



Utilization of freshwater mussel (*Lamellidens marginalis*) for the isolation of proteins through pH shift processing: characterization of isolates

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Abstract

Study was conducted to use underutilized freshwater mussel (*Lamellidens marginalis*) for the recovery of proteins using pH shift method and to study the functionality and characteristics of the recovered isolates. From the pH range tested (pH 2.0–13.0), maximum protein yields were obtained during solubilization at pH 2.0 and pH 13.0 ($p < 0.05$). During the protein recovery process, pH 13.0 was found to have minimal effect on proteins resulting in higher protein yields compared to pH 2.0. Isolates obtained by both acidic and alkaline solubilization processes had low stability and poor gel network. Total lipid content, total myoglobin, and pigment contents were reduced significantly ($p < 0.05$) during pH shift processing, resulting in whiter protein isolates and protein gels. All the essential amino acids were present in the isolates recovered by acid and alkaline solubilization, indicating the complete recovery of amino acids. No microbial counts were observed in any of the isolates prepared using acid and alkaline-aided processing. Acid and alkaline solubilization (pH shift) process was found to be promising for the recovery of proteins from underutilized freshwater mussel thus by reducing the supply demand gap.

Keywords Mussel · Protein · pH shift · Acid · Alkali · Isolate

Introduction

In the last 50 years, the daily intake of protein particularly from meat, eggs, milk, and dairy products rose from 39 g per capita in 1961 to 52 g in 2011, a 33% increase. Between 1961 and 2011, the daily per capita availability of protein from animal products rose from 9 to 20 g, an increase of 116%, which is projected to reach 22 g by 25 g by 2050 (FAO 2017). This increasing demand for animal protein will create

a greater pressure on conventional animal protein resources, causing their quick depletion. Globally, fish contribute around 18% of the total animal protein intake (FAO 2009) and it will be a major target source for future protein needs. In order to withstand the pressure on aquatic resources, they must be managed before and after the catch. In this way, low-cost fish and by-products should be used for human edible purposes as they contain valuable nutrients, which is otherwise a serious loss to human kind (Surasani 2018). In order to serve the increasing demand for protein and protein foods, there is an urgent need to search for low-cost unconventional protein resources and freshwater mussels can be a good source with great future potential. The freshwater mussel *Lamellidens marginalis* is widely distributed in ponds and water bodies of India and is a very good source of many nutrients (Yusufzi et al. 2010). Despite of the huge resources and availability in India, these mussels are not used for human edible purposes, which is a huge loss to mankind. In view of reducing the gap between supply and demand for nutritious food, valuable nutrients from the freshwater mussels should be recovered and used for human edible purpose.

Preliminary work done by a few scientists (Niki et al. 1985; Huang et al. 1997, etc.) on the recovery of nutritional

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components from surimi wash water was not found satisfactory due to poor protein yields caused by the loss of water soluble components (Table 1). In the later stages, Hultin and Kelleher (1999, 2000) patented acid and alkaline solubilization process for the isolation of fish muscle proteins with better stability, functionality, and recovery yields. Thereafter, many researcher used this process for the isolation of proteins from different low-cost fish, fish by-products, and fish processing waste (Cortes-Ruis et al. 2001; Kristinsson and Demir 2003; Kristinsson and Ingadottir 2006; Fatin et al. 2015; Surasani et al. 2017a, b; Surasani et al. 2018). Protein recovery yields and functionality depends on the method used for the protein isolation and the source of raw material.

Utilization of processing wastes and low-cost fish and shellfish for human consumption will reduce pollution problems as well as demand supply gap and product cost (Surasani 2017). Due to the greater abundance of freshwater mussels in India and its rich nutritional profile, the objectives of the study were set to isolate proteins from freshwater mussels meat using pH shift method (acid and alkaline solubilization) method. Characteristics and functionality of the proteins isolated through pH shift processing of freshwater mussels were also studied.

Materials and methods

Raw material

Live mussels were procured from local water bodies (Ludhiana, India) and transported to the laboratory in live

Table 1 Recovery of mussel proteins during solubilization at different pH

pH	Protein recovery (%)
2.0	73.63 ^g ± 0.12
3.0	17.71 ^b ± 0.04
4.0	8.78 ^a ± 0.03
5.0	8.89 ^a ± 0.01
6.0	17.73 ^b ± 0.02
7.0	20.52 ^c ± 0.71
8.0	26.45 ^d ± 0.28
9.0	30.35 ^e ± 0.61
10.0	38.12 ^f ± 0.57
11.0	73.88 ^g ± 0.36
12.0	87.99 ^h ± 1.20
13.0	90.91 ⁱ ± 2.10

*One-way ANOVA, mean ± SD, $n = 3$; values in the same column having different letters as superscript are significantly different ($p < 0.05$)

Process conditions: temperature: 4 °C; homogenate weight to solvent ratio: 1:6; centrifugation speed: 5000 rpm; extraction time: 60 min

condition. The shells of the mussels were opened followed by shucking the meat and grinding using a laboratory mincer to a fine and thick paste. This paste was used as raw material for the isolation of proteins. All the preparatory and processing steps including raw material processing were performed at a temperature < 5 °C.

