RESEARCH ARTICLE

Ni‑Zn/CeO2 nanocomposites for enhanced adsorptive removal of 4‑chlorophenol

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Abstract

Chlorophenols are one of the major organic pollutants responsible for the contamination of water bodies. This study explores the application of Ni-Zn/CeO₂ nanocomposites, synthesized via the aqueous co-precipitation method, as effective adsorbents for the 4-chlorophenol removal from aqueous solutions. The nanocomposites' chemical and structural characteristics were assessed using diferent physical characterization methods, viz. X-ray difraction, transmission electron microscopy, Fourier transform infrared spectroscopy, zeta potential, using a Box-Behnken design within response surface methodology, optimal conditions of pH 3, temperature 20 °C, contact time 120 min, adsorbent dosage 0.05 g, and 4-chlorophenol concentration 50 ppm are identifed. Among the nanocomposites tested, NZC 20:10:70, with 20% Ni and 10% Zn, achieves enhanced performance, removing 99.1% of 4-chlorophenol within 2 h. Adsorption kinetics follow the pseudo-second-order model and equilibrium data ft the Freundlich isotherm. Thermodynamic analysis indicates an exothermic and spontaneous process. The adsorption capacity of NZC 20:10:70 shows significant enhancement, growing from 19.85 mg/g at 10 ppm to 96.33 mg/g at 50 ppm initial concentration. Physical characterization confrms NZC 20:10:70's superior properties, including a high surface area of 118.471 m²/g. Evaluating economic viability, NZC 20:10:70 demonstrates robust reusability, retaining 85% efficiency over eight regeneration cycles. These results highlight NZC 20:10:70 as a promising adsorbent for effective and sustainable chlorophenol removal in water treatment.

Keywords Adsorption · Ni-Zn/CeO₂ · Nanocomposite · Response surface methodology · Freundlich · 4-Chlorophenol

Introduction

The rapid surge in environmental pollution can be primarily attributed to the process of industrialization (Lu et al. [2019\)](#page-17-0). It has resulted in increased production and use of toxic chemicals leading to ecological imbalance. The phenols, especially chlorophenols, used in insecticides, augment the severity of the problem by their toxicity (Mishra et al. [2023](#page-18-0); Azizi et al. [2021](#page-16-0)). The organic pollutants present in

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industrial wastewater are difficult to remove by conventional treatment.

Chlorophenols, classifed as endocrine-disrupting compounds in the phenolic category, are highly toxic and have carcinogenic effects (Hamidon et al. [2022](#page-17-1)). Phenolic pollutants are contaminating the environment, raising a threat to human as well as ecosystem health (Ki et al. [2017](#page-17-2)). Studies have indicated that prolonged consumption of water contaminated with chlorophenols can lead to serious health issues, including but not limited to anaemia and dizziness (Allaboun and Al-Rub [2016](#page-16-1)). Furthermore, it has the potential to impact critical bodily systems, such as the central nervous system and the liver (Varsha et al. [2022\)](#page-18-1).

Chlorophenols are widely used in various industries, serving as essential components in the production of pharmaceuticals, dyes, lubricants, preservatives, pesticides, fungicides, and herbicides (Yadav et al. [2023](#page-18-2)). The chlorophenols can enter water bodies from various sources, such as industrial waste, pesticide use, and from disintegration of chlorinated hydrocarbons (Zhao et al. [2022](#page-19-0)). Chlorophenols

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are a consequential byproduct of the chlorination process, which is commonly utilized to treat wastewater for sanitation purposes. However, the unintended formation of these by-products causes contamination of soil, groundwater, and surface water (Lu et al. [2019\)](#page-17-0). 4-Chlorophenol is the most toxic of the mono-chlorophenols and can be easily absorbed by humans. Its widespread presence in wastewater and high toxicity makes it urgent to develop methods for its removal from aqueous solutions (Gao et al. [2021](#page-17-3)).

Diferent approaches employed for the 4-chlorophenol removal from its aqueous solution include removal through membrane separation (Goel et al. [2010\)](#page-17-4), biological degradation (Gómez et al. [2012\)](#page-17-5), solvent extraction [Adeyemi et al. [2020\)](#page-16-2), and adsorption, catalytic oxidation (Wang et al. [2022](#page-18-3)). However, these methods have their own limitations. Adsorption stands out as the appropriate method for pollutant removal due to its simplicity in operation, exceptional efectiveness, cost-efectiveness, and the wide array of available adsorbents [Rahman and Ahmad [2023\)](#page-18-4).

Recent advancements in environmental remediation have highlighted the effectiveness of various nanocomposite materials for treating wastewater contaminated with phenolic compounds and their derivatives. These include the use of sulphur-doped activated carbon for catalytic oxidation of phenolic compounds (Guo et al. 2017), $ZrO₂/$ LDH under UV light for photocatalytic removal of phenols (Melchor-Lagar et al. [2020\)](#page-18-5), layered double hydroxides/ single-walled carbon nanotubes for both phenol and 4-chlo-rophenol (Zhang et al. [2019\)](#page-18-6), magnetic $Fe₃O₄/\text{activated}$ carbon for combined adsorption and Fenton oxidation of phenolic compounds (Duan et al. [2020\)](#page-17-7), porous and ultrafne nitrogen-doped carbon nanofbers from bacterial cellulose [Gao et al. [2021\)](#page-17-3), and even biodegradation methods using isolated *Bacillus subtilis* for chlorophenol removal [Patel et al. [2022](#page-18-7)). Bayramoglu and Arica [\(2023\)](#page-17-8) demonstrated the use of Lentinus sajor-caju immobilized in stable Caalginate beads for efficient phenol and derivative degradation. Further advancements include Doyo et al.'s ([2023\)](#page-17-9) Polyaniline@Waste Cellulosic nanocomposites for phenol decontamination and Jagaba et al.'s ([2023](#page-17-10)) biochar-based geopolymer nanocomposites, demonstrating phenol removal efficiencies of 61.94% and 74.44% for BEAS and GEAS bioreactors, respectively. Kumar et al. [\(2023](#page-17-11)) developed a cellulose/graphene-oxide composite, capable of removing 86% of phenol within 40 min, highlighting its rapid and efficient wastewater treatment potential. Several nanomaterials have further been investigated for their adsorptive efficiency towards a variety of phenolic and other organic pollutants including graphene oxide-bentonite nanocomposites (Ayoob et al. [2024](#page-16-3)), GO/bentonite/MgFeAl-LTH nanocomposite (Bahadi et al. [2024\)](#page-16-4), bio-derived carbon-based nanocomposites (DP-IO) (Ajmi et al. [2024\)](#page-16-5), and montmorillonite- $Fe₃O₄$ -humic acid (MFH) nanocomposites (Rodrigues et al. [2024](#page-18-8)). The recent literature review reveals that the mixedmetal oxide nanocomposite involving rare earth metals has been under-explored for their adsorption efficiency towards 4-chlorophenol and other organic pollutants.

