RESEARCH ARTICLE

Removal of fuconazole from aqueous solution by magnetic biochar treated by ball milling: adsorption performance and mechanism

Zhexi Huang1,2,3 · Yunqiang Yi1,2,3 · Nuanqin Zhang1,2 · Pokeung Eric Tsang4 · Zhanqiang Fang1,2,3

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Abstract

The problem of low adsorption capacity of pristine magnetic biochar for organic pollutants always occurs. It is of great signifcance to select a suitable method to improve the adsorption performance of magnetic biochar. In this study, magnetic biochar was treated by ball milling and tested for its fuconazole adsorption capacity. The maximum adsorption capacity of ball-milled magnetic biochar (BMBC) for fuconazole reached nearly 15.90 mg/g, which was approximately fve times higher than that of pristine magnetic biochar (MBC). Fluconazole adsorption by BMBC was mainly attributed to *π*–*π* interactions, hydrogen bonding, and surface complexation with oxygen-containing functional groups. The enhancement in fuconazole adsorption by BMBC was attributed to an increase in oxygen-containing functional groups. Batch adsorption experiments also illustrated that BMBC could be successfully applied in a wide range of pH values. The high efficiency of fluconazole removal confrmed that ball milling was an efective strategy to enhance the adsorptive performance of magnetic biochar.

Keywords Magnetic biochar · Ball milling · Fluconazole · Adsorption mechanism · Oxygen-containing functional groups

Introduction

Magnetic biochar is usually derived from biomass and transition metal salts, and it has been confirmed as a high-efficiency adsorbent for typical pollutants (such as antibiotics, organic dyes, and heavy metals) in aqueous solution (Xu et al. [2020;](#page-9-0) Yi et al. [2019a;](#page-9-1) Li et al. [2020a;](#page-8-0) Liu et al. [2019](#page-8-1)). Magnetic biochar has the advantage that it can be recovered from the reaction medium by magnetic separation (Rocha et al. [2020;](#page-8-2) Hassan et al. [2020;](#page-8-3) Li et al. [2018a](#page-8-4)). Therefore,

- School of Environment, South China Normal University, Guangzhou 510006, China
- ² Guangdong Technology Research Center for Ecological Management and Remediation of Water System, Guangzhou 510006, China
- ³ Guangdong Provincial Key Laboratory of Chemical Pollution & Environmental Safety, Guangzhou 510006, China
- Department of Science and Environmental Studies, The Education University of Hong Kong, Hong Kong 00852, China

environmental remediation technology based on magnetic biochar has been widely used.

Thus far, the methods used to synthesize magnetic biochar have mainly included impregnation–pyrolysis, the hydrothermal approach, and co-precipitation (Liang et al. [2019](#page-8-5); Cai et al. [2018](#page-8-6); Oladipo and Ifebajo [2017](#page-8-7)). However, irrespective of the method that is used to synthesize magnetic biochar, the adsorption performance of the unmodified product is limited. Therefore, metal element or metal oxide doping (Li et al. [2019](#page-8-8); Jung et al. [2017](#page-8-9)), acid–base activation (Tang et al. [2018](#page-8-10)), organic functional group grafting (Li et al. [2018a,](#page-8-4) [b](#page-8-11), [c;](#page-8-12) Zhou et al. [2018\)](#page-9-2), and chemical oxidation (Xu et al. [2020\)](#page-9-0) are generally used to enhance the adsorption performance of magnetic biochar. For instance, Li et al. ([2018a,](#page-8-4) [b](#page-8-11), [c\)](#page-8-12) demonstrated that surface functional groups of magnetic biochar were enriched by chitosan modifcation, which signifcantly improved the material's adsorption capability for Cd(II). Meanwhile, the maximum adsorption capacity of Pb(II) by $CeO₂$ -MoS₂-modified magnetic biochar was 263.6 mg/g, which was approximately 10 times higher than that of the original magnetic biochar (Li et al. [2019](#page-8-8)). However, despite their effectiveness in improving the adsorption performance of magnetic biochar, the methods mentioned above have some drawbacks, such as complex modifcation processes, high costs, and the use of toxic and harmful substances. Therefore, it is necessary to identify a green and efficient method to enhance the adsorption performance of magnetic biochar.

