

A sustainable approach for the removal of toxic 4-nitrophenol in the presence of H_2O_2 using visible light active Bi_2MoO_6 nanomaterial synthesized via continuous flow method

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Abstract

In the present study, a visible-light active nanosized Bi₂MoO₆ was prepared by a continuous flow method. The synthesized nanomaterials were characterized by powder X-ray diffraction (PXRD), scanning electron microscope (SEM) coupled with energy dispersive spectroscopy (EDS), UV-visible analysis, Fourier transform infrared spectroscopy (FTIR), and zero-point charge (pH_{ZPC}). The band gap energy of the photocatalyst was found to be 2.81 eV, which shows it is a visible light active material. The prepared catalyst was applied for the photocatalytic degradation of a harmful organic pollutant, 4-Nitrophenol (4-NP), under the irradiation of visible light, and its photodegradation was enhanced by hydrogen peroxide. Furthermore, photo-degradation efficiency was optimized by a statistical method, considering critical process parameters such as concentration of 4-NP, pH, temperature, catalyst loading, and time. The maximum photocatalytic activity was achieved when experimental parameters such as pH were maintained at about 7.0 and catalyst dosage, H₂O₂ concentration, and 4-NP concentration were 1 g/L, 0.025 mol/L, and 10 mg/L, respectively, at 35 °C. The maximum photodegradation was 93% and it was majorly governed by the participation of the OH⁻ radical. The pseudo-first order reaction kinetics was evaluated and fitted for the degradation of 4-NP. Furthermore, a possible mechanism based on the generation of electron holes for 4-NP degradation has also been proposed in the present work. This method is found to be efficient, environmentally friendly, and free of toxic materials.

Keywords Bismuth molybdate \cdot Photocatalysis \cdot 4-NP \cdot Degradation \cdot Statistical analysis

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Introduction

In the past few years, our water resources have been contaminated to a greater extent due to discharges of untreated effluents from different industries. A large number of organic pollutants are released by these effluents, which threaten the supply of potable water. 4-NP is among the most abundantly found organic pollutants in water as it is utilized in numerous intermediate industrial processes [1]. 4-NP is a benzene derivative and is formed by the connection of hydroxyl and nitro groups with the benzene ring, which is called para-nitrophenol. These compounds are used in dyes, drugs, pesticides, polymers, plasticizers, and explosives [2], and they are highly toxic and carcinogenic in nature. The permissible limit of such benzene derivatives in potable water is determined to be 0.5 ppb and 0.5 to 1.0 ppm in wastewater discharge [3]. A higher tendency of 4-NP to make derivatives leads to the formation of compounds like 4-chloronitrophenol, which is even more toxic and biodegradation resistant [4]. 4-NP is a basic key raw material for nitroaromatic derivatives and is used in the commercial production of paracetamol, also called acetaminophen, and in the production of pesticides such as methyl-parathion and parathion [5]. In the water discharge, these pesticides are also considered to be a major source of 4-NP detected in the environment since they can be converted to 4-NP under the action of hydrolase [6]. 4-NP is considered a persistent toxic pollutant [7, 8] and its toxicology and carcinogenicity have been studied [9, 10], and the acute toxicity of 4-NP leads to blood disorders, chromosomal abnormalities, feeling sleepy, and cyanosis [11, 12].

As a result, 4-NP is listed as a priority pollutant by regulatory bodies. Hence, removal of 4-NP from wastewater is an urgent need before being discharged into the environment. In the same direction, numerous methods have been reported by researchers for 4-NP degradation viz., bio-degradation [13], advance oxidation process (AOP) [14, 15], chemical redox [16, 17], heterogeneous photo-catalysis [18, 19], adsorption techniques [20], sonolysis [21] and Fenton chemistry [16, 22].

