

A comprehensive review of thermal enhancement techniques in microchannel heat exchangers and heat sinks

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Abstract

A novel framework has been employed in various contemporary studies, to enhance heat transfer in heat exchangers through microchannels. A microchannel heat exchanger (MCHE) is a miniature heat exchanger that can address issues such as rapid increases in heat flux in small spaces, storage space constraints, and the need for compact, lightweight heat exchangers. Four perspectives were used in the qualitative literature analysis: working fluid, flow disruption, microchannel material, and microchannel cross section. The findings revealed that various working fluids (air, water, refrigerants, oil, and nanofluids) are employed in microchannel heat exchangers (MCHE) and microchannel heat sinks (MCHS); however, almost all studies have shown that nanofluids as working fluids in microchannels exhibit better thermal behavior than other fluids. Enhanced thermal performance can be achieved by adding flow disrupters (wavy channels, ribs, dimples, and baffles). Based on several applications, various materials, including aluminum (Al), copper (Cu), silicon (Si), stainless steel, silver (Ag), and various other metals, are used for MCHE & MCHS construction. However, owing to the thermal property limitations and oxidation behavior of metallic materials researchers have used ceramic microchannels to avoid these problems. The outcomes of the present review suggest that microchannel-based applications have come a long way away, but there are still barriers to addressing the needs of heat transfer in modern industries, such as the prevalence of the use of conventional rectangular shapes, water-based working fluids, metals as construction materials, and numerical techniques. Based on a literature survey, the authors suggest that rectangular wavy microchannels made of ceramic material using Al₂O₃-water as a nanofluid have better hydrothermal behavior than any other microchannel.

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Graphical abstract



Keywords Microchannel heat sink \cdot Microchannel heat exchanger \cdot Nanofluid \cdot Flow disruption \cdot Wavy channels \cdot Ceramics

Abbreviati	ons	LWC	Longitudinal wavy channel
Ag	Silver	MCHE	Microchannel heat exchanger
AIN	Aluminum nitride	MCHS	Microchannel heat sink
Al_2O_3	Aluminum oxide	MWCNTs	Multiwall carbon nanotubes
Au	Gold	Nu	Nusselt number
Bi ₂ O ₃	Bismuth oxide	Re	Reynold number
BR	Bidirectional ribs	SCR	Semicircular ribs
BTR	Backward triangular ribs	SCRR	Sinusoidal cavities and rectangular ribs
CCZ-HS	Cross-cutting zigzag heat sink	SER	Semi elliptical ribs
CF	Carbon fluoride	SiC	Silicon carbide
CHF	Critical heat flux	SiO_2	Silicon dioxide
CNT	Carbon nanotubes	SOCRR	Secondary oblique channels rectangular ribs
CZ-HS	Continuous zigzag heat sink	SRC	Straight rectangular channel
Cu	Copper	SR	Spanwise ribs
CuO	Copper oxide	TGMCHS	Triangular groove microchannel heat sink
D _h	Hydraulic diameter	TiO ₂	Titanium dioxide
DÏ	Deionized	TWĈ	Transversal microchannel
Fe ₃ O ₄	Ferrous oxide	VR	Vertical ribs
Fe	Iron	ZnO	Zinc oxide
Hf	Hafnium	ZrB_2	Zirconium diboride
HVAC	Heat ventilated and air conditioning	-	
H_2O	Water		

IMCHS Interrupted microchannel heat sink

Introduction

The major problems in the ongoing decade are the conservation of energy and search for alternative energy sources. In the coming decades, it is anticipated that conventional energy sources will be depleted because of their ongoing use. To overcome these difficulties, some researchers have focused on substituting renewable energy sources with conventional ones. By contrast, other researchers have focused on using creative approaches to improve the energy performance of devices. Research on the development of energy-efficient devices has resulted in numerous subfields. Among the numerous methods, miniaturization of conventional devices is one. Several industries rely on heat exchangers and use conventional heat exchangers with a high thermal resistance and low efficiency. Therefore, the development of heat exchangers is required to lower thermal resistance, boost convective heat transfer, and enhance efficiency. A heat exchanger is designed to transfer heat from one fluid to another without losing heat to the surrounding environment. Two significant phenomena occur in a heat exchanger: fluid movement in passages and the transfer of energy between the channel walls and fluids. Hence, these devices can be made more efficient by enhancing the performances of these two phenomena. Because the heat transfer rate is dependent on the ratio of the surface area to the volume, smaller channel dimensions result in a higher heat transfer coefficient. Conventional heat exchangers employ tubes with a diameter of ≥ 6 mm; however, microchannels with a size of ≤ 1 mm are the next phase in the development of heat sink and heat exchangers. Owing to their high rate of heat transfer potential and lightweight, as well as their ability to save energy, space, and materials compared with conventional heat exchangers, this field of study is the subject of significant attention and analysis.

Microchannels are defined as narrow flow tubes of size 1 mm or less, that allow for heat transfer surface densities of 10,000 m² m⁻³ or higher [1], in contrast to conventional channels with a surface density of 700 m² m⁻³. Micro and minichannels differ from normal channels in terms of the channel hydraulic diameter (D_h). The classification methods proposed by Mehendafe et al. [2] and Kandlikar et al. [3], the

latter of which is becoming increasingly popular, are typically adopted. Table 1 lists the terminology used by these authors.

The amount of heat that can flow through the microchannels depends on the surface area which can facilitate heat transfer, which is determined by the hydraulic diameter $(D_{\rm h})$ of the channel. By contrast, the flow rate is determined by the cross-sectional area of the channel, which is proportional to $D_{\rm h}^2$. Therefore, as $D_{\rm h}$ decreases, the surface-areato-volume ratio increases, indicating that the surface area of the channel relative to its volume increases. The flow within the microchannels is typically laminar, and the local heat transfer coefficient varies inversely with $D_{\rm h}$. Consequently, a decrease in $D_{\rm h}$ was necessary to enhance the heat transfer coefficient. Tuckerman and Pease [4] suggested an initial study of the MCHS approximately 40 years ago. They assumed that reducing the $D_{\rm h}$ of the channel would increase heat transfer. This invention has strengthened the electronics industry, which has dealt with difficulties such as high heat dissipation in compact areas. Kandlikar et al. [5] studied the thermohydraulic performance of minichannels and microchannels in their literature. In the initial stages of microchannel development, there were significantly fewer publications. However, microchannels have slowly become the most crucial field of research, as shown in Fig. 1 (references are taken as per Scopus).

Microchannel heat sink (MCHS) and its applications

A heat sink is a device that uses extended surfaces to collect heat from a source and effectively disperses it into the environment effectively as shown in Fig. 2. The capacity of traditional channel heat sinks to dissipate heat is limited even with the use of forced convective cooling. However, as technology has progressed, concerns regarding high heat dissipation in small spaces have increased. Micro- and minichannels have provided appropriate solutions to meet these objectives. Heat sinks are classified as passive, active, liquid-cooled, or phase-change heat sinks depending on the cooling technology used for a specific application as shown in Table 2. The MCHS is particularly effective for removing high heat fluxes and maintaining electronic component temperatures within

Table 1	Channel taxonomy
based or	n hydraulic diameter

Mehendafe et al. [2]	Hydraulic diameter	Kandlikar and Grande[3]	Hydraulic diameter
Fraditional channels	>6 mm	Traditional channels	> 3 mm
Compact passages	1 mm to \leq 6 mm	Minichannels	200 μ m to \leq 3 mm
Mesochannels	100 μ m to \leq 1 mm	Microchannels	10 μ m to \leq 200 μ m
Microchannels	1 μ m to \leq 100 μ m	Transitional channels	0:1 μ m to \leq 10 μ m
		Molecular nanochannels	≤0:1 µm



Publications in microchannel heat exchangers

Fig. 1 Publications on microchannel heat exchanger as per Scopus



Table 2 Classification of heat sinks

Heat sink categ	gory			
	Active	Passive	Liquid cooling	Phase change cooling
Applications	High power intensity uses	Natural convection systems, simple power intensity uses	High power intensity uses	For high power output
Benefits	Heat sink with fan, large heat dissolution capacity	Consumer friendly, economical	High heat dissolution capacity compared to active and passive	Heat dispersed equally
Drawback	Expensive	Limited power dissolution capacity	Complicated & expensive	Expensive, complex, and requires more area
Examples	Fan, fins, heat sink	Metal plate	Liquid cold plate	Vapor firmness phase

acceptable limits. Unlike regular channels, microchannels can dissipate power densities up to 1000 W cm⁻², whereas conventional channels can only dissipate heat fluxes up to 20 W cm^{-2} . Xiang et al. [6] conducted a series of comparative experiments to assess the heat transfer capabilities of a microchannel heat sink in comparison with a conventional metal solid heat sink. The results indicate that the microchannel heat sink outperforms the conventional metal solid heat sink in terms of heat dissipation performance. This makes them an excellent choice for applications involving high power LEDs. To cool the electronic devices, Xiong et al. [7] proposed the use of microchannels as liquid-cooled thermospreaders linked to gas-cooled heat sinks. In addition to integrated circuits, these channels have been used in many other applications. Micropumps, microturbines, micromotors, microvalves, and microreactors are devices that are based on this technology [8]. Additionally, microscale development has spawned a new field of microfluidics.

Micro-/minichannel heat exchangers and applications

With respect to heat exchangers, Little et al. [9] were the first to realize the possibilities of micro- and minichannels. The authors suggested that these narrow channels could be used in small-scale Joule-Thomson refrigeration systems. Swift et al. [10] were the first to submit a patent application for the manufacturing process of microchannel heat exchangers (MCHE) with cross-flow. These heat exchangers can be used as energy-efficient alternatives to conventional HVAC (heating, ventilation, and air conditioning) systems. The additional benefit of MCHE in these systems is that they consume less refrigerant and have a greater overall system efficiency. However, owing to their high manufacturing costs and lack of "precise performance prediction tools," their commercial use is limited. MCHE, on the other hand, has found widespread use in refrigeration [11] and air-conditioning systems^[12], window air conditioning^[13], split air conditioners[14], chillers, air-cooled ammonia condensers[15], vapor compression refrigeration systems [16], and heat pumps[17] are just a few examples. A schematic of the various MCHE types is shown in Fig. 3, along with information about their uses, types, construction materials, and fabrication methods.

Classification of microchannel design

Numerous attempts have been made to reduce the thermal resistance of MCHS and enhance their heat transfer ability. Steinke and Kandlikar [5] examined the use of



Fig. 3 represent the classification of MCHE



Fig. 4 Heat transfer enhancement methods in microchannel design

passive and active strategies to improve the thermal properties of mini- and microchannels. Active methods for improving the heat transfer rely on additional vibrational, magnetic, and electric flux forces. In contrast to active techniques, which often depend on external factors, passive techniques enhance heat transfer by means such as flow disruption, changing the geometry, and altering the working fluid of the heat sink. In addition, they performed a comprehensive analysis and assessed the feasibility of using these methodologies in novel MCHS applications. This review discusses the essential heat transfer enhancement methods used in microchannel design, as shown in Fig. 4. Microchannel designs can be categorized based on several factors, such as the types of working fluids utilized in microchannels, materials utilized to construct microchannels, techniques employed in microchannels to disrupt flow to improve heat transfer, and microchannel geometries.

Working fluid

Microchannels in the twentieth century used various working fluids. The most frequently used fluid is water, followed by air and various gases. Other fluids include liquid and gaseous nitrogen, common refrigerants, alcohol, and lubricants. Water has been commonly employed as the primary working fluid in earlier research; however, its limited thermal conductivity in comparison with metals restricts its applicability in microchannels. Nanofluids have received considerable attention over the last two decades because of their exceptional thermophysical properties. Owing to their exceptional thermal properties, nanofluids can be used in various applications such as solar energy devices, aerospace, the automobile industry, electronic devices, medical applications, and manufacturing sector as shown in Fig. 5.