Proximate composition

The proximate composition (%), i.e., moisture, protein, ash, and fat content of the raw freshwater mussel meat, was determined by the method of AOAC (2000) (AOAC 950.46; AOAC 981.10; AOAC 920.153; AOAC 948.15). Protein content (%) of the sample was calculated by multiplying the obtained nitrogen value with factor of 6.25.

Preparation of homogenate

The meat paste obtained from the freshwater mussel was added with 6 volumes of cold deionized water and homogenized at 12,000 rpm for 60 s (2×30 s) using Ultra-Turrax homogenizer (Germany), equipped with T 25 element. After the homogenization, the homogenate was transferred to beakers for pH adjustment using 2 M HCl or 2 M NaOH under slow stirring condition (Surasani et al. 2017a, b). Diluted acid or alkali was used to keep the pH of the homogenate constant throughout the process.

Protein solubility

Solubility curve

pH of the homogenate, which was divided into different lots, was adjusted to pH 2.0 to 13.0 with 1.0 unit interval using 2 M HCl and 2 M NaOH. The solubility of proteins at each pH was calculated and used to draw the solubility curve. After the pH adjustment, 30 g of homogenate was taken at each pH and was transferred to 50-ml centrifuge tubes followed by centrifugation at $5000 \times g$ for 20 min using Sorvall ST 16R refrigerated centrifuge (Thermo Fisher Scientific, Germany). At each solubilization pH, 2 g of sample was taken before and after centrifugation to calculate total protein content using Biuret method (Robinson and Hogden 1940). Sample was diluted with cold de-ionized water (pH 11.0) to analyze the protein content, wherever is necessary.

Solubility after isoelectric precipitation

After constructing the protein solubility curve, pH with maximum solubility (pH 2.0 in acidic range and pH 13.0 in alkaline range) was selected and the homogenate was adjusted to these pH using 2 M HCl and 2 M NaOH under continuous stirring condition. After the pH adjustment, the homogenate

was kept for 60 min at 4 °C to aid protein solubilization (Surasani et al. 2017, b). This was followed by centrifugation at 5000×g for 20 min for separating the soluble fraction from insoluble matter. Supernatant was collected after screening through the two layered cheese cloth and was readjusted to precipitation pH of 5.5. pH adjusted samples were kept for 30 min at 4 °C to aid precipitation followed by centrifugation for 20 min at 5000×g. Two grams of sample was taken before and after the centrifugation to analyze the protein content using Biuret method.

Protein measurements

Total protein of homogenate was determined by taking a 2-g sample at each pH before centrifugation and diluting it 10 times with cold DI water at pH 11.0 to aid in solubilization of the proteins. The samples were homogenized with a hand held Tissue Tearor for 20 s and then analyzed for protein content using the Biuret method (Kristinsson and Ingadottir 2006). Supernatants were diluted 10 times with cold DI water at pH 11.0, followed by analyzing for protein content using the Biuret method. Ten percent deoxycholic acid was used to reduce the cloudiness formed by the lipids in the solution. T90+ UV/VIS spectrometer (PG Instruments Ltd., India) was used to read the absorbance at 540 nm. A standard curve with bovine serum albumin (BSA) (1–10-mg/ml concentration) was plotted and used for calculating protein concentrations based on the absorbance.

Protein recovery

Protein recovery at every step was expressed as recovery (%) and was calculated using the formula:

Protein recovery after 1st centrifugation :

$$\%Protein = \frac{(B \times W_B)}{(A \times W_A)} \times 100$$

Protein recovery after 2nd centrifugation : %Protein

$$= 100 - \left\{ \frac{(C \times W_C)}{(B \times W_B)} \times 100 \right\}$$

Total process recovery :

$$\%Protein = \left(\frac{(B \times W_B) - (C \times W_C)}{A \times W_A} \right) \times 100$$

where A: homogenate protein content, W_A: homogenate weight, B: protein content of supernatant obtained in 1st centrifugation, W_B: weight of the supernatant obtained in 1st centrifugation, C: protein content of the supernatant obtained in 2nd centrifugation, W_C: weight of the supernatant obtained in 2nd centrifugation.

