RESEARCH ARTICLE

Energy based techno‑economic and environmental feasibility study on PV/T and PV/T heat pump system with phase change material—a numerical comparative study

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Received: 22 July 2023 / Accepted: 12 January 2024 / Published online: 1 February 2024 © The Author(s), under exclusive licence to Springer-Verlag GmbH Germany, part of Springer Nature 2024

Abstract

A sustainable, afordable, and eco-friendly solution has been proposed to address water heating, electricity generation, space cooling, and photovoltaic (PV) cooling requirements in scorching climates. The photovoltaic thermal system (PV/T) and the direct expansion PV/T heat pump (PV/T DXHP) were numerically studied using MATLAB. A butterfy serpentine fow collector (BSFC) and phase change material (PCM) were assimilated in the PV system and MATLAB model was developed to evaluate the economic and enviroeconomic performance of the PV/T water system (PV/T-W), PV/T PCM water system (PV/T PCM-W), the PV/T DXHP system, and the PV/T PCM heat pump system (PV/T-PCM-DXHP). In this study, annual energy production, socioeconomic factors, enviro-economic indicators, and environmental characteristics are assessed and compared. Also, an economic, environmental, and enviro-economic analysis was conducted to assess the commercial viability of the suggested system. The PV/T PCM-DXHP demonstrated the highest electrical performance of 53.69%, which is comparatively higher than the other three confgurations. The discounted levelized cost of energy (DLCOE) and payback period (DPP) of the PV/T PCM-DXHP were ₹2.87 per kW-h and 3–4 years, respectively, resulting in a total savings of ₹67,7403 over its lifetime. Furthermore, installing this system mitigated 280.72 tonnes of $CO₂$ emissions and saved the mitigation cost by ₹329,700 throughout its operational lifecycle.

Keywords Solar PV · PV/T · Heat pump · Energy · COP · PCM · Economic · Environmental

Introduction

Among the renewable energy (RE) sources, solar energy (SE) is a precious resource with great potential for addressing India's energy defcit. India's solar PV energy generation capacity is less than 6.5% (Rauf et al. [2023](#page-19-0)). India's primary objective in the feld of energy is to give the most priority to energy conservation, energy efficiency, and the effective use of RE resources (Kaleshwarwar and Bahadure [2023](#page-19-1)). Solar energy has the ability to encounter the mounting energy demand in India (Gielen et al. [2019\)](#page-19-2). India's mammoth land area receives signifcant SE, estimated at 5000

Responsible Editor: Philippe Garrigues

 \boxtimes Prakash K. Babu kbprakash404@gmail.com trillion kW-h annually. India receives a daily average solar irradiation between 4 and 7 kW-h per m^2 of SE (Batool et al. [2023](#page-18-0)). Solar PV offers scalability, allowing for the deployment of solar energy systems at various capacities to meet the energy requirements of India (Bhanja and Roychowd-hury [2023\)](#page-18-1) and it contributes to mitigating climate change. The cultivation of SE is the only option to meet the target of the Paris agreement by reducing the annual reduction of 1.5 °C in ambient temperature (Fawzy et al. 2020). Further, this system mitigates the gases CO_2 , SO_2 , No_x , PM_2 , and PM_{10} which contribute to greenhouse gas emissions (Jäger-Waldau et al. [2020](#page-19-4); Kazem et al. [2023\)](#page-19-5). In addition to this pledge, India focuses on installing net zero energy in newly constructed buildings and almost energy-free buildings that get all the power they need from the sun, wind, or other RE resources. However, since solar PV productivity is so low, the practical utilization of SE in the power system is less than 10% (Dubey et al. [2013](#page-19-6); Alharbi and Kais [2015\)](#page-18-2). Therefore, hybrid PV/T-W systems have gained popularity recently because they combine the PV and solar

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water heating systems into a single module (Emmanuel et al. [2021](#page-19-7)). The PV system converts the SE into usable electricity and heat through photovoltaic and thermal conversion (Obalanlege et al. [2020](#page-19-8)). However, because of the incorporated thermal unit, the price of PV/T-W is signifcantly greater than traditional PV (Abdul Jabar et al. [2023](#page-18-3)). Hence, a cost–beneft analysis is needed to fgure out how benefcial these systems are in real life. Also, it is essential to identify the environmental benefts to society (Beniwal et al. [2023](#page-18-4)).

The PV/T-W systems, in particular, can breed power and hot water to the buildings (Sharaf et al. [2022\)](#page-19-9). Kalogirou and Tripanagnostopoulos ([2007\)](#page-19-10) evaluated the PV/T-W system, proving it saved more cost than the reference uncooled PV. Herrando and Markides ([2016](#page-19-11)) investigated an economic analysis of the PV/T-W, and it reduced the life cycle cost of energy (LCOE) and mitigated the $CO₂$ but with a higher capital cost for UK climatic conditions. Tse et al. ([2016\)](#page-19-12) studied an energy and economic analysis of the PV/T-W system in Hong Kong. They discovered the superiority of PV/T-W panels, which have a shorter payback period and higher performance efficiency due to using the panels' waste heat. Similarly, Canelli et al. [\(2015](#page-18-5)) performed a simulation in Italy on the same system and reduced 36.2% and 28.4% of $CO₂$ emissions and operating costs, respectively. Bianchini et al. [\(2017\)](#page-18-6) analyzed the PV/T-W system and found that LCOE is lower than the country's energy cost. PCMs are also employed to cool the PV system, and storing the excess heat from the PV panel rose the overall efficiency, decreasing the life cycle cost and $CO₂$ destruction (Lamba et al. [2023\)](#page-19-13). Hossain et al. ([2019\)](#page-19-14) conducted an experimental study in Malaysian climatic conditions on the PV/T PCM system and revealed that incorporating PCM increases thermal and electrical efficiency. The assimilation of PCM in the PV/T PCM system increased the life of the system. Cui et al. ([2022](#page-18-7)) invented that a PV/T system equipped with PCM has a 6 years shorter payback period, and is more economically viable than a PV/T system. The integration of PCM in the PV/T system saved the annual cost by 15% to 20%. The absence of adequate indulgence on the practicality and benefts of PVT-W and PV/T PCM-W has hindered the commercialization of PV/T PCM and water technologies. As a result, there is a growing amount of literature on employing heat pumps as a cost-efective and ecologically sound means of augmenting the thermal output of PV/T systems (Obalanlege et al. [2020\)](#page-19-8).