Nanofluids

A nanofluid is a mixture of a base fluid and suspended solid particles on a nanometer scale. Suspending tiny solid particles in energy-transfer fluids can significantly improve their thermal conductivity and provide a cost-effective novel technique for improving their thermal characteristics. The

Fig. 5 Various applications of nanofluids

concept of "nanofluid" was coined by Choi [18] to describe a mixture of base fluids such as water, glycerine, ethylene glycol, and oil with nanoparticles. This combination resulted in a significant enhancement of the thermal characteristics of the fluid. Standard fluids such as water and ethylene glycol have low thermal conductivities, but adding solid particles to the fluid can enhance the thermal conductivity because solid materials typically have a higher thermal conductivity than fluids. It is possible to employ metallic or nonmetallic solid particles. However, large micro- and macro-sized particles may block flow channels and have poor stability, making their use unjustifiable. Table 3 lists the metallic, metallic oxide, and carbonaceous materials and their corresponding thermal conductivities. Compared to commonly used heat transfer fluids such as water, ethylene glycol, and various oils, these materials exhibit significantly higher thermal conductivities.

Researchers have conducted several studies on the use of nanofluid in MCHS, necessitating a review of prior and current research to identify and carry out future research. The most important criterion before using a nanomaterial as a nanofluid in a microchannel is the material selection. The possible factors for selecting a nanomaterial for use in the creation of nanofluids for heat transfer in microchannels are the thermal characteristics, chemical stability, safety,



Туреѕ	Material	Thermal conductivity/W m ⁻¹ K ⁻¹
Liquids	Water	0.613
	Ethylene glycol	0.253
	Engine oil	0.15
Nonmetallic solids	Titanium	23
	Silicon	148
	Alumina	40.0
	Sodium	72.3
Metals	Copper	401
	Aluminum	237
	Zinc	112.2
	Nickel	67
	Ferrous	80
Metal oxide	Al_2O_3	40
	ZnO	13
	CuO	20
	SiO ₂	1.1–1.4
	TiO ₂	4.8
	Fe ₃ O ₄	17.65
Carbonaceous material	Diamond	≥1500
	CNT	≥3000

 $\label{eq:table_state} \begin{array}{l} \textbf{Table 3} & \textbf{Thermal conductivity of the various base fluid and base} \\ \textbf{materials of nanofluid} \end{array}$

compatibility with the base fluid, affordability, and accessibility [19, 20]. Figure 6 presents an overview of the aspects to be considered when selecting a nanomaterial for nanofluid creation.

Advances in nanofluid preparation

- *Synthesis Techniques* Different techniques have been developed to create stable nanofluids with controlled particle dispersion. These include chemical processes, physical processes (such as milling or laser ablation), and more contemporary approaches, such as electrochemical synthesis and green synthesis.
- *Characterization Techniques* Techniques like transmission electron microscopy (TEM), dynamic light scattering (DLS), and X-ray diffraction (XRD) were used to obtain a clear picture of the size, shape, distribution, and physical characteristics of the nanoparticles. These approaches aid in understanding the behavior and stability of nanofluids.
- *Surface Modification* Nanoparticles can be functionalized via surface modification methods, improving their dispersion stability and compatibility with the base fluid. Surfactant coating, polymer grafting, or chemical processes can be used to modify the surfaces.
- *Stability Enhancement* Researchers are working to find ways to make nanofluid more stable over time. The most common methods are the use of stabilizing agents, magnetic fields, and external fields such as ultrasound and electric fields to prevent nanoparticle agglomeration and sedimentation.

Effect of nanomaterial on the stability of nanofluids

Nanofluid are suspensions that remain in a stable equilibrium state when subjected to different forces, such as van der Waals, electrostatic, and gravitational forces. The ability to maintain this state is known as the stability of the nanofluid, and this ability of nanofluids is a crucial



Fig. 6 Classification of nanofluids based on selection criteria

characteristic to consider when employing in many applications, including MCHS and MCHE. The stability of nanofluids can be influenced by several factors, including the choice of nanomaterial, base fluid properties, nanomaterial concentration, surface chemistry, and temperature [21, 22]. The stability of a nanofluid can be evaluated by various methods, such as:

- Zeta potential analysis The zeta potential analysis evaluates the stability of nanofluids through the observation of the electrophoretic behavior of the fluid. Higher absolute zeta potential values (either positive or negative) indicate greater repulsion between the particles, leading to enhanced stability.
- *Electron microscopy methods* The particle size distribution of the nanofluid was measured using transmission electron microscopy (TEM) or scanning electron microscopy (SEM). SEM & TEM are widely used by researchers to investigate particle shape, size, and aggregation, as shown in Fig. 7.
- Sedimentation photograph capturing method In this method, the volume of agglomerated nanoparticles in a nanofluid is observed under an external force. This was done by placing a sample of the prepared nanofluid in a transparent glass vial; and the formation of sediments was observed by capturing photographs of the vial at equal intervals of time using a camera. The captured images were then compared to analyze the stability of the nanofluid. Thus, the characterized nanofluid is consid-

ered stable when the particle size and dispersity remain constant over time.

• *Centrifugation method* In this method, nanofluid sedimentation was performed using a dispersion analyzer centrifuge.

Achieving long-term stability in nanofluids is crucial for their practical application, as it ensures consistent performance and prevents issues such as clogging in microchannels or sedimentation during storage. Researchers continue to explore methods for enhancing and maintaining the stability of nanofluids to maximize their efficacy in heat transfer and other relevant applications. Various methods can be used to improve the stability are:

Surfactant stabilization Surfactants are chemical compounds that can be added to nanofluids to provide electrostatic or steric stabilization. They form a protective layer around the nanoparticles, preventing agglomeration. Surfactants can be anionic, cationic, or nonionic, and their selection depends on the nature of the nanoparticles and base fluid.

Surface modification Nanoparticle surfaces can be modified to enhance their stability. Surface functionalization involves attaching molecules or polymers to the nanoparticle surface, which can provide repulsive forces between the particles, reducing agglomeration. Functionalization can be achieved through various methods, such as silane coupling agents, polymer coating, or ligand exchange.



Fig. 7 SEM and TEM image Ref. [23]

pH adjustment Changing the pH of the nanofluid can affect its stability by altering the surface charge of the nanoparticles. The choice of pH adjustment depends on the nanoparticle material and surface chemistry. By adjusting the pH, repulsive forces can be enhanced, hindering agglomeration.

Ultrasonication Ultrasonication involves subjecting a nanofluid to high-frequency sound waves, typically in the range of 20–100 kHz. The acoustic cavitation generated during ultrasonication helps disperse and deagglomerate nanoparticles. This process breaks down the large agglomerates into smaller particles, enhancing their stability.

Mechanical stirring Mechanical stirring or mixing with the nanofluid can help distribute nanoparticles evenly throughout the base fluid. Agitation disrupts agglomerates and promotes the uniform dispersion of nanoparticles. The intensity and duration of stirring should be optimized to prevent excessive energy input, which can lead to excessive heating.

Characterization of nanofluids

The process of determining and understanding the properties, characteristics, and behavior is referred to as characterization. The characterization of nanofluids involves measuring various physical and chemical properties such as thermal conductivity, viscosity, density, surface tension, composition, surface morphology, and stability. It is crucial to understand these properties as they affect the thermo-fluidic behavior of nanofluids in microchannels. Some common methods used for nanofluid characterization are as follows:

- 1. Scanning electron microscopy (SEM)—is used to study the distribution of materials on a surface.
- 2. SEM & EDS—is used to measure the elemental composition in a sample.
- 3. Transmission electron microscopy (TEM)—which is used to visualize the smallest structures in matter, produces high-resolution images.
- 4. FTIR analysis—was used to identify unknown compounds, determine the purity of the sample, and monitor the chemical reactions in real-time.
- 5. Transient hot wire—determines the thermal conductivity
- 6. Laser flash method—determines the thermal conductivity
- Rheometer—was used to study fluid properties such as dynamic viscosity, flow behavior (Newtonian/non-Newtonian).
- 8. DSC—To measure the specific heat capacity of the nanofluid as a function of temperature.

- 9. Oscillation method—is used to measure the density of nanofluid.
- 10. Pendant drop method—is used to study the surface tension of nanofluids, which is a property of the interface between the fluid and surrounding air or another medium.

Therefore, characterization of nanofluids is essential for understanding their behavior. Table 4 presents various characterizations of the nanofluids and instruments used for their measurements.

Base working fluid used in microchannel

Water, oils, glycols, and glycol-water combinations are commonly used as base fluids to create nanofluids. Figure 8 shows that among the different base fluids, water-based nanofluids have received the most attention from researchers, likely because of their lower cost and higher thermal conductivity. Owing to their potential as high heat transfer fluids in microchannels, glycol-based nanofluids have also attracted attention.

Nanomaterial used for nanofluid formation

The nanoparticles commonly used for nanofluid creation are metals, metal oxides, carbonaceous materials, and hybrid nanoparticles. Figure 9 shows the distribution of publications on nanofluids employing various nanomaterials in microchannels. Although metal oxides exhibit lower thermal conductivities than metals, they appear to be the most suitable option for creating nanofluids. This is because metal oxides are chemically stable and are resistant to oxidation. Moreover, certain metal oxides have a lower density than their corresponding metals, which could lead to fewer particle-settling problems in nanofluid formulations. Owing to its high thermal conductivity and low density, alumina is widely used as a metal oxide for nanofluid formation. Based on the nanomaterial used for nanofluid creation in the present study. The authors reviewed all the journals on nanofluids and categorized them into four main types.

(a) Nanofluids used in various microchannel geometries suspended with metallic nanoparticles.

Metallic nanofluids (e.g., Ag, Cu, Fe, Au, etc.) generate higher effective thermal conductivity values. Therefore, various researchers have focused on using metallic nanomaterial for nanofluid creation, as presented in Table 5. Mghari et al. [24] conducted a numerical analysis of the heat transfer in a single horizontal smooth square tube. According to the findings of the research, either elevating the mass flux from 80 to 110 kg m⁻²-s or increasing the concentration of copper









Fig. 8 Base fluid use in microchannels for nanofluids formation

nanoparticles by 5% has the potential to increase the heat transfer coefficient by 20%.

Abbassi and Aghanajafi [25] examined the incorporation of Cu nanoparticles into MCHS. The results of their research showed that employing a nanofluid significantly improved the heat transfer in the MCHS, and this advantage became even greater as the Re and particle concentration increased. Additionally, they demonstrated that if the flow regime transitions into the turbulent domain, the enhancement in heat transfer could be greatly amplified.

Diao et al. [26] analyzed the performance of a microchannel surface in a vapor chamber using Cu-R141b as the working fluid. The authors recommended that with a volume concentration of 0.001–0.01 percent, R141b-based Cu nanofluids may enhance the thermal performance of microchannel surfaces, especially at lower operating pressures.



Fig. 9 Nanofluids used in various microchannel geometries

Boudouh et al. [27] analyzed the convective boiling heat transfer in a vertical rectangular channel using copper–water nanofluids and deionized water. They found that in comparison with the temperature and pressure of the base fluid, the Cu–water nanofluid exhibited a lower surface temperature and local heat flux at the same flow rate.

Using porous media and the least square method, Hatami and Ganji [28] investigated the thermal performance of a MCHS employing a nanofluid composed of copper and water. They observed that raising the volume fraction of nanoparticles encouraged Brownian motion and facilitated greater heat transfer.

Simsek et al. [29] employed suspensions of silver nanowires to enhance thermal performance in a MCHS for the first time. According to the outcomes, the utilization of silver nanowire suspensions in MCHS could lead to a rise in heat transfer coefficient of up to 56%, while causing only a minor increment in pumping power.

