

# Effects of salinity on simultaneous reduction of perchlorate and nitrate in a methane-based membrane biofilm reactor

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**Abstract** This study builds upon prior work showing that methane (CH<sub>4</sub>) could be utilized as the sole electron donor and carbon source in a membrane biofilm reactor (MBfR) for complete perchlorate (ClO<sub>4</sub><sup>-</sup>) and nitrate (NO<sub>3</sub><sup>-</sup>) removal. Here, we further investigated the effects of salinity on the simultaneous removal of the two contaminants in the reactor. By testing ClO<sub>4</sub><sup>-</sup> and NO<sub>3</sub><sup>-</sup> at different salinities, we found that the reactor performance was very sensitive to salinity. While 0.2 % salinity did not significantly affect the hydrogen-based MBfR for ClO<sub>4</sub><sup>-</sup> and NO<sub>3</sub><sup>-</sup> removals, 1 % salinity completely inhibited ClO<sub>4</sub><sup>-</sup> reduction and significantly lowered NO<sub>3</sub><sup>-</sup> reduction in the CH<sub>4</sub>-based MBfR. In salinity-free conditions, NO<sub>3</sub><sup>-</sup> and ClO<sub>4</sub><sup>-</sup> removal fluxes were 0.171 g N/m<sup>2</sup>-day and 0.091 g/m<sup>2</sup>-day, respectively, but NO<sub>3</sub><sup>-</sup> removal fluxes dropped to 0.0085 g N/m<sup>2</sup>-day and ClO<sub>4</sub><sup>-</sup> reduction was completely inhibited when the medium changed to 1 % salinity. Scanning electron microscopy (SEM) showed that the salinity dramatically changed the microbial morphology, which led to the development of wire-like cell structures. Quantitative real-time PCR (qPCR) indicated that the total number of

microorganisms and abundances of functional genes significantly declined in the presence of NaCl. The relative abundances of *Methylomonas* (methanogens) decreased from 31.3 to 5.9 % and *Denitratisoma* (denitrifiers) decreased from 10.6 to 4.4 % when 1 % salinity was introduced.

**Keywords** Methane-based membrane biofilm reactor · Nitrate · Perchlorate · Reduction · Salinity

## Introduction

Perchlorate (ClO<sub>4</sub><sup>-</sup>) is widely used in rocket fuel, fireworks, and explosives due to its high energetic value as a strong oxidant and its chemical stability (USEPA 2005). Its release into water resources causes contamination. Perchlorate can interfere with the synthesis and secretion of thyroid hormone, which affects human metabolism and hinders human growth and development (USEPA 2008). Though the US Environmental Protection Agency (USEPA) has not yet established a nationwide maximum contaminant level (MCL) for ClO<sub>4</sub><sup>-</sup>, some states have set up cleanup target levels from 2 to 18 µg/L in drinking water (Gu and Coates 2006). Nitrate (NO<sub>3</sub><sup>-</sup>) is a co-contaminant with ClO<sub>4</sub><sup>-</sup> in groundwater (USEPA 2001). Nitrate has been regulated by the USEPA at 10 mg N/L in drinking water (USEPA 2009).

Commonly used technologies for removing ClO<sub>4</sub><sup>-</sup> and NO<sub>3</sub><sup>-</sup> from water include membrane filtration, ion exchange, chemical reduction, and biological reduction (Coates and Achenbach 2004; Matos et al. 2008; Zhao et al. 2014). Membrane filtration and resin regeneration in ion exchange produce highly saline ClO<sub>4</sub><sup>-</sup> and NO<sub>3</sub><sup>-</sup> brines that need to be further treated or disposed of. Biological reduction can be used to directly treat ClO<sub>4</sub><sup>-</sup> and NO<sub>3</sub><sup>-</sup>-contaminated water or brines produced during membrane filtration or ion exchange. Compared to chemical reduction, biological reduction consumes less energy and requires less chemical addition because enzymes in microbes are used as the

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catalysts (Ye et al. 2012). During biological reduction, the perchlorate reductase (*pcrABCD*) reduces  $\text{ClO}_4^-$  to chlorite ( $\text{ClO}_2^-$ ) (Kengen et al. 1999), and chlorite dismutase (*clid*) catalyzes the disproportionation of chlorite ( $\text{ClO}_2^-$ ) to chloride ( $\text{Cl}^-$ ) and oxygen ( $\text{O}_2$ ) (Van Ginkel et al. 1996), which is subsequently reduced to  $\text{H}_2\text{O}$ . During the  $\text{NO}_3^-$  reduction, reductions of nitrate to nitrite (*narGHJI*), nitrite to nitric oxide (*nirSJFD/GH/L*),  $\text{NO}$  to  $\text{N}_2\text{O}$  (*norZ*), and  $\text{N}_2\text{O}$  to  $\text{N}_2$  (*nosZDFY*) are performed by various reductases (Ettwig et al. 2010).

