



# Study on the copper(II)-doped MIL-101(Cr) and its performance in VOCs adsorption

Dongfang Wang<sup>1</sup> · Guiping Wu<sup>2</sup> · Yufeng Zhao<sup>3</sup> · Longzhe Cui<sup>2</sup> · Chul-Ho Shin<sup>4</sup> · Moon-Hee Ryu<sup>1</sup> · Junxiong Cai<sup>5</sup>

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## Abstract

The metal-organic framework (MOF) materials, MIL-101(Cr), and copper-doped MIL-101(Cr) (Cu@MIL-101(Cr)) were prepared through hydrothermal method and were used to remove volatile organic compounds (VOCs) in this study. Morphological characterization demonstrated that MIL-101(Cr) and Cu-3@MIL-101(Cr) were octahedral crystal, with specific surface area of 3367 and 2518 m<sup>2</sup>/g, respectively. The results of XRD, TG, and FTIR showed that the copper doping procedure would not alter the skeleton structure, but it would affect the crystallinity and thermal stability of MIL-101(Cr). Besides, MIL-101(Cr) and Cu-3@MIL-101(Cr) displayed good removal efficiencies on benzene sorption, and the maximum sorption capacity was 103.4 and 114.4 mg/g, respectively. In competitive adsorptions, the order of adsorption priority on Cu-3@MIL-101(Cr) was as follows: ethylbenzene > toluene > benzene. Hence, it could be concluded that MIL-101(Cr) and copper-doped MIL-101(Cr) demonstrated good performance in VOCs adsorption and showed a promising potential for large-scale applications in the removal of VOCs.

**Keywords** MIL-101(Cr) · Cu doping · Hydrothermal method · Volatile organic compounds · Adsorption

## Introduction

Porous materials are always hot topics in research due to their special structural properties. In the late twentieth century, a novel kind of material, metal-organic frameworks (MOFs), was firstly reported by Hoskins (Hoskins and Robson 1989)

in 1989. This new material was composed of metal ions or metal ion clusters and multi-topic organic ligands (such as ethylenediamine, terephthalic acid, and glycine) and synthesized through the coordination reaction. So that, MOFs have a variety of tunable properties, such as charge, polarity, redox potential, photoactivity, hydrophobicity/hydrophilicity,

## Highlights

The adsorption behavior and mechanism of VOCs on MIL-101(Cr) and modified MIL-101(Cr) were investigated.

The copper-doped MIL-101(Cr) showed better adsorption performance of benzene than that of the metal-free MIL-101.

Surface pore diameter and polarity of MIL-101 were important factors affecting the adsorption capacity and affinity for VOCs.

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✉ Moon-Hee Ryu  
ryumoonhee123@gmail.com

✉ Junxiong Cai  
cjsxhbjkx@163.com

<sup>1</sup> Division of Biotechnology, College of Environmental and Bioresource Sciences, Chonbuk National University, Iksan 570-752, Republic of Korea

<sup>2</sup> College of Resources and Environmental, South-Central University for Nationalities, Wuhan 430-074, China

<sup>3</sup> Division of Semiconductor and Chemical Engineering, Chonbuk National University, Jeonju 561-756, Republic of Korea

<sup>4</sup> Seohae Environment Science Institute, Jeonju 561-211, Republic of Korea

<sup>5</sup> Hubei Academy of Environmental Sciences, Wuhan 430-072, China

aromatic/lipophilic character, and stereochemistry (Hasan and Jhung 2015; Liu et al. 2014). Besides, one of the most important features is that the synthesis process, which combines merits of numerous metal ions or clusters and organic ligands, can offer copious structural topologies with various porosities (Ahmed and Jhung 2014). Therefore, compared with other porous materials, due to the designability of assembly approach, MOFs have almost unlimited structural models. To date, MOFs have drawn immense attention, and a large number of MOF structures have been created and produced for multifarious applications, such as gas adsorption/storage (Wang et al. 2014a), separation (Li et al. 2015), sensors (Liu et al. 2013), magnetism (Wang et al. 2014b), drug delivery (He et al. 2014), as well as catalysis (Chen et al. 2015). During the many MOFs, MIL-101(Cr), which was designed by Férey et al. (2005) in 2005, has a cubic structure with both great pore volume and uniform pore size. As reported, MIL-101(Cr) has two kinds of quasi spherical cages with the internal diameters of 29 and 34 Å, and accessible through microporous windows of 12 and 16 Å, respectively (Férey et al. 2005). It exhibits good adsorption properties for gas adsorption and storage. Prasanth et al. (2011) studied the adsorption of H<sub>2</sub> on composite materials prepared by MIL-101(Cr) and single wall carbon nanotubes. The results showed that after being combined with single wall carbon nanotubes, the adsorption capacity of H<sub>2</sub> onto MIL-101(Cr) increased from 6.37 to 9.18 wt.% (77 K, 60 bar) and 0.23 to 0.64 wt.% (298 K, 60 bar), respectively. Darunte et al. (2016) prepared an amine-modified MOF material, MIL-101(Cr)-PEI-800, with poly(ethylene imine) (PEI-800) and studied its capturing ability for CO<sub>2</sub> in simulated air. According to the results, the adsorption capacity of MIL-101(Cr)-PEI-800 for CO<sub>2</sub> strongly depended on the amount of amine loading and achieved pseudoequilibrium CO<sub>2</sub> adsorption of 1.35 mmol/g with PEI-800 loading of 1.76 mmol/g MOF.