Tehrani et al. [30] conducted a numerical analysis on flow and heat transfer of an Ag–water nanofluid under varying heat flux, while considering different volume concentrations and Hartmann numbers. They suggested that because the Re of nanofluids inside microchannels is often low, "utilizing a higher volume fraction to enhance the Nusselt number (Nu) would be counterproductive in micro and nanoflows." Shahsavar et al. [31] conducted a numerical investigation to enhance the performance of a liquid-cooled heat sink. In this study, a water/silver nanofluid was used as the coolant. The researchers focused on two operational variables: nanoparticle concentration and Reynolds number. They also examined the impact of a structural parameter, specifically rifling the inlet tube of the coolant. The results revealed that the overall hydrothermal performance of the heat sink with a rifled inlet was 1.073–1.541 times higher compared to the heat sink with a plain inlet.

Table 5 indicates that copper and silver are the most commonly used nanomaterials for preparing working fluids in research, likely due to their high thermal conductivity compared to other metallic materials. Based on the research on metallic nanofluids, it can be concluded that increasing particle concentration results in nearly a 50% improvement in heat transfer in the microchannel in most cases. However, this may also cause an increase in pressure drop.

(b) Nanofluids used in various microchannel geometries suspended with metallic oxides nanoparticles

Despite their poorer thermal conductivities than those of metals, metal oxides have been frequently employed in the formulation of nanofluids. Metal oxides (e.g., Al_2O_3 , CuO, TiO₂, SiO₂, etc.) have several benefits over metal nanoparticles, including oxidation resistance and chemical stability. Furthermore, some metal oxides have lower densities than metals, resulting in less sedimentation when they are used in nanofluid formulations. This concept is a popular research topic because it is a viable solution for satisfying the temperature management requirements of the MCHS and MCHE. Tables 6–11 represent the literature on metallic oxide nanoparticles for the formation of nanofluids used in various microchannel geometries.

The study conducted by Bhattacharya et al. [38] on the heat transfer properties of an $Al_2O_3-H_2O$ nanofluid flowing through a rectangular MCHS showed that an increase in nanoparticle concentration resulted in a more pronounced improvement in MCHS performance with the use of the nanofluid.

In a study conducted by Ali et al. [39], the thermal performance of a circular MCHS was evaluated in the range of $100 \le \text{Re} \le 350$, using swirl flow and nanofluid. The coolant was a water-Al₂O₃ nanofluid with nanoparticle volume fractions ranging from 0 to 3%. The results indicated that the MCHS with swirl flow and maximum nanoparticle volume fraction had the lowest thermal resistance and contact temperature.

Meanwhile, Heidarshenas et al. [40] utilized an ionic liquid–Al₂O₃ nanofluid to enhance heat transfer in a cylindrical MCHS. Their findings showed that the use of ionic liquid–Al₂O₃ nanofluid increased the Nusselt number by up to 40%.

The thermal performance of a trapezoidal microchannel was studied by Li and Kleinstreuer [41] using pure water and CuO–water with volume fractions of 1% and 4%, respectively. They found that with a modest increase in pumping

Table	5 Effect of me	tallic nanomatei	rial in MCHS and M	CHE on various	geometry				
S. no.	Study type	Geometry	Reynolds number	Nanoparticle	Particle size/nm	Particle conc./%	Max HT. gain/%	Outcomes	Ref.
-	Experimental	Rectangular	I	Cu	20	0.001-0.1	50	The impact of nanofluid on thermal resistance is more apparent at lower operating pressures than at higher ones	[26]
7					35	5-50 mg/L	I	The concentration of Cu nanoparticles enhances heat transfer coefficient, vapor quality, & local heat flow	[27]
б			20-71	Ag	50-100	0-0.00357	56	For all microchannel diameters, Ag-water nanofluids produce lower thermal resistance than DI water	[29]
4			< 1500		5-10	0.01-0.1	I	Both the heat transfer coefficient and the pressure drop of the (MCHS) increased as the flow rate and mass concentration of nanofluid increased	[32]
5	Numerical	Rectangular	10-200	Ag	10	0-4	I	Utilizing a higher volume fraction to enhance the Nu would be counterproductive in micro and nanoflows	[30]
9		Trapezoidal, Rectangular, Triangular	1–100		50	0-4	100	The convective heat transfer coefficient of the working fluid increases with an increase in the nanoparticle volume percent- age	[33]
7		Triangular	5-500		25-75	0-4	I	The friction coefficient and pumping power do not show a significant dependency on nanoparticle diameter	[34]
8		Trapezoidal	10,000- 16,000		1	0-4	I	The average Nu and convection heat transfer coefficient rise as Re rises	[35]
6		Circular	1-1000	Cu	1	2-4	I	Reducing the channel height may result in the combination of boundary layers and the loss of the entrainment effect. Thus, decreasing the channel area may not necessarily lead to an increase in total heat flux	[36]
10		Parallel Plates	< 1400	Cu, NEPCM	36	1.3–5	I	Compared to both NEPCM and water, Cu-water nanofluid exhibits a higher average heat transfer coefficient	[37]
11		Square	< 700	Cu	I	0-5	20	Enhancement of the heat transfer coefficient by 20% may be achieved by either increasing the volume percentage of Cu nanoparticles by 5% or by raising the mass flow from 80 to $110 \text{ kg m}^{-2} \text{ s}^{-1}$	[24]
12		Rectangular	100- 2000	Cu	23	06	I	Transitioning to the turbulent regime of fluid flow can signifi- cantly increase the heat transfer enhancement of the nanofluid	[25]
13	Analytical	Rectangular	I	Cu	1–25	06	I	Increasing the volume fraction of nanoparticles results in an increase in Brownian motion, which in turn causes a decrease in the temperature differential between the coolant and the wall	[28]

S.no.	Study type	Reynolds number	Particle size/nm	Particle Conc./%	Max. H.T gain	Outcomes	Ref.
1	Numerical	200–1200	38	0–4	-	If temperature-dependent properties are incorporated, the temperature and aver- age shear stress on the bottom surface decrease	[47]
2		150-450	38.4	0–2	_	Compared to the constant property approach, the variable property tech- nique results in a higher heat transfer coefficient and Nusselt number	[48]
3		<450	-	0.5–3.5	-	Using a tear-drop dimple structure in combination with nanofluid can increase heat transfer while reducing pressure loss	[49]
4		0.025–250	-	0–2	-	The formulation of the Buongiorno model causes the incorporation of Brownian motions	[50]
5		5–300	25–100	0–2	-	Using nanoparticles with decreasing diameters and increasing the nanopar- ticles volume percentage increases heat transfer	[51]
6		100-400	_	0–4	12.67	Increasing either the volume percentage of nanoparticles or the aspect ratio of the fins may lead to an increase in heat transfer	[52]
7		< 500	36	1–4.5	-	The use of nanofluids as a cooling medium in electrical devices results in an increase in the power required for fluid pumping	[53]
8		200–1000	40	0.1–0.2	130	Increasing Re, increasing volume con- centration and decreasing nanoparticle size all result in an increasing average Nu	[54]
9		-	-	0–5	10.93	With the increase in Knudsen number, both temperature gradient and average Nu decrease	[55]
10		100–1000	_	1–5	_	Compared to a MCHS cooled with pure water, the use of nanofluids results in a slight increase in pressure loss across the system	[56]
11		5–150	_	0–5	-	The overall increase in cooling perfor- mance of nanofluid in microchannel system becomes more effective when water is employed as base fluid	[57]
12		-	_	0–1	-	The enhanced thermal performance of nanofluid-cooled MCHS is attributed to the intake flow velocity and effective thermal conductivity of nanofluid	[58]
13		10–1000	25	0.5–1.5	_	Increasing the volume percentage of solid nanoparticles and decreasing the size of the nanoparticles can enhance heat transfer	[59]
14		120–480	29,38.4, 47	0–4	-	Pumping power and frictional entropy contribution both decreases as heat transfer entropy diminishes	[60]

Table 6 Numerical, experimental, and analytical analysis of the effect of Al_2O_3 and water base nanofluid in a rectangular cross section microchannel

A	comprehensive	review	of thermal	enhancement	techniques in	microchannel	heat exchangers

Table	6 (continued)						
S.no.	Study type	Reynolds number	Particle size/nm	Particle Conc./%	Max. H.T gain	Outcomes	Ref.
15		_	33	0–2	_	The effect of inertia on the temperature profile of the channel wall is negligible; however, it has a substantial impact on the temperature profile of the coolant and the overall thermal resistance	[61]
16		250	20	0–3	-	The enhancement in MCHS performance due to the utilization of nanofluid becomes increasingly noticeable with an increase in the particle concentration	[38]
17		<1500	40	0–4	29	By applying a magnetic field, the thermal boundary layer formation is disturbed, leading to an improvement in heat transfer	[62]
18		150–700	0–2.5	-	-	Microchannel outperforms when elliptical ribs are employed instead of diamond ribs or no ribs	[63]
19		7–15	0–5	_	-	Raising the input velocity to maintain a constant Re, rather than increasing the particle concentration, is the primary way to raise the Nu for a given Re	[64]
20		5–25	-	0-4	17	The magnetic field does not influence heat transfer, but it may increase fric- tion up to 86%	[65]
21		-	_	0–2.5	-	Heat transfer coefficient and Nu fluctua- tion both decreases with flow direc- tion as the boundary layer thickness increases	[66]
22		1–100	50	0–4	350	An increase in particle volume fractions improves heat transfer & friction factor	[<mark>67</mark>]
23		_	-	0–2	8.49	The temperature of the nanofluids in the microchannel rises with the curve, con- tradicting the linear growth concept	[68]
24		200–1500	_	1–5	-	Throughout the channel length, there is an increase in the temperature of both the coolant and MCHS for all values of nanoparticle volume fractions	[69]
25		15,000-30,000	50	0–4	237	Fluid mixing is influenced by variations in the attack angle of the ribs and the creation of vortexes within the channel	[70]
26	Analytical	0–200	40	0–4	70	The thermal efficiency of nanoparticles may be improved by as much as 70% by lowering their diameter below the threshold value	[71]
27	Experimental	45-80	43	0.1–0.25	-	The thermal efficacy of nanofluids is quite high, which encourages the use of nanofluids in MCHS	[72]
28		-	-	0–2	-	The utilization of nanofluids in ribbed microchannels results in increased Nu and friction coefficient compared to ordinary microchannels. Additionally, this improvement is more significant with increased rib width	[73]

 $\textbf{Table 6} \hspace{0.1in} (continued)$

S.no.	Study type	Reynolds number	Particle size/nm	Particle Conc./%	Max. H.T gain	Outcomes	Ref.
29		_	40	0–0.2	-	Nanofluid considerably reduces flow instability without causing nanoparticle deposition	[74]
30		226–1676	33	0–2	70	A heat sink cooled by nanofluid has a higher average heat transfer coefficient compared to one cooled by water, making it superior in terms of heat dis- sipation performance	[75]
31		-	80	0–0.5	27	Nanofluids with higher concentrations exhibit higher thermal conductivity and viscosity	[76]
32		_	25	0.001-0.1	-	Nanoparticles in the liquid phase can significantly affect bubble dynamics formation	[77]

Table 7 Numerical and experimental analysis on the effect of Al_2O_3 and water base nanofluid in a circular microchannel

S.no	Study type	Reynolds number	Particle size/nm	Particle Conc./%	Max. H.T gain	Outcomes	Ref
1	Numerical	-	1–100	1-4	_	Nu variation diminishes along the flow direction	[78]
2		500–1900	38	1–4	_	Nanofluids temperature-dependent characteristics boost heat transfer while decreasing entropy, shear stress, and pressure loss	[79]
3		15–100	13–47	1–5	_	The thermal properties would be better when nanofluid is utilized as the working fluid	[80]
4		<250	29–47	0–4	_	The use of nanofluid has a major effect on pumping power, which rises with particle volume fraction and Re	[81]
5		0–58	36	0–2	-	Maximum thermal enhancement factor for symmetric ribs is 2.2517	[82]
6		2.7–87	36	9–13	_	The temperature-dependent fluid characteristics may have a substantial impact on the best outcomes	[83]
7		5–11,980	23	0–5	83	Laminar nanofluid flow enhances heat transfer more than turbulent nanofluid flow does	[84]
8	Experimental	200-1000	36	0–2	-	Nanoparticles cause catastrophic failure in two-phase cooling by depositing in massive clusters at the channel outlet	[85]
9		_	_	0–0.77	10.6	The Nu of nanofluids is higher than that of deionized water, and it increases with the growth of Re and particle concentration	[86]

power, the nanofluids enhanced the thermal performance of the microchannel.