Perchlorate-reducing bacteria (PRB) and denitrifiers can use a variety of electron donors to gain energy (Miller and Logan 2000; Sahu et al. 2009; Son et al. 2006; Yu et al. 2006). When the electron donor is a gas, such as hydrogen and methane, membrane biofilm reactors (MBfRs) are one of the most widely used reactors because they have close to 100 % gas utilization efficiency and high  $\text{NO}_3^-$  and  $\text{ClO}_4^-$  removal rates (Zhao et al. 2013; Tang et al. 2012a, b; Luo et al. 2015; Chen et al. 2016).

Compared with  $\text{CH}_4$ -based MBfRs,  $\text{H}_2$ -based MBfRs have been extensively studied and used at the field scale for  $\text{NO}_3^-$  and  $\text{ClO}_4^-$  removal. The effects of salinity on nitrate and perchlorate reduction in  $\text{H}_2$ -based MBfRs are well understood.  $\text{H}_2$ -based MBfRs reach simultaneous reduction of nitrate and perchlorate, but the reduction rate decreases as the salt concentration increases. Chung et al. (2007) reported that nitrate and perchlorate reduction was not affected by 2 % salinity (20 g/L NaCl) in a  $\text{H}_2$ -based MBfR, while 4 % salinity (40 g/L NaCl) decreased reduction by 40 %. Van Ginkel et al. (2008) investigated the kinetics of  $\text{ClO}_4^-$  and  $\text{NO}_3^-$  reduction in a  $\text{H}_2$ -based MBfR fed with brines. They found that the  $\text{NO}_3^-$  removal fluxes and  $\text{H}_2$  pressure were roughly first order but roughly zero order with  $\text{NO}_3^-$  concentration in  $\text{H}_2$ -based MBfR.  $\text{NO}_3^-$  and  $\text{ClO}_4^-$  were reduced simultaneously in a  $\text{CH}_4$ -based MBfR (Luo et al. 2015), but the effects of salinity on  $\text{NO}_3^-$  and  $\text{ClO}_4^-$  reduction in  $\text{CH}_4$ -based MBfRs are unknown.

$\text{CH}_4$ -based MBfRs have been much less studied compared to their  $\text{H}_2$ -based counterparts. Previous research has demonstrated the potential of using  $\text{CH}_4$ -based MBfRs to simultaneously remove  $\text{NO}_3^-$  and  $\text{ClO}_4^-$  from water (Luo et al. 2015; Chen et al. 2016); however, these studies were all conducted using synthetic fresh waters. Therefore, it is of interest to investigate how salinity affects biological perchlorate and nitrate reduction in a  $\text{CH}_4$ -based MBfR. The overall objective of this work is to investigate the effects of salinity on the simultaneous reduction of  $\text{NO}_3^-$  and  $\text{ClO}_4^-$  in a  $\text{CH}_4$ -based MBfR.

## Materials and methods

### MBfR setup

A two-column MBfR system similar to Zhao et al. (2011) was used in this study. The MBfR had composite hollow fibers (hydrophobic microporous polyethylene fiber, 280- $\mu\text{m}$  o.d.,

180- $\mu\text{m}$  i.d., and 0.1–0.15- $\mu\text{m}$  pore size) manufactured by Mitsubishi Rayon (Model MHF-200TL, Mitsubishi, Ltd., Japan). One column contained 32 fibers, and the other contained 20 fibers as “coupon fibers” for sampling purposes. Each fiber ran all the way through the column, with one end glued into a  $\text{CH}_4$  supply manifold and the other end sealed to avoid gas leakage. The total volume of the MBfR was 65 mL, and the total membrane surface area was 90.24  $\text{cm}^2$ . The MBfR was completely mixed via recirculation with a peristaltic pump (Longer Pump, Model 1515X, Longer Precision Pump Co, Ltd., China) at 100 mL/min.

