0.1030 | 5148 |
| 0.0545 | 0.4251 | 0.1497 | 14.43 | 28,555 | –304 | 0.1345 | 4054 |
| 0.0561 | 0.4105 | 0.1790 | 14.02 | 26,949 | –209 | 0.1644 | 2448 |
| 0.0574 | 0.3965 | 0.2070 | 13.91 | 26,133 | –147 | 0.1930 | 1632 |
| 0.0578 | 0.3834 | 0.2333 | 14.10 | 26,321 | –82 | 0.2201 | 1820 |
| 0.0584 | 0.3709 | 0.2581 | 13.56 | 25,051 | –61 | 0.2457 | 550 |
| 0.0587 | 0.3592 | 0.2815 | 13.84 | 25,436 | –30 | 0.2698 | 935 |
| 0.0593 | 0.3481 | 0.3037 | 13.10 | 23,824 | –50 | 0.2926 | –677 |
| 0.0596 | 0.3377 | 0.3247 | 13.02 | 23,556 | –77 | 0.3142 | –945 |
| 0.0604 | 0.3277 | 0.3447 | 13.00 | 23,224 | –112 | 0.3347 | –1277 |
| 0.0605 | 0.3182 | 0.3636 | 12.91 | 23,009 | –152 | 0.3541 | –1492 |
| 0.0607 | 0.3093 | 0.3815 | 12.75 | 22,665 | –199 | 0.3725 | –1836 |
| 0.0614 | 0.3007 | 0.3985 | 11.81 | 20,747 | –297 | 0.3900 | –3754 |
| 0.0627 | 0.2925 | 0.4151 | 12.56 | 21,605 | –369 | 0.4068 | –2896 |
| 0.0628 | 0.2847 | 0.4307 | 11.55 | 19,831 | –484 | 0.4229 | –4670 |
| 0.0628 | 0.2772 | 0.4455 | 11.71 | 20,115 | –585 | 0.4381 | –4386 |
| 0.0630 | 0.2702 | 0.4597 | 12.48 | 21,369 | –650 | 0.4526 | –3132 |
| 0.0637 | 0.2634 | 0.4732 | 11.83 | 20,025 | –746 | 0.4664 | –4476 |
| 0.0656 | 0.2568 | 0.4865 | 12.64 | 20,791 | –821 | 0.4799 | –3710 |
| 0.0656 | 0.2504 | 0.4991 | 12.05 | 19,820 | –916 | 0.4928 | –4681 |
| 0.0656 | 0.2444 | 0.5111 | 11.65 | 19,161 | –1022 | 0.5051 | –5341 |
| 0.0680 | 0.2385 | 0.5230 | 12.35 | 19,589 | –1117 | 0.5171 | –4912 |
| Section B (Sb _{0.5} Sn _{0.5}) third run, $i = \text{Ag}$, starting amount: $n_{\text{Sn}} = 6.244$ mmol, $n_{\text{Sb}} = 6.244$ mmol | | | | | | | |
| 0.0000 | 0.5000 | 0.0000 | – | – | –1423.78 | – | – |
| 0.0402 | 0.4855 | 0.0290 | 12.11 | 32,499 | –1150 | 0.0145 | 8024 |
| 0.0422 | 0.4712 | 0.0576 | 12.46 | 31,854 | –898 | 0.0433 | 7380 |
| 0.0423 | 0.4576 | 0.0847 | 11.95 | 30,467 | –700 | 0.0712 | 5992 |

Table III. Continued

| m_i (g) | x_{Sn} | x_i | Q_i (J) | Q_{mi} (J/mol) | $\Delta_{\text{mix}}H_m$ (J/mol) | $\Delta_{\text{mix}}\bar{H}$ | |
|---|-----------------|--------|-----------|------------------|----------------------------------|------------------------------|---------|
| | | | | | | x_i | (J/mol) |
| 0.0426 | 0.4448 | 0.1105 | 11.56 | 29,265 | -546 | 0.0976 | 4790 |
| 0.0428 | 0.4325 | 0.1349 | 11.63 | 29,309 | -398 | 0.1227 | 4834 |
| 0.0429 | 0.4209 | 0.1581 | 12.09 | 30,397 | -228 | 0.1465 | 5922 |
| 0.0444 | 0.4096 | 0.1809 | 11.22 | 27,258 | -147 | 0.1695 | 2784 |
| 0.0450 | 0.3987 | 0.2027 | 10.93 | 26,205 | -97 | 0.1918 | 1731 |
| 0.0453 | 0.3882 | 0.2235 | 10.70 | 25,489 | -68 | 0.2131 | 1014 |
| 0.0454 | 0.3783 | 0.2433 | 10.60 | 25,195 | -48 | 0.2334 | 720 |
| 0.0491 | 0.3682 | 0.2636 | 11.32 | 24,860 | -36 | 0.2535 | 385 |
| 0.0520 | 0.3580 | 0.2840 | 11.41 | 23,674 | -57 | 0.2738 | -801 |
| 0.0522 | 0.3483 | 0.3033 | 11.80 | 24,380 | -58 | 0.2936 | -95 |
| 0.0525 | 0.3391 | 0.3217 | 11.52 | 23,676 | -78 | 0.3125 | -798 |
| 0.0527 | 0.3304 | 0.3392 | 11.42 | 23,377 | -104 | 0.3305 | -1098 |
| 0.0531 | 0.3220 | 0.3560 | 11.12 | 22,594 | -149 | 0.3476 | -1881 |
| 0.0574 | 0.3134 | 0.3732 | 12.13 | 22,803 | -190 | 0.3646 | -1671 |
| 0.0577 | 0.3052 | 0.3896 | 11.38 | 21,268 | -269 | 0.3814 | -3207 |
| 0.0577 | 0.2974 | 0.4052 | 11.45 | 21,397 | -341 | 0.3974 | -3078 |
| 0.0581 | 0.2900 | 0.4200 | 11.22 | 20,838 | -423 | 0.4126 | -3637 |
| 0.0593 | 0.2828 | 0.4345 | 11.56 | 21,033 | -498 | 0.4273 | -3442 |
| 0.0624 | 0.2755 | 0.4489 | 11.87 | 20,524 | -586 | 0.4417 | -3950 |
| 0.0654 | 0.2684 | 0.4633 | 11.87 | 19,582 | -698 | 0.4561 | -4892 |
| 0.0668 | 0.2614 | 0.4772 | 12.12 | 19,568 | -808 | 0.4702 | -4907 |
| 0.0690 | 0.2546 | 0.4908 | 12.72 | 19,889 | -906 | 0.4840 | -4586 |
| Section C ($\text{Sb}_{0.30}\text{Sn}_{0.70}$), $i = \text{Ag}$, starting amount: $n_{\text{Sn}} = 8.875$ mmol, $n_{\text{Sb}} = 3.803$ mmol | | | | | | | |
| 0.0000 | 0.7000 | 0.0000 | - | - | -1199.86 | - | - |
| 0.0399 | 0.6802 | 0.0284 | 11.31 | 30,584 | -992 | 0.0142 | 6138 |
| 0.0406 | 0.6611 | 0.0556 | 11.67 | 31,002 | -780 | 0.0420 | 6555 |
| 0.0426 | 0.6422 | 0.0826 | 11.77 | 29,813 | -605 | 0.0691 | 5367 |
| 0.0439 | 0.6238 | 0.1088 | 11.68 | 28,706 | -465 | 0.0957 | 4260 |
| 0.0445 | 0.6063 | 0.1339 | 11.63 | 28,203 | -346 | 0.1214 | 3756 |
| 0.0472 | 0.5887 | 0.1591 | 12.17 | 27,822 | -238 | 0.1465 | 3375 |
| 0.0482 | 0.5717 | 0.1833 | 12.25 | 27,422 | -146 | 0.1712 | 2976 |
| 0.0503 | 0.5550 | 0.2071 | 12.39 | 26,574 | -80 | 0.1952 | 2127 |
| 0.0506 | 0.5392 | 0.2297 | 12.21 | 26,040 | -32 | 0.2184 | 1593 |
| 0.0540 | 0.5233 | 0.2524 | 12.45 | 24,865 | -19 | 0.2411 | 418 |
| 0.0551 | 0.5080 | 0.2743 | 12.39 | 24,254 | -24 | 0.2634 | -192 |
| 0.0554 | 0.4935 | 0.2950 | 11.98 | 23,335 | -55 | 0.2847 | -1112 |
| 0.0557 | 0.4797 | 0.3147 | 12.34 | 23,902 | -68 | 0.3049 | -544 |
| 0.0573 | 0.4663 | 0.3338 | 11.92 | 22,446 | -122 | 0.3243 | -2000 |
| 0.0581 | 0.4535 | 0.3522 | 12.12 | 22,507 | -172 | 0.3430 | -1939 |
| 0.0590 | 0.4412 | 0.3698 | 11.98 | 21,909 | -237 | 0.3610 | -2537 |
| 0.0590 | 0.4295 | 0.3865 | 11.83 | 21,636 | -305 | 0.3781 | -2811 |
| 0.0613 | 0.4180 | 0.4029 | 11.85 | 20,846 | -393 | 0.3947 | -3601 |
| 0.0616 | 0.4070 | 0.4185 | 11.95 | 20,929 | -475 | 0.4107 | -3517 |
| 0.0638 | 0.3963 | 0.4339 | 11.72 | 19,822 | -584 | 0.4262 | -4625 |
| 0.0639 | 0.3861 | 0.4485 | 11.64 | 19,652 | -693 | 0.4412 | -4794 |
| 0.0658 | 0.3761 | 0.4627 | 12.26 | 20,096 | -787 | 0.4556 | -4350 |
| 0.0659 | 0.3666 | 0.4763 | 11.81 | 19,331 | -897 | 0.4695 | -5116 |
| 0.0663 | 0.3575 | 0.4893 | 11.48 | 18,680 | -1017 | 0.4828 | -5767 |
| 0.0667 | 0.3488 | 0.5017 | 11.95 | 19,318 | -1117 | 0.4955 | -5128 |
| Section D ($\text{Ag}_{0.50}\text{Sn}_{0.50}$), $i = \text{Sb}$, starting amount: $n_{\text{Ag}} = 6.5719$ mmol, $n_{\text{Sn}} = 6.5723$ mmol | | | | | | | |
| 0.0000 | 0.5000 | 0.0000 | - | - | -870.77 | - | - |
| 0.0448 | 0.4864 | 0.0272 | 14.52 | 38,480 | -707 | 0.0140 | 4999 |
| 0.0478 | 0.4727 | 0.0547 | 14.93 | 37,088 | -582 | 0.0420 | 3607 |
| 0.0485 | 0.4595 | 0.0810 | 15.74 | 38,535 | -422 | 0.0695 | 5054 |
| 0.0522 | 0.4461 | 0.1078 | 15.97 | 36,326 | -324 | 0.0966 | 2844 |
| 0.0522 | 0.4335 | 0.1330 | 16.71 | 37,996 | -184 | 0.1231 | 4515 |
| 0.0525 | 0.4215 | 0.1570 | 16.26 | 36,766 | -86 | 0.1482 | 3285 |
| 0.0542 | 0.4098 | 0.1804 | 15.62 | 34,217 | -63 | 0.1723 | 735 |
| 0.0554 | 0.3985 | 0.2030 | 16.44 | 35,236 | -12 | 0.1956 | 1755 |