Previous studies have predominantly explored catalytic oxidation, photocatalytic degradation, biodegradation, and combined adsorption with oxidation processes using materials like activated carbon, metal oxides, and biocatalysts for removing 4-chlorophenol (4-CP) from aqueous solutions, with limited focus on adsorption studies. In this study, we explore and develop mixed-metal oxide nanocomposites containing rare earth metals for the efficient adsorption of 4-chlorophenol. Unlike conventional approaches using organic or graphene-based materials, this study focuses on leveraging the unique properties of rare earth metals within nanocomposites. The adsorption efficiency of Ni-Zn/CeO₂ nanomaterials (with three diferent compositions) has been investigated for the removal of 4-chlorophenol. The efects of optimization factors like pH, time, temperature, quantity of adsorbent dose, and concentration of 4-chlorophenol on the adsorption process were investigated using response surface methodology (RSM) and a Box-Behnken design (BBD). Also, the kinetic as well as thermodynamic studies of the adsorption process have been undertaken to deduce the infuence of experimental parameters on the adsorption ability of the nanocomposites.

Experimental

Materials

Nickel sulphate $(NiSO₄)$ (99% purity), cerium nitrate hexahydrate (Ce(NO₃)₃·6H₂O) 99%, zinc sulphate (ZnSO₄) 99%, 4-chlorophenol (Cl-C₆H₄OH) 99.9%, and cetyltrimethylammonium bromide (CTAB) 99% were of analytical grade and acquired from Sigma-Aldrich and were used as obtained. Throughout the study, deionized water was used for all purposes.

Synthesis route of Ni-Zn/CeO₂ nanocomposites

Three distinct compositions of Ni-Zn/CeO₂ nanocomposites were synthesized by the aqueous coprecipitation method (Semwal et al. [2023](#page-18-9)). According to the weight percentage of Ni, Zn, and Ce precursors, these three compositions have been named NZC 10:20:70 (means precursors of Ni/Zn/ Ce are in the ratio of 10:20:70), NZC 15:15:70, and NZC 20:10:70. The schematic synthesis of Ni-Zn/CeO₂ nanocomposites is illustrated in Fig. [1](#page-2-0) The aqueous solutions of $Niso_4$ and $ZnSO_4$ with a specific amount for each nanocomposite are prepared separately. Then, 100 mL of each of these solutions were then mixed to create a unifed metal **Fig. 1** Diagrammatic representation of the synthesis process of Ni-Zn/CeO₂ nanocomposites

precursor solution. While maintaining a temperature of 60 °C and stirring at 500 rpm, a cerium nitrate hexahydrate (70 wt%, 100 ml) solution was dropwise added and stirred for 30 min. This ensured thorough mixing and reaction between the cerium nitrate and Ni and Zn metal precursors. Subsequently, a solution of the CTAB (3.46 gm in 100 ml), which acts as a capping agent, was introduced drop by drop. Thereafter, the resultant mixture pH was brought to 10 by the addition of 1 M NaOH. After completing the reaction, the precipitate was collected through fltration, and extensive washing with deionized water was performed to remove unreacted metal precursors and other contaminants. The removal was ensured by testing the ions in the fltrate. The further process involved repeated washes with ethanol. The washed precipitate was then dried for 2 h at 80 $^{\circ}$ C in an oven. Subsequently, the dried material was further annealed in a high-temperature tube furnace at 400 °C for 4 h with a ramping rate of 5° C min⁻¹ to enhance its crystallinity and eliminate any remaining organic components. Finally, the material was fnely grounded and stored for further use.

Characterization

The determination of crystal structure was facilitated by X-ray diffraction (XRD), which was carried out with a Bruker D8-Advance P-X-ray difractometer that was operated at 40 mA and 30 kV utilizing Cu-Kα radiation. Crystal structure determination involved collecting difraction data throughout a 2θ range of 10°–90°.

Gas sorption analysis was determined by the Quantachrome® ASiQwin™-Automated Gas Sorption instrument, which provides valuable insights into the surface area and size of pores. Fourier transform infrared (FT-IR) analysis, was performed using the PerkinElmer Spectrum instrument. Scanning electron microscopy (SEM) with the Carl Zeiss Model Supra 55 instrument allowed for the visualization of surface morphology at high resolution. The thermogravimetric analysis (TGA) was performed using PerkinElmer and provided information on the thermal stability of the nanocomposites. Transmission electron microscopy (TEM) was analysed using the JEOL JEM 2100 PLUS which ofered detailed images and structural information at the nanoscale. Zeta potential measurement was performed using Anton Paar zeta potential analyser.

Experimental framework

A comprehensive investigation was performed on the impact of four key adsorption parameters on the adsorptive removal of 4-chlorophenol by NZC nanocomposites using a Box-Behnken design (BBD) under response surface methodology (RSM) approach with ANOVA. The result of BBD models involves a graphical analysis. This analysis includes examining the distribution of residuals and comparing the actual removal values with the predicted values for the elimination of 4-chlorophenol using the NZC 20:10:70 nanocomposite (as it shows excellent adsorptive removal among three nanocomposites), whereas analysis of variance (ANOVA) is a statistical technique applied to assess the validity of the applied models for 4-chlorophenol removal and evaluate the signifcance of the data associated with this removal process. The Stat-Ease Design Expert software was employed to design and analyse adsorption experiments as well as statistically evaluate the data. The levels and coded values of the independent parameters are represented in Table [1](#page-3-0).

