

# **Statistical study and a complete overview of nanofuid viscosity correlations: a new look**

**A. Barkhordar1 · R. Ghasemiasl1 · T. Armaghani[2](http://orcid.org/0000-0003-3758-9106)**

Received: 7 April 2021 / Accepted: 7 July 2021 / Published online: 22 August 2021 © Akadémiai Kiadó, Budapest, Hungary 2021

### **Abstract**

Nanofuids are considered the top candidates to replace surface cooling systems, making it essential to study the efect of nanoparticles on thermophysical properties of the base fuid when it is added. Viscosity is a crucial factor in heat transfer, especially convection heat transfer. In most of the studies published, the correlations obtained from experiments were performed without examining statistical tests, and the efect of diferent parameters, including temperature, volume (mass) fraction, etc., on the viscosity of nanofuid in the proposed correlations was not specifed. Moreover, some correlations it was shown that the elimination of one of the parameters had no efect on the response of that correlation. For statistical analysis, analysis of variance and sensitivity analysis were used to determine the relationship of the correlation with its variable parameters. The results showed that approximately 27.2% of the correlations presented for the ethylene glycolbased nanofuid and 27.7% of the correlations presented for the water-based nanofuid are reliable. Finally, as until now, no accurate correlation has been provided for the viscosity in a wide temperature and volume fraction range. According to the R-square statistical index, viscosity models were obtained in this study with an accuracy of 97.01% and 96.08% for water- and ethylene glycol-based nanofuids, regardless of the nanoparticle type. Also, the RMSE value was improved by 35.82% and 49.84% compared to the best correlation presented by the researchers for estimating the viscosity of water-based nanofuid and ethylene glycol-based nanofuid, respectively.

**Keywords** Nanofuid viscosity · Statistical analysis · Monte Carlo method

### **Nomenclature**

- T Temperature ( ${}^{\circ}$ C or K)
- $\varphi$  Concentration (%)
- $\mu$  Dynamic viscosity (mPa.s)
- d Diameter (nm)
- $\dot{v}$  Shear rate  $(s^{-1})$
- N Number of data
- θ Dimensionless temperature
- a, b Constant values

### **Subscripts**

- bf Base fluid
- nf Nanofuid
- $\boxtimes$  R. Ghasemiasl ghasemiasl@yahoo.co.in

 $\boxtimes$  T. Armaghani armaghani.taher@yahoo.com

<sup>1</sup> Department of Mechanical Engineering, West Tehran Branch, Islamic Azad University, Tehran, Iran

<sup>2</sup> Department of Mechanical Engineering, Mahdishahr Branch, Islamic Azad University, Mahdishar, Iran



w Mass concentration

### **Introduction**

One of the perspectives for solving conservation equations for nanofuids is the single-phase method. In this method, the thermophysical properties of the nanofuid replace the thermophysical properties of the base fluid  $[1-3]$  $[1-3]$ . The single-phase model is used by some investigations [[4–](#page-31-2)[7\]](#page-31-3). This shows the impact of thermophysical properties of the nanofluid, especially its viscosity, on heat transfer.  $[8-10]$  $[8-10]$ 

Among the thermophysical properties of nanofuids, viscosity indicates fuid resistance. Therefore, viscosity has determined the performance of energy and heating systems. [[11–](#page-31-6)[13\]](#page-31-7)

In industrial equipment and scientifc research, where heat transfer is in the forms of forced convection and natural convection, the viscosity of nanofuids plays a crucial role in determining the fow regime, pumping power, pressure drop, and workability of systems [\[14](#page-31-8)[–17\]](#page-31-9).

The frst viscosity model for suspensions containing metal particles was introduced by Einstein in 1906 [[18\]](#page-31-10). Later on, viscosity models proposed by Brinkman [[19](#page-31-11)], Batchelor [\[20](#page-31-12)], and other equations started to be used to model the heat transfer of nanofuids. However, these correlations each have weaknesses, including the inability to estimate the viscosity of nanofuids in a wide range of temperatures and concentrations used in heat transfer.

In the experiments conducted by Duangthongsuk and Wongwises  $[21]$  on the behavior of  $TiO<sub>2</sub>$  and water nanofluid, they presented a correlation by applying the effects of base fuid viscosity and volume fraction variables on the viscosity model. In their model, nanofuid's temperatures and volume fraction ranged between 15 to 35 °C and 0.2 to 2%, respectively.

In an experimental test performed by Esfe and Saedodin [\[22](#page-31-14)] on the viscosity of ZnO nanofluid with ethylene glycolbased fuid at a temperature between 25 and 50 °C and a volume fraction of 0.25 to 5%, the viscosity model with the variables of temperature and volume fraction and the viscosity of the base fuid presented that the ratio of mean variation of the model data compared to other the experimental values was less than 2%.

Sharifpur et al. [[23](#page-31-15)] also introduced a viscosity model based on the data derived from experiments using  $Al_2O_3$ and glycerin nanofuid with an accuracy of 0.9495. In their viscosity model, in addition to the variables of temperature and volume fraction and the viscosity of the base fuid, the efect of the thickness of the nanoparticles is also taken into account. It is used for nanofuids in the temperature range of 20 to 70 °C and volume fraction of 0 to 5%, and diameter of nanoparticles about 19 to 160 nm. But Aberoumand et al. [\[24](#page-32-0)] presented a viscosity model for oil-silver nanofuid that depends only on the variables of volume fraction and viscosity of the base fuid and is valid for nanofuids at temperatures between 25 and 60 °C and volume fraction of 0 to 2%.

In an experimental study performed by Akbari et al. [[25\]](#page-32-1) on Si  $O_2$  and ethylene glycol nanofluids in the temperature range of 30 to 50 °C and volume fraction of 0.5 to 3%, using temperature and volume fraction components and the viscosity of the base fuid proposed a viscosity model for the nanofuid. Li and Zuo [\[26](#page-32-2)] had proposed a viscosity model for a nanofluid including  $TiO<sub>2</sub>$  nanoparticles and a mixture of water-based fuid and ethylene glycol at a temperature between 20 to 50 °C and a volume fraction of 0.25 to 1%.

Yu et al. [\[27](#page-32-3)] also proposed a new viscosity model based on the data derived from experiments using multi-walled carbon nanotubes [MWCNT] and water nanofuids. In their model, in addition to the role of temperature, mass fraction, and base fuid viscosity, the efect of shear rate on viscosity variations is also considered. This model is valid in a temperature range of 275 to 283 Kelvin, and mass fraction range of 0.1 to 0.6 percent, and a shear rate of 10 to 1000 s<sup>-1</sup>. According to the experiment performed by Yan et al. [[28](#page-32-4)] on a hybrid nanofuid with multi-walled carbon nanotube [MWCNT] nanoparticles and  $TiO<sub>2</sub>$  with a base fluid of ethylene glycol at 25 to 55 °C and a volume fraction of 0.05 to 1%, the viscosity model with volume fraction and nondimensional temperature components has been presented with an accuracy of 0.995.

Figure [1](#page-1-0) is plotted to know the year of publication of the evaluated correlations in the present study. Therefore, it can be concluded that researchers have considered the study and presentation of models for the viscosity of nanofuids in recent years.

Figure [2](#page-2-0) is plotted to indicate the temperature range at which the viscosity models are valid. The correlations separated according to the temperature range they cover in diferent temperature ranges that difer by 10 degrees. (Temperature difference of less than five  $\mathrm{C}$  in the classification has been neglected.)

According to Fig. [2,](#page-2-0) 21.4 and 23.2% of the temperature range cover 30 and 40°, respectively, and only 23.2% of the correlations in the 50° temperature range can estimate the viscosity of the nanofuid.

Similar to the temperature diagram, the viscosity models were separated into 1% by volume (mass) fraction intervals



<span id="page-1-0"></span>**Fig. 1** Year of publication of evaluated correlations in articles

<span id="page-2-0"></span>

relative to the concentration range in which they are valid, and Fig. [3](#page-2-1) shows that only 19.6% of the correlations can cover the concentration range of 2 percent.

As the authors worked on the thermal conductivity of nanofuid based on present studies and introduced a new general model named MAG. [[29\]](#page-32-5) So this study must be done about nanofuid viscosity.

