

# **Aminated polyacrylonitrile fbers for the removal of hydrogen sulfde from natural gas at room temperature**

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## **Abstract**

 $H<sub>2</sub>S$  is a common toxic gas in natural gas processing, and adsorption is a promising technology for hydrogen sulfde removal. However, current desulfurization agents suitable for low ambient temperatures and easy regeneration remain a challenge. In this paper, aminated polyacrylonitrile was directly synthesized in a one-step reaction from widely available engineering PANF (polyacrylonitrile fiber) for  $H_2S$  removal at ambient temperature. The fber samples at various stages were characterized in detail, and the adsorption behavior of PANF-DETA (diethylenetriamine) on  $H_2S$ under diferent conditions (weight gain rate, temperature, moisture) was investigated. The results showed that the aminated fibers could rapidly absorb  $H<sub>2</sub>S$  by acid–base proton reaction. The optimal sulfur capacity of  $H_2S$  reached 16.2 mg/g when the weight increase rate of aminated fbers was 60%, which was 15 times greater than the adsorption capacity of pure polyacrylonitrile fbers. The saturated fber can be efectively regenerated through alkali rinsing. After ten consecutive regenerations, the sulfur capacity of the aminated fiber is  $13.6$  mg/g, which remains at more than 80% of the initial capacity. Overall, fber sorbents have excellent thermal stability, reusability, chemical stability. It can efectively adapt to various practical application environments and is a promising new type of adsorbent.

**Keywords** PANF · Amination reaction · Ambient desulfurization agent · Regeneration performance

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### **Introduction**

The presence of hydrogen sulfde, a common contaminant in natural gas processing, poses a signifcant threat to human health and causes catalyst poisoning, equipment pipe corrosion, and severe environmental contamination (e.g., acid rain) through sulfur dioxide generation  $[1-3]$  $[1-3]$  $[1-3]$ . In order to ensure the safety of natural gas production and use, it must be strictly removed. Over the years, scientists and researchers have developed a variety of  $H<sub>2</sub>S$  treatment technologies for complex desulfurization scenarios, including catalytic oxidation desulfurization [\[4](#page-14-2)], adsorption [\[5](#page-15-0)], wet absorption [[6\]](#page-15-1), and selective oxidation [[7](#page-15-2)]. Generally, natural gas with a hydrogen sulfde concentration of less than 2% (mol/%) or daily sulfur content of less than 5t/d is referred to as a medium to a low sulfur-bearing gas reservoir [\[8\]](#page-15-3). Adsorption is widely used to remove hydrogen sulfde from smalland medium-scale sulfur-bearing gas reservoirs because of its mild operating conditions, high degree of purifcation, energy, and cost savings. However, as the most extensively used commercial adsorbents, metal oxide-based adsorbents are limited by reaction kinetics and can only show strong  $H_2S$  purification capability in harsh medium to high-temperature conditions  $[9-12]$  $[9-12]$  $[9-12]$ . In addition, most of these used adsorbents are currently disposed of in the form of discard or landfll, which cannot achieve the efect of resource utilization and causes severe ecological pollution [\[13\]](#page-15-6). In order to avoid these problems, researchers are developing new strategies to provide more efective solutions.