Due to their electronic structure, metal oxide semiconductors such as ferric oxide (Fe₂O₃), titanium oxide (TiO₂), zinc oxide (ZnO), oxides of bismuth such as BiOBr, BiVO₄, BiWO₆, Bi₂O₃, sulphide of cadmium sulphide (CdS), zinc sulphide (ZnS), Sr₂Nb₂O₇, and Bi₂MoO₆ can act as sensitizers for light-reduced redox reactions [23, 24, 25]. Due to its potential for degrading organic and inorganic contaminants through a process known as heterogeneous photocatalysis, semiconductor- based photocatalysis has attracted a great deal of interest in recent times [26]. It is based on the generation of electron–hole pairs when a semiconductor is photo-illuminated with energy more than its energy gap. The reactive radicals produced by the charged species as they migrate to the semiconductor's surface begin redox reactions with the organics [27]. Heterogenous photocatalysis has been proven to be an efficient treatment method for the detoxification of phenolic substances. These semiconductor photocatalysts transform photon energy into chemical energy, and they have a lot of potential in the treatment of wastewater because they totally eliminate the contaminant rather than converting it into

another phase [28]. TiO_2 and bismuth molybdate have been the most considered photocatalysts in recent past due to their unique potential for water decontamination [29, 30].

The visible region accounts for the majority of solar light that reaches the earth's surface, but band gap of TiO₂ 3.2 eV makes it unsuitable for use in this region of sunlight. Hence, efforts have been made to develop an alternative to TiO₂ and Bismuth molybdates, among which is being determined to have excellent efficiency in solar light mediated systems and has been shown to be capable of water splitting and environmental sanitization [31]. Oxides of bismuth have high oxide ion conductivity and electrocatalytic activity to inter-convert molecular and ionic oxygen at low temperatures; hence, they are found to be potentially important for the generation of oxygen [32]. A smaller band gap of 2.5–2.8 eV is responsible for its activity under visible light (420–500 nm) to degrade organic pollutants and the splitting of water [33, 34]. The fast and shortest synthesis of Bi₂MoO₆ (koechlinite) and Bi₂MoO₆ and synthesis of bismuth molybdate, which is done by a continuous flow method in a custom-designed tubular flow reactor and has a higher capability for large-scale production.

In the present study, the synthesis of visible light active nanosized bismuth molybdate photocatalyst was conducted using a continuous flow method, which makes it preferable for use in organic pollutants' decontamination under the illumination of solar light at low cost. The evaluation of the synthesized material has been carried out for the photocatalytic mineralization of 4-NP under the irradiation of visible light. Moreover, factors affecting the efficiency of degradation of 4-NP have also been studied, and the best-optimized condition has been explored for maximum degradation with the bestfitted model and factor range. The catalyst Bi_2MoO_6 was found to be more efficient and effective for the mineralization of very toxic 4-NP in aqueous solution.

Material and methods

Materials

All the raw materials used in the present work were of AR grade and were used without any further purification. The chemicals such as bismuth nitrate $(Bi(NO_3)_3 \cdot 5H_2O)$, ammonium molybdate $((NH_4)_6Mo_7O_{24} \cdot 4H_2O)$, Nitric acid (HNO_3) , hydrochloric acid (HCl), sodium hydroxide (NaOH), 4-NP $(C_6H_5NO_3H)$ and hydrogen peroxide (H_2O_2) used for the synthesis of photocatalyst were procured from Thermo Fisher Scientific.

Synthesis of nanosized Bi₂MoO₆ photocatalyst

Synthesis of the catalyst was done as per our previously reported continuous flow method [36] with minor modification. Aqueous solutions of bismuth precursor (0.2 mol Bi(NO₃)₃·5H₂O in 200 ml of 2 M nitric acid) (via pump 1) and an aqueous solution of molybdate precursor (0.2 mol (NH₄)₆Mo₇O₂₄·4H₂O) in 400 ml of 2 M

aqueous NaOH) (via pump 2) were pumped with T mixture fed in preheated (at 210 °C, Zone-1, and pressure of 6–10 bar) in a custom-designed coil flow reactor and pH was maintained ~5–6. The process produces particle continuous flow to the cooling zone (at 50 °C, Zone-2, and pressure 6–10 bar) and the obtained slurry is continuously collected in a beaker from the exit of the back-pressure regulator. The collected slurry was centrifuged and the separated particles were washed with water and followed by ethanol, further dried in a hot air oven, and ground into a fine powder for further use.