Lipid content and its removal

Total lipids in the homogenate as well as protein isolates were estimated using soxhlet apparatus (AOAC 920.39B 2000). Lipid content (dry weight basis) was calculated using the formula:

$$\%Fat (dry weight) = \frac{g \text{ of fat in sample}}{g \text{ of dried sample}} \times 100$$

The reduction in lipid content was calculated using the formula:

$$Lipid \text{ reduction } (\%) = \left\{ 1 - \left(\frac{Lipid \text{ content of isolate}}{Lipid \text{ content of homogenate}} \right) \right\} \times 100$$

Total myoglobin content and its removal

Total myoglobin content in the homogenate as well as protein was estimated using the spectrometric method (Chaijan et al. 2006). Two grams of sample was added with 20 ml of 40 mM, pH 6.8 phosphate buffer and homogenized using a homogenizer at 3000×g for 30 min at 4 °C. The homogenate was filtered through Whatman no. 1 paper and the obtained supernatant/permeate was added with 0.2 ml of 1% (w/v) sodium dithionite and mixed well. The absorbance of the solution was measured at 555 nm using phosphate buffer (pH 6.8) as blank.

Myoglobin content was calculated using the formula:

$$Myoglobin \text{ content } (mg/g) = \frac{(A \times 16.111 \times F \times S \times WS \times 7.6)}{\times 100}$$

where A = absorbance, F = dilution factor, WS = sample weight in g, 7.6 = millimolar extinction coefficient, 16.111 = molecular weight.

Myoglobin removal (%) was calculated as:

$$\text{Myoglobin removal (\%)} = \left\{ 1 - \left(\frac{\text{myoglobin content in isolate}}{\text{myoglobin content in homogenate}} \right) \right\} \times 100$$

Total pigment content and its removal

Total pigments in the raw material as well as protein isolates were measured using the method of Rawdkuen et al. (2009). One-gram sample was added with 9 ml acetone acid (2% HCl, 90% acetone, and 8% deionized water) and incubated for 1 h. It was followed by filtration using Whatman no. 1 paper and the absorbance of the filtrate was measured at 640 nm with acetone as a blank. The concentration of pigments (hematin) was calculated by using the ratio of 680 and weight of the sample.

$$\text{Total pigment content (ppm)} = A_{640} \times 680$$

(A_{640} is the absorbance at 640 nm and 680 is the conversion factor for converting the total pigments into parts per million of hematin)

Total pigment removal (%) was calculated using the formula:

$$\text{Pigment removal (\%)} = \left\{ 1 - \left(\frac{\text{pigment content in isolate}}{\text{pigment content in homogenate}} \right) \right\} \times 100$$

Color analysis

Color was measured using HunterLab (Virginia, U.S.) as described by Lubana et al. (2016). Whiteness of the samples was calculated by using L (lightness), a (Red/Greenness) and b (Yellow/Blueness) values, obtained from the instrumental analysis.

$$\text{Whiteness} = 100 - \left\{ (100 - L^*)^2 + a^{*2} + b^{*2} \right\}^{1/2}$$

Foaming properties

Foaming capacity (%) and foaming stability (%) of protein isolates obtained by acid and alkaline solubilization were measured by using the methodology of Sathe et al. (1982). One gram of protein was dissolved in 50 ml distilled water by heating at 60 °C. The solution was homogenized at 9000 rpm for 5 min to prepare the foam. Homogenized solution was gently poured along the side wall into a measuring cylinder and the volume of foam was noted. The volume of foam was noted again after 30. Foaming capacity (%) was calculated as the ratio of volume of foam to the volume of original liquid. The foam stability (%) was calculated as the ratio of the initial volume of foam to the volume of foam after 30 min.

SDS-PAGE analysis

SDS-PAGE analysis was performed as per the method described by Laemmli (1970). Methodology of Harlow and Lane (1988) was used to prepare samples, reagents with slight modifications. Samples were added with 5× sample loading buffer (SDFCL, India) and incubated at 95 °C for 5 min and loaded into 5% stacking gel. Twelve percent gel was used to resolve proteins at a constant current of 20 mA for 3–4 h. Four-microgram broad range marker (SDFCL, India) was loaded on each gel. Gel was stained overnight with Coomassie Brilliant Blue R250 followed by destaining and observation of protein bands.

