

Proposed pathways for the reduction of a reactive azo dye in an anaerobic fixed bed reactor

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Abstract Some process has been proposed for azo dye degradation and anaerobic bioreactors are one of them, since for their reduction, the dye has to be the electron acceptor. An anaerobic fixed bed bioreactor packed with activated carbon (AC) is proposed to degrade the Reactive Red 272 azo dye. In the present paper a dye degradation mechanism in an anaerobic environment is explained. It is very important to consider the interaction dye-microorganism-AC, because the groups in the AC surface take part in the reaction besides being an excellent carrier for microorganism and an adsorbent for the dye. The aromatic compounds produced in the dye reduction are partially degraded as a function of inlet dye concentration and reactor residence time. In anaerobic environment the aromatic compounds are decomposed through hydroxylation, carboxylation and redox reactions, due to enzymatic reactions.

Keywords Azo dye · Anaerobic reactor · Degradation mechanism · Organic compound

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Introduction

The textile industry uses large volumes of water in its process; therefore, large quantities of wastewater are generated, containing a high load of pollutants, especially dyes. The kinds of dyes that are most extensively used are azo dyes; the main characteristic of these dyes is a double bond between two nitrogen atoms. A dye molecule can contain more than one azo group and that are bonded to aromatic groups.

Azo dye degradation is carried out in two steps: (1) the breaking or reduction of the azo bond and (2) the partial or complete mineralization of the aromatic or aliphatic amines generated (reduction products). It is very important to analyze the compounds in the reactor effluent and the reduction mechanism of the dye because the intermediary products of many azo dyes as benzidine, 2-naphthylamine and other aromatic amines can be toxic, carcinogenic or hazardous in some way.

In biological treatment process, the microorganisms degrade initially the more simple soluble substrates and afterwards the complex organic compounds. In general this process is carried out by enzymes and redox reactions, and can take place inside or outside the cell. Hydrolysis is the first step to degrade complex molecules; this consists in the addition of water molecules to the complex compounds by bacteria, with the aim of breaking the chemical bonds and to reduce to more simple compounds. This is catalyzed by extracellular enzymes (Gerardi 2006).

Azo dyes are complex molecules and can contain different aromatic groups. The aromatic groups are very stable due to resonance and to the π conjugated bond characteristic.

In anaerobic environment, the ring opening of the aromatic structures is carried out by hydroxylation and carboxylation reactions (Griebler et al. 2004) by the addition of $-OH$ and $-COOH$ or CO_2 to the molecule (Fig. 1)

from the dextrose anaerobic degradation products as fumarate and succinate (Meckenstock et al. 2004); then a series of redox reactions are carried out to degrade the complex molecule to carboxylic acids or other lower weight compounds as acetate, carbon dioxide and methane.

This kind of degradation reactions is carried out by radical enzymes; these are enzymes that contain radicals or catalyze reactions with radicals as intermediates (Buckel and Golding 2006). The enzyme contribute to the degradation transporting reducing equivalents (e^-) and specific groups ($-OH$, $-COOH$, fumarate, succinate), so the degradation redox reactions can occur and the compounds formed in the fading of the water can be obtained.

Some of the main kinds of bacteria that take part in these reactions are: the nitro-reducers that convert the *p*-cresol to hydroxybenzyl alcohol and hydroxybenzoate, and the sulfate-reducers that attack the methyl groups oxidizing it by the addition of fumarate (Schink 2006), as in Fig. 1.

The objective of this paper is to present some proposed pathways for the degradation reaction of the azo dye Reactive Red 272 (Fig. 2) in an upflow anaerobic fixed bed bioreactor, with the aim of understand and identify the reduction mechanism and the degradation of intermediates of these kind of complex compounds.

Materials and methods

Upflow anaerobic fixed bed reactor

The upflow reactor was made from Pyrex glass and it contains a fixed bed of AC (activated carbon) of 42% of working volume, 1.24 l y 541.17 g of AC. The reactor is outlined in Fig. 3 and their characteristics are shown in Table 1. At the beginning of the operation there was an adsorption stage to saturate the AC with the dye and do not

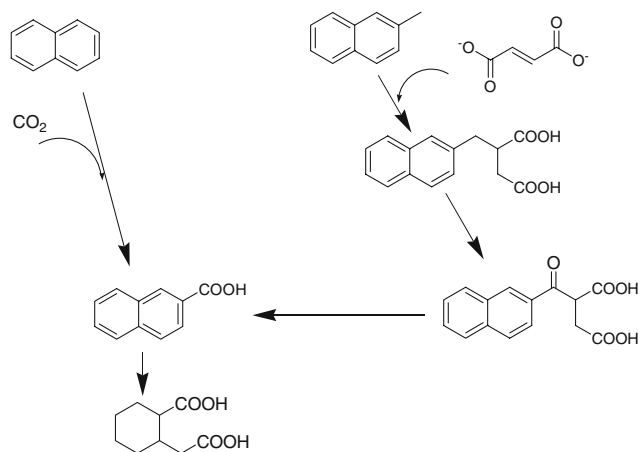


Fig. 1 Anaerobic degradation mechanism of naphthalene and substituted naphthalene (Meckenstock et al. 2004)