In recent years, many new porous adsorbents such as activated carbon [[14](#page-15-7)], graphene oxide [[15](#page-15-8)], zeolite [\[16\]](#page-15-9), mesoporous silica [[17\]](#page-15-10), and metal–organic frameworks (MOFs) [[18](#page-15-11)] materials have been used for the removal of  $H_2S$  from natural gas at room temperature and have demonstrated impressive performance. However, high preparation costs, complex preparation process, structural instability, and low reproducibility limit their further application in gas purifcation [[19](#page-15-12)]. In general, enhancing the regeneration capability of sorbents is crucial because the majority of sorbents currently utilized cannot be recycled and may even need to be disposed of in landflls [[20\]](#page-15-13). The carrier is a crucial factor afecting the lifetime of the adsorbent. As an essential component of solid adsorbents, there are generally strict requirements for their use. Developing green, stable, efficient, and universally applicable carriers have been one of the main focuses of adsorbent material design. As one of the three primary synthetic fbers used today, PANF (Polyacrylonitrile fber) has a high specifc surface area, is rich in cyano, and is chemically active, allowing it to be easily chemically modifed and converted into functionalized fbers with other functional groups [[21](#page-15-14)]. Protected by polymer chains, PANF also has excellent chemical resistance, high thermal stability, and good mechanical properties [[22](#page-15-15)]. In addition, as a very mature man-made fber, in the actual desulfurization scenario, people can use it according to the process requirements for its directional mechanical processing into suitable shapes (such as flament bundles, woolen strips, non-woven fabrics, fber columns), which provides even more advantages for its use as a substrate material for desulfurization agents [[23](#page-15-16)]. More importantly, unlike metal oxide-based adsorbents, PANF with a carbon chain backbone has the advantage of being naturally environmentally friendly. Currently, polyacrylonitrile materials have been widely used in the removal, separation enrichment, detection, and catalytic preparation of heavy metal ions and organic dyes [[24\]](#page-15-17). To the best of our knowledge, there are few studies on applying polyacrylonitrile fbers to acid gas adsorption. Most studies on using fibrous materials for  $H_2S$  capture have focused on improving the adsorption performance, neglecting the critical reusability for its practical application [\[25–](#page-15-18)[27](#page-15-19)].

Amine groups are one of the basic adsorption groups that exhibit a high binding ability to many acidic groups. In the feld of hydrogen sulfde removal, the widely used alcohol-amine method [\[28](#page-15-20)] utilizes the acid–base interaction between amine groups and hydrogen sulfde to achieve hydrogen sulfde uptake. In designing various solid adsorbents, researchers often graft amine groups onto the surface of the carrier to effectively improve the desulfurization efficiency. Since  $\gamma$  cyano  $(-CN)$  does not directly interact with  $H<sub>2</sub>S$ , the physical adsorption of  $H<sub>2</sub>S$  by PANF's pore structure alone cannot achieve the purifcation standard. Herein, we prepared aminated polyacrylonitrile fibers (PANF<sub>DETA</sub>) by a one-step reaction using commercially available polyacrylonitrile fbers as the base material and DETA as the modifying reagent to use them for hydrogen sulfde removal at room temperature. Desulfurization experiments investigated the adsorption behavior of fibers on  $H_2S$ , and the focus was on the excellent regeneration performance of the fber adsorbent to evaluate its potential as a desulfurizer substrate material. The fber samples at various stages were systematically characterized by Fourier transform infrared spectroscopy (FTIR), thermogravimetric analyzer (TGA), swept surface electron microscopy (SEM), and X-ray difractometer (XRD), aiming to provide new ideas for the removal of  $H_2S$  at room temperature.

## **Experimental**

#### **Materials and reagents**

Polyacrylonitrile fber (commercially available), diethylenetriamine, ethanol, hydrochloric acid, sodium hydroxide, acetic acid, and zinc chloride, analytically pure, were all purchased from Chengdu Kelong Chemical Reagent Factory.

#### **Apparatus and instruments**

The modifcations of the functional groups on the surface of the fbers were observed by using a Fourier transform infrared spectrometer (FT-IR, KBr, 4000- 500 cm1) BRUKE TENS OR27 (Germany). The thermal stability of the fbers was tested in a nitrogen atmosphere from room temperature to 800 °C at a rate of 10 °C min−1 using a TG/DTA 6300 simultaneous thermal analyzer (Netzsch Company, Germany). To track the changes in the elemental composition of the fbers, a Vario EL Cube elemental analyzer (Germany) was used (C, N, and O). Using a Japanese

XD series X-ray difractometer (CuK radiation at 40 kV and 30 mA), fbers with diferent interior crystal structures were highlighted. A PHS-3E pH meter (Shanghai Yidian Scientifc Instrument Co., China) measured the solution pH. The sample was dispersed uniformly on a conductive adhesive tape, which was bonded to the sample holder, and the excess sample was blown off using an ear wash ball. A Zeiss sigma300 observed the surface morphology of the fbers at diferent stages and swept the surface electron microscope.