A hybrid PV/T HP system is additionally used for PV cooling, water heating, and space cooling. This technology lowered the PV temperature, boosting the system's power conversion efficiency, heating value, and COP (Miglioli et al. [2021](#page-19-15)). Obalanlege et al. ([2020](#page-19-8)) executed a fnancial analysis on PV/T HP and reported that the system's payback period increases while increasing the system's cooling capacity. Obalanlege et al. [\(2022\)](#page-19-16) steered an economic and environmental analysis of the PV/T HP system under UK climatic conditions and reported that the recurring cost of the proposed system is low and destroys $CO₂$ by 610 kg annually throughout its lifetime. Zhang et al. ([2014\)](#page-20-0) investigated the socio-economic assessment of the IE PV/T HP system with a loop heat exchanger. They found that it is economically suitable for London's climatic conditions and environmentally most suitable for Shang-hai's climatic conditions. Liu et al. [\(2023](#page-19-17)) have done performance analysis and found the optimum design confguration for the PV/T-DXHP system. Abbas et al. [\(2023\)](#page-18-8) analyzed the PV/T-DXHP systems via MATLAB and reported a maximum COP of 5.68, and its payback period was 7.15 years. Most of the research was focused on the indirect expansion of hybrid PV/T HP systems (Liu et al. [2020](#page-19-18)) rather than the direct expansion of the PV/T HP system due to its lack of control in the heat load and refrigerant leakage issues (Dannemand et al. [2019,](#page-18-9) [2020](#page-18-10)).

Though many research works on PV/T-W and PV/T DXHP systems have been conducted, there is a scarcity of studies examining the energy-based economic and environmental analysis specifcally for these systems using hydrated salt PCM in hot Indian climate conditions. The novelty of this current work lies in the design and development of a new thermal collector/evaporator based on a butterfy serpentine fow confguration, and incorporating hydrated salt (HS36) PCM in the PV system for PV cooling, water heating, and space cooling applications. The numerical studies were carried out by assimilating the BSF collector and HS36 PCM in the PV system and their impact on annual energy production was found using MATLAB. Furthermore, this study aims to compare the commercial viability of PV/T systems and PV/T-DXHP systems in Indian buildings, specifcally focusing on energy, economic, and environmental characteristics in hot climatic regions of India. Various factors are considered in the comparison, including total electrical and thermal energy generation, discounted net present value (DNPV), discounted payback period (DPP), levelized cost of energy (DLCOE), as well as the quantities of CO_2 , SO_2 , NO_x , and PM_{10} mitigated, along with cost savings. The study aims to propose an economically and environmentally feasible system for Indian climatic conditions. By examining and comparing these aspects, the study wishes to deliver valuable insights into the performance and viability of PV/T-W, PV/T-PCM-W, PV/T-DXHP, and PV/T PCM-DXHP systems, ultimately recommending a system that is economically and environmentally suitable for the specifc climatic conditions found in India.

System description

The research involved in fnding the annual energy generation with a designed novel thermal collector and HS 36 PCM and predicting the economic and environmental

Fig. 1 Pictorial representation of Butterfy Serpentine Flow Profle

viability of the following systems. The annual energy analysis is simulated in MATLAB for the following five different confgurations: PV, PV/T with water as the working fuid (PV/T-W), PV/T with phase change material (PCM) energy storage and water as the working fuid (PV/T PCM-W), PV/T with a direct expansion heat pump (PV/T DXHP), and PV/T with PCM energy storage and a direct expansion heat pump (PV/T-PCM-DXHP). Figure [1](#page-2-0) provides a visual representation of the butterfy serpentine fow profle used in these PV/T confgurations (Prakash and Amarkarthik [2023](#page-19-19)),

which was integrated into PV and made as case-1 (PV/T-W), case-2 (PV/T PCM-W), case-3 (PV/T DXHP), case-4 (PV/T-PCM-DXHP), and case-5 (uncooled PV–basic standard PV system). These system configurations are shown in Table [1.](#page-2-1)

Earlier studies have explored designs such as parallel, concentric, web spiral, bionic, and serpentine fow copper coils placed underneath PV/T panels (Poredoš et al. [2020](#page-19-20)). The butterfy serpentine fow collector (BSFC) pattern is a design that resembles the shape of a butterfy and is used in the PV/T collector. Figure [1](#page-2-0) demonstrates the design of the PV/T collector, while Fig. [2](#page-2-2) portrays the diferent layers of the PV/T and PV/T PCM collectors used for the simulations. Hydrated salt (HS36) is selected as PCM to maintain thermal stability and enhance the cooling of the PV panel. The PCM helps control the temperature of the PV panel, when the melting temperature of the PCM is around 3 \degree C to 6 \degree C higher than the ambient temperature (Waqas and Jie [2018](#page-20-1); Velmurugan et al. [2021\)](#page-20-2).

$$
m_{PCM} = \frac{Q_{ch}}{Q_{LH-pcm} + \int_{i}^{m} C_{ps}(T)dT + \int_{m}^{f} C_{pl}(T)dT}
$$
 (1)

The simulation setup of the proposed system is shown in Fig. [3](#page-3-0) a and b. In this system, solar energy is incident upon the PV/T thermal system's panels. In the PV/T system, a water tank is a storage unit where water is pumped to the panel. This water tank acts as a reservoir to store the heat,

which is recovered from the system. In the PV/T DXHP system, a heat pump is employed to circulate refrigerant instead of water. The compressor extracts the refrigerant from the PV/T evaporator and increases its pressure to that of the condenser. As the refrigerant fows into the condenser tank, it transfers heat to the water in the tank. The pressure of the refrigerant signifcantly decreases as it passes through the expansion valve. In the meantime, the liquid refrigerant enters the PV/T evaporator, which contributes to the PV system's cooling by absorbing heat from the panels. Ultimately, the PV/T heat pump system cools the photovoltaic panels and heats the water.

