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In the various forms of semisolid processing such as thixoforming and thixoforging, the entry into the die occurs in a fraction of a second so it is the transient rheological behavior which governs the initial stages of flow. In experiments in the literature, this rheological behavior is probed through applying rapid transitions in shear rate under isothermal conditions. There is contradictory evidence as to whether the behavior during these transitions is shear thinning or shear thickening, although it is clear that once in the die the material is thinning. Here the data in the literature are reanalyzed to obtain a rationalization of the contradictions which has not previously been available. It is argued that if a suspension is initially in a disagglomerated state (*i.e.*, one which is initially sheared), the instantaneous behavior with a jump-up in shear rate is shear thickening (even if the long-term steady-state behavior is shear thinning) provided the fraction solid is greater than about 0.36 and the final shear rate at the end of the jump is greater than about 100 s^{-1} . If the jump-up in shear rate is made from rest then yield masks the shear thickening.

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I. INTRODUCTION AND BACKGROUND

PROCESSING of metals in the semisolid state is a widely established technology (*e.g.*,^[1] Thixoforming, thixocasting, thixoforging, thixomolding, rheocasting, and rheoforming are all semisolid processing methods. They rely on the *thixotropic* property of metallic alloys in the semisolid state which have a spheroidal rather than dendritic microstructure; when sheared the material thins but when allowed to stand, it thickens again.^[2,3] This behavior is exploited to drive the material into a die and obtain a near net shape component in one shot. Although the technology is established, the modeling of such complex systems still needs further development. In particular, the entry into the die occurs in a fraction of a second so it is the transient rheological behavior which governs the initial flow. In the literature, this rheological behavior is probed experimentally through applying rapid transitions in shear rate under isothermal conditions.

In this section, the scene will be set for the reanalysis by outlining the basic nature of thixotropy in semisolid metallic alloy systems; the distinction between steady-state behavior and that associated with a transient; the connection between discontinuous shear thickening as encountered for dense suspensions of cornstarch in water and the potential for shear thickening to be

masked by shear stress. In addition, the interplays between yield stress and thixotropy and the distinction between the existence of a yielded zone and shear banding/shear localisation are described. All these issues are relevant to the reanalysis here of the experimental data in the literature to arrive at a rationalization of the contradictory evidence as to whether shear thickening does occur in semisolid metals. Finally, in this section, the concept of ‘isostructure’ with rapid transitions in shear rate is highlighted along with the issues around the timescale for rapid shear rate jump experiments, before the aim of the paper is summarized.

A. Basic Nature of Thixotropy in Semisolid Metallic Alloy Systems

The particles here are spheroids of solid metal in a Newtonian liquid metal matrix and there is the potential for particle aggregation by the formation of minute ‘welds’ at the points where the spheroids contact by a mechanism very akin to sintering. The particles therefore show some *cohesion* in the terminology of soil mechanics. However, many of the mechanisms of interaction which apply in non-metallic suspension systems (*e.g.*, electrostatic, steric, induced electric or magnetic dipoles) do not apply here. When the material is allowed to stand, or is sheared at a relatively low shear rate, the particles gradually agglomerate, with the average size of the agglomerates related to the shear rate.^[3] If the solid fraction is fairly high (in the region of 0.4 or above), when the material is still, the spheroids develop a solid ‘skeleton’ that provides some rigidity. The authors have recently shown that the skeleton introduces an elastic-type response into the behavior during rapid compression from rest.^[4] When the shear rate increases, the agglomerates are broken up and, for a constant shear rate, a new characteristic agglomerate

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size is established. Therefore, in the steady state at a given shear rate, there is an equilibrium between agglomeration and disagglomeration.

B. Distinction Between Steady-State Behavior and Transients

It is important to distinguish here between steady-state behavior and that associated with a transient. So for alloys in the partially solid state, if the material is sheared for a substantial period at a particular shear rate, a steady state will be established (although this may be a quasi-steady state because some particle coarsening will be occurring by Ostwald ripening). If a series of such steady states are established and the viscosity for each calculated, a plot of viscosity vs shear rate can be derived. When the viscosity decreases with increasing shear rate, the material is termed shear thinning and, if it increases, shear thickening.^[5] For alloys with spheroidal microstructure in the semisolid state, the behavior in the steady state is always shear thinning.

C. Connection with Discontinuous Shear Thickening in Dense Suspensions of Cornstarch in Water: The Masking of Shear Thickening by a Yield Stress

A particularly dramatic form of shear thickening is that termed *discontinuous shear thickening* where the viscosity increases by many orders of magnitude for a small increase in shear rate. This is the phenomenon observed with dense suspensions of cornstarch in water, which allows someone to run across the surface of the suspension in a swimming bath for example (but when they stand still they sink in). Brown *et al.*^[6] have argued that all suspensions should show shear thickening under certain conditions because the underlying mechanisms (hydrodynamics,^[7,8] dilatation^[9–11]) are general but they demonstrate that shear thickening can be masked by a yield stress. They attribute discontinuous shear thickening to frictional particle contacts that form when dense particle arrangements begin to dilate and push against boundaries.^[12] The shear thickening could be enhanced to give a discontinuous effect if the hydroclusters (giving rise to continuous shear thickening) eventually become so large that they span the system and jam. Brown and Jaeger^[13] have recently identified for cornstarch in water that shear thickening can occur because of the confining stress at boundaries frustrating dilatation.

Micromechanical modeling applied on a Representative Volume Element containing solid globules, solid bonds, entrapped and free liquid has been developed and used to predict the strain rate sensitivity of the overall viscous material (Favier *et al.*^[14]). The solid phases were considered non-Newtonian with a strain rate sensitivity index lower than one, as for hot-deformed alloys, while the liquid phases were considered as Newtonian. The modeling, considering viscous interactions, was not able to produce a shear-thickening behavior. This result is consistent with the fact that the shear thickening response is not an intrinsic bulk material response but is related to interaction with the

boundaries which confine the suspension (Brown and Jaeger^[15]).