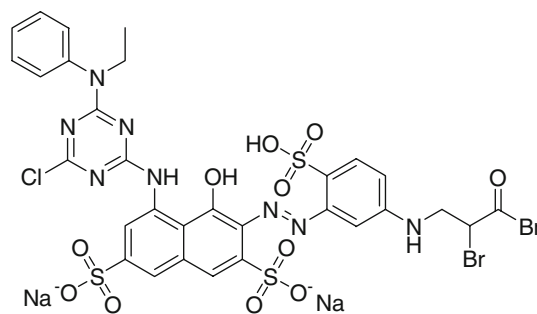


Fig. 2 Molecular structure of reactive Red 272 dye

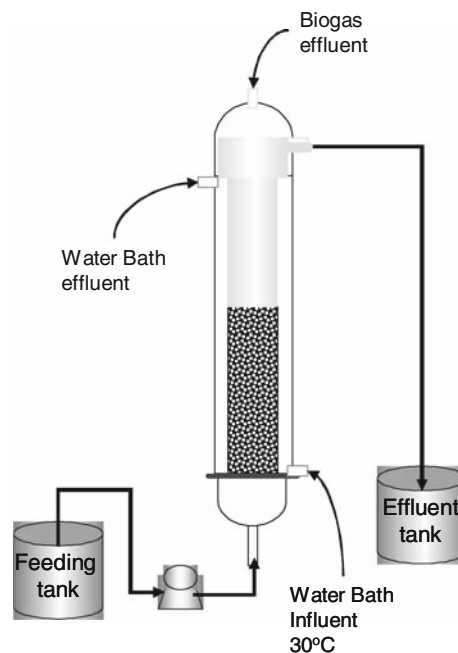


Fig. 3 Bioreactor system used for this investigation

allocate the fading of the solution to just possible adsorption on to AC, after that, the reactor was inoculated with an adapted anaerobic sludge (microorganism consortium) by recirculation of water with 10% of adapted sludge for

Table 1 Reactor characteristics for azo dye reactive red 272 degradation

Work volume, l	3
Inside diameter, cm	6
Inside diameter of the settle, cm	9.5
Total longitude, cm	105.5
Initial porosity of the bed	0.53
Steady state porosity	0.19
Fixed bed volume, l	1.24
Superficial velocity (average), cm/min	0.52
Volumetric flow (average), ml/min	18
TR _m (average), min	206.25

Table 2 Reactor efficiency, continuous operation (average results)

No.	Q ml/min	C ₀ dye	C ₀ dextrose	C ₀ yeast	OL kg/m ³ d	% R COD	% R dye
1	18	250	500	500	12.77	52.28	97.15
2	32	250	500	1,000	23.91	29.97	97.79
3	18	500	500	1,000	18.19	53.29	98.61
4	32	500	500	500	19.12	36.11	98.64
5	18	250	1,000	1,000	30.26	55.89	91.35
6	32	250	1,000	500	44.30	37.65	91.52
7	18	500	1,000	500	23.53	54.99	97.68
8	32	500	1,000	1,000	35.86	16.25	96.59

Q, volumetric flux; %R, removal rate; OL, organic load; C₀, Inlet concentration in mg/l

15 days, 11.586 mg SS/g CA were adsorbed at the beginning, forming a biofilm in the AC surface. Dextrose and yeast extract are the carbon and nitrogen source to the microorganism.

Identification of degradation products

The compounds in the reactor effluent were identified under different process conditions at the reactor effluent: increasing the inlet dye concentration in the reactor influent from 250 to 500 mg/l, and under different half residence time (RT_m) keeping constant the inlet dye concentration in 250 mg/l. Effluent samples were taken and extracted with ethyl acetate in agitated flask for 24 h, afterward, the extract was rota-vaporated and analyzed in a gas chromatographer coupled with a mass spectrometer (GC-MS, Perkin Elmer Clarus 500). The operation conditions of temperature-time for the analysis in the GC-MS were: 40° for 8 min and afterwards a 5 min slope until reaching 250° and keeping it for 30 min.

Analytical techniques

Absorbance was measured to 506 nm in the samples to follow the change in dye concentration using a spectrophotometer UV/VIS Perkin Elmer, Lambda25, and COD (Chemical Oxygen Demand) was measured by closed reflux method (APHA-AWWA-WPCF 1989).

Results and discussion

The results obtained by the continuous operation of the reactor showed that the proposed reactor works efficiently to remove the reactive azo dye with high removal percentages of almost 99%. COD removal rates were from 16.3 to 55.9%; these values indicate the degradation grade because when the dye molecule is reduced, occur the fading of the water, but the reduction products of the dye are complex organics that can be harder to degrade than the dye, as aromatic amines and substituted naphthalene. Table 2 shows some results of the