The place chosen for the simulation study is located at the coordinates of 11.4963° N, 77.2769° E, in Sathyamangalam, Tamilnadu, India. The average temperature of this feld is around 31 °C, the average wind speed is 6.5 m/h,

Fig. 3 a Schematic line diagram of the PV/T DXHP setup. **b** Schematic line diagram of the PV/T-W and PV/T PCM-W setup

air mass (AM) is 1.5, and the average relative humidity is 66%. The sun shines up to 5.8 h/day and the topography is close to the Western Ghats and the Bhavanisagar dam. In this study, the inclination of the PV was kept at 11.5° south. The latitude of the location chosen sets the angle (β) of the PV/T panel (Muthu and Ramadas [2023\)](#page-19-21). For the numerical study, a polycrystalline PV panel with a capacity of 260 W is chosen. Table [2](#page-4-0) highlights the panel's most salient features of PV, PV/T, and PCMs used in this numerical work. Similarly, Table [3](#page-4-1) provides the technical details of the heat pump used in the system.

System simulation model

For the numerical study, a polycrystalline PV panel with a capacity of 260 W is chosen. Table [2](#page-4-0) highlights the panel's most salient features. It is presumed that the panel functions in conditions that are consistent with a steady state. This assumption is reasonable because the temporal fuctuations of the boundary conditions are relatively slow compared to the dynamic response of the panel (Guarracino et al. [2016](#page-19-22)).

Table 2 Technical parameters of PV module and PCM

Parameters	Nomenclature	Value	Unit
PVGC thickness	δ_c	1	mm
PVGC emissivity	ε_c	0.84	$[-]$
PVGC transmissivity	$\tau_{\rm c}$	0.9	$[-]$
SC thickness	$\delta_{\rm pv}$	0.3	mm
SC emissivity	$\varepsilon_{\rm pv}$	0.96	$[-]$
SC absorbance	$a_{\rm pv}$	0.85	$[-]$
SC thermal conductivity	K_{pv}	203	$W/m \,^{\circ}C$
Reference SC electrical efficiency	η_{std}	16.0	%
SC temperature coefficient at SSC	β_{sc}	0.031	$\%$ /°C
SC temperature coefficient at VOC	$\beta_{\rm oc}$	-0.390	%/°C
SC temperature coefficient at FF	$\beta_{\rm ff}$	-0.166	$\%$ \degree C
Standard SC's SSC	$I_{\rm ref,sc}$	9.030	A
Standard SC's VOC	$V_{\text{ref,oc}}$	0.657	V
Standard SC's FF	FF_{ref}	0.820	$[-]$
No SC in the PV system	n	60	$[-]$
Tadlar absorbance	a _h	0.8	$[-]$
EVAG thickness	$\delta_{\rm FVA}$	0.5	mm
EVAG thermal conductivity	k_{EVA}	0.311	$W/m \cdot C$
Packing factor	$\beta_{\rm pv}$	0.9	$[-]$
PV/T module area	A	1.66	m ²
Aluminium sheet thickness	$\delta_{\rm rh}$	0.8	mm
Refrigerant type	ref	R410a	$[-]$
Melting point	$T_{\rm m}$	$^{\circ}C$	36.0
Freezing point	$T_{\rm fz}$	$^{\circ}C$	35.0
Latent heat	$Q_{\text{LH-pcm}}$	kJ/kg	166

Table 3 Parametric description of the DXHP system

PV/T system model

Equations (2) (2) , (3) (3) , (4) (4) , (5) (5) , (6) (6) , (7) (7) , (8) (8) , and (9) (9) express the glass cover model, PV model, heat absorber, Piping model, bonding model, working fuid model, insulation model, aluminium plate models (Obalanlege et al. [2022](#page-19-16)), and PCM models (Yang et al. [2019\)](#page-20-3).

$$
G\alpha_{g} = (h_{v,g-a} + h_{ra,g-s})(T_{g} - T_{a}) + h_{d,g-pv}(T_{g} - T_{pv})
$$
 (2)

$$
I\tau_{g}\alpha_{pv}[1 - PA\eta_{ra}(1 - \beta(T_{pv} - T_{a}))]
$$

= $h_{d,g-pv}(T_{pv} - T_{g}) + h_{d,pv-abs}(T_{pv} - T_{abs})$ (3)

$$
h_{\rm d,pv-abs}(T_{\rm pv} - T_{\rm abs}) = h_{\rm d,abs-t}(T_{\rm abs} - T_{\rm t}) + h_{\rm d,abs-ig}(T_{\rm abs} - T_{\rm ig})
$$
\n(4)

$$
h_{\rm d,abs-t}(T_{\rm abs} - T_{\rm t}) = h_{\rm v,t-w}\left(T_{\rm t} - \overline{T}_{\rm w}\right) + h_{\rm d,t-ig}\left(T_{\rm t} - T_{\rm ig}\right) \tag{5}
$$

$$
h_{\mathbf{v},\mathbf{t}-\mathbf{w}}\left(T_{\mathbf{t}}-\overline{T}_{\mathbf{w}}\right)A=\dot{m}_{\mathbf{w},\mathbf{p}\mathbf{v}\mathbf{t}}c_{\mathbf{p}}\left(T_{\mathbf{w},\mathbf{out}}-T_{\mathbf{w},\mathbf{in}}\right)
$$
(6)

$$
h_{\rm d,abs-ig}(T_{\rm abs} - T_{\rm ig}) + h_{\rm d,t-ig}(T_{\rm t} - T_{\rm ig}) = h_{\rm d,ig-ip}(T_{\rm ig} - T_{\rm ip})\tag{7}
$$

$$
h_{\rm d,ip-al}(T_{\rm ip} - T_{\rm al}) = h_{\rm v, al-a}(T_{\rm al} - T_{\rm a})
$$
\n(8)

$$
\rho_{g-pcm} = \rho_{pcm} \left[1 - B_{pcm} \left(T_{pcm} - T_{ref} \right) \right] \tag{9}
$$

Equations (2) (2) (2) , (3) (3) (3) , (4) (4) (4) , (5) (5) (5) , (6) (6) (6) , (7) (7) (7) , and (8) are given as model equations in MATLAB and simulated by the procedure shown in Fig. [4](#page-5-0) a. The temperature of the PV module and the inlet and outlet temperatures of the water were found. Equation [\(10](#page-5-1)) was used to get the electrical efficiency (η_{el}) of a 260-W photovoltaic panel, and Eq. (11) (11) (11) was used to determine the thermal efficiency (η_{th}) of the PV/T system. Finally, Eqs. ([12](#page-5-3)), [\(13\)](#page-5-4), and [\(14\)](#page-5-5) (Yang et al. [2019\)](#page-20-3) were used to calculate the total heat and electrical power generated throughout the year using simulated data from MAT-LAB. The combined energy produced from the PV/T systems was calculated using Eqs. [\(12](#page-5-3)), [\(13](#page-5-4)), and [\(14\)](#page-5-5) (Gu et al. [2018\)](#page-19-23).

