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Green preparation of Pd nanoparticles on SBA-15 via supercritical fluid deposition and application on Suzuki–Miyaura cross-coupling reaction

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Abstract A well-dispersed green Pd/SBA-15 catalyst with an average size of 13.7 nm and 492.6 m^2/g BET surface area is prepared via supercritical fluid deposition method with a new bipyridyl precursor that enables reduction at mild conditions at 80 °C and 17.2 MPa. The catalytic performance of Pd/SBA-15 prepared using $\sec{CO_2}$ with hydrogen reduction was assessed for Suzuki–Miyaura coupling reaction of bromobenzene and phenylboronic acid that was chosen as a model coupling reaction. The catalyst was tested in six different solutions and in three organic and inorganic bases during reactions. In general, the effect of bases is investigated when solvents are held constant and K_2CO_3 appears to have the best results in the activity studies used. For each of the 3 bases used, the highest catalytic activity was reached as the result of the solvent system being ethanol/water (1:1). The highest catalytic conversion was obtained in the ethanol- $K₂CO₃$ solvent-base pair. The catalyst synthesized in this study exhibited high activities and TON value was found as 160.8 at room temperature.

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Introduction

Green methods are more preferred in industrially important reactions due to the environmental concerns and thanks to developments in green chemistry. Especially in organic synthesis, alternative green processes can be eco-friendly and reduce costs (Beckman [2004](#page-10-0)). In this sense, the use of supercritical solvents instead of conventional organic solvents is an effective approach. The most commonly used green solvents for alternative in organic synthesis are supercritical carbon dioxide, supercritical, and subcritical water (Gang et al. [2003;](#page-10-0) Ulusal et al. 2015). Supercritical carbon dioxide (scCO₂) offers real potential as an alternative, environmentally benign reaction medium for the green preparation of organic molecules because it is nontoxic, cheap, and easily separable from reaction media (Meng et al. [2018](#page-11-0); Hiramatsu and Hori [2010](#page-10-0)). Thanks to these features, it gains importance day by day and is used as an alternative solvent. Especially, supercritical fluids have been used in various techniques such as organic synthesis (Ulusal et al. [2015;](#page-11-0) Morère et al. [2015a,](#page-11-0) [b\)](#page-11-0), deposition of metals on the solid materials (Meng et al. [2018](#page-11-0); Bozbag et al. [2012](#page-10-0)), extraction, food, cosmetics, pharmaceutics, materials, chemistry, sterilization, cleaning, impregnation, formulation, energy, and waste treatment (Xu et al. [1999](#page-11-0); Yuranov et al. [2003](#page-12-0); Kim et al. [2008](#page-11-0); Hayward et al. [2001;](#page-10-0) De Melo et al. [2014](#page-10-0)). Supercritical $CO₂$ deposition method, a green technique to prepare solid material supported metal nanoparticles, has taken significant attention for the last 20 years. The $\sec O_2$ deposition technique is briefly described as the dissolution of the metal-organic precursor in the $\sec O_2$, then the adsorption of the organometallic complex to the solid material surface, and finally the thermal (Bayrakceken et al. [2008](#page-10-0)) or chemical reduction (Bayrakceken et al. [2010](#page-10-0)) of the composite metal. Due to its high reduction properties, the most preferred reduction method that is thermal reduction is carried out in an inert atmosphere at atmospheric pressure or $scCO₂$. Another popular reduction method is a chemical reduction in $\sec O_2$ or at atmospheric pressure with a reducing agent such as hydrogen or alcohol. The particle size of metallic nanoparticles obtained by chemical reduction is greater than that obtained by thermal reduction (Saquing et al. [2005](#page-11-0); Sánchez-Miguel et al. [2017\)](#page-11-0). It is known that in these processes, parameters such as time, temperature, pressure, and solubility of the precursor in each stage are fundamental to achieve catalyst with the appropriate properties. The solubility of the precursor in $\sec 0$. is a significant criterion for the preference of appropriate metal complexes. Because, the metal loading of support, the crystal structure of metal nanoparticles on the support, the particle size and distribution are depended to the solubility of the precursor in deposition conditions (Zhang and Erkey [2006;](#page-12-0) Aggarwal et al. [2013\)](#page-10-0).