Amino acid analysis

Amino acid composition was analyzed using reverse phase HPLC on Water Picotag TM amino acids analysis system. Analysis was done after hydrolyzing the protein in the samples with 6 N HCl to yield free amino acid (Bidlingmeyer et al. 1984). The amino acid composition of protein isolates and raw material was expressed as g/100 g protein.

Microbial quality analysis

Microbial count of the raw material and protein isolates was determined by estimating the total plate count (AOAC 2000) and was expressed as CFU/ml or CFU/g.

Gel preparation

Protein isolate from mussel meat obtained through pH shift processing was cut into small pieces (1 cm thick) followed by mincing using a laboratory mincer. Salt (2.5%) was added to the isolates after adjusting the moisture of isolates to 80% (w/w). This mixture was finely mixed and chopped followed by stuffing into polyvinylidene chloride (PVC) casings with

2.5 cm diameter. Both ends of the stuffed casings were sealed tightly and kept for incubation for 30 min at 40 °C followed by heating for 20 min at 90 °C (Kristinsson and Ingadottir 2006). Heat set gels were kept in chilled water for 30 min and stored over night at 4 °C prior to analysis.

Gel quality analysis

Folding test

Folding test of protein gel was performed as per the method described by Kudo et al. (1973). Protein gel was cut into 3 mm slice and folded with hand at room temperature. The ability of gels to withstand the folding was assessed using a five point system. 5: No crack was observed after folding the gel into four, 4: no crack was observed when the gel was folded into two but there was a crack after folding it into four, 3: no crack was observed when the gel was folded into two but the gel was broken into two after folding it into four, 2: gel was cracked when it was folded into two, 1: gel was completely broken into two when it was folded into two.

Shear test

Shear/cutting test of the protein gels was performed using a texture analyzer as per the method used by Reddy (2016), with slight modification. Protein gels were cut using a blade set (HDP/BSW) with a test speed of 2 mm/s to 10 mm distance at 30 °C and 20 g force. Pre- and post-test speed of 2 mm/s was used. A total of six measurements were made for each lot and the average value was reported. A force-time graph was generated with a data acquisition rate of 200 pps and taxt-plus software was used to calculate the test results.

Expressible moisture

Expressible moisture content of the protein gels was measured using the method described by Feng and Hultin (2001). Protein gel was cut into 3-mm-thick pieces and was placed between five layers of Whatman filter paper. A standard metal weight of 3000 g was placed on the filter paper for 1 min. The difference in the weight of gel before and after pressing was used to calculate the expressible moisture content;

Expressible moisture (%)

$$= \frac{(\text{Pre pressed wei. of gel} - \text{after pressed wei. of gel})}{\text{Pre pressed wei. of gel}} \times 100$$

Statistics analysis

Results are expressed as mean \pm SD. Significant difference ($P < 0.05$) between the treatment attributes was analyzed using analysis of variance (ANOVA) and *t* test between treatments. SPSS Version 20 software was used for the analysis.

Results and discussion

Proximate composition

Protein recovery yields and their quality depend on the raw material composition and quality. Moisture, protein, fat, and ash content of the mussel meat used for the protein isolation was 79.88 ± 0.34 , 8.40 ± 0.22 , 1.04 ± 0.07 , and 2.63 ± 0.11 , respectively. Haldar et al. (2014) during their studies on mussel found the moderate amount of carbohydrate ($8.01 \pm 0.38\%$), protein ($8.30 \pm 0.67\%$) and less amount of crude fiber ($0.01 \pm .001\%$) and fat ($1.02 \pm 0.20\%$) in the mussel meat. Results obtained in this study were supported by previous reports.

Effect of pH on mussel protein solubility and recovery

Solubility and associated recoveries of the mussel proteins at each pH from pH 1.0 to 13.0 are given in Table 2. Maximum protein solubility was observed at pH 2.0 in the acidic pH range and at pH 13.0 in the alkaline pH range ($p < 0.05$). Maximum mussel protein was recovered at pH 13.0 (90.91%), while minimum protein recovery was observed at pH 4.0 and 5.0 (8.78 and 8.89%), respectively. A sudden increase in protein solubility was found when the pH was shifted from pH 3.0 to 2.0 and pH 10.0 to 11.0. Minimum protein solubility at pH 4.0–5.0 might be due to the low solubility of myosin, the major protein fraction with its isoelectric pH nearer to 5.0. When the pH is shifted either above or below of this pH range (pH 4.0–5.0), electrostatic repulsions between the proteins will be increased due to the increase in protein surface charges, causing more solubilization (Hamm

Table 2 Recovery of mussel proteins during acid and alkaline solubilization and precipitation

