

Degradation of a Toxic Mixture of the Pesticides Carbofuran and Iprodione by $UV/H₂O₂$: Evaluation of Parameters and Implications of the Degradation Pathways on the Synergistic Effects

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Received: 16 December 2015 /Accepted: 19 May 2016 /Published online: 30 May 2016 \oslash Springer International Publishing Switzerland 2016

Abstract The degradation of two pesticides, carbofuran (CBF) and ioprodine (IPR), was studied by the photolytic decomposition of hydrogen peroxide $(UV/H₂O₂)$. The influence of two experimental parameters, H_2O_2 concentration and initial pH, as well as their interactions, was investigated. Optimization was carried out where experimental parameters were determined for the treatment of each pesticide. Both pesticides were totally eliminated by $UV/H₂O₂$ system under optimal conditions. However, significant differences were found: CBF degradation was influenced by both parameters and their interactions, while IPR degradation was not statistically affected by initial pH. Interestingly, analysis of degradation pathways showed a major influence of photolysis process and oxidation due to hydrogen peroxide for the CBF degradation, while the synergistic combination between both of them played the most relevant role during IPR degradation. A mixture of both pesticides was also submitted to $UV/H₂O₂$ action in which a lower rate was observed for IPR elimination while CBF was not affected. A 90 % of chemical

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oxygen demand (COD) was removed and 75 % of mineralization was achieved after the treatment of the mixture. Almost 92 % of the toxicity was eliminated making this technique a promising process to treat toxic mixtures of these pesticides.

Keywords Synergistic effect \cdot UV/H₂O₂ \cdot Degradation pathways. Toxicity. Mineralization

Abbreviations

1 Introduction

Pesticides are widely used in different forms such as insecticides, herbicides, and fungicides in order to increase agricultural productivity. An example is the carbofuran (CBF), 2,3-dihydro-2,2-dimethyl-7 benzofuranyl methylcarbamate (Fig. [1a](#page-1-0)), which is widely used in agriculture as an insecticide and it is

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considered a broad spectrum pesticide mainly used for agricultural crops (Hmimou et al. [2014](#page-11-0)), ornamental gardens, and plants. CBF is used by spraying upon the plant and the application on the stored crop (Foo [2016](#page-11-0); Ruíz-Hidalgo et al. [2016\)](#page-12-0). Among others, there is the iprodione, (IPR) 3-(3,5-dichlorophenyl)-N-isopropyl-2,4-dioxoimidazolidine-1-carboxamide (Fig. 1b), a fungicide of the dicarboximide group. It is mainly used against Botrytis on ornamentals plants such as carnation, chrysanthemum, and rose. It is also used in agricultural crops such as potato, tomato, and onion (Lassalle et al. [2014](#page-11-0)).

The continuous use of these products has a significant contribution to water contamination (Campos et al. [2015](#page-11-0)); thus, it raises human health concern, due to their known human toxicity (de Siqueira et al. [2015](#page-11-0)). Specifically, CBF is known to be highly toxic (LD_{50}) 11 mg kg^{-1} in mice) and inhibitor of acetylcholinesterase, a vital enzyme to the functioning of the central nervous system (Campbell et al. [2004](#page-11-0)). Also, it has implications as a potential endocrine disruptor (Klotz et al. [1997](#page-11-0)) and it has a high mobility in soils and a high water solubility (700 mg L^{-1}). Additionally, the presence of this harmful compound in natural waters has been reported (Brkic et al. [2008\)](#page-11-0), which increase the concern about this pollutant. On the other hand, iprodione presents an acute oral toxicity (LD_{50}) >4640 mg kg⁻¹ and an acute dermal toxicity (LD₅₀) $>$ 2150 mg kg⁻¹ in rats. It is considered as being mobile in some soils and then will leach to groundwater (Tomlin [1997\)](#page-12-0). In fact, iprodione has been notified to be able to easily diffuse in water; therefore, it can contaminate living organisms of aqueous environments

Fig. 1 Chemical structures of a CBF and b IPR

(Wauchope et al. [1992](#page-12-0)). Additionally, IPR can cause oxidative damage through free radical production. Recently, it has been reported that its presence in natural waters induced oxidative damage in rainbow trout (Camiletti et al. [2016](#page-11-0); Radice et al. [2001](#page-12-0)).