Table III. Continued

| m_i (g) | x_{Sn} | x_i | Q_i (J) | Q_{mi} (J/mol) | $\Delta_{\text{mix}}H_m$ (J/mol) | $\Delta_{\text{mix}}\bar{H}$ | |
|---|-----------------|--------|-----------|------------------|----------------------------------|------------------------------|---------|
| | | | | | | x_i | (J/mol) |
| 0.0554 | 0.3878 | 0.2244 | 16.05 | 34,392 | 13 | 0.2180 | 911 |
| 0.0569 | 0.3774 | 0.2452 | 16.50 | 34,426 | 39 | 0.2394 | 944 |
| 0.0570 | 0.3675 | 0.2650 | 15.84 | 32,980 | 24 | 0.2599 | -501 |
| 0.0612 | 0.3575 | 0.2851 | 18.16 | 35,221 | 72 | 0.2801 | 1740 |
| 0.0630 | 0.3477 | 0.3046 | 18.08 | 34,074 | 87 | 0.3001 | 592 |
| 0.0632 | 0.3384 | 0.3232 | 17.34 | 32,568 | 59 | 0.3194 | -913 |
| 0.0638 | 0.3295 | 0.3410 | 18.12 | 33,708 | 64 | 0.3377 | 226 |
| 0.0643 | 0.3210 | 0.3580 | 19.04 | 35,150 | 106 | 0.3553 | 1669 |
| 0.0645 | 0.3129 | 0.3742 | 19.32 | 35,549 | 156 | 0.3720 | 2068 |
| 0.0654 | 0.3051 | 0.3898 | 18.53 | 33,643 | 156 | 0.3880 | 162 |
| 0.0654 | 0.2977 | 0.4046 | 18.68 | 33,904 | 163 | 0.4033 | 423 |
| 0.0656 | 0.2906 | 0.4188 | 18.89 | 34,178 | 176 | 0.4179 | 696 |
| 0.0663 | 0.2838 | 0.4325 | 19.63 | 35,147 | 211 | 0.4319 | 1665 |
| 0.0666 | 0.2772 | 0.4456 | 18.92 | 33,726 | 212 | 0.4453 | 245 |
| 0.0672 | 0.2709 | 0.4582 | 19.93 | 35,212 | 247 | 0.4582 | 1731 |
| 0.0692 | 0.2647 | 0.4706 | 19.71 | 33,817 | 249 | 0.4707 | 336 |
| 0.0700 | 0.2587 | 0.4826 | 20.23 | 34,301 | 262 | 0.4829 | 820 |
| Section E ($\text{Ag}_{0.25}\text{Sn}_{0.75}$), $i = \text{Sb}$, starting amount: $n_{\text{Ag}} = 3.2011$ mmol, $n_{\text{Sn}} = 9.5982$ mmol | | | | | | | |
| 0.0000 | 0.7500 | 0.0000 | - | - | 577.38 | - | - |
| 0.0403 | 0.7310 | 0.0252 | 10.27 | 30,253 | 479.7 | 0.0129 | -3203 |
| 0.0432 | 0.7118 | 0.0509 | 11.35 | 31,193 | 405.79 | 0.0390 | -2263 |
| 0.0440 | 0.6932 | 0.0756 | 11.82 | 31,882 | 352.89 | 0.0648 | -1574 |
| 0.0452 | 0.6751 | 0.0998 | 11.92 | 31,296 | 285.75 | 0.0897 | -2161 |
| 0.0456 | 0.6578 | 0.1229 | 12.59 | 32,765 | 260.11 | 0.1138 | -691 |
| 0.0458 | 0.6412 | 0.1449 | 12.09 | 31,330 | 198.82 | 0.1369 | -2126 |
| 0.0464 | 0.6253 | 0.1661 | 11.54 | 29,530 | 94.23 | 0.1589 | -3926 |
| 0.0481 | 0.6096 | 0.1871 | 12.75 | 31,457 | 40.61 | 0.1803 | -1999 |
| 0.0496 | 0.5942 | 0.2076 | 12.82 | 30,687 | -31.68 | 0.2014 | -2769 |
| 0.0511 | 0.5792 | 0.2276 | 13.30 | 30,903 | -96.81 | 0.2219 | -2554 |
| 0.0546 | 0.5639 | 0.2480 | 14.55 | 31,642 | -142.92 | 0.2424 | -1814 |
| 0.0586 | 0.5484 | 0.2687 | 15.83 | 32,063 | -177.95 | 0.2632 | -1393 |
| 0.0591 | 0.5336 | 0.2884 | 16.73 | 33,602 | -169.06 | 0.2837 | 146 |
| 0.0601 | 0.5194 | 0.3074 | 16.19 | 31,981 | -204.55 | 0.3032 | -1475 |
| 0.0609 | 0.5057 | 0.3257 | 16.68 | 32,507 | -224.5 | 0.3220 | -949 |
| 0.0615 | 0.4926 | 0.3432 | 16.20 | 31,272 | -276.14 | 0.3401 | -2184 |
| 0.0624 | 0.4799 | 0.3600 | 16.54 | 31,464 | -320.82 | 0.3574 | -1992 |
| 0.0643 | 0.4676 | 0.3765 | 17.31 | 31,957 | -351.62 | 0.3741 | -1499 |
| 0.0645 | 0.4558 | 0.3921 | 17.37 | 31,968 | -380.66 | 0.3903 | -1488 |
| 0.0653 | 0.4445 | 0.4072 | 17.61 | 32,017 | -407.35 | 0.4058 | -1439 |
| 0.0664 | 0.4336 | 0.4218 | 18.82 | 33,644 | -392.48 | 0.4207 | 188 |
| 0.0682 | 0.4229 | 0.4361 | 18.55 | 32,297 | -411.67 | 0.4352 | -1159 |
| 0.0657 | 0.4130 | 0.4492 | 17.43 | 31,485 | -448.4 | 0.4489 | -1971 |
| 0.0691 | 0.4032 | 0.4623 | 20.02 | 34,393 | -414.93 | 0.4620 | 937 |
| 0.0696 | 0.3937 | 0.4749 | 18.71 | 31,918 | -441.62 | 0.4749 | -1538 |

Q_i , heat effect from the drop; Q_{mi} , molar heat effect from the drop element; $\Delta_{\text{mix}}H_m$, integral mixing enthalpy of the liquid alloy; $\Delta_{\text{mix}}\bar{H}$, partial mixing enthalpy of the drop element.

Thermodynamic equilibrium of the samples was checked by using scanning electron microscopy (SEM) and chemical analysis by energy-dispersive x-ray spectroscopy (EDS) to verify the complete dissolution of the metallic pieces in the bath. A Lica Digital Microscope and a Zeiss EVO 40 SEM (Carl Zeiss SMT Ltd., Cambridge) operating at 20 kV and equipped with electron probe microanalysis (EPMA, INCA 300) were employed.

Several DSC measurements were performed on key-composition alloys synthesized by induction melting to determine the temperatures of the invariant reactions. DSC measurements were performed using a Setaram DSC 111 using closed quartz crucibles. All samples were heated and cooled in two different cycles from 20°C up to and over the melting temperature with a scanning rate of 1°C/min, followed by a second run at 0.3°C/min.

Table IV. Partial and integral enthalpies of mixing of liquid Ag-Sb-Sn alloys at 600°C (reference state: pure liquid components)

| m_i (g) | x_{Sn} | x_i | Q_i (J) | Q_{mi} (J/mol) | $\Delta_{\text{mix}}H_m$ (J/mol) | $\Delta_{\text{mix}}\bar{H}$ | |
|--|-----------------|--------|-----------|------------------|----------------------------------|------------------------------|----------|
| | | | | | | x_i | (J/mol) |
| Section A ($\text{Sb}_{0.7}\text{Sn}_{0.3}$), $i = \text{Ag}$, starting amount: $n_{\text{Sn}} = 3.6737$ mmol, $n_{\text{Sb}} = 8.5717$ mmol | | | | | | | |
| 0.0000 | 0.3000 | 0.0000 | – | – | –1068.38 | – | – |
| 0.0419 | 0.2908 | 0.0307 | 13.02 | 33,524 | –816 | 0.0154 | 7133 |
| 0.0419 | 0.2821 | 0.0597 | 13.55 | 34,889 | –538 | 0.0452 | 8497 |
| 0.0430 | 0.2737 | 0.0876 | 12.98 | 32,568 | –338 | 0.0736 | 6177 |
| 0.0434 | 0.2658 | 0.1141 | 12.7 | 31,571 | –178 | 0.1009 | 5179 |
| 0.0448 | 0.2580 | 0.1400 | 12.89 | 31,042 | –37 | 0.1271 | 4651 |
| 0.0449 | 0.2507 | 0.1644 | 12.53 | 30,100 | 70 | 0.1522 | 3709 |
| 0.0455 | 0.2437 | 0.1878 | 12.28 | 29,102 | 144 | 0.1761 | 2711 |
| 0.0461 | 0.2370 | 0.2102 | 12.41 | 29,032 | 213 | 0.1990 | 2641 |
| 0.0465 | 0.2305 | 0.2315 | 12.11 | 28,091 | 253 | 0.2209 | 1700 |
| 0.0468 | 0.2244 | 0.2519 | 12.18 | 28,068 | 291 | 0.2417 | 1677 |
| 0.0497 | 0.2183 | 0.2724 | 12.57 | 27,274 | 308 | 0.2622 | 883 |
| 0.0508 | 0.2123 | 0.2922 | 12.37 | 26,275 | 296 | 0.2823 | –116 |
| 0.0534 | 0.2064 | 0.3119 | 12.91 | 26,080 | 279 | 0.3020 | –312 |
| 0.0536 | 0.2008 | 0.3306 | 12.93 | 26,026 | 262 | 0.3212 | –365 |
| 0.0541 | 0.1955 | 0.3484 | 12.12 | 24,160 | 196 | 0.3395 | –2231 |
| 0.0554 | 0.1903 | 0.3658 | 12.44 | 24,215 | 133 | 0.3571 | –2177 |
| 0.0592 | 0.1850 | 0.3833 | 12.98 | 23,644 | 53 | 0.3745 | –2747 |
| 0.0601 | 0.1800 | 0.4001 | 13.17 | 23,639 | –23 | 0.3917 | –2753 |
| 0.0607 | 0.1751 | 0.4162 | 13.02 | 23,132 | –110 | 0.4082 | –3260 |
| 0.0631 | 0.1704 | 0.4321 | 13.4 | 22,915 | –201 | 0.4242 | –3476 |
| 0.0638 | 0.1658 | 0.4472 | 13.37 | 22,609 | –297 | 0.4397 | –3782 |
| 0.0648 | 0.1615 | 0.4618 | 13.51 | 22,483 | –392 | 0.4545 | –3908 |
| 0.0667 | 0.1572 | 0.4761 | 13.77 | 22,277 | –490 | 0.4689 | –4114 |
| 0.0688 | 0.1530 | 0.4900 | 14.03 | 21,992 | –594 | 0.4830 | –4400 |
| 0.0692 | 0.1490 | 0.5033 | 13.74 | 21,423 | –708 | 0.4966 | –4968 |
| Section B ($\text{Sb}_{0.5}\text{Sn}_{0.5}$) first run, $i = \text{Ag}$, starting amount: $n_{\text{Sn}} = 6.2103$ mmol, $n_{\text{Sb}} = 6.2109$ mmol | | | | | | | |
| 0.0000 | 0.5000 | 0.0000 | – | – | –1423.78 | – | – |
| 0.0454 | 0.4836 | 0.0328 | 14.73 | 34,991 | –1093 | 0.0164 | 8610.22 |
| 0.0478 | 0.4675 | 0.0650 | 15 | 33,860 | –805 | 0.0489 | 7479.33 |
| 0.0494 | 0.4519 | 0.0962 | 14.97 | 32,698 | –566 | 0.0806 | 6317.26 |
| 0.0503 | 0.4371 | 0.1259 | 14.62 | 31,343 | –383 | 0.1110 | 4962.3 |
| 0.0504 | 0.4232 | 0.1537 | 14.23 | 30,461 | –240 | 0.1398 | 4080.27 |
| 0.0506 | 0.4101 | 0.1799 | 13.99 | 29,821 | –124 | 0.1668 | 3440.28 |
| 0.0522 | 0.3974 | 0.2053 | 14.39 | 29,737 | –15 | 0.1926 | 3356.22 |
| 0.0523 | 0.3854 | 0.2292 | 13.38 | 27,589 | 23 | 0.2172 | 1208.25 |
| 0.0526 | 0.3741 | 0.2518 | 14.68 | 30,101 | 133 | 0.2405 | 3720.95 |
| 0.0535 | 0.3633 | 0.2735 | 13.54 | 27,290 | 157 | 0.2627 | 909.54 |
| 0.0550 | 0.3527 | 0.2946 | 13.82 | 27,103 | 174 | 0.2841 | 722.87 |
| 0.0558 | 0.3427 | 0.3147 | 13.27 | 25,644 | 149 | 0.3046 | –736.51 |
| 0.0560 | 0.3331 | 0.3338 | 12.96 | 24,957 | 107 | 0.3242 | –1423.23 |
| 0.0567 | 0.3240 | 0.3521 | 13.04 | 24,802 | 61 | 0.3429 | –1578.7 |
| 0.0573 | 0.3153 | 0.3695 | 13.64 | 25,680 | 42 | 0.3608 | –700.28 |
| 0.0582 | 0.3069 | 0.3863 | 13.24 | 24,537 | –7 | 0.3779 | –1842.95 |
| 0.0586 | 0.2988 | 0.4024 | 12.92 | 23,783 | –74 | 0.3944 | –2597.43 |
| 0.0587 | 0.2912 | 0.4176 | 13.9 | 25,545 | –93 | 0.4100 | –835.61 |
| 0.0597 | 0.2838 | 0.4324 | 13.08 | 23,628 | –159 | 0.4250 | –2752.57 |
| 0.0605 | 0.2767 | 0.4465 | 12.1 | 21,575 | –274 | 0.4394 | –4805.28 |
| 0.0607 | 0.2700 | 0.4601 | 12.95 | 23,005 | –349 | 0.4533 | –3375.72 |
| 0.0627 | 0.2633 | 0.4734 | 12.99 | 22,351 | –439 | 0.4667 | –4029.04 |
| 0.0629 | 0.2570 | 0.4861 | 12.74 | 21,848 | –537 | 0.4797 | –4532.53 |
| 0.0644 | 0.2508 | 0.4985 | 12.81 | 21,454 | –642 | 0.4923 | –4926.6 |
| 0.0656 | 0.2448 | 0.5105 | 13.07 | 21,499 | –743 | 0.5045 | –4881.81 |
| Section B ($\text{Sb}_{0.5}\text{Sn}_{0.5}$) second run, $i = \text{Ag}$, starting amount: $n_{\text{Sn}} = 6.1798$ mmol, $n_{\text{Sb}} = 6.1823$ mmol | | | | | | | |
| 0.0000 | 0.5000 | 0.0000 | – | – | –1423.78 | – | – |
| 0.0406 | 0.4851 | 0.0295 | 12.75 | 33,883 | –1162 | 0.0148 | 7429 |
| 0.0427 | 0.4705 | 0.0588 | 13.09 | 33,074 | –928 | 0.0442 | 6620 |