Characterization

The SEM analysis was carried out by JSM 4490 JEOL, Japan, equipped with EDS. FTIR (NICOLET 6700) made by Thermo Fisher Scientific, U.S.A. was used to analyse the presence of functional groups on the surface of materials. The crystalline nature of the catalyst was analysed by XRD using D8 Advance Eco (Bruker, Germany), and the pH_{ZPC} of the catalyst was determined by the pH drift method as described in previous literature [37]. The UV–visible spectrum scanning was done using a UV–visible spectrophotometer (117 Systemics, India Limited).

Photocatalytic degradation

The photocatalytic degradation experiments were carried out in a 250 mL beaker inside a wooden chamber. A tungsten lamp was used as the source of visible light, with a radiation of 500 Lux on the surface of the reaction mixture. For degradation experiments, a 100 mL volume of 10 mg/L 4-NP was taken in the beaker and a determined amount of catalyst and H_2O_2 were added to it. It was stirred on the magnetic stirrer at 100 RPM inside the wooden chamber. The shaking was performed first in the dark for 30 min to check the amount of 4-NP removed by adsorption and then in the irradiation of visible light for 120 min. A 3 mL aliquot was withdrawn at different time intervals from the reaction mixture to determine the remaining concentration of the 4-NP after separation of the catalyst by centrifugation. The concentration of the 4-NP was analysed using a UV–Visible spectrophotometer at 317 nm. The percentage degradation was calculated as shown below in Eq. 1:

$$\% Degradation = \frac{C_0 - C_t}{C_0} \times 100 \tag{1}$$

Here, C_0 and C_t represents the concentration of 4-NP initially and after degradation, respectively. The degradation process was optimized by varying different operating conditions like catalyst concentration, H_2O_2 concentration, pH, initial pollutant concentration, reaction time, and temperature.

Results and discussion

Characterization of the catalyst

The morphological features of the synthesized Bi_2MoO_6 were analyzed by SEM, which are shown in Fig. 1a. The particles appear as aggregates with irregular shapes, and the size of some separate particles is less than 100 nm. The SEM analysis of the Bi_2MoO_6 after its application in the photocatalytic degradation process is shown in Fig. 1b, which also shows particles with irregular shapes. However, most of the particles after photocatalysis were observed to be of similar size, unlike before photocatalysis. The EDS analysis shows that the elemental composition of the catalyst was Bi, Mo, and O (Fig. 1c). The weight percentage of the elements is shown in Fig. 1c.

The UV–Visible analysis of the Bi_2MoO_6 was done in the range of 350 to 550 nm and the results are represented in Fig. 1d. The catalyst absorbed the spectrum in the visible range, which means that the catalyst is visible light active.

The steep shape spectra suggest absorption occurred due to a band gap transition [38]. The binding energy of the Bi_2MoO_6 was calculated from the Tauc's plot, which is represented in inset Fig. 1d. It was calculated to be 2.81 less than the conventionally used photocatalyst TiO₂ [39].