Ball milling has been widely used to enhance surface area, reduce particle size, or enrich the surface functional groups of adsorbents, due to its advantages of simple operation, high efficiency, and low cost (Zhuang et al. 2021 ; Kumar et al. [2020;](#page-8-13) Zhang et al. [2019a](#page-9-4)). Xiang et al. ([2020\)](#page-9-5) revealed that ball milling efectively enhanced the specifc surface area of biochar. They also showed that the adsorption capacity of ball-milled biochar for tetracycline was three times higher than that of pristine biochar. Similarly, Li et al. [\(2020b](#page-8-14)) revealed that magnetic biochar was transformed into magnetic nanobiochar using ball milling, which signifcantly enhanced the adsorption capacity of magnetic biochar for tetracycline and Hg(II). Therefore, it is theoretically feasible to improve the adsorption performance of magnetic biochar by ball milling.

Fluconazole is a broad-spectrum antifungal drug, which has been detected as a pollutant in water bodies (Assress et al. [2020,](#page-8-15) [2019\)](#page-8-16). Residual fuconazole poses a great threat to aquatic ecological environments (Zhang et al. [2020](#page-9-6); Richter et al. [2016\)](#page-8-17). Therefore, it is of great signifcance to eliminate fuconazole from wastewater. In this study, ball-milled magnetic biochar was prepared and used for fuconazole adsorption. The following items were investigated: (1) the physicochemical properties of ball-milled magnetic biochar; (2) the adsorption kinetics and adsorption isotherms of fuconazole by ball-milled magnetic biochar; (3) the adsorption mechanism of fuconazole by ball-milled magnetic biochar; and (4) the infuence of pH, humic acid, and biomass type on the adsorption of fuconazole by ball-milled magnetic biochar.

Materials and methods

Reagents

Fluconazole (analytical purity), ferrous sulfate heptahydrate $(FeSO₄·7H₂O;$ analytical purity), sodium hydroxide (superior purity), ammonium formate, and acetonitrile were purchased from Energy Chemical Reagent Company, China. Hydrochloric acid (HCl; analytical purity) was purchased from Guangzhou Chemical Reagent Factory, China.

Material preparation

Ten grams of rice husk was mixed in 30 mL of dilute HCl (0.1 mol/L) for 6 h to remove impurities. This pretreated rice husk was added to 100 mL of Fe^{2+} solution (1.2 g/L) and stirred for 24 h. Subsequently, the mixture was centrifuged, and the residue was placed in a muffle furnace for 1.5 h at a pyrolysis temperature of 600℃ in a nitrogen atmosphere. Finally, after being milled and sieved to pass through a 100 mesh sieve, the obtained sample was labeled as pristine magnetic biochar (MBC). Subsequently, MBC (1 g) and steel balls were added into stainless steel vials and placed in a planetary ball mill (MBC to ball mass ratio=1:100 (Zhang et al. [2019a](#page-9-4), [b\)](#page-9-7); the mass ratio of 10-mm and 6-mm balls was 8:2). Ball milling was operated at 400 r/min for 24 h in ambient air conditions, and the direction of rotation was changed every 6 h. The obtained sample was labeled as ball-milled magnetic biochar (BMBC).

Material characterization

A surface analyzer (ASAP2020M; USA) was used to measure the specifc surface area and pore size distribution of MBC and BMBC. The surface morphology of MBC and BMBC was investigated using scanning electron microscopy (SEM; Tuscan mira3, Germany) equipped with energy-dispersive X-ray spectroscopy (Oxford X-MAX, UK). Fouriertransform infrared spectroscopy (FT-IR; Horiba, Emax, Japan) was conducted to obtain information on the surface functional groups of MBC and BMBC. The phase structures of MBC and BMBC were analyzed by X-ray difraction (D8 advance, Bruker, Germany). The valence states of elements on the surface of BMBC were measured by X-ray photoelectron spectroscopy (XPS; ESCALAB 250; Thermo-VG Scientifc, USA). The magnetic properties of BMBC were determined with a comprehensive physical measurement system (PPMS-9; Quantum Design, USA). The carbon (C), hydrogen (H), nitrogen (N), and oxygen (O) contents of BMBC were determined using an elemental analyzer (varia EL CUBE, Germany).