In this study, the correlations presented for the viscosity of nanofuids were wholly reviewed and investigated thoroughly in terms of compliance with the physics and viscosity of nanofuids. In the following, the relationship between viscosity and variables of temperature and volume (mass) fraction of nanofuids was evaluated according to the statistical test of variance. Moreover, all the correlations presented for nanofuid viscosity were investigated with the sensitivity analysis test to identify the variable with the most signifcant efect on the viscosity model. Finally, two general models for water-based nanofuids and ethylene glycol were presented to predict the viscosity behavior of nanofuids.

### **Strategy**

#### **Analysis of variance**

Statistics is a broad feld of mathematics that studies how data collection, summary, and conclusion are studied. Here, the status of variables related to the viscosity of nanofuid investigated using statistical science based on probability theory and mathematics.

ANOVA test or analysis of variance is a subset of statistical science, which analyzes and compares the means of different statistical groups and determines the effect of independent variables on the dependent variable. This method has been introduced by the famous statistician and geneticist "R. Fisher."[[30\]](#page-32-6)

This method tries to estimate the diferences between several statistical populations. In other words, using the mean index in statistical populations, we will be able to express the characteristics of the population; thus, if the mean of one group is diferent from other groups in society, we conclude that the statistical populations are not the same. In the oneway analysis of variance, the null hypothesis indicates that



<span id="page-2-1"></span>

the mean of the experimental groups is equal to each other. The opposite assumption is that at least one of the means is diferent from the others; if the null hypothesis is confrmed, it will be accepted that there is no diference between the means of the groups, and the variable has no role in the correlation. Therefore, to better understand the correspondence of variables on nanofuid viscosity, it is necessary to perform variance analysis. [\[31](#page-32-7)]

Thus, by groups that will be created in terms of temperature and concentration variables for each equation and with the help of a one-way ANOVA test, the results presented in Table [1](#page-4-0) are obtained.

In some of the correlations proposed by researchers due to the lack of attention to the response power of the correlation in the temperature range afecting the viscosity of nanofuids and also because the appropriate relationship is not used in correlations to express the relationship between temperature and viscosity of nanofuid and the correlation are not able to predict the nanofuid viscosity at sensitive temperature and do not express the role and importance of temperature variables in nanofuid viscosity models.

One of the issues that researchers had not been considered in presenting correlations is the efect of terms on the viscosity model. For example, Dalkılıça et al. [[32](#page-32-8)] presented Eq. [\(1](#page-3-0)) for nanofuid viscosity by experimental investigation of the viscosity of a hybrid nanofuid containing graphene and  $SiO<sub>2</sub>$  nanoparticles in a water-based nanofluid in the temperature range of 15 to 60 °C and a volume fraction of 0.001 to 0.02%.

models cannot respond commensurately with the expected concentration range in heat transfer.

By conducting experimental tests on nanofluids of  $A I_2 O_3$ and ethylene glycol, Li et al. [[33](#page-32-9)] presented the new viscosity model in compliance with the trend of temperature variation from 25 to 60 °C and a mass fraction of 0 to 2% in Eq. ([2](#page-3-1)).

<span id="page-3-1"></span>
$$
\mu_{\rm nf} = -334.9 \varphi_{\rm w}^{4.044} \left(\frac{1}{T}\right)^{10.03} + 296.8 \left(\frac{1}{T}\right)^{0.7795} - 6.841 (2)
$$

Concentration variable in term  $-334.9\varphi_w^{4.044}$  $\left( \right)$ *T*  $\big)^{10.03}$  less than  $0.01\%$  affects the nanofluid viscosity. Therefore, the viscosity model of Li et al. does not have the expected dependence on the concentration variable.

By evaluating the correlations presented for nanofuid viscosity, the situation of temperature and volume (mass) fraction variables in the correlations is determined. The results showed if there is a signifcant relationship between variables and nanofuid viscosity.

Therefore, it is necessary to consider the effects of variables on the viscosity models of nanofuids in the temperature range and volume (mass) fraction of heat transfer.

#### **Physical analysis of correlations**

Viscosity models at diferent dimensions in this part of the research are studied. First, the structure of the proposed correlations to calculate the viscosity has been examined

$$
\mu_{\rm nf} = \left[ 1.00527 \times \left( T^{0.00035} \right) \times \left( 1 + \varphi \right)^{9.36265} \times \left( \frac{\varphi_{\rm w, G}}{\varphi_{\rm w, SiO_2}} \right)^{-0.028935} \right] \mu_{\rm bf}
$$
(1)

In the case, where  $\varphi = 1$  and other components are a constant value, if the lower and upper-temperature limits are set in Eq. ([1\)](#page-3-0), the range of viscosity changes will be less than 0.04%. Therefore, Eq. ([1\)](#page-3-0) is not dependent on temperature, but the researcher had given in the equation, and this is not considered signifcant by the researcher.

In addition to the temperature variable, the concentration variable also has an undeniable role in the viscosity models of nanofuids. So that with increasing the concentration of nanofuid, the viscosity of nanofuid increases signifcantly; therefore, in most viscosity models, the prominent role of the concentration variable was considered by researchers. However, in some correlations recently published by researchers, the correlations have been measured in the range of inappropriate volume (mass) fractions and only at low concentrations. On the other hands, due to the use of irrational relationships to express the relationship between the viscosity of nanofuid and the concentration of nanoparticles, viscosity

<span id="page-3-0"></span>and then evaluated for analyzing complex, heterogeneous, or ambiguous components. Meanwhile, in another section, based on the experimental studies of researchers in the temperature range and volume (mass) fraction, the data extracted from the correlations are evaluated. Also, the accuracy of the experimental model for the case where the concentration of nanofuid is considered zero with the viscosity of base fuid has been investigated. Finally, the correlations have been measured in terms of the laws governing the physics of nanofuids and the changes due to an increase or decrease in temperature and concentration of nanofuids.

According to Table [1](#page-4-0) of the Term section, in most of the experimental relations studied for calculating viscosity, it is observed that mathematical expressions and terms do not interfere with the calculation of the viscosity of nanofuids. Thus, these expressions have only caused the complexity and inefficiency of empirical relations, which increases the possibility of errors in the viscosity calculations of nanofuids.

<span id="page-4-0"></span>



 $\underline{\textcircled{\tiny 2}}$  Springer









 $\underline{\textcircled{\tiny 2}}$  Springer





 $\underline{\textcircled{\tiny 2}}$  Springer









Data<sup>2</sup>: By considering the concentration of zero in the correlation, the ability of the correlation to estimate the viscosity of the base fluid is investigated. : According to the type of physical evaluation, the correlat Data<sup>2</sup>: By considering the concentration of zero in the correlation, the ability of the correlation to estimate the viscosity of the base fluid is investigated. : According to the type of physical

Terms<sup>3</sup>: correlations with multiple or irrational terms are identified Terms<sup>3</sup>: correlations with multiple or irrational terms are identified evaluation, the correlation, in this case, is not reliable

Trends<sup>4</sup>: According to the physical laws governing the viscosity of nanofluids, the decreasing or increasing trend of viscosity is evaluated according to changes in temperature and concentration Trends<sup>4</sup>: According to the physical laws governing the viscosity of nanofluids, the decreasing or increasing trend of viscosity is evaluated according to changes in temperature and concentration

Statistical<sup>5</sup>: Results of physical evaluations of correlations Statistical<sup>5</sup>: Results of physical evaluations of correlations

2 Springer

Given the above, Alarifi et al. [[34\]](#page-32-19) studied the viscosity of hybrid nanofuids, which are composed of a mixture of MWCNT and  $TiO<sub>2</sub>$  nanoparticles in oil, and they presented a new model by Eq. ([3\)](#page-16-0) for the viscosity of the nanofuid by examining the efects of temperature and concentration on the viscosity of the nanofuid. According to the equation, a trigonometric ratio has been used to express the relationship between concentration and viscosity. Therefore, a disproportionate function in relationships is not necessary and can only cause problems in calculations.

$$
\mu_{\rm nf} = 2.936T + \frac{2e^4}{1.68 + T - (1.68\varphi)} - 448.8 - \tan((1.68\varphi) - 1.68)
$$
\n(3)

Based on an experimental test on the viscosity behavior of SiO<sub>2</sub> nanoparticles dispersed in a mixture of water and ethylene glycol, Ruhani et al.[\[35](#page-32-21)] proposed a viscosity model in Eq. ([4](#page-16-1)), valid in the temperature range of 25 to 50 °C and a volume fraction of 0.1 to 1.5%. The temperature variable in the viscosity model is both in the position of the power function and is powered by the exponential function in terms of position. Therefore, using such functions one after the other is not justifed and causes the calculations to be complex.