Yang et al. [42] investigated a trapezoidal MCHS utilizing a CuO–water nanofluid as the cooling fluid. The results indicated that the two-phase model was more accurate than the single-phase model.

Duangthongsuk and Wongwises [43] conducted an experimental investigation of the heat transfer and pressure

drop in a zigzag MCHS. The study found that there was a 2–6% improvement in heat transfer performance between the cross-cutting zigzag heat sink (CCZ-HS) and continuous zigzag heat sink (CZ-HS). Additionally, the particle concentration had a significant impact on the heat transfer, but it did not affect the pressure drop.

Martinez et al. [44] investigated the thermal characterization and stability of water–ZnO nanofluids in a rectangular

Table 6 Numerical, experimental, and analytical analysis on the effect of AI_2O_3 and water base hanomulu in a parallel plate MCHS & W	Table 8	Numerical, experimental,	, and analytical analysis on	the effect of Al_2O_3 and wa	ater base nanofluid in a parallel p	late MCHS & MCH	E
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S.no.	Study type	Reynolds number	Particle size/nm	Particle Conc./%	Max. H.T gain	Outcomes	Ref.
1	Numerical	-	20	2–6	-	Nanomaterials facilitate the flow of fluid toward the wall as heat flux increases, thereby enhancing heat transfer	[87]
2		0.5–2	-	0-0.2	-	Entropy production reduces as the nanoma- terial volume % and suction Re increases, whereas the Grashof number, radiation parameter & conduction–radiation factor decreases	[88]
3		5–50	36	0-4	-	Recirculation zones generated behind the baffles are the major mechanism for improved heat transfer	[89]
4		<16	47	0-4	21	The enhanced thermal conductivity of nano- particles leads to a higher flow of energy through the fluid	· [90]
5	Analytical	<1	25	0–2	-	Heat transfer is reduced when the volume % of nanoparticles increases	[91]
6		-	1–10	0.02–0.1	-	Smaller nanoparticles work better in mag- netic fields than bigger ones	[92]
7		150	5	0-4	_	Under symmetric heating, nanofluids show the highest increase in heat transfer coef- ficient, with an average enhancement of 47%, compared to asymmetric heating	[93]
8		<2300	60.4	0–8	-	In the laminar regime considering the effect of viscous dissipation, the heat transfer coefficient significantly decreases with increase in nanoparticle volume percent- age	[94]
9		_	20	2–10	-	A strong magnetic field and high slip veloc- ity at the walls have a negative impact on the thermal performance of nanomaterials	[95]
10		_	1–10	2–10	-	The thermophysical parameters of nanoflu- ids have little effect on their flow fields and heat transfer behavior	[96]
11		-	_	0–8	-	The heat transfer performance improves with an increase in the volume fraction of nanomaterials	[<mark>97</mark>]
12	Experimental	-	-	0.001	_	With increase in mass flow and initial sub- cooling, critical heat flux rises	[<mark>98</mark>]

MCHS with Re ranging from 200 to 1200. The numerical findings revealed that using nanofluids promotes heat transfer at low Re, with the greatest increase in heat transfer coefficient (42.33%). At a concentration of 1 mass%, there was also a decrease in the base temperature of the microchannel, which was more noticeable at a low Re.

In addition, several researchers have conducted comparative investigations on various metallic oxide nanoparticles employed in microchannels. Mohammed et al. [45] investigated the influence of Al_2O_3 , Ag, CuO, diamond, SiO₂, and TiO₂ nanofluids on the cooling performance of triangular MCHS. They found that the addition of nanoparticles to the coolant resulted in a decrease in the thermal resistance of the triangular MCHS, with diamond-H₂O nanofluid showing the greatest improvement at a nanoparticle concentration of 1%. Salman et al. [46] numerically analyzed the thermal performance of microtubes. Various types of nanofluids, including Al_2O_3 , CuO, SiO₂, and ZnO, were utilized in the study. The nanoparticles had sizes of 25, 45, 65, and 80 nm, and the volume fractions ranged from 1 to 4%. Ethylene glycol was chosen as the base fluid for the nanofluids. According to their findings, the SiO₂–ethylene glycol nanofluid had the highest Nu. The Nu increased with the volume fraction in all circumstances but decreased as the diameter of the nanoparticles increased.

Table 6 displays a comparison of numerical, experimental, and analytical analyses investigating the impact of Al_2O_3 and water-based nanofluids on rectangular microchannels. Based on the table's results and study type, it can be inferred that more than half of the research on Al_2O_3 nanomaterial

S.no.	Study type	Reynolds number	Particle size/nm	Particle Conc./%	Max. H.T gain	Outcomes	Ref.
1	Numerical	1–100	10	0–5	100	In laminar forced convection, for Reynolds numbers below 10, the influence of Brownian force on flow and heat transfer properties is significant	[99]
2		100-1000	30	1–6	-	A novel correlation has been introduced to compute the Nu as a function of Re, Prandtl number, and blockage ratio	[100]
3		50	10	0.4	-	Nanofluid enhances heat transfer in both porous media and fin approaches	[101]
4		10,000–60,000	100	0–4	-	Using semi-attached rib in microchannel produces greater vortices, resulting in enhanced fluid layer mixing	[102]
5	Experimental	_	20-80	0.2–0.4	-	Elevating the bulk temperature of nanoflu- ids helps to prevent the aggregation of particles into larger clusters	[103]
6		<1800	40	0-0.2	40	At a Re of 1150, the heat transfer coef- ficient of nanofluid with a volume fraction of 0.2 exhibited an increase of approximately 40% compared to deion- ized water	[104]
7		< 5000	29	0-4.5	_	At a specific Re, the energy efficiency of nanofluids, as determined by the ratio of heat transfer to pumping power, is still lower than that of water	[105]

 Table 9
 Numerical and experimental investigation of the effect of CuO nanofluid in a rectangular microchannel

Table 10 Effect of TiO based nanofluid in a rectangular cross section microchannel

S.no.	Study type	Reynolds number	Particle size/nm	Particle Conc./%	Max. H.T gain	Outcomes	Ref.
1	Numerical	_	-	0.01–0.9	-	Nanofluids are an excellent choice for designs that need lower volume flow rates and have lower nanoparticle vol- ume fractions	[106]
2		100–250	21-60	1–2.3	-	Approximately 14% is the highest normal- ized efficiency of the longitudinal vortex generator microchannel in comparison with the plain channel. In addition, the use of nanofluid may boost the normal- ized efficiency by 27%	[107]
3		200-1200	6	1–3	19.66	At low Re, the findings indicate that the use of nanofluids and the lowering of microchannel height boost heat transfer	[<mark>108</mark>]
4	Experimental	50-850	25	0.25–2	_	In comparison with pure water, TiO ₂ parti- cles in the base fluid produced greater heat transfer and did not create an exces- sive rise in pressure drop	[109]
5		100–750	25	0–2	39.7	The heat resistance of the base fluid is reduced by introducing particles with an average diameter of less than 25 nm	[110]
6		250-1700	-	0–2	-	Using the Maxwell model to measure thermal conductivity provides an accu- rate estimation of the Nu	[111]
7		-	15	0-0.1	-	Nanofluids have distinct droplet-forming features based on temperature	[112]

e Geometry	 Reynolds number	Nanoparticle	Particle size/nm	Particle Conc./%	Max. H.T gain	Outcomes	Ref.
ntal Semicircle, trapezoidal, square	250-850	Al_2O_3	40–50	0-0.25	4.6	The Nusselt number (8.54% & 26.4%) and heat transfer rate (3.13% &5.87%) are higher in the trapezoidal channel compared to the square and semicircular channels	[113]
Trapezoidal	190–1020	Al_2O_3	56	0-0.26	15.8	Replacing water with nanofluids reduces thermal resist- ance of the MCHS at almost constant pumping power	[114]
Cylindrical	006 >	CuO	25	0.05-0.3	23	Pure water has lower Nu compared to nanofluids with 0.05 mass%, 0.1 mass%, and 0.3 mass% concentration, with percentage increases in Nu being 17%, 19%, and 23%, respectively	[115]
	006 >	Cu	25	0.05-0.3	I	The thermal resistances decreased by up to 21% when the mass fraction of particles increased from 0.05 to 0.3 mass%	[116]
Circular	500- 4000	Al ₂ O ₃ TiO ₂ SiO ₂	13 10–25 18	0-1	15.3	Al ₂ O ₅ nanofluid with a 1% volume concentration was found to have the greatest thermal performance	[117]
Rectangular	I	SiO ₂	35-190	1.4-7	I	The increase in viscosity of nanofluids can be explained using a conventional model, but with a modification based on the particle size, which affects the crowding factor	[118]
	100-350	Al ₂ O ₃ SnO ₂	I	0-5 0-1	13 14	The findings suggest that using 5% Al ₂ O ₃ and 1% SnO ₂ nanofluids in MCHE resulted in a heat transfer improvement of 13% and 14%, respectively, compared to the base fluid	[119]
	<100	CuO SiO ₂	43	0.1-0.25	32.8	Al ₂ O ₃ -water nanofluid outperforms SiO ₂ -water nanofluid in heat transfer due to its higher thermal conductivity	[120]
	I	Bi ₂ O ₃ Fe ₃ O ₄ TiO ₂ SiO ₂	200–300 90–210 50–100 <100	I	I	There exists a specific concentration limit for all nanoflu- ids, beyond which increasing the concentration does not lead to any further reduction in pressure drop or system drag	[121]
	200-500	Al ₂ O ₃ TiO ₂	S S	0-1	42.9	The thermal conductivity and dynamic viscosity of Al_2O_3 and TiO_2 nanofluids are positively affected by an increase in particle volume fraction	[122]
l Trapezoidal	<1200	CuO	100	1-4	I	Taking viscous dissipation into account, it is shown that pressure drop fluctuates relatively slow	[123]
	100-900	Al ₂ O ₃ TiO ₂	Ω Ω	0.1–1	36.6	When compared to a MCHS made of stainless steel at $Re = 900$, using copper instead can increase the total thermal resistance by up to 76%	[124]
Helical	I	Al ₂ O ₃	I	I	I	Helical-shaped geometry can greatly enhance convective heat transfer, and reducing the helix radius can further improve the thermal performance	[125]