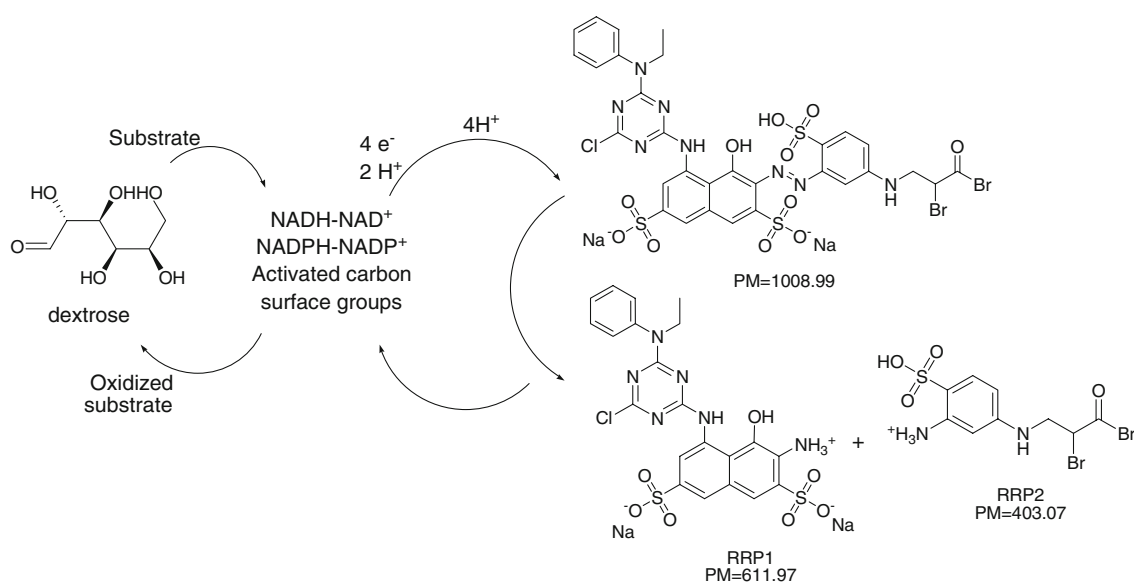

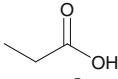
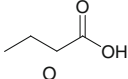

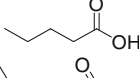
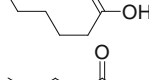
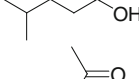
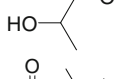
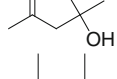
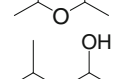
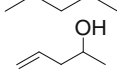
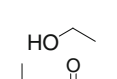
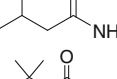
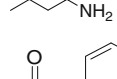
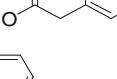
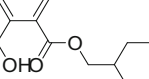



Fig. 4 Reduction of the azo-dye molecule. First pathway in the azo-dye degradation

Table 3 Identified compounds in the reactor effluent at good COD removal efficiency

Name	Molecular structure
Ammonium	NH_4^+
Carbon dioxide	$O=C=O$
Acetic acid	
Propionic acid	
Butyric acid	
Isobutyric acid	
Pentanoic acid	
Hexanoic acid	
4-methylpentanoic acid	
3-hydroxy-butan-2-one	
4-hydroxy-4-methylpenten-2-one	
2-isopropoxypropane	
4-methyl-penten-2-ol	
4-penten-2-ol	
Ethanol	
3-methylbutanamide	
3,3-dimethylbutanamide	
Benzene acetic acid	
1,2-Benzenedicarboxylic acid, mono(2-ethylhexyl)ester	

degradation tests in the reactor and the parameters used in each one.

The activated carbon (AC) used as a carrier provides a suitable surface for microorganism growth and enhance the biodegradation because the dye is adsorbed to their surface and then reduced through a reaction carried out by the interaction of microorganism, extracellular enzymes and the groups in the AC surface. The dye is transported from

the bulk to the bioparticle (biomass and activated carbon) surface and the dye reduction take place in the biofilm and in the AC surface. This effect and the data of adsorption of the dye to the AC were explained in a previous paper (Gonzalez-Gutierrez and Escamilla-Silva 2007).

In the first step of the degradation mechanism of the dye, it is carried out a reduction of the molecule by the breaking of the azo bond due to the transfer of electrons (reducing

equivalents), by means of a redox mediator that can be the quinolic groups in the activated carbon surface and extracellular enzymes or coenzymes (Fig. 4); when the dye is reduced in this first step, it loses color. Dextrose added to the water is a source of carbon for microorganism and electron donor for dye reduction in the reactor.

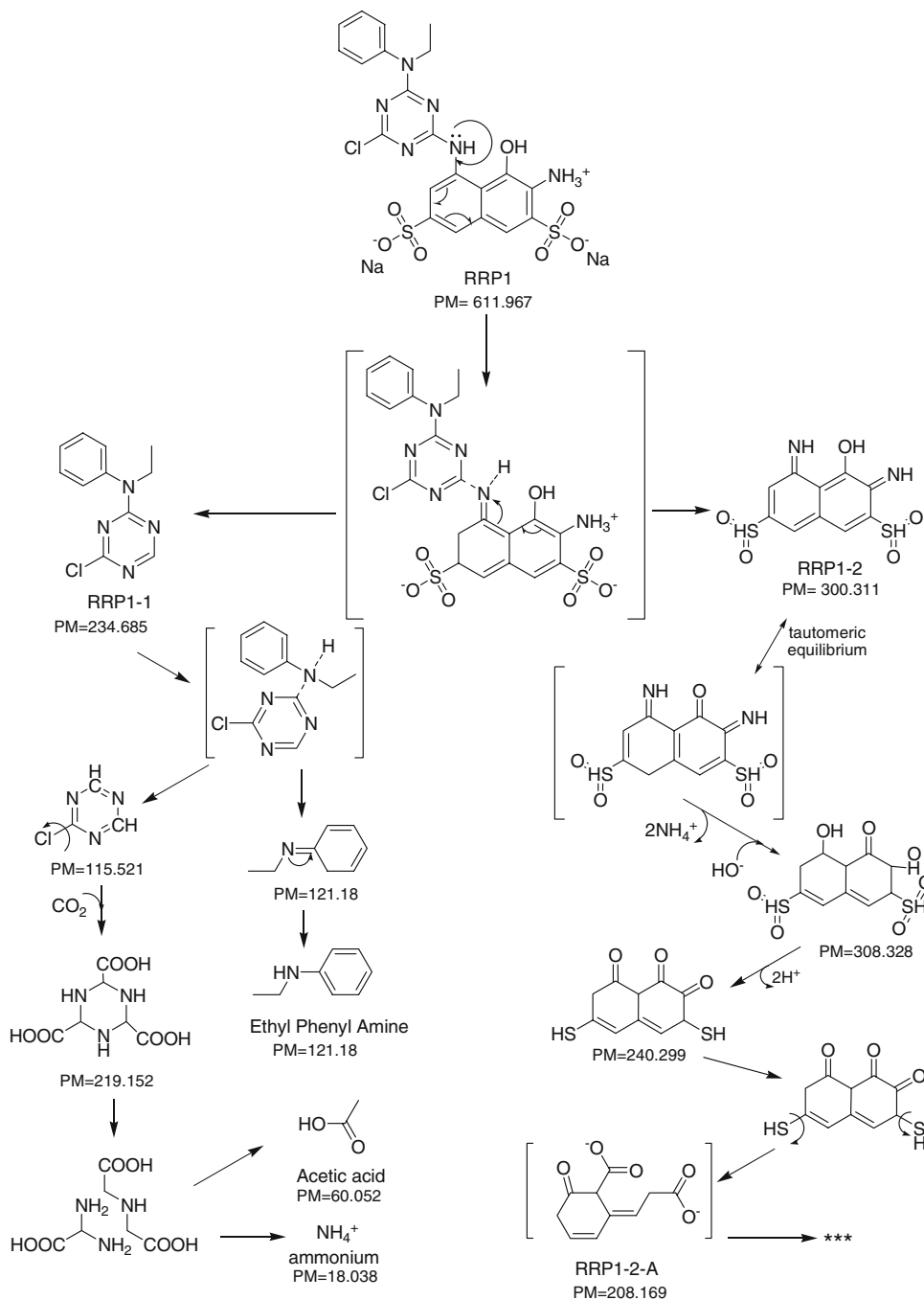
The compounds identified by GC-MS in the reactor effluent, change with the reactor operation conditions. Under the best operation conditions with a good COD removal rate (around 50%) it was achieved good degradation efficiency, the identified compounds corresponded mainly to carboxylic acids, esters and alcohols, and in smallest amount to aromatic acids. The more frequently identified compounds in the effluent in this case are shown in Table 3.