$$
\eta_{\rm el} = \eta_{\rm ref} \left[1 - \beta \left(T_{\rm PV} - T_{\rm ref} \right) \right] \tag{10}
$$

$$
\eta_{\text{th}} = \frac{\dot{m}_{\text{w,pvt}}c_{\text{p}}(T_{\text{out}} - T_{\text{in}})}{G \cdot A} \tag{11}
$$

$$
E_{pvt_t} = E_{dc_t} + E_{th_t},\tag{12}
$$

$$
E_{dc_{-}t} = (D_t \times G_t \times \eta_{dc} \times A_{dc})(1 - dg)^{t-1}
$$
 (13)

$$
E_{th_t} = (D_t \times G_t \times \eta_{th} \times A_{th})(1 - dg)^{t-1}
$$
 (14)

PV/T DXHP system model

Using MATLAB, the following Eqs. (15) (15) – (24) used to simulate the PV/T DXHP system and its simulation procedure are shown as a flow chart in Fig. [4](#page-5-0) b. Equations (15) (15) – (17) (17) are the energy balance equations used to model the compressor (Obalanlege et al. [2022\)](#page-19-16).

$$
\dot{m}_{k,r} = \omega_k V_k \rho_{k,r} \eta_k \tag{15}
$$

$$
\rho_{k,r} = f\left(P_{k,r}, h_{k,r}\right) \tag{16}
$$

Equation [\(17\)](#page-5-8) represents the condenser model (Zhou et al. [2019](#page-20-4)), which is derived based on enthalpy change in refrigerants.

$$
Q_{\text{cond}} = m_{\text{ref}} \left(h'_{\text{Con,out}} - h'_{\text{Con,in}} \right) = m_{\text{w}} C p_{\text{w}} \left(T_{\text{o}} - T_{\text{i}} \right) \tag{17}
$$

Equations (18) (18) – (21) (21) (21) show the solar PV/T evaporator models (Deng and Yu [2016\)](#page-19-24). Equation ([22](#page-6-0)) shows the expansion valve model.

$$
Q_{\rm e} = A_{\rm cl} [\alpha I_{\rm T} - U_{\rm Lc} (T_{\rm PV} - T_{\rm a})] = F I A_{\rm cl} [\alpha I_{\rm T} - U_{\rm Lc} (T_{\rm fm} - T_{\rm a})]
$$
(18)

$$
U_{\text{Lc}} = h_{\text{v}} + h_{\text{r}},\tag{19}
$$

$$
h_{v} = 2.8 + 3u_{w}
$$
 (20)

Fig. 4 a Flowchart of simulation methodology of case 2 system. **b** Simulation methodology of case 3 system

$$
h_{\rm r} = \varepsilon \sigma \left(T_{\rm p}^2 + T_{\rm a}^2 \right) \left(T_{\rm p} + T_{\rm a} \right) \tag{21}
$$

2 Springer

Fig. 4 (continued)

$$
h_{\rm c,r} = h_{\rm e,r} \tag{22}
$$

b

Equation (23) (23) mentions the thermal efficiency (η_{thHP}) of the PV/T HP system (Lu et al. [2019\)](#page-19-25).

$$
\eta_{\text{thHP}} = \frac{Q_{\text{cond}} - P_{\text{com}}}{A * G} \tag{23}
$$

Economic model

The techno-economic evaluation inside this work divides the system's initial cost of investment and implementation expenses (Ehyaei et al. [2019\)](#page-19-26). The system's initial investment cost is divided further into expenses for the components used and their corresponding installation charges. These prices were received from the dealer as quotes. Table [4](#page-7-0) shows the pricing and suppliers. The system's operational and servicing costs are included in the yearly expenses. The total combined cost (TCC) is the summation of all the costs a system has incurred over its lifetime. It is expressed in Eq. (24) (Coffey et al. [2016\)](#page-18-11). The annual cash flow (ACF) analysis is an excellent way to compute the annual economic result of the case 1 and 2 systems with the impact of discount rates (*r*) and infation rates (*i*). Discounted net present value (DNPV) calculates the current value of an investment by taking into account its overall value during its whole duration and adjusting for the time value of money. It is calculated using Eqs. (25) (25) and (26) (26) (Herbohn et al. [2002](#page-19-27)). The discounted payback period (DPP) indicates the

duration required for an investment to recoup its initial expenditure while considering the impact of the time value of money (Bhandari [2009;](#page-18-12) Rappaport [1965\)](#page-19-28). Similarly, levelized cost of energy (LCOE) replicates the lifecycle expense of the system per unit of electricity produced (Obalanlege et al. [2022\)](#page-19-16), which are expressed using Eqs. (27) – (29) . All the equations of economic and environmental models were given as input model to MATLAB and results were found.

$$
TCC_n = C_0 + C_{\text{grid}} + \sum_{n=1}^{tL} C_{0\&M}
$$
 (24)

$$
ACF = \sum_{n=1}^{tL} CF_n * \frac{(1+i)^n}{(1+r)^n}
$$
 (25)

$$
DNPV = -C_0 + \sum_{n=1}^{tL} CF_n * \frac{(1+i)^n}{(1+r)^n}
$$
 (26)

$$
DPP = \frac{\ln\left[\frac{C_0(i-r)}{C_s} + 1\right]}{\ln\left[\frac{1+i}{1+r}\right]}
$$
\n(27)

$$
C_s = E_{\text{produced}} + Q_{\text{produced}} - C_{0\&\text{M}}
$$
 (28)

$$
LCOE = \frac{C_0 + \sum_{n=1}^{tL} C_{0\&M} * (1+i)^{i-1} (1+r)^{-i}}{\sum_{n=1}^{tL} (E_{\text{produced}} + Q_{\text{produced}})(1+r)^{-i}} \tag{29}
$$