Recently, air pollutants have attracted wide attention because they are harmful to human health, ecosystems, and atmosphere, especially volatile organic compounds (VOCs). It cannot only cause the greenhouse effect and lead to global warming, but also increase the ozone depletion in the stratosphere and the formation of ozone in the troposphere (Durmusoglu et al. 2009). VOC pollution has gradually become the global environmental issue, which makes many researchers begin to investigate. Considering the structural characteristics, numerous scholars tried to explore the application of MOFs in VOC adsorption. Zhao et al. (2011a) synthesized MIL-101(Cr) through microwave synthesis method, and its uptake of benzene was 16.5 mmol/g at 56 mbar and 288 K. Kun and his co-workers (Yang et al. 2013) reported the MOF-177 which was obtained through solvothermal synthesis at 85 °C for 48 h. The results showed that the adsorption capacity of VOCs on MOF-177 was more than 200.0 mg/g, especially the adsorption capacities of benzene and acetone were as high

as 800.0 mg/g and 589.0 mg/g, respectively. Huang et al. (2011) designed a quartz crystal microbalance system to probe the adsorption behavior of MIL-101(Cr) for VOCs and proved that MIL-101(Cr) had high affinity to the VOCs which are composed of heteroatom or aromatic ring and the adsorption capacity could be controlled by adjusting the unsaturated metal sites. Thus, MOFs, with high adsorption ability and affinity to VOCs, are promising materials for the adsorption and storage of VOCs.

To improve the adsorption properties of MOFs, a feasible method is importing unsaturated metal sites into the adsorbent, and there are mainly two approaches to carry it out (Dincă and Long 2008; Zhou et al. 2008). One is that after synthesizing of MOF materials, new unsaturated metal sites can be formed by heating or vacuumizing through dislodging the weakly bound guest water and residual solvent molecules from the metal coordination sites. Llewellyn et al. (2008) had removed the water molecules which were combined with Cr trimers in MIL-101. As a result, the adsorption capacity of CO<sub>2</sub> on MIL-101(Cr) increased from 28.0 to 40.0 mmol/g at 50 bar and 304 K. The second way is inserting metal ions into MOFs by post-synthesized method. Bloch et al. (2010) reported that when copper (II) ions were supported in MOF-253, although the BET surface areas decreased from 2160 to 705 m<sup>2</sup>/g, the adsorption percent of CO<sub>2</sub> on MOF-253 increased from 6.2 to 11.7 wt.%. In addition, many researchers had also proved that embedding copper nanoparticles into MOFs materials can enhance gas uptake activity (Wang et al. 2012; Yang 2012). Copper nanoparticles are very useful materials for their remarkable conductivity, good biocompatibility, and economical cost. These properties make them popular and widely utilized in many applications (Gwilherm et al. 2008; Kidwai et al. 2010; Mitsudome et al. 2008).

The purpose of this work was to explore the adsorption performance of MIL-101(Cr) and copper-doped MIL-101(Cr) on VOCs at atmospheric pressure and room temperature. The MIL-101(Cr) and copper-doped MIL-101(Cr) (Cu@ MIL-101(Cr)) were synthesized and the characterizations were analyzed by X-ray diffraction (XRD), Brunauer–Emmett–Teller (BET) analysis, scanning electron microscopy (SEM), transmission electron microscopy (TEM), X-ray photoelectron spectroscopy (XPS), thermogravimetry (TG), and Fourier transform infrared spectroscopy (FTIR). Then, a suitable experimental scheme, i.e., isotherms, kinetics, and competitive adsorption, was designed and carried out.

## Experimental section

### Materials

All reagents used in this work were at least analytical grade. Chromium nitrate (99%, Cr(NO<sub>3</sub>)<sub>3</sub>·9H<sub>2</sub>O), copper nitrate

(99%,  $\text{Cu}(\text{NO}_3)_2 \cdot 3\text{H}_2\text{O}$ ), terephthalic acid (99%,  $\text{C}_8\text{H}_6\text{O}_4$ ), hydrofluoric acid (40 wt.%, HF), dimethylformamide (99.5%,  $\text{HCON}(\text{CH}_3)_2$ ), methanol (99.9%,  $\text{CH}_3\text{OH}$ ), ethanol (99.7%,  $\text{CH}_3\text{CH}_2\text{OH}$ ), trichloromethane (98%,  $\text{CHCl}_3$ ), benzene (99.5%,  $\text{C}_6\text{H}_6$ ), toluene (99.5%,  $\text{C}_7\text{H}_8$ ), and ethylbenzene (99.5%,  $\text{C}_8\text{H}_{10}$ ) were purchased from Sinopharm Chemical Reagent Co., Ltd. (Shanghai, China) and were used as received from vendors without further purification.

### Synthesis of MIL-101(Cr) and Cu@MIL-101(Cr)

Hydrothermal method was employed to synthesize MIL-101(Cr) as previous literatures (Férey et al. 2005). In this study, some steps were improved as following: 4.042 g of chromium nitrate (10 mM), 1.342 g of terephthalic acid (8 mM), and 125  $\mu\text{L}$  of hydrofluoric acid (40 wt.%) were added to 70 mL deionized water; then, the mixture was blended by sonication for 30 min and transferred into a teflon-sealed reaction kettle. The reaction kettle was kept in an oven at 210 °C for 8 h. After that, the green samples were obtained by being washed with deionized water and dried in a vacuum oven at 80 °C for 12 h. Afterwards, the dried samples were purified by dimethylformamide (DMF) in Soxhlet extraction system for 3 h. The purification process was repeated thrice. Finally, the resulted crystals were washed three times using chloroform ( $\text{CHCl}_3$ ) and then dried in a vacuum oven for 12 h at 80 °C for subsequent experiments.

Synthesis procedures of Cu@MIL-101(Cr) were as follows: 4.042 g of chromium nitrate (10 mM) and various concentration of copper nitrate (0.244 g, 10 wt.%; 0.488 g, 20 wt.%; 0.732 g, 30 wt.%) were added to 70 mL deionized water in a beaker, then 1.342 g of terephthalic acid (8 mM) was added slowly with continuous stirring. The following experimental steps were the same as the synthesis process of MIL-101(Cr) mentioned previously, and the products were marked as Cu-1@MIL-101(Cr), Cu-2@MIL-101(Cr), and Cu-3@MIL-101(Cr), respectively.