The detrimental impact on the environment caused by these pesticides has turned the attention to the use of feasible treatment technologies for their removal or their transformation into products with no adverse effects on the environment or in human health. Biological treatments are usually the most convenient process to promote natural decontamination (Marco et al. [1997\)](#page-12-0). Unfortunately, many organic pollutants are not biodegradable and so they are known as bio-recalcitrant organic compounds (Trzcinski et al. [2016](#page-12-0)). This is the case of CBF and IPR which given their relative high toxicity, their degradations could not be reached by biological treatments (de Siqueira et al. [2015\)](#page-11-0). Among the conventional treatments, there are also physical processes, which disadvantage is associated to the pollution phase transfer. Therefore, the need of finding new decontamination processes for these types of compounds increases over the time (Lu et al. [2011a](#page-11-0); Zhu et al. [2012\)](#page-12-0).

As alternative technologies of water treatment, advanced oxidation processes (AOPs) have demonstrated to be effective methods for organic pollutants degradation (Chiron et al. [2000](#page-11-0); De la Cruz et al. [2013](#page-11-0); Brienza et al. [2016;](#page-11-0) Gupta and Mittal [2016](#page-11-0)). Particularly, the combination of ultraviolet (UV) light and hydrogen peroxide (H_2O_2) , so-called UV/ H_2O_2 process, has shown high efficiency for the treatment of natural waters and wastewaters contaminated with non-biodegradable and/or toxic organic compounds. The UV/H_2O_2 process is based in the photolysis of H_2O_2 to produce hydroxyl radicals (HO•) (Chiron et al. [2000;](#page-11-0) Zhou et al. [2012\)](#page-12-0), which promotes organic pollutants degradation according to the following reactions:

$$
H_2O_2/HO_2^- + hv \rightarrow 2HO \bullet (1)
$$

 $HO^* +$ Pollutant \rightarrow degradation products (2)

On the other hand, despite all environmental and human risks of these type of pollutants, up to the date, there are few investigations (Lopez-Alvarez et al. [2011,](#page-11-0) [2012\)](#page-11-0) were the dangerous pesticides, cabofuran and ioprodine, are intent to be degraded by any AOP but any of those had tested UV/H_2O_2 process. Moreover,

most investigations are based on individual pesticides degradation, but for a real condition, a mixture of the pollutants should be considered. However, under the authors knowledge, there is any report where the effects of a mixture between CBR and IPR have been evaluated. Therefore, the aim of this study is to investigate the efficiency of $UV/H₂O₂$ as possible treatment of carbofuran and iprodione, as individual targets, and as a mixture. Operating variables of the $UV/H₂O₂$ process, such as pH and hydrogen peroxide dosage, were studied as well as the synergistic and antagonism effects during the pesticides degradation. Degradation routes for each pesticide were also investigated. Finally, the degradation extent in terms of mineralization, chemical oxygen demand, and toxicity removal was also evaluated.

2 Experimental

2.1 Reagents

CBF raw grade (99.10 % of purity), the commercial grade Furadan, with a formulation of 330 g L^{-1} of CBF and iprodione commercial grade (Rovral), with a formulation of 500 g L^{-1} of iprodione were supplied by Bayer. IPR raw grade (99.1 % of purity) material was supplied by Bayer Cropscience. Acetonitrile, formic acid, dichloromethane, sodium carbonate, sodium bicarbonate, sodium hydroxide, sulphuric acid, ethyl acetate, and hydrogen peroxide 30 % w/w were supplied by Merck. Potassium hydrogen phthalate was obtained from Carlo Erba. All chemicals were used without any further purification. Milli-Q water was used throughout for the preparation of aqueous solutions. All reagents were the highest available purity and were used as received.

2.2 Experimental Design

In this study, the statistical software Statgraphics Plus 5.1 was used. Using this software, multivariate analysis and factorial design were carried out to evaluate the effects and optimize the two experimental variables: the initial pH (3–9) and the hydrogen peroxide concentration (50–200 mg L^{-1}). Fixed pesticide concentrations were used in order to optimize the process: CBF 55 mg L⁻¹ and IPR 12 mg L⁻¹. Additionally, the polynomial equation associated to the reaction, as well as the response surface and the Pareto diagram, was obtained for both pesticides.

This study was performed with a confidence level of 95 %. The degradation percentage was chosen as the response factor after 60 min of irradiation for CBF and 80 min for IPR, which were selected to accomplish with the best statistical validity and qualification of experiments.