Recovery (%)	pH 2.0	pH 13.0
Recovery after 1st centrifugation	$83.31^a \pm 0.53$	$93.82^b \pm 0.09$
Recovery after 2nd centrifugation	$76.25^a \pm 0.06$	$89.68^b \pm 0.03$
Total process recovery	$63.08^a \pm 0.50$	$85.03^b \pm 0.07$

**T* test, mean \pm SD, $n = 3$; values in the same row having different letters as superscript are significantly different ($p < 0.05$)

Process conditions: temperature: 4 °C; homogenate weight to solvent ratio: 1:6; centrifugation speed: 5000 rpm; extraction time: 60 min

1994; Kelleher and Hultin 2000). The sudden increase in protein solubility was attributed to more ionizable groups, having pKa values between those pH values (Undeland et al. 2002). Similar results were also reported by Chen et al. (2007) and Surasani et al. (2017a, b).

Process yields are very much important in any extraction process, on which the viability of the process depends (Surasani et al. 2018). Recovery yields obtained during mussel protein isolation through pH shift processing are given in Table 3. High protein yields were obtained by alkaline-aided processing than the acid-aided processing ($p < 0.05$). The total process recoveries obtained during acid- and alkaline-aided processing of mussel proteins were 63.08 and 85.03%, respectively. Similar results were reported by Varelziz and Undeland (2012) during their studies on blue mussel. They reported that acid-aided (pH 2.6) and alkaline-aided (pH 12.0) processing of blue mussel gave recovery yields of 43.0% and 58.0%, respectively. Solubilization of common carp proteins at pH 12.5 and pH 2.5 gave protein yields of 87.6% and 76.3%, respectively (Tian et al. 2016). Acid- and alkaline-aided solubilization of sardine proteins resulted in protein yields of 73.0 and 77.0%, respectively. Acid solubilization of common carp and silver carp gave protein yields of 70.20% and 75.18%, while alkaline solubilization resulted in the protein yields of 64.5% and 80.89%, respectively (Shabanpour et al. 2015). Similar findings were also reported by Surasani et al. (2017a, 2018) during acid and alkaline processing of pangas proteins.

Characteristics of isolates

Color

Color values of mussel protein isolates and protein gels made of isolates recovered by pH shift process are given in Table 4. Protein gels were found to have highest L (lightness) and whiteness values followed by isolates and raw material ($p < 0.05$). None of the color values showed significant differences between the isolates and their gels. Raw material was

found to have low values of b (yellowness) and high values of a (redness) than protein isolates and gels indicating the significant removal of the pigments during acid and alkaline solubilization process. pH shift processing caused an increase in L (lightness) values and decrease in a (redness) values, resulting in higher whiteness of isolates (Panpipat and Chaijan 2016). Color of isolates and their gels in the present study followed the same trend as reported by earlier studies. Nolsøe et al. (2011) reported that the whiteness values were maximum for blue whiting surimi gels, followed by protein isolates and starting mince. Similar findings were observed in the present study. The lower whiteness values for protein isolates compared to their gels might be due to differences in light reflection from the protein-protein aggregations.

Total lipid, myoglobin, and pigment content

Total lipids, pigments, and myoglobin content in the raw material as well as the protein isolates were reduced significantly by acid- and alkaline-aided solubilization (Table 6). Acid-aided process could cause greater removal of total lipids (88.48%), compared to alkaline-aided process (83.91%). During the alkaline solubilization, there might be a reaction between lipids and the added alkali that caused the soap formation and associated co-precipitation of lipids during the isoelectric precipitation process (Panpipat and Chaijan 2016). Surasani et al. (2018) found that the acidic and alkaline processing caused lipid reductions of 97.11 and 90.33% in pangas protein isolates. Rawdkuen et al. (2009) and Kristinsson et al. (2005) observed lipid reductions of 85.2% and 85.4% during the pH shift processing of tilapia and catfish muscle concentrates, respectively. Lipid reductions obtained through pH shift processing of mussel protein isolates were supported by the earlier findings (Batista et al. 2007; Freitas et al. 2015; Surasani et al. 2018).

pH shift processing resulted in significant reductions ($p < 0.05$) of myoglobin content in the mussel protein isolates (89.11 and 89.47%). There was no significant difference found between the removal percentage of these two processes.