Table IV. Continued

| m_i (g) | x_{Sn} | x_i | Q_i (J) | Q_{mi} (J/mol) | $\Delta_{\text{mix}}H_m$ (J/mol) | $\Delta_{\text{mix}}\bar{H}$ | |
|---|-----------------|--------|-----------|------------------|----------------------------------|------------------------------|---------|
| | | | | | | x_i | (J/mol) |
| 0.0441 | 0.4563 | 0.0872 | 12.85 | 31,443 | -749 | 0.0730 | 4988 |
| 0.0442 | 0.4429 | 0.1140 | 12.63 | 30,824 | -599 | 0.1006 | 4369 |
| 0.0444 | 0.4302 | 0.1394 | 12.36 | 30,021 | -479 | 0.1267 | 3566 |
| 0.0448 | 0.4181 | 0.1636 | 12.27 | 29,554 | -379 | 0.1515 | 3099 |
| 0.0476 | 0.4060 | 0.1878 | 12.37 | 28,034 | -322 | 0.1757 | 1579 |
| 0.0489 | 0.3943 | 0.2113 | 13.05 | 28,792 | -245 | 0.1996 | 2337 |
| 0.0500 | 0.3829 | 0.2340 | 13.32 | 28,736 | -173 | 0.2226 | 2281 |
| 0.0515 | 0.3719 | 0.2560 | 13.57 | 28,429 | -111 | 0.2450 | 1974 |
| 0.0519 | 0.3615 | 0.2769 | 13.42 | 27,899 | -67 | 0.2665 | 1444 |
| 0.0535 | 0.3513 | 0.2973 | 13 | 26,213 | -72 | 0.2871 | -241 |
| 0.0536 | 0.3416 | 0.3166 | 12.83 | 25,820 | -88 | 0.3070 | -635 |
| 0.0538 | 0.3325 | 0.3350 | 12.63 | 25,318 | -116 | 0.3258 | -1137 |
| 0.0563 | 0.3234 | 0.3531 | 13.33 | 25,535 | -138 | 0.3440 | -919 |
| 0.0564 | 0.3148 | 0.3703 | 12.55 | 23,994 | -200 | 0.3617 | -2461 |
| 0.0567 | 0.3066 | 0.3868 | 12.65 | 24,060 | -257 | 0.3786 | -2395 |
| 0.0567 | 0.2988 | 0.4023 | 12.62 | 24,004 | -313 | 0.3946 | -2451 |
| 0.0571 | 0.2913 | 0.4173 | 12.52 | 23,660 | -374 | 0.4098 | -2794 |
| 0.0599 | 0.2839 | 0.4321 | 12.81 | 23,067 | -451 | 0.4247 | -3388 |
| 0.0616 | 0.2766 | 0.4466 | 12.78 | 22,378 | -544 | 0.4394 | -4077 |
| 0.0625 | 0.2696 | 0.4606 | 13.3 | 22,957 | -619 | 0.4536 | -3498 |
| 0.0625 | 0.2630 | 0.4739 | 12.96 | 22,367 | -704 | 0.4673 | -4088 |
| 0.0630 | 0.2566 | 0.4867 | 12.87 | 22,043 | -794 | 0.4803 | -4412 |
| 0.0699 | 0.2499 | 0.5001 | 14.13 | 21,801 | -895 | 0.4934 | -4654 |
| Section C ($\text{Sb}_{0.3}\text{Sn}_{0.7}$), $i = \text{Ag}$, starting amount: $n_{\text{Sn}} = 8.6522$ mmol, $n_{\text{Sb}} = 3.7076$ mmol | | | | | | | |
| 0.0000 | 0.7000 | 0.0000 | - | - | -1199.86 | - | - |
| 0.0419 | 0.6787 | 0.0305 | 12.88 | 33,152 | -957 | 0.0152 | 6780 |
| 0.0438 | 0.6577 | 0.0604 | 13.11 | 32,291 | -744 | 0.0454 | 5920 |
| 0.0441 | 0.6379 | 0.0887 | 12.12 | 29,639 | -624 | 0.0746 | 3267 |
| 0.0446 | 0.6190 | 0.1157 | 12.26 | 29,658 | -508 | 0.1022 | 3286 |
| 0.0449 | 0.6011 | 0.1413 | 12.32 | 29,597 | -400 | 0.1285 | 3226 |
| 0.0450 | 0.5842 | 0.1654 | 12.63 | 30,272 | -279 | 0.1533 | 3900 |
| 0.0454 | 0.5681 | 0.1885 | 11.91 | 28,301 | -218 | 0.1770 | 1929 |
| 0.0464 | 0.5525 | 0.2108 | 12.23 | 28,435 | -155 | 0.1996 | 2063 |
| 0.0481 | 0.5372 | 0.2326 | 12.76 | 28,615 | -89 | 0.2217 | 2243 |
| 0.0512 | 0.5218 | 0.2546 | 13.14 | 27,692 | -48 | 0.2436 | 1321 |
| 0.0514 | 0.5072 | 0.2754 | 12.2 | 25,599 | -69 | 0.2650 | -773 |
| 0.0519 | 0.4933 | 0.2953 | 12.6 | 26,184 | -72 | 0.2854 | -188 |
| 0.0601 | 0.4781 | 0.3170 | 13.74 | 24,656 | -123 | 0.3062 | -1716 |
| 0.0601 | 0.4638 | 0.3374 | 14.2 | 25,490 | -145 | 0.3272 | -882 |
| 0.0604 | 0.4503 | 0.3567 | 13.59 | 24,270 | -202 | 0.3471 | -2102 |
| 0.0615 | 0.4373 | 0.3753 | 13.83 | 24,251 | -258 | 0.3660 | -2121 |
| 0.0615 | 0.4251 | 0.3928 | 12.06 | 21,147 | -397 | 0.3840 | -5225 |
| 0.0618 | 0.4135 | 0.4094 | 13.6 | 23,737 | -458 | 0.4011 | -2635 |
| 0.0629 | 0.4022 | 0.4254 | 13.1 | 22,472 | -551 | 0.4174 | -3899 |
| 0.0649 | 0.3913 | 0.4410 | 13.47 | 22,391 | -645 | 0.4332 | -3981 |
| 0.0651 | 0.3809 | 0.4559 | 13.84 | 22,930 | -719 | 0.4485 | -3441 |
| 0.0658 | 0.3709 | 0.4701 | 13.41 | 21,991 | -815 | 0.4630 | -4381 |
| 0.0668 | 0.3613 | 0.4838 | 13.18 | 21,289 | -925 | 0.4770 | -5083 |
| 0.0680 | 0.3521 | 0.4971 | 13.24 | 20,998 | -1039 | 0.4904 | -5374 |
| 0.0694 | 0.3431 | 0.5099 | 13.3 | 20,667 | -1158 | 0.5035 | -5705 |
| Section D ($\text{Ag}_{0.5}\text{Sn}_{0.5}$), $i = \text{Sb}$, starting amount: $n_{\text{Ag}} = 6.6702$ mmol, $n_{\text{Sn}} = 6.6709$ mmol | | | | | | | |
| 0.0000 | 0.5000 | 0.0000 | - | - | -877.42 | - | - |
| 0.0405 | 0.4879 | 0.0243 | 13.75 | 41,333 | -714 | 0.0122 | 5827 |
| 0.0436 | 0.4754 | 0.0492 | 13.92 | 38,881 | -610 | 0.0368 | 3375 |
| 0.0441 | 0.4634 | 0.0732 | 14.09 | 38,907 | -509 | 0.0612 | 3401 |
| 0.0449 | 0.4519 | 0.0963 | 14.06 | 38,123 | -431 | 0.0847 | 2617 |
| 0.0449 | 0.4409 | 0.1183 | 14.21 | 38,540 | -346 | 0.1073 | 3034 |
| 0.0451 | 0.4303 | 0.1394 | 13.97 | 37,707 | -286 | 0.1289 | 2202 |
| 0.0476 | 0.4197 | 0.1606 | 14.22 | 36,362 | -257 | 0.1500 | 856 |