D. Existence of a Yielded Zone; Distinction Between a Yielded Zone and Shear Banding/Shear Localisation

The interplay between yield stress and thixotropy is discussed in Møller *et al.*^[16] They argue that below a critical shear rate, all the flow is localized in a region near the shearing wall, and *if the globally imposed shear rate is increased it is not the shear rate in the sheared region that increases but rather the extent of the sheared region which grows – to fill the entire gap of the shear cell exactly at the critical shear rate.* (Note that this localization is distinct from wall slip). Møller *et al.*'s^[16] paper is concerned with the steady state rather than transients, and is supported by experimental data for semisolid metal alloys.^[17] Alexandrou *et al.*^[18,19] focus on the early stages of breakdown by applying finite element modeling to the fluid in the rheometer gap, presenting graphs which show, for shear rates below a critical shear rate, the yielded zone initially expands but then the boundary between yielded and unyielded material reaches a stationary position (and if the gap is relatively narrow this will be equivalent to the whole gap having yielded). In addition, the boundary can in fact retract.

There is a distinction between the existence of a yielded zone and issues of shear banding and shear localisation. Essentially, once shear localisation starts to occur, it becomes a self-exacerbating phenomenon with shear being increasingly concentrated in that band. Gourlay and Dahle have discussed this in a paper in *Nature*^[20] with illustrations of banding from a vane rheometer (Figure 1(a)). However, in the quenched samples from concentric cylinder rheometers (*e.g.*, Liu's thesis^[21]), there is no evidence of such banding (Figure 1(b)). This may well be because the number of particles spanning the gap is much smaller than in the Gourlay and Dahle experiments.^[20] Also the Gourlay and Dahle hypothesis is essentially based around dilatation. In contrast with Gourlay and Dahle, in the concentric cylinder rheometer experiments reviewed here, there are relatively few particles spanning a gap which is long and narrow, giving severe restriction on dilatation. This is consistent with the argument in Brown and Jaeger^[12] about the confining stress of boundaries frustrating dilatation.

E. The Concept of 'Isostructure' and the Timescale for Rapid Shear Rate Jump Experiments

The behavior during such transient conditions of shear rate for semisolid alloys has been represented by Quak^[22] as shown in Figure 2. When a rapid jump-up in shear rate occurs (the upper part of Figure 2), immediately after the jump (in that *instant*), the material is 'isostructure' with the starting material. A fast process of deagglomeration (breaking of bonds between spheroids) then occurs. Subsequently, a much slower diffusion controlled process of coarsening and spheroidisation takes place (note the change in *shape* of particles). For a

jump-down in shear rate (the lower part of Figure 2), the processes after 'isostructure' are 'fast' agglomeration followed by a slow growth of necks between spheroids and coarsening (although it should be noted that the agglomeration in the jump-down in the lower half of Figure 2 is significantly slower than the deagglomeration in the upper half with the jump-up).

A rapid jump-up in shear rate then has to be fast enough to ensure isostructure, *i.e.*, it has to be faster than the characteristic disagglomeration time. Kumar

et al.^[23] evaluate this to be of the order of seconds but Liu *et al.*^[24] find it to be in the region of ~ 0.16 s (their Table I). The time for the transient in shear rate is of the order of 10 ms in Kumar *et al.*^[23] and 100 ms in Liu *et al.*^[24] thus satisfying this requirement. The timescale for the transient in Koke and Modigell^[25] is not stated but is short. Peng and Wang^[26] have a transient time of 0.1 s. In practice, a purely isostructural jump will be impossible to achieve because some microstructural processes will always start to occur during the jump.

F. Aim of the Paper

There is contradictory evidence in the literature^[22–29] as to whether the behavior during rapid increases in shear rate is shear thinning or shear thickening, although it is clear that once in the die the material is thinning.^[30] Kumar *et al.*^[23,27] and Koke and Modigell^[25,28] (with further analysis of Reference 28 by Burgos *et al.*^[29]) find their material to be shear thickening during the transient, Quaak^[22] and Liu *et al.*^[24] observe the material is shear thinning. Peng and Wang^[26] study the behavior but do not state a conclusion. Here the data in the literature are reanalyzed, aiming to answer the question 'Does shear thickening occur in semisolid metals?'. This paper does not present new experimental results but rather a new, consistent, objective, analysis to rationalize apparent contradictions. The experimental results from the literature have never been compared and contrasted in this systematic way before. The analysis is not dependent on the constitutive equation assumed by the authors of the experimental papers but rather takes their experimental data and deduces whether the behavior is shear thickening or shear thinning, using classical rheological understanding of the definitions of shear thickening

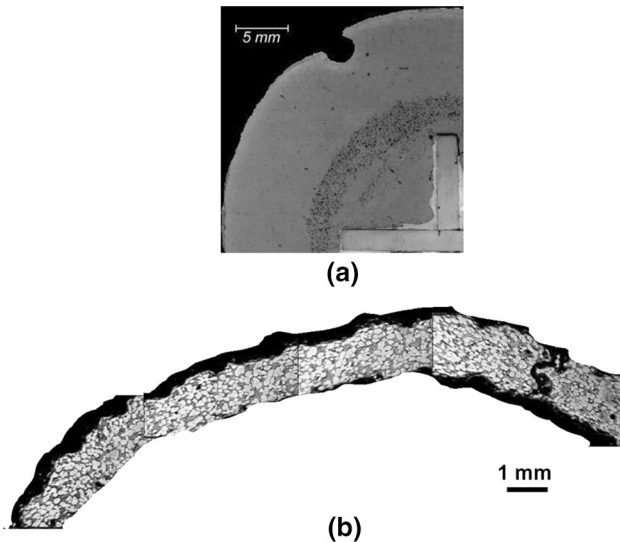


Fig. 1—(a) Vane rheometry of partially solidified Mg alloy showing shear banding evidenced by a localized band of porosity approximately 11 grains wide, taken with permission from Ref. [20]. (b) Sn 15 pct Pb alloy quenched in a cylindrical rheometer gap showing that no shear banding or discontinuity across the microstructure in the gap is evident, taken with permission from Ref. [21].