Adsorption experiments

For adsorption kinetic experiments, BMBC (1 g/L) was added to a conical fask containing 100 mL of fuconazole solution (20 mg/L, $pH = 5.6$). The flasks were shaken in a thermostatic oscillator (200 r/min, 30 °C \pm 0.5 °C). At the pre-selected time, the suspensions were immediately fltered through chemical analytical flter paper. The remaining fuconazole in the solutions was measured by high-performance liquid chromatography. Detailed testing methods are shown in our previous studies (Zhang et al. [2020](#page-9-6)). The removal efficiency of fluconazole was calculated using the following equation:

$$
\eta = \frac{C_0 - C_e}{C_0} \times 100\%
$$
 (1)

where C_0 and C_e are the initial and equilibrium concentrations of fuconazole (mg/L), respectively.

The equilibrium adsorption capacity was calculated using the following equation:

$$
Q_e = \frac{(C_0 - C_e)xV}{W}
$$
 (2)

where Q_e is the adsorption capacity (mg/g), C_0 and C_e are the initial and equilibrium concentrations of fuconazole in the solution, and *V* and *W* are the volume of solution (mL) and the dosage of BMBC (g/L), respectively.

The data for adsorption kinetics were ftted by the pseudofrst-order (Eq. [3\)](#page-2-0), pseudo-second-order (Eq. [4](#page-2-1)), and Elovich (Eq. [5\)](#page-2-2) models, respectively. The kinetic models are represented as:

$$
Q_t = Q_e \left(1 - e^{-k_1 t} \right) \tag{3}
$$

$$
\frac{t}{Q_t} = \frac{1}{Q_e}t + \frac{1}{k_2 Q_e^2}
$$
\n(4)

$$
Q_t = \alpha + \beta \ln t \tag{5}
$$

where Q_e represents the adsorption capacity of fluconazole at equilibrium, Q_t (mg/g) is the adsorption capacity for fluconazole at time *t*, and k_1 and k_2 are the pseudo-first-order rate constant (min−1) and the pseudo-second-order rate constant ($g/mg/min$), respectively. α is the initial adsorption rate (mg/kg), and β is the desorption constant (kg/mg).

For adsorption isotherm measurement, BMBC was placed into a conical fask containing 100 mL of solution of different concentrations of fuconazole (5, 10, 15, 20, 25, and 30 mg/L). The mixture was shaken for 6 h at diferent temperatures (20 °C \pm 0.5 °C, 30 °C \pm 0.5 °C, and 40 °C \pm 0.5 ℃). The experimental data were ftted using the Langmuir (Eq. [6\)](#page-2-3) and Freundlich (Eq. [7](#page-2-4)) models as follows:

$$
\frac{C_e}{Q_e} = \frac{1}{K_L Q_m} + \frac{C_e}{Q_m} \tag{6}
$$

$$
Q_e = K_F C_e^{\frac{1}{n}} \tag{7}
$$

where Q_m (mg/g) is the maximum adsorption capacity for fluconazole, K_L (L/mg) is the Langmuir isotherm constant, K_F (mg/g (L/mg)ⁿ) is the Freundlich isotherm constant, and *n* is the measure of adsorption intensity.