### Instrumental information

X-ray diffraction (XRD) patterns were measured by X-ray diffractometer (Bruker Advanced D8, Germany), which was operated at 40 kV for Cu  $\text{K}\alpha$  ( $\lambda = 1.5418 \text{ \AA}$ ) radiation from 3° to 30° ( $2\theta$  angle range) with a scanning speed of 3°/min. The pore properties were characterized with nitrogen adsorption/desorption at liquid nitrogen temperature (77 K) by using Autosorb-1C-Ms (Quantachrome, USA). The surface morphology and element information were carried out by a scanning electron microscope (SEM, supra 40vp, Carl Zeiss, Germany) operated at 10.0 kV and a combined WDS/EDS (JEOL, JSM-6000 series WDS/EDS system, Japan), and the transmission electron microscope (TEM, Tecnai G20, FEI, USA) images were taken at 80 kV. X-ray photoelectron

spectroscopy (XPS) was conducted on AXIS-NOVA (Kratos Analytical, UK), which used a monochromic Mg  $\text{K}\alpha$  X-ray source to determine the atoms on the surface of the samples. All binding energies were corrected based on the neutral C 1s peak at 284.6 eV to remove the surface charging effects. The thermal stability was studied with thermal gravimetric analysis (TGA, TG 209 F3, Netzsch, German) by heating the samples from 30 to 600 °C with a rate of 5 °C/min in nitrogen atmosphere. The FTIR spectrum (Nicolet-6700, Thermo, USA), in the wavenumber range from 4000 to 400  $\text{cm}^{-1}$ , was determined with KBr as the standard substance. VOC concentrations were investigated by a gas chromatograph (Shimadzu GC-2010, Japan) equipped with a flame ionization detector.

### Adsorption experiments

Adsorption experiments were implemented in a sealed glass vessel with a mini fan. Before experiments, remove the air in the glass vessel as much as possible by using a vacuum pump. After that, a certain amount of VOC solution was added into the glass vessel and insured that the VOC solution was volatilized completely (the concentration of VOCs in the glass vessel kept constant). Then, adsorbents were added into the glass vessel and the concentrations of VOCs were determined by using a GC-FID equipment when the adsorption equilibrium was reached. The adsorption capacity of MOFs for VOCs was calculated by the following equation:

$$q_e = \frac{(c_0 - c_e)V}{m} \quad (1)$$

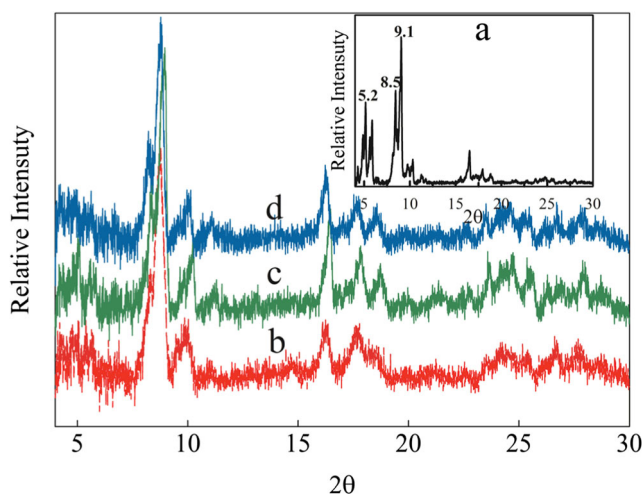
where  $q_e$  is the adsorbed amount of VOCs per gram of adsorbent in equilibrium (mg/g),  $C_0$  and  $C_e$  are the initial and equilibrium VOC concentrations ( $\text{mg}/\text{m}^3$ ), respectively.  $V$  is the working volume (L), and  $m$  is the dried mass of adsorbent (g).

### Effect of adsorbent dosage

A series of adsorption experiments were carried out with different sorbent dosage from 0.01 to 0.04 g/L in the glass vessel which contained 600  $\text{mg}/\text{m}^3$  of benzene at room temperature. The concentrations of benzene were determined as mentioned before and the removal rate was studied by Eq. (2):

$$R = \frac{c_0 - c_e}{c_0} \times 100\% \quad (2)$$

where  $R$  is the removal efficiency of the VOCs on the adsorbent (%),  $C_0$  and  $C_e$  are the initial and equilibrium VOC concentrations ( $\text{mg}/\text{m}^3$ ), respectively.



**Fig. 1** XRD pattern of various adsorbents (**a** (inset) MIL-101(Cr); **b** Cu-1@MIL-101(Cr); **c** Cu-2@MIL-101(Cr); **d** Cu-3@MIL-101(Cr))

### Adsorption kinetics

Kinetic experiments were undertaken as following process: 0.1 g of adsorbent was added into the glass vessel in which 600 mg/m<sup>3</sup> of benzene was prepared previously. Samples were collected at a fixed time interval and the residual concentrations were analyzed by GC. The uptake of VOCs at time  $t$ ,  $q_t$  (mg/g), was calculated by the following formula:

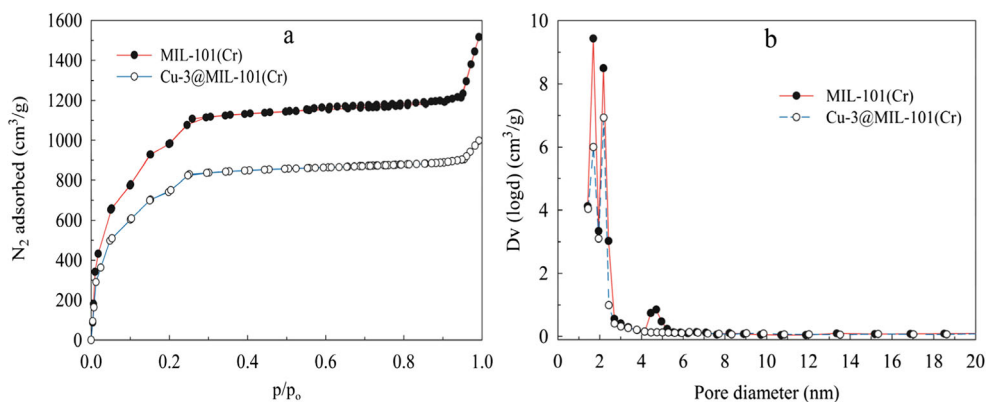
$$q_t = \frac{(c_0 - c_t)V}{m} \quad (3)$$

where  $C_t$  is the concentration of VOCs at any time  $t$  (mg/m<sup>3</sup>). The kinetic mechanism was evaluated by non-linear pseudo-first-order and pseudo-second-order models.