Table 1 Code, actual variables, and corresponding levels in BBD

Variable	Low	High
pН	2	10
Contact time (min)	10	120
Adsorbent dose (g/L)	0.01	0.05
Temperature $(^{\circ}C)$	10	60

To investigate the adsorption isotherm, 0.05 g/L of adsorbent was in contact with 100 mL of 4-chlorophenol solutions at various concentrations at pH 3.0. This contact was maintained for 2 h with constant agitation at room temperature. The contact time study revealed that after 2 h, the equilibrium was reached, and calculating the difference between the two concentration levels yielded the amount of 4 chlorophenol absorbed (in %) on the adsorbent's surface. The efficiency of adsorption depicted as adsorption efficiency of adsorbent towards 4-chlorophenol is determined by applying Eq. [1](#page-3-1) (Semwal et al. [2023\)](#page-18-9):

adsorption efficiency =
$$
\frac{(C_o - C_e)}{C_o} \times 100
$$
 (1)

where C_0 denotes the initial concentration of the 4-chlorophenol solution (mg/L) and *Ce* represents the fnal concentration of 4-chlorophenol in the sampled aliquot (mg/L).

The adsorbent was extracted from the reaction mixture using a standardized leaching procedure. The procedure required multiple washing using organic solvents, deionized water, and sodium hydroxide (NaOH), and then drying for two hours at 100 °C in a hot air oven. To evaluate the adsorbents' recyclability ability subsequent adsorption assays were also undertaken (*vide infra)*.

Adsorption isotherm

An isotherm provides insights into the quantity of adsorbent that adheres to the surface per unit mass of the adsorbate at a specifc temperature (Lan et al. [2022\)](#page-17-12). Adsorption capacity at equilibrium is expressed by q_e , whereas the concentration of adsorbate in the liquid phase is denoted by *Ce*. To explain the isotherm curve, three distinct isotherm models were used, namely the Langmuir, Freundlich, and Temkin isotherm models.

The Langmuir model can be presented in linear form by Eq. [2](#page-3-2) (Langmuir [1918\)](#page-17-13):

$$
\frac{C_e}{q_e} = \frac{1}{q_m K_L} + \frac{C_e}{q_m} \tag{2}
$$

$$
q_e = \left(\frac{C_o - C_e}{m}\right) * V \tag{3}
$$

The symbol C_e represents the 4-chlorophenol concentration at equilibrium (mg/L), q_e (calculated by Eq. [3](#page-3-3) (Arica et al. [2022](#page-16-6))) stands for the quantity of 4-chlorophenol adsorbed (mg/g), and q_m signifies the adsorption capacity measured in mg/g, whereas the Langmuir constant is denoted as K_L , and it depends on the material's porosity and surface area, C_0 represents the initial 4-CP Concentration, *V* is the volume of the solution (L), and *m* is the mass of adsorbent in gm.

The Freundlich isotherm is expressed as Eq. [4](#page-3-4) (Freundlich and Heller [1939\)](#page-17-14):

$$
\log q_e = \log K_F + \frac{1}{n} \log C_e \tag{4}
$$

where K_F represents the adsorption capacity (L/mg) and $1/n$ represents the adsorption intensity.

The Temkin isotherm model postulates a linear decrease in adsorption heat for all layers as surface coverage increases, accounting for the infuence of indirect interaction of adsorbent-adsorbate (Ayawei et al. [2017](#page-16-7)).

The Temkin Isotherm is expressed in Eq. [5](#page-3-5) (Emmett and Kummer [1943\)](#page-17-15)]:

$$
q_e = \frac{RT}{b_T} \ln A_T + \frac{RT}{b_T} \ln C_e \tag{5}
$$

where b_T represents Temkin heat of adsorption constant $(L.mg^{-1})$, R represents gas constant, and A_T represents equilibrium binding constant.

Thermodynamics studies

The thermodynamic parameters such as Gibbs free energy change (ΔG°), entropy change (ΔS°), and enthalpy change (∆H°), of the process of adsorption of 4-chlorophenol onto $Ni-Zn/CeO₂$ nanomaterials were also determined by carrying out the thermodynamic studies. The experiments were conducted at temperatures ranging from 10 to 60 °C (283–333 K). and ΔG^0 is calculated by Eq. [6](#page-3-6) (Tran et al. [2021](#page-18-10)):

$$
\Delta G^{\circ} = -RT \ln K \tag{6}
$$

where K_{ads} is equilibrium adsorption constant and it is calculated in Eq. [7](#page-3-7):

$$
K_{ads} = \frac{q_e}{C_e} \tag{7}
$$

where q_e (mg/g) represents the equilibrium adsorption capacity and Ce (mg/g) is the equilibrium concentration of the pollutant in the solution.

 ΔH° and ΔS° were calculated by plotting ln K_{ads} vs 1/T and applying Van't Hoff's Eq. [8](#page-4-0) (Al-Ghouti and Al-Absi [2020\)](#page-16-8):

$$
\ln K_{ads} = \frac{\Delta S^o}{R} - \frac{\Delta H^o}{T} \left(\frac{1}{T}\right) \tag{8}
$$

where ΔS^{o} is the standard entropy change.

Kinetic studies

The kinetics of adsorption gauges the speed at which adsorption of 4-chlorophenol occurs on the Ni-Zn/CeO₂ nanocomposite. In our experiments, the data underwent analysis utilizing both the pseudo-frst and pseudo-second order rate equations to examine the adsorption process and ascertain the step controlling the rate. Equation [9](#page-4-1) (Lagergren [1898\)](#page-17-16) illustrates the pseudo-frst-order model as follows:

$$
q_t = q_e \left(1 - e^{-k_1 t} \right) \tag{9}
$$

Here, q_e signifies the equilibrium capacity measured in milligrams per gram (mg/g) , q_t represents the adsorption capacity at time t in mg/g, and K_1 (in min⁻¹) denotes the rate constant for the pseudo-first-order reaction. The pseudo-second-order model is articulated through Eq. [10](#page-4-2) (Ho and McKay [1999\)](#page-17-17):

$$
q_t = \frac{q_e^2 k_2 t}{1 + q_e k_2 t}
$$
\n(10)

where K_2 denotes the pseudo-second-order rate constant.

 q_t which represents the adsorption capacity at time t is calculated by Eq. [11](#page-4-3) (Arica et al. [2022\)](#page-16-6):

$$
q_t = \left(\frac{C_o - C_t}{m}\right) * V \tag{11}
$$

Fig. 2 XRD characteristics of NZC nanocomposite **a** NZC 10:20:70, **b** NZC 15:15:70, and **c** 20:10:70

where C_0 is the initial concentration of the adsorbate in the solution (mg/L), C_t is the concentration of the adsorbate in the solution at time t (mg/L) , V is the volume of the solution (L), and m is the mass of the adsorbent (g).