Table IV. Continued

| m_i (g) | x_{Sn} | x_i | Q_i (J) | Q_{mi} (J/mol) | $\Delta_{\text{mix}}H_m$ (J/mol) | $\Delta_{\text{mix}}\bar{H}$ | |
|---|-----------------|--------|-----------|------------------|----------------------------------|------------------------------|---------|
| | | | | | | x_i | (J/mol) |
| 0.0487 | 0.4094 | 0.1812 | 15.24 | 38,112 | -187 | 0.1709 | 2606 |
| 0.0488 | 0.3996 | 0.2008 | 14.75 | 36,801 | -152 | 0.1910 | 1295 |
| 0.0491 | 0.3902 | 0.2197 | 14.33 | 35,545 | -147 | 0.2103 | 40 |
| 0.0492 | 0.3812 | 0.2377 | 15.36 | 38,011 | -86 | 0.2287 | 2506 |
| 0.0534 | 0.3718 | 0.2563 | 15.93 | 36,321 | -64 | 0.2470 | 816 |
| 0.0543 | 0.3628 | 0.2744 | 15.56 | 34,888 | -77 | 0.2654 | -618 |
| 0.0555 | 0.3540 | 0.2919 | 17.51 | 38,404 | -5 | 0.2832 | 2898 |
| 0.0573 | 0.3454 | 0.3092 | 17.6 | 37,390 | 41 | 0.3006 | 1885 |
| 0.0575 | 0.3372 | 0.3257 | 17.2 | 36,409 | 61 | 0.3174 | 904 |
| 0.0576 | 0.3293 | 0.3414 | 17.65 | 37,309 | 102 | 0.3336 | 1803 |
| 0.0582 | 0.3217 | 0.3566 | 17.87 | 37,389 | 143 | 0.3490 | 1884 |
| 0.0593 | 0.3143 | 0.3714 | 18.13 | 37,231 | 180 | 0.3640 | 1726 |
| 0.0632 | 0.3068 | 0.3864 | 19.16 | 36,905 | 209 | 0.3789 | 1399 |
| 0.0670 | 0.2992 | 0.4015 | 20.78 | 37,764 | 259 | 0.3940 | 2259 |
| 0.0682 | 0.2919 | 0.4162 | 21.11 | 37,690 | 306 | 0.4089 | 2185 |
| 0.0684 | 0.2849 | 0.4302 | 21.09 | 37,534 | 348 | 0.4232 | 2029 |
| 0.0687 | 0.2782 | 0.4436 | 20.79 | 36,836 | 371 | 0.4369 | 1330 |
| 0.0687 | 0.2718 | 0.4564 | 20.77 | 36,813 | 392 | 0.4500 | 1308 |
| Section E (Ag _{0.25} Sn _{0.75}), $i = \text{Sb}$, starting amount: $n_{\text{Ag}} = 3.2382$ mmol, $n_{\text{Sn}} = 9.0943$ mmol | | | | | | | |
| 0.0000 | 0.7500 | 0.0000 | - | - | 528.78 | - | - |
| 0.0352 | 0.7336 | 0.0218 | 10.12 | 34,145 | 484 | 0.0112 | -1488 |
| 0.0381 | 0.7167 | 0.0444 | 10.85 | 33,793 | 429 | 0.0339 | -1840 |
| 0.0409 | 0.6994 | 0.0675 | 11.47 | 33,305 | 360 | 0.0573 | -2327 |
| 0.0415 | 0.6826 | 0.0899 | 11.35 | 32,467 | 274 | 0.0805 | -3165 |
| 0.0484 | 0.6641 | 0.1146 | 13.49 | 33,089 | 196 | 0.1046 | -2544 |
| 0.0486 | 0.6464 | 0.1381 | 13.6 | 33,211 | 125 | 0.1292 | -2422 |
| 0.0506 | 0.6290 | 0.1613 | 14.14 | 33,173 | 54 | 0.1530 | -2460 |
| 0.0521 | 0.6121 | 0.1839 | 14.73 | 33,566 | -5 | 0.1762 | -2067 |
| 0.0547 | 0.5952 | 0.2064 | 15.28 | 33,168 | -74 | 0.1991 | -2464 |
| 0.0549 | 0.5792 | 0.2277 | 15.48 | 33,479 | -131 | 0.2214 | -2153 |
| 0.0554 | 0.5639 | 0.2481 | 15.87 | 34,016 | -171 | 0.2425 | -1617 |
| 0.0570 | 0.5490 | 0.2680 | 16.13 | 33,585 | -221 | 0.2629 | -2048 |
| 0.0596 | 0.5342 | 0.2877 | 16.25 | 32,374 | -305 | 0.2830 | -3259 |
| 0.0626 | 0.5195 | 0.3073 | 18.05 | 34,235 | -335 | 0.3028 | -1397 |
| 0.0634 | 0.5054 | 0.3261 | 18.51 | 34,659 | -353 | 0.3222 | -973 |
| 0.0635 | 0.4921 | 0.3439 | 18.46 | 34,516 | -373 | 0.3406 | -1117 |
| 0.0636 | 0.4794 | 0.3608 | 18.63 | 34,779 | -386 | 0.3581 | -853 |
| 0.0642 | 0.4672 | 0.3770 | 18.38 | 33,990 | -418 | 0.3748 | -1642 |
| 0.0676 | 0.4551 | 0.3932 | 19.62 | 34,457 | -438 | 0.3911 | -1176 |
| 0.0685 | 0.4434 | 0.4088 | 19.96 | 34,593 | -454 | 0.4071 | -1040 |
| 0.0693 | 0.4322 | 0.4238 | 20.1 | 34,427 | -473 | 0.4224 | -1206 |
| 0.0698 | 0.4214 | 0.4381 | 20.56 | 34,963 | -478 | 0.4371 | -670 |
| 0.0722 | 0.4109 | 0.4522 | 20.79 | 34,181 | -503 | 0.4514 | -1452 |
| 0.0739 | 0.4006 | 0.4659 | 20.31 | 32,626 | -566 | 0.4653 | -3006 |

Q_i , heat effect from the drop; Q_{mi} , molar heat effect from the drop element; $\Delta_{\text{mix}}H_m$, integral mixing enthalpy of the liquid alloy; $\Delta_{\text{mix}}\bar{H}$, partial mixing enthalpy of the drop element.

After DSC measurement, microstructural analysis was carried out using light optical microscopy (LOM), SEM, and chemical analysis performed using EDS.

Mixing Enthalpy Determination

During each drop (i th) of element A in the liquid bath, a certain amount of heat Q_i is exchanged in the measuring cell:

$$Q_i = Q_{i1} + Q_{i2} = n_i \Delta H_1 + \Delta_{\text{mix}} H_i,$$

where n_i refers to the mole number of the i th drop and ΔH_1 is given by $H(A, T_c, l) - H(A, T_r, s)$, corresponding to the enthalpy change of 1 mole of A from the solid state at the drop temperature T_r to the liquid state at the calorimetric temperature T_c , expressed in Kelvin. The enthalpies of these two states were calculated by applying polynomials from

Table V. Partial and integral enthalpies of mixing of liquid Ag-Sb-Sn alloys at 630°C (reference state: pure liquid components)

| m_i (g) | x_{Sn} | x_i | Q_i (J) | Q_{mi} (J/mol) | $\Delta_{\text{mix}}H_m$ (J/mol) | $\Delta_{\text{mix}}\bar{H}$ | |
|--|-----------------|--------|-----------|------------------|----------------------------------|------------------------------|---------|
| | | | | | | x_i | (J/mol) |
| Section A (Sb _{0.7} Sn _{0.3}) first run, $i = \text{Ag}$, starting amount: $n_{\text{Sn}} = 3.7882$ mmol, $n_{\text{Sb}} = 8.8517$ mmol | | | | | | | |
| 0.0000 | 0.3000 | 0.0000 | – | – | –1068.38 | – | – |
| 0.0358 | 0.2920 | 0.0256 | 12.32 | 37,116 | –799 | 0.0128 | 9479 |
| 0.0369 | 0.2845 | 0.0506 | 12.21 | 35,684 | –571 | 0.0381 | 8047 |
| 0.0406 | 0.2767 | 0.0767 | 13.1 | 34,806 | –358 | 0.0637 | 7169 |
| 0.0425 | 0.2690 | 0.1026 | 13.38 | 33,961 | –172 | 0.0896 | 6325 |
| 0.0429 | 0.2616 | 0.1272 | 13.4 | 33,703 | 0 | 0.1149 | 6066 |
| 0.0458 | 0.2541 | 0.1521 | 13.69 | 32,232 | 131 | 0.1396 | 4595 |
| 0.0466 | 0.2470 | 0.1759 | 13.66 | 31,609 | 239 | 0.1640 | 3972 |
| 0.0466 | 0.2402 | 0.1985 | 13.83 | 32,002 | 352 | 0.1872 | 4365 |
| 0.0483 | 0.2336 | 0.2206 | 13.39 | 29,911 | 405 | 0.2096 | 2274 |
| 0.0488 | 0.2272 | 0.2418 | 13.5 | 29,841 | 454 | 0.2312 | 2204 |
| 0.0494 | 0.2212 | 0.2621 | 13.74 | 29,995 | 505 | 0.2519 | 2358 |
| 0.0528 | 0.2150 | 0.2826 | 13.18 | 26,916 | 471 | 0.2723 | –721 |
| 0.0553 | 0.2089 | 0.3029 | 14.56 | 28,404 | 479 | 0.2927 | 767 |
| 0.0572 | 0.2030 | 0.3227 | 14.43 | 27,215 | 453 | 0.3128 | –422 |
| 0.0586 | 0.1973 | 0.3418 | 14.04 | 25,841 | 390 | 0.3322 | –1796 |
| 0.0587 | 0.1918 | 0.3600 | 14.66 | 26,931 | 360 | 0.3509 | –705 |
| 0.0587 | 0.1867 | 0.3771 | 14.03 | 25,790 | 300 | 0.3685 | –1847 |
| 0.0596 | 0.1817 | 0.3936 | 14.63 | 26,478 | 262 | 0.3854 | –1159 |
| 0.0597 | 0.1770 | 0.4093 | 13.54 | 24,466 | 173 | 0.4015 | –3171 |
| 0.0611 | 0.1725 | 0.4245 | 14.24 | 25,143 | 104 | 0.4169 | –2494 |
| 0.0615 | 0.1681 | 0.4391 | 13.79 | 24,188 | 14 | 0.4318 | –3448 |
| 0.0616 | 0.1639 | 0.4530 | 13.31 | 23,307 | –93 | 0.4460 | –4330 |
| 0.0630 | 0.1599 | 0.4665 | 14.2 | 24,316 | –173 | 0.4597 | –3321 |
| 0.0661 | 0.1559 | 0.4799 | 14.48 | 23,622 | –269 | 0.4732 | –4015 |
| 0.0716 | 0.1517 | 0.4937 | 15.59 | 23,484 | –373 | 0.4868 | –4153 |
| Section A (Sb _{0.7} Sn _{0.3}) second run, $i = \text{Ag}$, starting amount: $n_{\text{Sn}} = 3.6568$ mmol, $n_{\text{Sb}} = 8.5322$ mmol | | | | | | | |
| 0.0000 | 0.3000 | 0.0000 | – | – | –1068.38 | – | – |
| 0.0358 | 0.2921 | 0.0265 | 11.9 | 35,853 | –823 | 0.0133 | 8197 |
| 0.0361 | 0.2845 | 0.0518 | 11.97 | 35,768 | –590 | 0.0392 | 8112 |
| 0.0368 | 0.2771 | 0.0764 | 11.82 | 34,659 | –394 | 0.0641 | 7003 |
| 0.0373 | 0.2700 | 0.0999 | 12.09 | 34,968 | –197 | 0.0882 | 7312 |
| 0.0373 | 0.2633 | 0.1224 | 11.4 | 32,964 | –60 | 0.1111 | 5308 |
| 0.0381 | 0.2568 | 0.1441 | 11.59 | 32,824 | 70 | 0.1332 | 5168 |
| 0.0398 | 0.2503 | 0.1657 | 12.15 | 32,936 | 201 | 0.1549 | 5280 |
| 0.0456 | 0.2432 | 0.1892 | 13.89 | 32,851 | 342 | 0.1775 | 5195 |
| 0.0482 | 0.2362 | 0.2126 | 13.92 | 31,156 | 433 | 0.2009 | 3500 |
| 0.0482 | 0.2296 | 0.2347 | 13.63 | 30,504 | 500 | 0.2236 | 2848 |
| 0.0485 | 0.2233 | 0.2557 | 13.47 | 29,966 | 550 | 0.2452 | 2310 |
| 0.0486 | 0.2173 | 0.2756 | 12.73 | 28,247 | 551 | 0.2657 | 591 |
| 0.0498 | 0.2115 | 0.2950 | 12.57 | 27,236 | 525 | 0.2853 | –420 |
| 0.0509 | 0.2059 | 0.3137 | 13.28 | 28,143 | 524 | 0.3043 | 487 |
| 0.0601 | 0.1996 | 0.3346 | 14.86 | 26,677 | 479 | 0.3241 | –979 |
| 0.0611 | 0.1936 | 0.3545 | 15.44 | 27,267 | 453 | 0.3446 | –389 |
| 0.0619 | 0.1879 | 0.3736 | 14.89 | 25,952 | 389 | 0.3641 | –1704 |
| 0.0635 | 0.1824 | 0.3920 | 15.56 | 26,433 | 342 | 0.3828 | –1223 |
| 0.0663 | 0.1770 | 0.4101 | 15.5 | 25,218 | 259 | 0.4010 | –2438 |
| 0.0687 | 0.1717 | 0.4277 | 16.28 | 25,566 | 189 | 0.4189 | –2090 |
| 0.0692 | 0.1667 | 0.4444 | 15.41 | 24,021 | 77 | 0.4361 | –3635 |
| 0.0693 | 0.1619 | 0.4602 | 16.22 | 25,251 | 6 | 0.4523 | –2405 |
| 0.0699 | 0.1574 | 0.4753 | 15.11 | 23,322 | –115 | 0.4678 | –4334 |
| 0.0717 | 0.1530 | 0.4899 | 16.13 | 24,260 | –206 | 0.4826 | –3396 |
| 0.0734 | 0.1488 | 0.5040 | 15.96 | 23,455 | –317 | 0.4970 | –4201 |
| Section B (Sb _{0.5} Sn _{0.5}), $i = \text{Ag}$, starting amount: $n_{\text{Sn}} = 6.2017$ mmol, $n_{\text{Sb}} = 6.2021$ mmol | | | | | | | |
| 0.0000 | 0.5000 | 0.0000 | – | – | –1423.78 | – | – |
| 0.0353 | 0.4871 | 0.0257 | 11.46 | 35,012 | –1194 | 0.0129 | 7497 |
| 0.0373 | 0.4743 | 0.0515 | 11.97 | 34,628 | –975 | 0.0386 | 7112 |