### Inoculum source and culture medium

We inoculated the MBfR with a 10-mL culture from a  $\text{CH}_4$ -based MBfR (Luo et al. 2015). The medium contained the following mineral salts (analytical grade or purer) per liter of deionized water: 1 mg  $\text{CaCl}_2$ , 0.3 g  $\text{NaHCO}_3$ , 5 mg  $\text{MgSO}_4 \cdot 7\text{H}_2\text{O}$ , 0.2 g  $\text{KH}_2\text{PO}_4$ , 0.4 g  $\text{NaH}_2\text{PO}_4 \cdot 12\text{H}_2\text{O}$ , 1-mL acid trace element solution (100 mM HCL, 2.085 g  $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$ , 68 mg  $\text{ZnSO}_4 \cdot 7\text{H}_2\text{O}$ , 14 mg  $\text{H}_3\text{BO}_3$ , 120 mg  $\text{CoCl}_2 \cdot 6\text{H}_2\text{O}$ , 500 mg  $\text{MnCl}_2 \cdot 4\text{H}_2\text{O}$ , 320 mg  $\text{CuSO}_4$ , 95 mg  $\text{NiCl}_2 \cdot 6\text{H}_2\text{O}$  per liter), and 1-mL alkaline trace element solution (10 mM NaOH, 67 mg  $\text{SeO}_2$ , 50 mg  $\text{Na}_2\text{WO}_4 \cdot 2\text{H}_2\text{O}$ , 242 mg  $\text{Na}_2\text{MoO}_4 \cdot 2\text{H}_2\text{O}$  per liter). The medium was degassed with  $\text{N}_2$  for 15 min to maintain anaerobic conditions. The medium pH was adjusted to  $7.5 \pm 0.2$  with hydrochloric acid. The influent feeding rate was 0.5 mL/min (hydraulic retention time (HRT) of 130 min), the  $\text{CH}_4$  pressure was 10 psig (0.69 bar), and the temperature was  $29 \pm 1$  °C for all experiments.

### Start up and continuous operation of the MBfR

After inoculation, the MBfR was fed with  $\text{NO}_3^-$  and  $\text{ClO}_4^-$  at  $\sim 15$  and  $\sim 10$  mg/L, respectively, and maintained for more than 20 days to allow sufficient biomass to accumulate. After the startup stage, we fed the reactor with 2 mg/L of perchlorate from stage 1 to stage 5. To investigate the effects of salinity on  $\text{ClO}_4^-$  and/or  $\text{NO}_3^-$  reduction, we set up salinity at 1 % (10 g/L of NaCl) in stage 2 and 0.2 % (2 g/L of NaCl) in stages 5 and 6. To further investigate if nitrate inhibition plays a role in the inhibition mechanisms, we varied the nitrate concentrations in different stages: 10 mg  $\text{NO}_3^-$ /L in stages 1, 2, and 3 and 5 mg  $\text{NO}_3^-$ /L in stage 6. We allowed each stage to reach steady state, which was defined as when effluent concentrations were stable (<10 % variation) at least three times the HRT.

### Analyses

Liquid samples were taken from the MBfR with 5-mL syringes and filtered immediately through 0.2- $\mu\text{m}$  membrane filters

(LC + PVDF membrane, Shanghai Xinya, China).  $\text{NO}_3^-$  and  $\text{NO}_2^-$  were assayed using ion chromatography (Metrohm 833 Basic IC plus, Switzerland) with an A-Supply-5 column and an eluent containing 3.2 mM  $\text{NaHCO}_3$ , 1.0 mM  $\text{Na}_2\text{CO}_3$ , and 5 % acetone at a flow rate of 1 mL/min.  $\text{ClO}_4^-$  was measured using ion chromatography (DIONEX ICS-1000, USA) with an AS 16 column and AG 16 precolumn, an eluent concentration of 35 mM KOH, and a 1.0 mL/min flow rate. The pH values of the influent and effluent were measured using a pH meter (Seven Easy, Mettler Toledo, Switzerland) and were between 7.5 and 7.7 for all stages. The bacterial morphology on the surface of membrane at the end of each stage was analyzed using scanning electron microscopy (SEM).