Table 3 Color values of fish protein gels and protein isolates recovered at pH 2.0 and pH 13.0

Sample	L value	a value	b value	Whiteness
Raw material	44.77 ^a ± 0.89	2.86 ^c ± 0.63	15.66 ^a ± 0.63	42.51 ^a ± 0.83
pH 2.0 isolate	52.26 ^b ± 0.96	1.64 ^a ± 0.17	17.42 ^b ± 0.29	49.15 ^b ± 0.92
pH 13.0 isolate	50.70 ^b ± 0.96	1.70 ^a ± 0.35	17.82 ^b ± 0.89	47.54 ^b ± 0.97
pH 2.0 gel	55.04 ^c ± 0.82	1.84 ^{ab} ± 0.13	16.07 ^{ab} ± 1.65	52.19 ^c ± 0.27
pH 13.0 gel	55.3 ^c ± 1.09	2.08 ^b ± 0.11	18.14 ^b ± 1.34	51.77 ^c ± 1.51

*One-way ANOVA, mean ± SD, $n = 3$; values in the same column having different letters as superscript are significantly different ($p < 0.05$)

Process conditions: temperature: 4 °C; homogenate weight to solvent ratio: 1:6; centrifugation speed: 5000 rpm; extraction time: 60 min

Table 4 Total pigment, lipid, and myoglobin content of mussel protein isolates recovered at pH 2.0 and pH 13.0

Properties	Raw material	pH 2.0 isolate	pH 13.0 isolate
Lipid content (%)	1.04 ^b ± 0.07	0.12 ^a ± 0.02	0.16 ^a ± 0.02
Lipid removal (%)		88.48 ^b ± 0.73	83.91 ^a ± 2.11
Total pigment content (ppm)	58.93 ^c ± 1.71	32.18 ^a ± 0.39	36.04 ^b ± 1.36
Pigment removal (%)		45.35 ^b ± 1.64	38.85 ^a ± 0.57
Total myoglobin content (ppm)	460.71 ^b ± 9.26	50.16 ^a ± 3.40	48.39 ^a ± 5.33
Myoglobin removal (%)		89.11 ^a ± 0.68	89.47 ^a ± 1.33
Foaming capacity (%)		50.93 ^b ± 1.44	43.48 ^a ± 1.27
Foaming stability (%)		45.16 ^a ± 0.92	49.71 ^b ± 1.27

*One-way ANOVA and *T* test, mean ± SD, *n* = 3; values in the same row having different letters as superscript are significantly different (*p* < 0.05)

Process conditions: temperature: 4 °C; homogenate weight to solvent ratio: 1:6; centrifugation speed: 5000 rpm; extraction time: 60 min

Similar observations were made by Surasani et al. (2018) during protein isolation from pangas waste. When compared to surimi processing, pH shift process caused significant reductions in the myoglobin content of the protein isolates (Chaijan et al. 2006; Rawdkuen et al. 2009). Factors that influence the efficiency to extract myoglobin include type of fish, variety and composition of raw material used, washing process, and the time of storage (Chaijan and Benjakul 2006).

Pigment content was also reduced significantly during acid and alkaline solubilization process (*p* < 0.05). Acid- and alkali-aided solubilization caused a pigment reduction of 45.35% and 38.85%, respectively. Similar results were observed by Panpipat and Chaijan (2016) and Surasani et al. (2018) during their studies on protein isolation from big eye snapper and pangas. Extreme acidic pH might have caused the degradation of heme pigments resulting in high pigment removal, compared to alkaline pH (Panpipat and Chaijan 2016). Another reason for this might be the proton-catalyzed displacement process and a protoporphyrin IX ring destruction at high acidic pH that promoted haem loss (Chaijan and Undeland 2015). Similar observations were also made by Jafarpour et al. (2013) and Shabanpour et al. (2015).

Foaming capacity and foaming stability

Foaming properties of mussel proteins recovered by pH shift process are presented in Table 5. Proteins obtained by acid-aided solubilization were found to have high foaming capacity, than the proteins obtained by alkali-aided solubilization (*p* < 0.05). These differences might be due to the difference in hydrophobic residues of proteins (Surasani et al. 2017a, b). Similar observations were made by Surasani et al. (2018) during their studies on pangas protein isolates. Information on foaming properties of pH shift processed proteins is scanty. Improvement in foaming capacity can be done by reducing the surface tension and by increasing the exposure of hydrophobic residues at air-water interface (Mutilangi et al. 1996). The additional hydrophobic residues at air-water interface can form a large hydrophobic sphere on surface that will result in excess foaming (Jongjareonrak et al. 2010).