Table V. Continued

| m_i (g) | x_{Sn} | x_i | Q_i (J) | Q_{mi} (J/mol) | $\Delta_{\text{mix}}H_m$ (J/mol) | $\Delta_{\text{mix}}\bar{H}$ | |
|---|-----------------|--------|-----------|------------------|----------------------------------|------------------------------|---------|
| | | | | | | x_i | (J/mol) |
| 0.0379 | 0.4618 | 0.0763 | 12.02 | 34,214 | -774 | 0.0639 | 6698 |
| 0.0407 | 0.4492 | 0.1015 | 12.4 | 32,873 | -606 | 0.0889 | 5358 |
| 0.0422 | 0.4368 | 0.1263 | 12.5 | 31,942 | -468 | 0.1139 | 4427 |
| 0.0423 | 0.4251 | 0.1498 | 12.56 | 32,017 | -334 | 0.1380 | 4502 |
| 0.0423 | 0.4140 | 0.1720 | 12.24 | 31,224 | -228 | 0.1609 | 3708 |
| 0.0435 | 0.4031 | 0.1937 | 12.54 | 31,106 | -128 | 0.1829 | 3590 |
| 0.0444 | 0.3926 | 0.2147 | 12.52 | 30,428 | -49 | 0.2042 | 2912 |
| 0.0493 | 0.3816 | 0.2368 | 13.65 | 29,867 | 18 | 0.2258 | 2351 |
| 0.0501 | 0.3710 | 0.2580 | 12.88 | 27,728 | 24 | 0.2474 | 212 |
| 0.0511 | 0.3608 | 0.2785 | 13.47 | 28,436 | 49 | 0.2683 | 920 |
| 0.0517 | 0.3510 | 0.2980 | 13.21 | 27,554 | 48 | 0.2883 | 38 |
| 0.0522 | 0.3416 | 0.3168 | 13.15 | 27,174 | 38 | 0.3074 | -341 |
| 0.0546 | 0.3323 | 0.3353 | 13.82 | 27,298 | 31 | 0.3260 | -218 |
| 0.0555 | 0.3234 | 0.3531 | 13.57 | 26,373 | -1 | 0.3442 | -1143 |
| 0.0558 | 0.3149 | 0.3701 | 13.67 | 26,430 | -29 | 0.3616 | -1085 |
| 0.0598 | 0.3063 | 0.3874 | 13.88 | 25,046 | -96 | 0.3787 | -2470 |
| 0.0602 | 0.2981 | 0.4038 | 13.73 | 24,609 | -171 | 0.3956 | -2907 |
| 0.0606 | 0.2903 | 0.4195 | 13.7 | 24,392 | -249 | 0.4116 | -3124 |
| 0.0617 | 0.2827 | 0.4346 | 13.97 | 24,429 | -323 | 0.4270 | -3087 |
| 0.0630 | 0.2754 | 0.4493 | 13.78 | 23,601 | -416 | 0.4419 | -3915 |
| 0.0639 | 0.2683 | 0.4634 | 14.27 | 24,094 | -493 | 0.4563 | -3422 |
| 0.0709 | 0.2609 | 0.4782 | 15.59 | 23,724 | -584 | 0.4708 | -3792 |
| 0.0718 | 0.2538 | 0.4924 | 15.38 | 23,103 | -689 | 0.4853 | -4413 |
| Section C ($\text{Sb}_{0.3}\text{Sn}_{0.7}$), $i = \text{Ag}$, starting amount: $n_{\text{Sn}} = 8.7920$ mmol, $n_{\text{Sb}} = 3.7684$ mmol | | | | | | | |
| 0.0000 | 0.7000 | 0.0000 | - | - | -1199.86 | - | - |
| 0.0382 | 0.6808 | 0.0274 | 11.95 | 33,738 | -998 | 0.0137 | 6153 |
| 0.0387 | 0.6624 | 0.0537 | 11.97 | 33,359 | -815 | 0.0406 | 5774 |
| 0.0410 | 0.6439 | 0.0801 | 12.25 | 32,229 | -663 | 0.0669 | 4644 |
| 0.0431 | 0.6256 | 0.1062 | 12.68 | 31,738 | -526 | 0.0931 | 4153 |
| 0.0436 | 0.6081 | 0.1312 | 12.52 | 30,970 | -417 | 0.1187 | 3385 |
| 0.0440 | 0.5915 | 0.1550 | 12.41 | 30,429 | -327 | 0.1431 | 2844 |
| 0.0454 | 0.5752 | 0.1783 | 12.54 | 29,783 | -258 | 0.1667 | 2198 |
| 0.0464 | 0.5594 | 0.2008 | 12.66 | 29,433 | -200 | 0.1895 | 1848 |
| 0.0486 | 0.5438 | 0.2231 | 12.73 | 28,255 | -176 | 0.2119 | 670 |
| 0.0496 | 0.5288 | 0.2446 | 13 | 28,269 | -152 | 0.2338 | 684 |
| 0.0503 | 0.5144 | 0.2652 | 12.51 | 26,828 | -169 | 0.2549 | -757 |
| 0.0510 | 0.5005 | 0.2849 | 12.79 | 27,044 | -179 | 0.2751 | -541 |
| 0.0556 | 0.4863 | 0.3053 | 13.54 | 26,272 | -211 | 0.2951 | -1313 |
| 0.0583 | 0.4721 | 0.3255 | 14.21 | 26,286 | -243 | 0.3154 | -1299 |
| 0.0613 | 0.4582 | 0.3455 | 14.53 | 25,572 | -295 | 0.3355 | -2012 |
| 0.0620 | 0.4448 | 0.3645 | 14.59 | 25,380 | -351 | 0.3550 | -2205 |
| 0.0623 | 0.4322 | 0.3825 | 14.16 | 24,516 | -428 | 0.3735 | -3069 |
| 0.0625 | 0.4202 | 0.3996 | 14.25 | 24,601 | -499 | 0.3911 | -2983 |
| 0.0646 | 0.4085 | 0.4163 | 14.64 | 24,446 | -572 | 0.4080 | -3139 |
| 0.0648 | 0.3974 | 0.4322 | 14.06 | 23,413 | -670 | 0.4243 | -4172 |
| 0.0665 | 0.3867 | 0.4476 | 14.57 | 23,626 | -759 | 0.4399 | -3959 |
| 0.0686 | 0.3762 | 0.4626 | 14.79 | 23,249 | -856 | 0.4551 | -4336 |
| 0.0713 | 0.3658 | 0.4774 | 15.15 | 22,923 | -961 | 0.4700 | -4661 |
| 0.0728 | 0.3558 | 0.4917 | 15.51 | 22,980 | -1060 | 0.4845 | -4605 |
| Section D ($\text{Ag}_{0.5}\text{Sn}_{0.5}$), $i = \text{Sb}$, starting amount: $n_{\text{Ag}} = 6.4764$ mmol, $n_{\text{Sn}} = 6.4771$ mmol | | | | | | | |
| 0.0000 | 0.5000 | 0.0000 | 0 | - | -879.91 | - | - |
| 0.0402 | 0.4876 | 0.0249 | 13.18 | 39,912 | -771 | 0.0124 | 3501 |
| 0.0409 | 0.4756 | 0.0489 | 13.56 | 40,358 | -655 | 0.0369 | 3947 |
| 0.0427 | 0.4636 | 0.0728 | 14.07 | 40,108 | -545 | 0.0608 | 3697 |
| 0.0430 | 0.4522 | 0.0956 | 13.85 | 39,210 | -463 | 0.0842 | 2799 |
| 0.0434 | 0.4412 | 0.1176 | 13.64 | 38,251 | -407 | 0.1066 | 1840 |
| 0.0452 | 0.4303 | 0.1394 | 14.34 | 38,614 | -343 | 0.1285 | 2203 |
| 0.0474 | 0.4195 | 0.1611 | 15.49 | 39,790 | -249 | 0.1502 | 3379 |
| 0.0475 | 0.4091 | 0.1817 | 15.08 | 38,651 | -187 | 0.1714 | 2240 |