Palladium catalyst has received significant attention due to its application in industrially important areas such as hydrogenation, C-C cross-coupling reactions (Yılmaz and Güzel [2014;](#page-11-0) Yılmaz et al. [2017;](#page-11-0) Baran et al. [2018;](#page-10-0) Ghasemi and Karim [2018\)](#page-10-0), oxidation reactions, and hydrogen storage (Erünal et al. [2018\)](#page-10-0). In addition to being able to catalyze many reactions, palladium is a major issue, and the synthesis of organometallic compounds of palladium is quite simple, under favorable conditions. Besides, the availability of palladium as both homogeneous and heterogeneous catalyst brings ease of use. It has also taken an important place in nanocatalyst synthesis, where both homogeneous and heterogeneous catalyst systems are targeted.

The impregnation of Pd precursor via $\sec O_2$ deposition on the SBA-15 was carried out at 40 °C under 8.5 MPa while the reduction was carried out at 40 °C under H_2 pressures at 60 bar (6 MPa) (Morère et al. [2011\)](#page-11-0). Also, an additional thermal treatment was carried out after the reduction with hydrogen. In another study, impregnation of the Pd(0) complex on the SBA-15 surface was carried out at 41.4 MPa and 85 °C for 4 h. Owing to that complex used, no reduction is necessary after impregnation (Hunt et al. [2014\)](#page-10-0). On the other hand, use of various co-solvents is another way to prepare dispersed nanoparticles by increasing the solubility of the precursor. Lee et al. dissolved the Pd precursor in THF and evaporate on the SBA-15 surface at 60 °C and 10 MPa for impregnation and then reduced to 80 °C at a pressure of 17.2 MPa with a $CO₂/H₂$ mixture (Lee et al. [2006\)](#page-11-0). Besides, when H₂ reduction is used in $\sec O_2$ deposition studies, relatively larger particle sizes are obtained if compared to thermal reduction. For example, Tenorio et al. reported 5.2–7.9 nm particle sizes with 30–50 nm length from their study which Pd impregnation was carried out at 40–80 °C under 8.5–14 MPa following $H₂$ reduction at 40 and 60 bar (6 MPa) $H₂$ pressure (Tenorio et al. [2012\)](#page-11-0). The novelty of the current study is to achieve much smaller nanoparticles in length without the usage of co-solvent and still applying much lower temperature and H_2 pressure (80 °C under 1.03 MPa H2 pressure, 17.2 MPa total pressure).

The fact that the temperature and H_2 pressure used are much lower (80 \degree C and 1.03 MPa) is a key novelty factor in our work. In addition, it is observed that the nanoparticles obtained in the $\sec O_2$ deposition methods in which the hydrogen reduction step is used are mostly large. The impregnation of Pd precursor via $\sec 0₂$ deposition on the SBA-15 was carried out at 40–80 °C under 8.5–14 MPa while the reduction was carried out at 40 °C under H_2 pressures at 60 bar (6 MPa) (Tenorio et al. [2012\)](#page-11-0). In this study, they reported particles 5–8 nm (limited by the pore size) and 30–50 nm long. But the long of the nanoparticles obtained in our study is much smaller than similar methods. In our study, we carried out the deposition process without adding the organic co-solvent.