<span id="page-16-6"></span><span id="page-16-0"></span>**Fig. 4** Comparison of the results of Yan et al.'s correlation [[28](#page-32-4)] and the currently proposed correlation with experimental data

$$
\mu_{\rm nf} = \left[2.030 - \left(931.616 \times \varphi^{0.9305} \times 5.4597 \times T^{-3.4574}\right) - \exp\left(-0.0028 \times \varphi^{2.1421} \times T^{1.0133}\right)^2\right] \mu_{\rm bf}
$$
(4)

Yan et al. [[28\]](#page-32-4) have presented Eq. ([5\)](#page-16-3) for the hybrid nanofluid of MWCNT and  $TiO<sub>2</sub>$  in ethylene glycol in the temperature range of 25 to 55 °C and at the volume fraction between 0.05 and 1%;

$$
\mu_{\text{nf}} = [0.90463 + 280.20104\varphi + 0.25734\theta + 368.05239\theta\varphi
$$
  
-28643.68399\varphi^2 - 0.012051\theta^2 - 1968.73612\varphi^2\theta  
-235.04729\theta^2\varphi + 2.09629 \times 10^6\varphi^3 - 0.099694\theta^3]\mu\_{\text{bf}} (5)

Equation [\(5](#page-16-3)) has many terms that entering the equation for subsequent heat transfer calculations may be associated with many errors. On the other hands, by reducing the terms of the equation with increasing the accuracy, the equation becomes easier to use. Therefore, Eq. ([5](#page-16-3)) can be presented more simply as Eq.  $(6)$  $(6)$ .

$$
\mu_{\rm nf} = (0.0029741 + \varphi^{1.07982}) \times (T^{-1.25573}) \times 311157 \quad (6)
$$

Equation ([6\)](#page-16-5) has been obtained by the nonlinear regression method from experimental data of Yan et al. [\[28](#page-32-4)] for hybrid nanofuid viscosity.

According to Fig. [4,](#page-16-6) the proposed model in Eq. ([6\)](#page-16-5), while having higher accuracy than Eq.  $(5)$  $(5)$  $(5)$ , has a simpler form compared to Eq.  $(5)$  $(5)$ . Figure  $(4)$  $(4)$  plotted at a volume fraction of 0 to 1% and a temperature of 30 °C for nanofuids.

<span id="page-16-2"></span><span id="page-16-1"></span>
$$
\mu_{\rm nf} = a_1 + a_2 T + a_3 \varphi + a_4 T^2 + a_5 T \varphi + a_6 \varphi^2 + a_7 T^3 + a_8 T^2 \varphi + a_9 T \varphi^2
$$
  
+ 
$$
a_{10} \varphi^3 + a_{11} T^3 \varphi + a_{12} T^2 \varphi^2 + a_{13} T \varphi^3 + a_{14} \varphi^4
$$
 (7)

Huminic et al. [[36\]](#page-32-26) proposed Eq. ([7\)](#page-16-2) for  $La_2O_3$  and water nanofuids in the temperature range of 293 to 323 K and a volume fraction between 0 and 0.03%.

<span id="page-16-3"></span>According to Eq. [\(7](#page-16-2)), there are many components in the correlation that are similar to Eq. ([5\)](#page-16-3), and the experimental data provided by Huminic et al. are used, and Eq. [\(8\)](#page-16-4) is presented as follows.

<span id="page-16-4"></span>
$$
\mu_{\rm nf} = \left(0.458474 + \varphi^{1.10104}\right) \times \left(\frac{T}{323}\right)^{-0.636006} \times 1.5773\tag{8}
$$

<span id="page-16-5"></span>According to Fig. [5,](#page-17-0) Eq. [\(8](#page-16-4)), simplicity has accuracy more than 2% more than Eq. ([7\)](#page-16-2).

A closer look reveals similar cases in which researchers try to present complex correlations; however, using the same experimental data, simple and sometimes linear equations can be given with much higher accuracy than the desired equations, so Eqs.  $(6)$  $(6)$  and  $(8)$  $(8)$  can replace Eqs.  $(5)$  $(5)$  and  $(7)$  $(7)$ .

While the models proposed for nanofuid viscosity by Esfe et al.  $[37, 38]$  $[37, 38]$  $[37, 38]$  $[37, 38]$  presented in Eq.  $(9)$  $(9)$  and  $(10)$  $(10)$ , there are several terms in the viscosity model; therefore, the presence



<span id="page-17-0"></span>**Fig. 5** Comparison of the results of Huminic et al.'s [[36](#page-32-26)] correlation and the proposed correlation with experimental data

of multiple terms in the equations is not necessary and makes the equations more complex, and these multiple components in viscosity calculation will lead to increased computational error.

concentration independently and directly afect the nanofuid viscosity, so that with increasing temperature, the viscosity of nanofuid decreases, and by adding nanoparticles to the base fuid, the viscosity of nanofuid increases. Therefore, at this stage, the variation trend of viscosity values at diferent temperatures and concentrations according to the physical laws governing nanofuid viscosity is investigated. The results of this analysis are presented in Table [1](#page-4-0) of the Trend section.

According to the presented issue, in the viscosity model proposed by Esfe and Esfandeh [\[39\]](#page-32-14) for the viscosity of nanofuids, including oil and hybrid particles, the variation trend of viscosity values with increasing concentration is contrary to the physical laws governing nanofuid viscosity.

Table [1](#page-4-0) exhibits the correlations presented for nanofuid viscosity by various researchers from 2009 to 2020, along with statistical analysis and physical analysis. Statistical analysis of ANOVA test was performed, and terms related to physical examination [Data, Term, Trend] entirely have been presented for each experimental equation.

<span id="page-17-1"></span>In addition, the validity range of the equations and the overall conclusion have been presented by the correlation evaluation.

$$
\mu_{\text{nf}} = 679.7806 + 259.62463\varphi - 33.64131T - 0.045393\dot{\gamma} - 6.0695 \times \varphi T \n-0.00031841\varphi\dot{\gamma} + 0.00129007T\dot{\gamma} - 236.23287\varphi^2 + 0.65796T^2 + 2.31776E - 06\dot{\gamma}^2 \n+1.55167\varphi^2 T + 0.049085\varphi T^2 - 9.63258E - 8T\dot{\gamma}^2 + 94.57115\varphi^3 \n-0.0051586T^3 + 0.0000000001\dot{\gamma}^3
$$
\n(9)

$$
\mu_{\text{nf}} = 688.46 + 347.09\varphi - 33.12T - 0.04\dot{\gamma} - 7.36\varphi T - 0.0087\varphi\dot{\gamma} + 0.0014T\dot{\gamma} \n-305.24\varphi^2 + 0.61T^2 + 1.49 \times 10^{-6}\dot{\gamma}^2 + 0.0001\varphi T\dot{\gamma} + 0.46\varphi^2 T + 0.0014\varphi^2\dot{\gamma} \n+ 0.065\varphi T^2 + 1.87 \times 10^{-7}\varphi\dot{\gamma}^2 - 7.25 \times 10^{-6}T^2\dot{\gamma} - 7.33 \times 10^{-8}T\dot{\gamma}^2 + 169.62\varphi^3 \n-0.0043T^3 + 0.00000000011\dot{\gamma}^3
$$
\n(10)

In the continuation of reviewing the results and data extracted from viscosity models, it has been observed that sometimes the equations at zero concentration and in a certain range of temperature and concentration have an unusual response. The results of this analysis are presented in Table [1](#page-4-0) of the Data section.

For example, Huminic et al. [[36](#page-32-26)] presented the viscosity model for  $La_2O_3$  and water nanofluids in the temperature range of 293–323 K and at a volume fraction between 0 and 0.03 contrary to the researcher claims, the correlation is not able to respond at zero concentration.