### Adsorption isotherms

Isotherm experiments were conducted with the initial concentrations of VOCs in the range from 0 to 2000 mg/m<sup>3</sup> and adsorbent dosage of 0.02 g/L at room temperature. Similarly, the concentrations of VOCs were determined by GC.

**Fig. 2** **a** N<sub>2</sub> adsorption isotherms and **b** pore size distributions (N<sub>2</sub> isotherms were measured at 77 K)



### Competitive adsorption study

Competitive adsorption studies were carried out to investigate the adsorption behavior and patterns of Cu-3@MIL-101(Cr) in the mixed compounds, namely benzene, toluene, and ethylbenzene. To explore the impact of concentration on adsorption pattern, concentrations of 500, 1000, and 1500 mg/m<sup>3</sup> were chosen to represent low, medium, and high concentration levels, respectively. Firstly, the same concentration of benzene and ethylbenzene (500, 1000, and 1500 mg/m<sup>3</sup>) was prepared in the glass vessel, then 0.02 g/L of Cu-3@MIL-101(Cr) was added. When the reaction reached equilibrium, the adsorption capacities of VOCs were calculated by Eq. (1). After that, competitive adsorptions between benzene and toluene and toluene and ethylbenzene were studied under the initial concentration of 1500 mg/m<sup>3</sup>, respectively.

## Results and discussion

### Characterization

#### X-ray diffraction analyses

The powder X-ray diffraction patterns of MIL-101(Cr) (Fig. 1a) and Cu@MIL-101(Cr) (Fig. 1b–d) showed that all of the XRD patterns contained the main peaks at 5.2°, 8.5°, and 9.1° which were highly coincident with that of MIL-101(Cr) reported in previous literature (Chen et al. 2013; Férey et al. 2005; Zhao et al. 2011b). It indicated that the products of MIL-101(Cr) were successfully synthesized in this work, and furthermore, copper doping did not change the cage construction of MIL-101(Cr) regardless of the different metal contents (XRD pattern of MIL-101(Cr) prepared by original method was showed in Fig. S1). However, there were some differences in the patterns when the copper was doped into MIL-101(Cr). Especially with the increase of Cu concentration, the XRD patterns showed more impure peaks and lower peak intensity. It implied that copper doping would

**Table 1** Texture properties of materials

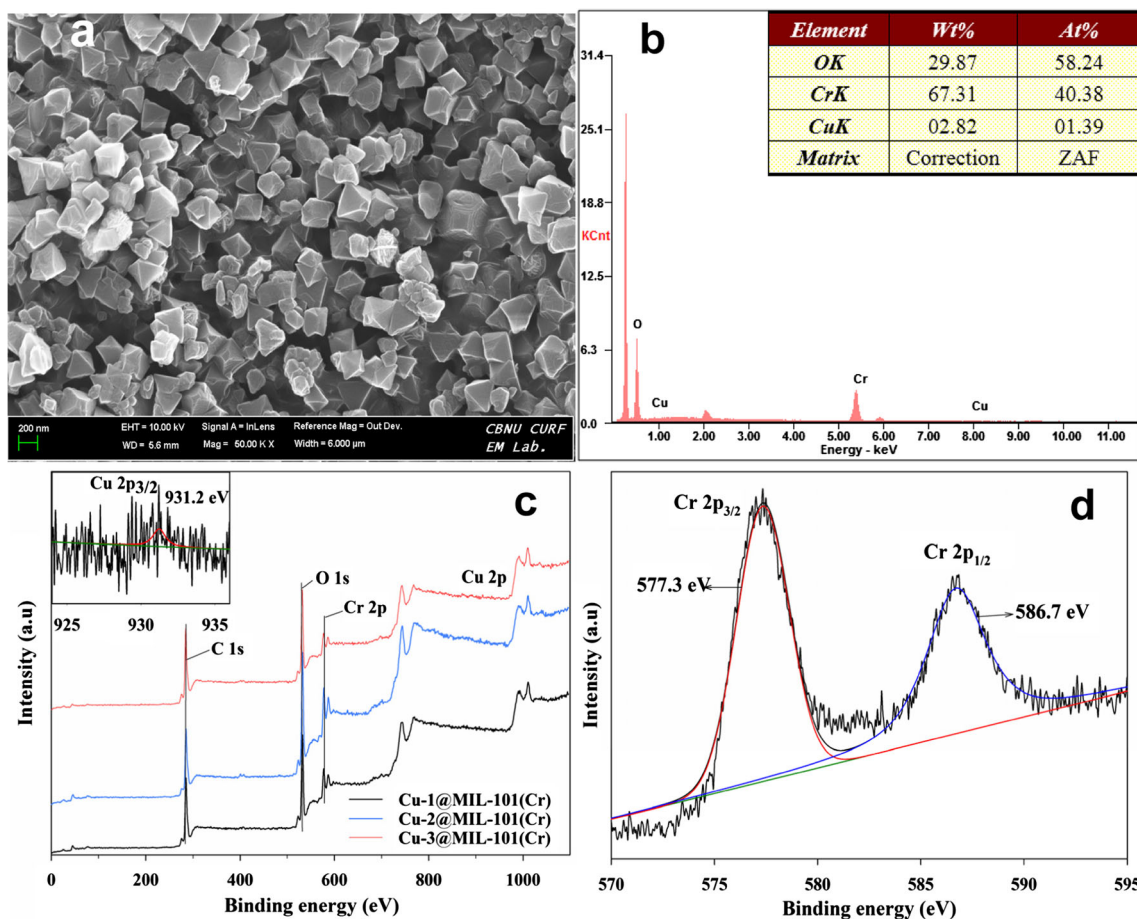
Materials	S <sub>BET</sub> (m <sup>2</sup> /g)	Pore volume (cm <sup>3</sup> /g)	Reference
MIL-101(Cr)	3367	2.35 (at p/p <sub>o</sub> = 0.99)	Present work
Cu-3@MIL-101(Cr)	2518	1.55 (at p/p <sub>o</sub> = 0.99)	Present work
MIL-101(Cr)	4100	2.00	(Férey et al. 2005)
MIL-101(Cr)	2887	1.45	(Prasanth et al. 2011)
MIL-101(Cr)	2800	1.37	(Llewellyn et al. 2008)
MIL-101(Cr)	2014	1.18	(Santiago-Portillo et al. 2015)
MIL-101(Cr)	3060	1.45	(Wickenheisser et al. 2015)

affect the crystallinity of MIL-101(Cr), namely the crystallinity would be decreased with the increased copper concentration (Shen et al. 2015).