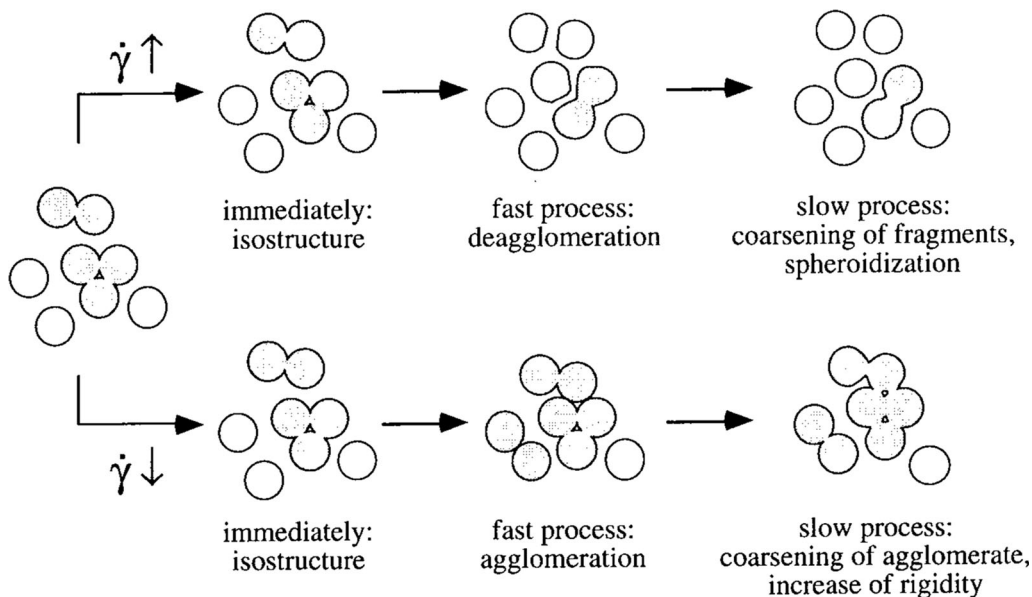


Fig. 2—Schematic diagram^[22] showing that when a rapid jump-up in shear rate occurs, immediately after the jump, the materials are 'isostructure' with the starting material. A fast process of deagglomeration (breaking of bonds between spheroids) then occurs. Subsequently, a much slower diffusion controlled process of coarsening and spheroidisation takes place (note the change in *shape* of particles). When the shear rate jump is down, the processes are a fast process of agglomeration and a slow process of neck growth and coarsening.

and shear thinning. It is assumed that deformation is homogeneous but the potential existence of a yielded zone is discussed to identify where this is relevant.

II. ANALYSIS

In this section, firstly, the experimental results in the literature for rapid shear rate jumps are summarized, and then, the method is given for the new analysis of those results.

A. Experimental Results in the Literature for Rapid Shear Rate Jumps

The experimental details for experiments on Sn15 pct Pb (which are concentrated on here as it is the 'model system' for the rheology of semisolid alloys) are summarized in detail in Table I as a series of experimental factors might explain the contradictions. All the results in Table I involve applying jumps in shear rate in cylindrical rheometers over very short time periods and measuring the consequent shear stress response. Table I identifies how each research work has reached its conclusion about whether the behavior is shear thinning or shear thickening as this is critical for what follows. The deliberate strategy here is to keep the extensive detail about the experiments in the literature, and how those authors analyze their data, in the table so that the flow of the argument in the main part of the paper is clear.

B. Method of Analysis in this Paper

Classical rheological understanding of the definitions of shear thickening and shear thinning means that absolute peak shear stress during the jump should be plotted against the shear rate the jump finishes on (Figure 3). Here, experimental data from the literature papers are used, and the analysis is not dependent on any constitutive equation. The deformation is however assumed to be homogeneous. The right-hand column in Table I identifies how the data for this figure have been obtained from the data in the literature. If the curve has as increasing slope with increasing shear rate, it represents shear-thickening behavior, and a decreasing slope with increasing shear rate is shear thinning. To obtain results which can be compared, a conditioning shear rate (*i.e.*, the shear rate before the jump) has been identified which is common between the results of Koke and Modigell^[25] (their Figure 18(b)) and the results of Liu *et al.*^[24] (their Table IV). The only common shear rate is 100 s^{-1} . There are no results where the fraction solid is the same. The plot for Koke and Modigell^[25] with a fraction solid 0.41 curves upwards and hence is shear thickening. For Liu *et al.*^[24] at a fraction of solid of 0.5, there is a slight trend upwards, again indicating shear thickening. For a lower fraction of solid of 0.36 from Liu *et al.*, the curve is clearly shear thinning (see Figure 3(b)). Results from Kumar *et al.*^[27] have also been plotted. Although these are not from the common starting shear rate of 100 s^{-1} (they are based on Figure 2

in Reference 27 paper I), they do allow some examination of trends and again show shear thickening. Liu *et al.*'s^[24] result for a fraction of solid of 0.36 is therefore the unusual result. This might be explained if there is some transition between 0.36 and 0.41. The Peng and Wang^[26] results then support the hypothesis that there is a transition. Their results are for a conditioning shear rate of 200 s^{-1} . For fractions solid of 0.2 and 0.36, there is little or no evidence of shear thickening but at fractions solid of 0.46 and 0.5 there is. The other observation from Figure 3(b) is that, for jumps to a shear rate of 100 s^{-1} or less, where the fraction solid is less than or equal to ~ 0.36 , shear thickening is not apparent, and for the higher fractions solid, it is hardly discernible. Most of the results for Liu *et al.*^[24] are in this regime which helps to explain their thinking that they do not observe shear thickening.