#### **Preparation of fber adsorbent**

The specifc preparation steps of aminated fbers are as follows: Firstly, PANF is torn into fne flaments and placed in ethanol for 6–8 h to wash away possible impurities on the fber surface. The fbers are removed, washed with distilled water to neutral, dried at 50 °C to constant weight, and sealed for storage. In order to prevent cyanohydrolysis and the generation of amide structures, a pure amine solution was chosen as the reaction solvent. Take 10 g of pretreated PANF submerged in anhydrous diethylenetriamine (analytical purity), raise the temperature to 125–130℃, continuous refux stirring for 4–6 h and observe the fber state, stop the reaction when the fber starts to melt. After the reaction was completed, to thoroughly clean the organic amine residue on the fber surface, the fbers were removed after the fask was cooled entirely and rinsed repeatedly with hot water at 70–80 °C until the fltrate pH was 7–8. Next, the fbers were rinsed with distilled water and anhydrous ethanol until the pH was stabilized at pH 7. Finally, the fibers were dried at 50  $\degree$ C to a constant weight and weighed to obtain golden yellow aminated fbers. The reaction schematic of the preparation process is shown in Fig. [1](#page-3-0).As an important indicator to



(b) Synthetic schematic diagram of modified fiber

<span id="page-3-0"></span>**Fig.1** Preparation of aminated fber adsorbent: **a** schematic diagram of modifcation reaction; **b** synthetic schematic diagram of modifed fber

evaluate the degree of amination reaction, the rate of fber weight gain is determined by the Eq.  $(1)$  $(1)$ :

<span id="page-4-0"></span>
$$
W = \frac{m_2 - m_1}{m_1} \times 100\%
$$
 (1)

*W* is the weight gain rate (%);  $m_1$  and  $m_2$  are the masses (g) of fibers before and after the reaction.

#### **Desulfurization and regeneration experiments**

The adsorption experiments were performed in a fxed-bed metal reactor (height 8 cm, diameter 6 mm). Stainless steel columns were used as fxed beds for H2S adsorption to achieve smooth and well-dispersed adsorbent. The sulfur-containing gas used was a standard gas with a mass concentration of 5300 ppm. The gas fow rate used for the experiments was 5 ml/min, controlled by a mass fow meter. The fber dosage was 0.5 g. This gas was passed into the metal tube containing the adsorbent for the desulfurization experiments. The room temperature was 40  $^{\circ}$ C. The composition of the efuent gas was analyzed with a gas analyzer (Methanex, Inc., USA) with a detection limit of 0.1 ppm. The  $H_2S$  concentration in the exhaust gas is measured every 5 min until the  $H_2S$  concentration in the outflow gas reaches 4 ppm; then, the experiment is stopped, and the corresponding time is recorded as the penetration time.

Prepare 50 ml of diferent concentrations of sodium hydroxide solution for the desorption of saturated fbers. After the desulfurization experiment, the fbers were taken out and immersed in sodium hydroxide solutions with diferent concentrations for a predetermined time and then taken out and repeatedly washed with distilled water and anhydrous ethanol until the pH of the eluent was between 7 and 8. Finally, the fibers were dried to a constant weight at  $60-80$  °C for the next desulfurization experiment. This process is considered a complete regeneration process.