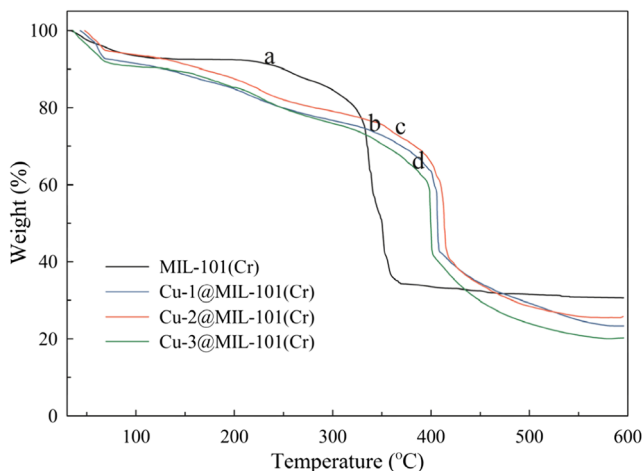
**Specific surface areas and pore sizes**

The nitrogen adsorption and desorption isotherms of MIL-101(Cr) and Cu-3@MIL-101(Cr) (Fig. 2a) both displayed a typical type I profile with secondary uptakes, which demonstrated that two kinds of microporous windows existed in the

samples (Férey et al. 2005; Rouquerol et al. 2013). Type I adsorption isotherm usually indicates that the adsorption occurs on the surface of materials or monolayer adsorption happens caused by a strong interaction between the adsorbent and the adsorbate (Kruk and Jaroniec 2001). Moreover, the pore size distributions (Fig. 2b) exhibited that the surface pore diameters were mainly allocated between 1.43 and 2.42 nm; thus, micropores and mesoporous were the major pores in the materials. The structural parameters of the materials prepared in this work and other works are listed in Table 1.



**Fig. 3** a SEM image of Cu-3@MIL-101. b EDX analysis of Cu-3@MIL-101. c XPS analysis of Cu@MIL-101 (inset shows the binding energies of Cu). d XPS Cr 2p binding energies

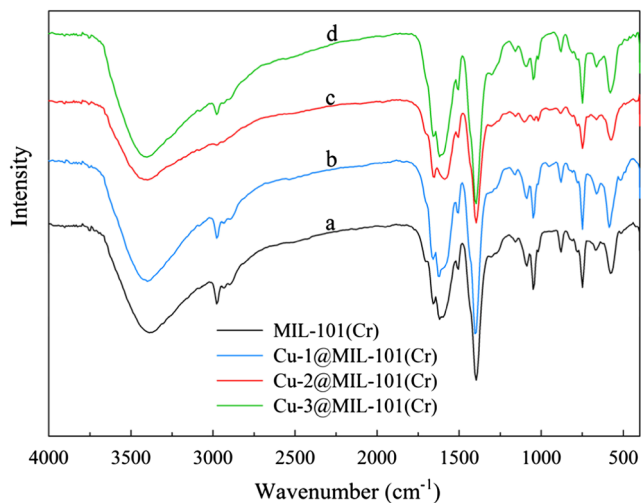


**Fig. 4** TG curve of various adsorbents (a MIL-101(Cr); b Cu-1@MIL-101(Cr); c Cu-2@MIL-101(Cr); d Cu-3@MIL-101(Cr))

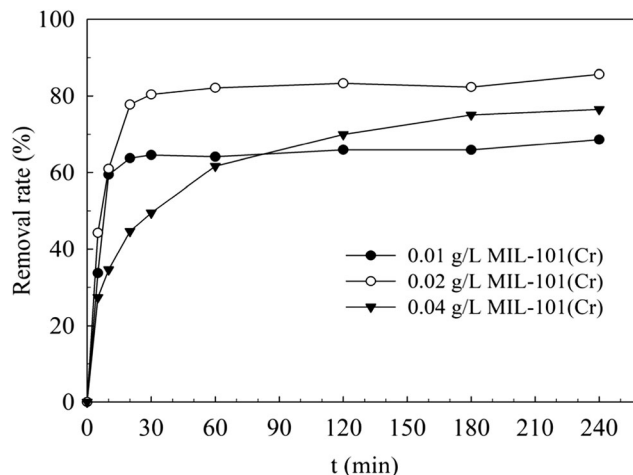
The data in Table 1 revealed that the MIL-101(Cr) samples synthesized in this work had a large BET-specific surface area ( $3367 \text{ m}^2/\text{g}$ ) and a high total pore volume ( $2.35 \text{ cm}^3/\text{g}$ ). But after copper doping, the parameters decreased to  $2518$  and  $1.55 \text{ cm}^3/\text{g}$ , respectively. The reason for this phenomenon may be that copper ions occupied the interspace of the pores when the doping occurred.