### Biofilm sampling and DNA extraction

When the reactor reached a steady state, biofilm was collected.  $\text{N}_2$  gas was sparged at the sampling point to preclude  $\text{O}_2$  exposure. We cut off one 5-cm-long section from a coupon fiber and then sealed the remaining fiber by tying the end into a knot. The DNA was extracted using a DNeasy Blood & Tissue Kit (Qiagen, USA) as previously described by Zhao et al. (2011).

### Quantification of bacterial 16S rRNA and functional genes

Plasmids containing target fragments were used as positive controls and to produce calibration curves (Zhao et al. 2011). The primers and qPCR conditions were the same as previously described: *pcrA* for  $\text{ClO}_4^-$  reductase (Nozawa-Inoue et al. 2008), *nirS* for  $\text{NO}_2^-$  reductase (Throbaeck et al. 2004), *mcrA* for the formation of methane by most of methanogens and reverse methanogenesis (Steinberg and Regan 2008), *pMMO* for  $\text{CH}_4$  monooxygenase (Paszczynski et al. 2011), and *16S* ribosomal RNA (*rRNA*) gene for bacteria (Maeda et al. 2003). We used the SYBR Premix Ex Taq Kit (Takara Bio Inc., Japan) and performed qPCR as previously described by Zhao et al. (2011). The copy numbers of each gene were calculated by comparison to standard curves. Negative controls included water instead of template DNA in the PCR reaction mix. We performed triplicate PCR reactions for all samples and negative controls. The functional genes (*pcrA*, *nirS*, *pMMO*, *mcrA*) and *16S rRNA* gene abundances in different stages are shown in Fig. 3.

## Results and discussion

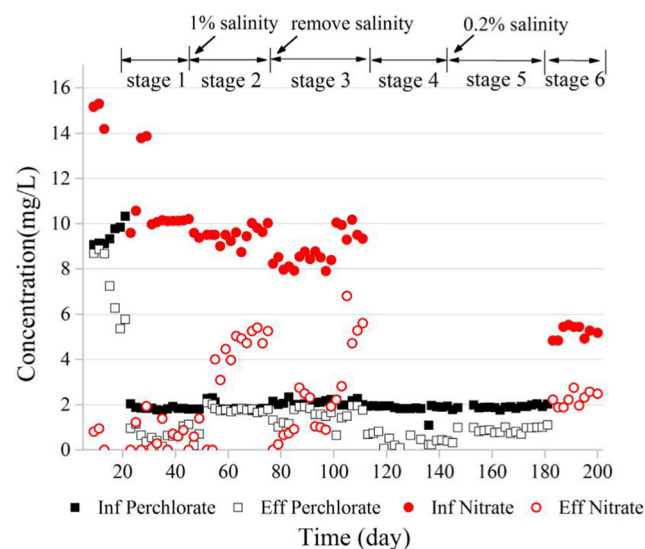
### Perchlorate and nitrate reduction

$\text{CH}_4$  pressure was set at 10 psig throughout the experiment, which made  $\text{CH}_4$  available in all stages (Table S1). The influent

and effluent concentrations of  $\text{ClO}_4^-$  and  $\text{NO}_3^-$  for the MBfR are plotted in Fig. 1. The reactor was operated for 23 days in batch mode before stage 1 to accumulate sufficient biomass to reduce up to 5 mg/L of perchlorate and 15 mg/L of nitrate.

The  $\text{NO}_3^-$  and  $\text{ClO}_4^-$  surface loadings in stage 1 were 0.171 g N/m<sup>2</sup>-day and 0.091 g/m<sup>2</sup>-day, respectively. Without salinity, the nitrate was fully removed and 57.2 % of the  $\text{ClO}_4^-$  was reduced after the reactor reached steady state. When 1 % salinity was applied in stage 2, the  $\text{NO}_3^-$  removal percentage dropped to ~50 %, and  $\text{ClO}_4^-$  reduction was completely inhibited. Obviously, the perchlorate and nitrate reductions were both severely affected by the salinity in the  $\text{CH}_4$ -based MBfR. Van Ginkel et al. (2008) reported that in a  $\text{H}_2$ -based MBfR,  $\text{NO}_3^-$  removal was not affected at NaCl concentrations less than 20 g/L (i.e., 2 %). Chung et al. (2007) demonstrated that both nitrate and perchlorate were reduced in the presence of NaCl ranging from 10 to 40 g/L (i.e., 1–4 %) in a  $\text{H}_2$ -based MBfR. By comparison, microorganisms using methane as the electron donor are thus more sensitive to salinity than the microorganisms using  $\text{H}_2$ .