III. DISCUSSION

A. Factors which Might Explain the Discrepancies and Contradictions

Factors which might explain the discrepancies include the following:

- (1) Differences in the shear rate ranges and fractions solid considered;
- (2) Whether inertia (both of the measuring head and of the semisolid fluid itself) has been appropriately considered;
- (3) The size of the particles in relation to the size of the gap between the inner bob and outer cup of the rheometer;
- (4) The existence of a yield stress masking the shear thickening phenomenon as argued by Brown *et al.*^[6]

B. Shear Rate Range and Fraction Solid

The shear rate range for the experiments by Kumar and co-workers^[23,27] is higher than that for the experiments by Koke and Modigell^[25,28] and Liu *et al.*^[24] (and higher shear rate ranges would be expected to exacerbate shear rate thickening if it is due to hydrodynamics or dilatation). However, the latter two sets of experiments overlap in their shear rate ranges but are still apparently contradictory according to their authors. In terms of fraction solid, Kumar *et al.*^[23,27] give results for 0.45 and above, Peng and Wang^[26] for 0.2 through to 0.5, Koke and Modigell^[25] for 0.41 and above, and Liu *et al.*^[24] for 0.36 and 0.5. For fractions solid of 0.36 and less, the spheroids are quite widely separated and may well be less susceptible to clustering and jamming than for the higher fractions of solid.

C. Inertia

There are two types of inertia to consider; that of the measuring head and that of the semisolid fluid itself. Kumar considers inertia in the semisolid fluid in detail in

Table I. Comparison of Rheology Experiments by Kumar *et al.*,^[23,27] Peng and Wang,^[26] Modigell *et al.*,^[28] Koke and Modigell,^[25] Liu *et al.*,^[24]

References	Rheometer	Material/Volume Fraction Solid	Particle Size, Morphology and Size Distribution	Time Scale of Transient, Data Acquisition Rate, Conditions	Shear Rate Jumps	Comments (Including How We Derive Our Data in Fig. 3 from the Data in the Literature)
Kumar <i>et al.</i> ^[23,27]	Couette (constructed at MIT) and bob grooved. $T \pm 0.5$ K (0.5 °C) axially and radially. Argon atmosphere. Gap 3 mm. Characteristic time for fully developed flow across gap calculated as ms	Sn-15 wt pct Pb. Volume fractions estimated using temperature-volume fraction curve from Joly PhD Thesis MIT 1974. ^[31] 475 K (202 °C)-0.3, 471.6 K (198.6 °C)-0.4, 469 K (196 °C)-0.45	Particle size stated as 50 to 100 μm in Ref. 23. Fig. 1 in [27] consistent with this but paper states average diameter of 150 μm in experiments. Fig. 1(a) in Ref. [27] suggests spheroids almost perfectly spheroidal but with extensive inter-particle bonding	~10 ms, 100 Hz. ^[23] 200 Hz. ^[27] In fact, Kumar thesis ^[23] identifies 100 Hz for shear rate ramp and 200 Hz for jump experiments. Starting from the steady state, the temperature is lowered from liquid to the desired temperature while stirring at $\dot{\gamma}_0$. Fluid sheared at $\dot{\gamma}_0$ for 25 min	$\dot{\gamma}_0 = 300 \text{ s}^{-1}$ to a range of shear rates up to 800 s^{-1}	Kumar in his PhD thesis ^[22] , p.96) calculates the microscopic Reynolds number $\text{Re}^{\text{micro}} = \frac{\rho R_c \dot{\gamma}}{\mu}$, where ρ is density, d is particle diameter, $\dot{\gamma}$ is average shear rate, and μ_{eff} the effective viscosity of the slurry. This is of the order of 10^{-1} for Sn15 pct Pb (using a typical particle size of 100 μm , a minimum effective viscosity of 0.5 Pa s, and a maximum average shear rate of 800 s^{-1}). He double-checks the magnitude of the inertial effects with the Bagnold number and concludes there are no significant inertial effects. He then looks at macroscopic R_c , and shows (using gap as length parameter) that R_c is about 200, i.e., well below the level where inertial effects would occur. There is no mention in the papers by Kumar <i>et al.</i> , ^[23,27] or in the Kumar thesis ^[23] of any consideration of the inertia of the measuring head but inspection of the experiments with shear rate transients at varying shear rates suggests this is not an issue. $f_s > 0.45$ produced large spikes in torque that are attributed to the formation of particulate 'bridges' between the cup and the bob (also seen by Turing and Wang ^[8,33] in semisolid metal slurries and Brady and Bossis ^[9] in hard sphere suspensions). Kumar <i>et al.</i> conclude shear thickening is occurring because the graph of shear stress vs shear rate for shear rate transients has an upward curve. The Kumar <i>et al.</i> results in our Fig. 3 are based on Fig. 2 in paper 1 Ref. 27 which shows peak shear stress vs final shear rate for a series of jumps from an initial, conditioning shear rate of 300 s^{-1}