2.3 Photolytic System

After pH adjustment of the CBF solution from pH 5.6 (natural pH) and IPR solution from pH 5.3 (natural pH) to the desired initial pH condition, hydrogen peroxide was added at the appropriate concentration and the resulting mixture was stirred. The tests were carried out under constant stirring in a pilot reactor (manufactured by Atlantic Ultraviolet Corporation) containing 19 L of the pesticides solution. The storage tank with the solution was introduced into recirculation system with the reactor. The tests were performed with a mercury lamp low pressure Atlantic Ultraviolet, model MP36B, surrounded by a stainless steel housing. The lamp tube was 86 cm long and 1.5 cm diameter with a maximum output of 38 W. The UV lamp was a monochromatic wavelength of 254 nm. The system had an inlet and outlet of water and a volumetric capacity of 7 L (see SM 1).

2.4 Analysis

The quantification of the pesticides was performed by liquid chromatography (HPLC) in an Agilent 1100 Series instrument. A Zorbax SB C18 column and a diode array UV detector, set at 220 nm for CBF and 210 nm for IPR, were used. The mobile phase was 40/60 acetonitrile/water for CBF and 40/60 acetonitrile/water with formic acid 0.1 % for IPR. Isocratic mode at 1 mL min^{-1} for both pesticides was used. For the quantification of the pesticides mixture, IPR conditions were used.

The complete mineralization of organic compounds, i.e., the transformation of organic matter into CO_2 , H_2O and inorganic ions, was done by measuring the total organic carbon (TOC). This was determined in a COT1010 OI-Analytical instrument. During the irradiation time, samples were taken at timed intervals and filtered with filters of 0.45 μm PVDF Millipore Millex[®]-HV to remove impurities. A solution of potassium phthalate was used as the calibration standard.

Chemical oxygen demand (COD) measurements were carried out according to the closed reflux titrimetric method (APHA [2005\)](#page-11-0) in a Nanocolor 500D instrument. The reduction of toxicity was analyzed by using Vibrio Fisheri with a Biofix® Lumi-10 instrument. Chlorine quantification was determined by ionic chromatography Dionex ICS-1000 equipped with an IonPac®AS14A column.

3 Results and Discussion

3.1 Effect of H_2O_2 Concentration and Initial pH During the Degradation of Carbofuran and Iprodione

Two of the most important chemical parameters in the evaluation of UV/hydrogen peroxide system are the initial pH of the solution and the hydrogen peroxide concentration (Rubio-Clemente et al. [2014\)](#page-12-0). In order to evaluate the influence of these two parameters on the degradation of carbofuran and iprodione by UV/ H_2O_2 , a factorial design was implemented using the Statgraphics Plus 5.1 software. Table [1](#page-4-0) shows the matrix design obtained by the computer program. The table shows the experimental conditions and the response factor for each experiment, defined as the percentage of degradation after 60 and 80 min of treatment for CBF and IPR, respectively.

Figure 2 shows the response surface methodology (RSM) obtained for the two pesticides (Fig. 2a for CBF and Fig. 2b for IPR). As shown in Fig. 2 and Table [1,](#page-4-0) the elimination of both pesticides increases by the rise of H_2O_2 concentration. As stated in Eq. [2,](#page-1-0) the increment of hydrogen peroxide concentration increases the formation of HO• radicals that consequently improve CBF and IPR degradation. However, for both pesticides, maximum degradation is reached when H_2O_2 concentration was around 170 mg L^{-1} ; and then elimination processes became inhibited at higher doses of hydrogen peroxide. This behavior is associated to H_2O_2 overdosing that would consume radical species (Eqs. 3–6). A similar situation has been previously reported in other investigations (Guzmán et al. [2016](#page-11-0)).

$$
HO^{\bullet} + H_2O_2 \rightarrow HO_2^{\bullet} + H_2O \tag{3}
$$

$$
HO_2^{\bullet} + HO_2^{\bullet} \rightarrow H_2O_2 + O_2 \tag{4}
$$

$$
HO_2^{\bullet} + HO^{\bullet} \rightarrow H_2O + O_2 \tag{5}
$$

$$
2HO^{\bullet} \rightarrow H_2O_2 \tag{6}
$$

Significant differences were observed when the effect of initial pH was evaluated. For a relative low concentration of hydrogen peroxide (50 mg L^{-1}), CBF degradation showed to be improved by the increase of pH. In fact, CBF elimination increased almost 15 % from acidic $pH(3)$ to neutral $pH(7)$ reaching up almost 80 % of elimination and followed by a plateau (Fig. 2a). On the other hand, the pH showed a minor effect for a relative high concentration of hydrogen peroxide (200 mg L^{-1}) with a variation of only less than 5 % and reaching up total elimination of CBF at neutral pH.

