



# Efficient phosphate removal by Mg-La binary layered double hydroxides: synthesis optimization, adsorption performance, and inner mechanism

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Received: 8 November 2023 / Accepted: 5 March 2024 / Published online: 3 April 2024  
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## Abstract

Layered double hydroxides (LDH) hold great promise as phosphate adsorbents; however, the conventional binary LDH exhibits low adsorption rate and adsorption capacity. In this study, Mg and La were chosen as binary metals in the synthesis of Mg-La LDH to enhance phosphate efficient adsorption. Different molar ratios of Mg to La (2:1, 3:1, and 4:1) were investigated to further enhance P adsorption. The best performing Mg-La LDH, with Mg to La ratio is 4:1 (LDH-4), presented a larger adsorption capacity and faster adsorption rate than other Mg-La LDH. The maximum adsorption capacity (87.23 mg/g) and the rapid adsorption rate in the initial 25 min of LDH-4 (70 mg/(g·h)) were at least 1.6 times and 1.8 times higher than the others. The kinetics, isotherms, the effect of initial pH and co-existing anions, and the adsorption-desorption cycle experiment were studied. The batch experiment results proved that the chemisorption progress occurred on the single-layered LDH surface and the optimized LDH exhibited strong anti-interference capability. Furthermore, the structural characteristics and adsorption mechanism were further investigated by SEM, BET, FTIR, XRD, and XPS. The characterization results showed that the different metal ratios could lead to changes in the metal hydroxide layer and the main ions inside. At lower Mg/La ratios, distortion occurred in the hydroxide layer, resulting in lower crystallinity and lower performance. The characterization results also proved that the main mechanisms of phosphate adsorption are electrostatic adsorption, ion exchange, and inner-sphere complexation. The results emphasized that the Mg-La LDH was efficient in phosphate removal and could be successfully used for this purpose.

**Keywords** Phosphate removal · Adsorption · Mg-La LDH · Metal ratio · chemisorption · Ion exchange

## Highlights

- The Mg-La LDH powder was successfully synthesized by the traditional co-precipitation method.
- The Mg/La ratio of 4:1 in the preparation of Mg-La LDH results in high affinity to P due to the excellent crystallinity and stable lamellar structure.
- The maximum adsorption capacity for P can reach 81.96 mg/g when the equilibrium concentration is 0.5 mg/g.
- The adsorption mechanism involved electrostatic attraction, ion exchange, and complexation.
- Mg-La LDH possibly emerged as the promising material for the effective removal of P from water.

Responsible Editor: Tito Roberto Cadaval Jr

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## Introduction

Phosphorus is an essential nutrient for all living organisms whereas its excessive presence in natural water bodies has gradually become a global environmental problem (Cordell et al. 2009). The major status of phosphorus in natural water bodies and wastewater is phosphate (P). The phosphorus concentration higher than 0.02 mg/L would lead to the eutrophication of biological systems (Yin et al. 2021). The US Environmental Protection Agency (US-EPA) requires the total phosphorus limit in surface water (river, lake) to be 0.02 to 0.1 mg/L (Liu et al. 2021). The demand for phosphorus removal in water treatment facilities is steadily increasing, necessitating the development of a cost-effective and efficient technology for phosphorus removal. As a typical phosphorus removal process, adsorption technology exhibits better performance than other processes and has been widely accepted for phosphorus

removal from water/wastewater, especially for low-concentration phosphorus removal due to its high efficiency, low energy consumption, and flexibility (El-Qelish et al. 2024; Xiong et al. 2017).

In water treatment, commonly employed adsorbents for phosphate removal includes activated carbon and biochar (Chen et al. 2023), metal oxides (Lin et al. 2019a; Lin et al. 2019b), waste modified material (Qiao et al. 2022; Yin et al. 2021), clay, chitosan-based materials (Feng et al. 2022a), montmorillonite (Zou et al. 2020), porous silicon dioxide (Shin et al. 2004), and layered double hydroxides (LDH) (Feng et al. 2022a). Among these adsorbents, LDH, a versatile ionic layered compound, has been considered a promising adsorbent for phosphorus removal. The composition elements and preparation conditions of these compounds can be fine-tuned over a broad range, thereby imparting them with a highly adjustable hydrotalcite structure. Previous studies have proposed many LDH in P removal; the P adsorption capacity of Mg Al LDH prepared by co-precipitation method such as Dox et al. (Dox et al. 2019) was 61 mg/g. The Mg Al LDH prepared by Ribeiro et al. (2023) could complete the adsorption in 60 min. These can fully demonstrate the high efficiency of LDH for P adsorption in water. However, it is worth noting that the high P adsorption capacity of binary LDH in most studies was due to the extremely high initial P concentrations (100–500 mg/L), whereas P concentrations often fluctuated around 5–10 mg/L in real-world wastewater. A high initial P concentration would not only inevitably lead to high adsorption capacity but also result in a high remaining concentration of P (~ 50 mg/L). Therefore, the theoretical adsorption capacity derived from this scenario would not be applicable in real applications. Consequently, the synthesis of binary LDH should be further optimized for better P adsorption performance.

Previous reports have demonstrated that the element La could be used as an efficient functional material in adsorption which exhibits a strong affinity for phosphate and possesses low toxicity and chemical stability (Koilaraj and Sasaki 2017; Wu et al. 2007). For instance, the P adsorption capacity of lanthanum hydroxide and lanthanum carbonate prepared by Wu et al. (2022) could achieve efficient adsorption performance at low P equilibrium concentrations. It was hypothesized that the incorporation of La in LDH synthesis would also exhibit commendable P adsorption performance. However, there is a scarcity of studies on the synthesis of efficient binary LDHs with La.

The present study reported the successful synthesis of a novel Mg-La LDH via the traditional co-precipitation method. This study aimed to fabricate a novel binary LDH using Mg and La to achieve efficient adsorption performance at low P equilibrium concentrations. The optimum preparation conditions of Mg-La LDH were determined through single-factor

analysis and comparison of adsorption capacity. The effects of kinetics, adsorption isotherms, and solution pH were investigated to confirm the optimal ratio of Mg and La. Various isotherm and kinetic models for the adsorption and interaction between the P and Mg-La LDH were applied. Subsequently, the potential for phosphorus removal and the regeneration possibility of Mg-La LDH on actual wastewater was assessed by examining the impact of coexisting ions and conducting cyclic desorption experiments. Finally, the changes in structure and chemical composition of Mg-La LDH before and after phosphate adsorption were investigated by means of SEM, XRD, FTIR, and XPS. The underlying adsorption mechanism of this composite material was further discussed.

## Materials and methods

### Materials

Magnesium chloride ( $\text{MgCl}_2 \cdot 6\text{H}_2\text{O}$ ), lanthanum chloride ( $\text{LaCl}_3 \cdot 7\text{H}_2\text{O}$ ), ferric chloride ( $\text{FeCl}_3$ ), aluminum chloride ( $\text{AlCl}_3$ ), hydrochloric acid (HCl), sodium hydroxide (NaOH), and potassium dihydrogen phosphate ( $\text{KH}_2\text{PO}_4$ ) were purchased from Sinopharm Chemical Reagent Co, Ltd. (Shanghai, China). A stock solution of phosphorous was prepared by dissolving 4.394 g of  $\text{KH}_2\text{PO}_4$  in 1000 mL of deionized water. In addition, phosphate solutions of different concentrations were prepared by diluting the stock solution. All chemicals used in this study were of analytical grade.

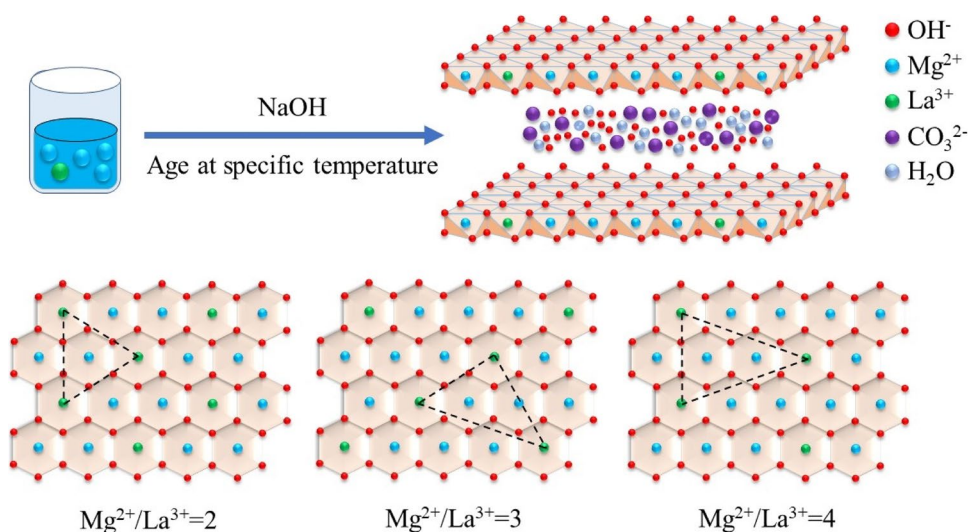
### Synthesis of LDH powder

Mg-La LDH powder was synthesized by the traditional co-precipitation method (Li et al. 2022; Zhang et al. 2021c). Specifically,  $\text{MgCl}_2 \cdot 6\text{H}_2\text{O}$  and  $\text{LaCl}_3 \cdot 7\text{H}_2\text{O}$  were added into 150 mL deionized water to prepare a mixed solution with the  $\text{Mg}^{2+}:\text{La}^{3+}$  molar ratio of 2:1, 3:1, and 4:1, respectively. Then, under stirring, 1.0 mol/L NaOH solution was slowly added to the above solution to adjust the pH to 10. After stirring for 30 min, this reaction mixture was further aged for 10 h at 80 °C. The final precipitate was washed with deionized water and dried in an oven at 80 °C. The adsorbents were named LDH-X, where the X represents the ratio of  $\text{Mg}^{2+}:\text{La}^{3+}$ . According to the above method, the LDH-Fe ( $\text{Mg}^{2+}:\text{Fe}^{3+}$  molar ratio of 2:1) and LDH-Al ( $\text{Mg}^{2+}:\text{Al}^{3+}$  molar ratio of 2:1) were synthesized (Fig. 1).