### Surface morphology and composition

SEM and EDS images of Cu-3@MIL-101(Cr) are shown in Fig. 3a, b (morphological images of MIL-101(Cr) prepared by original and improved method are shown in Fig. S2), respectively. It could be seen that the Cu-3@MIL-101(Cr) particles were well dispersed, and obvious octahedron structures were clearly displayed as reported previously, with the dimensions



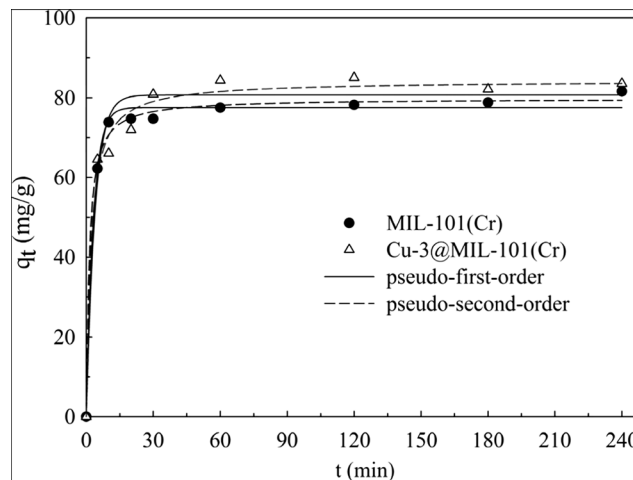
**Fig. 5** FTIR spectra of materials (a MIL-101(Cr); b Cu-1@MIL-101(Cr); c Cu-2@MIL-101(Cr); d Cu-3@MIL-101(Cr))



**Fig. 6** Effect of sorbent dosage on the removal of benzene using MIL-101(Cr) (initial concentration:  $600 \text{ mg}/\text{m}^3$ , room temperature)

of the crystals ranging from  $0.2$  to  $0.4 \mu\text{m}$  (Zhao et al. 2011a). Besides, the EDS analysis revealed the existence of Cu, which could indicate that the copper was doped into the MIL-101(Cr).

XPS analysis was used to verify the surface element composition of the modified materials (Fig. 3c, d). Figure 3c shows the wide scan XPS spectra of Cu@MIL-101(Cr), and inset of Fig. 3c, d shows the Cu 2p and Cr 2p core-level spectra of Cu-3@MIL-101(Cr), respectively. In the wide spectra, C 1s, O 1s, Cr 2p, and Cu 2p peaks were detected at  $284.6$ ,  $531.8$ ,  $577.3$ , and  $931.2 \text{ eV}$ , respectively. Furthermore, due to the binding energy of Cr  $2p_{3/2}$  at  $577.3 \text{ eV}$  (Fig. 3d) and Cu  $2p_{3/2}$  at  $931.2 \text{ eV}$  (inset of Fig. 3c), Cr and Cu in Cu-3@MIL-101(Cr) were identified with  $3+$  and  $1+$  states, respectively. The peak intensity of Cu 2p also demonstrated that copper was grafted on the surface of MIL-101(Cr).



**Fig. 7** Adsorption kinetic curves of benzene on MIL-101(Cr) and Cu-3@MIL-101(Cr) (adsorbent dosage:  $0.1 \text{ g}$ , initial concentration:  $600 \text{ mg}/\text{m}^3$ , room temperature)

**Table 2** Kinetic parameters of benzene adsorbed by MIL-101(Cr) and Cu-3@MIL-101(Cr), the parentheses are standard deviations

Adsorbent	Pseudo first-order model			Pseudo second-order model		
	$q_m$ (mg/g)	$k_1$ (min <sup>-1</sup> )	$R^2$	$q_m$ (mg/g)	$k_2$ (g/(mg·min))	$R^2$
MIL-101(Cr)	77.56(0.88)	0.32(0.03)	0.994	79.83(0.84)	0.0097(0.0014)	0.996
Cu-3@MIL-101(Cr)	80.70(2.28)	0.26(0.05)	0.962	84.26(1.65)	0.0061(0.0012)	0.987

### Thermostability study

As seen from the TG curves, MIL-101(Cr) (Fig. 4a) and Cu@MIL-101(Cr) (Fig. 4b–d) had different thermostability. For MIL-101(Cr), three obvious steps of weight loss were observed. At first, the weight was reduced slightly and slowly in the range of 30.0–214.5 °C, which was caused by the loss of guest water molecules in the large cages. The second step ranged from 214.5 to 324.3 °C and could be due to the loss of guest water molecules from the medium-sized cages. In the third step (above 324.3 °C), the weight was rapidly decreased by nearly 50%, which was attributed to the reduction of OH/F groups caused by the decomposition of the frameworks (Hong et al. 2009). For Cu@MIL-101(Cr), there were also three but different weight loss steps. The weight of materials in the first step (30.0–244.6 °C) reduced about 20%, which would correspond to the loss of weakly bound guest water molecules, gas, and residual solvent from the pores and the Cr trimers (Carson et al. 2013). Compared to MIL-101(Cr), the more weight loss meant the more unsaturated metal sites released on Cu@MIL-101(Cr). So that the adsorption capacity for VOC molecules would be raised because more binding site can be used (Llewellyn et al. 2008). The second and third weight loss steps were situated within the range of 244.6–394.2 °C and above 394.2 °C, respectively.

### FTIR spectra

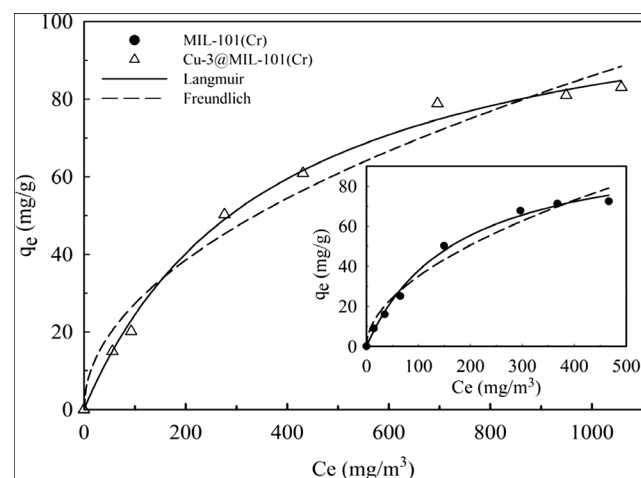
Infrared spectroscopy was applied to explore the functional groups of MIL-101(Cr) and Cu@MIL-101(Cr). It was obviously that the FTIR spectra of the materials obtained in this work (Fig. 5) were similar as that of the MIL-101(Cr) reported in the previous researches (Awadallah-F et al. 2011; Wickenheisser et al. 2015), which confirmed that copper doping did not change the functional groups of MIL-101(Cr). The broad band from 3700 to 3000 cm<sup>-1</sup> was associated with the O–H stretching vibrations (Zhang et al. 2011). The peak at 2978 cm<sup>-1</sup> was due to the stretching vibrations of the aliphatic-CH<sub>2</sub>. The strong bands at 1612 and 1396 cm<sup>-1</sup> could be assigned to the vibrational stretching frequencies of O–C–O groups, confirming the presence of dicarboxylate linker in the framework (Jhung et al. 2007; Maksimchuk et al. 2008). And

valence vibration bands at 1049 and 748 cm<sup>-1</sup> revealed the presence of benzene rings (Gu and Yan 2010). The bands at 578 cm<sup>-1</sup> were most likely to ascribe to in-plane and out-of-plane bending modes of COO<sup>-</sup> groups (Maksimchuk et al. 2008).