Result and discussion

Powder X‑ray difraction analysis

XRD patterns of the three synthesized nanomaterials are shown in Fig. [2a](#page-4-4)–c. XRD spectrum of NZC 15:15:70 (Fig. [2b](#page-4-4)) has only the standard peaks of $CeO₂$ at 2 θ values 28.5, 33.9, 47.8, 56.2, 58.5, and 69.10 corresponding to (111), (200), (220), (311), (222), and (400) lattice planes, respectively (Ramasamy et al. [2018](#page-18-11)). There are no peaks related to Ni/ NiO or Zn/ZnO. It reveals the formation of a solid solution where Zn and Ni are incorporated in the lattice of $CeO₂$ preferably by replacing the Ce ions. The shifting of the peaks towards the right to the standard values further supports the doping of Ni and Zn to the $CeO₂$, leading to the formation of bimetal doped cerium oxide nanoparticles at this composition.

Whereas XRD of NZC 10:20:70 (Fig. [2](#page-4-4)a) has two characteristic peaks of Zn at 2θ values 36.4° and 43.28° along with the standard peaks of $CeO₂$ mentioned in the previous paragraph (Qasim et al. [2016\)](#page-18-12), but this material has no peaks for Ni/ NiO, further revealing that Ni ions which are in smaller ratios get incorporated into the $CeO₂$ lattice. However, the element with a higher ratio (Zn in this case) is expressed as a diferent phase leading to the formation of a multiphase nanocomposite that has $CeO₂$ along with Zn. The XRD of NZC [2](#page-4-4)0:10:70 (Fig. 2c) also reveals the same trend. It has Ni elements in higher ratios. The XRD has two characteristic

peaks of Ni at 44.53° and 52.26° along with the standard peaks of $CeO₂$ but no peak for Zn (Al-Thabaiti et al. [2019](#page-16-9)).

Overall, the XRDs confrm that when Ni and Zn are mixed with $CeO₂$, there is a threshold ratio until which the elements are incorporated into the lattice of the $CeO₂$ which is 15:15:70. There is a formation of bimetal doped $CeO₂$ nanoparticles until this ratio of doping. But once the element crosses this limit, it is no longer incorporated into the lattice and forms a diferent phase leading to the formation of nanocomposite. Similar facts have been reported in literature where mixing to a certain extent forms doped nanomaterial and mixing beyond this extent leads to the formation of nanocomposites (Saravanan et al. [2013](#page-18-13); Wang et al. [2014](#page-18-14)).

In a nutshell, NZC 15:15:70 is a bimetal doped $CeO₂$ nanoparticle, whereas NZC 10:20:70 and NZC 20:10:70 is a nanocomposite with two phases.

The Debye-Scherrer formula (Eq. [12](#page-5-0) (Basak et al. [2022](#page-17-18))) is utilized to determine the crystallite size of the synthesized NZC nanocomposites (NCs):

$$
crystallite size (\phi) = \frac{0.94\lambda}{\beta \cos\theta}
$$
 (12)

where the symbol β denotes the full-width at half-maximum (FWHM) of the X-ray difraction (XRD) peak with the highest intensity and θ represents the corresponding Bragg diffraction angle. The X-ray source employed had a wavelength

of 0.1504 nm. The shape factor, known as the constant, was established at 0.94. The average crystallite size was found to be 5.09 ± 0.60 nm for NZC 10:20:70, 5.34 ± 0.60 nm for NZC 15:15:70, and 5.28±0.92 nm for NZC 20:10:70. So bimetal-doped nanoparticles have bigger crystallite size than the nanocomposites.

FT‑IR analysis

All three nanomaterials were subjected to the FT-IR analysis before the adsorption process and after the adsorption experiments. The FT-IR graphs for each case are given in Fig. [3](#page-5-1)a–f.

Among the synthesized nanomaterials, NZC 20:10:70 shows the highest adsorptive removal capacity toward 4-chlorophenol. Its FT-IR spectra before adsorption have the Zn-O vibrations at 495.38 and 598.99 cm⁻¹ (Murali et al. [2017](#page-18-15)), C–O stretching (1104.32 cm⁻¹) (Nurfani et al. [2020](#page-18-16)), O–H deformation $(1636.43 \text{ cm}^{-1})$ (Bai et al. [2014](#page-16-10)), and axial O–H stretching $(3243.21 \text{ cm}^{-1})$ (Da Silva et al. 2019), while post-adsorption, new peaks emerge at 1046.09 cm^{-1} (C–OH stretching) (Zhang et al. [2022](#page-18-17)), 1515.31 cm⁻¹ (C = C stretching) (Pancholi et al. 2022), and 3310.80 cm⁻¹ (-O–H bond absorption) (Shi et al. [2022\)](#page-18-19), elucidating molecular changes on the catalyst surface. The other two compositions also have diferent pre- and post-adsorption peaks in IR spectra which have been tabulated in Table [2](#page-6-0).

Fig. 3 FT-IR of NZC nanocomposite before and after adsorption (**a**), (**b**) NZC 10:20:70 (**c**), (**d**) NZC 15:15:70 (**e**), **(f**) NZC 20:10:70 (pH = 3, 4-CP concentration = 50 ppm, adsorbent dose = 0.05 g, contact time = 0 min and 120 min, T = 20 °C, volume of solution = 100 ml)

Nanocomposites	Peak at (before adsorption) (cm^{-1})	Functional groups (before adsorption)	Reference	adsorption) (cm^{-1})	Peak at (after Functional groups) (after adsorption)	References
NZC 10:20:70 Fig. $3a-b$	599.09	$Zn-O$	(Murali et al. 2017)	1109.18	C-O stretching vibrations	(Nurfani et al. 2020)
	1107.23	C-O stretching Vibrations	(Nurfani et al. 2020)	1484.23	vibration of the benzene ring	(Arya et al. 2023)
	1635.18	$C=O$ stretching vibration	(Zhang et al. 2022)	3368.52	OH-Bond	(Shi et al. 2022)
	3305.48	strong absorption band of -O-H bond	(Shi et al. 2022)			
NZC 15:15:70 Fig. $3c-d$	1114.89	symmetric C-O-C stretching	(Arya et al. 2023)	499.87	$Zn-O$	(Murali et al. 2017)
	3215.09	strong O-H stretch- ing,	(Da Silva et al. 2019)	1206.23	Asymmetric C=O	(Balakrishnan et al. 2022)
				115037	Aromatic ring	(Al Lafi and Hay 2019)
				1484.24	vibration of the benzene ring	(Arya et al. 2023)
				3339.62	strong absorption band of -O-H bond	(Shi et al. 2022)

Table 2 FT-IR analysis for Ni-Zn/CeO₂ nanocomposites

SEM analysis

The SEM images as shown in Fig. [4](#page-6-1) of the Ni-Zn/CeO₂ nanomaterials (NZC 20:10:70) shows mixed distribution of nanoparticles, where some regions exhibit densely clustered aggregates while others showcase more dispersed individual nanoparticles.