Table I. continued

References	Rheometer	Material/Volume Fraction Solid	Particle Size, Morphology and Size Distribution	Time Scale of Transient, Data Acquisition Rate, Conditions	Shear Rate Jumps	Comments (Including How We Derive Our Data in Fig. 3 from the Data in the Literature)
Peng and Wang ^[26]	Couette	Sn-15 wt pct Pb, Volume fraction 0.2, 0.35, 0.46, 0.54		*The start-up time for the rotating cup to reach its steady state velocity is less than 0.1 s and the maximum data-sampling rate is 200 Hz. The time needed for molten metal to reach the new shear stress after a shear rate change jump is corresponding to the inertial time scale of the molten metal which depends on the viscous diffusion of the material. Therefore, the peaks observed are mainly caused by the slurry system rather than the viscometer itself	200 s ⁻¹ up to 400 and 800 s ⁻¹ and 100 s ⁻¹ up to 200 s ⁻¹ . 200 s ⁻¹ down to 50 and 100 s ⁻¹ . 400 and 800 down to 200 s ⁻¹ .	One of the Peng and Wang conclusions is 'The shear stress response with a sudden increase in the shear rate shows an overshoot before it decreases to the final steady state, while that of a molten metal shows no overshoot. The overshoot usually increases with fraction solid, step size in shear rate change and rest time.'
Modigell <i>et al.</i> ^[28]	Couette	Sn-15 wt pct Pb, Volume fraction 0.35, 0.45, 0.5		Step changes both up and down between a series of different shear rates	Variety of jumps. Lowest shear rate 11.2 s ⁻¹ , Highest 179 s ⁻¹	To obtain the Peng and Wang data in our Fig. 3, we use the data from their Tables II and IV which have 200 s ⁻¹ as the starting shear rate. The data are given in terms of $\frac{\tau_{\text{steady state}} - \tau_{\text{peak}}}{\tau_{\text{peak}}}$ and for the analysis in this paper τ_{peak} is needed.
Koke and Modigell ^[27]	Searle (Physica UDS 200). Axial temperature difference kept within range 0.2-0.5 K (0.2-0.5 °C). Hot nitrogen atmosphere. Gap 4 mm with grooved inner cylinder.	Sn-14.2 wt pct Pb, 468 K (195 °C)-0.53, 471 K (198 °C)-0.48, 473 K (200 °C)-0.44. It is not clear whether the Joly Thesis curve ^[31] has also been used here. For their Fig. 18 isothermal flow curve, the conditions are Sn-15.8 pct Pb, T 471 K (198 °C), $f_s = 0.41$, and shear rate of 100 s ⁻¹ as the equilibrium shear rate	Particle size vs time is measured and a method is presented for correcting the rheology data for particle coarsening during the experiment. Micrographs in Fig. 7 suggest a significant degree of agglomeration over time (even after 1 h shearing). The particle size after 1 h shearing is ~550 μm and after 3 h ~600 μm (Fig. 8)	The temperature is lowered from liquid to the desired temperature while stirring. Fluid is stirred for 60 min at 100 s ⁻¹ and then the shear rate is dropped to 25 s ⁻¹ before step-wise changes up to 400 s ⁻¹ and then decreases to 100 s ⁻¹ . In the second set of experiments, after each shear rate jump, semisolid is sheared again at 100 s ⁻¹ to re-establish equilibrium before the next jump (in contrast to results in ^[28])	Variety of shear rate jumps. Max. shear rate 400 s ⁻¹	τ_{peak} is obtained by deducing $\tau_{\text{steady state}}$ using Peng and Wang's Eq. [2] and their parameters as in the text just below Eq. [2]
				The isostructural flow curve is then obtained as shown in Fig. 18, plotting the peak at the instant of the jump on the shear stress axis and the absolute value of the shear rate after the jump on the shear rate axis.		Inertia is dominant for 1 to 1.5 s after the jump so the first 60 to 100 values are disregarded. (Private communication ^[32]). Koke and Modigell conclude after a shear rate change an overshoot was observed that resulted from short-time shear-thickening behavior. In the first set of experiments (their Fig. 4), the particle diameter is ~600 μm (see their Fig. 8). This is relatively large in comparison with the gap size (4 mm) and consequently shear thickening could be likely via a 'particle bridging' effect. Continuous shearing over a long period of time shows some instabilities in the viscosity vs time curve, which Koke and Modigell attribute to 'blocking of huge agglomerates in the measuring gap.' They therefore limited their experiments to <180 min to avoid these instabilities. Their Fig. 18(b) is an isostructural curve which fits a Herschel-Bulkley model with a shear thickening exponent of 2.07 for a fraction solid of 0.41 i.e., $\tau = \tau_y + k\dot{\gamma}^n$ where $n = 2.07$.

Table I. continued

References	Rheometer	Material/Volume Fraction Solid	Particle Size; Morphology and Size Distribution	Time Scale of Transient, Data Acquisition Rate, Conditions	Shear Rate Jumps	Comments (Including How We Derive Our Data in Fig. 3 from the Data in the Literature)
						<p>To illustrate how they have obtained this figure, using Fig. 4 in Koke and Modigelli, focus on the curve for fraction solid 0.44 and the jump between 100 s^{-1} and 200 s^{-1} at 6300 s on the time axis. The peak stress at the instant of the jump is $\sim 300 \text{ Pa}$. This is then the value that would be plotted on the vertical axis in the equivalent of Fig. 18 (b) (which is only shown for a fraction solid of 0.41) with 200 s^{-1} as the absolute value of the shear rate at the end of the jump plotted on the horizontal axis. This procedure is repeated for a series of jumps to obtain the isostructural flow curve. It should be noted that the initial 'conditioning' shear rate (<i>i.e.</i>, the shear rate before the jump) should be the same for each jump so Fig. 4 cannot be used to obtain an overall equivalent of Fig. 18 (b) for each of the fractions solid other than 0.41.</p> <p>To obtain the points shown in the analysis in Fig. 3 in the current paper for Koke and Modigelli, the data have been taken directly from Fig. 18 (b) for the fraction solid 0.41</p>