Finally, according to studies by researchers on the viscous behavior of nanofuids, variables of temperature and

#### <span id="page-17-2"></span>**Sensitivity analysis with Monte Carlo test**

The sensitivity analysis method has been used to continue the statistical study process of relationships and know the position of variables in correlations. According to the general defnition in statistics, sensitivity analysis is the study of the efectiveness of output variables from a set of assumed input variables in a statistical model.

As a result, the researcher can determine how changes in a component afect the model's output. Therefore, in the continuation of the statistical study article, the sensitivity analysis will give a deeper look at viscosity models with the <span id="page-18-2"></span>**Fig. 6** Result of sensitivity analysis on the correlation proposed by Li and Zou [\[26\]](#page-32-2). (green color: base fuid viscosity variable/ blue color: volume fraction variable/ purple color: temperature variable)



<span id="page-18-3"></span>**Fig. 7** Result of sensitivity analysis on the correlation proposed by Saeedi et al. [[55](#page-32-31)]. (green color: base fuid viscosity variable/ blue color: volume fraction variable/ purple color: temperature variable)

variables of base fuid viscosity, temperature, and concentration. [[80\]](#page-33-19)

Therefore, to obtain a complete conclusion about the performance of viscosity models and the efectiveness of variables, only the correlations in which the variables have the expected dependence on the viscosity equations in terms of variance test are examined.

In the present study, to analyze viscosity models, also a method known as the Monte Carlo test is used.

Variables with little efect and little change on the equations are displayed as fat lines in the graph. So the more curved lines show the more dependence of the variable on the equation.

Li and Zou [[26](#page-32-2)] introduced the viscosity model of Eq. ([11\)](#page-18-0) for nanofluids consisting of  $Al_2O_3$  nanoparticles and water-based nanofuid, and Saeedi et al. [[55](#page-32-31)] proposed the viscosity model of Eq.  $(12)$  $(12)$  for Ce O<sub>2</sub> nanoparticles dispersed in ethylene glycol.

<span id="page-18-1"></span>
$$
\mu_{\rm nf} = 0.838 \varphi^{0.188} T^{0.089} \mu_{\rm bf}^{1.1} \tag{12}
$$

The test results in Figs. [6](#page-18-2) and [7](#page-18-3) show that the curvature of the green line is greater than that of the blue and purple lines, and the presence of the variable of the viscosity of the base fuid in correlation is more important than other variables. In addition, concentration and temperature, respectively, have an infuential role in the equations.

Equation [\(13](#page-18-4)) presents Nabil et al. [[62\]](#page-33-1) viscosity model for the hybrid nanofluid of  $TiO<sub>2</sub>$  and  $SiO<sub>2</sub>$  in a mixture of water and ethylene glycol.

<span id="page-18-4"></span>
$$
\mu_{\rm nf} = \left[37\left(0.1 + \frac{\varphi}{100}\right)^{1.59}\left(0.1 + \frac{T}{80}\right)^{0.31}\right]\mu_{\rm bf} \tag{13}
$$

<span id="page-18-0"></span>In Fig. [8](#page-19-0), the green line has higher curvature than the blue and purple lines. Therefore, the sensitivity analysis results showed that the variables of base fuid viscosity,

$$
\mu_{\rm nf} = \left[ 781.4 \times T^{-2.117} \times \varphi^{0.2722} + \frac{0.05776}{T^{-0.7819} \times \varphi^{-0.04009}} + 0.511 \times \varphi^2 - 0.1779 \times \varphi^3 \right] \mu_{\rm bf}
$$
(11)

<span id="page-19-0"></span>**Fig. 8** Result of sensitivity analysis on the correlation proposed by Nabil et al. [[62](#page-33-1)]. (green color: base fuid viscosity variable/ blue color: volume fraction variable/ purple color: temperature variable)



<span id="page-19-2"></span>

concentration, and temperature significantly affect Eq.  $(13)$  $(13)$ , respectively.

The variables of base fuid viscosity, temperature, and concentration are available in the above viscosity equations. The variable of base fuid viscosity applies the value of the base fuid viscosity in proportion to the reference temperature in the viscosity model. Therefore, the dependence of the viscosity equations on the viscosity variable of the base fuid expresses the relationship of the equations on temperature. On the other hands, the sensitivity analysis results show that the variable of the base fuid viscosity has a more contribution in estimating the viscosity of nanofuid than other variables. Therefore, considering the mentioned conditions, it is concluded that the temperature factor indirectly has a more signifcant efect on viscosity equations than other variables.

Esfe et al. [[48\]](#page-32-23) have presented Eq. ([14\)](#page-19-1) for the viscosity of hybrid nanoparticles of MWCNT and  $Ti O<sub>2</sub>$  in a mixture of water-based nanofuid and ethylene glycol;

<span id="page-19-1"></span>
$$
\mu_{\text{nf}} = 6.35 + 2.56\varphi - 0.24T - 0.068\varphi T + 0.905\varphi^2 + 0.0027T^2
$$
\n(14)

<span id="page-19-3"></span>According to the sensitivity analysis results presented in Fig. [9,](#page-19-2) the effect of the temperature is greater than the concentration in the equation because the curvature of the green line is more signifcant.

$$
\mu_{\text{nf}} = 688.46 + 347.09\varphi - 33.12T - 0.04\dot{\gamma} - 7.36\varphi T - 0.0087\varphi\dot{\gamma} + 0.0014T\dot{\gamma} \n-305.24\varphi^2 + 0.61T^2 + 1.49 \times 10^{-6}\dot{\gamma}^2 + 0.0001\varphi T\dot{\gamma} + 0.46\varphi^2 T + 0.0014\varphi^2\dot{\gamma} \n+ 0.065\varphi T^2 + 1.87 \times 10^{-7}\varphi\dot{\gamma}^2 - 7.25 \times 10^{-6}T^2\dot{\gamma} - 7.33 \times 10^{-8}T\dot{\gamma}^2 + 169.62\varphi^3 \n-0.0043T^3 + 0.000000000011\dot{\gamma}^3
$$
\n(15)

<span id="page-20-0"></span>**Fig. 10** Result of sensitivity analysis on the correlation proposed by Esfe et al. [[37](#page-32-22)]. (green color: temperature variable/ blue color: volume fraction variable/purple color: variable of shear rate)



<span id="page-20-2"></span>

Esfe et al. [\[38\]](#page-32-18) presented the nanofuid viscosity model for the MWCNT and  $AI_2O_3$  hybrid nanoparticles dispersed in oil in Eq. [\(15](#page-19-3)).

The sensitivity analysis results in Fig. [10](#page-20-0) showed that the green line has higher curvature than the purple and blue lines, so the efect of the temperature is greater than the concentration in the equation.

According to the results and the role of temperature and concentration in Eq.  $(15)$  $(15)$ , the shear rate of nanofluid is also efective in calculating the viscosity of nanofuid.

The results of sensitivity analysis of the previous two equations show that when the variable of base fuid viscosity is not present in the viscosity equations, conditions are created that the efect of temperature factor is directly applied in the viscosity equations, and thus, the temperature variable has a more infuential role than other variables.

Equation ([16\)](#page-20-1) presents Li et al. [\[79\]](#page-33-18) model for the viscosity of SiC and water nanofuids.

<span id="page-20-1"></span>
$$
\mu_{\rm nf} = \left[1.07879 + 0.45546\varphi + 0.4051\varphi^2 - 0.2871\varphi^3\right]\mu_{\rm bf}
$$
\n(16)

Based on the sensitivity test results in Fig. [11](#page-20-2) and given the curvature of the green line, the viscosity of base fuid has a higher contribution to the concentration variable in calculating the viscosity of the nanofuid.

There is a base fluid viscosity variable  $\mu_{\text{bf}}$  in most of the correlations reviewed here and in the known nanofuid viscosity models, and this factor determines the viscosity value of the base fuid relative to the reference temperature in the viscosity models, so the efects of temperature through the base fuid viscosity variable are considered in viscosity models. Therefore, the high dependence of the viscosity models on the variable of base fuid viscosity is due to the dependence of the viscosity models on temperature.

It is concluded that the efects of temperature are not directly considered in the correlations, and the  $\mu_{\rm bf}$  component is not an independent variable, which can cause problems.