The aggregations are predominantly comprised of $CeO₂$ nanoparticles, closely amalgamated with Zn and Ni nanoparticles (Manibalan et al. [2021\)](#page-18-20). The minuscule size and consistent dispersion of the nanoparticles can be attributed to the stabilizing agent used during the synthesis process.

Fig. 4 SEM images of Ni-Zn/ CeO₂ nanocomposites (NZC 20:10:70) **a** at 500 nm, **b** at 3 μm, **c** at 5 μm, and **d** EDAX analysis

TEM analysis

Transmission electron microscopy (TEM) analysis of assynthesized Ni-Zn/CeO₂ nanomaterials (Fig. 5) indicates the average grain size for Ni-Zn/CeO₂ nanoparticles of 4.5 \pm 1.0 nm. The high-resolution TEM image in Fig. [5](#page-7-0)b reveals lattice stripes of 0.528 nm and 1.08 nm of Ni-Zn/CeO₂ nanoparticles, corresponding to the (XYZ) and (XXZ) planes of $CeO₂$, respectively. The selected area electron diffraction (SAED) (Fig. [5](#page-7-0)c) demonstrates the difraction rings assigned

> **2.1 2.4 2.7 3.0 3.3 3.6 3.9 4.2 4.5 4.8 5.1 5.4 Average Particle Size (nm)**

to the orthorhombic phase of $CeO₂$, in agreement with the XRD analysis. The STEM and energy dispersive X-ray (EDX) elemental mapping (Fig. [5](#page-7-0)d) of this sample shows the presence and uniform distribution of Ce, Zn, Ni, and O.

BET analysis

The nitrogen adsorption/desorption isotherms were employed for the determination of the pore structure and surface area of all the synthesized Ni-Zn/Ce O_2 nanomaterials.

Fig. 5 TEM images at **a** NZC 20:10:70 (20 nm), **b** NZC 20:10:70 (10 nm), **c** SAED pattern of NZC 20:10:70, **d** EDS mapping pattern of NZC 20:10:70 nanocomposite and particles size distribution curve, **e** NZC 20:10:70 at 20 nm, **f** NZC 20:10:70 at 10 nm

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Average Particle Size (nm)

As depicted in Fig. [6,](#page-8-0) the N2 physisorption isotherm displayed Type IV behaviour as classified by the IUPAC standards indicating the presence of mesopores within the $Ni-Zn/CeO₂$ nanocomposite (Villarroel-Rocha et al. [2021\)](#page-18-21) (Schlumberger and Thommes [2021](#page-18-22)). The textural characteristics of the synthesized nanomaterials are provided in Table [3.](#page-8-1) As it is evident, the mean pore diameter of all nanocomposites fell within the range typical of mesoporous materials. The results indicate that the surface area of the Ni-Zn/CeO₂ nanocomposites with compositions of $20:10:70$ exhibited the highest surface area of $118.471 \text{ m}^2/\text{g}$, respectively. The NZC 20:10:70 potentially promotes the formation of a more porous structure or enhances surface roughness, leading to increased surface area. Additionally, the larger pore diameter observed (6.448 nm) in NZC 20:10:70 suggests a more open pore structure, which contributes to its higher total pore volume (0.256 cc/g) (Liu et al. [2019\)](#page-17-21).

The mesoporous structure of these nanomaterials is expected to play a critical role in boosting the adsorption of 4-chlorophenol molecules on their surface (*vide infra*). This is primarily due to the mesoporous structure's ability to facilitate the fast difusion of 4-chlorophenol molecules through the adsorbent, thus improving the overall adsorption efficiency.

TGA analysis

Thermogravimetric analysis (TGA) was used to explore the carbonation temperature, decomposition kinetics, and thermal stability of Ni-Zn/CeO₂ nanomaterials. As illustrated in Fig. [7](#page-8-2)a, the TGA fndings for all compositions of Ni-Zn/ $CeO₂$ nanocomposites unveiled a biphasic decomposition process during the pyrolysis. The frst phase, occurring between 100 and 150 °C, involved dehydration, resulting in weight loss of 10% for 10:20:70, 8% for 15:15:70, and 5% for 20:10:70 compositions (Hsieh et al. [2018\)](#page-17-22). In the subsequent stage, from 150 to 750 °C, the NZC 10:20:70 composition experienced a substantial 25% weight loss due to the pyrolytic decomposition of residues. Notably, the TGA curves for NZC 15:15:70 and NZC 20:10:70 showed a shift to higher temperatures (150–700 °C) with weight loss of around 10% and 14%, respectively. These trends are attributed to the decomposition of residues. TGA measurements were also undertaken for NZC 20:10:70 sample after the adsorption of 4-chlorophenol to evaluate the nanocomposite's stability. As shown in Fig. [7](#page-8-2)b, the nanocomposite remains stable even at elevated temperatures. The initial weight loss observed is due to the desorption of 4-chlorophenol that had been

Fig. 6 BET nitrogen adsorption-desorption isotherms graphs of $Ni-Zn/CeO₂$ nanomaterials

Table 3 BET characteristics of Ni-Zn/CeO₂ nanocomposites

Nanomaterial	Surface area m^2/g		Pore diameter (nm)
NZC 10:20:70	102.675	0.182	4.305 nm
NZC 15:15:70	62.252	0.193	3.813 nm
NZC 20:10:70	118.471	0.256	6.448 nm

Fig. 7 TGA analysis: a TGA before adsorption and **b** TGA after adsorption (NZC 20:10:70)

^aThe model *F*-value of 60.29 indicates that the model is significant, with only a 0.01% probability that such a substantial that *F*-value could arise from random noise

adsorbed on the nanocomposite's surface. Once the entire 4-chlorophenol content is removed (typically occurring between 500 and 600 °C) (Tum and Kariuki [2020](#page-18-23)), the TGA curve stabilizes, indicating the nanocomposite's stability at higher temperatures.