### Adsorption studies

#### Effect of dosage

Removal efficiencies of benzene on MIL-101(Cr) at different adsorbent dose are shown in Fig. 6 (reuse of MIL-101(Cr) on benzene absorption is shown in Fig. S3). It could be seen that with the increasing dosage, the removal rate of benzene increased at first and then decreased. At the dosage of 0.01 and 0.02 g/L, the reactions could reach equilibrium within 15 min, with the removal rate of 68 and 85%, respectively. However, when the dosage increased to 0.04 g/L, the reaction balance time was more than 120 min, as well as the removal rate decreased to 76%. That was because the materials overlapped together which hindered the contact between sorbent and adsorbate. According to this result, the dosage of sorbent in further experiments was 0.02 g/L.



**Fig. 8** Adsorption isotherms of benzene on MIL-101(Cr) and Cu-3@MIL-101(Cr) (adsorbent dosage: 0.02 g/L, initial concentration: 0 to 2000 mg/m<sup>3</sup>, room temperature)

**Table 3** Langmuir and Freundlich isotherm parameters of benzene adsorbed by MIL-101(Cr) and Cu-3@MIL-101(Cr)

Adsorbent	Line type	Langmuir model			Freundlich model		
		$q_m$ (mg/g)	$K_L$ (L/mg)	$R^2$	$K_F$ (L/g)	$n$	$R^2$
MIL-101(Cr)	Non-linear	103.4	0.0058	0.994	3.07	1.89	0.974
	Linear	101.79	0.006	0.992	1.81	1.60	0.983
Cu-3@MIL-101(Cr)	Non-linear	114.4	0.0027	0.996	2.74	2.00	0.974
	Linear	115.4	0.003	0.991	1.39	1.65	0.972

### Adsorption kinetics

The effects of reaction time on the adsorption process of benzene by MIL-101(Cr) and Cu@MIL-101(Cr) are shown in Fig. S4. It demonstrated that the adsorption of benzene on MIL-101(Cr) reached equilibrium within 10 min, which was faster than that on Cu-3@MIL-101(Cr). That was because the pore volume in MIL-101(Cr) (2.35 cm<sup>3</sup>/g) was larger than that in Cu-3@MIL-101(Cr) (1.55 cm<sup>3</sup>/g), and it was easier for benzene molecules to be adsorbed on the pores of MIL-101(Cr). Combined with the analysis of pore size, there were both micropores and mesopores in MIL-101(Cr). However, with the copper doped, the mesopores with diameter range of 2–5 nm almost disappeared and the amount of micropores also decreased in Cu-3@MIL-101(Cr), leading to the relatively slow adsorption rate. Furthermore, the adsorption kinetics (Fig. 7) were investigated by Lagergren pseudo-first-order and pseudo-second-order models. The models were expressed as follows:

$$q_t = q_e (1 - e^{-k_1 t}) \quad (4)$$

$$q_t = \frac{k_2 q_e^2 t}{1 + k_2 q_e t} \quad (5)$$

where  $q_t$  (mg/g) and  $q_e$  (mg/g) are the adsorption capacity at time  $t$  (min) and equilibrium, respectively;  $k_1$  (min<sup>-1</sup>) and  $k_2$  (g/mg·min) are the kinetic rate constants for the pseudo-first-order and the pseudo-second-order models, respectively. The correlation coefficients (Table 2) for pseudo-second-order model were higher than that for pseudo-first-order model, which meant that chemical process played a crucial role in the adsorption (Lin et al. 2011). Meanwhile, it indicated that the electron transfer, exchange, or sharing were generated and chemical bonds were formed in the adsorption process (Ge et al. 2012).

### Adsorption isotherms

The adsorption isotherms were studied at different initial concentrations that ranged from 0 to 2000 mg/m<sup>3</sup>. As is well known, the maximum adsorption capacity is an important parameter for sorbents, while Langmuir and Freundlich models are commonly used to calculate it (Freundlich 1906; Langmuir 1918). The non-linear and linear equations of isotherm models were expressed as follows:

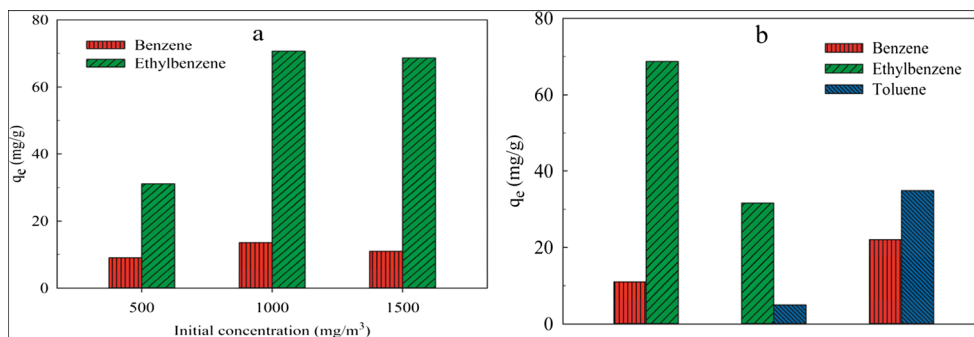
$$\text{Langmuir equation : } q_e = \frac{q_m K_L c_e}{1 + K_L c_e} \quad (\text{non-linear}) \quad (6)$$