In order to better evaluate the regeneration performance of  $PANF<sub>DETA</sub>$ , we used the desorption rate to evaluate the degree of regeneration of the aminated fbers. Considering the presence of HS- in saturated fbers and the fact that the sulfur ion content in the solution cannot be detected by conventional titration means under alkaline conditions. To avoid the volatilization of  $HS<sup>-</sup>$  to  $H<sub>2</sub>S$  under strongly acidic conditions, we frst neutralized the remaining NaOH by adding acetic acid to the lye, adjusted the pH to about 5, and titrated the content of  $S^{2-}$  in the regenerated lye by adding ZnCl<sub>2</sub> dropwise. The amount of ZnCl<sub>2</sub> consumed equals the actual  $S^{2-}$  in the solution. After elution, the fbers were rinsed with deionized water and anhydrous ethanol to thoroughly wash the remaining alkali on the fber surface and dried under vacuum at 60  $\degree$ C for 2 h. Dry the fiber and remove it for subsequent use. The desorption rate is calculated according to Eq. [\(2](#page-4-1)):

<span id="page-4-1"></span>
$$
D = \frac{n_0}{n_1} \times 100\%
$$
 (2)

where  $n_1$  is the amount of H<sub>2</sub>S adsorbed on the fiber and  $n_0$  is the amount of S<sup>2−</sup> obtained by titration in the eluent after desorption.

## **Result and discussion**

#### **Characterization results of PANF**

#### **FTIR spectroscopy**

Figure [2](#page-5-0) shows the infrared spectra of the fbers before and after the modifcation reaction. Compared to the original fiber, the broad peak area at  $3700-3150$  cm<sup>-1</sup> of the aminated fber is signifcantly larger, corresponding to the N–H stretch at the amide bond generated by the reaction between the primary amine group and the cyano group in DETA [\[29](#page-15-21)]. The intensity of the absorption peak at 2240 cm−1 of the aminated fber can be observed to be signifcantly reduced due to the consumption of the cyano group in the reaction but still maintains a certain intensity, indicating that only part of the cyano group is involved in the reaction. Due to the multi-amine structure of DETA, the broad peaks at 1297 cm<sup>-1</sup> and 1553 cm<sup>-1</sup> of the aminated fbers correspond to the N–H bending peaks in the amine group and the N–H bending interactions in  $C-N-H$ , respectively  $[30]$  $[30]$ . In addition, it is not difficult to find an increase in the peak area of the C–N stretching peak at  $1456 \text{ cm}^{-1}$  before and after the reaction, which proves the introduction of the carbon chain in DETA [[31\]](#page-15-23). These results indicate that DETA was successfully grafted onto the PANF substrate through the amination reaction with –CN.

#### **Elements analysis**

The results of elemental fber analysis at each stage are shown in Table [1.](#page-6-0) The carbon content of  $PANF<sub>DETA</sub>$  is significantly lower, and the hydrogen content is higher than the original fber. This is caused by the fact that the carbon content of the

<span id="page-5-0"></span>



<span id="page-6-0"></span>

DETA portion of the fber graft is lower than that of PANF, while the hydrogen content is higher than that of PANF. In addition, the signifcant decrease in nitrogen content also indicates that the modifcation reaction was accompanied by a cross-linking reaction of polyacrylonitrile, which suggests that PANF did undergo the expected chemical reaction with DETA and successfully introduced amines to some extent  $[32]$  $[32]$ . It is noteworthy that the C, H, and N contents of PANF<sub>DETA</sub>-1 and PANF $_{\text{DETA}}$ -10 are essentially the same as those of PANF $_{\text{DETA}}$ . The slight decrease in N and C contents may be due to the shedding of a small number of amine groups during the desulfurization–regeneration process and the adhesion of unwashed NaOH molecules to the fber surface. The decrease of N content is less than 3% compared with fresh fibers after ten times of use, indicating that  $PANF<sub>DFTA</sub>$ is structurally stable. Overall, the elemental analysis results indicate that  $PANF<sub>DFTA</sub>$ is structurally stable and has good reusability.