Zeta potential analysis

The surface charge, characterized by zeta potential, signifcantly infuences the adsorption of 4-chlorophenol onto Ni-Zn-CeO₂ nanocomposites. Under neutral conditions, the nanocomposite typically exhibits a slightly negative zeta potential value of − 6 mV, while 4-chlorophenol remains predominantly neutral (Yang et al. [2017](#page-18-24)). During adsorption, interactions are primarily driven by weak forces such as hydrogen bonding and π - π or dipole-dipole interactions between the neutral molecules and the nanocomposite surface.

In acidic environments, the nanocomposite surface undergoes protonation, leading to a positively charged surface (Li et al. [2020\)](#page-17-23). Despite 4-chlorophenol remaining neutral due to the presence of excess H^+ ions, the positive surface charge creates a conducive environment for the molecules to approach and interact with the nanocomposite. In alkaline conditions where 4-chlorophenol exists predominantly as the phenolate ion (negatively charged), interactions between 4-chlorophenol and surfaces such as NZC nanocomposite would typically involve electrostatic repulsion rather than attraction (Zhang et al. [2019\)](#page-18-6).

Analysis of variance and BBD model analysis

We employed the Box-Behnken Design under Response Surface Methodology (BBD-RSM) to investigate how different adsorption factors infuenced the removal of 4-chlorophenol using the NZC 20:10:70 nanocomposite, which was identified as the most efficient among the three nanomaterials. The primary parameters examined included pH of the solution, temperature, adsorbent dosage, and contact time. A statistical analysis of the experimental results related to the removal of 4-chlorophenol by the NZC 20:10:70 nanocomposite was conducted using ANOVA, and the outcomes are tabulated in Table [4.](#page-9-0)

The ANOVA fndings for NZC 20:10:70, particularly the F-values, indicate the quality of the models utilized, for 4-chlorophenol, in its removal. In this instance, the F-value for NZC 20:[1](#page-9-1)0:70 is 21.70, and the corresponding p^1 -value is less than 0.0001, implying a high degree of signifcance and data accuracy (Jawad et al. [2020](#page-17-24)). Generally, terms with *p* values above 0.05 are considered statistically insignifcant in the context of 4-chlorophenol removal efficiency, and those with *p* values under 0.05 are considered statistically signifcant (Andrade [2019\)](#page-16-13).

¹ The *P* value is like a measure of how likely it is that any differences we see between groups happened by random chance, assuming there is actually no real effect. It helps us figure out if our findings are reliable or just random [Dahiru [2011](#page-17-25)). Model terms with *p* values less than 0.0500 are signifcant.

The R^2 (determination coefficient) for the removal of 4-chlorophenol is *ca~* 0.9530, indicating a close proximity between the experimental and calculated data.

As a result, the terms in the 4-chlorophenol removal model, including A, B, C, D, AB, AC, AD, BC, BD, CD, A^2 , B^2 , and $C²$, have been determined to be statistically significant. After performing the correlation analysis, second-order quadratic polynomial models involving the responses (4-chlorophenol removal) and the tested factors were established, as shown in Eq. [13](#page-10-0) (analysed by Design Expert Software):

Removal efficiency:
$$
+ 60.9839 - 9.30995 \, \text{A} + 18.4774 \, \text{B}
$$

\n $+ 4.43128 \, \text{C} - 5.94134 \, \text{D} - 3.58586 \, \text{AB}$

\n $+ 3.80018 \, \text{AD} + 4.47591 \, \text{BC} + 3.18368 \, \text{CD}$

\n $- 11.7459 \, \text{A}2 - 15.6631 \, \text{B}2 + 14.2883 \, \text{D}$

\n(13)

Figure [8a](#page-10-1) illustrates the efficiency of the NZC $20:10:70$ nanocomposite in removing 4-chlorophenol. As evident, the tightly clustered data points along a single line indicate the model's efectiveness and reliability of the ANOVA results (Kusuma et al. [2021](#page-17-26)). Figure [8b](#page-10-1) compares the predicted results with the actual results for the elimination of 4-chlorophenol. A strong alignment between the model's predictions and the actual observed outcomes indicates the reliability of the data used in the formulation of the model.

Synergistic efects of variables

The 3D response surface diagrams were plotted to assess the impact of various factors on the removal of 4-chlorophenol using NZC nanomaterials. Figure [9](#page-11-0)a and b depict the combined effects of adsorbent dosage (NZC 20:10:70) and pH on the rate of 4 chlorophenol removal, with temperature held constant at 10°C and a fxed contact time of 120 min.

From the results presented in Fig. [9](#page-11-0)a and b, it becomes clear that the adsorption efficiency of 4 chlorophenol by NZC 10:20:70 is signifcantly enhanced under acidic conditions at pH 3 and decreases as the pH becomes more basic, approaching pH 10. Meanwhile, as shown in Fig. [7](#page-8-2)b, the removal efectiveness of 4-chlorophenol is boosted by increasing the adsorbent dosage (from 10 to 50 mg) and contact time (10–20 min), while maintaining the pH at 3 and the temperature fxed at 10 °C. The maximum removal efficiency achieved by NZC 10:20:70 was 91.3%.

Figure [9c](#page-11-0) and d illustrate the adsorption of 4 chlorophenol by NZC 15:15:70 nanocomposites, and the same experimental conditions and parameters were followed as in the case of NZC 10:20:70, showing similar trends. However, this particular nanocomposite exhibits a lower adsorption capacity. Under optimal conditions of pH 3, a temperature of 10 °C, a contact duration of 120 min, and an adsorbent dosage of 50 mg, it achieves a maximum removal of 79.1%. These same experimental conditions

Fig. 8 a Normal probability plot of residuals for a NZC 20:10:70 nanocomposite. **b** Graphical representation depicting the correlation between predicted and actual values of 4 chlorophenol removal for NZC 20:10:70

and parameters were applied to NCC 20:10:70 nanocomposites (Fig. [9e](#page-11-0) and f) resulting in an impressive 99.1% removal of 4-chlorophenol in 120 min. In summary, these experiments allow us to deduce the optimal conditions and trends for 4-chlorophenol removal from NZC nanocomposites. Removal efficiency is higher under acidic pH conditions, while it decreases under alkaline pH. Both adsorbent dosage and contact time exhibit a similar pattern, with an increase in these parameters leading to enhanced removal of 4-chlorophenol. The temperature was kept at (lowest value) 10 °C in these responsive curve diagrams