Environmental model

It is crucial to assess and compare the carbon emissions over the lifespan of power production systems that pose risks to public health to determine the level of tolerance for each cases. With aid of Eqs. (32) (32) and (33) (33) (33) , the annual $CO₂$ reduction and cost saving by mitigation of the proposed systems are calculated (Tiwari et al. [2015](#page-19-29)). The worldwide

Table 4 Price and supplier details of the components

Table 5 The details of the intensity and cost of pollutant mitigation (den Elzen et al. [2011](#page-19-32); Caliskan et al. [2012](#page-18-14))

Average equivalent intensity Components for standard coal		Mitigation cost	
CO ₂	2.493 kg/kg	1200 ₹/ton	
SO ₂	0.075 kg/kg	7500 ₹/ton	
NO_{x}	0.0375 kg/kg	45,000 ₹/ton	
PM_{10}	5.40 g/kg	52,000 ₹/ton	

carbon price ranges between 13 and 16 dollars per tonne of $CO₂$. As a result, the mean values of 14.5 \$/t $CO₂$ are used to calculate the environmental cost, provided in Eq. ([33\)](#page-7-7) (Rajoria et al. [2013\)](#page-19-30). Similarly, SO_2 mitigation (ϕ_{SO_2}), NO_x mitigation (ϕ_{NO_x}), and particulate matter ($\phi_{\text{PM}_{10}}$) mitigation and cost savings for this reduction are also calculated using Eqs. (32) (32) (32) and (33) (Amoatey et al. [2019](#page-18-13)). Table [5](#page-7-8) shows the details of the intensity and cost of pollutant mitigation.

$$
\phi_{\text{CO}_2} = \frac{\Psi_{\text{CO}_2} * E_{\text{overall}}}{1000} \tag{32}
$$

$$
Z_{\text{CO}_2} = Y_{\text{CO}_2} * \phi_{\text{CO}_2}
$$
 (33)

Validation of model

The RMSD (root mean square deviation) approach is used to prove that the fndings of the simulation with the experimental observations are merely identical (Guo et al. [2015](#page-19-31)):

RMSD =
$$
\sqrt{\frac{1}{n} \sum_{i=1}^{n} [(X_{\text{sim},i} - X_{\text{exp},i}) / X_{\text{exp},i}]^2}
$$
 (34)

Validation of result

With the help of MATLAB, simulation results were developed, and the results were compared with the actual data obtained in real-time experimentation. The detailed

Fig. 5 a Validation of η_{el} between simulated and experimental values. **b** Validation of T_{PV} between simulated and experimental values

Fig. 6 Ambient conditions of chosen location for simulation study: **a** day; **b** year

experimentation is explained in the author's previous article (Prakash and Amarkarthik [2023\)](#page-19-19). The comparative analysis of the experimental data and the simulation data of electrical efficiency is depicted in Fig. 5 a, for case 1, 2, 3, and 4 systems. The values of RMSD for the η_{el} of the case 1, 2, 3, and 4 systems were 2.66%, 2.25%, 2.54, and 2.56%, respectively. Similarly, Fig. 5 b 5 b compares the T_{PV} of simulation and experimental results for all four systems. The RMSD values of PV/T cell temperature for case 1, 2, 3, and 4 systems were 2.60%, 3.25%, 2.78%, and 2.06%, respectively. Therefore, the efficiency and cell temperature found in the simulation are close to the efficiency found in the experiment. Hence, it is proved that the results obtained through simulations are valid. This variation could be the consequence of experimental error, which would include errors caused by the instruments as well as the impact of the environment on the testing.

Result and discussion

This investigation used two working fuids for the case 1 and 3 systems: water and refrigerant R410a. The default time step for the iteration computation was set to 150 s. This choice was made because although a shorter time interval would improve accuracy slightly, it would signifcantly increase the computational workload without providing substantial benefts. The iteration process terminated when the final water temperature reached 60 °C, serving as the criterion for completion. The numerical analysis was

conducted in MATLAB, and the energy analyses covered a year-long period from November, 2021, to October, 2022, in a hot climatic region. The weather station present in the study location was used as weather data for this numerical study. Figure [6](#page-9-0) presents the environmental characteristics for the entire year, including the average daily solar irradiation per month, monthly average wind speed, and monthly ambient temperature.

The flow of the subsequent sections is as follows: The simulation results for electrical efficiency and its average values throughout the year were discussed first. Based on these values, the total electrical power generated over the year is determined. Then, a thermal performance analysis is conducted, simulating the monthly average thermal efficiency and calculating the average total heat energy generation over the year. The combined electrical and thermal outputs are then used to evaluate the economic and environmental performance of the case 1, 2, 3, and 4 systems.

Simulations on case 1, 2, 3, 4, and 5 systems

Simulation on case 1, 2, 3, 4, and 5 systems were done in MATLAB for a day and discussed in this section. Figure [7](#page-10-0) a depicts the comparative simulation results of P_{max} and η_{el} of case 1, 2, 3, and 4 with the case 5 system. The average power productions of cases 1, 2, 3, and 4 were 10.51%, 20.93%, 30.74%, and 35.88% higher than the case 5 system. Similarly, the average electrical efficiencies were 10.45% , 20.40%, 29.20%, and 33.99% higher than the case 5 system. Figure [7](#page-10-0) b illustrates the variation of T_{PV} , COP, and η_{th} of the all four systems. The average T_{PV} of case 1, 2, 3, and 4 systems were 57.50 °C, 52.98 °C, 38.12 °C, and 34.54 °C, which are 10.51%, 22.13%, 40.53%, and 45.95% lower than

Fig. 8 Graphical representation of monthly average η_{el} of all systems

the case 5 system. The average maximum η_{th} of case 1, 2, 3, and 4 systems were 76.76%, 91.75%, 114.62%, and 162.06%, respectively. Cases 3 and 4 had the highest COPs of 4.03 and 4.96, respectively. The power consumptions by cases 3 and 4 were 4.26 kWh and 3.38 kWh, respectively.