	Ref.		reducing the aspect [126] flow velocity within the	educing the aspect [126] flow velocity within the e is lost by all particles [127] t transfer is greatest least for H ₂ O-SiO ₂	educing the aspect [126] flow velocity within the e is lost by all particles [127] t transfer is greatest least for H ₂ O-SiO ₂ nce, the Nu is at its [128]	educing the aspect [126] flow velocity within the e is lost by all particles [127] t transfer is greatest least for H ₂ O-SiO ₂ nce, the Nu is at its [128] the thermal conductivity [129] ecreases, resulting in a	educing the aspect [126] flow velocity within the e is lost by all particles [127] t transfer is greatest least for H ₂ O-SiO ₂ nce, the Nu is at its [128] the thermal conductivity [129] ecreases, resulting in a agenetic field initially [130] the to heat transfer, but it	educing the aspect [126] flow velocity within the e is lost by all particles [127] t transfer is greatest least for H ₂ O-SiO ₂ nce, the Nu is at its [128] nce, the Nu is at its [129] e thermal conductivity [129] ecreases, resulting in a agnetic field initially [130] the to heat transfer, but it nanofluid has a lower [131]
	les	the convergence angle and reducin the channel increases the flow ve	lel	ict the same amount of pressure is los outed in water; however, heat transl of -diamond nanofluids and least fi luids	the same amount of pressure is los outed in water; however, heat transl of -diamond nanofluids and least fo luids st	the same amount of pressure is los outed in water; however, heat trans) of -diamond nanofluids and least fo luids tuid enters the channel entrance, th est volume fraction increases, the therr ncreases and heat capacity decrease srature drop	the same amount of pressure is los outed in water; however, heat transl O -diamond nanofluids and least fi inids luid enters the channel entrance, th est volume fraction increases, the therr nereases and heat capacity decrease rature drop lication of a non-uniform magneti es the entropy production due to he quently increases	the same amount of pressure is los outed in water; however, heat transl of -diamond nanofluids and least fi luids luid enters the channel entrance, th est volume fraction increases, the therr oreases and heat capacity decrease arature drop neceases and heat capacity decrease esture drop nectases and heat capacity decrease esture drop stature drop nection of a non-uniform magneti es the entropy production due to he quently increases same volume fraction, TiO ₂ nanofl al resistance than SiC
Dutcomes Raising the converge ratio of the channe	Raising the converge ratio of the channe	CITAIIIEI	Almost the same am distributed in wate for H ₂ O -diamond nanofluids		When fluid enters th greatest	When fluid enters the greatest As the volume fracti also increases and temperature drop	When fluid enters the greatest As the volume fracti also increases and temperature drop The application of a reduces the entrop' subsequently incre	When fluid enters the greatest As the volume fracti also increases and temperature drop The application of a reduces the entrop; subsequently incre For the same volume thermal resistance
IX. H.T gain O	R		4		м	W A	X < F	х т т
nc./% Max	8	DV	I		I	1 1	1 1 1	1 1 1 1
Particle Cc	~~~~~~~ m т	0-0.5	0-1	000	0-0-0	0.4-0.8	0.4-0.8	0.4-0.8 0-4 1-9
•	ticle size/nm							
	cle Part	10	I	13		I	30	- 30
	Nanopartic	TiO_2	SiO ₂	$\mathrm{Fe}_{3}\mathrm{O}_{4}$	۲ م	t 5	7	SiC, JiO2
Revnolds number		100-600	< 100	140 - 1400		140-1400	140-1400	140-1400
	Geometry	Converging	Rectangular					
	Study type							
	S.no.	14	15	16		17	17 18	17 18 19

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for nanofluid production is based on numerical analysis. The table also indicates that the use of smaller diameter nanoparticles and increasing the volume percentage of nanoparticles enhances heat transfer. Moreover, higher heat transfer coefficients are observed in flow regimes with higher Re.

(c) Hybrid nanofluids used in various microchannel geometries

Hybrid nanofluids are advanced nanofluids that are created by mixing two distinct nanoparticles in a base fluid. Preparation method of hybrid nanofluid is shown in Fig. 10. Hybrid nanofluids have superior thermal characteristics compared with base fluids and nanofluids. These fluids exhibit better characteristics than ordinary fluids, such as

- Offer superior thermophysical properties in comparison with mono-nanofluids.
- High dispersion stability and Brownian motion of particles.
- A remarkable increase in thermal conductivity with varying particle concentrations.
- Reduction in pumping power compared with conventional fluid power.
- High surface area and high heat transfer between fluid and particles.
- Increased control over thermodynamic and transport properties.

Turcu et al. [133] were the first to use polypyrrole–carbon nanotubes (CNTs) and multiwall carbon nanotubes (MWCNTs) on magnetic Fe_3O_4 hybrid nanoparticles to create hybrid nanofluids. Jha et al. [134] combined silver nanoparticles with multiwall carbon nanotubes (MWCNTs) to create hybrid nanofluids. The results show the improved



Fig. 10 Preparation of hybrid nanofluid

thermal properties of the hybrid nanofluids. Suresh et al. [135] created hybrid nanofluids by mixing Al₂O₃ and Cu and found that there was an enhancement in thermal conductivity of 12.11% with a volume concentration of 2%. To improve the thermal performance of MCHE, an experimental investigation was conducted by Yushuang Huang et al. [136]. They incorporate β -cyclodextrin-ZrO₂ as a nanoparticles and ethylene glycol as the base fluid for construction of nanofluids. They found that fabrication of nanofluids utilizing β-cyclodextrin-modified ZrO₂ nanoparticles holds significant potential for enhancing heat transfer in microelectronic microchannels. Table 12 shows numerous studies in MCHS and MCHE that use hybrid nanofluids as their working fluid. Table 12 shows that nearly 50% of hybrid nanofluid research relies on numerical analysis. The most commonly used nanomaterials for creating hybrid nanofluids are alumina and copper oxide. Additionally, rectangular cross sections are frequently utilized for constructing microchannels in comparison with other geometries. Based on the outcomes of the above literature survey, it can be concluded that increasing particle concentration and Re leads to improved heat transfer in the microchannel, although this may also result in higher pumping power requirements. Mansouri et al. [137] conducted an experiment to assess the convective heat transfer of a hybrid nanofluid consisting of graphene oxide and gold in a CPU. They varied the concentrations of graphene oxide and gold (ranging from 0.0044 to 0.0114% by mass) as well as the Reynolds number (ranging from 676 to 2185) to optimize the overall performance of the device. The experimental findings indicated that the nanofluid composed of graphene oxide and water, decreased the CPU's surface temperature by 10.6% and 16.2%, respectively, compared to using DI water alone.

Srivastava and Sahoo [138]conducted an experiment to examine the impact of nanoparticles with different shapes on the thermo–hydro performance of a microchannel heat sink (MCHS). The experiment utilized water as the reference fluid. The results showed that the hybrid nanofluid composed of dissimilar-shaped nanoparticles demonstrated improved performance in terms of heat transfer coefficient, Nusselt number, as well as inlet and outlet exergy.

(d) Nanofluids used in various microchannel geometries suspended with carbon nanoparticles

Studies have investigated the cooling performance of MCHS using carbon nanotubes (CNT). Ebrahimi et al. [155] investigated the cooling performance of an MCHS using carbon nanotubes (CNT). It is found that increasing the nanolayer thickness of multiwalled carbon nanotubes (MWCNTs) decreased the MCHS temperature gradient.

Arabpour et al. [156] performed a numerical simulation of an MCHS using kerosene nanofluid/MWCNTs and found

S.no	Study type	Geometry	Reynolds Number	Nanoparticle	Particle size/nm	Particle Conc./%	Max. H.T gain	Outcomes	Ref
1	Numerical	Trapezoidal	300-1100	Al ₂ O _{3,} CuO	20–60	0–8	_	The findings dem- onstrate that when particles are 34 nm in size, the average Nu rises fast; however, when particles are 60 nm in size or larger, heat transfer is not significantly affected	[139]
2		Rectangular	200–600	Al ₂ O _{3,} CuO	43 29	0–4	-	For higher and lower Re, the pumping power and performance index are not affected by volume fraction	[140]
3			100-800		30	1–4	39	Higher heat transfer improvement may be seen by increasing the volume percentage of nanoparticles	[141]
4			100–900		29–36	0–5.3	53.06	Irreversibility in the MCHS with longitu- dinal vortex generator might be decreased by employing nanofluids as the working fluid	[142]
5			-		35–50	0–4	-	Cu–water nanofluid is a better thermal conduc- tor than Al ₂ O ₃ –water nanofluid	[143]
6			-		-	1–5	-	When flow rates are large, the volume flow rate dominates heat transfer, and nanoma- terials have little effect on the heat absorption	[144]
7			-	Cu, Diamond	6 2	0–1	-	Using water–diamond nanofluid in a MCHS at a fixed pumping power of 2.25 W can improve its cooling performance by around 10% compared to pure water	[145]
8		Trapezoidal grooved	266–798	Al ₂ O _{3,} CuO, ZnO, SiO ₂	25	0–4	_	In grooved MCHS, sec- ondary flow increases both the hydrodynamic & thermal boundary layer disturbances, resulting in higher heat transfer	[146]

Table 12 Hybrid nanofluids used in various microchannel geometries

Table 12 (continued)

S.no	Study type	Geometry	Reynolds Number	Nanoparticle	Particle size/nm	Particle Conc./%	Max. H.T gain	Outcomes	Ref
9		Semicircle	-	CuO, Al ₂ O ₃	28.6–29 38.4–47	_	_	Enhanced heat transfer can be achieved by raising both the volume fraction of nanoparticles and Re	[147]
10		Parallel Plates	10–100	Al ₂ O _{3,} Ag	10	0–4	-	Increasing slip coef- ficient reduces Nusselt number (Nu), while higher Hartmann numbers lead to larger slip velocity	[148]
11	Experi- mental	Rectangular	200–500	Al ₂ O _{3,} TiO ₂	5 5	0–1	42.9	Using Al ₂ O ₃ nanofluids, a fan-shaped MCHS exhibits better heat transfer performance compared to a rectan- gular MCHS	[122]
12			-	Nano PCM	120	0–3	-	The heat transfer coef- ficient of a slurry containing 30% bare indium nanoparticles can achieve up to $47,000 \text{ W m}^{-2} \text{ K}^{-1}$ when the flow rate is 3.5 mL s^{-1}	[149]
13			500– 2000	Al ₂ O _{3,} CuO	20 40	0–1	49 27	CuO nanoparticles in a water-based fluid are more prone to deposi- tion than Al ₂ O ₃ , but they exhibit superior heat transfer perfor- mance.	[150]
14		Serpentine	100– 1500	CuO, Al ₂ O ₃	15	0-0.3	_	Compared to Al ₂ O ₃ -H ₂ O and base fluids, CuO- H ₂ O nanofluid has a higher heat transfer coefficient	[151]
15	Analytical	Rectangular	_	Al ₂ O _{3,} CuO	25-45	0–4	_	An increase in nanopar- ticle volume fraction enhances Brownian motion, which signifi- cantly affects the heat transfer process by dissipating heat to the surroundings	[152]
16			-	Cu, Al ₂ O _{3,} Ag, TiO ₂	25-45	0–8	-	Increasing the volume % of nanoparticles enhances Brownian motion, reducing the temperature difference between the coolant and the wall	[153]

Table 12 (continued)

S.no	Study type	Geometry	Reynolds Number	Nanoparticle	Particle size/nm	Particle Conc./%	Max. H.T gain	Outcomes	Ref
17		Circular	10,000	Al ₂ O _{3,} Cu	_	2–6	-	Compared to the larger nanoparticles, smaller nanoparticles gener- ated less entropy in nanofluids of all concentration	[154]

that Nu was strongly influenced by the application of an oscillating heat flux at Re values of 10 and 100.

Studying the impacts of porous media on fluid flow and heat transfer in a microchannel filled with MWCNT/Oil Nanofluid. Nojoomizadeh and Karimipour [157] studied the impacts of porous media on fluid flow and heat transfer in a microchannel filled with MWCNT/oil nanofluid and found that a higher Re resulted in a decrease in the heat transfer time between the nanofluids and walls, resulting in a higher local Nusselt number. Table 13 lists various carbonaceous nanofluids used in MCHE and MCHS.

Table 13 indicates that over 50% of research on carbon nanomaterial suspended nanofluids relies on numerical analysis. Rectangular cross sections are also commonly used in constructing microchannels, as noted in the table. According to the literature survey, the use of carbon nanoparticles in nanofluid creation leads to a decrease in thermal radiation and improved thermal performance at high temperatures. Furthermore, the enhancement in heat transfer is more prominent at higher Re.