Fig. 2 Optimization of H_2O_2 concentration and initial pH during the treatment by UV/H₂O₂ system of a CBF (55 mg L⁻¹) after 60 min and b IPR (11 mg L−¹) after 80 min of treatment using a response surface diagram

Test	pH	H_2O_2 (mg L^{-1})	CBF			IPR		
			Experimental $(\%)$	Calculated $(\%)$	Error $(\%)$	Experimental $(\%)$	Calculated $(\%)$	Error $(\%)$
1	3.00	50	64.89	64.77	0.19	75.91	78.44	3.23
$\overline{2}$	9.00	50	78.50	78.32	0.23	55.73	54.90	1.51
3	3.00	200	92.46	91.78	0.74	59.61	63.06	5.47
$\overline{4}$	9.00	200	96.31	95.57	0.77	86.50	86.59	0.10
5	3.00	125	88.44	89.24	0.90	85.74	84.48	1.49
6	9.00	125	96.97	97.90	0.95	88.47	84.48	4.72
7	6.00	50	75.00	75.30	0.40	80.00	78.30	2.17
8	6.00	200	96.00	97.43	1.47	90.00	86.46	4.09
9	6.00	125	98.30	97.32	1.01	92.65	96.12	3.61
10	6.00	125	97.90	97.32	0.60	96.82	96.12	0.73
11	6.00	125	97.48	97.32	0.16	96.94	96.12	0.85

Table 1 Experimental design for carbofuran and iprodione degradation by $UV/H₂O₂$ and comparison between experimental data and calculated from the mathematical model

In contrast, for 50 mg L^{-1} of added H₂O₂, IPR degradation showed to be negatively affected by the increment of the solution pH (Fig. [2b](#page-3-0)). In this case, IPR elimination decreased approximately 20 % from acidic medium (pH 3) to basic medium (pH 9) with a maximum of ∼80 % of elimination at pH 5. Interestingly, the pH effect was contrary for 200 mg L^{-1} of hydrogen peroxide showing a remarkable increment of IPR elimination while the pH increases from 3 to 7, reaching a maximum of ∼90 % of degradation.

These results could be attributed to the selfdecomposition of H_2O_2 at high pH or to the hydroxyl radical scavenger property of the OH[−] ions which are highly concentrated at basic pH (Zhou et al. [2012](#page-12-0)) and compete with the pesticides for the produced hydroxyl radicals. However, both effects are less notable for a relative high concentration of H_2O_2 (200 mg L^{-1}) where the production of HO• radicals is higher and the scavenger effect or the self H_2O_2 decomposition can be offset. Furthermore, in the case of CBF degradation, this effect is not significant suggesting that an additional degradation process besides HO• radicals could be involved.

Moreover and based on the interaction plots (SM2), no significant interaction between the variables (pH and H_2O_2 concentration) was obtained during CBF treatment where the changes in the response were almost parallel. In the case of IPR degradation, in an opposite way, inverse tendencies in the change in response factors were observed, which suggests a significant interaction between the variables for this pollutant. These findings support that different degradation routes are involved in the elimination of the pesticides CBF and IPR.

3.2 Optimization of CBF and IPR UV/H₂O₂ Degradation

In order to optimize the process, it is necessary to evaluate which variables, and interactions between these variables, have a significant effect on the $UV/H₂O₂$ process. The Pareto diagram (Fig. [3a](#page-5-0) for CBF and Fig. [3b](#page-5-0) for IPR) represents a valuable tool to evaluate this by showing both magnitude and significance of the effects (variables and interactions) (Rodríguez-Chueca et al. [2012](#page-12-0)). A positive effect of a variable indicates that the CBF or IPR degradation increases at high values of the respective variable, while negative effect indicates that the degradation increases at low values of the var-iable. According to Fig. [3a](#page-5-0), both variables $(H_2O_2 \text{ con-}$ centration and pH) can be considered statistically important for the treatment of CBF. Positive effects indicate that CBF degradation increases with the increase of hydrogen peroxide concentration and pH value. Additionally, the Pareto diagram shows a negative effect by the interaction between both variables (AB) on the response factor representing an antagonist effect on the degradation process.