### Batch experiments

A series of batch experiments were carried out to investigate and compare the adsorbents by figuring out the effect of adsorption time, P concentration, and pH on the adsorption

**Fig. 1** Schematic illustration for the preparation of Mg-La LDH by co-precipitation and the structure of them



capacity. All adsorption experiments were performed at room temperature (25 °C) with the same adsorption dose (0.4 g/L). The P after the reaction was determined by the ascorbic method (APHA, 2017) and detected by a UV-spectrophotometer (HACH, DR2800) at 700 nm. To make the data reliable, three parallel samples were used for each experiment, and the data were average value.

The equilibrium adsorption capacity ( $q_e$ ) and the removal rate ( $R$ ) of phosphate were calculated using the following equation:

$$q_e = \frac{(C_0 - C_e)V}{m} \quad (1)$$

$$R = \frac{(C_0 - C_e)}{C_0} * 100\% \quad (2)$$

where  $C_0$  and  $C_e$  (mg/L) are the initial and equilibrium concentrations,  $m$  (g) is the mass of adsorbent, and  $V$  (L) is the volume of the solution.

### Adsorption models

The adsorption data in this study was fitted by the kinetic models and adsorption isotherms for further interpretation. Three adsorption kinetics, pseudo-first-order model, pseudo-second-order model, and intraparticle diffusion model were represented by Eqs. (3) to (5), respectively (Li et al. 2021a).

$$\ln(q_e - q_t) = \ln q_e - K_1 t \quad (3)$$

$$\frac{t}{q_t} = \frac{1}{K_2 q_e^2} + \frac{t}{q_e} \quad (4)$$

$$q_t = k_i t^{\frac{1}{2}} + I \quad (5)$$

where  $q_t$  (mg/g) is the adsorption capacity at time  $t$ ,  $K_1$  ( $\text{min}^{-1}$ ) and  $K_2$  ( $\text{g}/(\text{mg}\cdot\text{min})$ ) are the adsorption rate constant of pseudo-first-order and pseudo-second-order,  $k_i$  ( $\text{mg}/(\text{g}\cdot\text{h}^{1/2})$ ) is the adsorption rate constant of the intraparticle diffusion model, and the  $I$  (mg/g) is the constant associated with the boundary layer reaction.

The adsorption isotherms such as Langmuir isotherm and Freundlich isotherm were used in this study (Yang et al. 2022). Both models can be expressed as Eqs. (6) and (7):

$$q_e = \frac{q_m K_L C_e}{1 + K_L C_e} \quad (6)$$

$$q_e = K_F C_e^{1/n} \quad (7)$$

where  $q_m$  (mg/g) represents the theoretical maximum adsorption capacity of the adsorbent and  $K_L$  (L/mg) is the equilibrium constant related to the binding energy. The  $K_F$  (mg/g) is the Freundlich adsorption capacity, and the  $n$  is the Freundlich constant which has a higher value for a less heterogeneous surface. Furthermore, the dimensionless factor  $R_L$  is defined by Eq. (8):

$$R_L = \frac{1}{1 + K_L C_0} \quad (8)$$

The adsorption nature is irreversible at  $R_L = 0$ , favorable at  $0 < R_L < 1$ , or unfavorable at  $R_L > 1$  (Li et al. 2023).

### Characterization of the adsorbents

The surface morphology of the adsorbent was analyzed by scanning electron microscopy (SEM) (Hitachi, S-4800),

and the crystal structure of the adsorbent was analyzed via X-ray diffraction (XRD) (Bruker, D8 ADVANCE). The analysis was based on the Bragg equation (Santos et al. 2020), which established a relationship between the intensity of diffraction peaks and the angle of incidence as well as the spacing of the lattice, as follows:

$$n\lambda = 2d \sin \theta \quad (9)$$

where  $d$  (Å) is the lamella distance,  $n$  is the reflection order of the peak,  $\lambda$  (Å) is the wavelength of the ray, and  $\theta$  (°) is the Bragg Angle determined by the peak diffraction.

The adsorption and desorption of  $N_2$  by the adsorbent were characterized using Brunauer-Emmett-Teller (BET) (Quantachrome Instruments, Autosorb-iQ) methods to determine the specific surface area. The thermal stability of solid samples was determined using thermogravimetric analysis (TG) (HITACHI STA200). Fourier transform infrared spectra (FTIR) (Nicolet, 6700) was employed to characterize the characteristic functional groups of the adsorbent before and after phosphorus removal, while energy dispersive X-ray photoelectron spectroscopy (XPS) (Thermo Scientific, K-Alpha X) was utilized to analyze the elements of the adsorbent before and after adsorption, thereby facilitating further discussion on the adsorption mechanism.

## Mg-La LDH regeneration

To explore the reusability of Mg-La LDH, an adsorption-desorption cycle experiment was carried out. In this study, the optimal desorption solution was determined by single-factor analysis. Based on the results and extensive literature research,  $Na_2CO_3$  was identified as a suitable desorbing agent for LDH. Therefore, sodium carbonate was used for desorption purposes. The desorption solution was supplemented with the adsorbent after the adsorption of phosphorus, and the concentration of phosphate in the desorption solution was determined to calculate the desorption rate. Subsequently, adsorption experiments were performed to evaluate the reuse performance through an adsorption-desorption cycle.

## Results and discussion

### Synthesis optimization

In the process of preparing LDH, in order to obtain a stable lamination structure, metal cations with little difference in ionic radii (0.065–0.080 nm) were

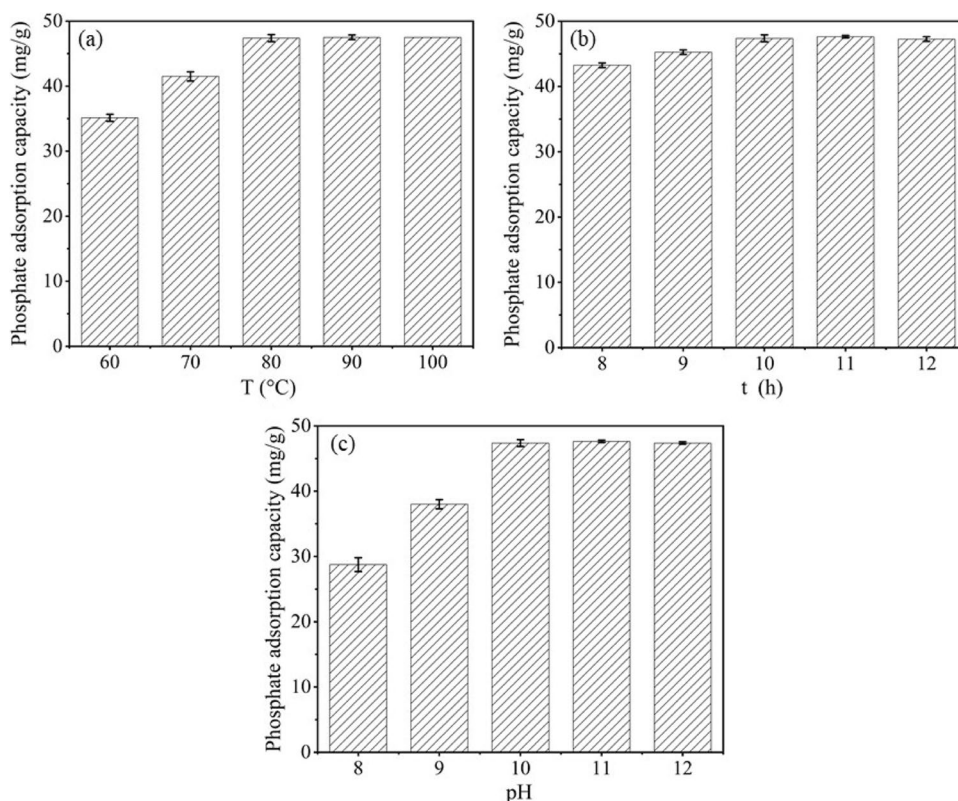
generally used as layered structures, and the ratio of divalent and trivalent metal cations was controlled to be 2–4 (Feng et al. 2022b). The radii of Mg and La ions used in this paper were not similar, so the synthesis ratio and preparation conditions had higher requirements. Based on previous research (Zubair et al. 2017; Daud et al. 2019), the reaction temperature, reaction pH, and reaction time were three significant operational parameters that exhibited great influences on the properties and structure of LDH. Therefore, in this study, the effect of these three parameters was first investigated.