#### **X‑ray difraction spectroscopy (XRD) analysis**

In polyacrylonitrile fbers, polymer chains are tightly clustered in an irregular helical conformation. Although there is no strict crystalline region, the highly ordered arrangement of polyacrylonitrile molecules allows acrylic fbers to maintain high stability and mechanical strength [\[33\]](#page-15-25). This structural feature is refected in the X-ray powder difraction pattern by the presence of distinct spikes at 2θ angles of 17°, 29.5°, and 37.75° [[34](#page-15-26)]. As seen in Fig. [3,](#page-6-1) the intensity of the characteristic difraction peaks of the aminated acrylic fbers decreased signifcantly,

<span id="page-6-1"></span>



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which indicates that the high-order arrangement of polyacrylonitrile underwent a certain degree of dissolution and destruction by DETA, but still maintained a specifc strength. The XRD patterns of the fbers after desulfurization and regeneration after 1 time and 10 times were not signifcantly diferent from those of the aminated fbers, which proved that the high-order arrangement of the fbers was not further destroyed during the subsequent desulfurization and regeneration process [\[35\]](#page-15-27). The fbers still maintained good mechanical properties, which is signifcant in the practical application of the fbers.

#### **Scanning electron microscope (SEM)**

The surface morphology of the original, modifed, and after-desulfurized fbers under the scanning electron microscope is shown in Fig. [4,](#page-7-0) respectively. There was no signifcant change in the surface of the fbers before and after the reaction. The images of PANF<sub>DETA</sub> fibers obtained at  $1000 \times$  and  $5000 \times$  magnification show a smooth surface with almost no cracks, indicating that the modifed fbers can maintain good stability. Due to the chemical grafting reaction and the expansion of the fibers, the diameter of PANF<sub>DETA</sub> increased significantly compared to the original fbers. The fber diameter increases the contact area between the fber and the adsorbent, which facilitates adsorption [\[36](#page-15-28)]. Fine particles cover the



<span id="page-7-0"></span>**Fig. 4** The SEM images of **a** PANF, **b** PANAF, and **c** PANAF-H2S magnifcations are 100, 1000, and 5000 times

fber's surface after desulfurization due to the interaction with hydrogen sulfde. However, it can be observed that the fber surface remains fat without apparent damage, indicating that the overall structure is well maintained.

#### **Thermogravimetric analysis**

Thermogravimetric spectra were used to study the thermal stability of the fbers. Thermogravimetric spectra were recorded from 30 °C to 800 °C at a heating rate of 10 °C per minute under a nitrogen atmosphere. The results are shown in Fig. [5.](#page-8-0) The original PANF showed almost no mass loss at 300 °C. When the temperature reached 800 °C, the remaining mass was still more than 50%, showing its high thermal stability. As for the functionalized fibers,  $PANF<sub>DETA</sub>$  shows substantial mass loss phases in the temperature range of 100–450 °C, which can be attributed to the evaporation of moisture and volatile residues, the decomposition of the modifed groups on the fber surface, and the gradual destruction of the polyacrylonitrile fber backbone, respectively [\[37](#page-15-29)]. Compared with the original PANF, the thermal stability of  $PANF<sub>DETA</sub>$  decreases significantly. Therefore, in practical applications, the use temperature should be kept within 100  $\degree$ C to maintain the stability of the active components on the fber surface and the backbone structure [[38\]](#page-15-30).

#### **Desulfurization performance study of adsorbent**

#### **Efect of diferent weight gain rates on desulfurization performance**

The higher weight gain rate means more amino groups are grafted on the fber surface. The introduction of amino groups can provide an active site for  $H_2S$  molecules and promote the diffusion of H<sub>2</sub>S molecules inside the fibers [[39\]](#page-15-31). Figure [6](#page-9-0)a and b shows the H<sub>2</sub>S breakthrough curves measured on fibers with different weight gain rates and corresponding sulfur capacity distributions, respectively. For comparison, we also measured the  $H_2S$  breakthrough curves on unmodified PANF. Figure [6a](#page-9-0) shows that the unmodifed PANF sample has the quickest breakthrough time and