Annual electrical energy analysis

Figure [8](#page-11-0) illustrates the simulated monthly electrical efficiency (η_{el}) results for case 1, 2, 3, and 4 systems. The electrical efficiency of these systems fluctuated with the G and reached its peak in April, 2022. Although the solar intensity in April was slightly higher than that in May and June, the average outdoor temperature in April was lower. As a result, the conversion efficiency of electrical energy was higher in April compared to May and June, but lower than in March due to the lower ambient temperature in March. Moreover, the solar intensity was lower in June and July due to cloudier and wetter days compared to April and May, resulting in decreased electricity generated during those months. The η_{el} of case 1, 2, 3, and 4 systems was higher in the winter and monsoon seasons compared to the summer, primarily due to the lower ambient temperature during those periods. However, the difference in η_{el} among all cases was relatively small during the winter and monsoon seasons. Consequently, the average η_{el} of case 1, 2, 3, and 4 systems were 16.03%, 25.53%, 40.49%, and 53.32% higher, respectively. The average yearly η_{el} of case 1, 2, 3, and 4 systems were 9.77%, 10.57%, 11.83%, and 12.91%, respectively, while it was only 8.42% for the case 5 system. The percentage of rise in η_{el} is high due to the efective cooling of PV cells due to the usage of cooling medium, i.e., water, PCM, and refrigerant. Therefore, Fig. [8](#page-11-0) displays a greater degree of diversity across the different scenarios in terms of η_{el} .

The monthly electrical energy production of diferent systems is depicted in Fig. [9](#page-12-0) a–d. In April, case 1, 2, 3, and 4 systems generated the highest amounts of electrical energy, 33.95 kW-h/month, 37.11 kW-h/month, 41.19 kW-h/month, and 45.41 kW-h/month, respectively. The case 5 system produced 29.4 kW-h/month during the same period. Similarly, in July, the energy production was 23.38 kW-h/month, 25.19 kW-h/month, 28.23 kW-h/month, and 30.62 kW-h/ month for case 1, 2, 3, and 4 systems, with 19.98 kW-h/ month in June. July experienced cloudy and muggy conditions, resulting in lower radiation and consequently reduced electrical energy generation. Comparatively, the average electrical energy productions of case 1, 2, 3, and 4 systems were 16.03%, 25.53%, 40.49%, and 53.32% higher than case 5. The total electrical energies generated per year by case 1, 2, 3, and 4 systems were 325.18 kW-h/year (1170.4 MJ), 351.98 kW-h/year (1267.13 MJ), 393.92 kW-h/year (1418.11 MJ), and 430.02 kW-h/year (1548.07 MJ), respectively. Based on these fndings, the case 4 system surpasses the other three systems in power generation due to incorporating two cooling sources, namely, PCM and refrigerant. Consequently, the case 4 system offers enhanced cooling for the PV panel, leading to increased power generation.

Annual thermal energy analysis

Figure [10](#page-13-0) provides information on the monthly average thermal efficiency (η_{th}) of case 1, 2, 3, and 4 systems. During **Fig. 9** Monthly average electrical energy generation

April, the highest monthly average η_{th} values were achieved, namely, 41.61%, 51.2%, 86%, and 94.54% for cases 1, 2, 3, and 4, respectively. Conversely, the lowest monthly average η_{th} values of 35.32%, 42.84%, 81.1%, and 89.5% were recorded for cases 1, 2, 3, and 4, respectively, in July. It is noteworthy that the highest thermal energies were obtained during the spring and summer seasons due to the greater solar radiation. In contrast, the lowest thermal energies were observed during the winter and monsoon seasons due to reduced solar radiation. Figure [11](#page-14-0) displays the monthly average thermal energy produced by case 1, case 2, case 3, and case 4 systems. In April, the maximum thermal energy outputs were 531.9 MJ, 654.52 MJ, 1099.3 MJ, and 1207.9 MJ for cases 1, 2, 3, and 4, respectively, while in July, the corresponding values were 303.95 MJ, 368.76 MJ, 697.7 MJ, and 770.18 MJ. Throughout the entire year, case 1, 2, 3, and 4 systems generated 4538.66 MJ, 5534.03 MJ, 9981.07 MJ, and 11010.17 MJ of heat, respectively. Figure [12](#page-15-0) provides an overview of the combined annual energy (electrical and thermal energy) produced by case 1, 2, 3, and 4 systems. The total energies generated by these systems, in terms of electrical and thermal energy, were 5709.35 MJ (1585.9 kW-h), 6801.16 MJ (1889.21 kW-h), 12,299.18 MJ (3416.4 kW-h), and 13,638.24 MJ (3788.4 kW-h), respectively.

Fig. 10 Monthly average thermal efficiency of all systems

Economic analysis

The fnancial analyses of case 1, case 2, case 3, and case 4 systems provide valuable insights into their feasibility in Indian climatic conditions. To assess their fnancial viability, the discount rate of 5.5% and the infation rate of 6.15% were utilized for various calculations, including discounted cash flow analysis (DCFA), discounted net present value (DNPV), discounted payback period (DPBP), discounted annual cost savings (DACS), and discounted levelized cost of energy (DLCOE). This section presents these metrics, focusing on comparing all four systems with the case 5 system. In India, people are using solar water heaters, solar PV systems, and HVAC systems for water heating, electricity generation, and space cooling purposes, respectively, as individual systems. Each system has its own disadvantages. Hence, to solve its limitations and to avoid the usage of diferent systems, hybrid systems were proposed and the economic and environmental viability of these systems for non HVAC building and HVAC building applications is evaluated and presented. In this work, the hybrid system is designed for 1 kW electricity generation per hour and 1 tons refrigeration system with 500 L hot water capacity. In India, the average rates of 1 kW PV system, solar water heater, and air conditioner cost are ₹70,000, ₹20,000 and ₹35,000, respectively.