Foam stability is the measure of protein-protein interaction in the matrix (Mutilangi et al. 1996; Jongjareonrak et al. 2010). In this study, proteins obtained by alkali-aided solubilization were found to have high foam stability, than the proteins obtained by acid-aided solubilization (*p* < 0.05). These

Table 5 Physical quality of protein gels obtained from the mussel protein isolates recovered at pH 2.0 and pH 13.0

Attributes	pH 2.0 protein gel	pH 13.0 protein gel
Expressible moisture content (%)	42.05 ^b ± 0.33	31.70 ^a ± 0.29
Folding test score	1.0 ^a ± 0.0	1.0 ^a ± 0.0
Cutting strength (N)	0.28 ^a ± 0.01	1.37 ^b ± 0.14
Distance at failure (mm)	7.12 ^a ± 0.56	9.83 ^b ± 0.16
Work of shear (N.sec)	0.79 ^a ± 0.11	4.55 ^b ± 0.75

**T* test, mean ± SD, *n* = 3; values in the same row having different letters as superscript are significantly different (*p* < 0.05)

Process conditions: temperature: 4 °C; homogenate weight to solvent ratio: 1:6; centrifugation speed: 5000 rpm; extraction time: 60 min

differences in foam stability might be because of protein aggregation that interferes the protein water interactions needed for the formation of foam (Kinsella 1976). Similar observations were made by Surasani et al. (2018) during their studies on pangas proteins.

SDS-PAGE pattern

SDS-PAGE analysis of mussel proteins showed that the protein bands ranging from 6–10 to 200 kDa (Fig. 1). Protein in the supernatants obtained using acid- and alkali-aided solubilization had a band of 124 kDa, which might be the dissociated fraction of heavy meromyosin. All the protein samples showed a band at approximately 43 kDa, which might be actin. Acid-solubilized protein showed more number of bands compared to alkaline-processed protein, including bands at approximately 6–10 kDa which might be due to protein denaturation at extreme acidic pH and associated proteolysis. Similar observations were recorded by Varelziz and Undeland (2012) during protein recovery from blue mussel. During the pH shift process, proteolytic enzymes will be activated, causing hydrolysis of heavy meromyosin chain (Kelleher and Hultin 2000). Maximum number of protein bands were disappeared in supernatants obtained after 2nd centrifugation indicating the maximum protein precipitation and recovery. Similar findings were reported by Kristinsson and Liang (2006), Varelziz and Undeland (2012), and Surasani et al. (2018).

Amino acid profile

Amino acid profile of mussel meat homogenate and protein isolates obtained through pH shift processing is given in Table 6. In the present study, the effect of processing on amino acids was minimum and all the amino acids that were present in the homogenate were recovered into isolates. The total number of essential amino acids that were present in the homogenate were also found in the protein isolates, indicating

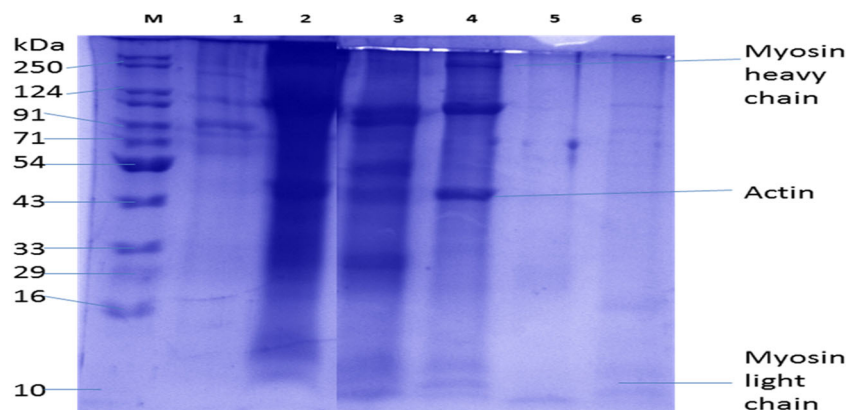
Table 6 Amino acid profiling of the mussel meat and protein isolates recovered at pH 2.0 and pH 13.0

Amino acid	Raw mussel meat	pH 2.0	pH 13.0
Aspartic acid	√	√	√
Glutamic acid	√	√	√
Serine	√	√	√
Glycine	√	√	√
Histidine	√	√	√
Arginine	√	√	√
Threonine	√	√	√
Alanine	√	√	√
Proline	√	√	√
Tyrosine	√	√	√
Valine	√	√	√
Methionine	√	√	√
Cystine	√	√	√
Isoleucine	√	√	√
Leucine	√	√	√
Phenylalanine	√	√	√
Lysine	√	√	√

“√” presence of amino acid, “x” absence of amino acid

their complete recovery. Álvarez et al. (2017) during their studies on ultrasound-assisted protein recovery from mackerel stated that pH shift processing could recover all the amino acids that were present in the homogenate. Similar observations were noted by Surasani et al. (2017a, 2018) during their studies on protein isolates recovered from pangas waste. They found that the pH shift processing recovered all the amino acids that were present in the homogenate. Findings in the present study are in agreement with the earlier findings. Some recent studies also reported that pH shift process caused enrichment of essential amino acids in the protein isolates (Surasani et al. 2017a and 2018). However, the final amino acid profile of the protein isolates obtained through pH shift processing depends on the quality of raw material used and the pH at which the protein was solubilized.