Table I. continued

References	Rheometer	Material/Volume Fraction Solid	Particle Size, Morphology and Size Distribution	Time Scale of Transient, Data Acquisition Rate, Conditions	Shear Rate Jumps	Comments (Including How We Derive Our Data in Fig. 3 from the Data in the Literature)
Liu <i>et al.</i> ^[24]	Searle (Haake ME500). Temperature accuracy within 1 K (1 °C). Nitrogen or argon used to prevent oxidation. Gap 1.45 mm. Cup and bob grooved	Sn15 wt pct Pb. F_s 0.2, 0.36, 0.5	Figs. 9 and 10 suggest a typical size of $\sim 150 \mu\text{m}$ when at rest for f_s 0.36 and $\sim 210 \mu\text{m}$ for f_s 0.5. The average particle size grows considerably with standing time ($\sim 400 \mu\text{m}$ after 2 h for f_s of 0.5). There is some evidence of agglomeration although not quite as much as in Ref. 25 examining the number of particle-particle bonds	~ 100 ms. 1 kHz. Stirring occurs from the liquid state until the desired semisolid temperature is reached and continued until an apparent steady state is established. Some tests are carried out from rest and after standing at rest	Variety of jumps. Maximum shear rate 200 s^{-1}	Several sources of error are examined: (1) Effects of momentum diffusion through slurry; (2) Inertia effects of measuring head; (3) Electronic switching during the step change in shear rate. Calculation suggests that, in Sn15 wt pct Pb, momentum diffusion will be significantly faster than the jump time. The inertia effect of the measuring head is dealt with by carrying out a test in air and subtracting the resulting curve from the test result. (None of the other workers mentioned for inertia of the measuring head.) Electronic switching in the viscometer's controller is allowed for by only taking results after the shear rate has reached 90 pct of the specified final shear rate. On the effect of particle size. For accurate measurements the particle size must be less than 1/3 of the gap width. For the system here, it was found that the largest particle size measured is less than one third of the gap width. Liu in his thesis ^[24] has considered the inertia of the fluid by calculating the macroscopic Reynolds number. He obtains a value of 36 (which is roughly consistent with Kumar given different gap sizes). The experimental results were thought to show only shear thinning. For the current paper, the Liu <i>et al.</i> points in Fig. 3 have been obtained using their Table IV and assuming that to translate from 'Initial or Peak Stress Viscosity' to 'Peak Stress' involves multiplying the peak stress viscosity by the final shear rate at the end of the jump. The rest time data points are obtained from Table II multiplying the viscosity at the peak by the final shear rate to obtain the peak stress

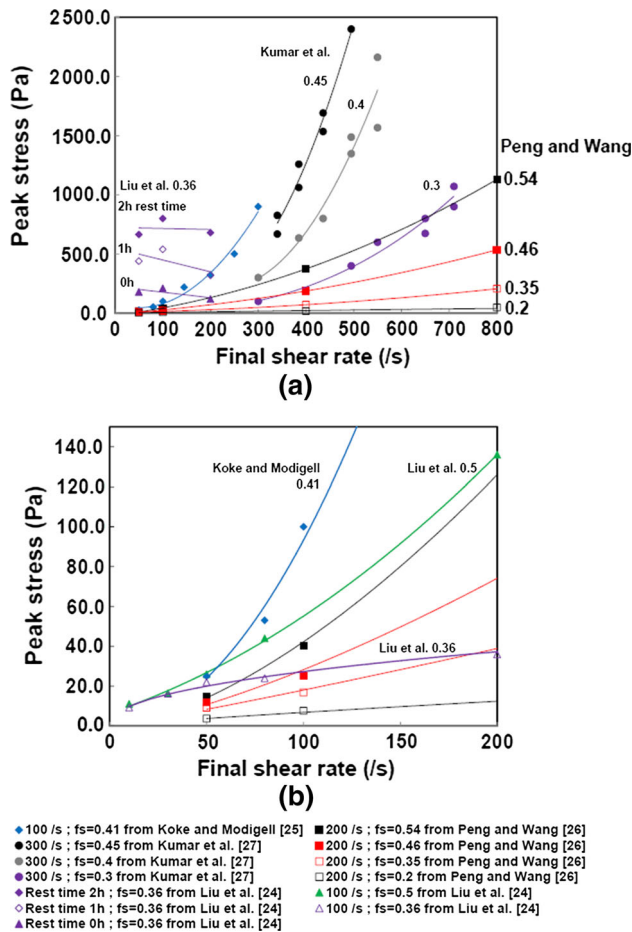


Fig. 3—Plot of the peak shear stress during a shear rate jump against the final shear rate after the jump. The shear rate in the legend is the initial, ‘conditioning’ shear rate. (b) is a magnified version of the bottom left hand corner of (a).

his thesis,^[32] looking at microscopic Reynolds number (*i.e.*, on the scale of the particle) and the Bagnold number. He concludes it is safe to ignore the inertial effects in the analysis and confirms this by carrying out shear rate transients at different rates and obtaining results which are essentially unchanged. There is no mention in the papers by Kumar *et al.*^[23,27] or the Kumar thesis^[32] of any consideration of the inertia of the measuring head, although the experiments with shear rate transients at varying rates suggest that this is not an issue. Peng and Wang^[26] consider that the peaks observed in their work are due to the inertia of the fluid but do not then correct for the effect. Koke and Modigell^[25] state ‘inertia effects were excluded from the data evaluation.’ A subsequent private communication from Modigell^[34] identifies that calculation and tests suggest that inertia may be dominant in tin-lead systems for 1 to 1.5 s. Since the sampling rate is 60 Hz, the first 60 to 100 values in the shear stress response were therefore disregarded for the evaluation of the ‘isostructure’ effect. The rheometer is the same type as in the experiments by Liu *et al.*^[24] (*i.e.*, Searle-type with a rotating bob and static cup), and the plot of shear stress against time in their Figure 7 suggests that the decay in the shear stress after the transient occurs in less than

about 0.2 s. In disregarding the first 1 to 1.5 s of values, the effect of any inertia from the measuring head will also have been dealt with, as the results of Liu *et al.*^[24] suggest that the peak due to this in air (their Figure 5) is dissipated well within 0.2 s. Liu *et al.*^[24] deal with inertia of the measuring head by carrying out an identical test in air to that with the semisolid fluid. A peak in shear stress, immediately after the transient in shear rate is initiated, suggests that inertia is occurring. This is corrected for subsequently, subtracting results for an experiment in air from those for the equivalent shear rate jump with the semisolid fluid. Liu, in his thesis,^[21] calculates the Reynolds number for the fluid moving in the gap and concludes that the inertia of the fluid is not an issue. Since inertia of the fluid will increase as the height of the shear rate jump increases, if inertia does exist, and is not corrected for, it will tend to increase the tendency for there to be apparently shear-thickening behavior. However, it can be concluded that inertia has been appropriately dealt with *via* the various approaches the experimentalists have applied in the literature.