In the $\rm{s}\rm{c}\rm{CO}_{2}$ deposition method, a limited number of precursors are used, and these precursors are cyclooctadiene, β-diketonate, dithiocarbamate, amine, and their derivatives. These precursors are difficult to prepare, expensive, and sometimes require cosolvent during deposition because of low solubility. It also has disadvantages due to the high temperature (100–300 C) and pressure requirement during the deposition. We have contributed to the literature new precursor classes used for the green preparation of supported metallic nanoparticles in our previous studies. Pd (II) complexes of phenanthrenequinonedioxime and dimethylglyoxime ligands were synthesized by our group and used for deposition on alumina supports in the scCO_{2} medium (Ulusal et al. [2017](#page-11-0)). Also, we synthesized Pd precursor with the perfluoroalkyl chain group and used for deposition on the MW-CNTs (Tezcan et al. [2018](#page-11-0)). Moreover, we carried out the deposition of bipyridyl and phenanthroline-derived Pd (II) complexes, which we designed as a new precursor class, on SBA-15 (Ulusal and Güzel [2018;](#page-11-0) Ulusal [2017](#page-11-0)) and MW-CNTs (Erünal et al. 2018) in the scCO₂ medium. In our previous work, we have shown that the palladium complex of 2,2′ bipyridyl can be an alternative to the precursors in the literature on the deposition technique in which chemical reduction is carried out with the help of hydrogen. It is particularly preferred because it is very easy to prepare in a short time like 15 min and is suitable for storage at low temperature and pressure. The small size of the molecule used means that there is a little steric hindrance between the molecules and that there is more Pd precursor at the surface during deposition. This helps to form more homogeneously dispersed Pd nanoparticles. A further advantage of the Pd (II) complex of 2,2′ bipyridyl is that according to the TGA result, a small energy of 78.42 J/g is required to separate the two bipyridyl molecules in the structure, and this allows the deposition to occur at lower temperatures and pressures. Also, the melting point of the precursor was found as 413.8 °C that temperature is very important for the \rm{scCO}_{2} deposition process. The relationship between the precursor melting point and the ideal solubility conditions used in the nanoparticle process by the SCFD method has been reported to be a major problem. Accordingly, if the precursor used is larger than the melting point of the temperature of the deposition conditions, large particles are formed and accordingly, low activity catalysts are obtained (Incera Garrido et al. [2008;](#page-10-0) Türk [2014](#page-11-0); Türk and Erkey [2018\)](#page-11-0). In this present paper, the effect of the precursor on the structure of nanoparticles inside and onside of SBA-15 porous was investigated. Mesoporous SBA-15-supported Pd nanoparticles were

prepared with supercritical carbon dioxide ($\sec O_2$) deposition method by H_2 -assisted chemical reduction. For this aim, Pd (II) complexes of 2,2′-bipyridyl were used successfully for preparation of SBA-15-supported metallic Pd nanoparticles.

Experimental

Materials

2,2′bipyridyl was purchased from Sigma-Aldrich. Palladium (II) chloride used for precursor synthesis was supplied from ABCR GmbH. SBA-15 template silica (SBA-15) with mesoporous structure, < 150 μm particle size, pore size 6 nm, hexagonal pore morphology, which is used as solid support for deposition were obtained from Sigma-Aldrich with a purity of \geq 99.9%. All chemicals were used without further purification.

Solubility tests in supercritical carbon dioxide

Palladium (II) complex of 2,2′-bipyridyl was prepared to be used as a $\sec O_2$ precursor according to the methodology given our previous research (Erünal et al. [2018](#page-10-0)). The solubility of bis(2,2′ bipyridyl) palladium (II) chloride precursor was tested for four different pressures as 10.3, 13.8, 17.2, and 20.7 MPa at 80 °C in the high-pressure reactor (sapphire window, 0.1 L). Approximately 150 mg of the complex was placed in the clear vessel. The vessel was warmed up to 80 °C and filled with $CO₂$ up to the desired pressures with a syringe pump. After obtaining saturated solutions, the saturated supercritical solution was taken to a 5-mL receptacle at the 80 °C. Then, the sample into the holder was transferred to 5 mL of ethanol in Schlenk tube. To finish the solubility test, the receptacle was washed with hot ethanol ~ 10 mL) for the purpose of removing the residual and added to the washing solution. Final ethanol solutions were tested with a Perkin Elmer Lambda 25 UV-Vis spectrophotometer for determination of solubility. The solubility tests of the complexes were repeated three times, and average solubility value was calculated.

Fig. 1 Schematic diagram of $\sec O_2$ deposition system. (1) $CO₂$ syringe pump, (2) $H₂/CO₂$ mixing unit, (3) inlet valve, (4) water circulator for cooling, (5) vessel, (6) heating jacket, (7) SBA-15, (8) precursor, (9) nanoparticle, (10) magnetic stirrer, (11) safety disc, (12) vent

Green preparation of Pd/SBA-15 nanoparticles by ScCO_2 deposition method

Pd/SBA-15 samples were prepared by the hydrogenassisted using supercritical deposition technique. A stainless steel high-pressure reactor with an internal volume of 54 mL was used for the deposition studies.