Figure [13](#page-15-1) presents the annual cash flow analysis for 25 years for case 1, 2, 3, 4, and 5 systems. The average yearly cash fows for cases 1, 2, 3, and 4 are ₹4323, ₹5335, ₹15,523, and ₹22,022, respectively, and their expected payback times are 5–6, 6–7, 4–5, and 3–4 years, respectively. Figure [14](#page-16-0) illustrates the discounted net present values (DNPV) of cases 1, 2, 3, and 4 systems, all of which have positive values. Therefore, the installation of these systems yields a proft of ₹110,449, ₹140,083, ₹454,570, and ₹677,403, respectively, over their lifetime. The discounted payback periods (DPBPs) for cases 1, 2, 3, and 4 are 9–10, 8–9, 5–6, and 3–4 years, respectively. Moving to Fig. [15,](#page-16-1) it display the discounted annual cost savings (DACS) and the discounted levelized cost of energy (DLCOE) for cases 1, 2, 3, and 4 systems. The DLCOE values for these systems are ₹2.92 per kWh, ₹2.78 per kWh, ₹2.34 per kWh, and ₹1.79 per kWh, respectively, whereas the DLCOE for the case 5 system without water heating cost is ₹3.62 per kW-hr. Cases 1, 2, 3, and 4 have lower DLCOE values than the reference PV system, with higher operational and maintenance costs and additional water and refrigerant pumping power. The DLCOE of the systems in cases 1, 2, 3, and 4 were lower, and likewise, the DLCOE is lower, even though all the systems have higher operational and maintenance costs and additional water and refrigerant pumping power. It is worth noting that the DLCOE values for all systems fall within the range provided by the International Renewable Energy Agency (IRENA) for residential PV installations in 2019 (₹5.25 to ₹22 per kW-h). Additionally, the DACS per year for case 1, 2, 3, and 4 systems are ₹4418, ₹5603, ₹18,183, and ₹27,096, respectively, resulting in savings of ₹110,449, ₹140,083, ₹454,570, and ₹677,403, respectively, over their lifetime. Furthermore, compared to the cost of the case 5 system, cases 1, 2, 3, and 4 saved 8.97%, 11.64%, 40.05%, and 60.16% times yielded the higher cost, respectively.

Taking into account the discounted costs and the smaller size of the reference PV system, it can be inferred that its payback period will be longer. However, considering the DPB, case 1, 2, 3, and 4 systems become proftable after

Fig. 11 Monthly average thermal energy generation by cases

1, 2, 3, and 4 systems

9–10, 8–9, 5–6, and 3–4 years, respectively. Additionally, the Indian government offers a 20% subsidy for renewable energy system installations, which further reduces the payback period. Consequently, the DLCOE values are lower for all the four cases when considering the water heating cost. Despite this, the DLCOE for all four systems is lower than India's average energy cost of ₹6.15 per kW-h. Moreover, the DNPV and DACS parameters demonstrate favorable outcomes compared to the case 5 system. Furthermore, the cell temperatures of case 1, 2, 3, and 4 systems are lower than that of the case 5 system, indicating that their lifespan will likely exceed 25 years. Consequently, it is found that all the proposed systems are economically viable.

Environmental analysis

This section summarizes the annual pollution mitigation and cost savings achieved by all four systems. Figure [16](#page-17-0)a depicts the $CO₂$ emission mitigation and cost savings, where these four systems collectively eliminate 71.28 tons, 89.98 tons, 202.69 tons, and 280.72 tons of carbon dioxide, resulting in total cost savings of ₹83,725, ₹105,675, ₹238,050, and ₹329,700 over their lifetimes. The $CO₂$ mitigation and cost savings of case 1, 2, 3, and 4 systems are 3.41, 4.30, 9.68, and 13.42 times greater than case 5 system, which mitigates 20.93 tons of CO_2 and saves a total cost of ₹24,575 throughout its lifespan.

Fig. 12 Total energy generation by cases 1, 2, 3, 4, and 5 systems

Figure [16](#page-17-0) b demonstrates the SO_2 emission mitigation and cost savings achieved by reducing pollutants. Over their lifetimes, cases 1, 2, 3, and 4 systems eliminate 2.14 tons,

2.71 tons, 6.1 tons, and 8.45 tons of SO_2 , resulting in total cost savings of ₹26,050, ₹32,900, ₹74,100, and ₹102,600, respectively. The SO_2 mitigation and cost savings of case 1, 2, 3, and 4 systems are 3.41, 4.30, 9.68, and 13.42 times higher than those of the case 5 system, which mitigates 0.63 tons of SO_2 and saves a total cost of ₹7650 throughout its lifespan.

Figure [16](#page-17-0) c focuses on reducing NO_x emissions and the associated cost savings achieved by case 1, 2, 3, and 4 systems. These systems collectively mitigate 1.07 tons, 1.35 tons, 3.05 tons, and 4.22 tons of NO_x , resulting in cost savings of ₹477,700, ₹603,000, ₹1,358,275, and ₹1,881,175, respectively, over their lifetimes. Furthermore, case 1, 2, 3, and 4 systems mitigate NO_x by 3.45, 3.49, 9.84, and 13.61 times higher than the standard PV system, which mitigates 0.31 tons of NO_x and saves a total cost of ₹140,250 throughout its lifespan.

Finally, Fig. [16](#page-17-0) d illustrates the reduction of PM_{10} emissions and associated cost savings achieved by case 1, 2, 3, and 4 systems. These systems mitigate 154.41 kg, 194.91 kg, 439.04 kg, and 608.05 kg of PM_{10} emissions, resulting in cost savings of ₹93,800, ₹118,400, ₹266,725, and ₹369,400, respectively. Case 1, 2, 3, and 4 systems mitigate PM_{10} emissions by 3.41, 4.30, 9.69, and 13.41 times higher than the standard PV system, which mitigates 45.33 kg of PM_{10} and saves a total cost of ₹27,550 throughout its lifespan.

Fig. 13 Annual cash fow diagram of all cases

Fig. 14 Comparison of DPB and DNPV for cases 1, 2, 3, 4,

and 5

It can be inferred that the usage of case 1, 2, 3, and 4 systems effectively reduces CO_2 , SO_2 , NO_x , and PM_{10} emissions, contributing to a reduced environmental impact. Therefore, the ecological and enviroeconomic cost analyses of case 1, 2, 3, and 4 systems are valid and demonstrate their worthiness. The results of the cost assessments reveal that the PV/T PCM-DXHP system is more afordable and preferable compared to the solar PV system and HVAC system working alone in the long term. As a result, more non-HVAC buildings should install solar PV/T PCM-W systems, and HVAC-system-integrated buildings should install PV/T PCM-DXHP systems to beneft from the economic rewards and enjoy a pristine environment for the foreseeable future.