As the organic load increases because a raise in dye concentration or a reduction in the half residence time of the reactor, the COD removal efficiency was reduced, and as a result the amount of aromatic compounds identified in the effluent was raised. In this case the identified compounds correspond to substituted aromatic acids, benzene-substituted rings and naphthalene-hydrated rings, as a result that were not enough conditions to take the degradation to a mayor extent, these are shown in Table 4. While dye concentration at the inlet continues increasing, the same compounds are found in the reactor effluent, although the abundance of some of them goes increasing as naphthalene, benzene acetic acid, xylene, ethyl benzene.

Table 4 Aromatic compounds identified in the reactor effluent at low COD removal efficiency

Name	Molecular structure
2-phenylethanol	
<i>p</i> -cresol	
2-benzylmalonic acid	
(R)-2-acetamido-3-phenylpropanoic acid	
1,2,3,4-tetrahydro naphthalene	
Naphthalene	
1-isobutyl-4-methylbenzene	
1-ethylbenzene	
<i>p</i> -xylene	
<i>m</i> -xylene	
1-ethyl-3-methyl benzene	
1-(4-ethylphenyl)ethanone	
Benzenepropanoic acid	
1-ethyl-2,4-dimethyl benzene	
1,2,3,4-tetramethyl benzene	
Ethyl 2-phenylacetate	