Infuence of concentration

The influence of concentration on removal efficiency was investigated by altering the concentration of 4-chlorophenol from 10 to 50 ppm while keeping a constant adsorbent

dosage of 50 mg at 20 °C and 120 min of contact time and pH 3.0. The results, as depicted in Fig. [10,](#page-12-0) clearly demonstrate a decline in removal efficiency with increasing 4-chlorophenol concentration. In the adsorption studies using different nanocomposites, the adsorption capacity (q_e) shows a consistent increase as the initial concentration of the solution rises from 10 ppm to 50 ppm. For NZC 10-20-70, q_e rises from 18.88 mg/g at 10 ppm to 92.47 mg/g at 50 ppm. Similarly, NZC 15-15-70 exhibits an increase in q_e from 17.82 mg/g at 10 ppm to 80.65 mg/g at 50 ppm, while NZC 20-10- 70 demonstrates growth from 19.85 mg/g at 10 ppm to 96.33 mg/g at 50 ppm. For all three nanomaterials, achieving equilibrium at a higher concentration of 4-chlorophenol required a relatively longer period. The greater mass resistance that the adsorbate molecules experience when trying to penetrate through the deeper layers of the immobilized adsorbent is the cause of this extended equilibration time (Bahrudin et al. [2020](#page-16-14)).

Fig. 10 Impact of concentration on removal efficiency of 4-chlorophenol by Ni-Zn/CeO₂ nanocomposites (pH=3, 4-CP concentration = 10–50 ppm, adsorbent dose $= 0.05$ g, contact time $= 120$ min, T $= 20$ \degree C, volume of solution = 100 ml)

Infuence of temperature

Temperature dependence of 4-chlorophenol removal by $Ni-Zn/CeO₂$ nanocomposites was examined within a temperature range of 10°C to 60°C (Fig. [11](#page-12-1)). The data reveal an inverse linear relationship between removal efficiency and temperature for all three nanocomposites. Low-temperature conditions favoured the removal of 4-chlorophenol, suggesting the involvement of weak adsorptive forces during the process. These forces are compromised by high temperatures lead to their disruption and fnally causing a decline in the removal efficiency of 4-chlorophenol (Semwal et al. [2023\)](#page-18-9).

Adsorption isotherm

The adsorption isotherm for NZC nanocomposites was studied by three models namely Langmuir, Freundlich, and Temkin models (Fig. [12](#page-13-0)a, b, and c respectively). The Freundlich model efectively described the adsorption phenomenon, as shown in Table [5.](#page-13-1) In comparison to Langmuir and Temkin isotherms, the R^2 values for Freundlich isotherms were higher for all three nanocomposites. The Freundlich isotherm model's R^2 value was in the range of 0.99 for all three nanocomposites indicating a strong ft. Additionally, the calculated heterogeneity factor (*n*) falls within the range of 1–3, suggesting that the reaction is favourable. If $1 < n <$ 10, which confrms that the adsorption was favourable (Zhao et al. [2020\)](#page-19-1). A combined analysis of the Langmuir (Fig. [12](#page-13-0)a) and Freundlich isotherm models (Fig. [12b](#page-13-0)) revealed that 4-chlorophenol adsorption onto NZC nanocomposites was a complex process comprising both chemical and physical adsorption, as well as monolayer and multilayer adsorption.

Fig. 11 Impact of temperature on removal efficiency of 4-chlorophenol by Ni-Zn/CeO₂ nanocomposites (pH = 3 , 4-CP concentration = 50 ppm, adsorbent dose = $0.05g$, contact time = 120 min, T = 10–60 $°C$, volume of solution = 100 ml

The Temkin model's ftting results in this study were moderate (Fig. [12c](#page-13-0)). This fnding suggests that electrostatic interaction is likely one of the mechanisms involved in the adsorption of 4-chlorophenol onto $Ni-Zn/CeO₂$ nanocomposites [Rajahmundry et al. [2021\)](#page-18-25).

Thermodynamic parameters

Diferent thermodynamic parameters for the adsorption of 4-chlorophenols on the synthesized nanomaterials were determined and logically interpreted. These values are appended in Table [6.](#page-13-2)

The ΔG^0 values observed in the range of -0.4 to -1.7 kJ/mol (Fig. [13a](#page-14-0)) suggest a sorption process that begins as physisorption (physical adsorption). Physisorption is typically characterized by ΔG_{ads}^0 values between 0 and $-$ 20 kJ/mol (Darla et al. [2023](#page-17-27)). The negativity of ΔG^0 supports the viability of 4-chlorophenol adsorption onto the synthesized Ni-Zn/CeO₂ nanocomposites, and the process of adsorption is spontaneous. A negative ΔS^0 value indicates the affinity of the Ni-Zn/CeO₂ nanocomposites for 4-chlorophenol and decreases in the randomness at the solid-solution interface (Kashipazha et al. [2023\)](#page-17-28). The calculated values of ΔH^0 are negative, which confirms that the nature of the adsorption process is exothermic, aligning with the experimental data demonstrating a decrease in adsorption with increasing temperature (Jery et al. [2024](#page-17-29)). The higher the negative value ΔH^0 , the stronger the exothermic interaction between the 4-chlorophenol and the nanocomposite surface.

Fig. 12 Adsorption isotherm linear ftted plots of 4-CP by NZC nanocomposites **a** Langmuir, **b** Freundlich, and **c** Temkin isotherms (pH = 3 , 4-CP concentration = 10-50 ppm, adsorbent dose = 0.05 g, contact time = 120 min, T = 20 °C, volume of solution = 100 ml)

Table 5 $Ni-Zn/CeO2$ nanocomposites' isotherm constants for the adsorption of 4-chlorophenol	Nanocomposites	Langmuir			Freundlich			Temkin	
		$R_{\rm L}^2$	K_L	q_{max}	$R_{\rm F}^2$	$\rm K_{\scriptscriptstyle E}$	n	В	R^2
		(mg/g)		$(mg/g)(Lmg^{1})^{1/n}$					
	NZC 10:20:70	0.9864	0.329	118.2	0.9971	$1.9*10^5$	1.25	16.103	0.9656
	NZC 15:15:70	0.9775	0.277	68.27	0.9989	$7.69*10^5$	1.52	08.399	0.9275
	NZC 20:10:70	0.9383	0.014	59.1	0.9948	$1.8*10^{6}$	2.11	11.763	0.9702