The deposition process was carried out in 3 steps: (1) dissolution of the precursor in $\sec O_2$ under 17.2 MPa pressure and at 80 °C, (2) adsorption of the precursor on the surface of SBA-15 in same conditions, and (3) reduction of palladium complex to $Pd(0)$ by H_2 gas. The schematic diagram of the high-pressure reactor used is given in Fig. 1.

Two hundred milligrams of SBA-15 and the precursor in the required amount of Pd were added in a highpressure reactor with a window of sapphire glass. The expected theoretical Pd loading was 5.16% of the catalyst (That was calculated as the ratio of the mass of Pd to the total catalyst mass). In order to completely remove the oxygen in the vessel, it was pre-treated with $CO₂$ for 1 h. During the first step, the reactor was gradually heated up to 80 °C with a circulating heater/cooler and was then filled with 17.2 MPa $CO₂$ gas with a syringe pump (Isco 260D). After the system was allowed to be saturated for 1 h under these conditions, the gas in the reactor was evacuated and the gas pressure was reduced to 10.3 MPa. Then, 23 mmol H_2 gas and CO_2 gases (with a total pressure of 17.2 MPa) in a 10-mL intermediate volume were transferred to the system. Finally, the reactor was pressurized at 17.2 MPa with a syringe pump and stirred under these conditions for 24 h. At

Substance	$S (10^{4} \text{ mol/L})$							
	$235.6^a/10.3^b$	$337^{\rm a}/13.8^{\rm b}$	$377^{\rm a}/13.8^{\rm b}$	501.7 $^{a}/17.2^{b}$	$551^{\rm a}/20.7^{\rm b}$	606.8 $\frac{a}{20.7}$	$672^{\rm a}/27.6^{\rm b}$	
$PdPyr_2Cl_2^c$	0.612		2.653	3.877		5.713		
PdPhenCl ₂ ^c	0.605		3.170	5.199		6.454		
Pd $(PTQD)2d$		1.991			4.959		8.171	
Pd $(DMG)2d$		2.681			7.138		10.691	

Table 1 Experimental data for the solubility (S) of the investigated precursor in $\sec O_2$ at different pressures and densities (kg m⁻³)

 a_{ρ} (kg m⁻³)

 b P (MPa)

 $\rm ^{c}$ 80 °C, $\rm ^{d}$ 90 °C

the end of this period, the system was brought to room temperature and the gas inside was slowly discharged. The obtained gray Pd/SBA-15 nanoparticles (catalyst) were washed with ethanol and dried in an 80 °C oven. The quantitative amount of total palladium in the prepared catalyst was quantified by ICP-OES (Perkin Elmer 2100 DV). HR_TEM (Jeol 2100F HR_TEM) was used for analyzing the surface morphology. Particle

Fig. 3 HR-TEM images and particle size distribution of SBA-15 supported Pd nanoparticles. The gray background is corresponding to SBA-15 support while black dots on the gray background are Pd nanoparticles. Pd nanoparticles have a homogeneous

dispersion with any agglomeration. a, b 50 nm. c 5 nm. d The size distribution of Pd nanoparticles: the mean diameter of 259 particles is 13.9 ± 2.1 nm

Fig. 4 Nitrogen adsorption– desorption isotherms of a SBA-15 and b SBA-15-supported Pd catalyst at 77.4 K. (Inset: pore size distributions of the corresponding samples from adsorption branch)

size and crystal structure were analyzed by XRD (Rigaku Miniflex, CuK α , $\lambda = 0.154$ nm). A Micromeritics Tristar II 3020 instrument was used to analyze the surface areas and pore properties N_2 adsorption–desorption isotherms recorded at 77.4 K. The pure support and catalyst were degassed at 300 K for 3 h under vacuum before treatment. The Brunauer– Emmett–Teller (BET) equation was used to calculate the specific surface areas. Pore volume and pore size were determined with the Barrett–Joyner–Halenda (BJH) model, and the adsorption branches of nitrogen physisorption isotherms were used to calculate the pore size and pore volume. X-ray photoelectron spectroscopy (XPS) measurements were performed in Thermo Scientific Al K-Alpha.