Fig. 1 a and b SEM analysis of Bi_2MoO_6 before and after photocatalysis, c EDS analysis and d UV-visible analysis (with Tauc's plot inset) of Bi_2MoO_6

The XRD analysis shows sharp peaks, which correspond to the crystalline nature of the catalyst (Fig. 2a). The peaks observed at $2\theta = 28.5^{\circ}$ are attributed to the characteristic peak of Bi₂MoO₆ representing crystal plane 131 [40, 41]. Other peaks which were observed at positions $2\theta = 11.5^{\circ}$, 23.69° , 33.3° , 36.0° , 38.6° , 39.91° , 46.7°, 47.33°, 55.5° and 58.4° corresponding to (060), (131), (222), (151), (400), (240)/(042), (202), (202), (331)/(133) and (262) planes of Bi₂MoO₆ (JC-PDS file 21-0102) [42, 43, 44, 45, 46]. The XRD pattern also shows minor impurities of bismuth and molybdate oxides, peaks presents at $2\theta = 25.8^{\circ}$, 27.4° attributed to γ -Bi₂O₃ [47, 48] and peak at $2\theta = 49.06^{\circ}$ is attributed to MoO₃ [49]. Results of FTIR analysis of Bi₂MoO₆ before and after photocatalysis of 4-NP are depicted in Fig. 2b. The spectrum was scanned in the range of 4000 to 400 cm⁻¹ and shows a major peak at 3390 cm⁻¹, which corresponds to the vibrations in –OH bonds. This bond on the surface may appear due to the formation of hydroxides on exposure to the ambient environment or adsorption of water molecules. The peaks observed at wavelengths of 738 and 830 cm⁻¹ correspond to the stretching of the Mo-O bond, asymmetric and symmetric, respectively, [50]. And a peak near 530 cm⁻¹ represents the stretch in the Bi-O and Bi-O-Bi bonds [51]. The FTIR analysis of Bi₂MoO₆ after photocatalysis shows similar peaks, but the intensity of the peaks has changed. A new peak at ~ 3000 cm⁻¹ appeared after photocatalysis corresponding to the C-H stretch [52]. The appearance of new peaks and changes in peak intensities may be caused by surface bond deformation caused by the adsorption of pollutants and degradation



Fig. 2 a XRD analysis, b FTIR analysis and c $\rm pH_{ZPC}$ analysis of $\rm Bi_2MoO_6$

products molecules on the catalyst's surface. The plot for pH_{ZPC} is shown in Fig. 2c, and the value of pH_{ZPC} was found to be 4.5.

Photocatalytic degradation of 4-NP

Control experiments

Prior to degradation experiments, six control experiments were run to confirm photocatalytic degradation of 10 mg/L 4-NP for 4 h at pH 7 and temperature 25 °C. Control 1 and 2 were run with Bi_2MoO_6 (BM) only under dark and under visible light irradiation (UVI). Controls 3 and 4 were run with H_2O_2 only, under the dark and under UVI, and controls 5 and 6 were run using BM in combination with H_2O_2 under the dark and under UVI. Results are expressed in Fig. 3a, control 1, 3, 4, and 5 showed a removal % of 4-NP < 10%. Maximum removal % was found in control 6 which was run with $BM + H_2O_2$ under UVI (93.8 ± 0.10) followed by control 2 (34.66±0.26) which was run under UVI using BM only. The result shows that the effective removal of 4-NP was achieved under UVI using $BM + H_2O_2$ and BM only,



Fig. 3 a Control experiments ($C_0 = 10 \text{ mg/L}$, Photocatalyst = 1 g/L, H_2O_2 concentration = 0.025 M, pH 7, Temperature = 25 °C), b Effect of photocatalyst amount ($C_0 = 10 \text{ mg/L}$, H_2O_2 concentration = 0.025 M, pH 7, Temperature = 25 °C), c effect of H_2O_2 concentration (Photocatalyst = 1 g/L, $C_0 = 10 \text{ mg/L}$, pH 7, Temperature = 25 °C) and d effect of pH (Photocatalyst = 1 g/L, $C_0 = 10 \text{ mg/L}$, H_2O_2 concentration = 0.05 M, Temperature = 25 °C)

representing that the removal of 4-NP was resulted by photocatalytic degradation by BM under UVI only and the degradation % was enhanced by the addition of H₂O₂.