Table V. Continued

| m_i (g) | x_{Sn} | x_i | Q_i (J) | Q_{mi} (J/mol) | $\Delta_{\text{mix}}H_m$ (J/mol) | $\Delta_{\text{mix}}\bar{H}$ | |
|---|-----------------|--------|-----------|------------------|----------------------------------|------------------------------|---------|
| | | | | | | x_i | (J/mol) |
| 0.0477 | 0.3993 | 0.2015 | 14.83 | 37,845 | -148 | 0.1916 | 1434 |
| 0.0497 | 0.3895 | 0.2211 | 15.11 | 37,015 | -130 | 0.2113 | 604 |
| 0.0498 | 0.3801 | 0.2398 | 15.22 | 37,203 | -108 | 0.2305 | 792 |
| 0.0509 | 0.3710 | 0.2580 | 15.85 | 37,918 | -69 | 0.2489 | 1507 |
| 0.0521 | 0.3621 | 0.2758 | 15.96 | 37,293 | -46 | 0.2669 | 883 |
| 0.0528 | 0.3536 | 0.2929 | 16.18 | 37,304 | -24 | 0.2843 | 893 |
| 0.0540 | 0.3452 | 0.3096 | 17.6 | 39,674 | 54 | 0.3013 | 3263 |
| 0.0542 | 0.3372 | 0.3256 | 16.87 | 37,903 | 87 | 0.3176 | 1492 |
| 0.0570 | 0.3292 | 0.3417 | 17.32 | 37,002 | 99 | 0.3336 | 591 |
| 0.0611 | 0.3210 | 0.3580 | 19.13 | 38,113 | 139 | 0.3499 | 1702 |
| 0.0611 | 0.3132 | 0.3736 | 18.98 | 37,813 | 170 | 0.3658 | 1402 |
| 0.0646 | 0.3054 | 0.3893 | 20.29 | 38,248 | 211 | 0.3815 | 1837 |
| 0.0648 | 0.2979 | 0.4042 | 20.42 | 38,369 | 254 | 0.3968 | 1958 |
| 0.0662 | 0.2906 | 0.4188 | 20.53 | 37,749 | 280 | 0.4115 | 1338 |
| 0.0681 | 0.2835 | 0.4330 | 21.01 | 37,564 | 302 | 0.4259 | 1153 |
| 0.0692 | 0.2766 | 0.4468 | 21.51 | 37,848 | 329 | 0.4399 | 1437 |
| 0.0700 | 0.2700 | 0.4600 | 21.47 | 37,344 | 344 | 0.4534 | 933 |
| Section E ($\text{Ag}_{0.25}\text{Sn}_{0.75}$), $i = \text{Sb}$, starting amount: $n_{\text{Ag}} = 3.3226$ mmol, $n_{\text{Sn}} = 9.9680$ mmol | | | | | | | |
| 0.0000 | 0.7500 | 0.0000 | 0 | - | 505.51 | - | - |
| 0.0347 | 0.7343 | 0.0210 | 9.82 | 33,610 | 428 | 0.0108 | -3090 |
| 0.0396 | 0.7171 | 0.0439 | 11.48 | 34,399 | 363 | 0.0332 | -2300 |
| 0.0397 | 0.7006 | 0.0658 | 11.19 | 33,453 | 278 | 0.0562 | -3247 |
| 0.0399 | 0.6849 | 0.0868 | 11.36 | 33,799 | 205 | 0.0781 | -2900 |
| 0.0404 | 0.6696 | 0.1072 | 11.58 | 34,015 | 139 | 0.0993 | -2684 |
| 0.0408 | 0.6549 | 0.1269 | 11.75 | 34,175 | 79 | 0.1197 | -2525 |
| 0.0427 | 0.6401 | 0.1465 | 12.31 | 34,219 | 20 | 0.1397 | -2480 |
| 0.0427 | 0.6260 | 0.1653 | 12.05 | 33,494 | -52 | 0.1593 | -3205 |
| 0.0437 | 0.6122 | 0.1837 | 12.36 | 33,574 | -122 | 0.1782 | -3126 |
| 0.0442 | 0.5989 | 0.2015 | 12.68 | 34,060 | -178 | 0.1966 | -2639 |
| 0.0469 | 0.5853 | 0.2196 | 13.24 | 33,524 | -247 | 0.2148 | -3176 |
| 0.0475 | 0.5722 | 0.2371 | 13.6 | 33,991 | -303 | 0.2328 | -2708 |
| 0.0486 | 0.5594 | 0.2542 | 14.36 | 35,084 | -333 | 0.2503 | -1615 |
| 0.0491 | 0.5470 | 0.2707 | 14.29 | 34,561 | -374 | 0.2673 | -2139 |
| 0.0493 | 0.5351 | 0.2865 | 14.21 | 34,219 | -420 | 0.2837 | -2480 |
| 0.0501 | 0.5235 | 0.3019 | 14.43 | 34,197 | -466 | 0.2995 | -2503 |
| 0.0515 | 0.5122 | 0.3171 | 15.09 | 34,789 | -498 | 0.3150 | -1911 |
| 0.0521 | 0.5012 | 0.3318 | 15.14 | 34,485 | -536 | 0.3300 | -2214 |
| 0.0524 | 0.4905 | 0.3460 | 15.45 | 34,991 | -561 | 0.3446 | -1708 |
| 0.0562 | 0.4796 | 0.3605 | 16.86 | 35,606 | -573 | 0.3590 | -1093 |
| 0.0586 | 0.4688 | 0.3750 | 17.36 | 35,159 | -595 | 0.3736 | -1541 |
| 0.0634 | 0.4576 | 0.3899 | 18.96 | 35,502 | -610 | 0.3884 | -1197 |
| 0.0634 | 0.4469 | 0.4041 | 18.49 | 34,626 | -644 | 0.4031 | -2073 |
| 0.0725 | 0.4353 | 0.4196 | 21.7 | 35,532 | -658 | 0.4180 | -1167 |

Q_i , heat effect from the drop; Q_{mi} , molar heat effect from the drop element; $\Delta_{\text{mix}}H_m$, integral mixing enthalpy of the liquid alloy; $\Delta_{\text{mix}}\bar{H}$, partial mixing enthalpy of the drop element.

Ref. 54. $\Delta_{\text{mix}}H_i$ refers to the contribution of the i th drop to the integral enthalpy of mixing.

All the enthalpies are considered in the standard state, but the superscript “o” is omitted, for clarity, in the text.

After i drops, the total contribution to the mixing enthalpy due to dropping A into the original bath is

$$\sum_{j=1}^i \Delta_{\text{mix}}H_j = \sum_{j=1}^i (Q_j - n_j \Delta H_l).$$

Considering n_0 moles of pure B bath, after i drops of A, we obtain the integral mixing enthalpy

$$\Delta_{\text{mix}}H = \sum_{j=1}^i \Delta_{\text{mix}}H_j.$$

For a measurement performed starting with n_0 moles of the bath formed by a binary liquid alloy, the excess mixing enthalpy of the binary bath $\Delta_{\text{mix}}H_0 = n_0 \Delta_{\text{mix}}H_m$ must be taken into account.

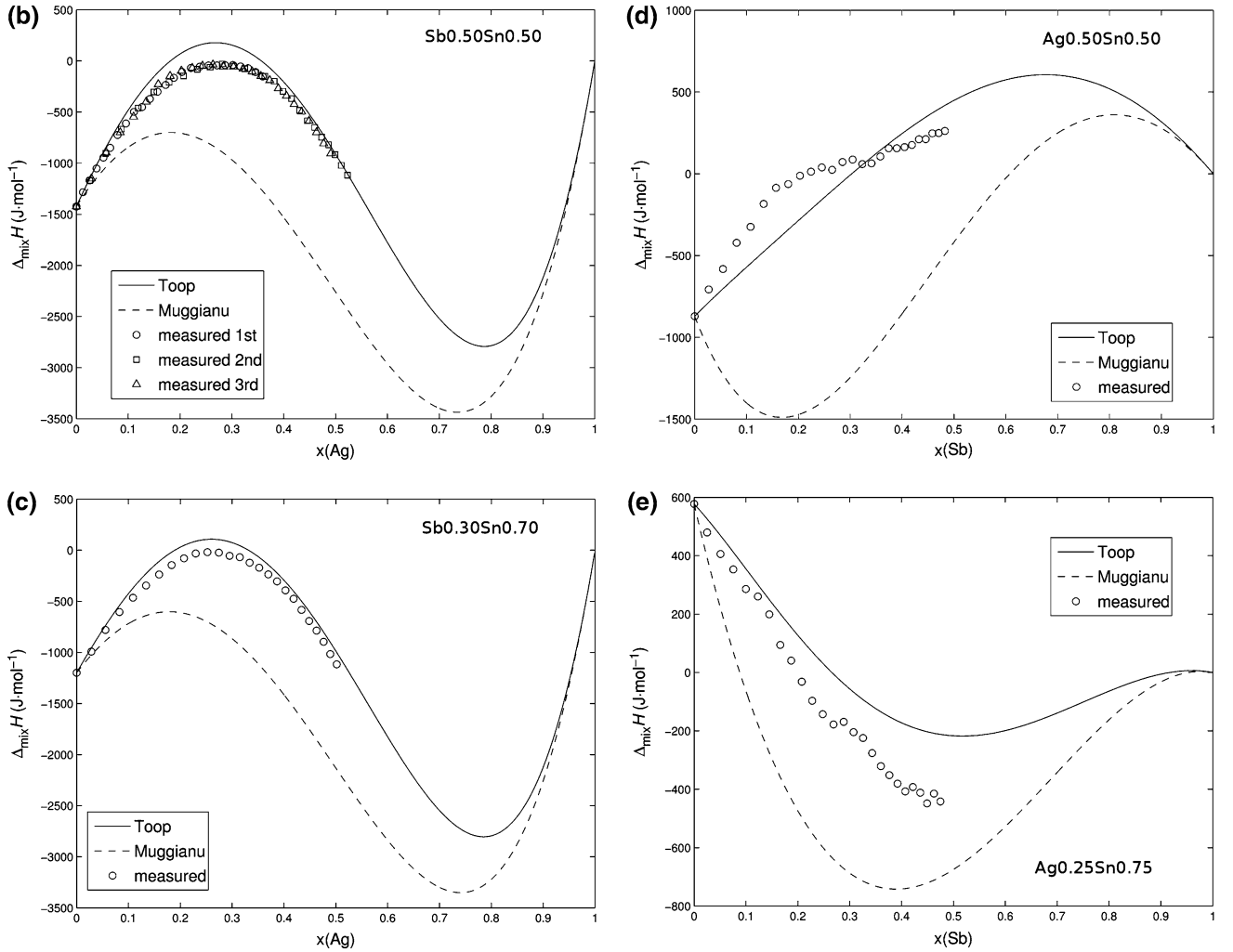


Fig. 1. Integral molar enthalpies of mixing of liquid Ag-Sb-Sn alloys at 530°C. The experimental values are presented together with those calculated by Toop and Muggianu methods. Reference state: pure liquid components. The letters refer to the measured sections (also indicated inside each figure): B: $\text{Sb}_{0.5}\text{Sn}_{0.5}$; C: $\text{Sb}_{0.3}\text{Sn}_{0.7}$; D: $\text{Ag}_{0.5}\text{Sn}_{0.5}$; E: $\text{Ag}_{0.25}\text{Sn}_{0.75}$.

Therefore, after i drops, the total mixing enthalpy of the liquid alloy is

$$\Delta_{\text{mix}}H = \Delta_{\text{mix}}H_0 + \sum_{j=1}^i \Delta_{\text{mix}}H_j.$$

For all the measurements, the molar mixing enthalpy can therefore be expressed as follows:

$$\Delta_{\text{mix}}H_m = \frac{\Delta_{\text{mix}}H}{\sum_{j=0}^i n_j}.$$

In case n_i is very small, $n_i \ll m$, where m is the number of moles of the alloy $\text{A}_x\text{B}_y\text{C}_z$; the reaction of mixing and thus the heat effect can be related only to n_i moles of solid metal A added without a significant change in the global composition, and the partial mixing enthalpy can be derived directly as

$$\Delta_{\text{mix}}\bar{H}_m = \frac{\Delta_{\text{mix}}H_i}{n_i}.$$

EXPERIMENTAL RESULTS AND DISCUSSION

The experimental results along with the experimental conditions, which include the starting amount of the bath, the experimental temperature, and the mass of each drop, are reported in Tables III–V. The integral enthalpy refers to the alloy concentration after each drop, while the averaged composition before and after each drop was considered for the partial enthalpy. The excess mixing enthalpy values for the binary bath alloys were taken from the COST MP0602 database.⁵⁵ In all, six measurements were performed along section B (pure Ag dropped into a $\text{Sb}_{0.5}\text{Sn}_{0.5}$ liquid bath). For all three temperatures studied, the integral mixing enthalpies became positive as the Ag concentration increased, and the trend showed a maximum at around 30 at.% Ag. The values obtained from different runs for the same temperature and composition are close to each other, with a