The thermodynamic parameters, including standard free energy change (ΔG), standard enthalpy change (ΔH), and standard entropy change (ΔS) , were calculated using Eqs. [8](#page-2-5) and [9](#page-2-6) as follows:

$$
\Delta G = -RT \ln K \tag{8}
$$

$$
\ln K = \Delta S / R - \Delta H / (RT) \tag{9}
$$

where *K* is the adsorption equilibrium constant, $T(K)$ is the absolute temperature, and R (8.314 J/mol/K) is the gas constant. Δ*H* and Δ*S* could be calculated from the slope and intercept of ln *K* versus 1/*T*.

Finally, the infuences of pH, humic acid, and biomass species on the adsorption of fuconazole by BMBC were investigated. Each experiment was conducted in duplicate.

Results and discussion

Material characterization

The structure and phase compositions of MBC and BMBC were observed by XRD (Fig. S1 (a)). For MBC, the broad difraction peaks at 20°–30° are generally considered to represent silica, graphitic carbon, and amorphous iron oxides (Huang et al. [2020](#page-8-18); Zhong et al., [2018](#page-9-8)). The peak at 44.3° corresponded to the (110) plane of Fe⁰in MBC, and the (220), (100), and (440) planes of $Fe₃O₄$ were also observed in MBC. After ball milling, the (100) plane of $Fe₃O₄$ and the (110) plane of Fe⁰ were strengthened, indicating that ball milling was beneficial to the crystallinity of $Fe₃O₄$ and $Fe⁰$ in MBC. Meanwhile, the saturation magnetization of BMBC (Fig. $S1$ (b)) was 55.15 emu/g, which was nearly 2.38 times higher than that of MBC. The above results provide evidence that ball milling improved the crystallinity of iron and iron oxides in the MBC and alignment of the magnetic domains in the crystal structure (Fu et al. [2019](#page-8-19)).

SEM images (Fig. [1\)](#page-3-0) revealed that MBC exhibited an abundant porous structure, and iron oxides adhered to the surface of MBC. After ball milling, the pore structure of BMBC disappeared. Additionally, the particles of iron oxides in BMBC were signifcantly reduced in size, and most of them approached the nanoscale. The results of element mapping (Fig. [2\)](#page-4-0) suggested that Fe, C, and O were evenly distributed on the surface of BMBC. The specifc surface area of MBC (Fig. $S2$ (a)) was 211.18 m²/g, whereas that of BMBC was reduced by a factor of 1.69. The above results were possibly attributable to the pore structure of MBC being destroyed by ball milling, which is consistent with the results of SEM.

Surface functional groups of MBC and BMBC are presented in Fig. S2 (b). The peak at 3429 cm−1 was considered to be due to the stretching vibration of O–H (Zou et al. 2021). The peak at 1617 cm⁻¹ represented the vibration of aromatic $C = C$ and $C = O$ (Wang et al. [2019\)](#page-8-20). The vibra-tion of –C–O–C appeared at 1099 cm⁻¹ (Zhang et al. [2018](#page-9-10)). The peak at 805 cm−1 was attributed to the vibration of C–H in pyridine or furan, which are heterocyclic compounds (Wang et al. 2019). A peak at 469.1 cm⁻¹ was assigned to the stretching of Si–O (Zhou et al. [2018](#page-9-2)). The results of

Fig. 1 Scanning electron microscopy images of pristine magnetic biochar (**a**, **b**) and ball-milled magnetic biochar (**c**, **d**)

FT-IR demonstrate that ball milling had little efect on the surface functional groups of magnetic biochar.

XPS spectra of MBC and BMBC are indicated in Fig. [3.](#page-4-1) Three difraction peaks of C, O, and Fe were observed in MBC and BMBC. The Fe2p spectra of MBC and BMBC could be deconvoluted into three peaks of $Fe^0(707 \text{ eV})$, Fe(II) (710.0 and 724.0 eV), and Fe(III) (712.0 and 726.3 eV) (Jiang et al. [2019a;](#page-8-21) Zhang et al. [2018;](#page-9-10) Yang et al. [2016](#page-9-11)). Compared with MBC, the characteristic peak of Fe⁰ in BMBC decreased slightly, indicating that ball milling reduced the content of $Fe⁰$ in MBC. In addition, the intensity ratio of Fe(II)/Fe(III) in MBC decreased from 1.7 to approximately 0.9 after ball milling, demonstrating that Fe(II) was oxidized during ball milling. The O1s spectra of the materials showed binding energies of 531.1–531.8, 532.2–533.3, and $534.0 - 535.4$ eV, which corresponded to $-C=O$, $-C=O$, and –OH groups, respectively (Jiang et al. [2019b;](#page-8-22) Zhou