Fig. 5 Mechanism proposes of the route of degradation for the RRP1 molecule

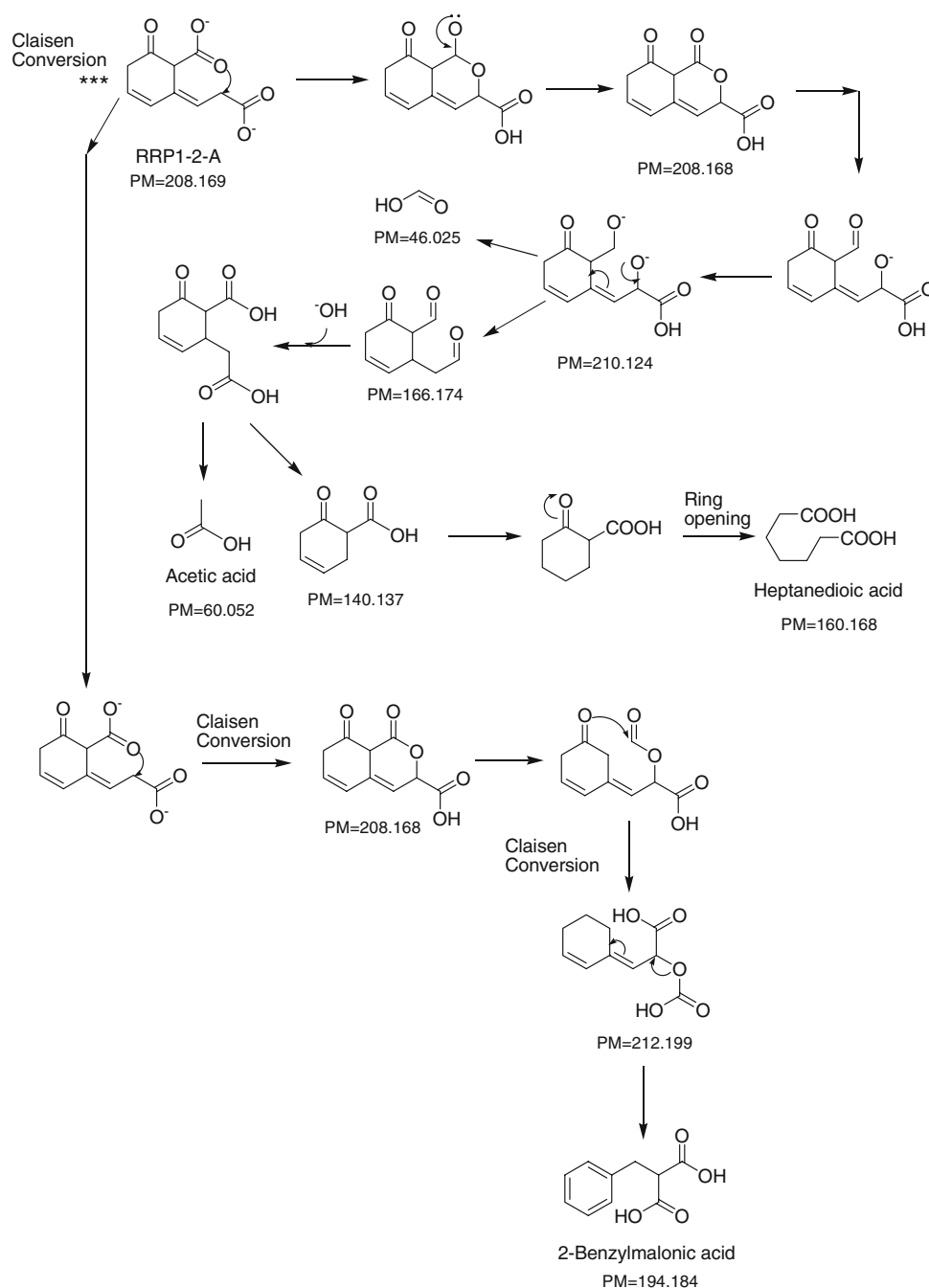


Despite the amount of aromatic compounds found in the reactor effluent, no aromatic amines were identified. Some authors state that aromatic amines are the most difficult compounds to degrade in azo dyes reduction (Field 2002; dos Santos et al. 2003; Supaka et al. 2004; HeFang et al. 2004; Plum and Rehorek 2005; Sponza and Isik 2005; van der Zee and Villaverde 2005; Khehra et al. 2006; Kumar et al. 2006); this indicate that the proposed process is efficient even at high dye concentration (400–500 mg/l). Anaerobic degradation of nitro aromatic compounds or aromatic amines has been

demonstrated by other authors (Donlon et al. 1996; Kudlich et al. 1999; Chen 2002; Chen et al. 2006). Therefore, in the best operation conditions of the bioreactor with a COD removal of 50%, it is possible to degradation most of the aromatic compounds produced in the reduction of the reactive azo dye.

As was stated before, in anaerobic environment the aromatic compounds degradation is carried out by hydroxylation and carboxylation reactions, adding to the aromatic molecule $-OH$, CO_2 , $-COO$ as well as fumarate ($C_4H_2O_4^{2-}$) and succinate ($C_4H_4O_4^{2-}$) groups, with the

Fig. 6 Mechanism proposes of the route of degradation for the RRP1 2-A compound



aim that the necessary redox reactions can be achieved. According to this and to the achieved results in the identification of the products at the bioreactor effluent, some degradation pathways are proposed for the partial mineralization of the Reactive Red 272 Azo dye. Nevertheless, the produced compounds in the dye reduction reactions can be degraded in different pathways by enzymes, metabolism and co-metabolism of the cells.

From the reduction of the dye showed in Fig. 4, two products are formed: RRP1 and RRP2. The degradation pathway proposed for the product RRP1 is showed in

Fig. 5. The product RRP1 is divided in two main fractions: Chlorotriazine-Ethyl Phenyl Amine (EPhA), and the naphthalene-substituted group. The Chlorotriazine separates from the EPhA and is enzymatically carboxylated, and afterwards the ring opens and ammonium and acetic acid are produced.

In the Naphthalene-substituted molecule, the amino groups are substituted by $-OH$, through a nucleophilic substitution mechanism, and later loose the protons to give place to ketone groups. Subsequently, sulphone groups are reduced to sulphide through reductases and one of the rings

opens, at this moment the sulphide groups are released as a consequence of the resonance and the compound marked as RRP1-2-A is produced (Fig. 5).

The degradation pathway for the RRP1-2-A is described in Fig. 6. The proposed pathway for this compound occurs through Claisen conversions and are produced CO_2 and Acetic, Formic and Heptanedioic acid, which are low molecular weight compounds and can be metabolized by the microorganisms; 2-benzylmalonic acid is produced also in this stage in a parallel pathway and the route for its decomposition is shown in Fig. 7.

Claisen conversion is a mechanism that happens to the aryl-phenyl-ethers chemically by heating; this consist in the movement of six electrons and a transient high energy compound is formed which is quickly tautomerized to produce the final compound. The Claisen mechanism is used usually to refer to changes in aryl-phenyl-ethers arrays, including the tautomerism stages in the production of phenolic compounds (Miller 1998).

The proposed degradation pathway of 2-benzylmalonic acid results in the production of benzenedicarboxylic acid-mono (2-ethyl-hexyl) ester (BAME) through the addition

of fumarate and transpositions; this compound was found almost in every sample at the reactor effluent. In addition, in this stage are produced: Benzyl acetic acid, Benzoic acid, Phenol and Pthalic acid, and after the ring opening, the Octanedioic acid which can be easily metabolized and split in other low molecular weight organic acids. At this stage of the degradation reactions of the dye, are produced the compounds identified more frequently in the reactor effluent as the BAME, Benzylacetic acid and Phenol, and through the degradation of the Octanedioic acid can be formed the Hexanoic and acetic acids or the Pentanoic and Propionic acids which were the organic acids found regularly in the water samples.