<span id="page-8-0"></span>





<span id="page-9-0"></span>**Fig.6 a** Breakthrough curves for fibers with different weight gain rates  $(T = 40^{\circ}C, H_2S$  feed gas = 5300 ppm,  $N_2$  balance, gas flow = 5 ml/min). **b** Sulfur capacity corresponds to fibers with different weight gain rates

the least  $H_2S$  removal capacity, corresponding to an  $H_2S$  breakthrough capacity of just 1.1 mg/g (Fig. [6](#page-9-0)b). The H<sub>2</sub>S removal capacity of the amination-modified fibers increased signifcantly. It showed a volcano-like trend with an increasing weight gain rate. The fiber sample with a  $60\%$  weight gain rate had the highest  $H_2S$  breakthrough capacity of 16.2 mg/g. Notably, the adsorption capacity of the fber for H2S decreased as the weight gain rate continued to increase. This may be due to the continuation of the amination reaction destroying the fber skeleton structure and collapsing the internal pore structure. This not only limits the diffusion of  $H_2S$ molecules inside the fber but also reduces the mechanical strength of the fber. In addition, it is evident from the breakthrough curves that the fber samples with different weight gain rates exhibit similar adsorption behavior. They can all adsorb H2S efficiently at the initial stage to maintain their  $H_2S$  concentration at the tail gas to meet the purifcation index, and then breakthrough occurs rapidly, which implies fast reaction kinetics of  $H_2S$  adsorption by the fibers [[40\]](#page-15-32).

### **Efect of diferent temperatures on desulfurization performance**

The reaction temperature infuences the adsorption of gas molecules on the catalyst surface and the chemical reaction. At lower temperatures, the outside world cannot provide enough activation energy for the chemical reaction to proceed efectively, and the chemisorption efect is poor. Too high a temperature generates a lot of energy consumption and wastes resources [\[41](#page-15-33)]. The efect of temperature on the performance of fber adsorbent desulfurization is shown in Fig. [7](#page-10-0). With increasing temperature, the corresponding permeation time increases slightly, suggesting that the increase in temperature facilitates this adsorption process. At 20 °C, the fbers have the lowest purification time of 175 min. At 50  $\degree$ C, this value reaches a maximum of 201 min. Increasing the reaction temperature enhances the mass transfer and increases the chemical reaction rate, which is more favorable for the rapid binding

<span id="page-10-0"></span>

of H2S to the functional groups on the fber surface. Temperature increase can promote the chemisorption process but not the physical adsorption process, which, to some extent, also indicates that the adsorption of  $H<sub>2</sub>S$  by fibers is mainly chemisorption [[37\]](#page-15-29). Continuing to increase the temperature, the fbers' purifcation capacity decreased at 60 °C. This may be because the increase in reaction rate reduces the time that  $H<sub>2</sub>S$  molecules can effectively contact the surface-active sites, leading to a decrease in fber purifcation capacity. Since the fbers exhibited a breakthrough time of 201 min at both 40 °C and 50 °C, 40 °C was considered the optimal reaction temperature considering energy saving and milder reaction conditions.

 $\overline{50}$ 

100

Time(min)

150

200

### **Efect of moisture on desulfurization performance**

Since the aminated fbers have good water absorption and some moisture is inevitably and commonly incorporated in the actual industrial gas stream, it is necessary to study the effect of moisture on  $H_2S$  removal  $[42]$  $[42]$ . Figure [8](#page-10-1) compares breakthrough

<span id="page-10-1"></span>**Fig.8** Breakthrough curves for fbers with diferent Moisture content.  $(T=40. °C, H<sub>2</sub>S$  feed  $gas = 5300$  ppm, N<sub>2</sub> balance, gas  $flow = 5$  ml/min)