As given in Fig. 2(a, b), increasing the synthesis temperature and extending the synthesis time within an appropriate range can help improve the P removal. However, excessive heating time led to a slight decrease in the adsorption effect. This was because the primary laminate formed in the early stage could not form a well-crystallizable LDH structure at a low synthesis temperature and time, resulting in a poor adsorption effect. The increase in temperature facilitated the morphological transformation of LDH, leading to a gradual enhancement in the crystallinity of LDH structure. Consequently, this promoted the formation of LDH with a well-developed crystal structure and abundant pores, thereby enhancing its adsorption capacity (Iqbal and Fedel 2018). However, excessive temperature or prolonged synthesis time can lead to gradual degradation of the LDH structure, resulting in reduced crystallinity and subsequent formation of other phases, ultimately leading to a decrease in adsorption capacity.

As shown in Fig. 2c, an increase in pH within the appropriate range helped to improve the removal of P, but if the pH was above 12, the effect would slightly decrease. This was because the primary laminates could not be formed well at low pH, so the LDH structure was not formed during subsequent heating and aging, resulting in poor adsorption capacity (Bukhtiyarova 2019). When the pH was excessively high, on the one hand, the formation of LDH layer structure would be unstable during heating aging, leading to easy precipitation of metal ions and their transformation into metal hydroxide precipitates, thereby resulting in poor crystallinity of LDH. On the other hand, it would lead to the increase of Na ions in the solution, so that the Na phase may appear in the LDH structure, resulting in the instability of the LDH structure. Both aspects ultimately contribute to diminished adsorption capabilities. According to the results of the single-factor analysis, the optimum synthesis parameters were determined as follows: synthesis temperature of 80 °C, synthesis pH of 10, and synthesis time of 10 h, and these parameters were used in the following experiments.



**Fig. 2** The effect of reaction temperature (a), reaction time (b), and reaction pH (c) on the P adsorption performance of LDH-4



### Characterization of the adsorbents

To characterize the morphology of the synthesized Mg-La LDH, the SEM images of Mg-La LDH with different molar ratios of Mg/La are given in Fig. 3. All three LDH samples exhibited uniform particle size, smooth surface topography, abundant porosity, and compact structure. This suggested that the successful synthesis of Mg-La LDH particles was not easily affected by different molar ratios of Mg/La. However, through comparison, it was evident that LDH-4 (Fig. 3c, f) possessed a more obvious crystal structure on the surface, smoother surface texture, and superior crystallinity than the other two LDHs.

The FTIR spectra of three LDHs are shown in Fig. 4a. A sharp peak at  $3694\text{ cm}^{-1}$  corresponded to hydroxyl stretching resulting from the presence of interlayer water and hydroxyl groups (Cavani et al. 1991). The stretching vibration at  $3435\text{ cm}^{-1}$  represented O-H, and the bending vibration at  $1441$  and  $1439\text{ cm}^{-1}$  corresponded to O-H as well. The vibrational bands at  $856\text{ cm}^{-1}$  and in the range of  $700\text{--}724\text{ cm}^{-1}$  were attributed to the Mg-La LDH interlayer carbonate anion group, specifically corresponding to the carbonate  $\nu_2$  and  $\nu_4$  vibrations, respectively (Li et al. 2023). It was noteworthy that LDH-4 exhibited a low intensity in the vibration zone of  $856\text{ cm}^{-1}$  and only displayed a single peak in  $700\text{--}724\text{ cm}^{-1}$ . This observation suggested a limited presence of  $\text{CO}_3^{2-}$ , thereby indicating that the internal

anion of LDH-4 exhibits a higher concentration of OH. That may be attributed to the different composition and irregular ordering of internal anions caused by different metal ratios. Moreover, the peaks observed at  $1487$  and  $1484\text{ cm}^{-1}$  represented La-O bonding interactions, whereas that detected at  $651\text{ cm}^{-1}$  was the tensile vibration associated with M-O and M-O-M (M represents Mg or La) (Santosa et al. 2008). Overall, these results of FTIR confirmed that the structure of the three LDHs consisted primarily of metal hydroxide layers with intermediate layers composed of both hydroxide and carbonate anions.

The crystal phase results (Fig. 4b) demonstrated that Mg-La LDH exhibited four distinct diffraction peaks at  $2\theta = 11.6^\circ$  (003),  $23.5^\circ$  (006),  $34.1^\circ$  (009), and  $39.3^\circ$  (015). These peaks corresponded to the characteristic LDH structure, confirming the successful formation of a layered double hydroxide structure (Isidoro Ribeiro et al. 2023). Three additional crystalline phases  $\text{La}(\text{OH})_3$ ,  $\text{LaCO}_3\text{OH}$ , and  $\text{Mg}(\text{OH})_2$  were observed in the Mg-La LDH system. Among them, LDH-4 was predominantly composed of  $\text{La}(\text{OH})_3$  while the other two were dominated by  $\text{LaCO}_3\text{OH}$ . This observation was consistent with the weak  $\text{CO}_3^{2-}$  peak observed in LDH-4 using FTIR spectroscopy. On one hand, this can be attributed to the limited remote ordering ability resulting from the strong Jahn-Teller effect resulting from the extended M-O distance (Cavani et al. 1991). On the other hand, it

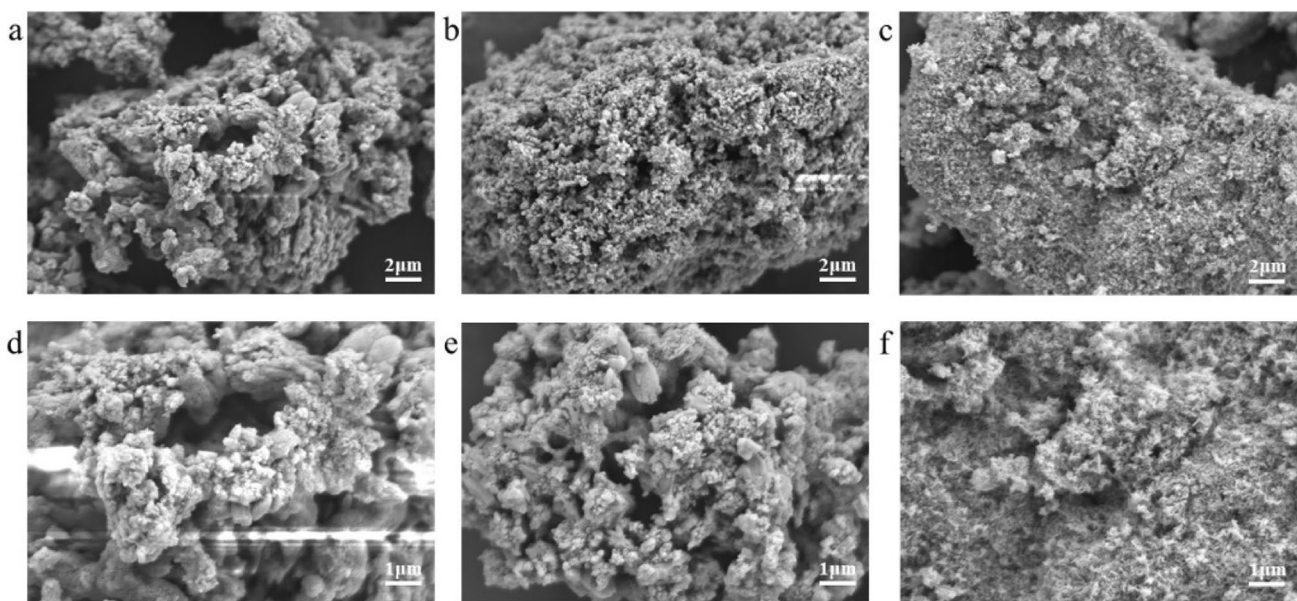


Fig. 3 SEM images of LDH-2 (a, d), LDH-3 (b, e), and LDH-4 (c, f)