Fig. 3 Pareto diagram of the degradation of a CBF (55 mg L^{-1}) . **b** IPR (11 mg L^{-1}) by $UV/H₂O₂$. Figure obtained with the Statgraphics Plus 5.1 software according to the design of experiments presented in Table [1](#page-4-0)

On the other hand, Fig. 3b shows that only the $H₂O₂$ concentration (B) has significant effect on IPR degradation. Moreover, interaction (AB) between the two variables (pH and H_2O_2 concentration) shows a synergistic effect, while AA and BB showed a negative contribution represented at the mathematical description (Eqs. 7 and 8). A relevant fact must be mentioned about the initial pH, where despite the observed effect in Fig. [2b,](#page-3-0) the Pareto diagram indicates that changes are not statistical significant for the degradation of IPR.

This experimental design methodology also leads to obtaining a mathematical model that directly relates the influential variables and interactions with the response factor (% degradation) thereby the study of the pollutant degradation is facilitated. For this purpose, it becomes relevant to involve the sign of the quadratic value of each variable. Then, for both pesticides, AA as well as BB have negative coefficients (Fig. 3a, b). After multiple regressions using the statistical software, the mathematical models are obtained for CBF (Eq. 7) and IPR (Eq. 8), where Y (%) represents the degradation percentage.

$$
Y_{CBF}(\%) = 16.6368 + 7.8026 [pH] + 0.699572 [H2O2] - 0.41693 [pH]2 - 0.0108444 [pH] [H2O2] - 0.0019479 [H2O2]2
$$
 (7)

$$
Y_{IPR}(\%) = 43.8576 + 8.97197 [pH] + 0.351116 [H_2O_2] - 1.29246 [pH]2
$$

+ 0.0523 [pH] [H₂O₂] - 0.00244215 [H₂O₂]² (8)

Table [1](#page-4-0) shows the comparison between experimental results and those predicted by the models (Eqs. [7](#page-5-0) and [8\)](#page-5-0). As shown in Table [1,](#page-4-0) the proposed models predict the experimental results quite accurately. In fact, less than 1.5 % of error was obtained between experimental and calculated data for CBF, while a maximum of 5.5 % of error was observed for IPR degradation. Additionally, the fraction of the variation response (R^2) was 89.5 % for both models, which demonstrates a sufficient validity between them.

Therefore, according to the response surface diagrams (Fig. [2a, b](#page-3-0)) and the reduced models (Eqs. [7](#page-5-0) and [8\)](#page-5-0), the optimal values for the photocatalytical degradation of the pesticides under the work conditions are initial pH 7.28 and 160 mg L^{-1} of H₂O₂ for CBF, while initial pH 6.54 and 142 mg L^{-1} of H₂O₂ for IPR.

Both pesticides degradation by UV/H_2O_2 system showed a common pseudo-first order profile which lead to a kinetic model that describes each process (SM 3). Then, the kinetic models can be compared to the statistic models (Eqs. [7](#page-5-0) and [8\)](#page-5-0) by determining the elimination of the pollutants under optimal conditions. Based on the models, 7 % of difference between the statistic model and the kinetic model can be observed for the case of CBF degradation and only 4 % for IPR degradation. This small difference indicates a good correlation between both models describing the degradation processes of the pollutants.

3.3 Characteristics of the Photolytic UV/ H_2O_2 Degradation of CBF and IPR Under Optimal Conditions

3.3.1 Main Degradation Pathways

During the degradation of organic pollutants using the photolytic decomposition of hydrogen peroxide, different processes could be involved according to the target molecules. Given that UV/H_2O_2 is a photolytic process and several organic pollutants are considered photoactive, degradation due to direct photolysis of the pesticides must be evaluated. Additionally, the use of hydrogen peroxide contributes to the degradation of many organic compounds given that it is a powerful oxidative agent. Figure [4a](#page-7-0) shows the contribution of both UV radiation and hydrogen peroxide oxidation to the degradation of CBF during $UV/H₂O₂$ process. For

deeper investigation, experiments using the optimal conditions were carried out (initial pH 7.28 and 160 mg L⁻¹ of H₂O₂ for CBF (55 mg L⁻¹); initial pH 6.54 and 142 mg L⁻¹ of H₂O₂ for IPR (12 mg L⁻¹).