To investigate if the biofilm could be recovered after salinity shock, we removed salinity in stage 3 so that the operating conditions in stage 3 were the same as in stage 1. To our surprise, the perchlorate and nitrate removal reached only 28.3 and 64.4 %, respectively. This removal is slightly higher than that observed in stage 2 but much lower than that in stage 1. The biofilm was possibly irreversibly damaged by the high salinity. Park et al. (2001) reported that the activity of denitrifying bacteria decreased after adding salt to the system. Gingras and Batista (2002) reported that the  $\text{ClO}_4^-$  reduction rate declined to 10 % when 1–1.5 % salt concentrations were present in culture.



**Fig. 1** The  $\text{NO}_3^-$  and  $\text{ClO}_4^-$  concentrations in the influent and effluent of the MBfR. Stage 2 and stage 5 were operated with 1 and 0.2 % salinity, respectively. Salinity was defined as the quantity of dissolved salt content of the water

To investigate if  $\text{NO}_3^-$  contributed to the inhibition of  $\text{ClO}_4^-$  reduction, we removed  $\text{NO}_3^-$  from the influent in stage 4. Without feeding  $\text{NO}_3^-$ , the  $\text{ClO}_4^-$  bioreduction improved to around 70 %. Therefore, it is possible that, in stage 2, the dual inhibitions of nitrate and salinity caused the absence of  $\text{ClO}_4^-$  reduction. In a model, Tang et al. (2012a, b) explained that in a  $\text{H}_2$ -MBfR simultaneously reducing  $\text{NO}_3^-$  and  $\text{ClO}_4^-$ , a high load of  $\text{NO}_3^-$  ( $>0.6 \text{ g N/m}^2\text{-day}$ ) strongly inhibits  $\text{ClO}_4^-$  reduction.

To test the perchlorate or nitrate reduction under lower salinity, we reduced the salinity to 0.2 % NaCl in stages 5 and 6.  $\text{ClO}_4^-$  was the only electron acceptor in stage 5, and  $\text{NO}_3^-$  was the only electron acceptor in stage 6. The  $\text{ClO}_4^-$  and  $\text{NO}_3^-$  removals were 53.3 and 59.2 %, respectively. This performance is much worse than that in stage 1, which can be explained by the 0.2 % salinity inhibition and the irreversible inhibition in stage 2. The inhibition mechanisms will be further explored in “Microbial morphology” section.

### Microbial morphology

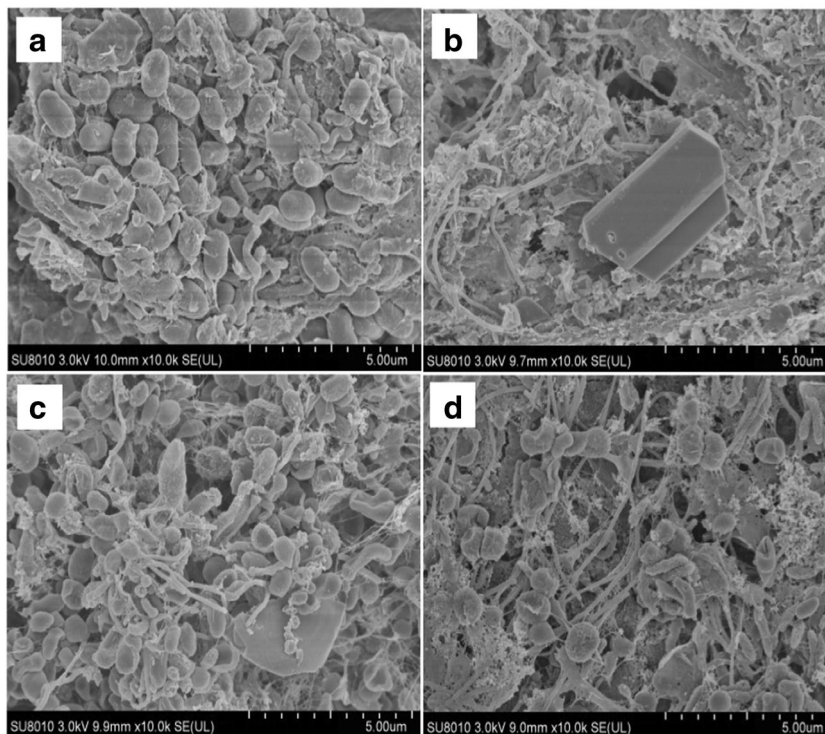
To investigate the bacterial morphological change, we analyzed biomass samples from each stage at steady state using SEM. Figure 2 compares the microbial morphologies at stages 1 (Fig. 2a), 2 (Fig. 2b), 3 (Fig. 2c), and 6 (Fig. 2d). Stage 2 had the highest salinity (1 %). Correspondingly, it has the most wire-like structures and the cell surfaces had the most wrinkles (Fig. 2b). These bacterial filaments may be a way for the microorganisms to accommodate the change in osmotic