Viscosity correlations of Acceptable (reliable)/% Rejected nanofluids		$(unreliable)/\%$
Statistically status	53.6	46.4
Physical examination	73.2	26.8
Total status	35.7	64.3

<span id="page-21-0"></span>**Table 2** Status of statistical and physical analysis of all equations of Table [1](#page-4-0)

According to the issues mentioned above and based on the sensitivity analysis results performed on viscosity models, the temperature factor plays a decisive role in viscosity models. Therefore, the results show the inherent dependence of nanofuid viscosity on temperature.

### **Overall analysis of empirical correlations**

Table [1](#page-4-0) is statistically and physically examined the prediction correlations of nanofuid viscosity. In the statistical study, variance analysis for temperature and volume (mass) fraction of nanofuid has been performed, and the results have been presented in the column related to the statistical study. In addition, in physical examination, three factors of Data, Term, and Trend have been considered. The Data column in Table [1](#page-4-0) examines the experimental correlations' ability to respond at zero concentration to reach the value of the base fuid viscosity. In the Term column of Table [1,](#page-4-0) the results have been mentioned regarding the existence of numerous and irrational terms for estimating the viscosity of the mentioned experimental correlations. The compliance and the role of the variables introduced in the empirical correlations presented in Table [1](#page-4-0) relative to the physics governing the viscosity of the nanofuid are evaluated in the Trend column of Table [1.](#page-4-0)

In evaluating viscosity relationships, it was observed that there are relationships that have good conditions in the physical examination but are not statistically similar. Also, reverse conditions for equations are possible. Therefore, it was decided to report the relationships with good status in two physical and statistical states in the total section.

By examining all the correlations in Table [1](#page-4-0) and their statistical analysis and examining the physical performance of the correlations and the validity of each equation, it can be concluded that 53.6% of the equations are statistically valid. Also, 73.2% of the equations have accuracy and simplicity in terms of performance; in total, 35.7% of the equations in both physical and statistical states have an acceptable condition (Table [2\)](#page-21-0).

The results of the evaluation of the experimental correlations presented in Table [1](#page-4-0) for nanofuids based on water and ethylene glycol, which are widely used in the feld of <span id="page-21-1"></span>**Table 3** Status of evaluation of viscosity equations based on waterbased nanofuid



<span id="page-21-2"></span>



research, have been developed. Accordingly, in a comprehensive study on the correlations of Table [1](#page-4-0) for water-based nanofuids, it is statistically and physically determined that statistically, 38.9% of the correlations are acceptable, 83.3% are physically reliable correlations, and a total of 27.7% of the correlations are acceptable. The results of this study are presented in Table [3.](#page-21-1)

Suppose the examination for water-based nanofuid is performed again for ethylene glycol-based nanofuids, as shown in Table [4](#page-21-2). In that case, 54.5% of the correlations are statistically acceptable, 54.5% are physically reliable, and a total of 27.2% of the ethylene glycol-based nanofuid equations in both physical and statistical states had an acceptable condition.

Thus, the statistically and physically acceptable correlations for the water- and ethylene glycol-based nanofuid are presented in Tables [5](#page-22-0) and [6](#page-22-1).

### **Proposing a viscosity model and its validation**

#### **Preliminary analysis**

By studying the correlations proposed by the researchers, the relationship of variables with the viscosity of nanofuid was determined. Therefore, it was confrmed by the analysis of variance that temperature and concentration variables play a decisive role in the relationship between the viscosity of nanofuids. In addition, the results of the statistical tools of sensitivity analysis showed that the viscosity of nanofuid is directly dependent on the temperature factor.

<span id="page-22-0"></span>

No	Author	Correlation	Material Nanoparticle (Base fluid)
	Duangthongsuk and Wong- wises $\lceil 21 \rceil$	$\mu_{\rm nf} = [(a_1 + a_2 \varphi + a_3 \varphi^2)] \mu_{\rm bf}$	$TiO2$ (water)
2	Moldoveanu et al. [53]	Al <sub>2</sub> O <sub>3</sub> : $\mu_{\text{nf}} = [4135\varphi^2 - 91.72\varphi + 2.06]\mu_{\text{hf}}$ $\text{SiO}_2$ : $\mu_{\text{nf}} = \left[-769\varphi^2 + 42\varphi + 1.1\right]\mu_{\text{bf}}$	$Al_2O_3$ , SiO <sub>2</sub> , Hybrid Separately (Water)
3	Moldoveanu et al. [54]	Al <sub>2</sub> O <sub>3</sub> : $\mu_{\text{nf}} = [0.6152\varphi^2 - 1.5449\varphi + 2.3792]\mu_{\text{hf}}$ $\text{TiO}_2$ : $\mu_{\text{nf}} = [0.2302\varphi^2 - 0.3202\varphi + 1.5056]\mu_{\text{bf}}$	$Al_2O_3$ , TiO <sub>2</sub> , Hybrid Separately (Water)
$\overline{4}$ 5	Toghraie et al. [68] Dalkilic et al. 2016	$\mu_{\rm nf} = [1.01 + (0.007165T^{1.171}\varphi^{1.509}) \times \exp(-0.00719T\varphi)]\mu_{\rm bf}$ $\mu_{\rm nf} = 1.1686\mu_{\rm bf} + 1.3764 \times 10^{-4} \varphi - 1.8027 \times 10^{-4}$	$Fe3O4$ (water) Graphite (Water)

<span id="page-22-1"></span>**Table 6** Acceptable correlations for the viscosity of ethylene glycol-based nanofuid



<span id="page-22-2"></span>**Fig. 12** Three-dimensional representation of the viscosity dispersion of nanofuids with water-based nanofluid. [[21](#page-31-13), [43](#page-32-13), 64, 78, 81-84]



Given that the volume fraction variable of nanoparticles afects nanofuid's viscosity, and the rate of viscosity changes relative to the volume fraction of nanoparticles depends on the type of the base fuid.

On the other hands, it is crucial for the viscosity of the nanofuid with water-based nanofuid and ethylene glycol, which does not have limited use in terms of temperature, volume fraction, and especially particle material. Therefore, in the present study, two models with very high accuracy for nanofuids with water-based nanofuid in a wide range of volume fractions and temperature have been presented, and this important has been done for ethylene glycol-based nanofluid.

Evaluating the experimental studies on the viscosity of nanofuids in proportion to temperature and concentration, approximately the physical conditions of more than 1200

<span id="page-23-0"></span>

experimental data were examined, and dispersed viscosity values were observed for the experimental data under the same physical conditions. Therefore, to increase the accuracy of the proposed correlation, a group of articles has been removed, and articles with appropriate and centralized experimental data have been selected to provide the correlation.

Figure [12](#page-22-2) is plotted in terms of temperature and volume fraction of the water-based nanofuid to know the physical condition of the experimental data used. [[21](#page-31-13), [43](#page-32-13), [64](#page-33-3), [78,](#page-33-17) [81](#page-33-20)[–84](#page-33-21)]

Figure [12](#page-22-2) shows that the congestion of experimental data for the viscosity of water-based nanofuid at concentrations less than 1%, and the temperature range of 30 to 40 °C is higher.

Also, the dispersion of experimental data to present the viscosity model is shown in Fig. [13](#page-23-0) in terms of temperature and volume fraction of ethylene glycol-based nanofuid. [[55,](#page-32-31) [85](#page-33-22)[–88](#page-33-23)]

Also, according to Fig. [13,](#page-23-0) at low concentrations and the temperature range of 30 to 50 °C, the viscosity of ethylene glycol-based nanofuid has higher congestion.

### **Proposed correlation**

Experimental viscosity correlations proposed by previous researchers cover a limited temperature range and volume fraction. Most experimental correlations proposed for nanofuid viscosity are unable to estimate the base fuid viscosity. On the other hands, in the analysis of variance, it was found that most of the mentioned correlations do not depend on the independent variables of those correlations. The sensitivity analysis results also showed that the factor of temperature

directly affects the viscosity of nanofluid, and the variable of temperature has a more signifcant contribution in estimating the viscosity of nanofuid than other variables. In such conditions, to eliminate these shortcomings, a model has been presented for estimating the viscosity of water- and ethylene glycol-based nanofuid entitled BAG, Barkhordar-Armaghani-Ghasemiasl. The summary of the statistical and physical study of the BAG model is given in Table [7.](#page-24-0) According to the variance analysis, the temperature variable and the volume fraction have the appropriate P Values for the BAG model.