Table 6 Thermodynamic constants for adsorption of 4-chlorophenol on Ni-Zn/CeO₂ nanocomposites

Kinetic study

The kinetic models of pseudo-second-order (PSO) and pseudofrst-order (PFO) were applied in order to study the adsorption process of 4-chlorophenol (4-chlorophenol) onto Ni-Zn/ $CeO₂$ nanocomposites. The higher $R²$ values obtained for the PSO models (0.9996, 0.9980, and 0.9976) for the three nanocomposites, NZC 10:20:70, NZC 15:15:70, and NZC

Fig. 13 Thermodynamic study of adsorptive removal of 4-chlorophenol by Ni-Zn/CeO₂ nanocomposites kinetics studies: **a** $\Delta G^{\rm o}$ values at different temperature and **b** thermodynamic Van't Hoff plot ln K_{ads} vs $1/T$ $(pH = 3, 4$ -CP concentration = 50 ppm, adsorbent dose $= 0.05$ g, contact time $= 120$ min, T $=$ 10–60 °C (283–333 K), volume of solution $= 100$ ml)

20:10:70, respectively, indicate that the PSO model (Fig. [14b](#page-14-1)) suited the data obtained from experiment better than the PFO model (Fig. [14a](#page-14-1)) (Revellame et al. [2020;](#page-18-26) Simonin [2016\)](#page-18-27). The enhanced efficacy of the PSO model implies that chemisorption, which involves the establishment of strong chemical interactions between 4-chlorophenol molecules and the nanocomposite surface, is the primary mechanism governing the adsorption process (Bagheri et al. [2022](#page-16-15)). Additionally, the proximity between the calculated adsorption capacity values $(q_{e \text{ calc}})$ from the PSO model and the experimental q_{e} values (qe_{exp}) further supports the relevance of the PSO model in explaining the adsorption kinetics of 4-chlorophenol onto $Ni-Zn/CeO₂$ nanocomposites indicated in Table [7.](#page-14-2)

20:10:70 nanocomposite, with the adsorbent being isolated and subjected to multiple washes with NaOH and deionized water after each cycle (Tazik et al. [2023\)](#page-18-28).

The reusability analysis was performed on NZC 20:10:70 nanocomposite as it gives the best removal efficiency among all the nanocomposites. As illustrated in Fig. [15](#page-15-0), the fndings indicated that the rate of adsorption was decreased by approximately 15% after eight regeneration cycles. This small decrease is signifcant because it shows that these nanocomposites can be reused many times without losing their efectiveness. For sustainability and cost-efective option, these nanocomposites should retain their adsorption performance over multiple uses.

Desorption and reusability studies

The economic signifcance of adsorbent reusability must be overemphasized. In seeking this, the efficiency of adsorption was assessed over eight (8) consecutive cycles for the NZC

Fig. 14 Non-linear ftted curve of **a** pseudo-frst-order kinetics and **b** pseudo-second-order kinetics for adsorption of 4-chlorophenol on Ni-Zn/CeO₂ nanocomposites ($pH = 3$, 4-CP $concentration = 50$ ppm, adsorbent dose $= 0.05$ g, contact time = $20 - 120$ min, T = 20 °C, volume of solution $= 100$ ml)

Comparative analysis with existing literature

Table [8](#page-15-1) summarises a comparative analysis of diferent nanoadsorbents, contact time for the removal, and the corresponding removal efficiencies for chlorophenol from aqueous solution.

Fig. 15 Regeneration cycles of removal of 4-chlorophenol by using NZC 20:10:70 nanocomposite (pH = 3, 4-CP concentration = 50 ppm, adsorbent dose = 0.05 g, contact time = 120 min, T = 20 °C, volume of solution $= 100$ ml)

Adsorption mechanism

The adsorption of 4-chlorophenol onto $Ni-Zn/CeO₂$ nanocomposites is a multi-step process involving physical and chemical interactions. The FT-IR peak at 1515.31 cm^{-1} , representing C=C stretching of an aromatic group, proposes that the aromatic ring of 4-chlorophenol interacts with the nanocomposite surface via π - π stacking or hydrogen bonding. The close association of adsorbate molecules with the nanocomposite surface facilitates chemical bonds formation (chemisorption) between the surface and 4-chlorophenol molecules.

In addition to adsorption through chemical bond formation, the O-H bonds present on the surface of nanocomposites lead to hydrogen bonding interactions between 4-chlorophenol's -OH groups. Overall, the proposed adsorption mechanism of 4-chlorophenol on Ni-Zn/CeO₂ nanocomposites involves physisorption, chemisorption, aromatic interactions, and hydrogen bonding as illustrated in Fig. [16](#page-15-2).

Fig. 16 Adsorption mechanism for removal of 4-chlorophenol by NZC nanocomposites

Conclusion

The Ni-Zn/CeO₂ nanocomposites were successfully synthesized using an aqueous co-precipitation method. It was demonstrated that the nanocomposites efectively remove 4-chlorophenol from aqueous solutions. The optimal conditions for this removal were identifed as a solution pH of 3, an adsorbent dosage of 0.05 g/L, and a temperature of 10°C. XRD analysis confrmed the formation of two phases within the $CeO₂$ matrix. The pseudo-second-order kinetics and Freundlich isotherm were followed during the adsorption process. The adsorption of 4-chlorophenol is mainly facilitated by chemical forces, such as hydrogen bonding, π -π interactions. TEM analysis revealed that particle size ranges from 3 to 5 nm, and TGA analysis also confrmed that the nanocomposites can withstand high temperatures even post-adsorption process. The nanocomposite with the composition NZC 20:10:70 exhibited the highest removal capacity for 4-chlorophenol. This nanocomposite removed approximately 99.1% of 4-chlorophenol within an equilibrium time of 2 h. The nanocomposites exhibit excellent reusability, enabling their repeated use for removing phenolic pollutants.

Author contribution N.S.: conducted experiments, collected data, drafted the original manuscript

- D.M.: conducted experiments, collected data
- M.C.: data analysis, review
- R.K.: data analysis

M.C.A.: conceptualisation, supervision, reviewing and editing of manuscript

Data availability The data will be made available on reasonable request.

Declarations

Consent to participate Not applicable.

Consent for publication Not applicable.

Competing interests The authors declare no competing interests.

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