In Fig. 8 are shown the degradation pathways for the RRP2 product; at this point, are outlined four possible fractions in which the molecule could be broken. Two probable fractions are aromatic sulphone-amines; in their molecule, the amino groups are displaced by $-\text{OH}$ groups through nucleophilic substitution mechanism, then, the sulphone groups are convert to sulphide and afterwards are released. Phenol and Resorcinol are produced afterwards the last reductions and substitutions, which generate

Fig. 7 Mechanism proposes of the route of degradation for the 2-Benzylmalonic acid

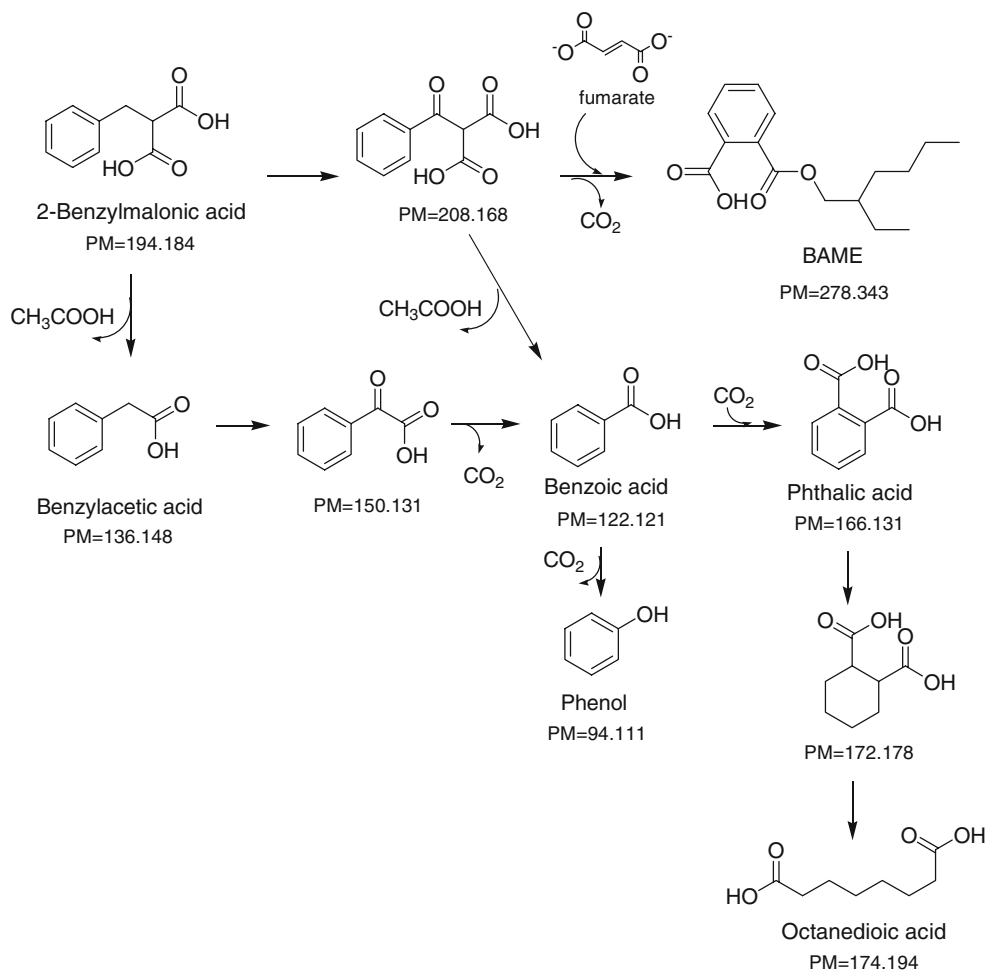
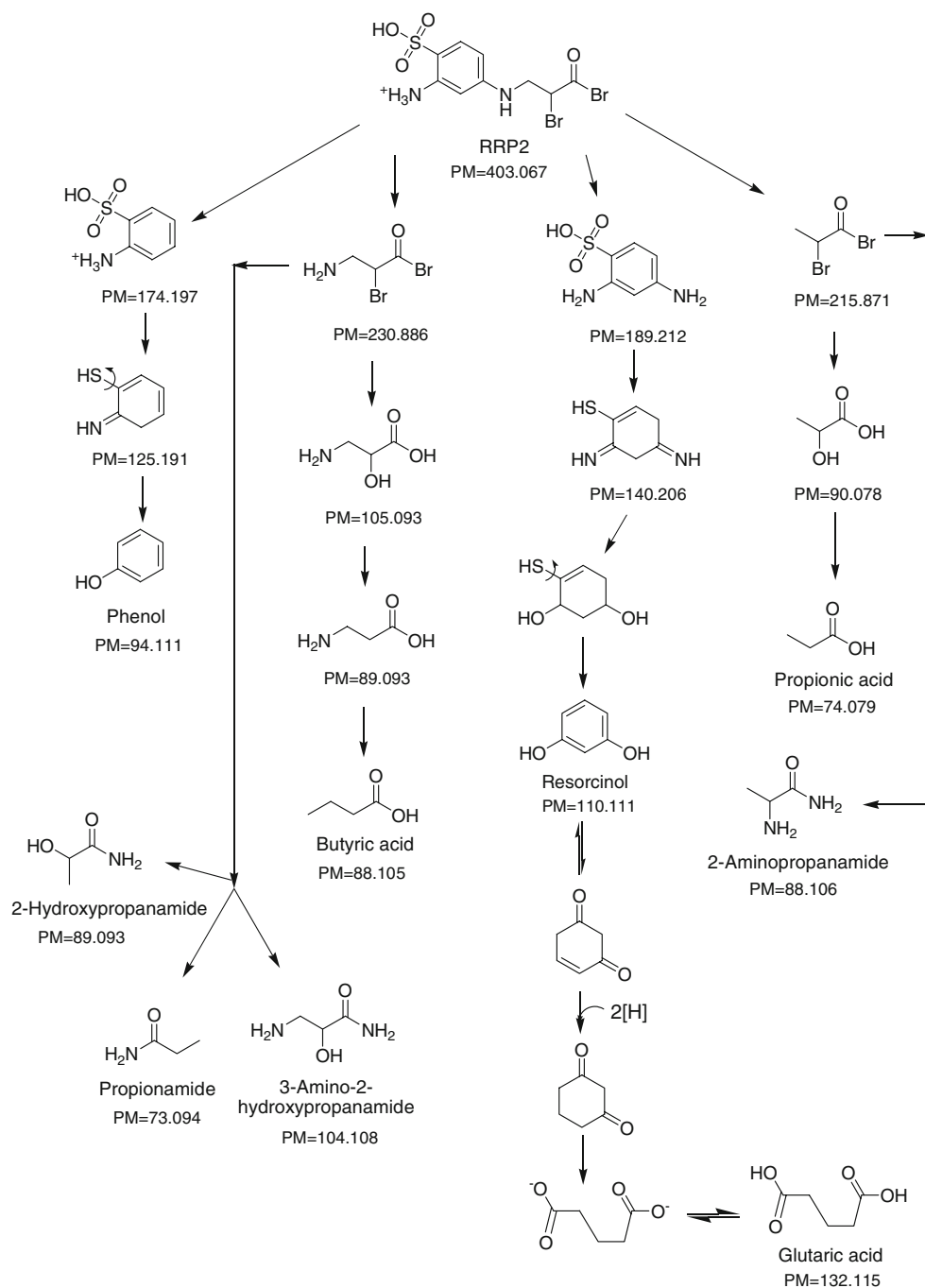