Catalytic tests

The Suzuki–Miyaura C-C cross-coupling reaction of a phenylboronic acid and bromobenzene at room temperature was chosen as a model reaction to test the catalytic performance of prepared Pd/SBA-15 nanoparticles. In these reactions, triethylamine, which is an organic base,

and K_2CO_3 and NaOH, which are inorganic bases, are used as bases.

An Agilent 6850 Gas Chromatography (GC) instrument was used to calculate the reaction efficiency. Before analysis by GC, the products were extracted and purified from the column containing silica gel and anhydrous Na₂SO₄.

Results and discussion

The solubility of precursor in $ScCO₂$

The solubility results were evaluated in the scCO_{2} medium, and the highest resolution condition was selected as the deposition conditions for 80 °C and 20.7 MPa pressure. The solubilities of the present precursor $(PdPvr_2Cl_2)$ and our other precursor (Ulusal et al. [2017](#page-11-0); Ulusal and Güzel [2018\)](#page-11-0) in previous studies at different pressures and densities are shown in Table [1.](#page-3-0)

It was found that fluorinated complexes have a high solubility compared with the corresponding nonfluorinated complexes. Alkyl groups in the ligands

 V_p (cm³/g)

Fig. 5 Survey XPS spectrum of Pd/SBA-15 nanoparticles (a). High-resolution XPS spectra of Pd3d (b) orbitals

enhance the solubility of the complex. On the other hand, aryl groups lead to a lower solubility (Aschenbrenner et al. [2007\)](#page-10-0). So, we expect that the solubility of $PdPyr_2Cl_2$ in $\sec O_2$ is similar to the used precursor in literature. It is concluded that the solubility of PdPyr₂Cl₂ is similar to the solubility of PdPhenCl₂ which we used in our previous studies.

Characterization of Pd/SBA-15

The amount of total Pd in the catalyst was determined around 5.0% by ICP-OES measurements. The catalyst was prepared according to the theoretical Pd loading around 5.16%. From the obtained data, the deposition efficiency was found as 96.9%.

To analyze the size and crystal structure of the catalyst, XRD measurement was performed. The wideangle XRD pattern of SBA-15 and Pd/SBA-15 is shown in Fig. [2](#page-4-0). Amorphous $SiO₂$ support peak appeared 2 θ degrees of ca. 23° with a shallow and very board reflection (JCPDS card number is 01-086-1561). The presence of very intensive sharp peaks observed at $2\theta =$ 40.29 ° assigned to (111), $2\theta = 46.87$ ° assigned to (200), $2\theta = 68.18$ ° assigned to (220), and $2\theta = 82.6$ ° assigned to (311) reflections of the face-centered cubic Pd lattice system, with the space group referred to Fm-3m (JCPDS card number is 46-1043). Pd peaks indicated that particles are very small. Pd nanoparticle size was calculated via the Scherrer equation as 13.7 nm due (111) peak.

HR-TEM images of pure SBA-15 and Pd/SBA-15 are shown in Fig. [3.](#page-4-0) The dark nanoparticles are homogeneously distributed on the surface of the SBA-15 with the gray-colored parallel channel. It can be seen from Fig. [3a](#page-4-0), b that the resulting Pd nanocatalysts are mostly deposited both on the exterior surface of the support and between its channels. It can be estimated that the nanoparticles forming in the channels are larger than those formed on the surface and distributed over a wider surface. The particles are dispersed homogeneously on the support without agglomeration on the surface. Although some of the Pd nanoparticles on the surface of SBA-15 are very small, some of them are together (it can be seen from Fig. [3](#page-4-0)c). Despite the possibility of Pd nanoparticles forming in the SBA-15 pores, there is no definite conclusion in this regard as there is no image from the pores. However, it can be said that this probability is very low because the particle size obtained from XRD is larger than the pores (Liu et al. [2008](#page-11-0)). The mean particle size diameters were calculated as 13.9 ± 2.1 nm that also supports XRD data.