curves of wet and dry fibers under an  $H_2S$  gas mixture. The figure shows that the breakthrough time for  $H_2S$  in dry gas is 160 min. In the presence of moisture, the corresponding breakthrough time for the fber adsorbent under wetting is 201 min. This is mainly because the reaction between  $H<sub>2</sub>S$  and the active sites on the fiber surface is a gas-solid reaction, and it is difficult for the two to contact and interact with each other fully. The moisture entry can form a water film on the fiber surface, which directly enhances the gas–solid mass transfer and promotes the ionization of H<sub>2</sub>S into HS<sup>−</sup>. It has been shown that the affinity between the charged HS<sup>−</sup> and the active site is more potent than between the gaseous  $H_2S$ . On the other hand, water can promote the swelling of fibers, which makes  $H_2S$  molecules diffuse quickly into the fibers, and this also promotes the adsorption of  $H_2S[43]$  $H_2S[43]$  $H_2S[43]$ .

#### **Regeneration performance study of adsorbent**

### **Efect of sodium hydroxide concentration and soaking time on regeneration performance**

During the regeneration process, the  $H_2S$  molecules adsorbed on the fibers are eluted by reacting with sodium hydroxide to form  $Na<sub>2</sub>S$  or NaHS. Theoretically, the grafted amino groups on the fber surface will be restored to their initial state, restoring the sulfur capacity. However, in actual use, the grafted amino groups on the fber surface may fall off, decreasing desulfurization performance. On the other hand, since polyacrylonitrile fbers are not resistant to an alkaline environment, improper control in an alkaline environment, such as too high a concentration of alkali and too long contact time, will cause damage to the –CN functional group structure on the fiber backbone<sup>[[44\]](#page-15-36)</sup>. To ensure the reusability of fibers, it is necessary to investigate the efect of sodium hydroxide concentration and soak time on regeneration performance. The efects of diferent lye concentrations on fber regeneration capacity are



<span id="page-11-0"></span>**Fig.9 a** Effect of lye concentration on fiber regeneration performance( $T = 40^\circ$ C, lye concentration=0.8 mol/l). **b** Effect of immersion time on fiber regeneration performance (T=40 °C, immersion time=5 min)

shown in Fig. [9a](#page-11-0). Similar to the trend of immersion time, the higher the lye concentration, the better the fber regeneration per unit of time. When the lye concentration was increased to 15 mol/L, the fber sulfur capacity showed a relatively signifcant decrease, which indicated that the high lye concentration had already caused damage to the fber frame structure. In order to minimize the damage of the lye to the fiber structure, the optimal soaking lye concentration for  $0.5$  g saturated fiber was chosen as 0.8 mol/L. On this basis, Fig. [9b](#page-11-0) shows the efect of soaking time on fber regeneration performance. It is not difcult to fnd that the desulfurization capacity of the regenerated fbers is signifcantly lower than that of the fresh fbers when the soaking time is less than 5 min. When the soaking time was between 5 and 20 min, the regenerated fbers regained their frst desulfurization capacity, indicating that the fbers had been regenerated. As the soaking time continued to be extended, the sulfur capacity of the regenerated fbers showed a decreasing trend, indicating that the lye had eroded the fbers and caused damage to the fber structure. In order to obtain better desulfurization performance and minimize the regeneration time, the optimal soaking time for 0.5 g saturated fber should be 5 min. In addition, the changes in the desorption rate of  $H_2S$  on the fiber by the lye showed the same trend for diferent lye concentrations and soaking times. The desorption rate increased with the increase in soaking time and lye concentration. When the lye concentration reached 0.8 mol/L and the soaking time reached 5 min, the desorption rate no longer increased by increasing the concentration or extending the time, indicating that the H2S adsorbed on the fber had been fully eluted. In summary, we chose 0.5 g of fber placed in 0.8 mol/L alkali soaking for about 5 min as the best regeneration operating conditions.