Fig. 8 Mechanism proposes of the route of degradation for the RRP2 molecule



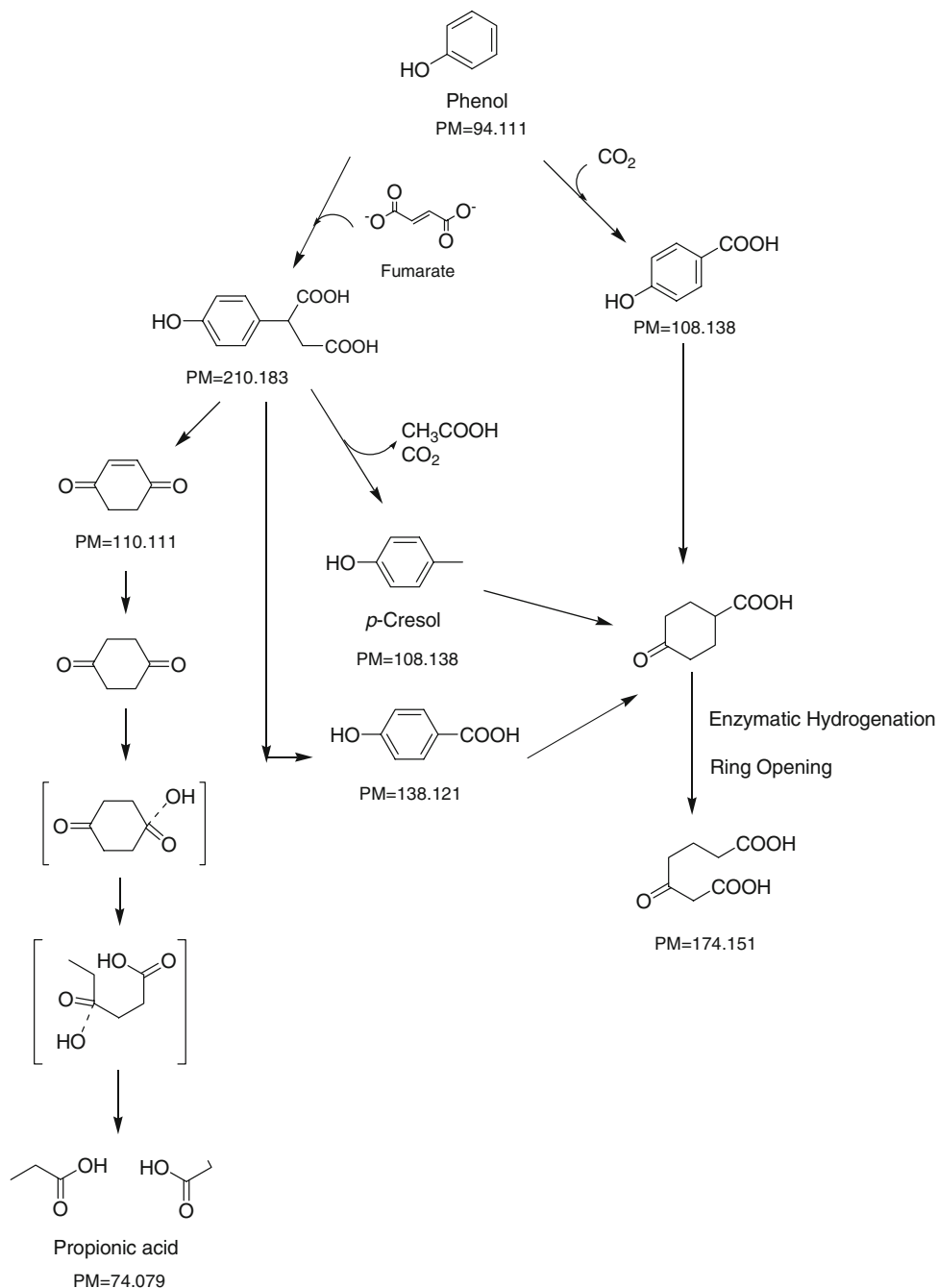
the corresponding quinone to give place to the ring opening. Phenol and derived products can be produced starting from different pathways in the dye degradation mechanism; the proposed route for its decomposition is analyzed in Fig. 9.