A direct photolysis can be observed reaching 30 % of CBF elimination. However, a plateau is obtained after 100 min of irradiation. On the other hand, the effect of hydrogen peroxide as oxidative agent eliminates 50 % of CBF after 140 min of reaction. These results suggest that CBF could be only partially oxidized by UV light or $H₂O₂$, making necessary the application of stronger oxidative techniques, such as $UV/H₂O₂$, for its complete removal. In contrast, UV/H_2O_2 process reaches total elimination of CBF after 140 min of treatment. Then, these findings indicate that photolysis as well as H_2O_2 oxidation and •OH radicals is involved during CBF degradation by $UV/H₂O₂$ process.

On the other hand, the degradation profile of IPR shows a different behavior (Fig. [4b](#page-7-0)). As observed, UV radiation removes only 17 % of the pollutant after 240 min and hydrogen peroxide removes 22 %. These results indicate that IPR can be considered a more resistant compound than CBF against UV or H_2O_2 action. Despite that, the combined action of UV radiation and the oxidant $(UV/H₂O₂$ system) leads to the total elimination of the pesticide after 160 min of treatment.

The contribution of UV radiation and hydrogen peroxide during the oxidation of both pesticides could result in synergistic or antagonistic effects, which must be determined to a better understanding and optimization of the system. Synergy (S) for both CBF and IPR degradation, by UV/H_2O_2 system, can be determined using the following equation (Torres et al. [2008\)](#page-12-0):

$$
S = \frac{\% \text{ Removed } UV / H_2O_2}{\% \text{ Removed } UV + \% \text{ Removed } H_2O_2}
$$
(9)

where % Removed corresponds to the removed percentage of each organic pollutant by each applied system (UV/H₂O₂, UV, and H₂O₂). An S value larger than 1 indicates a synergistic effect. Oppositely, S values smaller than 1 indicate an antagonistic effect among the combined processes. In spite after 100 min of treatment more than 90 % for both pesticides is eliminated (Fig. [4a, b](#page-7-0)), interesting differences in synergy were found. In fact, the calculated synergies were $S_{\text{CBF}}=1.3$ and $S_{IPR} = 7.2$. The high synergistic effect found during Fig. 4 a CBF degradation profiles by UV radiation, H_2O_2 action, and $UV/H₂O₂$ system under optimal conditions. 55 mg L^{-1} of CBF; initial pH 7.28 and 160 mg L^{-1} of H₂O₂. **b** IPR degradation profiles by UV radiation, H_2O_2 action, and UV/ $H₂O₂$ system; and chlorine accumulation during $UV/H₂O₂$ treatment under optimal conditions. 11 mg L^{-1} of CBF; initial pH 6.54 and 142 mg L^{-1} of $H₂O₂$

IPR degradation suggests that this pesticide is much more influenced by HO• radicals, which come from the combined action of UV light and hydrogen peroxide. In contrast, the poor synergistic effect for CBF states that photolysis and hydrogen peroxide action, acting individually, play the main role in the process.

Based in the fact that the main degradation pathway of CBF is through photolysis and hydrogen peroxide action, according to the literature, some possible CBF by-products can be proposed. During the photodecomposition of CBF, the attack on the C-O bond of the carbamate group is probably the first step of the degradation route. The break of this bond leads to a cation on a basic nitrogen and a phenolic anion that is stabilized by an H- or OH-abstraction to produce 7phenolcarbofuran or carbamic acid, respectively. The continuous irradiation could produce another by-product identified as 2,3-dihydro-2,2-dimethylbenzofuran-7-ol (Bachman and Patterson [1999\)](#page-11-0). Under our knowledge, no by-products coming from the attack of hydrogen peroxide have been reported. On the other hand, as early indicated, in a lower extend CBF is also degraded by HO•. Therefore, the HO• could attack the C-O bond of the carbamate group to produce 7-phenolcarbofuran and carbamic acid as initial step. Subsequently, hydroxylations have been reported leading to 3-hydroxycarbofuran and 3 hydroxy-7-phenolcarbofuran followed by successive oxidations to produce 3-ketocarbofuran and 3-keto-7 phenolcarbofuran (Fenoll et al. [2013;](#page-11-0) Lu et al. [2011b;](#page-12-0) Lopez-Alvarez et al. [2012\)](#page-11-0).