et al. [2017\)](#page-9-12). It is worth mentioning that compared with MBC, the content of –OH groups in BMBC decreased significantly, while the proportion of $-C=O$ increased significantly. In the C1s spectra, the binding energies of 284.0, 284.5, and 285.0 eV corresponded to $-C=C/-C-C$, $-C-O$, and $-C=O$ groups, respectively (Reguyal and Sarmah [2018](#page-8-23); Ahmed et al. [2017](#page-8-24)). The relative content of $-C=O$ increased after ball milling, implying that ball milling could signifcantly increase the content of $-C=O$ functional groups in MBC.

The elemental compositions of MBC and BMBC are listed in Table [1.](#page-5-0) In BMBC, the content of C was lower than that in MBC, while the contents of H, O, and N were higher. In addition, the O/C, H/C, and $(N+O)/C$ values of the magnetic biochar increased after ball milling, suggesting that ball milling reduces the hydrophobicity and improves the polarity of magnetic biochar.

Fig. 2 Element mapping of ball-milled magnetic biochar (**a**), carbon mapping of ballmilled magnetic biochar(**b**), oxygen mapping of ball-milled magnetic biochar(**c**), and iron mapping of ball-milled magnetic biochar(**d**)

Fig. 3 X-ray photoelectron spectra (**a**), Fe2p spectra (**b**), O1s spectra (**c**), and C1s spectra (**d**)

Table 1 Element analysis of pristine magnetic biochar (MBC) and ball-milled magnetic biochar (BMBC)

Adsorption of fuconazole by MBC and BMBC

The adsorption kinetics of fuconazole by MBC and BMBC are shown in Fig. [4a.](#page-5-1) Although MBC and BMBC had different adsorption capacities for fuconazole, both reached adsorption equilibrium within approximately 6 h. The equilibrium adsorption capacity of BMBC for fuconazole was nearly 13.5 mg/g, which was approximately three times that of MBC. Furthermore, the ftting results of the three adsorption kinetic models are shown in Table S1. The correlation coefficient (R^2) of the Elovich model was > 0.99, which was greater than that of the pseudo-frst-order and pseudosecond-order kinetic models, indicating that fuconazole adsorption by BMBC mainly occurs by chemical adsorption (Han et al. [2016;](#page-8-25) Zhang et al. [2013](#page-9-13)).

The experimental data were ftted by the Langmuir and Freundlich models (Fig. [4b\)](#page-5-1), and the adsorption model parameters are listed in Table S2. With an increasing concentration of fuconazole, the adsorption capacity of the magnetic materials for fuconazole increased and gradually reached adsorption equilibrium. For MBC, the correlation coefficient of the Freundlich model was lower than that of the Langmuir model, illustrating that the adsorption of fuconazole by MBC was dominated by monolayer physical adsorption, and the adsorption capacity of MBC for fuconazole increased with an increase in reaction temperature. In contrast, the adsorption of fuconazole by BMBC was consistent with the Freundlich model, which may be attributable to the change in particle size and the surface structure of magnetic biochar caused by ball milling. In addition, 1/*n* is generally considered to be related to adsorption strength. For BMBC, the 1/*n* value decreased with an increase in temperature, but remained between 0.3 and 0.4, indicating that BMBC had a strong adsorption capacity for fuconazole (Yan et al. [2015\)](#page-9-14). Finally, according to the Langmuir ftting data, the adsorption capacity of BMBC for fuconazole was higher than that of MBC, which again showed that ball milling could efectively improve the adsorption performance of magnetic biochar.