**Table 4** Comparison of VOCs adsorption property on various adsorbents

Adsorbates	Adsorbents	Temperature (°C)	Adsorption capacity	Reference
Benzene	Cu-3@MIL-101(Cr)	25	114.4 mg/g	Present work
Benzene	IRMOF-3	25	56 mg/g	(Britt et al. 2008)
Benzene	IRMOF-62	25	109 mg/g	(Britt et al. 2008)
Benzene	MOF-5	25	2 mg/g	(Britt et al. 2008)
Benzene	MOF-74	25	96 mg/g	(Britt et al. 2008)
Benzene	MOF-199	25	176 mg/g	(Britt et al. 2008)
Benzene	HZSM-5 Zeolite	30	1.9 mmol/g	(Jhung et al. 2007)
Benzene	SBA-15	30	3.0 mmol/g	(Jhung et al. 2007)
Toluene	MIL-101(Cr)	25	0.53 mmol/g	(Huang et al. 2011)
Toluene	Y-Zeolite	20	1.625 mmol/g	(Kim et al. 2007)
Ethylbenzene	MOF-5	150	99 mg/g	(Gu et al. 2009)
Ethylbenzene	MIL-47	130	35 wt.%	(Finsy et al. 2008)



**Fig. 9** Competitive adsorptions of VOCs on Cu-3@MIL-101(Cr) (a bi-VOCs system, b tri-VOCs system)



$$\frac{c_e}{q_e} = \frac{1}{q_m K_L} + \frac{c_e}{q_m} \quad (\text{linear}) \quad (7)$$

Freundlich equation :  $q_e = K_F c_e^{1/n}$  (non-linear) (8)

$$\log q_e = \frac{1}{n} \log c_e + \log K_F \quad (\text{linear}) \quad (9)$$

where  $q_e$  (mg/g) is the adsorption capacity at equilibrium,  $c_e$  (mg/m<sup>3</sup>) is the benzene concentration at equilibrium,  $q_m$  (mg/g) and  $K_L$  are the Langmuir constants, representing the maximum adsorption capacity for the solid phase loading and the energy constant related to the heat of adsorption, respectively. The  $K_F$  and  $1/n$  are Freundlich constants related to adsorption capacity and intensity of adsorption, respectively. The non-linear adsorption isotherm curves are demonstrated in Fig. 8 (linear fitting curves are displayed in Fig. S5) and the constants are presented in Table 3.

As seen in Table 3, both the non-linear and linear coefficients of determination ( $R^2$ ) for Langmuir model were more than 0.99 and higher than those for Freundlich model, which suggested that the adsorption of benzene on MIL-101(Cr) and Cu-3@MIL-101(Cr) could be described well by Langmuir model and it was principally monolayer adsorption (Langmuir 1918). In addition, the maximum adsorption capacity of benzene on MIL-101(Cr) and Cu-3@MIL-101(Cr), calculated by non-linear Langmuir model, was 103.4 and 114.4 mg/g, respectively. As mentioned before, copper doping would cause the decrease of specific surface area and pore volume on MIL-101(Cr), resulting in a decrease in adsorption capacity. But at the same time, it also introduced unsaturated metal sites, which would improve the adsorption performance of the materials (Chowdhury et al. 2009). As a consequence, influenced by the two factors, Cu-3@MIL-101(Cr) had a better adsorption property. The adsorption capacities of Cu-3@MIL-101(Cr) in the present work and other adsorbents reported previously are listed in Table 4. Cu-3@MIL-101(Cr) showed a good adsorption capacity for benzene as compared with other adsorbents, suggesting that Cu-3@MIL-101(Cr) was a promising adsorbent in the removal of VOCs.

### Competitive adsorption

Competitive adsorption was studied through bi-VOCs and tri-VOCs systems. For bi-VOCs system, adsorptions between benzene and ethylbenzene on Cu-3@MIL-101(Cr) at different concentrations (500, 1000, and 1500 mg/m<sup>3</sup>) are exhibited in Fig. 9a. It was obviously that the adsorption capacities of ethylbenzene were much higher than that of benzene and increased with the rising concentration. However, when the concentration was over 1000 mg/m<sup>3</sup>, the adsorption capacity remained almost constant. That was because the content of VOCs exceeded the maximum adsorption capacity of adsorbents. Tri-VOCs system for competitive adsorptions among benzene, toluene, and ethylbenzene at the concentration of 1500 mg/m<sup>3</sup> is shown in Fig. 9b. The results illuminated that the priority of adsorption followed this order: ethylbenzene > toluene > benzene, and mutual interference among benzene, toluene, and ethylbenzene, which caused the low adsorption capacity, might exist. It might be ascribed to the functional groups and pore diameters on the surface of materials and the polarity of VOCs (Yaghi et al. 1995). What is more, compared with the only hexatomic ring of benzene, the branched chain in both toluene and ethylbenzene could more easily enter the small pore and combine with MIL-101(Cr) which was of energetic heterogeneity (Huang et al. 2011). Moreover, the longer chain of ethyl, which can get into the pore more deeply, might combine with sorbent more firmly than the short chain of methyl.

### Conclusion

In this work, typical metal-organic framework materials of MIL-101(Cr) and Cu@MIL-101(Cr) had been successfully synthesized by improved hydrothermal method. The characterizations showed that the MIL-101(Cr) and Cu@MIL-101(Cr) were octahedral crystal with large specific surface area. Moreover, copper doping did not change its skeleton structure, but there would be some effects on the crystallinity and thermal stability. The VOCs adsorption capacities were investigated by kinetic and isotherm experiments, while Cu-

3@MIL-101(Cr) showed the best performance in absorbing benzene among the four materials with the maximum adsorption capacity of 114.4 mg/g. The Cu@MIL-101(Cr) had better performance in uptake of benzene than the metal-free MIL-101(Cr), probably because it provided more adsorption sites. The competitive adsorption systems of bi-VOCs and tri-VOCs revealed that mutual interference among benzene, toluene, and ethylbenzene might exist in the adsorption process. Furthermore, Cu-3@MIL-101(Cr) preferentially adsorbed ethylbenzene, followed by toluene and finally benzene. In a word, copper doping is an effective modification method to improve the adsorptive property of MIL-101(Cr), and the materials can have good applications in the adsorption, removal, and storage of VOCs and other gases.

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