Effect of photocatalyst concentration

The effect of photocatalyst concentration on the degradation of 4-NP was studied in the range of 1.0 g/L to 2.0 g/L with a 10 mg/L initial concentration of 4-NP at pH 7. Fig. 3a shows that the degradation of the 4-NP was increased with increasing the concentration of photocatalyst from 1.0 to 2.0 g/L due to an increase in active sites for the generation of reactive species [53]. Similarly, Fahoul et al. [54] also observed an increase in photocatalytic degradation of acid red 1 by increasing the concentration of photocatalyst from 0.5 to 1.5 g/L due to an increase in active sites. However, a further increase in catalyst concentration up to 2.0 g/L resulted in less degradation. A lesser degradation percentage on further increasing the catalyst concentration may result due to the agglomeration of the catalyst particles due to which active sites in opacity of the solution, which reduces the penetration of photons to the catalyst [55, 56, 57]. For the rest of the study, a 1.0 g/L concentration of catalyst was used.

Effect of H₂O₂ concentration

 H_2O_2 acts as an electron acceptor, increasing the generation of reactive species (OH) in the photocatalytic system. The concentration of H_2O_2 below or above the optimum concentration negatively affects the degradation process. The lower concentration of H_2O_2 generates an insufficient number of OH radicals, while the higher concentration of H_2O_2 generates an excessive number of OH radicals, which get destroyed by their collision with each other or H_2O_2 molecules [58, 59]. Therefore, the optimization of H_2O_2 concentration is required. In the present work, the effect of H_2O_2 concentration was studied in the range of 0.01 to 0.1 M (Fig. 3b), with an initial 4-NP concentration of 10 mg/L and pH 7. Hence, 0.05 M H_2O_2 was found to be optimum for the degradation of 4-NP and it was selected for further experiments.

Effect of pH

Operating pH is also an important factor in the catalytic degradation process it influences the charge on catalyst surface and degree of ionization of pollutant molecules [21]. The pH effect was studied by degrading 4-NP at pH 3, 5, 7 and 10 with 10 mg/L concentration of 4-NP. The degradation percentage was found to be increased with increasing pH. Maximum degradation was found at pH 5 and 7 while minimum 4-NP degradation was found at pH 3 (Fig. 3c). At pH 10 also the removal percentage was reduced slightly. Hence the Bi_2MoO_6 catalyst synthesized in this work was active for the degradation of 4-NP.

Effect of 4-NP concentration

The initial concentration of 4-NP was increased from 10 to 50 mg/L as shown in Fig. 4a. The degradation percentage was found to decrease with increasing its concentration. A maximum of 93.84 ($\pm 0.105\%$) degradation was achieved at 10 mg/L and the minimum degradation was found to be 78.59 ($\pm 0.389\%$) at 50 mg/L. However, the degradation percentage at 20 mg/L (92.26 $\pm 0.237\%$) and 30 mg/L (87.69 $\pm 2.107\%$) decreased slightly. The number of OH radicals generated in the degradation reaction is fixed when the catalyst and H₂O₂ concentration is fixed, and when the initial concentration of the pollutant is increased, the number of molecules to be degraded exceeds the number of OH radicals, so the degradation percentage decreases [60].



Fig. 4 a Effect of initial 4-NP concentration (Photocatalyst=1 g/L, pH 7, H₂O₂ concentration=0.05 M, Temperature=25 °C) and **b** effect of temperature on the degradation of 4-NP (Photocatalys t=1 g/L, pH 7, H₂O₂ concentration=0.05 M, C₀=10 mg/L)

Effect of reaction time

The reaction time was studied along with the study of the initial 4-NP concentration effect. The reaction time was increased from 15 to 120 min (Fig. 4a). The degradation percentage increased with increasing reaction time. The rate of increase was higher at the initial time up to 60 min, while beyond 60 min, the rate of degradation percentage increased slowly (Fig. 4a). On an increase in reaction time, more radicals are produced, which degrade a greater number of pollutants. At the initial time, the maximum amount of H_2O_2 reacts with the vacant surface of the catalyst and produces the maximum number of OH radicals. Hence, the degradation rate was observed to be faster in the initial time, while after some time of reaction, the catalyst surface is covered by the adsorbed pollutant or degradation products, which reduces the generation of OH radicals. Furthermore, after 60 min, more than half of the pollutants and H_2O_2 reacted, leading to a decrease in their concentration in the reaction mixture due to their interaction with the catalyst, which may also cause a decrease in degradation [61].