D. Particle Size and Rheometer Gap Size

The particle size in Kumar *et al.*'s experiments is stated to be $\sim 150 \mu\text{m}$ but it is not clear either in the papers^[23,27] or in the original thesis by Kumar^[32] that there has been any check for coarsening during the experiments. The gap size is 3 mm (assumed to mean between the closest surfaces of the cup and the bob *i.e.*, not including the grooves). For Koke and Modigell,^[25] the gap size is 4 mm, and the paper itself is focussed on analyzing particle coarsening during shearing and correcting rheological data for the effects of that. At 198 K (fraction solid, $f_s \sim 0.41$), the particle size after 1 hour stirring at 100 s^{-1} (the ‘conditioning’ phase prior to the jump) is about $550 \mu\text{m}$. This is significant in relation to the gap size. They observe that, if they continuously shear over a long period of time, some instabilities occur in the viscosity *vs* time curve. They attribute these to ‘blocking of huge agglomerates in the measuring gap’ and therefore limit their experiments to shorter time periods where these instabilities are not observed. This is mentioned here because clearly Koke and Modigell have set out to ensure their rapid shear rate jump results are not interfered with by discontinuous shear rate thickening (the instabilities) but they have found it can occur intermittently even under steady-state conditions if the particles are large enough in relation to the gap size. Kumar *et al.*^[23,27] limit their volume fraction solid to 0.45 and less because, above 0.45, they observed large ‘spikes’ in torque which they attribute to the formation of particulate ‘bridges’ between the cup and the bob. The gap size is smallest in the experiments by Liu *et al.*,^[24] at 1.45 mm. Particle sizes are $\sim 150 \mu\text{m}$ prior to a shear rate jump for $f_s \sim 0.36$ and $\sim 210 \mu\text{m}$ for $f_s \sim 0.5$. Liu *et al.* argue that for accurate measurements the particle size must be less than 1/3 of the gap width and that their experiments satisfy this requirement. Their results in Figure 3(b) show that there is evidence of shear thickening for a fraction of solid of 0.5 (*i.e.*, the lines curve upwards) but not for the lower fraction of

solid of 0.36 (where the lines do not show such an upward trend), where the particle size is smaller. Fundamentally, there is an interrelationship between the particle size, the fraction solid, and the gap size with jamming more likely to occur with large particles at high fractions of solid in small gaps.

E. Yield Stress Masking Shear Thickening?

Figure 3 also shows the results for Liu *et al.*^[24] where the material has been allowed to rest before the jump. Liu *et al.*^[24] identify that there is a clear increase in peak stress with rest time prior to the jump and attribute this to the evolving degree of particle agglomeration. The longer the rest period in the semisolid state prior to semisolid processing, the greater the resistance to deagglomeration in the initial stages of flow. Brown *et al.*^[6] have argued that yield masks shear thickening. This is consistent with the argument in Alexandrou *et al.*^[18,19] about the existence of a yielded zone for low shear rates. However, the evidence suggests that where a conditioning shear rate has been applied (in this case 100 s^{-1} or above), such yielded zones are not relevant. They only influence the results for shear rate transients if the jump is from rest to a low shear rate with a relatively large gap size.

F. Rationalization

From these findings, three conclusions are identified in terms of what determines whether shear rate thickening is observed for the transient in shear rate:

- (1) Shear rate thickening is not observed if the fraction solid is ~ 0.36 or less;
- (2) Shear rate thickening is barely discernible if the final shear rate of the jump is in the region of 100 s^{-1} or less and then only if the fraction solid is above ~ 0.36 .
- (3) Shear rate thickening is not observed if the material has been at rest prior to the jump in shear rate because the yield phenomenon masks any shear thickening tendency;

This analysis can rationalize the apparently contradictory results from Kumar *et al.*,^[23,27] Peng and Wang,^[26] Koke and Modigell^[25], and Liu *et al.*^[24] The reanalysis shows that Liu *et al.*^[24] do have results (for a fraction solid of 0.5) which display shear thickening but only when the shear rate jump is occurring from a finite shear rate. If it takes place from rest then the yield stress masks any underlying behavior as discussed by Brown *et al.*^[6] where it is argued that yield can mask shear thickening. For the jumps from a finite shear rate for fractions solid of greater than about 0.36, an instantaneous shear thickening response is occurring (even if the steady-state behavior is shear thinning) almost certainly for the reasons identified by Brown and Jaeger^[12] *i.e.*, the confining stress at boundaries frustrating dilatation.

Figure 3 in Brown and Jaeger^[12] is very similar to Figure 3 in this paper when plotted using a log–log scale. This strengthens the argument for our conclusions

below. Also in Jiang *et al.*,^[35] a suspension of cornstarch was found to exhibit discontinuous shear thickening (such as that we have observed for semisolid metals) for a volume fraction above 0.34, which is close to the 0.36 value we have been referencing for semisolid metals. As mentioned by Brown and Jaeger,^[15] shear thickening starts to gradually appear at a packing fraction of typically around 0.3–0.4, and the slope on shear stress–shear rate curve increases with increasing volume fraction.^[15,35]

Jorstad *et al.*^[36] indicate that in thin sections, solid particles cannot migrate away from the deformation area, so solid–solid interactions increase, resulting in increase in viscosity and so the possibility to have laminar flow at very high velocities. The mechanisms described are very similar to those related to jamming and discontinuous shear thickening. From a practical point of view, shear thickening is therefore potentially relevant for thixoforming at high velocities because it might contribute to ensure laminar flow.