pressure and protect the cells from salt shock. The damaging effect of salinity on bacteria leads to cell content emission and the formation of extracellular polymeric substances (EPS)/soluble microbial products (SMP) (Di Bella et al. 2013; Jang et al. 2013; Reid et al. 2006). Some studies argue that the accumulation of cell contents and intermediate products and bacterial autolysis are the responses to salt toxicity (Sharghi et al. 2014; Pendashteh et al. 2011; Sun et al. 2010). However, stage 6 had a medium salinity (0.2 %) and the biofilm also had some wire-like structures. Similarly, Jin et al. (2007) observed that under higher osmotic stress, the structure of a nitrifying bacterial community was disrupted and microbial diversity decreased. Therefore, salinity inhibition likely played a role in the decrease of nitrate removal in stage 6.

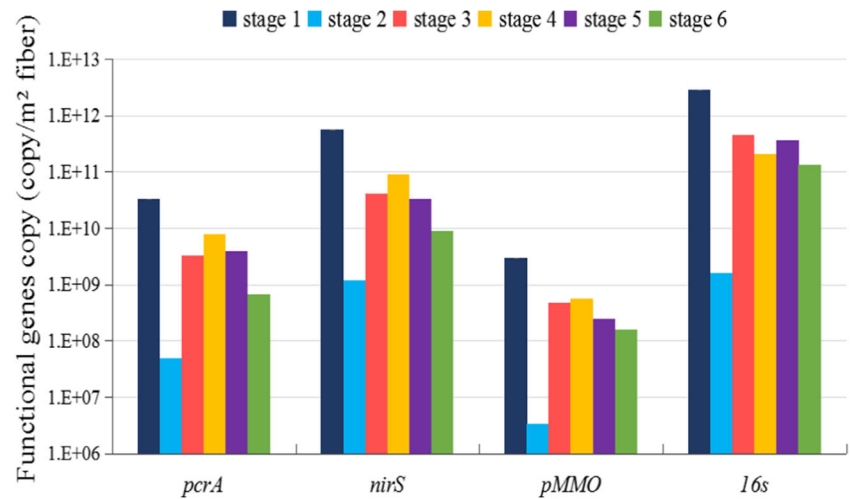
### Functional community structure

Figure 3 shows the functional and *16S rRNA* gene copy numbers of the microbial community at all stages. The bacterial community was very dense in stage 1, illustrated by the highest copy numbers of the *16S rRNA* gene ( $2.84 \times 10^{12}$  copies/ $\text{m}^2$  fiber). The functional respiration genes such as *pcrA* and *nirS* and methane oxidation gene *pMMO* reached the highest in stage 1, indicating a very good correlation between methane oxidation and nitrate/perchlorate reduction. When 1 % salinity was added in stage 2, the abundances of all tested genes dropped by three orders of magnitude and reached their lowest points, which was consistent with the

**Fig. 2** The SEM images of biomass samples from different stages. **a** Stage 1 at 10,000 magnification (10 mg/L  $\text{NO}_3^-$ , 2 mg/L  $\text{ClO}_4^-$ ). **b** Stage 2 at 10,000 magnification (10 mg/L  $\text{NO}_3^-$ , 2 mg/L  $\text{ClO}_4^-$ , and 10 g/L NaCl). **c** Stage 3 at 10,000 magnification (10 mg/L  $\text{NO}_3^-$ , 2 mg/L  $\text{ClO}_4^-$ ). **d** Stage 6 at 10,000 magnification (5 mg/L  $\text{NO}_3^-$ , 2 g/L NaCl)