The RRP2 product can be decomposed in other two fractions that correspond to the aliphatic part of the molecule: an acid bromide and an acid amino-bromide. Generally, acid halides are derived from carboxylic acids used in the synthesis of some compounds as esters, amides and aromatic acids. The halogen atom of an acid

halide subtracts inductively the electronic density of the carbon in the carbonyl group, increasing its electrophilic nature and turning the molecule predominantly reactive for the nucleophilic substitution of the acid group, therefore, the halide acts as good group to be removed (Wade 2004).

Based in the last statement there were proposed some degradation routes for the acid bromides; the bromide is nucleophilically substituted for the hydroxyl group ($-\text{OH}$) and produce the corresponding acid, or by the amino group ($-\text{NH}_2$) producing amides. The bromide in the position 2 of

Fig. 9 Mechanism proposes of the route of degradation for the phenol



the molecule can be replaced also by the hydroxyl or amino group, producing amino-amides.

Phenols are highly reactive substrates in aromatic electrophilic substitution since the non bonded electrons of the hydroxyl group stabilize the sigma complex that is formed due to an electrophilic attack in the *ortho* or *para* position. Therefore, the hydroxyl group is highly activator and *ortho-para* director (Wade 2004). The proposed pathway to degrade phenol consist in forming a carboxylic group through the addition of fumarate or CO₂ (electrophilic addition), which are bonded to the molecule in the *para*

position. This mechanism occurs in the contrary way of the Phthalic acid production shown in Fig. 7, were the carboxylic group enters in the *Meta* position because -COOH is *Meta* director.

A substitute electron donor as -OH in the phenol molecule activates mainly the *ortho* and *para* positions, and a substitute electron subtractor as the group -COOH disables these positions.

After the electrophilic addition the corresponding redox reactions take place to take the molecule through different routes to the formation of Benzoquinone, *p*-cresol or

hydroxybenzoic acid. Phenols oxidize producing aromatic ketones or diketones named quinones (Wade 2004); once the quinone is formed, the ring opening takes place to produce carboxylic acids.

The *p*-cresol or the hydroxybenzoic acid formed previously are dehydrogenated to form the carbonyl in the –OH position and afterwards is carried out an enzymatic hydrogenation and the ring opening producing a dicarboxylic acid that can be metabolized by bacteria to produce CO₂ and lower weight carboxylic acids.

Ye et al. (2004) presented a review about the biodegradation of nitroaromatic compounds by aerobic and anaerobic media and the degradation pathways that they present for similar compounds, especially for triazines that are difficult to degrade, agree with the routes presented in this work. Tauber et al. (2005) presented a research in which they degraded azo dyes using fungus and ultrasound and they identify as the reduction products: Phenol, CO₂, and carboxylic acids as Oxalic, Malonic, Formic, Propionic and Acetic acid; they also state that the degradation of Phenol produces Catechol, Hydroquinone and Benzoquinone, which are also proposed in this work as Phenol degradation intermediaries to carboxylic acids.

From the products showed in Fig. 9, the *p*-cresol and the propanoic acid were found usually in the water samples at the reactor effluent.

In the proposed degradation pathways are not described all the identified products in the reactor effluent because, as was stated before, it can be carried out several routes due to the cell metabolism or due to extracellular enzymatic reactions, besides, the identification studies were applied only to the water at the effluent instead of analyze the water at different reactor height, in order to identify other higher weight intermediaries to outline the degradation mechanism of the dye. However, there were carried out studies at different conditions, in such a way that, changing the residence time in the reactor and the dye inlet concentration the reaction is restricted, and then we achieve a lower degradation grade at higher dye concentration and at lower residence time; therefore, the aromatic compound identified under these conditions (Table 4) are the main reaction intermediaries.

One of the major compounds identified is the butanamide (3-methyl and 3, 3-dimethyl) that would be produced from the degradation of the previously formed Ethyl-Phenyl-Amine (Fig. 5), amides (Fig. 8), carboxylic acids or from the amino acids of the media. Amides are derived from the acids that are formed through the combination of an acid and ammonia or an amine (Wade 2004), therefore, given the conditions inside the reactor (carboxylic acids and ammonia are produced), these compounds can be produced.

Concluding remarks

A degradation pathway for the degradation of the azo dye Reactive red 272 was explained and proposed based in hydroxylation, carboxylation and redox reactions carried out by enzymes and by means of the interactions with the activated carbon as a carrier and with the substrate, in this case, dextrose.

The achieved degradation grade is a function of the dye concentration at the influent as well as the reactor residence time. Therefore, the degradation grade and the presence of aromatic compounds and amines can be manipulated handling these factors in the treatment of textile wastewater effluents, and so, avoid problems in further treatment process or dispose.

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