Flow disruption in MCHS

To enhance heat transfer performance, flow disruption is an effective approach that increases mixing and heat transfer by inducing flow instabilities. Turbulent flow is a prevalent method for flow disruption, but in many cases, low velocities or small hydraulic diameters prevent the flow from reaching the crucial Reynolds number. To overcome this, efforts are being made to introduce geometrical alterations to the channel sidewalls, such as grooves, ribbed channels, wavy channels, dimples, and fins, which act as periodic disturbance promoters. These promoters induce self-sustaining oscillations, leading to flow instability and improved mixing. Many studies have investigated the use of different disturbance promoters to enhance flow mixing in conventional channels.

Flow disruption in MCHS introduces various types of wavy channels

Rectangular straight channels are a common choice for MCHS due to their low pumping power and laminar flow

resulting in almost straight streamlines. However, these channels have several disadvantages. Firstly, the heat transport is poor due to insufficient fluid mixing caused by the linear streamlines. Secondly, the flow and heat transfer boundary layers thicken throughout the flow path because of the single-direction flow characteristics, leading to a larger temperature difference across the channels, especially at high heat fluxes. Thirdly, these channels are not effective in removing local high heat fluxes in microelectronic devices with hot spots. To overcome these challenges, several theoretical, experimental, and computational methods have been used to enhance the flow and heat transfer performance of MCHS by introducing different channel designs, such as grooves, ribbed channels, wavy channels, dimples, and fins, that promote flow instability and mixing.

When a fluid flows through a curved channel, it experiences not only primary motion but also a secondary motion in the plane of the cross section, which is referred to as the Dean vortex. The Dean vortices arise from centrifugal forces that act on the fluid as it flows through the curved channel. The presence of these vortices induces flow components to stretch and fold, which enhances the fluid mixing and heat transfer. The Dean vortices have been shown to be particularly effective at promoting mixing and heat transfer in microchannels, where the low Reynolds numbers limit the potential for turbulent flow. Consequently, many researchers have investigated the use of curved channels or modified channel geometries that induce Dean vortices as a means of improving the flow and heat transfer performance of microchannels. Sui et al. [165] proposed a new design for an MCHS, which was influenced by Dean vortices. Instead of using straight channels, they suggested using wavy channels that showed superior heat transfer performance when compared to straight microchannels of equivalent cross section. However, the use of wavy channels resulted in a pressure drop penalty, which could be offset by enhancing the heat transfer capability.

In addition, Sui et al. [166] performed experiments to compare the performance of MCHS with wavy channels and those with straight channels. They calculated both the overall Nusselt number and the friction factor to confirm the superior performance of the wavy design. Wavy MCHS with rectangular cross sections and amplitudes ranging from

Tab	le 1	3	Nanof	luids	used	in	various	MCHS	&	MCHE	sus	pended	with	carbon	nano	particl	es
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S.no.	Study type	Geometry	Reynolds number	Particle size/nm	Particle conc./%	Max. H.T	Outcomes	Ref.
1	Numerical	Helical	1–100	30	0-0.25	_	The increase in Nu is more significant at higher Re when the slip coefficient and mass percentage of nanoparticles are increased	[158]
2		Rectangular	-	25	0–1	-	Increasing nanolayer thickness in MCHS enhances thermal conductivity and reduces the temperature gradient	[155]
3			10–100	-	-	-	Addressing thermal radiation in the near-field media can lead to further improvement in heat transfer in microchannels using nanofluids	[159]
4			10–100	_	0–8	-	Using oscillating heat flux has a substantial impact on the profile figure of the Nu in various Reynolds numbers	[156]
5			150–700	_	0–8	-	As Re and nanoparticle volume fraction increase, heat transfer increases and thermal resistance decreases	[160]
6			0.1–10	30	0-0.4	-	The rise in the local Nu would be higher, for higher Re, low porosity and Darcy	[157]
7			-	9.2 nm 1.5 μm	0-0.1	13	Thermal resistance is reduced by 3% at 40 °C when CNT nano- fluid is used in place of water	[<mark>161</mark>]
8		Parallel Plates	0–100 1592– 478	-	0–0.25	30	It is noted that a lower Darcy Number results in a greater local Nu and porous medium causes higher slip velocity	[162]
9	Analytical	Rectangular	-	9–10 nm 15 μm	-	13	Nanofluids as working fluids decrease overall thermal resist- ance and improve the thermal performance at high tempera- tures	[163]
10	Experimental		100–1400	-	0.01–0.1 mass	29	Increasing flow rate and mass concentration enhances heat transfer coefficient in MCHS, while higher heat fluxes have minor impact	[164]

125 to 500 m were investigated numerically by Mohammed et al. [167]. According to their findings, the friction factor and wall shear stress increased in direct proportion to micro-channel amplitude.

Liquid-cooling parallel-flow and counter-flow doublelayer wavy MCHS with Re of 50–110 were studied by Xie et al. [168]. The findings show that the counter-flow doublelayer wavy MCHS operates better at higher flow rates and provides a more consistent temperature rise. Using nanofluids as coolants, Sakanova et al. [169] investigated for the first time how the wavy walls of an MCHS promote heat transfer. The findings revealed that the wavy MCHS outperformed a regular rectangular MCHS. There is a 5.34–24.1% increase in heat transfer and a pressure drop of around 150–421.7%. Chiam et al. [170] conducted a numerical investigation to study fluid flow in microchannels with secondary branches in the Re range of 50–200. The numerical results show that the heat transfer performance of the system can be improved by adding extra branches. Pandey et al. [171] conducted a numerical analysis to assess the performance of a straight MCHE with wavy channels. Their findings indicate that wavy channels outperform straight channels in terms of thermal performance. On the other hand, when considering pumping power, straight channels exhibit better characteristics. Table 14 represent various studies on wavy channels, along with the most important conclusions from each.

Flow disruption in microchannels by introducing various types of ribs

Several experimental and computational studies have been carried out to assess the impact of ribs on the thermohydraulic efficiency of MCHS & MCHE. Ribs are implemented to enhance heat transfer by disrupting the thermal and hydraulic boundary layers. These ribs are frequently referred to as turbulators or roughness components, respectively. Ribs can also promote flow mixing by producing vortices and causing chaos during advection. However, the heat transfer boost provided by the ribs was accompanied by a large pressure loss penalty. Consequently, optimizing the ribs was necessary to ensure a lower pressure drop. Table 15 presents the impact of ribs on the hydrothermal performance of MCHS and MCHE.

In an experimental and numerical analyses, Wang et al. [177] examined the heat transfer performance of an MCHS

Table 14	Investigation	of wavy	channels	used in	microchannels
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S.no.	Wavy pattern type	Shape of microchannel	Reynold number	Outcomes	Ref.
1	Left-right	y superior to the second secon	100–600	The utilization of a curved path increases the transfer of heat and the resistance to flow by 53% and 154% correspondingly	[165]
2	Wavy channel with a rectangular cross section	y superior to the second secon	300-800	The transfer of heat and loss of pressure were both elevated by 49% and 111%, respectively	[166]
3	Left-right		100–1000	Wavy microchannels exhibit better heat transfer performance than straight microchannels of equal cross-sectional area	[167]
4	periodic, wavy shape with rectangular channel		65–333	Liquid flowing through bends produces Dean vortices, or symmetric secondary flow, as a consequence of steady flow	[172]
5	Double-Layer Wavy MCHS		50–110	The double-layer counter-flow wavy MCHS performs better at higher flow rates and the temperature rise is more consistent	[168]
6	Longitudinal & transversal-wavy MCHS		50–320	Increase in heat transfer between 6.1% to 27.3% and a decrease in pressure between 123.3% to149.2% is found	[173]
7	Wavy channels with alternate secondary branches	10 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	50-200	Introducing secondary branches has the potential to increase performance	[170]
8	Up-down		10–100	In comparison with microchannels with straight walls, wavy channels enhance overall performance by up to 26%	[174]
9	Up-down) - 1 at ² / ₂ / ₂	50-150	Compared to channels with straight walls, a 55% improvement in total performance	[164]
10	Up-down		100–240	Wavy channel has a positive influence because it reduces the thermal and hydrodynamic boundary layer	[176]

with bidirectional ribs (BR) at Reynolds numbers from 100 to 1000. Their findings indicated that the Nusselt number (Nu) of the BR microchannel could reach up to 1.42 times higher than that of a microchannel featuring vertical or spanwise ribs.

Interrupted MCHS in transverse microchambers with various rib forms have been studied by Chai et al. [178]. The transverse microchambers in the interrupted MCHS exhibit a decrease in thermal resistance of 4–31% and a reduction in entropy production rates of 4–26% compared to those of the straight MCHS.

With fan-shaped ribs on the sidewalls, Chai et al. [179] numerically investigated the thermal and hydraulic parameters of laminar flow in an MCHS. The findings indicated that the heat transfer properties were significantly influenced by the height and spacing of the fan-shaped ribs, while the width of the ribs had a lesser impact.

Desrues et al. [180] examined heat transfer and pressure loss in 3D channels featuring alternating opposing ribs. The study found that while the pressure drops increased consistently with Re, heat transfer only improved after Re exceeded a critical value.

Chai et al. [181] utilized numerical simulations to evaluate the thermohydraulic performance of an MCHS that incorporated triangular ribs on the sidewalls. The implementation of these ribs successfully restricted the temperature increase of the heat sink base and prevented a decrease in the local heat transfer coefficient in the flow direction.

The effects of rib shape and fillet radius on the thermalhydrodynamic performance of an MCHS were investigated numerically by Derakhshanpour et al. [182]. The study revealed that increasing the rib corner curvature resulted in a higher heat transfer coefficient, but also led to an increase in the pressure drop. Using a water– TiO_2 nanofluid, Gravndyan et al. [183] conducted investigation on the thermal performance of a rectangular MCHS and studied the impact of rib aspect ratio. The study found that the friction factor was independent of the rib aspect ratio, but dependent on the volume percentage of nanoparticles in the nanofluid.

The use of ribs in microchannels can cause significant pressure loss due to high-flow disruptions, so the optimization of rib geometry is necessary. In order to improve heat transfer while maintaining a minimum pressure drop, grooves or cavities are used to restrict flow and redevelop the thermal boundary layer. Cavities can enhance heat transfer by encouraging mixing between fluid layers near the wall and core through the action of jets and flow throttling. The idea of the ribs and cavities working together has also been used as an effective way to improve heat transfer. Ghani et al. [184] investigated the thermohydraulic characteristics of a microchannel with both sinusoidal cavities and rectangular ribs (MC-SCRR). The results showed that MC-SCRR performed better in terms of thermal performance compared to both rectangular microchannel ribs and sinusoidal microchannel cavities alone. This suggests that the combination of ribs and cavities is an effective way to enhance heat transfer. Xia et al. [185] conducted a numerical analysis to investigate thermal enhancement in an MCHS by using fanshaped reentrant cavities & internal ribs. They found that the Nu for the fan-shaped reentrant cavities was 1.3–3 times higher than that for a rectangular microchannel. The heat transfer characteristics of an MCHS with triangular cavities and rectangular ribs were numerically studied by Li et al. [186]. Their findings revealed a significant improvement in heat transfer for microchannels equipped with triangular and rectangular cavities.

On the other hand, the combination of ribs and grooves was found to be effective way in enhancing heat transfer and reducing pressure drop. This is due to the high-flow disruption capability of ribs and the lower pressure drop of grooves. To validate this Zhu et al. [187] investigated the thermal and hydraulic performance of an MCHS with rectangular grooves and ribs and found that the combination of grooves and ribs was effective in enhancing heat transfer and reducing pressure drop due to the high-flow disruption capability of ribs and the lower pressure drop of grooves. They concluded that the combination of grooves and ribs can significantly increase the overall performance. Further, the thermal performance of an MCHS with ribs and grooves was experimentally and numerically investigated by Wang et al. [188] for chip cooling applications. Their findings showed that rib-grooved microchannels had a Nu 1.11-1.55 times higher than smooth microchannels.