Effect of temperature

The increase in operating temperature from 25 to 45 °C led to a slight decrease in the degradation process, and the decrease was further increased at 55 °C (Fig. 4b). The reduction in degradation percentage at higher temperatures reveals that the degradation of 4-NP by Bi_2MoO_6 was exothermic in nature and an external input of temperature adversely affected the degradation process. It might be due to the decomposition of H_2O_2 molecules at higher temperatures, which reduces the generation of OH radicals [62].

Degradation kinetics

The nonlinear least-squares analysis is more effective method for fitting data to kinetics in comparison to the linearized formulas. The kinetic data of 4-NP degradation was analyzed by least-square non-linear fits of pseudo-first order and pseudo-second order. The expressions for pseudo-first order and pseudo-second order kinetics are represented below in Eqs. 2 and 3 [34]:

$$C = C_0 \times \exp(-k_1 \times t) \tag{2}$$

$$C = C_0 / (1 + C_{0x} k_2 t)$$
(3)

Here C_0 is the initial and C is the residual 4-NP concentration, and k_1 and k_2 are pseudo-first order and pseudo-second order rate constants, respectively.

Fig. 5a and b, show plots for pseudo-first order and pseudo-second order kinetics. The value of k_1 was 0.02 (±0.003 min) and value of k_2 was 0.0044 (±0.0001) L/mol/min. The degradation data of 4-NP was fitted best with pseudo-second



Fig. 5 a and b Plot for pseudo-first order and pseudo-second order kinetics, (Photocatalyst = 1 g/L, pH 7, $C_0 = 10 \text{ mg/L}$, H_2O_2 concentration = 0.05 M, Temperature = 25 °C), c effect of different capturing agents and d Regeneration of catalyst

order kinetics with value of $R^2 = 0.9908$, while the value of R^2 for pseudo-first order was found to be 0.9900.

Capture of active species for the confirmation of photocatalysis

The photocatalytic process involves the generation of various active species such as hydroxyl radical (OH), superoxide radical (O_2^{-}), electron hole (h^+), and free electron (e^-) by the interaction of the photocatalyst with light. These active species react with toxic organic pollutants and convert them into simpler, non-toxic forms and mineralize them ultimately. To assess the participation of these active species in the degradation process of 4-NP, different scavenging agents were added to the reaction. As a scavenging or capturing agent for OH isopropyl alcohol (IPA), for O_2^- p-benzoquinone (PBQ), for h^+ sodium oxalate (SO), and for e^- sodium sulfate (SS) was used [63, 64], and the concentration of all scavenging agents was 1 mM. Fig. 5c shows the results of the present study.

The degradation percentage was decreased most in the presence of IPA, followed by PBQ. The result indicates that the 4-NP degradation was mostly governed by the participation of OH radicals, which may occur due to the addition of H_2O_2 in the reaction mixture, which enhances the generation of OH radicals. The

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Catalyst	Degradation method	Removal %	References
Modified graphite felt	Electro-Fenton process	78.7% in 20 min	[65]
Hybrid montmorillonite-alginate beads	Photo-Fenton degradation	75% 40 min	[99]
Natural limonite	Electro-Fenton	96% in 6 h	[67]
FeSO_4	Ultrasound assisted advanced Fenton process	66.4% in 1.5 h	[22]
Iron doped TiO ₂ nanoparticles	Visible light driven photocatalytic degradation	92% in 5 h	[68]
Bi_2MoO_6	Visible light driven photocatalytic degradation	93.84±0.105% in 4 h	Present work

Table 1 4-NP degradation efficiency of ${\rm Bi}_2{\rm MoO}_6$ in comparison with some previous reported catalysts

degradation of 4-NP was found to be successful via the photocatalytic degradation by the synthesized Bi_2MoO_6 catalyst. A comparison of the 4-NP degradation of Bi_2MoO_6 was compared with some previously prepared catalysts, shown in Table 1, and the efficiency of Bi_2MoO_6 was found to be better.