The main adsorption thermodynamic parameters are provided in Table S3. The ΔG values were negative at all three temperatures for both MBC and BMBC, suggesting that adsorption was feasible and spontaneous (Jung et al. [2017](#page-8-9)). The absolute values of Δ*G* indicated that the driving force of adsorption for BMBC was higher than for MBC. The positive Δ*S* values revealed that fuconazole adsorption by MBC or BMBC was random rather than orderly (Yan et al. [2015](#page-9-14)). The Δ*H* values of BMBC and MBC indicate that the adsorption process was endothermic. The Δ*H* value of BMBC was nearly two times higher than that of MBC, showing that the endothermicity was increased (Jung et al. [2017;](#page-8-9) Yan et al. [2015](#page-9-14)).

Mechanism of fuconazole adsorption by BMBC

The XPS spectrum (Fig. [5](#page-6-0)) illustrates that the main components of spent BMBC were C, Fe, and O, and the peaks of O and C functional groups changed after BMBC was used (Table S4). Specifically, the binding energy of $-C=C/C-C$ shifted from 284.0 to 284.22 eV, that of –C–O shifted from 284.49 to 284.862 eV, and that of $-C=O$ changed from 285.0 to 285.61 eV. Moreover, the relative content of these functional groups also changed after BMBC was used. For example, the relative content of $-C=C/C-C$ increased

Fig. 4 Adsorption kinetics (**a**) and adsorption isotherms (**b**) of fuconazole by pristine magnetic biochar (MBC) and ball-milled magnetic biochar (BMBC)

from 24.84 to 31.13%, indicating that fuconazole was successfully adsorbed by BMBC (Zhang et al. [2019b](#page-9-7); Zhou et al. [2018](#page-9-2)). Conversely, the relative content of –C–O and $-C=O$ in BMBC decreased, suggesting that these functional groups participated in fuconazole adsorption. The O1s spectrum also showed that the binding energy of O-containing functional groups in BMBC changed after the reaction. Specifcally, the relative content of the functional group –C–O decreased from 55.97 to 48.05%, revealing that there was a chemical reaction between BMBC and fuconazole. Finally, from the Fe2p spectrum, it can be seen that the binding energy and content of Fe with diferent valence states changed only weakly after the reaction, indicating that Fe oxides in BMBC have little efect on fuconazole adsorption. Therefore, the C– and O-containing functional groups in BMBC contributed to fuconazole adsorption.

FT-IR (Fig. S3a) revealed no obvious diference in the infrared spectra of fresh and spent BMBC, illustrating that the types of functional groups in BMBC were unchanged. However, the peaks of some functional groups in BMBC shifted. For example, the peaks of aromatic $C = C$ and $C = O$ shifted from 1620.88 to 1618.15 cm⁻¹, the peaks of –C–O–C shifted from 1095.21 to 1097.95 cm⁻¹, and the peaks of C–H shifted from 802.73 to 806.77 cm⁻¹. This confirms that the functional groups in BMBC participated in fuconazole adsorption (Li et al. [2018c;](#page-8-12) Ahmed et al. [2017\)](#page-8-24). The results of XRD (Fig. S3b) illustrated that the phase composition and crystal structure of BMBC were relatively unafected in the process of fuconazole adsorption, providing further evidence that Fe oxides, silica, and other components in BMBC contributed less to fuconazole adsorption. Finally, the results of SEM, specifc surface area, and the efect of pH on fuconazole adsorption by BMBC (Fig. S4) identifed that the contributions to pore-flling and electrostatic interaction on fuconazole adsorption were negligible.