IV. CONCLUSIONS

There is contradictory evidence in the literature as to whether the behavior during transitions in shear rate for semisolid metals with non-dendritic (*i.e.*, spheroidal) microstructures is shear thinning or shear thickening. Here the data in the literature have been systematically reanalyzed to rationalize the apparent contradictions. It is argued that if the suspension is disagglomerated before the shear rate jump (*i.e.*, it has been initially sheared rather than the jump being from rest), the instantaneous behavior with a jump-up in shear rate is shear thickening (even if the long-term steady-state behavior is shear thinning) provided the fraction solid is greater than about 0.36 and the final shear rate at the end of the jump is greater than about 100 s^{-1} . If the jump-up in shear rate is made from rest then yield masks the shear thickening.

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REFERENCES

1. H.V. Atkinson: *Prog. Mater. Sci.*, 2005, vol. 50, pp. 341–412.
2. D.B. Spencer, R. Mehrabian, and M.C. Flemings: *Metall. Trans.*, 1972, vol. 3, pp. 1925–32.
3. M.C. Flemings: *Metall. Trans. A*, 1991, vol. 22A, pp. 957–81.
4. V. Favier and H.V. Atkinson: *Acta Mater.*, 2011, vol. 59, pp. 1271–80.
5. H.A. Barnes: *J. Rheol.*, 1989, vol. 33, pp. 329–66.
6. E. Brown, N.A. Forman, C.S. Orellana, H. Zhang, B.W. Maynor, D.E. Betts, J.M. DeSimone, and H.M. Jaeger: *Nat. Mater. Lett.*, 2010, vol. 9, pp. 220–24.
7. J.F. Brady and G. Bossis: *J. Fluid Mech.*, 1985, vol. 155, pp. 105–29.
8. B.J. Maranzano and N.J. Wagner: *J. Chem. Phys.*, 2001, vol. 114, pp. 10514–527.
9. R.L. Hoffmann: *Adv. Colloid Interface Sci.*, 1982, vol. 17, pp. 161–84.
10. D. Lootens, H. van Damme, Y. Hémar, and P. Hébraud: *Phys. Rev. Lett.*, 2005, vol. 95, Article No. 268302.
11. A. Fall, N. Huang, F. Bertrand, G. Ovarlez, and D. Bonn: *Phys. Rev. Lett.*, 2008, vol. 100, Article No. 018301.
12. E. Brown and H.M. Jaeger: *Science*, 2011, vol. 333, pp. 1230–31.
13. E. Brown and H.M. Jaeger: *J. Rheol.*, 2012, vol. 56, pp. 875–923.
14. V. Favier, P. Cezard, and R. Bigot: *Mater. Sci. Eng., A*, 2009, vol. 517, pp. 8–16.
15. E. Brown and H.M. Jaeger: *Rep. Prog. Phys.*, 2014, vol. 77, Article No. 046602.
16. P.C.F. Möller, J. Mewis, and D. Bonn: *Soft Matter*, 2006, vol. 2, pp. 274–83.
17. A.R.A. McLelland, N.G. Henderson, H.V. Atkinson, and D.H. Kirkwood: *Mater. Sci. Eng., A*, 1997, vol. A232, pp. 110–18.
18. A.N. Alexandrou and G. Georgiou: *J. Non-Newton. Fluid Mech.*, 2007, vol. 142, pp. 199–206.
19. A.N. Alexandrou, N. Constantinou, and G. Georgiou: *J. Non-Newton. Fluid Mech.*, 2009, vol. 158, pp. 6–17.
20. C.M. Gourlay and A.K. Dahle: *Nature*, 2007, vol. 445, pp. 70–73.
21. T.Y. Liu: PhD Thesis, University of Sheffield, 2002.
22. C.J. Quak: PhD Thesis, Technische Universiteit Delft, 1996, ISBN 90-5651-019-3.
23. P. Kumar, C.L. Martin, and S. Brown: *Metall. Trans. A*, 1993, vol. 24A, pp. 1107–16.
24. T.Y. Liu, H.V. Atkinson, P.J. Ward, and D.H. Kirkwood: *Metall. Mater. Trans. A*, 2003, vol. 34A, pp. 409–17.
25. J. Koke and M. Modigell: *J. Non-Newton. Fluid Mech.*, 2003, vol. 112, pp. 141–60.
26. H. Peng and K.K. Wang: in *Proc. 4th Int. Conf. on Semi-Solid Processing of Alloys and Composites*, D.H. Kirkwood and P. Kapranos, eds., Publ. University of Sheffield, Sheffield, UK, June 1996, pp. 2–9.
27. P. Kumar, C.L. Martin, and S. Brown: *Acta Metall. Mater.*, 1994, vol. 42, pp. 3595–602 and 3603–14.
28. M. Modigell, J. Koke, and J. Petera: in *Proc. 5th Int. Conf. on Semi-solid Processing of Alloys and Composites*, A.K. Bhasin, J.J. Moore, K.P. Young, and S. Midson, eds., Publ. Colorado School of Mines, Golden, Colorado, USA, June 1998, pp. 317–326.
29. G.R. Burgos, A.N. Alexandrou, and V. Entov: *J. Mater. Process. Technol.*, 2001, vol. 110, pp. 164–76.
30. H.V. Atkinson and P.J. Ward: *JOM*, 2006, vol. 8, pp. 21–23.
31. P.A. Joly: PhD Thesis, Massachusetts Institute of Technology, Cambridge, MA, 1974.
32. P. Kumar: PhD Thesis, Massachusetts Institute of Technology, Cambridge, MA, 1994.
33. L.S. Turng and K.K. Wang: *J. Mater. Sci.*, 1991, vol. 26, pp. 2173–83.
34. M. Modigell: AVT at RWTH Aachen University, Germany, and German University of Technology in Oman (GUTech), Private Communication, July 2011.
35. W. Jiang, S. Xuan, and X. Gong: *Appl. Phys. Lett.*, 2015, vol. 106, Article number 151902.
36. J.L. Jorstad, A.N. Alexandrou, and E. Mitsoulis: *Solid State Phenom.*, 2015, vols. 217–218, pp. 159–65.