The results of estimating the viscosity of water- and ethylene glycol-based nanofuid based on the BAG model in Table [7](#page-24-0) compared to the experimental data in Figs. [12](#page-22-2) and [13](#page-23-0) based on  $\mathbb{R}^2$  of water-based nanofluid are 97.01% and for ethylene glycol-based nanofuid are 96.08%.

### **Evaluation of BAG viscosity model**

For assessing the validity of the accuracy of the presented correlations, it is necessary to compare the obtained results with the conventional and selected correlations. For this purpose, some conventional correlations in articles are introduced as follows. Einstein [\[1](#page-31-0)] was the frst to introduce a microfuidic viscosity model for suspensions containing metal particles in 1906. This correlation applies to the viscosity of microfuid with spherical particles at a volume fraction of less than 5%. This model is given in Eq. ([17\)](#page-23-1).

$$
\mu_{\rm nf} = (1 + 2.5\varphi)\mu_{\rm bf} \tag{17}
$$

<span id="page-23-1"></span>Brinkman [\[19\]](#page-31-11) proposed a new model in 1952 according to Einstein's model. This correlation is suitable for

#### <span id="page-24-0"></span>**Table 7** BAG models for nanofuids viscosity



suspensions with a volume fraction of less than 4%. This correlation is given in Eq. [\(18\)](#page-24-1), used in most studies by researchers.

$$
\mu_{\rm nf} = \left(\frac{1}{\left(1-\varphi\right)^{2.5}}\right) \mu_{\rm bf} \tag{18}
$$

In 1977, Batchelor [[20\]](#page-31-12) proposed a viscosity model for single-phase suspensions based on the Brownian motion of particles. Moreover, Eq. [\(19\)](#page-24-2) is derived according to the Einstein equation and the existence of spherical particles.

$$
\mu_{\rm nf} = (1 + 2.5\varphi + 6.2\varphi^2)\mu_{\rm bf} \tag{19}
$$

In recent studies, Wang et al. [\[89](#page-33-24)] performed experiments on  $Al_2O_3$  nanofluids separately for water and ethylene glycol-based nanofluid. Equations  $(20)$  and  $(21)$  $(21)$  $(21)$  are obtained for water-based  $Al_2O_3$  nanofluid and ethylene glycol-based  $Al_2O_3$  nanofluid.

$$
\mu_{\rm nf} = (1 + 7.3\varphi + 123\varphi^2)\mu_{\rm bf} \tag{20}
$$

$$
\mu_{\rm nf} = (1 + 4.6\varphi + 6.7\varphi^2)\mu_{\rm bf} \tag{21}
$$

In another study, Chen et al. [[90\]](#page-33-25) presented Eq. [\(22\)](#page-24-5) for nanofuid viscosity. This correlation has been used in numerous previous articles.

$$
\mu_{\rm nf} = (1 + 10.6\varphi + (10.6\varphi)^2)\mu_{\rm bf} \tag{22}
$$

Ho et al. [\[91\]](#page-33-26) then performed an experimental experiment based on convection heat transfer and examined the variation trend of viscosity with increasing nanofuid concentration and presented Eq. ([23\)](#page-24-6).

<span id="page-24-6"></span>
$$
\mu_{\rm nf} = (1 + 4.93\varphi + 222.4\varphi^2)\mu_{\rm bf} \tag{23}
$$

<span id="page-24-1"></span>Then, the results of estimating the viscosity of waterbased nanofuid based on the BAG I model in row 1 of Table [7](#page-24-0) have been evaluated with the conventional and selected correlations in Eqs.  $(17)$  $(17)$  to  $(23)$  $(23)$  according to the experimental data in Fig. [12.](#page-22-2)

<span id="page-24-2"></span>In Fig. [14](#page-25-0), parts a and b, the results for the nanofuid viscosity have been plotted at the temperature of 20 and 50 °C and a variable volume fractions of 0 to 3%, respectively. In the results, where scattered data are available, the values estimated by the BAG I model are more accurate than the points where the data are most concentrated.

<span id="page-24-3"></span>Given that the present study uses a variety of experimental data, the experimental data used in this study have been extracted from several sources; also, the existence of data scatter in constant physical conditions seems reasonable. Therefore, in such cases, it is expected that BAG models can predict the values in which the data are more focused.

<span id="page-24-4"></span>According to Fig. [14,](#page-25-0) parts c and d, the results for the nanofuid viscosity have been plotted at volume fractions of 0.1 and 1% and a variable temperature of 20–60 °C, respectively. The results indicated the BAG I model accurately predicts nanofuid viscosity according to the trend of temperature changes.

<span id="page-24-5"></span>In another analysis, the BAG I model with the acceptable correlations in Table [1](#page-4-0) for water-based nanofuid has been examined based on the experimental data in Fig. [12.](#page-22-2)



<span id="page-25-0"></span>**Fig. 14** Comparison of BAG I model with conventional correlations in Eqs. [\(17\)](#page-23-1) to [\(23\)](#page-24-1)

However, the accuracy range of the acceptable correlations in Table [1](#page-4-0) is not the same as the range of experimental data in Fig. [12](#page-22-2), but to quantitatively express the estimation of the considered correlations relative to the BAG I model, which can estimate over a wide range of temperature 5–60 °C and volume fraction 0–3%. The results in the same physical conditions in Fig. [14](#page-25-0) is also shown in Fig. [15](#page-26-0); as can be seen, the results obtained from the BAG I model relative to the acceptable correlations in Table [1](#page-4-0) are in good agreement with the experimental data.

RMSE measures the error rate of two datasets. This parameter compares the predicted values and the experiment's values with each other, and the lower value leads to the lower error of the model. Thus, RMSE is an appropriate tool to compare correlations.

Based on Eqs. [24](#page-26-1) and [25,](#page-26-2) to determine the error of the equations in predicting the experimental viscosity values, the "root mean square error," or RMSE index, has been used. Also, the accuracy of the equations in estimating the experimental viscosity values is expressed by the R-squared index.

Table [8](#page-26-3) shows the RMSE values obtained for the conventional correlations and acceptable correlations in Table [1](#page-4-0) and the BAG I model on the experimental points for estimating the viscosity of the water-based nanofuid.



<span id="page-26-0"></span>**Fig. 15** A comparison of the BAG I model with acceptable correlations appeared in Table [1](#page-4-0)

<span id="page-26-3"></span>**Table 8** The RMSE value of the BAG I model compared to other correlations for water-based nanofuids

Equations	<b>RMSE</b>
Einstien $[18]$	0.083422758
Batchelor [20]	0.083058883
Wang $[89]$	0.066209608
Chen $[90]$	0.062280061
Ho $[91]$	0.069636179
Duangthongsuk [21]	0.060700168
Moldoveanu [53]	0.173518889
Dalkilic [78]	0.081515186
BAG I	0.038959537

<span id="page-26-1"></span>RMSE = 
$$
\sqrt{\frac{\sum_{i=1}^{N} (\mu_{\text{pre}} - \mu_{\text{exp}})^2}{N}}
$$
 (24)

<span id="page-26-2"></span>
$$
R^{2} = 1 - \frac{\sum_{i=1}^{N} (\mu_{\text{pre}} - \mu_{\text{exp}})}{\sum_{i=1}^{N} (\mu_{\text{pre}} - \overline{\mu_{\text{exp}}})}
$$
(25)

Findings based on the RMSE value indicate that the BAG I model has a 35.82% lower performance error than the best correlation presented by the researchers to estimate the viscosity of water-based nanofuids.

<span id="page-27-0"></span>



In addition, the diagram of the results of the  $R^2$  coefficient for the conventional and acceptable correlations of Table [1](#page-4-0) and the BAG I model is presented in Fig. [16.](#page-27-0) Besides the reasonable accuracy of other correlations in estimating nanofuid viscosity, the BAG I model has higher accuracy than other correlations in estimating nanofuid viscosity according to the trend of nanofuid viscosity changes.

In most studies on the viscosity of nanofuids, especially the conventional correlations, the correlations cannot predict the viscosity of nanofuids with the ethylene glycol-based nanofuid. One of the reasons for the weakness of these correlations is the high concentration of ethylene glycol-based nanofuid viscosity relative to water. On the other hands, usual correlations have been optimized for the viscosity of low concentration nanofuids. Therefore, conventional correlations do not respond proportionally to the nanofuid's viscosity with the ethylene glycol-based nanofuid. With these interpretations, the BAG II model for the viscosity for the nanofuids with ethylene glycol-based nanofuid has high accuracy for estimating viscosity.