#### **Efect of the number of cycles on the regeneration performance**

Ten desulfurization–regeneration experiments were carried out using 0.8 mol/L sodium hydroxide solution as the desorption agent, and the results are shown in Fig. [10.](#page-12-0) The adsorption capacity of the aminated fbers gradually decreased with the increase of the number of uses, which may be due to the adsorption sites  $(-NH -/-NH<sub>2</sub>)$  groups) on the fiber surface being shed during the use

<span id="page-12-0"></span>



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or regeneration process[\[45\]](#page-15-37). It is noteworthy that after ten cycles of the adsorption–desorption process,  $\text{PANF}_{\text{DETA}}$  was still able to maintain the desorption rate of  $H_2S$  at about 90%, which indicates the cause of the decrease in sulfur capacity is not due to incomplete regeneration but to the structural damage of the fiber itself. The sulfur capacity of  $PANF<sub>DETA</sub>$  after ten cycles of adsorption and desorption is still 13.6 mg  $g^{-1}$ , 83.9% of the initial adsorption capacity. This is unquestionably excellent. Based on the above results, we believe that  $PANF<sub>DFTA</sub>$ has excellent regeneration performance, which is favorable for its practical application.

#### **Mechanism**

A possible mechanism of adsorption and desorption occurring on the fber surface was proposed in conjunction with the experimental phenomena, as shown in Fig. [11](#page-13-0). The introduction of amine groups on the fber surface provides many bindable alkaline sites for hydrogen sulfde or sulfur hydride, which plays a crucial role in enhancing the sulfur capacity. The acid–base reaction between the two and the physical adsorption by the pore structure of the fber itself is the fundamental reason for the ability of the fiber to adsorb  $H_2S$ . The process is chemisorption, so an appropriate increase in temperature facilitates the adsorption process. Similarly, moisture can promote the ionization of hydrogen sulfde, and the afnity between the charged sulfur hydrogen root and the amine group is more potent [\[46\]](#page-15-38), so the presence of moisture can facilitate the adsorption reaction. The following reactions will occur in the solution during the lye immersion [[47\]](#page-15-39).

$$
R - NH3+HS- + NaOH = R - NH2 + H2O + NaHS
$$
 (3)

$$
NaHS + NaOH = Na2S + H2O
$$
 (4)

$$
R - NH_3^+HS^- + Na_2S = R - NH_2 + 2NaHS
$$
 (5)



<span id="page-13-0"></span>Fig.11 Possible adsorption and desorption reactions on the fiber's surface

The lye can effectively elute the HS<sup>−</sup> immobilized on the fiber surface, and the amine group is restored to its original state to achieve regeneration.

## **Conclusion**

In this work, aminated polyacrylonitrile was synthesized directly from commercially available polyacrylonitrile fbers to remove hydrogen sulfde from natural gas at ambient temperature. Desulfurization experiments were used to study the adsorption behavior of PANF $_{\text{DETA}}$  under different conditions on H<sub>2</sub>S. In addition, we focused on the excellent regenerative properties of fbers as desulfurizer substrate materials to evaluate their potential as desulfurizer matrix materials. The results showed that the sulfur capacity of the aminated fber increased by as much as 15 times compared to the pure fber. Surprisingly, after ten cycles of continuous desulfurization–regeneration under optimal regeneration conditions, the aminated fbers still maintained 83.9% of the sulfur capacity level of the fresh sample. The alkali solution could effectively elute the adsorbed  $H_2S$  molecules from the fibers during this process. The relevant characterization results of the samples also confrm this to some extent. These results of our study suggest that polyacrylonitrile may be a suitable substrate material for desulfurizers, which will provide new ideas for removing hydrogen sulfde from natural gas at room temperatures. Based on this, our future research will focus on further enhancing the adsorption capacity.

**Author contributions** ZL and KQ conceived the presented idea. ZL undertook the bulk of the experiments and completed the manuscript. YW, JP, SC, and XS participated in the experiment. Sun Gang and Ma Yue helped us with our experiments outside of school. KQ supervised the fndings of this work. All authors discussed the results and contributed to the fnal manuscript.

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**Availability of data and materials** All data generated or analyzed during this study are included in this published article.

#### **Declarations**

**Confict of interests** The authors declare that there is no competing fnancial or non-fnancial interest that could have appeared to infuence the work reported here.

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