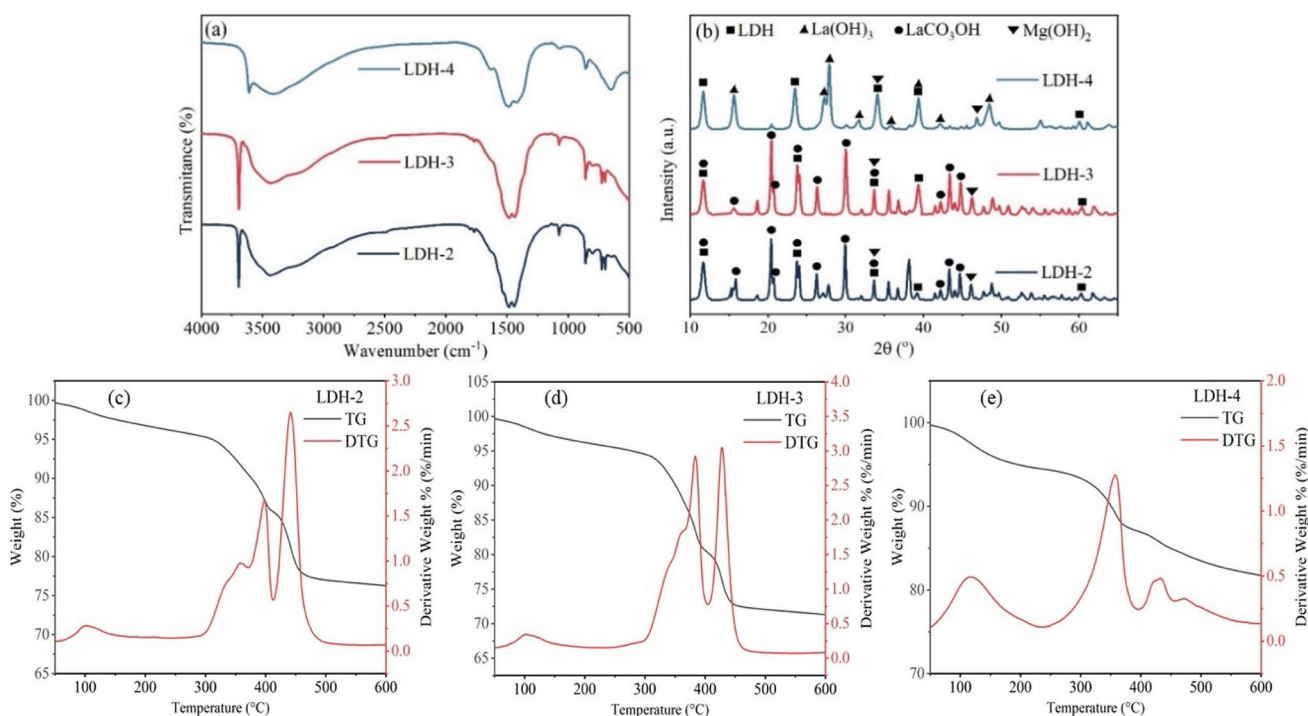


Fig. 4 FTIR spectra (a), XRD patterns (b), and TG-DTG analysis (c–e) of Mg-La LDHs

may also be influenced by differences in assembly due to varying metal ratios.

According to the formula calculation, all LDH crystal parameters are presented in Table 1. It can be observed that the surface spacing ( $d_{003}$ ) of LDH-2, LDH-3, and LDH-4 is 7.60 Å, 7.58 Å, and 7.57 Å, respectively. Notably, LDH-4 exhibited the smallest value which further substantiated that

OH<sup>-</sup> predominantly constituted the middle layer anion of LDH-4. The  $d_{003}$  layer spacing of LDH-4 closely approximated twice that of  $d_{006}$  layer spacing, indicating that Mg:La = 4:1 synthesis yields a lamellar structure with superior crystallinity among other ratios tested (Ookubo et al. 1992; Bukhtiyarova 2019). This was further supported by the crystal parameters  $a$  and  $c$ , both exhibiting their maximum

**Table 1** Crystallographic parameters of Mg-La LDH

Parameter	LDH-2	LDH-3	LDH-4
$d_{003}$	7.60	7.58	7.57
$d_{006}$	3.76	3.75	3.78
$a = 2d_{110}$	3.07	3.07	3.08
$c = 3(d_{003} + d_{006})/2$	22.68	22.62	22.70

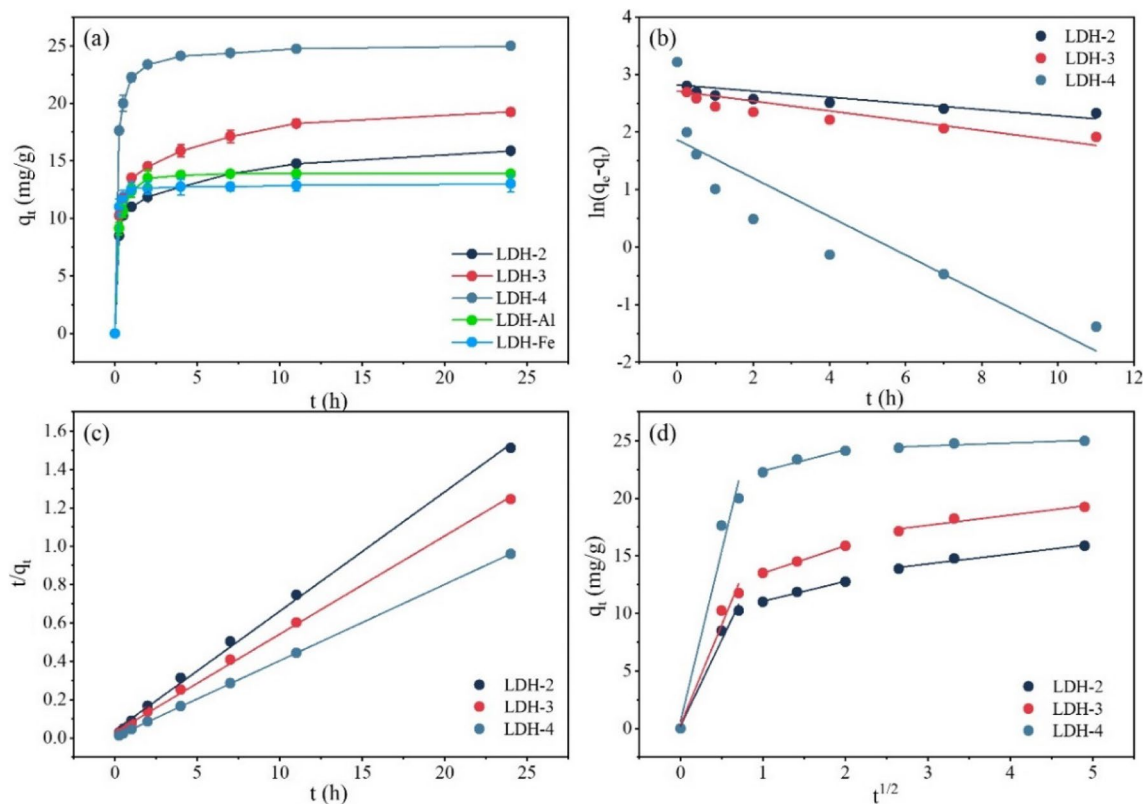
values when the Mg:La=4:1 ratio was employed, suggesting its favorable conditions for nucleation and growth resulting in highly crystalline LDH formation. This phenomenon may be attributed to the difference in ionic radii between Mg and La ions; at lower Mg/La ratios, distortion occurs within the hydroxide layer leading to reduced crystallinity and inferior properties (Ahmed et al. 2012).

TG-DTA measurements were performed to elucidate the thermophysical changes across endothermic and exothermic effects. Figure 4 (c–e) demonstrated the TG-DTA graphs (50–800 °C) of LDH-2, LDH-3, and LDH-4, respectively. In this study, the first weight loss occurred at about 120 °C. This weight loss can be attributed to the removal of the H<sub>2</sub>O molecules as well as the dehydration of interlayer species in Mg-La LDH (Wang et al. 2016; Maged et al. 2023a). The

high temperature region between 250 and 450 °C had been attributed to the decomposition of LDH (Tang et al. 2018). Notably, LDH-4 had the smallest weight loss, which indicated that LDH-4 had a more crystalline and stable structure.

### Adsorption kinetics

In order to investigate the adsorption rate of these LDHs, adsorption kinetics experiments were carried out. As shown in Fig. 5a, in the initial 60 min, a high adsorption rate can be observed, with the adsorption capacity reaching more than 70% of the equilibrium (specifically, LDH-2 is 71%, LDH-3 is 70%, and LDH-4 is 90%). This finding demonstrated the rapid phosphate removal performance of Mg-La LDH from water, especially for LDH-4. As the adsorption process proceeded, the number of active sites on different LDHs decreased gradually, resulting in relatively slower adsorption progress afterward. Under the condition of initial P of 10 mg/L, dosage of 0.4 g/L, and initial pH of 7, it took around 12 h for all three types of LDH to reach equilibrium, achieving adsorption performance of 15.88 mg/g, 19.25 mg/g, and 25.00 mg/g, for LDH-2, LDH-3, and LDH-4, respectively. On the contrary, conventional LDHs (LDH-Al and LDH-Fe) exhibited poor adsorption capacity. Furthermore, the



**Fig. 5** 10 mg/g concentration curve (a), pseudo-first-order model (b), pseudo-second-order model (c), and intraparticle diffusion model (d) for the adsorption of phosphate



complete removal of P from water by LDH-4 within 12 h further demonstrated the high efficiency of Mg-La LDH.