Conclusion

Energy, economic, and environmental numerical analyses were carried out on PV/T-W, PV/T PCM-W, PV/T DXHP, and PV/T PCM-DXHP systems with a butterfy serpentine flow profile and HS36 PCM. The following is a summary of the most critical conclusions from the evaluation:

Energy performance: The average yearly electrical efficiencies of PV/T-W, PV/T PCM-W, PV/TDXHP, and PV/T PCM-DXHP systems are 9.77%, 10.57%, 11.83%, and 12.91%, which are 16.03%, 25.53%, 40.5%, and 53.32% higher than the reference PV system. The PV/T-W, PV/T PCM-W, PV/T DXHP, and PV/T PCM-

Fig. 15 Comparison of DACS and LCOE for cases 1, 2, 3, 4, and 5

Fig. 16 Emission reduction and Environmental cost savings by cases 1, 2, 3, and 4: **a** CO₂, **b** SO₂, **c** NO_x, and **d** PM₁₀

DXHP systems produced 5709.35 MJ, 6801.16 MJ, 12,299.18 MJ, and 13,638.24 MJ, respectively. All the four systems with a BSF collector and HS36 PCM demonstrated improved energy performance. These systems produced higher electrical and thermal energy than the reference PV system. Notably, the PV/T PCM-DXHP system exhibited the highest energy production due to the integration of PCM and refrigerant for cooling.

Economic viability: The economic analysis showed a good result based on a discounted payback period of 8, 7, 6, and 5 years and the costs of energy production are ₹4.08 per kW-h, ₹3.67 per kW-h, ₹3.37 per kW-h, and ₹2.87 per kW-h for PV/T-W, PV/T PCM-W, PV/T DXHP, and PV/T PCM-DXHP systems, respectively. The fnancial analyses indicated that all four systems are economically viable. These systems' discounted net present values (DNPV) and discounted annual cost savings (DACS) were favorable, suggesting long-term proftability. Additionally, the payback periods for these systems were shorter than the reference PV system, further indicating their economic feasibility.

Environmental impact: The environmental analysis also showed a good result, and the proposed four systems mitigated the $CO₂$ of 64.72 tons, 90.45 tons, 117.35 tons, and 156.49 tons throughout their lifetimes. It saved the cost by ₹75,075, ₹104,925, ₹136,175, and ₹181,525. The PV/T- W, PV/T PCM-W, PV/T DXHP, and PV/T PCM-DXHP systems demonstrated signifcant reductions in greenhouse gas emissions and other pollutants compared to the reference PV system. These systems contributed to the mitigation of carbon dioxide $(CO₂)$, sulfur dioxide $(SO₂)$, nitrogen oxides (NO_x) , and PM10 emissions. The magnitude of emissions reduction and cost savings varied among the diferent systems, with the PV/T PCM-DXHP system yielding the highest environmental benefts.

In conclusion, all the four systems with a butterfy serpentine fow profle and HS36 PCM demonstrated enhanced energy performance, economic viability, and environmental benefts. The fndings support the feasibility and efectiveness of these systems for sustainable energy generation and environmental mitigation.

It is benefcial for the HVAC buildings to use the PV/T PCM-DXHP system, which can last up to at least 5 years because the results of the cost assessments reveal that the PV/T PCM -DXHP system is more afordable and more acceptable than the solar PV system and HVAC system working alone in the long term.

Subsequently, more non-HVAC buildings should install solar PV/T PCM-W systems and HVAC-system-integrated buildings should install PV/T PCM-DXHP systems to beneft from the economic rewards and relish in a pristine environment for the foreseeable future.

Nomenclature

DC: Direct current; *dg*: Module degradation; *Dt*: No. of days; *PVGC*: PV glassing cover; *SC*: Solar cell; *SSC*: Shirt circuit current; *FF*: Fill factor; *EVAN*: EVA grease; *EI*: Electrical insulation;

OD: Outer diameter; *ID*: Inner diameter

Symbols

β: PV system slope (°); *A*: PV area (m²); *C*: Cost; *CF*: Cash flow; *G*: Solar irradiation (W/m²); *m*: Mass (kg); *P*: Power (W); *p*: Pressure (bar); *η*: Efficiency (%); *P*: Electrical power (W); *ΔP*: Change in power (W); *Q*: Heat (kJ); *w*: Speed of the compressor; *T*: Temperature (${}^{\circ}$ C); \dot{m}_{ref} : The mass flow rate of refrigerants; *E*: Net energy (kWh/year); *i*: Infation rate; *r*: Discount rate; *ø*: Mitigation per annum; *ø*: Emissions equivalents intensity for coal-fred electricity generation; *h'*: Enthalpy; *h*: Heat transfer coefficient; *U*: Overall heat transfer coefficient; *cl*: Collector; *d*: Conduction; *v*: Convection; *r*′: Radiation; *u*: Velocity; *V*: Displacement volume; *Cp*: Specifc heat; $ρ$: Density; *L*: Length; *α*: Absorption coefficient; *δ*: Thickness;

τ: Transmissivity; *g*: Glass; *abs*: Absorber

Symbols (subscript)

a: Ambient; *c*: Cell; *com*: Compressor; *con*: Condenser; *Eva*: Evaporator; *ε*: Efectiveness; *exp*: Experimental; *El*: Electrical; *h*: Enthalpy; *iso*: Isometric; *in*: Inlet; *max*: Maximum; *min*: Minimum; *n*: Yearly; *o*: Initial Investment; *out*: Outlet; *O&M*: Operation and maintenance; *S*: Entropy; *S*: Sun; *S/Z*: Cost savings; *sim*: Simulation; *th*: Thermal; *t*: Year (no. of days); *tL*: Lifetime of components; *u*: Useful; *w*: Water; *X*: Readings; *Y*: Carbon price per ton

Acknowledgements The authors would like to mention their heartfelt gratitude and appreciation to the management of Bananri Amman Institute of Technology, India, for generously providing the necessary facilities and invaluable support to this research.

Author contribution All authors contributed to the study's conception and design. Methodology, material preparation, and data collection were performed by Prakash K. Babu and Amarkarthik Aruanchalam. Data collection and analysis were performed by Prakash K. Babu, Subramaniyan Chinnasamy, and Chandrasekaran Manimuthu. The frst original draft of the manuscript was written by Prakash K. Babu and Subramaniyan Chinnasamy, and all authors commented on previous versions of the manuscript. All authors read and approved the fnal manuscript.

Data availability The article contains the data that was utilised to support the fndings of this investigation. Additional data can be provided upon request.

Declarations

Ethical approval Not applicable.

Consent to participate Not applicable.

Consent for publication Not applicable.

Conflict of interest The authors declare no competing interests.

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