Then, the results of estimating the viscosity of ethylene glycol-based nanofuid based on the BAG II model in row 1 of Table [7](#page-24-0) have been evaluated with the conventional and selected correlations in Eqs.  $(17)$  to  $(23)$  $(23)$  according to the experimental data in Fig. [13.](#page-23-0)

In Fig. [17](#page-28-0), parts a and b, the viscosity of the nanofuid is, respectively, at 30 and 50 °C and the variable concentration. In sections c and d, the results for the nanofuid viscosity have been plotted at volume fractions of 0.2 and 0.8% and variable temperature, respectively.

As expected, because the conventional correlations for the viscosity of nanofuids with the water-based nanofuid have been optimized, they cannot estimate the viscosity of nanofuids with ethylene glycol-based nanofuid. Considering the experimental data, the viscosity values predicted by the BAG II relation are much more accurate than the conventional relations.

In another analysis, the BAG II model with the acceptable correlations in Table [1](#page-4-0) for ethylene glycol-based nanofuids has been investigated based on the experimental data in Fig. [13.](#page-23-0)

However, the accuracy range of the acceptable correlations in Table [1](#page-4-0) is not the same as the range of experimental data in Fig. [13](#page-23-0), but to quantitatively present the estimation of the considered correlations relative to the BAG II model, which can estimate in a wide range of temperature 20 to 60 °C and volume fraction 0 to 2%. Also, the results are presented in Fig. [18](#page-29-0).

According to parts a and b of Fig. [18](#page-29-0), at the volume fraction range of 1–2% and temperatures of 30 and 50 °C, the BAG II model is significantly more accurately predicted than the other correlations.

Also, in Fig. [18](#page-29-0), parts c and d, at volume fractions of 0.2 and 0.8% and in the temperature range of 20–60 °C, the BAG II model has mainly provided better results than other correlations.

Table [9](#page-29-1) shows the RMSE values obtained for the conventional correlations and acceptable correlations in Table [1](#page-4-0) and the BAG II model on the experimental points for estimating the viscosity of the ethylene glycol-based nanofuid.

Findings based on the RMSE value indicate that the BAG II model has a 49.84% lower performance error than the best correlation presented by the researchers to estimate the viscosity of ethylene glycol-based nanofuids.



<span id="page-28-0"></span>**Fig. 17** Comparison of BAG I model with conventional correlations in Eqs. [\(17\)](#page-23-1) to [\(23\)](#page-24-1)

To know the accuracy of the BAG II model for ethylene glycol in terms of  $\mathbb{R}^2$  coefficient, Fig. [19](#page-29-2) is plotted. The results show that the accuracy of the BAG II model is signifcantly higher than other correlations.

The base fluid viscosity parameter  $\mu_{bf}$  is available in most of the correlations presented in Table [1](#page-4-0) and the conventional correlations for calculating nanofuid viscosity. In this case, the viscosity of the base fuid plays the role of the variable temperature of the base fuid in addition to its role in the calculations so that the viscosity of the base fuid changes with the change of temperature. Therefore, the viscosity of the base fuid must also show the efect of temperature. Thus, by assuming the nanofuid type to be constant with temperature change, the base fuid viscosity in the nanofuid viscosity estimation correlation changes. On the other hands, in the nanofuid viscosity estimation correlations, the nanofuid temperature factor is not directly present in the above correlations. Therefore, these correlations alone are not able to estimate the nanofuid viscosity. Thus, when the nanofuid temperature is variable, the mentioned correlations increase the error probability in the calculations.



<span id="page-29-0"></span>**Fig. 18** A comparison of the BAG II model with acceptable correlations appeared in Table [1](#page-4-0)

<span id="page-29-1"></span>**Table 9** The RMSE value of the BAG II model compared to other correlations for ethylene glycol-based nanofuid





<span id="page-29-2"></span>**Fig. 19** The value of  $\mathbb{R}^2$  in the BAG II model compared to other correlations for ethylene glycol-based nanofuid



<span id="page-30-0"></span>**Fig. 20** Estimation of water- and ethylene glycol-based nanofuid viscosity using the BAG model

Also, while solving numerical problems of heat transfer due to temperature changes in the problem, it is sometimes impossible to change the base fuid's viscosity in the problem, which deviates the answer from the correct path. Therefore, the presence of a temperature variable in viscosity models is also felt here. Under such circumstances, the BAG model in Table [7](#page-24-0) could be a turning point for other viscosity models in the future.

According to the above, another strength of BAG models is the ability to estimate the viscosity of the base fuid in the conventional temperature range used in heat transfer, which is less likely to provide a suitable response at zero concentration. To demonstrating the relationship ability of BAG, the values predicted by the BAG relation are examined with the experimental values of the viscosity of waterbased nanofuid and ethylene glycol in Fig. [20](#page-30-0), parts a and b, respectively.

### **Conclusions**

The viscosity component plays a crucial role in heat transfer, especially convection heat transfer. The addition of nanoparticles to the base fuid is commonly considered to increase the viscosity rate. With the increase in the number of nanofuid viscosity models proposed, it has become necessary to review these models in the present study. We also evaluated the correlations in terms of physical compatibility with the viscosity of nanofuids and performed statistical tests of variance and sensitivity analysis on the viscosity models.

Finally, based on the weakness identifed in previous models, through our statistical and correlation evaluations, two general equations for water- and ethylene glycol-based nanofuids were presented to predict the behavior of nanofuids. A summary of the results presented in this study is as follow;

- The results of variance analysis on the viscosity correlations showed the non-dependence of 42.2% of the correlations on the temperature component and another 27.3% on the volume (mass) fraction component.
- The volume (mass) fraction variables in nanofluid viscosity models are valid only in a certain range, and most correlations are not able to provide a solution at a zero volume (mass) fraction. Therefore, most nanofuid viscosity models do not cover the range of volume (mass) fractions used in heat transfer.
- In some of the viscosity models introduced by researchers, correlations sometimes have complex and long terms unrelated to viscosity physics. The presence of such terms in viscosity models only increases the likelihood of errors in calculations. However, many of these correlations can be corrected and modifed with simple and short models.
- According to the study conducted physically and statistically on the viscosity models of nanofuids, only 53.6% of the correlations are statistically acceptable, and 73.2% of the correlations are physically reliable, and a total of 35.7% of the correlations have acceptable conditions.
- Sensitivity analysis revealed the signifcant contribution of temperature component in estimating nanofuid vis-

cosity. It is while the efect of temperature in the form of nanofuid viscosity models is not directly considered. Instead, the effect of temperature is determined by the independent variable of base fluid viscosity  $\mu_{\text{bf}}$  in the desired viscosity models. Therefore, the viscosity models cannot estimate the nanofuid's viscosity in proportion to the temperature variation trend, and this factor can cause problems.

- For modeling, the viscosity of nanofluids separated to water or ethylene glycol-based nanofuids, which is valid in a wide temperature and volume fraction range and function independent of the type of nanoparticles, BAG models were introduced.
- The BAG models presented for nanofluid viscosity for water- and ethylene glycol-based nanofuid have 97.01% and 96.08% accuracy, respectively. Also, the RMSE value improved by 35.82% and 49.84% compared to the best correlation presented by the researchers for estimating the viscosity of water-based and ethylene glycolbased nanofuids, respectively.
- Most of the viscosity models have been optimized for nanofuids with water-based nanofuids. However, the BAG model has the ability to estimate the viscosity of nanofluid with ethylene glycol-based nanofluid with much higher accuracy than other correlations.
- Unlike other correlations, the results of BAG models showed that by changing the temperature of the nanofuid, BAG models maintain the ability to estimate the viscosity of the nanofuid accurately. Also, when the nanoparticle concentration is zero, the viscosity of the base fuid is well predicted.

Given that nanofuid with the oil base such as the applied fuids in industry and few correlations have been provided for oil-based nanofuids. Therefore, developing correlations for oil-based nanofuids is a challenge and an open feld of research.