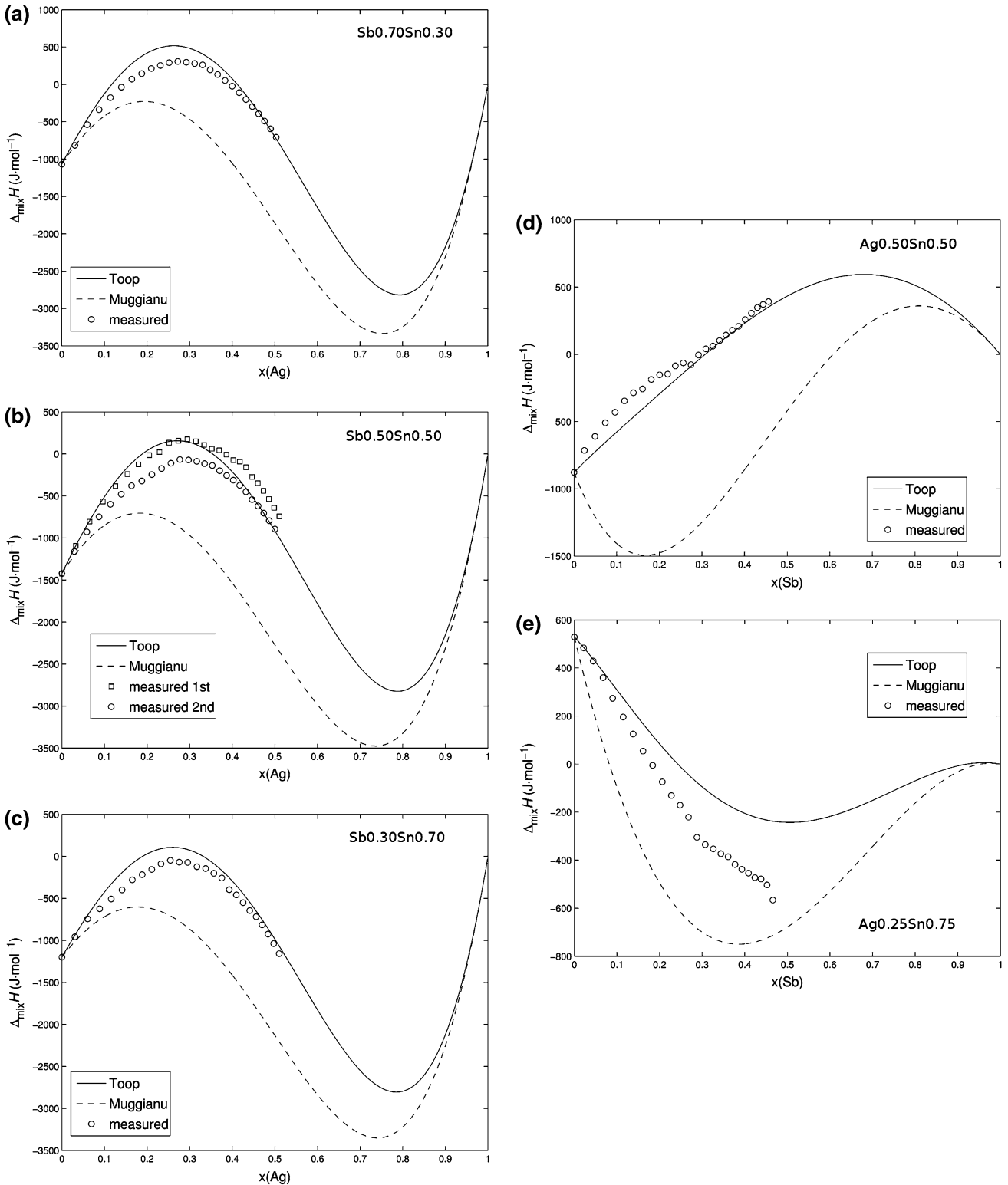


Fig. 2. Integral molar enthalpies of mixing of liquid Ag-Sb-Sn alloys at 600°C. The experimental values are presented together with those calculated by Toop and Muggianu methods. Reference state: pure liquid components. The letters refer to the measured sections (also indicated inside each figure): A: Sb0.7Sn0.3; B: Sb0.5Sn0.5; C: Sb0.3Sn0.7; D: Ag0.5Sn0.5; E: Ag0.25Sn0.75.

maximum difference of about 250 J/mol. The three measurements performed at 530°C show almost the same values, and very good reproducibility can be observed.

Muggianu⁵⁶ and Toop⁵⁷ extrapolation models were used to calculate the enthalpy of mixing for the Ag-Sb-Sn ternary system from those of the constituent binary systems in order to compare the measured and

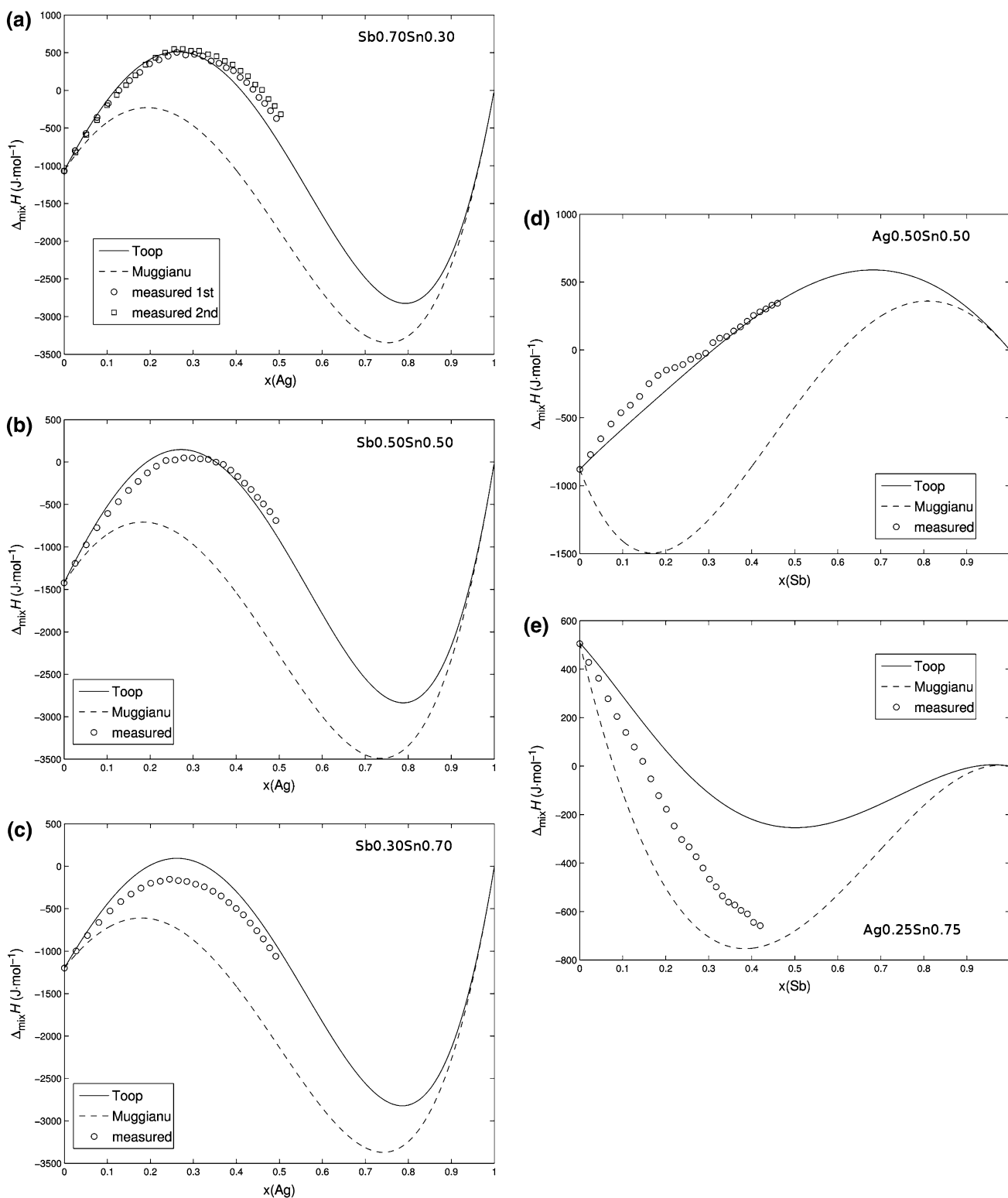


Fig. 3. Integral molar enthalpies of mixing of liquid Ag-Sb-Sn alloys at 630°C. The experimental values are presented together with those calculated by Toop and Muggianu methods. Reference state: pure liquid components. The letters refer to the measured sections (also indicated inside each figure): A: Sb_{0.7}Sn_{0.3}; B: Sb_{0.5}Sn_{0.5}; C: Sb_{0.3}Sn_{0.7}; D: Ag_{0.5}Sn_{0.5}; E: Ag_{0.25}Sn_{0.75}.

predicted values. With the Toop model, Ag was chosen as element A, which is treated differently from the other two elements on the basis that the mixing

enthalpy curve Sb-Sn is symmetric, showing a regular solution behavior, and the curves of Ag-Sb and Ag-Sn show a similar S-shape trend. From the

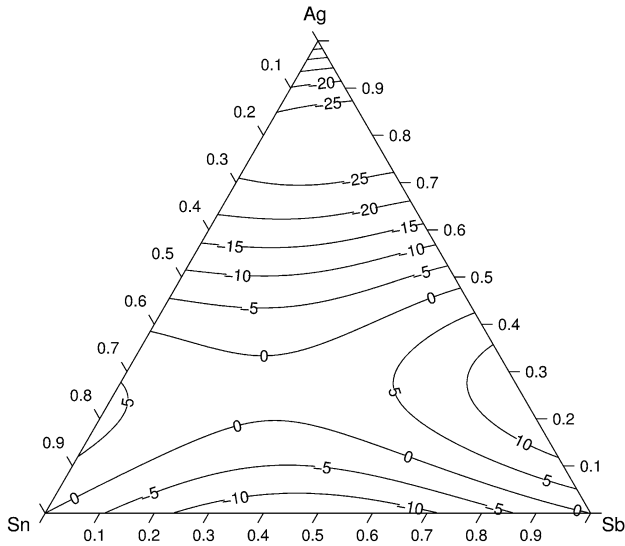


Fig. 4. Isoenthalpy curves (100 J/mol) of the ternary Ag-Sb-Sn alloys at 550°C, obtained using the Toop model (standard states: pure liquid metals).

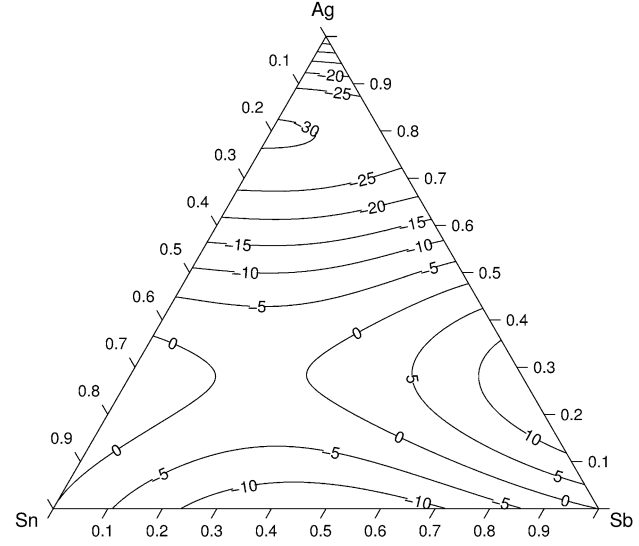


Fig. 5. Isoenthalpy curves (100 J/mol) of the ternary Ag-Sb-Sn alloys at 950°C, obtained using the Toop model (standard states: pure liquid metals).

literature data available for these two binary systems, we may observe a maximum point at the Ag-poor side, indicating a demixing tendency of the liquid alloys and a minimum point in the Ag-rich region which implies a potential compound formation behavior near these compositions, which is consistent with the binary phase diagrams.

The calculated results compared with the experimental measurements along different sections at 530°C, 600°C, and 630°C are shown in Figs. 1–3, respectively.

For sections A ($\text{Sb}_{0.7}\text{Sn}_{0.3}$), B ($\text{Sb}_{0.5}\text{Sn}_{0.5}$), and C ($\text{Sb}_{0.3}\text{Sn}_{0.7}$) in which Ag is the dropped element (Figs. 1c, 2c, 3c, 1b, 2b, 3b, 2a, and 3a), both models predict a similar S-shape trend, and the values calculated with the Toop model are much closer to the experimental values. Generally, the values calculated with the Toop model are always higher than the measured ones, and the difference between the extrapolated and measured values is small, with a maximum difference of about 200 J/mol. Thus no ternary interaction parameters are necessary in order to fit the experimental values.