The porosities of SBA-15 and Pd/SBA-15 were further studied by N_2 adsorption–desorption isotherms. N_2 adsorption–desorption isotherms of support and catalyst can be seen in Fig. [4.](#page-5-0) These two obtained isotherms exhibit a type IV which is a characteristic isotherm of mesoporous materials such as SBA-15 and MCM-41 according to the IUPAC classification. Table [2](#page-5-0) shows textural properties (BET surface area (S_{BET}) , pore size and pore volume (Vp)) obtained from these isotherms (Al-Othman [2012](#page-10-0)). BET surface area of SBA-15 was 647.2 m²/g, total pore volume was 0.97 cm³/g, and the pore diameter was 3.7 nm. After deposition of Pd on the SBA-15, BET surface area was $492.6 \text{ m}^2/\text{g}$, total pore volume was $0.76 \text{ cm}^3/\text{g}$, and pore diameter was 3.8 nm. Adsorption isotherm of Pd/SBA-15 is very similar to the

$Pd/SBA-15$ $B(OH)_2$ Br $^{+}$ solvent, base, T							
Phenylboronic acid		bromobenzene			biphenyl		
Exp. No.	Catalyst	Base	Solvent	$T (^{\circ}C)$	t(h)	Yield $(\%)^*$	TON
1	Pd/SBA-15	K_2CO_3	Ethanol	30	24	80.4	160.8
$\mathbf{2}$	Pd/SBA-15	K_2CO_3	Methanol	30	24	13.1	26.2
$\overline{\mathbf{3}}$	Pd/SBA-15	K_2CO_3	NMP	30	24	43.8	87.6
$\overline{\mathbf{4}}$	Pd/SBA-15	K_2CO_3	DMF	30	24	37.5	75
5	Pd/SBA-15	K_2CO_3	Acetonitrile	30	24	31.2	62.4
6	$Pd/SBA-15$	K_2CO_3	Dioxane	30	24	33.6	67.2
$\overline{7}$	$Pd/SBA-15$	NaOH	Ethanol	30	24	52.2	104.4
8	Pd/SBA-15	NaOH	Methanol	30	24	12.9	25.8
9	Pd/SBA-15	NaOH	NMP	30	24	42.2	84.4
10	$Pd/SBA-15$	NaOH	DMF	30	24	11.3	22.6
11	$Pd/SBA-15$	NaOH	Acetonitrile	30	24	18.2	36.4
12	Pd/SBA-15	NaOH	Dioxane	30	24	34.8	69.6
13	Pd/SBA-15	Et ₃ N	Ethanol	30	24	31.9	63.8
14	$Pd/SBA-15$	Et_3N	Methanol	30	24	6.6	13.2
15	$Pd/SBA-15$	Et ₃ N	NMP	30	24	11.4	22.8
16	Pd/SBA-15	Et ₃ N	DMF	30	24	10.9	21.8
17	Pd/SBA-15	Et ₃ N	Acetonitrile	30	24	3.6	7.2
18	$Pd/SBA-15$	Et_3N	Dioxane	30	24	21.1	42
19	Pd/SBA-15	K_2CO_3	Ethanol	60	1.5	100	200
20	Pd/SBA-15	K_2CO_3	Ethanol	80	0.5	100	200
Reaction ingredient: Pd (0.0050 mmol), bromobenzene (1.0 mmol), phenylboronic acid (1.20							
mmol), base (2.0 mmol), organic solvent (2.0 ml) and water (2.0 ml)							

Table 3. Suzuki-Miyaura Cross-Coupling Reactions of phenylboronic acid and bromobenzene via SCF deposited Pd/SBA-15

*** Isolated yields**

TON (Turnover number of catalyst): moles of bromobenzene converted per mole of Pd.