To further interpret the adsorption data, different kinetic models were used and fitted. As given in Table 2, the  $R^2$  value of the pseudo-second-order kinetic model was closer to 1, and its calculated  $q_e$  aligned more closely with the experimental data compared with pseudo-first-order kinetic. These findings indicated that the adsorption process was more consistent with the pseudo-second-order kinetic model, thereby providing evidence for the existence of chemisorption, such as ion exchange, inner-sphere complexation, and pore filling (Song et al. 2020; Maged et al. 2023b). Furthermore, the estimated adsorption rate in the initial 25 min of Mg-La LDH was calculated based on the experimental data. The calculated values were 34.0, 41.2, and 70.0 mg/(g·h), for LDH-2, LDH-3, and LDH-4, respectively. The obtained value of LDH-4 was 2.05 and 1.70 times than that of LDH-2 and LDH-3. These results explained the faster initial adsorption of LDH-4 compared to LDH-2 or LDH-3.

As for the intraparticle diffusion model, Fig. 5d exhibited three distinct stages during the adsorption process without origin, indicating that the in-particle diffusion process was not the only limiting factor during phosphate adsorption but also affected by external surface adsorption and boundary layer diffusion (Qiao et al. 2022; Jung et al. 2019). In the first stage, the three LDH fitting intercepts were smaller, indicating that the boundary layer thickness was thinner and the surface mass transfer opportunity was larger. Compared with LDH-2 and LDH-3, LDH-4 had a larger slope, indicating that there were more adsorption sites on the surface of LDH-4, thus providing a driving force for promoting adsorption and faster removal of phosphate (Li et al. 2021b; Seftel et al. 2018). In the second stage, the surface site had been occupied at this time, and the main process was that phosphate

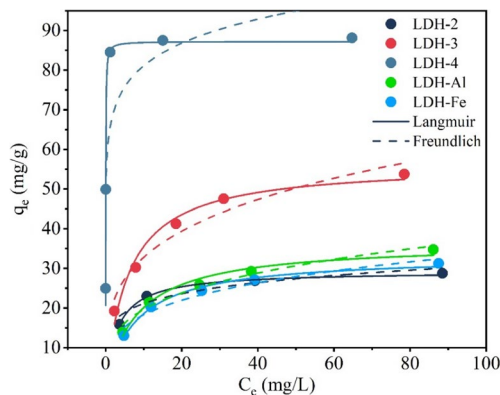
penetrates the internal pores of the adsorbent, which was affected by the intra-granular diffusion mechanism (Zhang et al. 2021b; Li et al. 2021b). With the increasing diffusion resistance of the inner hole, the adsorption enters the final stage. At this time, the dynamic equilibrium process of adsorption-desorption mainly occurred. Therefore, based on these results, the adsorption of P onto these LDHs was dominated by the chemical process, and the LDH-4 exhibited faster adsorption kinetics than others.

### Adsorption isotherms

In order to investigate the maximum adsorption capacity of these LDH adsorbents, adsorption experiments were conducted with different initial phosphate concentrations, and the obtained data were fitted by Langmuir and Freundlich isotherm models. As shown in Fig. 6, with the initial concentration increased, the adsorption capacity of these LDH also increased. Meanwhile, only LDH-4 showed a sharp increasing trend in adsorption capacity. The adsorption capacity of LDH-4 surged to around 85 mg/g with nearly no phosphate remaining in the solution. When the initial concentration of phosphate solution reached above 35 mg/L, the adsorption capacity of LDH-4 almost did not increase anymore. This observation indicated that the substantial P adsorption performance of LDH-4 was achieved by its superior adsorption performance rather than the high surrounding P concentration. However, in comparison, the LDH-2, LDH-3, and the common LDHs exhibited considerably slower and smoother curves of adsorption capacity: their adsorption capacities increased gradually with the higher initial concentrations. Therefore, the commendable performance of LDH-4 was not only about its higher adsorption capacity but also its extremely low equilibrium P concentration. This advantage would be perfectly suited to real situations and facilitate its applications.

**Table 2** Simulation parameters of pseudo-first-order, pseudo-second-order, and intraparticle diffusion models for phosphate adsorption by Mg-La LDH in wastewater

Kinetic model	Parameter	LDH-2	LDH-3	LDH-4
Pseudo-first-order model	$R^2$	0.581	0.676	0.786
	$k_1$ (min <sup>-1</sup> )	0.0537	0.0855	0.3336
	$q_e$ (mg/L)	16.76	15.02	6.76
Pseudo-second-order mode	$R^2$	0.998	0.999	0.999
	$k_2$ (g/(mg·min))	0.098	0.0871	0.271
	$q_e$ (mg/L)	16.10	19.52	25.12
Intra-particle diffusion mode	$R_1^2$	0.984	0.971	0.968
	$K_1$ (mg/(g·h <sup>1/2</sup> ))	14.96	17.33	29.57
	$R_2^2$	0.990	0.999	0.955
	$K_2$ (mg/(g·h <sup>1/2</sup> ))	1.73	2.37	1.84
	$R_3^2$	0.975	0.932	0.886
	$K_3$ (mg/(g·h <sup>1/2</sup> ))	0.86	0.89	0.26



**Fig. 6** Phosphate adsorption isotherms of Mg-La LDH simulated by the Langmuir and Freundlich models



As for the fitting results of Langmuir and Freundlich isotherms (Table 3), the  $R^2$  values of the Langmuir model of the three LDHs were closer to 1, indicating a better fitting with the Langmuir model and suggesting a uniform single-layer adsorption process (Lin and Chen 2021). Through Langmuir fitting, the maximum adsorption capacities ( $q_{\max}$ ) of the three LDHs were determined as 29.29 mg/g, 56.29 mg/g, and 87.23 mg/g, respectively. The adsorption capacity of LDH-4 was 2.98 and 1.55 times higher than LDH-2 and LDH-3, confirming a positive effect can be achieved by increasing the molar ratio of Mg to La during Mg-La LDH synthesis. Additionally,  $R_L$  in the Langmuir model was calculated as 0.238, 0.371, and 0.003 for each LDH sample respectively, all of them were between 0 and 1. These indicated that phosphate could be effectively adsorbed onto LDHs and the adsorption was mainly chemisorption, which was consistent with the conclusions from kinetic results. These findings also suggested the favorability of the sorption process and implied a strong binding between Mg-La LDH and P (Wakejo et al. 2024). Moreover, a more representative value,  $q_{0.5}$ , which described the P adsorption capacity of the adsorbents with equilibrium P concentration at 0.5 mg/L, was calculated based on the Langmuir isotherm. The calculated values were 4.04, 4.41, and 81.96 mg/g, for LDH-2, LDH-3, and LDH-4, respectively. The obtained  $q_{0.5}$  value of LDH-4 was 20.29 and 18.59 times that of LDH-2 and LDH-3. These results confirmed the superior performance of LDH-4 over others in the potential applications of real wastewater.

To compare the maximum phosphate adsorption capacity of the Mg-La LDH under study, Table 4 presented these data with the maximum phosphate adsorption capacity by researchers who investigated the removal of P using different LDHs. The results demonstrated that there was a great potential for LDH adsorbents to enhance phosphate adsorption by using La as the component metal in LDH synthesis.

## Effect of pH

During the adsorption process, pH is the most important factor that affects the adsorption performance. The pH condition not only determines the predominant phosphate species in the solution but also affects the surface charge of the adsorbent. Therefore, the effect of initial pH conditions was investigated in this study.

As shown in Fig. 7, the adsorption effects of the three LDHs were all affected by pH, wherein a decrease in adsorption capacity with increasing pH within the range of 3 to 11 could be observed. Notably, the adsorption effects of LDH-2 and LDH-3 showed a higher sensitivity to pH change compared to LDH-4. Compared to alkaline conditions, the adsorption performance under acidic conditions of LDH-2 and LDH-3 was considerably better. This was mainly due to the poor crystallinity or malformation of the metal hydroxide layer. All of them would lead to the weakening of LDH ion exchange capacity. The adsorption effect of LDH-2 and LDH-3 were significantly influenced by solution pH also due to the higher difficulty for  $\text{CO}_3^{2-}$  anions in the LDH layer to undergo ion exchange compared to  $\text{OH}^-$ . It was further demonstrated that the performance of LDH synthesized at the Mg/La ratio of 4:1 exhibited superior performance. The adsorption efficiency of LDH-4 exhibited a slight decline with increasing pH. At pH 7.5, the predominance of  $\text{H}_2\text{PO}_4^-$  in the solution shifted towards  $\text{HPO}_4^{2-}$ , which was unfavorable for ion exchange with LDH (Ashekuzzaman and Jiang 2017). Moreover, as the pH increased, the positive surface charge of the adsorbent gradually diminished. When  $\text{pH} > \text{pH}_{\text{pzc}}$  was applied, the surface of the adsorbent became negatively charged and produced electrostatic repulsion with phosphate ions (Jiang et al. 2019). The slight decrease in the adsorption effect also indicated that electrostatic attraction is not the main adsorption mechanism of LDH-4.