Considering the measurements made when Sb pieces are dropped in Ag-Sn binary bath (section D, $\text{Ag}_{0.50}\text{Sn}_{0.50}$ and section E, $\text{Ag}_{0.25}\text{Sn}_{0.75}$, see Figs. 1d, 2d, 3d, 1e, 2e, and 3e) the two models show different predictions. Concerning section D, the Toop model as well as the measured data indicate increasing mixing enthalpy values with increasing Sb content. The curve calculated using the Toop model shows a single maximum value around 70 at.% Sb content (for which no experimental data are available), while the integral mixing enthalpy extrapolated using the Muggianu model shows an S-shape trend. Using this model, the mixing enthalpy becomes negative with increasing Sb, reaching a

minimum value around 18 at.% Sb, which does not fit with the experimental results. Experimentally, we observed a peculiar systematic trend of the mixing enthalpy for all the investigated temperatures, which cannot be reasonably explained. In the composition range from 0 at.% to 30 at.% Sb we observe an irregular trend with a kink around 30 at.% Sb. Beyond this point, for $T = 600^\circ\text{C}$ and 630°C good agreement between the experimental and the calculated values obtained with the Toop Model may be observed. Concerning the experimental results obtained for section E, we observed a rapid decrease in the mixing enthalpy values with increasing Sb content. Moreover, we may observe a kink and a slope change at around 30 at.% Sb, which becomes more regular when the temperature changes from 530°C to 600°C and 630°C. The experimental trend lies between the two curves calculated using the Toop and Muggianu models. This experimental behavior could be explained by the possible existence of a liquid miscibility gap which extends up to compositions around 30 at.% Sb. This hypothesis is under evaluation by using CALPHAD modeling.

The isoenthalpy curves of liquid Ag-Sb-Sn alloys calculated at 550°C and 950°C using the Toop model are shown in Figs. 4 and 5. The general shape of the isoenthalpy lines are the same for the two temperatures, with a saddle point in the central part of the Gibbs triangle. At 950°C, the extrapolated values agree quite well with the experimental results obtained by Gather et al.³⁹ across the whole composition range. When the temperature changes from 550°C to 950°C, the enthalpy values near the saddle point change from positive to negative, in agreement with the results of Ref. 39.

The DSC analysis data obtained for the Ag-Sb-Sn samples with key selected compositions are

Table VI. Ag-Sb-Sn alloys: experimental DSC results and SEM/EDS global composition

| Sample | SEM/EDS Composition | | | Temperature Detected on Heating (°C) | | Temperature Detected on Cooling (°C) | | Effects |
|--------|---------------------|----------|----------|--------------------------------------|---------------------------------|--------------------------------------|---------------------------------|--|
| | x_{Ag} | x_{Sb} | x_{Sn} | 1st Run (1°C/min) | 2nd Run (0.3°C/min) | 1st Run (1°C/min) | 2nd Run (0.3°C/min) | |
| | 1DSC | 0.46 | 0.40 | 0.14 | 375 440 464 | 375 439 466 | 374 433 448 | |
| 2DSC | 0.27 | 0.37 | 0.36 | 229 305 373 392 434 | 228 305 374 391 432 | 228 375 388 397 | 228 374 375 375 386 | U ₃ U ₂ U ₁ Valley Liquidus |
| 3DSC | 0.30 | 0.22 | 0.48 | 231 308 346 440 | 231 308 346 442 | 230 300 339 389 | 230 306 328 408 | U ₃ U ₂ Valley Liquidus |
| 4DSC | 0.23 | 0.58 | 0.19 | 375 428 468 | 375 428 459 | 375 389 451 | 375 395 451 | U ₁ Valley Liquidus |
| 5DSC | 0.17 | 0.29 | 0.54 | 231 309 325 390 | 231 309 323 385 | 230 309 313 370 | 229 309 315 365 | U ₃ U ₂ Valley Liquidus |
| 6DSC | 0.16 | 0.37 | 0.48 | 228 306 367 393 | 230 306 366 388 | 228 300 348 349 | 229 300 346 349 | U ₃ U ₂ Valley Liquidus |

summarized in Table VI together with the compositions of the alloys obtained by SEM/EDS analysis after DSC measurements. All samples were processed twice: the first heating/cooling was performed at 1°C/min rate and the second at 0.3°C/min. The temperature values obtained at different rates (1°C/min and 0.3°C/min) are reported in Table VI. Figure 6 shows the DSC curve of sample 6DSC (Table VI), while Fig. 7 displays a micrograph of sample 4DSC showing large primary crystals of (Sb)_{ss} surrounded by ϵ phase and by a mixture of ϵ and β phases. Three ternary invariant reactions have been identified, and good reproducibility of the transformation temperatures obtained may be observed in Table I. The temperatures assigned in this work are in very good agreement with the literature data. The temperature observed for the U₂ invariant reaction ($L + \beta \leftrightarrow \epsilon + Sn_3Sb_2$, 308°C) is lower than the p₆ invariant reaction temperature,^{38,50,51} confirming the U-type invariant equilibrium, in agreement with Refs. 42 and 48.

According to the literature data and our measurements, a reaction scheme for the Ag-Sb-Sn system is proposed in Fig. 8. This scheme is divided by a dashed line: the upper part is in good agreement with the reaction scheme reported by Ref. 48. The part below the dashed line is proposed in order to complete the Scheil diagram. Taking into account that Sn₃Sb₂ is not stable at room temperature,^{50,51} one more invariant reaction must be taken into

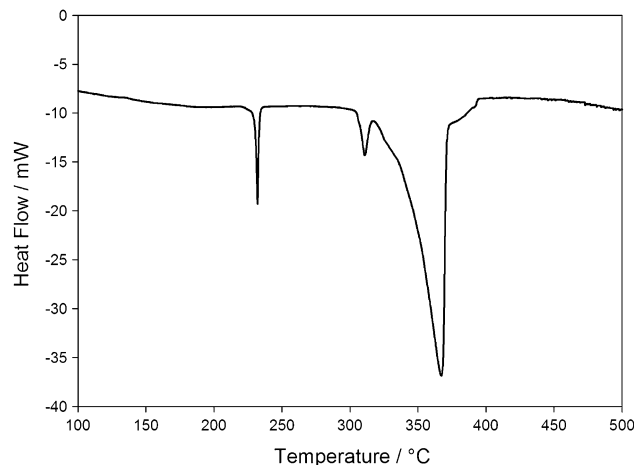


Fig. 6. DSC curve on heating (1°C/min) of sample 6DSC, see Table VI.

account, connecting e₂, U₂ and U₃, and an E-type reaction, $Sn_3Sb_2 \leftrightarrow \epsilon + \beta + (Sn)$, is here proposed.

CONCLUSIONS

A set of mixing enthalpy measurements at 530°C, 600°C, and 630°C obtained by using a high-temperature Calvet-type calorimeter is presented for the Ag-Sb-Sn ternary system. The ternary liquid alloys have been investigated along five different

sections: $\text{Ag}_{0.25}\text{Sn}_{0.75}$, $\text{Ag}_{0.50}\text{Sn}_{0.50}$, $\text{Sb}_{0.30}\text{Sn}_{0.70}$, $\text{Sb}_{0.50}\text{Sn}_{0.50}$, and $\text{Sb}_{0.70}\text{Sn}_{0.30}$. No significant temperature dependence of the mixing enthalpy could be observed in the temperature range considered.

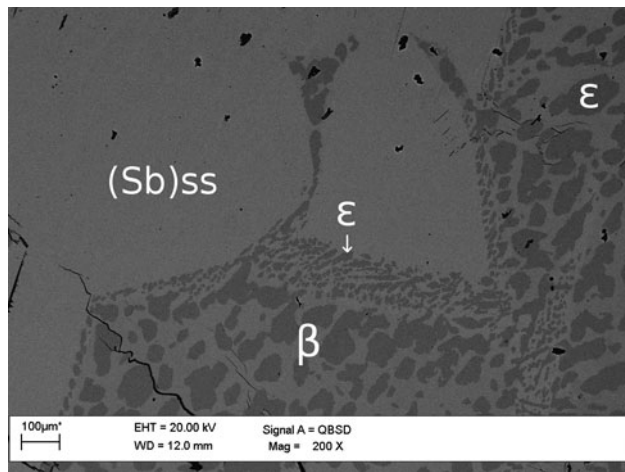


Fig. 7. SEM image (BSE mode) of sample 4DSC (see Table VI). Large primary crystals of $(\text{Sb})_{\text{ss}}$ are surrounded by ε phase and by a mixture of ε and β phases.

The experimental data were compared with those calculated from the extrapolation methods, and generally the Toop model gives a suitable representation of the enthalpy of mixing for the liquid ternary system. Unusual behavior was observed experimentally for the addition of pure Sb to the $\text{Sn}_{0.75}\text{Ag}_{0.25}$ liquid bath, giving an indication of the possible existence of a liquid miscibility gap in the ternary system. Comparing the values of the enthalpy of mixing reported in the literature for the Ag-Sn binary system, we may observe the effect due to the Sb addition following the composition of the Ag-Sn metallic bath. The mixing enthalpy of the $\text{Ag}_{0.50}\text{Sn}_{0.50}$ alloy becomes less negative when Sb is added, while for the $\text{Ag}_{0.25}\text{Sn}_{0.75}$ liquid bath, we notice an incremental exothermicity. We should expect that this will affect the thermophysical properties, such as surface tension and wettability, and the reaction products produced at the interface during the soldering process.

DSC measurements have also been performed on samples having selected key compositions in order to identify and confirm the invariant ternary reactions present in the ternary system. No ternary intermetallic compounds were observed in the

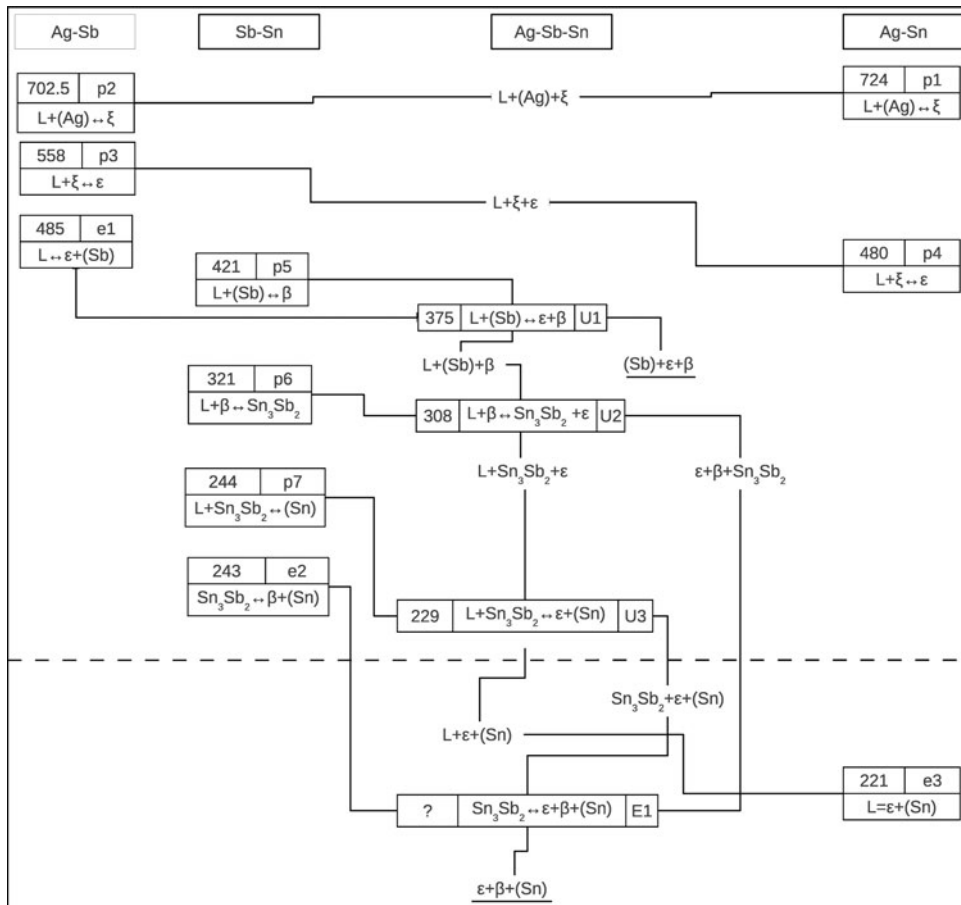


Fig. 8. Ag-Sb-Sn reaction scheme (Scheil diagram). The reported temperatures ($^{\circ}\text{C}$) of the Ag-Sb-Sn ternary invariant reactions have been obtained during this work. The part below the dashed line is proposed to complete the reaction scheme.

Ag-Sb-Sn ternary system, in agreement with the literature information.

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