Reaction ingredient: Pd (0.0050 mmol), bromobenzene (1.0 mmol), phenylboronic acid (1.20 mmol), base (2.0 mmol), organic solvent (2.0 ml) and water (2.0 ml)

* Isolated yields

TON (Turnover number of catalyst): moles of bromobenzene converted per mole of Pd.

support; as a result, it can be said that metal addition on the support does not affect the porous structure (Morère et al. [2015a,](#page-11-0) [b;](#page-11-0) Matei et al. [2016](#page-11-0); Duan et al. [2017\)](#page-10-0), but the amount of adsorbed nitrogen is decreased. Both SBA-15 and Pd/SBA-15 isotherms exhibit a sharp capillary condensation step in the P/P_0 range of 0.6–0.8 dissociation between 0.6 and 0.8. This is an indication of the uniformity of the pore sizes (Wang and Liu [2011\)](#page-11-0). When the hysteresis loops of SBA-15 and Pd/SBA-15 analyzed, it can be said that palladium loading makes the hysteresis smaller with decreasing surface area, total pore volume, and increasing pore diameter. The decreases of surface area could be due to the incorporation of Pd nanoparticles into the pores of SBA-15 and/or the block by the Pd nanoparticles (Yao et al. [2015\)](#page-11-0). Total pore volume of Pd/SBA-15 demonstrate an average shift of $0.21 \text{ cm}^3/\text{g}$ with palladium loading. It can be said that the slight increase in pore size can be explained as a cause with Pd inclusion.

X-ray photoelectron spectroscopy analysis of Pd/SBA-15 is shown in Fig. [5](#page-6-0) (Pd3d). XPS analyses were used to specify the chemical state of palladium in the catalyst.

Catalyst	Yield(%)	Time	Temp. $(^{\circ}C)$	Solvent	TON	Base	Reference
Pd/SBA-15	21	0.5 _h	100	Ethanol	Unvalued	K_3PO_4	Zheng et al. (2010)
Pd/dendrimer	97	20 _h	101 (Reflux)	1.4-dioxane	Unvalued	K_3PO_4	Wu et al. (2006)
Pd/SBA-15	80.2	3 h	110	Ethanol	1360	Et ₃ N	Noube et al. (2015)
Pd/SBA-15	90	6 h	90	Ethanol	900	K_2CO_3	Sarkar et al. (2015)
Pd/SBA-15	80.4	24 _h	Room temp.	Ethanol	160.8	K_2CO_3	Present study
Pd/SBA-15	100	1.5h	60	Ethanol	200	K_2CO_3	Present study

Table 4 Comparison between catalytic performances of mesoporous silica-supported palladium nanocatalyst and different catalysts in the Suzuki–Miyaura cross-coupling reactions

Metallic palladium (Pd0) was observed with two characteristic peaks that correspond to Pd $3d_{3/2}$ (336.08 eV) and Pd $3d_{5/2}$ (341.28 eV) which is in agreement with literature data (Duan et al. [2017](#page-10-0)). These results show that palladium is in metallic form in the catalyst verifying the XRD data. Since metallic palladium is more active than palladium oxide in the heterogeneous catalyst, the activity of the catalyst is expected to be high for the coupling reaction. On the other hand, the peaks of the high-resolution XPS spectrum (Si_{2p}) , C_{1s} , Pd_{3d}, O_{3s} , and Pd_{3p}) are provided in Fig. [5](#page-6-0) (Survey). Moreover, the absence of Cl peaks in the catalyst supports the complete removal of the ligands from the catalyst.

Application of Pd/SBA-15 as a catalyst in Suzuki–Miyaura cross-coupling reaction

The catalytic performance of 0.5 mol% Pd/SBA-15 was assessed for Suzuki–Miyaura cross-coupling reaction of bromobenzene and phenylboronic acid at room temperature under atmospheric conditions. Even though there

are many studies about Pd-catalyzed Suzuki–Miyaura cross-coupling reaction of Pd (0) and Pd (II) on the various supports, room temperature conditions are not satisfactory for many of them. In order to find the optimum conditions for the prepared catalyst, it was tested in six different solutions (2.0 mL) of ethanol, methanol, DMF, NMP, acetonitrile, and 1,4-dioxane. The influence of organic and inorganic bases (2.0 mmol) , K_2CO_3 , NaOH, and triethylamine were also investigated during the reactions. The obtained results are summarized in Table [3](#page-7-0).