## Effect of co-existing anions

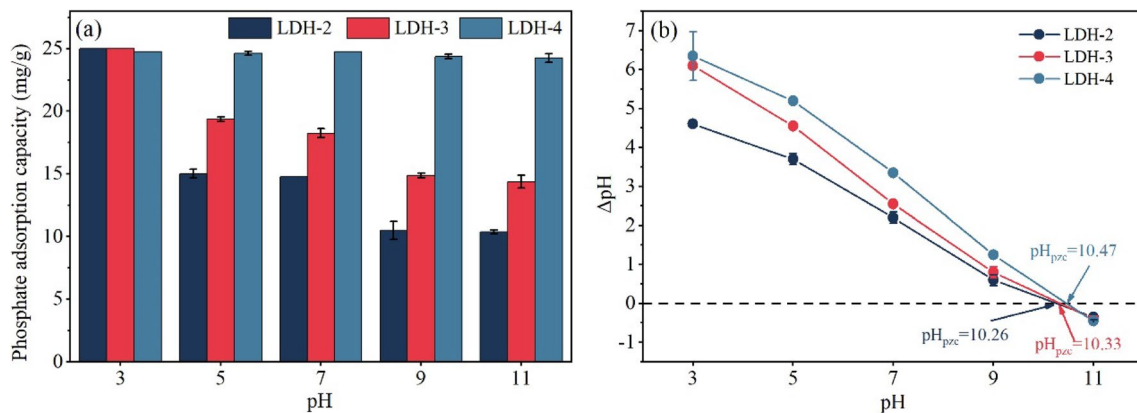
The presence of co-existing anions has been demonstrated to result in competition with phosphate for active sites,

**Table 3** Fitting parameters of isotherm models for phosphate adsorption by Mg-La LDH in wastewater

Adsorbent	Langmuir				Freundlich		
	$q_m$ (mg/g)	$K_L$ (L/mg)	$R_L$	$R^2$	$K_F$ (mg/g)	$n$	$R^2$
LDH-2	29.29	0.32	0.238	0.995	14.57	6.19	0.898
LDH-3	56.29	0.17	0.371	0.974	17.87	3.79	0.954
LDH-4	87.23	31.09	0.003	0.991	64.69	9.89	0.781
LDH-Al	36.46	0.12	0.45	0.975	10.38	3.61	0.974
LDH-Fe	33.15	0.12	0.44	0.989	9.97	3.79	0.955

**Table 4** Comparison of phosphate adsorption capacity of the adsorbents applied in the present study and reported in the literature

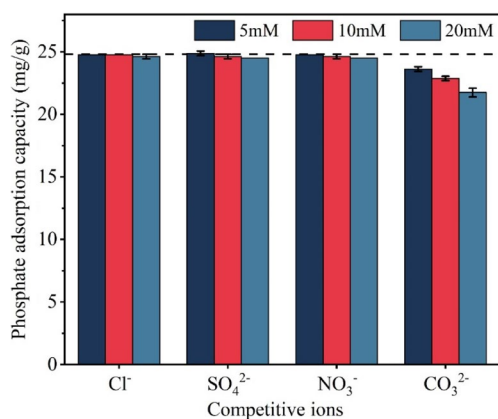
Absorbent	Reaction conditions	Maximum adsorption capacity of the adsorbent (mg/g)	References
LDH-2	Absorbent dosage: 0.4 g/L Initial concentrations: 10–100 mg/L	29.29	This study
LDH-3	Absorbent dosage: 0.4 g/L Initial concentrations: 10–100 mg/L	56.29	This study
LDH-4	Absorbent dosage: 0.4 g/L Initial concentrations: 10–100 mg/L	87.23	This study
Mg-Al-CO <sub>3</sub> LDH-Chitosan composite	Absorbent dosage: 0.3 g/L Initial concentrations: 10–120 mg/L	106.35	(Isidoro Ribeiro et al. 2023)
Mg-Al-CO <sub>3</sub> LDH	Absorbent dosage: 0.3 g/L Initial concentrations: 10–120 mg/L	54.9	(Isidoro Ribeiro et al. 2023)
Mg-Al-CO <sub>3</sub> LDH	Absorbent dosage: 0.1 g/L Initial concentrations: 0.5–10 mg/L	31.3	(Yang et al. 2014)
Mg-Fe-LDH/BC	Absorbent dosage: 0.5 g/L Initial concentrations: 5–80 mg/L	50.6	(Zhang et al. 2021a)
Mg-Al-LDH/BC	Absorbent dosage: 0.5 g/L Initial concentrations: 5–80 mg/L	35.2	(Zhang et al. 2021a)
F-LDH	Absorbent dosage: 0.5 g/L Initial concentrations: 5–80 mg/L	58.8	(Feng et al. 2022a)
O-LDH	Absorbent dosage: 0.5 g/L Initial concentrations: 5–80 mg/L	36.8	(Feng et al. 2022a)

**Fig. 7** (a) Effect of solution pH on adsorption and (b) measurement of  $pH_{pzc}$ 

either through electrostatic attraction or complex formation, thereby influencing the adsorption process of adsorbents. Based on the aforementioned analysis, LDH-4 exhibited superior performance and was chosen for further investigations.

As given in Fig. 8, the effect of different co-existing anions on P adsorption onto LDH-4 was revealed. The presence of  $Cl^-$ ,  $NO_3^-$ , and  $SO_4^{2-}$  had minimal influence on phosphate adsorption, whereas  $CO_3^{2-}$  had a significant impact on the adsorption. The presence of  $CO_3^{2-}$  in water altered the solution pH, causing the pH to rise and

resulting in a decrease in the adsorption performance of LDH. Furthermore, anions would be enriched at the surface of the adsorbent through electrostatic interaction and then formed complexes where the co-existing anions and phosphates competed for positive attachment sites (Li et al. 2021a). Therefore,  $CO_3^{2-}$  had a strong binding ability that affects the adsorption effect of LDH on phosphates. However, even when the concentration of  $CO_3^{2-}$  reached 20 mM, only a marginal decrease (12.30%) in phosphate removal capacity was observed. These findings demonstrated that LDH-4 displayed a remarkable selectivity



**Fig. 8** Effects of co-existing anions with different concentrations on the adsorption of phosphate

towards phosphate and was particularly suitable for real wastewater treatment.

### Study on desorption regeneration of the LDHs

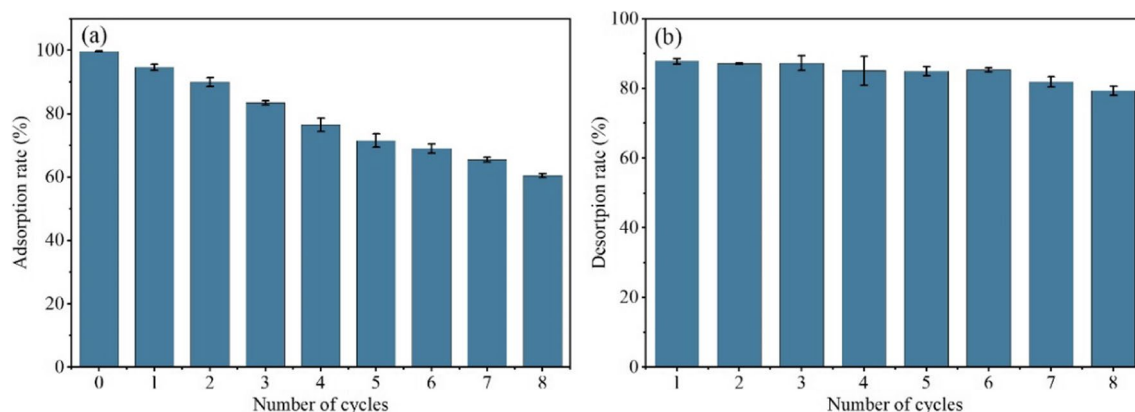
The recycling performance of adsorbents is an important parameter to evaluate its potential in real wastewater treatment, as it can significantly reduce the costs in practical applications. In this study, 1 M Na<sub>2</sub>CO<sub>3</sub> solution was used for regeneration. The adsorbed LDH was placed into a conical flask containing eluent and regenerated for 2 h at 25 °C to release pollutants and then used to remove phosphate. As illustrated in Fig. 9, it was observed that the utilization of 1.0 M Na<sub>2</sub>CO<sub>3</sub> for desorption resulted in a desorption efficiency exceeding 80%. After 8 sorption-desorption cycles, the phosphorus removal efficiency decreased from 99.65 to 60.50%. The decrease in adsorption capacity may be related to the presence of an irreversible active adsorption site, specifically the strong complexation between metal cations and phosphates during the

regeneration process (Zhang et al. 2021a; Wu et al. 2019). Under adsorption conditions, phosphate was adsorbed by ion exchange and complexation mechanisms. During the desorption process, excess CO<sub>3</sub><sup>2-</sup> would diminish the affinity between Mg-La LDH and phosphate, facilitating the successful release of the phosphate. Specifically, P adsorbed through ion exchange could be effectively desorbed using Na<sub>2</sub>CO<sub>3</sub>, while P removed via complexation exhibited a higher resistance to desorption. Several cycle experiments showed that the adsorption rate remained at 60.50% and the desorption efficiency remained above 80%, thereby fully indicating that the Mg-La LDH prepared in this study had excellent recycling ability.