In addition, the use of porous media is a viable solution to mitigate the high pressure drop associated with the implementation of ribs in MCHS. Porous media are frequently employed in heat transfer applications due to their large surface area that comes in contact with the fluid, which enhances the heat transfer performance. The thermohydraulic characteristics of microchannels with solid and porous ribs have been numerically examined by Li et al. [189]. They found that the thermal performance of microchannels with ribs was better than that without ribs. However, the pressure drops and friction factors were higher for microchannels with solid ribs compared to those with porous ribs. By replacing solid ribs with porous ones in center, symmetrical, and staggered rib arrangements, the pressure drops were reduced by 67%, 57%, and 12%, respectively. Wang et al. [190] conducted a numerical investigation to examine how the combined use of porous/solid fins and nanoparticles affects the cooling efficiency of microchannel heat sinks (MCHS). The results showed that, under constant Reynolds number conditions, heat sinks composed of metallic foam exhibited superior cooling performance. These heat sinks were capable of significantly reducing the surface temperature of the heat sink compared to other configurations. In

an					
S.no	. Geometry	Shape	Re. No.	Dutcomes	Ref.
	MCHS with sinusoidal cavities & rectangular ribs SCRR		100-800	MCHS with SCRR outperforms both MCHS rectangular ribs and MCHS with sinusoidal cavities in terms of thermal performance	[184]
0	MCHS with secondary oblique channels in alternate directions & rectangular ribs (SOCRR)		100-500	MC-SOCRR outperformed both MC-RR and MC-SOC in terms of overall performance	[194]
ς	MCHS with bidirectional ribs (BR)	e e e e e e e e e e e e e e e e e e e	100-1000	Vu of the BR microchannel is up to 1.4–2 & 1.2–1.42 times higher than vertical ribs microchannels & spanwise rib microchannel, respectively	[777]
4	Interrupted MCHS (IMCHS) with ribs		187–715	In comparison to a straight MCHS, IMCHS with ribs in the transverse microchambers exhibit a 4–31% drop in thermal resistance and 4–26% drop in entropy production	[178]
Ś	MCHS with truncated rib on the sidewall		100-1000	Fruncated rib may improve the thermal performance by minimizing the pressure drop penalty while maintaining heat transfer	[195]
9	Rectangular, triangular, and semicircular ribs		1000	Micro-ribs can improve the heat transfer rate of microchannels but they also increase the pressure drop penalty	[196]
	MCHS with offset ribs on sidewalls		(190≤Re≤838) (Offset ribs lead to a considerable improvement in heat transfer but also result in a higher pressure drop	[791]

Table 15 Flow disturbance of MCHS & MCHF using ribs

S.no.	Geometry	Shape	Re. No.	Outcomes	Ref.
×	MCHS with fan-shaped ribs on sidewalls		187–715	Height and spacing of fan-shaped ribs have a big influence on heat transfer capabilities, whereas rib width has less impact	[179]
6	Rectangular duct with streamwise-periodic transverse rectan- gular ribs	14 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	75-2000	Pressure drop increases monotonically with Re, but heat trans- fer is improved only when Re exceeds a threshold value	[180]
10	Semicircular ribs (MC-SCR), semi-elliptic ribs (MC-SER), semicircular ribs with fileted corner (MC-SCR-FR) and semi- elliptic ribs and fileted corner (MC-SER-FR)	The second secon	198	Microchannel with semicircular ribs and MC-SER heat sinks, the two designs of MC-SCR-FR and MC-SER-FR increase the Nusselt No. by 18–21% and 0.5–10%, respectively	[198]
11	fan-shaped reentrant cavities with various ribs	A set of the set of th	> 300	When the Re exceeds 300, the combination of fan-shaped reentrant cavities and trapezoidal ribs appears to be the most viable option, while the use of circular ribs in fan-shaped reentrant cavities provides the best results	[199]
12	MCHS with fan-shaped reentrant cavities and internal ribs		150-600	Nu for fan-shaped reentrant cavities is between 1.3 & 3 times that of rectangular MCHS	[185]
13	Rectangular channel with trapezoidal cavities and four different ribs		140-600	Diamond rib combination had the best thermal performance and the backward triangular rib combination had the largest entropy production	[200]

Table 15 (continued)



another research to improve the hydrothermal property of MCHS, an investigation was conducted by Li et al. [191]. They incorporate embedded module ribs and pin with fins. Their outcomes indicate that at a Reynolds number of 458, the heat transfer efficiency increased by 63.91%, resulting in a 67.65% enhancement in temperature uniformity. Furthermore, the pressure drops experienced a modest rise of merely 10.24%.

Polat et al. [192] conducted a numerical investigation to examine the heat transfer performance of a microchannel heat sink (MCHS) equipped with micro pin-fins, focusing on steady laminar flow conditions. Using ANSYS Fluent, simulations were carried out to analyze the heat and fluid flow within MCHSs featuring circular, square, and diamond-shaped micro pin-fins of equal hydraulic diameter. The arrangement of micro pin-fins in each MCHS configuration was optimized for performance using a multi-objective genetic algorithm known as Non-dominated Sorting Genetic Algorithm (NSGA-II). The results of the optimization process revealed that the square-shaped pin-fin configuration exhibited unfavorable performance compared to the other pin-fin shapes. However, among all the configurations tested, the diamond-shaped pin-fins demonstrated a significant improvement in heat transfer while maintaining an acceptable pressure drop ratio. Therefore, the diamondshaped pin-fins were identified as the most effective choice for enhancing heat transfer within the MCHS.

Zhang and Du [193] proposed a method to enhance the heat dissipation of a MCHS by introducing fins that generate a secondary flow. In their study, they compared the performance of the finned MCHS with a straight microchannel heat sink. The experiments were conducted under a mass flow rate of 3.5 gs^{-1} . The results indicated that the finned MCHS achieved improved heat dissipation compared to the straight microchannel heat sink. Specifically, the maximum temperature of the finned MCHS was reduced by 3.04 K (equivalent to a 6.67% decrease) compared to the straight microchannel heat sink. Additionally, the average temperature of the finned MCHS was reduced by 2.86 K (equivalent to a 6.75% decrease) compared to the straight microchannel heat sink.

Channel material

The literature reviewed shows that the flow channels used in various experimental and numerical investigation were made of various materials such as aluminum (Al), copper (Cu), silicon (Si), stainless steel, & various other metals [186–188]. The use of Si is preferred in electronic devices due to its compatibility with micromachining and microfabrication techniques used in semiconductor manufacturing processes, making it well suited for the electronics industry [204]. Generally, water is used as a working fluid which causes corrosion in metallic heat exchangers, owing to thermal property limitations of metallic heat exchangers, these materials become ineffective under extremely high temperatures conditions. To overcome these limitations nowadays numerous researchers have focused on ceramic microchannels.

Ceramic microchannel heat exchangers/heat sink

Metals are commonly used in heat exchangers; however, metallurgical issues or significant deformations are extremely troublesome at high heat-flux settings [190–193]. Furthermore, some fluids are corrosive, and the use of metals increases the production costs [194–197]. Ceramics are one of the finest options for high-temperature applications according to various prior studies [213, 214]. These materials exhibit excellent oxidation, sulfidation, and corrosion resistance. Ceramics generally have low thermal conductivities (e.g., zirconia [215], silicon nitride (SiC) [216]). However, a group of ceramics, such as titanium diboride (TiB₂) [217], zirconium diboride (ZrB₂), hafnium diboride (HfB₂) [218], aluminum nitride (AlN) [219], and beryllium oxide (BeO₂) [220], have better thermal conductivity.

Alm et al. [221] studied the performance in cross-flow and counter-flow regimes of an Al_2O_3 MCHE using demineralized water to measure the heat transfer rate. The efficiency varied from 0.10 to 0.22 in cross-flow heat exchangers at mass flow rates of 20–120 kg h⁻¹, while the heat transfer coefficient was 22 kW m⁻² K⁻¹. A miniaturized heat exchanger composed of SiC was experimentally investigated by Fend et al. [222] at elevated temperatures. Two SiC heat exchangers with various wall thicknesses and widths were tested and compared at temperatures up to 950 °C. The sample with a larger channel width worked better in these studies because of its lower wall thickness. Furthermore, these heat exchangers were observed to have a large heat transfer surface area to volume ratio of 995 m³ m⁻² and a high efficacy of up to 65%.

Villanueva et al. [223] explored the use of ceramics in plate heat exchangers with fins. The findings reveal that the development of vortices in the frontal area of the fins leads to an increase in the heat transfer. Lewinsohn [224] investigated a small SiC ceramic plate MCHE, reported the efficacy, temperature variations, change in pressure, and stresses developed in hot & cold fluid plates. The findings revealed that a microturbine power cycle made of ceramics may achieve greater power cycle efficiency.

Carman et al. [225] examined the impact of an MCHE composed of silicon carbon nitride (SiCN) ceramic material on a microturbine. The study suggests that design optimization can lead to an improvement in the thermal efficiency of the cycle by approximately 9%. Ponyavin et al. [226]

investigated small heat exchangers made of SiC employed for hydrogen generation. The high thermal conductivity of silicon carbide helped to eliminate temperature gradients between the channel walls and maintain low stresses, according to the results. Monteiro and de Mello [227] conducted a study on the thermal efficiency and pressure drop of plate heat exchanger with fins made of alumina. Their findings showed that increasing the mass flow rate resulted in a reduction in the pressure drop, which in turn reduced the device's efficiency. Nekahi et al. [228] studied the viability of TiB₂-SiC composites doped with a two mass% carbon fiber in an MCHE. They found that the TiB₂-SiC and TiB₂-SiC-C_f composites improved heat transfer by 15.5 percent as compared to Al₂O₃. Fattahi et al. [229] conducted a study to investigate the effect of using aluminum nitride (AlN) for constructing MCHE on its heat transfer performance. By replacing Al₂O₃ with AlN, the heat transfer and efficiency of the MCHE were improved by 59% and 26%, respectively. Vajdi et al. [230] conducted a numerical study on an MCHS made of ZrB₂ to analyze pressure drop and heat transfer. The study found that the high thermal conductivity of the ceramics resulted in an effective heat transfer rate. Table 16 summarizes numerous literature studies that use ceramic as a microchannel material.

Channel geometry

The flow in the MCHS was predominantly laminar due to the small channel size. Traditional MCHS experiences a growing thermal boundary layer which causes hotter fluids to be collected on the channel wall, while cooler fluids circulate through the core channel. Therefore, early research efforts focused on improving the thermal efficiency of a typical straight rectangular MCHS by modifying the channel length, aspect ratio, and wall thickness. While some researchers have attempted to disrupt the MCHS boundary layer, others have altered the microchannel cross section to enhance its performance, such as circular, triangular, square, and trapezoidal shapes. However, rectangular cross sections were used in most studies, as seen in Tables 5–13, possibly because of their simpler manufacturing process compared to other shapes.

Yogesh and Prajapati [236] conducted a numerical investigation to analyze how altering the fin height of a rectangular MCHS affects its thermo-hydro properties. They explored seven different heat sink designs in the Re range of 100–400 and the heat-flux range of 100–500 kW m⁻². Their findings indicate that raising the height of fin enhances the heat transfer from the MCHS, but only until the fin height reaches 0.8 mm. Longer fins obstruct the flow channel more, resulting in increased pressure loss. To see the effect of various crystal structure on the thermomechanical

Ref.