Fig. 1 SDS-PAGE profile of the mussel proteins and the protein isolates recovered at pH 2.0 and pH 13.0. M. protein marker; 1. pH 2.0 homogenate; 2. pH 13.0 homogenate, 3. Supernatant after 1st centrifugation obtained at pH 2.0; 4. Supernatant after 1st centrifugation obtained at pH 13.0; 5. Supernatant after 2nd centrifugation obtained at pH 2.0; 6. Supernatant after 2nd centrifugation at pH 13



Microbial stability

During food production and storage, one of the important parameters to measure is its microbial quality (Nolsøe and Undeland 2009). Immediately after harvesting, live fish or fresh fish are dominated by psychrotrophic Gram negative bacteria (Huss 1983). Acid- or alkali-aided processing results in extreme food pH that has a killing effect on microbes (Jay 1986). In the present study, raw mussel meat had a total plate count of 4.56×10^2 , while isolates showed no microbial counts. Similar reports were published by Surasani et al. (2017a, b) and Surasani et al. (2018) during their studies on protein isolates recovered from pangas and rohu processing waste.

Gel quality

Gel texture Shear test results of the protein gels made of mussel protein isolates are given in Table 5. Gels from mussel proteins obtained by acid-aided processing had low shear strength and work of shear values than the protein gels from alkali-aided processing ($p < 0.05$). Lower shear test values of protein gels from acid process indicate poor gel network resulting poor gel strength, which is also supported by the high expressible moisture content ($p < 0.05$). Surasani et al. (2018) and Kristinsson and Liang (2006) observed that the protein gels obtained from the acid-aided processing of pangas and tilapia had better gel strength compared to protein gels from alkali-aided processing. Similar findings were reported by Hultin and Kelleher (1999) during protein recovery from mackerel and cod. Differences in gel forming ability are due to the effect of processing on protein integrity and bonding (Chaijan et al. 2006). Factors that influence protein gelling ability include type of fish or species, extraction method used, and the time of extraction (Freitas et al. 2015).

Expressible moisture content Expressible moisture is the measure of integrity of the gel to hold water. Expressible moisture content (%) of gels from proteins obtained by acid-aided processing was high than the protein gels from alkali-aided processing ($p < 0.05$), indicating the poor gel network of acid-processed proteins (Table 5). During the studies on proteins recovered from pangas processing waste, Surasani et al. (2018) found that proteins from acid-aided processing had gels with low expressible moisture content than gels made of alkali-processed proteins. Similar observations were made by Freitas et al. (2011) and Fatin et al. (2015) during their studies on Argentine anchovy residue and Japanese scad proteins. In the present study, a reverse trend was observed, which might be due to protein denaturation at extreme acidic pH than alkaline pH.

Folding test Gels made of protein isolates obtained by acid- and alkali-aided solubilization had an average folding test score of 1, indicating the poor gelling ability of these proteins. Gels made of herring protein isolates had very strong gels that had folding test score of 5 (Marmon and Undeland 2010). Surasani et al. (2018) reported that the gels made of acid- and alkaline-processed isolates of pangas had folding test scores of 5 and 1, indicating the strong gel network in gels made of acid-processed proteins, compared to alkaline-processed isolate gel. In the present study, gels made of both acid- and alkali-processed isolates had poor gel network which might be due to protein denaturation at extreme pH values during the extraction process.

Conclusions

Proteins from freshwater mussel meat can be recovered using pH shift processing with good yields and functionality. Alkali-aided process was found to be more satisfactory for recovering proteins from mussel proteins, as acid-aided processing resulted in low protein yields and weaker protein gels. Despite of the higher yields, proteins obtained by alkali-aided solubilization had poor functionality, which might be due to protein denaturation at high alkaline pH. Further studies are needed to find out the optimum alkaline pH that can result in minimum protein denaturation and maximum yields. pH shift processing found to be promising in the utilization of freshwater mussels for the recovery of functional proteins thus by reducing the supply demand gap as well pollution problems.

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