Regeneration of the catalyst

The regeneration ability of the catalyst is an essential factor to make its application practical. Fig. 5d shows the regeneration of the synthesized Bi_2MoO_6 catalyst, the degradation efficiency of the catalyst was very less affected by the regeneration up to five cycles. Maximum degradation was found in first cycle 93.84 \pm 0.105%, while, the lowest degradation percentage was found in fifth cycle 85.62 \pm 0.183. A higher degradation efficiency of the catalyst even after five regeneration cycle represents that the catalyst was stable and retained its catalytic efficiency after five cycles.

Degradation mechanism

The photocatalytic degradation of phenol by bismuth molybdate photocatalyst (P) takes place by the adsorption of light having energy more than the band gap energy of photocatalyst (2.8 eV). On the adsorption of light there is a simultaneous generation of electron and hole pair, the generated electron at conduction band is taken up by molecular oxygen to form superoxide radicals (O_2^{--}). Whereas, the electron holes generated on valence band react with H_2O_2 or water molecules or hydroxyl ion to form hydroxyl radicals (OH). Both OH and O_2^{--} are highly reactive radicals and can participate in the degradation mechanism by attacking the phenol molecules. The reactions that take place in the degradation are discussed below in Eqs. 4–7:

$$P + hv \to P(e_{cb}^{-}) + P(h_{vb}^{+}) \tag{4}$$

$$P(h_{\nu b}^{+}) + H_2 O \to^{\circ} OH + H^{+} + P$$
(5)

$$P(e_{cb}^{-}) + O_2 \to O_2^{\circ -} + P \tag{6}$$

$$OH^{-}/O_{2}^{-} + Phenol \rightarrow intermediate \ compounds \rightarrow CO_{2} + H_{2}O$$
 (7)

As discussed above in capture of active species the degradation of phenol was mainly driven by generation of OH radicals, followed by electron holes and O_2^{-1} radicals. The higher influence of OH radicals in the degradation of phenol was resulted due to addition of H_2O_2 which is good oxidizing agent and source of OH radicals as well. Upon catalytic decomposition one H_2O_2 molecule to two OH radicals take place. A proposed mechanism has been shown in Fig. 6.



Fig. 6 Proposed mechanism for the degradation of phenol using bismuth molybdate catalyst

Conclusion

The present study concludes a successful synthesis of a visible light active photocatalyst via the continuous flow method. The catalyst synthesized was nanosized and crystalline in nature. It had good efficiencies for the degradation of 4-NP in aqueous solution. The optimum conditions for the degradation were found as catalyst concentration of 1 g/L, H₂O₂ concentration of 0.05 M, pH 5-7, initial 4-NP concentration of 10 and 20 mg/L, irradiation time of 120 min, and temperature of 25 °C. The degradation reaction was exothermic and was best followed by a pseudo-first order kinetic model. The use of various scavengers to capture active species revealed that the degradation was governed by OH radicals. The continuous flow synthesis method allows the mass production of nanomaterials with controllable process parameters, which saves time and overall energy input in comparison with the batch mode synthesis process. Furthermore, the degradation process carried out in this was visible light active, which ensures the use of renewable and infinite sources of light, i.e., the Sun, which further reduces the adverse environmental impacts of the remediation process and makes it affordable and scalable. In the combination of both these features, this study is a sustainable approach for the remediation of toxic water pollutants.

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Declarations

Conflict of interest The authors declare that they have no conflict of interests.

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