Regarding the IPR degradation, little information is currently available describing its degradation. Given that IPR is a dichloride organic molecule, the evolution of Cl- was also investigated during this pesticide degradation process. Results show a perfect opposite behavior of IPR elimination with chlorine ion accumulation (Fig. [4b](#page-7-0), secondary axis). The inverse relationship between the target molecule and Cl- indicates an easily loss of Cl ring substituents, suggesting the HO• attack into the carbon-chloride bond as one of the firsts steps during IPR degradation. The susceptibility of these bonds have been also reported during the photodecomposition of IPR leading to the substitution of the Cl atoms by OH groups (Lassalle et al. [2014](#page-11-0)).

3.3.2 Degradation Extend by H_2O_2 Photolytic Process

It is well known that pollutant removal is not enough evidence to test the efficiency of certain applied treatment. Previous reports have shown that in some cases, AOPs can transform the initial substrate into more dangerous contaminants (Giraldo et al. [2010\)](#page-11-0). That is the case of halogenated organic molecules that could be degraded into hazardous compounds such as mono, di or trichloromethane and chlorobenzenes, which are known to be high carcinogenic molecules. Therefore, in order to guarantee the efficiency of the treatment of waters contaminated with CBF or IPR, the evolution of COD, TOC, and the toxicity $(1/EC_{50})$ of the photo-treated solutions were evaluated (Fig. [5a, b](#page-9-0), respectively). For the case of CBF, the toxicity of the initial solution was considerably reduced from 0.09 to almost 0.01 after 390 min of treatment. Additionally, only 16 % of COD and 18 % of TOC remains in the solution at the end of the treatment (390 min). Under this panorama, toxicity could be attributed either to the remained concentration of pesticide or to the presence of toxic degradation by-products. However, the decreasing behavior of both COD and TOC suggest the hazardous compounds could be totally eliminated so as their toxicity with longer process.

In the case of IPR, after 240 min, solution toxicity (1/EC₅₀) was reduced into ∼88 % (Fig. [5b\)](#page-9-0). In it turn, COD measurement showed an elimination of ∼82 % after 240 min, while at the same time, TOC was 76 % removed. Additionally, the elimination tendencies of COD, TOC, and toxicity rapidly achieved a plateau after 160 min of treatment, which is the time where IPR was totally removed from the treated solution. These findings suggest that toxicity is mainly attributed to IPR, but also there some intermediates that are recalcitrant to UV/ $H₂O₂$ action although they could be considered less dangerous given that toxicity was significantly removed. Furthermore, the TOC removal from the beginning of the experiment suggests that in addition to the IPR dechlorination, others parallel degradation routes, which lead to a fast mineralization of the pesticide, also occur.

The previous discussed differences in terms of synergy during both pesticides degradation turn interesting to investigate this phenomenon for the degradation extents. In order to evaluate this, COD and TOC removal were calculated for each involved process after 60 and 100 min of treatment, respectively (data not shown). Regarding CBF, 14 % of COD and 4 % of TOC was removed by UV irradiation. The sole H_2O_2 action leads to 8 % of COD and 8 % of TOC removal, while for the combination UV/H₂O₂ 57 % of COD and 26 % of TOC removal was observed. The same experiment was performed with IPR as target molecule. Results show that 15 and 8 % of COD and TOC were removed in the solution using the sole UV irradiation. 12 % of COD and 12 % of TOC were eliminated by hydrogen peroxide action but 72 and 70 % of COD and TOC, respectively, were eliminated by the combination of the processes $(UV/H₂O₂$ system). Using Eq. [9](#page-6-0), synergistic effect for the degradations extents (S_{COD} and S_{TOC}) can be determined: $S_{\text{COD,CBF}} = 2.6$, $S_{\text{TOC-CBF}} = 2.1$, $S_{\text{COD,IPR}} = 2.7$ and $S_{\text{TOC,IPR}} = 3.5$. These results indicate a synergistic effect on both the COD and TOC removal for both pesticides during UV/H_2O_2 system attributed to the formation of hydroxyl radicals, which efficiently promote the oxidation of the organic compounds.