### Adsorption mechanism

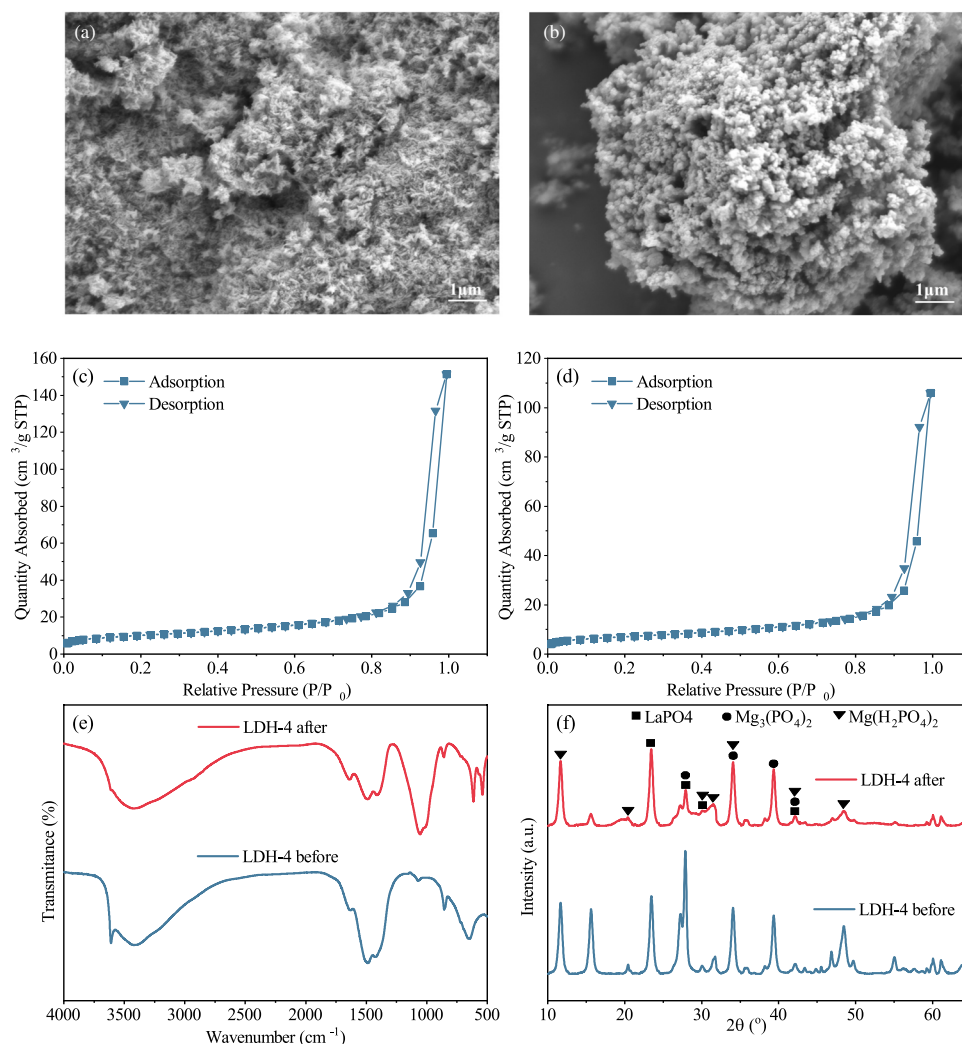
The SEM images of Mg-La LDH before and after adsorption are presented in Fig. 10 (a, b). After phosphate adsorption (Fig. 10b), the structure of Mg-La LDH remained intact while the surface smoothness decreased. Additionally, crystal characteristics became evident on the surface and the number of pores decreased, which could be attributed to phosphorus adsorption on the LDH surface.

The N<sub>2</sub> adsorption/desorption isotherm of Mg-La LDH before and after adsorption is shown in Fig. 10 (c, d), respectively. The isotherm was typical type IV, and the hysteresis loop was type H3, which was characteristic of mesoporous materials (Liu et al. 2019; Burtch et al. 2014). The results indicated that Mg-La LDH had a layered structure and the typical fissure pores were formed by the aggregation of nanoplates. The specific surface area of Mg-La LDH decreased from 134.01 to 87.11 m<sup>2</sup>/g, and the total pore volume decreased from 0.23 to 0.16 cm<sup>3</sup>/g. This was because P was adsorbed on the surface of the adsorbent and complexed with LDH metal ions, resulting in partial pore blockage on the surface. It was further proved that more adsorption sites



**Fig. 9** Changes of adsorption rate (a) and desorption rate (b) in the recycling of phosphate adsorption by LDH

**Fig. 10** SEM images of Mg-La LDH (a) and Mg-LDH+P (b), the  $N_2$  adsorption-desorption isotherm of Mg-La LDH (c) and Mg-La LDH+P (d), and FTIR spectra (e) and XRD patterns (f) of Mg-La LDH and Mg-La LDH+P



provided by high specific surface area and pore volume were conducive to the improvement of adsorption capacity.

The FTIR spectra (Fig. 10e) confirmed the involvement of inner-sphere complexation in the adsorption process. The disappearance of OH on the surface of Mg-La LDH at  $3698\text{ cm}^{-1}$  indicated the ion exchange between Mg-La LDH and phosphate in solution. Apart from the -OH group on the surface, the hydroxide and carbonate ions within the interlayer also participated in the phosphate adsorption in the form of ion exchange. The weakening or disappearance of hydroxyl at  $1439\text{ cm}^{-1}$  and carbonate vibrations at  $856\text{ cm}^{-1}$  could prove that they were involved in ion exchange processes. Additionally, a significantly weakened intensity was observed for M-O and M-O-M (M represents Mg or La) bands on the adsorbed LDH at  $651\text{ cm}^{-1}$ , indicating that functional groups associated with M-O and M-O-M participated in the adsorption mechanism (Wu et al. 2018). A new band at  $1053\text{ cm}^{-1}$  corresponded to the  $\nu_3$  stretching vibration of phosphate and  $538\text{--}614\text{ cm}^{-1}$  corresponded to the bending vibration of P-O ( $\nu_4$ ), confirming the formation

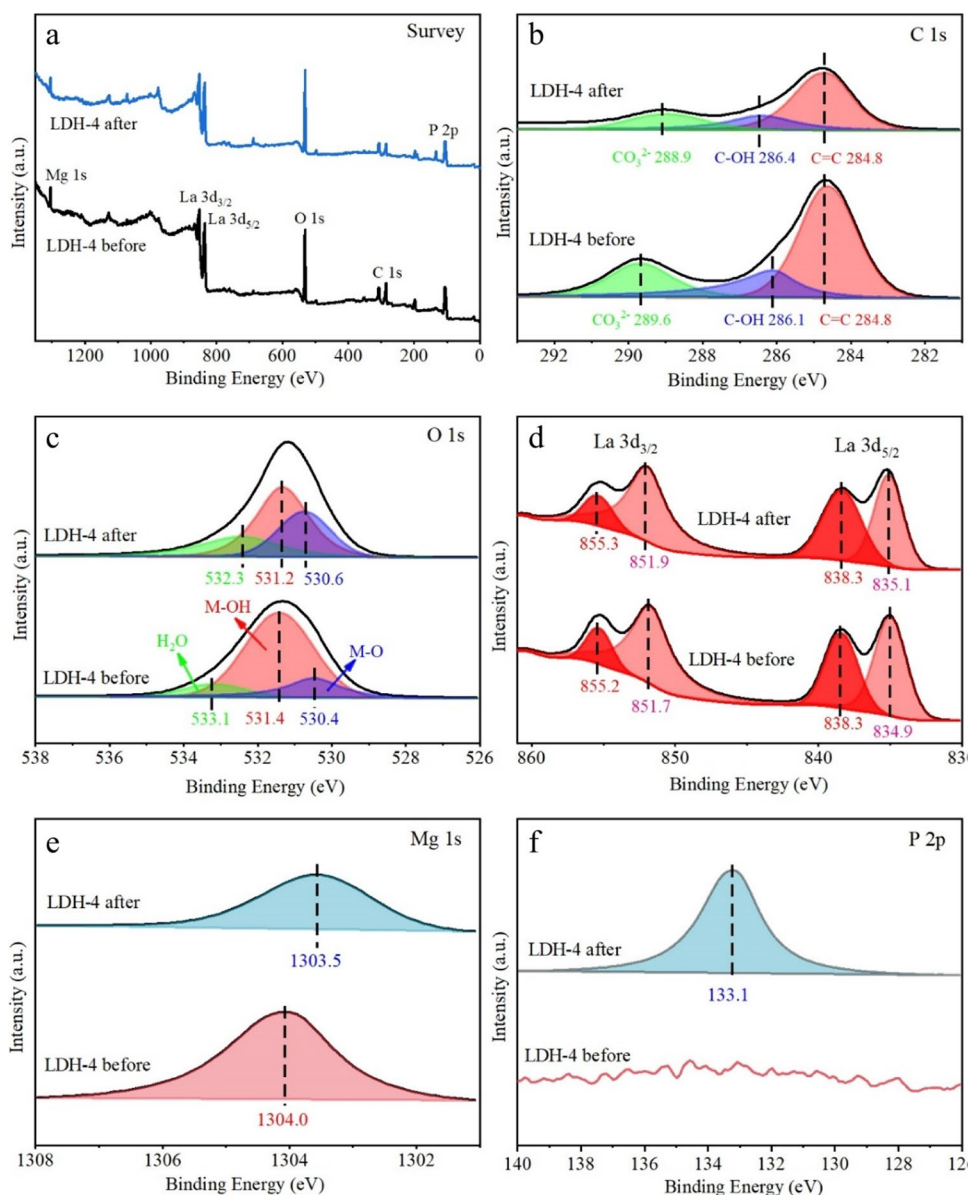
of M-O-P spherical complexation on the surface of Mg-La LDH (He et al. 2015; Li et al. 2023).