Based on the above analysis, the mechanism of fuconazole adsorption by BMBC can be summarized as follows (Fig. [6](#page-7-0)): (1) The aromatic structure of fuconazole makes it a *π*-electron acceptor; meanwhile, the results of XRD show that the BMBC had a graphite-like structure. Therefore, *π*–*π* electron donor–acceptor interactions were responsible for fuconazole adsorption; (2) the results of XPS and FT-IR illustrate that fuconazole adsorption was also attributable to H bonding; (3) O-containing functional groups in BMBC complexed with fuconazole, which also contributed to fuconazole adsorption; (4) the pore-flling and hydrophobic efects had little contribution to fuconazole adsorption by BMBC. Therefore, $\pi-\pi$ interactions, H bonding, and the complexation of O-containing functional groups were the main contributors to fuconazole adsorption, and the increase

Fig. 6 The adsorption mechanism of fuconazole by BMBC

in O-containing functional groups was the key reason for the improvement in fuconazole adsorption by BMBC.

Infuence of pH, humic acid, and biomass type on fuconazole adsorption by BMBC

Efects of pH

The infuence of pH on fuconazole adsorption by BMBC is shown in Fig. S4. Acidic conditions were slightly more conducive to fuconazole adsorption, and the maximum adsorption capacity reached 13.5 mg/g at $pH = 3.0$. With an increase in pH, the adsorption capacity of BMBC for fuconazole decreased. However, even at pH=11.0, the adsorption capacity of BMBC for fuconazole only decreased by 3.3 mg/g, indicating that BMBC has better pH shock resistance, and will undoubtedly have good practical application prospects.

Efects of humic acid

Humic acid commonly exists in water bodies. Previous studies have confrmed that the presence of humic acid can signifcantly afect the adsorption of target pollutants by adsorbents (Yang et al. [2017](#page-9-15); Lian et al. [2015](#page-8-26)). Therefore, it is necessary to explore the effect of coexisting humic acid on fluconazole adsorption by BMBC. The effect of humic acid on fuconazole adsorption by BMBC is shown in Fig. S5. With the increase in humic acid concentration, the capacity of BMBC to adsorb fuconazole decreased only slightly, reaching 12.4 mg/g when the concentration of humic acid was 30 mg/L, which was only 1.4 mg/g lower than that of the system without humic acid. This illustrated that the infuence of humic acid on fuconazole adsorption by BMBC was weak.

Efect of biomass type

The performance of magnetic biochar is closely related to the type of biomass from which it is prepared (Yi et al. [2019b](#page-9-16)). The infuence of biomass type on fuconazole adsorption by MBC and BMBC is shown in Fig. S6. The best adsorption capacity for fuconazole (nearly 3 mg/g) was observed with the magnetic biochar prepared from rice husk, while the fuconazole adsorption capacity of magnetic biochar synthesized from wheat straw was lowest $\left($ < 1.5 mg/g). However, no matter what type of biomass was used as a raw material to synthesize magnetic biochar, the adsorption capacity for fuconazole signifcantly improved after ball milling and ranged from 3 to 11 times that of magnetic biochar without ball milling. These results show that the benefts of ball milling are efective for all types of magnetic biochar.

Conclusion

In this paper, magnetic biochar was prepared by impregnation–pyrolysis and treated by ball milling. Ball milling efectively improved the adsorption rate and capacity of magnetic biochar for fuconazole. The mechanism of fuconazole adsorption by BMBC included $\pi-\pi$ interactions, H bonding, and complexation with O-containing functional groups. Batch experiments for fuconazole adsorption confrmed that BMBC was applicable across a wide range of pH and was resistant to interference. The results of fuconazole adsorption by BMBC from diferent biomass sources confrmed that ball milling is benefcial for diferent types of magnetic biochar.

Supplementary Information The online version contains supplementary material available at<https://doi.org/10.1007/s11356-021-17964-8>.

Author contribution Zhexi Huang: investigation, experiment, formal analysis, writing – original draft.

Yunqiang Yi: supervision, project administration, funding acquisition, writing original draft, software, writing – review and editing.

Nuanqin Zhang: investigation, formal analysis, writing – original draft.

Pokeung Eric Tsang: writing – review and editing. Zhanqiang Fang: writing – review and editing.

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Data availability The concerned data and materials are available from the principal investigator and corresponding author.

Declarations

Ethics approval Not applicable.

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Competing interests The authors declare no competing interests.

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