3.4 Evaluation of the Photocatalytical Degradation of CBF and IPR in a Mixture

Despite UV/H_2O_2 system have shown to be an efficient technique to degrade the two tested pesticides, it becomes important to investigate the viability of the process to treat a solution containing a mixture of both pollutants. To evaluate this, a new set of experiments were carried out using an equimolar solution containing 3.3×10^{-5} mol L⁻¹ of each pesticide at pH 7.00 and 150 mg L⁻¹ of H₂O₂. Figure [6a](#page-10-0) shows the degradation profiles of the two pesticides individually and both of them at the mixture. Interestingly, CBF showed the same profile in the mixture as individually, which indicates that the presence of IPR in the mixture did not Fig. 5 TOC, COD, and toxicity evolution during $UV/H₂O₂$ system using optimal conditions. \mathbf{a} CBF. 55 mg L⁻¹ of CBF; initial pH 7.28 and 160 mg L⁻¹ of H₂O₂. **b** IPR. 11 m L^{-1} of CBF; initial pH 6.54 and 142 mg L^{-1} of H_2O_2

affect the elimination of carbofuran. In the presence and absence of iprodione, carbofuran is practically eliminated after 100 min of treatment. In an opposite way, IPR elimination was significantly inhibited by the presence of CBF. In fact, in the presence of CBF, UV/H_2O_2 process reached ∼65 % of IPR elimination after 120 min, while 100 % of IPR elimination was achieved at the same time in its absence. As above stated, there is a contribution of each individual process (UV light and H_2O_2) to promote CBF degradation. Consequently IPR, which is mainly degraded by HO• radicals, do not affect CBF degradation. On the other hand, CBF consume a considerably proportion of both photons and H_2O_2 and therefore hydroxyl radicals are generated in a lesser extent. As a result, IPR degradation is inhibited by presence of CBF.

On the other hand, Fig. [6b](#page-10-0) shows the evolution of TOC and COD for the mixture of both pesticides. Results showed a ∼90 % of COD elimination and a ∼75 % of TOC removal. The remaining COD and TOC in solution could be attributed to the amount of IPR that could not be oxidized after 300 min of treatment in the mixture solution and the presence of some by-products. A notable tendency of COD and TOC reduction is observed, which makes possible the application of this technique in a mixture of two pollutants. In order to provide more information about the treated solution, toxicity evolution was determined. As observed in Fig. [6b,](#page-10-0) almost 92 % of the mixture toxicity was eliminated after only 300 min of treatment, which confirms the high potential of the UV/ $H₂O₂$ as alternative to the environmental concerns associated to the presence of these pesticides in waters.

Fig. 6 a Degradation profile of CBF, IPR, and their equimolar mixture using $UV/H₂O₂$ system at initial pH 7.0 and 150 mg L^{-1} of H₂O₂. **b** COD, TOC, and toxicity evolution during the treatment of an equimolar mixture of CBF and IPR by $UV/H₂O₂$ at initial pH 7.0 and 150 mg L⁻¹ of H₂O₂

4 Conclusions

The evaluation of H_2O_2 and initial pH effects by experimental design methodology showed that both parameters are statistically significant during CBF degradation. However, for IPR degradation, H_2O_2 concentration was the only variable statistically significant. The optimal conditions were determined for each pesticide: pH 7.28 and 160 mg L^{-1} of H₂O₂ for CBF, while pH 6.54 and 142 mg L^{-1} of H₂O₂ for IPR. Different processes were involved during the degradation of the pesticides. CBF degradation was mainly promoted by the additive action of direct photolysis and hydrogen peroxide oxidation. In contrast, the main degradation route of IPR was to the attack of HO• radicals produced by the UV/H₂O₂ system. Additionally, the inverse relationship between the released chloride ions and IPR along the treatment suggested the attack of HO• radicals into the C-Cl bond as the first step in the degradation process. Both pesticides were totally eliminated under optimal conditions by $UV/H₂O₂$ system; where approximately 80 % of COD and TOC were eliminated for CBR and IPR after 6 and 4 h of treatment, respectively. Different behaviors were found when a mixture of the two pesticides was treated. CBF degradation was not significantly affected by the presence of IPR in the mixture solution, while IPR

elimination was inhibited. A 90 % of COD was removed during the treatment of an equimolar mixture of the pesticides and 75 % of mineralization was reached after the treatment. The toxicity of the mixture solution was reduced in about 92 %, which highlight the application of this technique as alternative for the treatment of toxic mixtures of the pesticides, transforming them into nontoxic substances.

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