The XRD pattern of Mg-La LDH before and after adsorption is shown in Fig. 10f. The XRD patterns also demonstrated the role of ion exchange and inner-sphere complexation in adsorption. The high similarity of the main diffraction peaks of Mg-La LDH before and after adsorption indicated that the main crystal structure of LDH barely changed after adsorption. However, the diffraction peaks associated with Mg-La LDH after adsorption exhibited varying degrees of shift towards lower angles, which was due to the anion exchange between the interlayer anions and phosphate ions (Feng et al. 2022a). The movement of  $2\theta$  to a smaller angle also indicated that the Mg-La LDH surface spacing increased after phosphate adsorption. The adsorbed Mg-La LDH is roughly matched with the crystalline phases associated with metal-bound phosphates (LaPO<sub>4</sub>, Mg(H<sub>2</sub>PO<sub>4</sub>)<sub>2</sub>, Mg<sub>3</sub>(PO<sub>4</sub>)<sub>2</sub>), which indicated the inner-sphere complexation between M-OH and phosphates on the surface of Mg-La LDH.

In order to further clarify the adsorption mechanism of Mg-La LDH on phosphate, XPS analysis of LDH before and



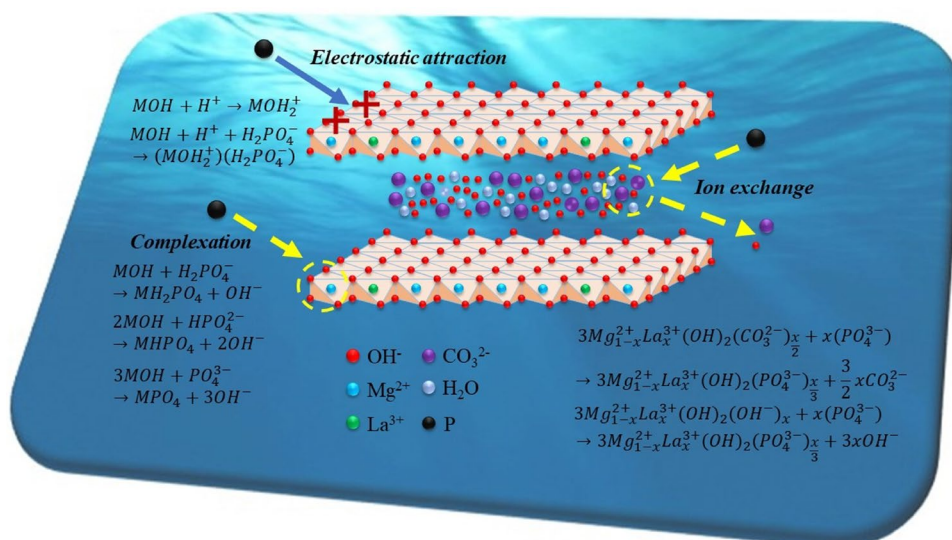
**Fig. 11** XPS spectra of Mg-La LDH before and after adsorption: (a) XPS survey, (b) C 1s, (c) O 1s, (d) La 3d, (e) Mg 1s, and (f) P 2p



after adsorption was performed, and the results are shown in Fig. 11. Initially, four elements (Mg, La, C, O) were found in the survey scan of Mg-La LDH in Fig. 11a and an obvious P 2p peak appeared at approximately 133.1 eV after adsorption, indicating that phosphate was successfully adsorbed in LDH. The C 1s spectrum (Fig. 11b) was deconvoluted into three peaks at 284.6 eV, 286.1 eV, and 289.6 eV corresponding to C-C, C-OH, and  $\text{CO}_3^{2-}$ , respectively. The proportion of  $\text{CO}_3^{2-}$  in total C 1s was significantly reduced after the adsorption process, which further indicated that  $\text{CO}_3^{2-}$  intercalation anion participated in phosphate adsorption. The convolution results of XPS O 1s spectra in Mg-La LDH are shown in Fig. 11c. Based on different forms of oxygen species, it can be divided into three peaks, M-O, M-OH, and  $\text{H}_2\text{O}$  (Xu et al. 2017). Among these peaks, M-O (530.4 eV) primarily

corresponded to La-O and Mg-O bonds in the Mg-La LDH lattice, while M-OH (531.4 eV) is mainly related to Mg-OH and La-OH groups. The hydroxyl density of Mg-La LDH decreased significantly after phosphate adsorption, which further confirmed the interaction between phosphate and hydroxyl oxygen. Moreover, the energy position of La  $3d_{3/2}$  and La  $3d_{5/2}$  shifted by 0.2 eV after phosphate adsorption. The peak shift towards higher energy can be attributed to the transfer of electrons from the valence band of the ligand atom to the La atom's 4f orbital, suggesting the formation of a new P complex with La (Qu et al. 2020; Koh et al. 2020). In addition, there was a 0.5 eV shift towards lower binding energy in the Mg 1s XPS peak of Mg-La LDH, indicating that the adsorption site was extracted from the negatively charged phosphate O resulting in electron density (Gupta et al. 2020).

**Fig. 12** Schematic diagram of possible phosphate adsorption mechanism of Mg-La LDH



According to the experimental results and characteristics mentioned above, three main mechanisms for the adsorption of phosphate by Mg-La LDH can be identified: (1) electrostatic attraction between phosphate and Mg-La LDH, (2) exchange of hydroxyl ions or carbonate ions between phosphate and Mg-La LDH, and (3) binds between phosphate and Mg-OH or La-OH to form monodentate complexes or bidentate complexes. The proposed mechanism is summarized in the Fig. 12.

## Conclusion

A novel layered double hydroxide (LDH) with desirable characteristics and excellent performance in the removal of P from aqueous solutions was prepared using Mg and La as metal cations in this study. The optimum synthesis parameters of Mg-La LDH were obtained as follows: Mg:La = 4:1, synthesis temperature of 80 °C, synthesis pH of 10, and synthesis time of 10 h. The results of FTIR and XRD analysis confirmed that the Mg:La = 4:1 ratio was more favorable to crystal nucleation and growth, and Mg-La LDH with higher crystallinity could be synthesized. The adsorption kinetic study showed that 90% of the adsorption process of LDH-4 could be completed within the initial 60 min. The isotherm study showed that the maximum adsorption capacity of LDH-4 was 87.23 mg/g, and the adsorption capacity could reach 81.96 mg/g while only 0.50 mg/L of P remained in the solution, which was higher than most binary LDH adsorbents. The adsorption process was better fitted by the pseudo-second-order kinetic model and Langmuir model, indicating that the adsorption was a single-layer adsorption process dominated by

chemisorption. The adsorption mechanism of P primarily includes electrostatic adsorption, ion exchange, and inner-sphere complexation. Due to the higher crystallinity and more complete structure of LDH-4, the adsorption of P was less affected by pH and different co-existing anions. Mg-La LDH regeneration experiment showed that even after undergoing eight repeated cycles of use, the phosphorus removal efficiency and desorption efficiency remained above 60.5% and 80%, respectively. In conclusion, Mg-La LDH exhibited significant potential for efficient phosphate adsorption in water treatment applications.

**Author contribution** Yanming Xu: conceptualization, methodology, investigation, formal analysis, visualization, and writing—original draft. Yue Yin: conceptualization, investigation, formal analysis, and writing—review and editing. Ya-Nan Luan: writing—review and editing. Qing Wang: Investigation, Methodology. Zhuo Zhao: Investigation, Methodology. Zhonghong Guo: Investigation, Methodology. Changqing Liu: supervision, funding acquisition, resources, writing—review and editing, and project administration.

**Funding** This study was funded by the Project of Qingdao Science and Technology Benefiting People Program (23-2-7-zdfn-2-nsh).

**Data availability** The data that support the findings of this study are available on request from the corresponding author, Changqing Liu.

## Declarations

**Ethical approval** This study does not violate any ethical rules.

**Consent to participate** All authors agree to participate.

**Consent for publication** All authors agree to publish the article.

**Competing interests** The authors declare no competing interests.

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