**Fig. 3** The functional genes (*pcrA*, *nirS*, *pMMO*, *mcrA*) and *16S rRNA* gene abundances in different stages. Abundance refers to gene copy numbers per square centimeter fiber



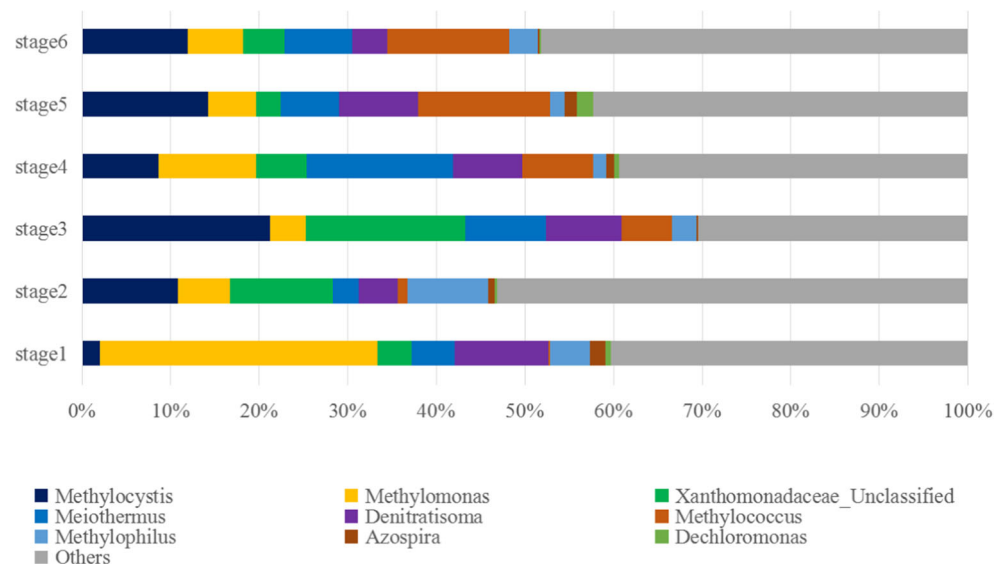
drop in nitrate and perchlorate bioreduction. All the functional genes increased in stages 3 and 4, concurrent with the removal of NaCl, and decreased in stages 5 and 6 when 0.2 % salinity was added to the influent. Throughout the whole experiment, the functional gene abundance correlated very well with the salinity.

### Microbial community structure

We analyzed the diversity and structure of the MBfR microbial communities using pyrosequencing of the 16S rRNA gene from the MBfR biofilm samples. Figure 4 shows the relative abundance of dominant microbial phylotypes at the genus level, while Fig. S1 shows the class level. *Methylomonas* was the dominant (31.3 %) bacterium in stage 1. Its abundance sharply decreased to 5.9 % in stage 2 when 1 % salinity was introduced and remained at low levels in the

latter stages. *Methylomonas* are known methanotrophs and sensitive to salinity. For example, Sherry et al. (2016) reported the disappearance of *Methylomonas* when NaCl was higher than 1 g/L. Cunliffel et al. (2008) analyzed samples from surface (lower salinity) and subsurface (higher salinity) water of the Blyth estuary and found that *Methylomonas* was present in the surface samples but not in subsurface samples. In our MBfR, *Methylococcus* emerged in stage 2 (1.1 %), and its abundance continued to increase in the rest of stages. *Methylococcus* grows on CH<sub>4</sub> under low O<sub>2</sub> concentrations (Ward et al. 2004). Some studies show that *Methylococcus* is highly abundant in coastal saline soil (Mishra et al. 2012; Yousuf et al. 2012). Another methanotroph, *Methylocystis*, was present at a low abundance (2.1 %) in stage 1 but increased to ~10 % in stage 2 at 1 % salinity and further increased to 21.3 % in stage 3 when the salinity was removed. Its abundance decreased to ~10 % in stage 4 when nitrate was

**Fig. 4** Clustering based on relative abundance analysis of the microbial community structure at the genus level





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