[227] [222]

[223] [224] [226]

[231]

[225] [228]

[229]

[232]

[230]

[233]

[234]

[235]

S.no.	Material	Findings
1	Al ₂ O ₃	For mass flow rates of 20 to 120 kg h^{-1} , the efficacy ranged from 0.10 to 0.22 and the heat transfer coefficient extended to 22 kW m^{-2} K ⁻¹
2		Increasing the flow rate of mass reduces the pressure drop, but it also reduces the efficacy of the device
3	SiC	Heat exchangers were observed to have a massive heat transfer surface to volume ratio of $995 \text{m}^3 \text{ m}^{-2}$ and high efficacy of up to 65 percent
1		A vortex formed in the frontal area of a fin results in a notable improvement in heat transfer
5		Ceramic heat exchangers may achieve greater cycle efficiency
5		Due to an extraordinarily high coefficient of thermal conductivity of silicon carbide, the temperature gradi- ents between channel walls was eliminated and maintains low stresses
7		A porous ceramic heat exchanger with multiple scales offers thermal performance of over 2.5 times greater than printed-circuit heat exchangers
3	SiCN	The results indicate that design optimization can improve the thermal efficiency of the cycle by nearly 9%
Ð	TiB ₂ –SiC doped with 2 mass% carbon fiber	TiB_2 -SiC and TiB_2 -SiC-Cf composites improved the heat transfer by 15.5 percent as compared to alumina
10	AlN	The effectiveness and thermal conductivity of the MCHE, which was fabricated using AlN rather than Al_2O_3 , were enhanced by 26% and 59%, correspondingly
11		A reduction of approximately 31% in the overall thermal resistance of the heat sink was reported due to the higher thermal conductivity of AlN
12	ZrB ₂	The research findings indicated that the high heat transfer rate was due to the superior thermal conductiv- ity of ceramics
13	BeO	When the mass flow rate is fixed at 30.5 kg h^{-1} , BeO's better thermal properties result in a more evenly distributed temperature and a 219% increase in the efficiency of MCHE with trapezoidal fins compared to MCHE made of alumina
14	AlN and BeO	When compared to alumina, AlN and BeO ceramics MCHS exhibited thermal performance improvements of about 3.72 and 4.22 times, respectively, at a Reynolds number of 300
15	ZrB ₂ -SiC-CNT	The findings indicate that the ZrB ₂ composite, which is reinforced with 20 vol.% SiC, experiences the most notable decrease in temperature when subjected to ultra-high heat flux. Subsequently, at Re 250, the ZrB ₂ composite reinforced with 20 vol.% SiC and 10 vol.% CNT also shows a considerable reduction

Table 16 Investigation on various ceramic material used for construction of MCHS & MCHE

performance of a MCHE, a numerical experiment was conducted by Wu et al. [237]. They employed multi-physics mathematical model using thermal-fluid–structure interaction (TFSI) to investigate the thermomechanical performance of a MCHE. They found that in comparison with simple cubic crystal structure, the thermal–hydraulic performance factors of FCC and BCC corrugated straight plate MCHE were 2.20 and 1.70.

in temperature

Through numerical simulations, Kumar and Kumar [238] studied the thermo-hydro properties of a rectangular MCHS featuring arc grooves on its surface. The inclusion of grooves has been observed to generate a pseudo-secondary flow, which enhances heat transfer but results in a higher Poiseuille number. Ma et al. [239] presented their findings on thermal characteristics of laminar regime in 3D microchannels having rectangular cross section, where the aspect ratios ranged from 0.1 to 1. They discovered that as the aspect ratio of rectangular microchannels increases and the Reynolds number decreases, the dimensionless thermal entry length also increases uniformly. Lan et al. [240] studied the impact of truncated and offset pin-fins on the thermal

behavior and entropy production in a rectangular MCHS that had different flow characteristics. They discovered that increasing the height of the pin-fins generally resulted in higher heat transfer but also increased fluid resistance. Kose et al. [241] conducted a numerical investigation to assess the heat transfer performance of microchannel heat sinks (MCHS) with different shapes. They compared rectangular, triangular, and trapezoidal microchannels under identical design constraints in order to determine efficient MCHS designs. The study revealed that the rectangular microchannel configuration exhibited the highest thermal and hydrodynamic performance among the three shapes. In terms of heat transfer efficiency, the rectangular microchannel required 17% and 40% less pumping power than the trapezoidal and triangular microchannels, respectively, while achieving the same amount of heat transfer. Fani et al. [242] examined how the size of particles affects the thermo-fluidic properties of nanofluids in a MCHS having trapezoidal cross section. The experiment employed CuO nanoparticles with sizes ranging from 100 to 200 nm and volume concentrations of 1% to 4%, using water as the base fluid. The findings revealed that enlarging the nanoparticles led to a decrease in heat transfer and an increase in pressure drop. Furthermore, the base fluid had a more significant effect on the thermal performance than the nanoparticles.

Weilin et al. [243] investigated the fluidic behavior of water in microchannels constructed of silicon having trapezoidal shapes with channel diameters in the range $51-169 \mu m$. They proposed that the equation of motion should include viscosity, specifically eddy viscosity during turbulent flow. Song et al. [244] conducted numerical simulations to investigate the thermo-fluidic properties of trapezoidal microchannel heat sinks (TMCHS). They analyzed six different configurations of TMCHS and compared their thermo-fluidic characteristics. The results showed that among the six designs, the TMCHS with the reverse channel counter-flow large inlet (RCCFLI) design had the most efficient thermal performance. Ahmed et al. [245] studied how different geometrical parameters affect the laminar flow and heat transfer performance in a grooved MCHS. They found that the trapezoidal groove MCHS had the most efficient thermal design among various grooved MCHS, with an increase in the Nu by 51.59 percent and an increase in friction factor by 2.35 percent.

Mohammed et al. [246] used numerical simulations to assess the impact of incorporating nanofluids in a parallelflow MCHE having square cross section. Their results demonstrated that the use of nanofluids can enhance the thermal characteristics and performance of the heat exchanger, despite causing a slight increase in pressure drop. Zheng et al. [247] conducted a study on the thermo-fluidic performance of circular and annular microchannels with dimples or protrusions. They investigated the impact of various factors, including Re, size of dimples/protrusions, combinations of dimples/protrusions, and positioning patterns. Their research demonstrated that protrusions in circular microchannels are particularly beneficial for energy conservation.

The effect of particle shape on the thermo-fluidic behavior of MCHS with various geometries, i.e., circular, elliptical, triangular, and hexagonal, was studied by Monavari et al. [248]. Their findings showed that the triangular MCHS had the highest heat transfer coefficient value, followed by the elliptical, hexagonal, and circular MCHS in decreasing order. Wang et al. [249] conducted a numerical investigation on the impact of geometric factors on the thermohydraulic performance of microchannel heat sinks (MCHS) with rectangular, trapezoidal, and triangular geometries. Their research showed that the rectangular MCHS had the lowest thermal resistance among the three types, followed by the triangular and trapezoidal MCHS in increasing order of thermal resistance. In another research Tan et al. [250] conducted a numerical investigation to analyze the heat exchange mechanism and optimization of structural parameters for a built-in series combined MCHS. Through an orthogonal test, they investigated the impact of multiple parameters on the heat exchange efficiency. The study revealed that the shape of the microchannel plays a significant role in determining the heat exchange phenomena.

Conclusions

In this study, the focus was on techniques to improve heat transfer in microchannel heat exchangers (MCHE) and microchannel heat sinks (MCHS). Various techniques were reviewed, including the utilization of different working fluids, flow disruptions, different materials for constructing microchannels, and modifications to microchannel geometries. Additionally, statistical factors such as bibliographic analyses were conducted. The main findings of the study are summarized below.

Microchannels have exceptional heat transfer properties that enable them to absorb substantial heat fluxes in very small areas. However, despite their potential, commercially available microchannels have not yet replaced conventional channels due to the high cost of the specialized manufacturing processes required to produce micro- and minichannels. Nearly half of the studies conducted on microchannel heat sinks (MCHS) and microchannel heat exchangers (MCHE) have utilized numerical approaches. In the past decade, there has been a proliferation of numerical studies, with a relative decrease in analytical and experimental research.

Although there have been notable advances in the development of microchannel heat sinks (MCHS) for electronic cooling applications, research in large-scale thermal and energy applications has been limited. In practical thermal applications, heat exchangers often incorporate core components with complex geometric designs. However, most of the studies conducted on microchannel heat exchangers (MCHE) and MCHS have focused on fundamental microchannel geometries, particularly rectangular ones, and working fluids. To accurately represent real-world heat exchangers, extensive research is required on a wide range of configurations, manifold geometries, materials, and working fluids.

Numerous studies have demonstrated that the optimal method for removing high heat flux from small volumes and spaces is by allowing the working fluid to flow through a microchannel. The addition of nanoparticles in small quantities to the base fluid can further enhance the thermal and fluid flow characteristics of the microchannel. Al_2O_3 is the most commonly used nanofluid due to its low density and high thermal conductivity. However, the use of nanofluid has a negative impact on energy consumption since it requires more electricity for pumping.

The use of flow disruption techniques, such as the wavy microchannel design, has been found to have a significant

impact on the heat transfer performance of microchannel heat sinks. The effectiveness of this technique can be attributed to three main mechanisms. Firstly, it increases the surface area available for convective heat transfer. Secondly, it alters the parabolic velocity profile, leading to improved convective heat transfer. Finally, it creates Dean vortices & chaotic advection, resulting in improved convective fluid mixing. While the wavy channel design may cause pressure losses, the benefits to heat transfer outweigh the associated pressure drop penalty.

The researchers evaluated various materials for constructing microchannels, including metals, ceramics, and polymers. Based on their findings, ceramics were determined to be the optimal material for high-temperature applications due to their ability to address metallurgical issues and corrosion problems.

Future scope

Here are some suggestions and recommendations for future work based on the published studies on heat transfer improvement in microchannel heat sinks/heat exchangers:

- (i) Use of combined active and passive techniques in microchannel heat sinks/heat exchangers for further heat transfer augmentation.
- (ii) The use of ultra-high-temperature ceramics in place of metals and superalloys in high-temperature power generating applications can solve the metallurgical constraint of the high inlet temperature of microturbines and increase the efficiency of the plant.
- (iii) The thermal performance of microchannels has to be further enhanced, and other manufacturing processes for miniaturization are needed to cut their cost.
- (iv) Further research is needed to explore the potential of nanofluids in enhancing the thermal and fluid flow characteristics of microchannels. The effects of different types and concentrations of nanoparticles, as well as their impact on pump power consumption, need to be thoroughly investigated.
- (v) More studies are needed to investigate the effects of various flow disruption techniques and microchannel geometries on heat transfer enhancement. In particular, further research should focus on exploring the performance of wavy microchannels and their potential applications in large-scale thermal and energy systems.
- (vi) Future studies should consider a wider range of working fluids to explore their potential in microchannel heat sinks/heat exchangers. Researchers should also focus on investigating the effects of fluid properties, such as viscosity and surface tension, on the thermal and fluid flow characteristics of microchannels.

- (vii) The development of advanced manufacturing techniques that can produce cost-effective and high-performance microchannel heat sinks/heat exchangers should be prioritized. This could involve exploring the use of 3D printing and other novel fabrication techniques.
- (viii) Further studies should explore the effects of operational conditions such as flow rate, inlet temperature, and pressure drop on the performance of microchannel heat sinks/heat exchangers.
- (ix) The potential of microchannel heat sinks/heat exchangers in applications beyond electronic cooling, such as in the fields of energy and biomedicine, should be explored.
- (x) Finally, researchers should focus on developing accurate numerical models and experimental methods to predict and measure the thermal and fluid flow characteristics of microchannel heat sinks/heat exchangers.

Author declaration There is no review paper which compiles all the heat transfer enhancement techniques on MCHS & MCHE. Also, information on ceramic MCHE and MCHS is limited. In this paper, the authors have tried to review all the journal papers that dealt with improvement in thermal performance of MCHS and MCHE. The effort behind this work can be divided into four main aspects: working fluid, flow disruption techniques, the material of construction, and the geometry of the channel.

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