Heterogeneous Pd nanoparticles generally need high temperatures 100–120 °C in Suzuki–Miyaura reactions because of the high activation energy in mechanism steps (Li et al. [2013;](#page-11-0) Molnar [2011](#page-11-0); Dumbre et al. [2016](#page-10-0)). Reaction temperature rise increases the product yield automatically.

Turnover number of catalyst (TON) was calculated as moles of desired product formed/number of total catalyst. To calculate the TON value, the amount of Pd

Table 5. Pd/SBA-15 recycles study in Suzuki reaction

Br	Pd/SBA-15 (reused) $PhB(OH)_2$, EtOH-H ₂ O, K_2CO_3 , 60 °C			
Run	Yield $(\%)$			
	100			
	98			
	96			
	90			
5	83			
6	70			
	52			
Reaction ingredient: Pd (0.0050 mmol), bromobenzene (1.0 mmol),				
phenylboronic acid (1.20 mmol), K_2CO_3 (2.0 mmol), ethanol (2.0 ml) and				
water (2.0 ml), 24 h				

in the Pd/SBA-15 was determined by ICP-OES. The calculated TON results obtained are given in Table [3.](#page-7-0) Although the TON values are quite high for a heterogeneous catalyst, the highest value was found as 160.8 in the ethanol- K_2CO_3 pair. It can be said that the nanocatalyst prepared when the TON values are compared with the literature has high efficiency (given in Table [4\)](#page-8-0).

The reaction conversion graphs in different solvents and bases are given in Fig. [6](#page-8-0). In general, K_2CO_3 , which is an inorganic base for virtually all used solvents, appears to have the best results when examining the effect of the bases when the solvents are held constant. For each of the 3 bases used, the highest catalytic activity was reached as the result of the solvent system being ethanol/water. The highest catalytic conversion was obtained in the ethanol- K_2CO_3 solvent-base pair. Also, it is clear that the solvent-base pair with the lowest conversion is Et_3N -acetonitrile. The catalyst shows higher yields at lower temperatures than many catalysts in the literature. Table [4](#page-8-0) shows the comparison of our catalyst and the catalytic activities of other catalysts in the literature. As seen in the table, although the Suzuki reaction is usually carried out above 50 °C, our catalyst exhibits high activity at room temperature. When the literature given in Table [4](#page-8-0) is examined, the catalytic activity results at room temperature show high activity at much lower temperatures than similar reactions. Also,

according to the activity results at 60 °C, 100% efficiency was obtained in as short as 1.5 h.

The lifetime of Pd/SBA-15 catalyst at 60 °C with the same reaction conditions were also tested. The results were given in Table 5. It is seen that the catalyst can be reused four times without a significant decrease in catalytic activity under these conditions.

Conclusions

The deposition of Pd nanoparticles on SBA-15 templated mesoporous silica was successfully carried out using synthesized Pd (II) complex of 2,2′bipyridyl as a precursor in supercritical carbon dioxide under mild conditions. Prepared SBA-15-supported Pd nanoparticles were used to catalyze Suzuki–Miyaura crosscoupling reaction of a phenylboronic acid and bromobenzene at room temperature. Moreover, homogeneously well-dispersed metallic palladium nanostructures were obtained with particles 13.7 nm determined from XRD. Palladium was in metallic form in the catalyst according to XPS results. It was found that Pd loading is very high according to nanoparticles prepared with similar methods. The catalytic activities at room temperature of Pd/SBA-15 were tested in various organic solvent:water (1:1) ethanol, methanol, NMP, DMF, 1,4-dioxane, and acetonitrile with the different bases

 K_2CO_3 , NaOH, and Et₃N, separately. The best catalytic activity was obtained in the reaction using ethanol/water solution and K_2CO_3 base at room temperature, and its TON value was 160.8 which is better than many catalysts in literature. Catalyst re-usability was achieved at 60 °C and activity was found to continue to a significant extent at 4 uses.

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Compliance with ethical standards

Conflict of interest The authors declare that they have no conflict of interest.

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