## **References**

- <span id="page-31-0"></span>1. Mondal S, et al. A theoretical nanofuid analysis exhibiting hydromagnetics characteristics employing CVFEM. J Braz Soc Mech Sci Eng. 2020;42(1):1–12.
- 2. Seyyedi SM, Dogonchi A, Hashemi-Tilehnoee M, Ganji D, Chamkha AJ. Second law analysis of magneto-natural convection in a nanofuid flled wavy-hexagonal porous enclosure. Int J Numer Methods Heat Fluid Flow. 2020;30:4811.
- <span id="page-31-1"></span>3. Dogonchi A, Waqas M, Seyyedi SM, Hashemi-Tilehnoee M, Ganji D. A modifed Fourier approach for analysis of nanofuid heat generation within a semi-circular enclosure subjected to MFD viscosity. Int Commun Heat Mass Trans. 2020;111:104430.
- <span id="page-31-2"></span>4. Tlili I, Seyyedi SM, Dogonchi A, Hashemi-Tilehnoee M, Ganji D. Analysis of a single-phase natural circulation loop with hybridnanofuid. Int Commun Heat Mass Trans. 2020;112:104498.
- 5. Dogonchi A, Waqas M, Gulzar MM, Hashemi-Tilehnoee M, Seyyedi SM, Ganji D. Simulation of Fe3O4-H2O nanoliquid in a triangular enclosure subjected to Cattaneo-Christov theory of heat conduction. Int J Numer Methods Heat Fluid Flow. 2019;29:4430.
- 6. Seyyedi SM, Dogonchi A, Hashemi-Tilehnoee M, Waqas M, Ganji D. Investigation of entropy generation in a square inclined cavity using control volume fnite element method with aided quadratic Lagrange interpolation functions. Int Commun Heat Mass Transf. 2020;110:104398.
- <span id="page-31-3"></span>7. Abdelmalek Z, Tayebi T, Dogonchi A, Chamkha A, Ganji D, Tlili I. Role of various confgurations of a wavy circular heater on convective heat transfer within an enclosure flled with nanofuid. Int Commun Heat Mass Trans. 2020;113:104525.
- <span id="page-31-4"></span>8. Sadeghi M, Tayebi T, Dogonchi A, Nayak M, Waqas M. Analysis of thermal behavior of magnetic buoyancy-driven fow in ferrofuid–flled wavy enclosure furnished with two circular cylinders. Int Commun Heat Mass Trans. 2021;120:104951.
- 9. Hashemi-Tilehnoee M, Dogonchi A, Seyyedi SM, Sharifpur M. Magneto-fuid dynamic and second law analysis in a hot porous cavity flled by nanofuid and nano-encapsulated phase change material suspension with diferent layout of cooling channels. J Energy Storage. 2020;31:101720.
- <span id="page-31-5"></span>10. Dogonchi A, Asghar Z, Waqas M. CVFEM simulation for Fe3O4- H2O nanofuid in an annulus between two triangular enclosures subjected to magnetic feld and thermal radiation. Int Commun Heat Mass Trans. 2020;112:104449.
- <span id="page-31-6"></span>11. Dogonchi A, Selimefendigil F, Ganji D. Magneto-hydrodynamic natural convection of CuO-water nanofuid in complex shaped enclosure considering various nanoparticle shapes. Int J Numer Methods Heat Fluid Flow. 2019;5:1663.
- 12. Selimefendigil F. Natural convection in a trapezoidal cavity with an inner conductive object of diferent shapes and flled with nanofuids of diferent nanoparticle shapes. Iran J Sci Technol Transact Mech Eng. 2018;42(2):169–84.
- <span id="page-31-7"></span>13. Selimefendigil F, Öztop HF (2020) Efects of a rotating tube bundle on the hydrothermal performance for forced convection in a vented cavity with Ag–MgO/water hybrid and CNT–water nanofuids. J Therm Anal Calorim, pp. 1–18, 2020
- <span id="page-31-8"></span>14. Chamkha AJ, Molana M, Rahnama A, Ghadami F. On the nanofuids applications in microchannels: a comprehensive review. Powder Technol. 2018;332:287–322.
- 15. Izadi S, Armaghani T, Ghasemiasl R, Chamkha AJ, Molana M. A comprehensive review on mixed convection of nanofuids in various shapes of enclosures. Powder Technol. 2019;343:880–907.
- 16. Molana M. A comprehensive review on the nanofuids application in the tubular heat exchangers. Am J Heat Mass Transf. 2016;3(5):352–81.
- <span id="page-31-9"></span>17. Pandya NS, Shah H, Molana M, Tiwari AK. Heat transfer enhancement with nanofuids in plate heat exchangers: a comprehensive review. Eur J Mech B/Fluids. 2020;81:173–90.
- <span id="page-31-10"></span>18. Einstein A (1905) Eine neue bestimmung der moleküldimensionen, ETH Zurich
- <span id="page-31-11"></span>19. Brinkman H. The viscosity of concentrated suspensions and solutions. J Chem Phys. 1952;20(4):571–571.
- <span id="page-31-12"></span>20. Batchelor G. The effect of Brownian motion on the bulk stress in a suspension of spherical particles. J Fluid Mech. 1977;83(1):97–117.
- <span id="page-31-13"></span>21. Duangthongsuk W, Wongwises S. Measurement of temperaturedependent thermal conductivity and viscosity of TiO2-water nanofuids. Exp Thermal Fluid Sci. 2009;33(4):706–14.
- <span id="page-31-14"></span>22. Esfe MH, Saedodin S. An experimental investigation and new correlation of viscosity of ZnO–EG nanofuid at various temperatures and diferent solid volume fractions. Exp Therm Fluid Sci. 2014;55:1–5.
- <span id="page-31-15"></span>23. Sharifpur M, Adio SA, Meyer JP. Experimental investigation and model development for efective viscosity of Al2O3–glycerol

nanofuids by using dimensional analysis and GMDH-NN methods. Int Commun Heat Mass Transfer. 2015;68:208–19.

- <span id="page-32-0"></span>24. Aberoumand S, Jafarimoghaddam A, Moravej M, Aberoumand H, Javaherdeh K. Experimental study on the rheological behavior of silver-heat transfer oil nanofuid and suggesting two empirical based correlations for thermal conductivity and viscosity of oil based nanofuids. Appl Therm Eng. 2016;101:362–72.
- <span id="page-32-1"></span>25. Akbari M, Afrand M, Arshi A, Karimipour A. An experimental study on rheological behavior of ethylene glycol based nanofuid: proposing a new correlation as a function of silica concentration and temperature. J Mol Liq. 2017;233:352–7.
- <span id="page-32-2"></span>26. Li W, Zou C. Experimental investigation of stability and thermophysical properties of functionalized β-CD-TiO2-Ag nanofuids for antifreeze. Powder Technol. 2018;340:290–8.
- <span id="page-32-3"></span>27. Yu L, Bian Y, Liu Y, Xu X. Experimental investigation on rheological properties of water based nanofuids with low MWCNT concentrations. Int J Heat Mass Transf. 2019;135:175–85.
- <span id="page-32-4"></span>28. Yan SR, Kalbasi R, Nguyen Q, Karimipour A (2020) Rheological behavior of hybrid MWCNTs-TiO2/EG nanofuid: a comprehensive modeling and experimental study. J Mol Liq. p. 113058
- <span id="page-32-5"></span>29. Molana M, Ghasemiasl R, Armaghani T (2021) A diferent look at the efect of temperature on the nanofuids thermal conductivity: focus on the experimental-based models. J Therm Anal Calorim, pp. 1–25
- <span id="page-32-6"></span>30. Fisher RA (1992) Statistical methods for research workers. In: Breakthroughs in statistics: Springer, 1992, pp. 66–70
- <span id="page-32-7"></span>31. Schefe H. The analysis of variance. New Jersey: John Wiley & Sons; 1999.
- <span id="page-32-8"></span>32. Dalkılıç AS, et al. Experimental investigation on the viscosity characteristics of water based SiO2-graphite hybrid nanofuids. Int Commun Heat Mass Transfer. 2018;97:30–8.
- <span id="page-32-9"></span>33. Li L, Zhai Y, Jin Y, Wang J, Wang H, Ma M. Stability, thermal performance and artifcial neural network modeling of viscosity and thermal conductivity of Al2O3-ethylene glycol nanofuids. Powder Technol. 2020;363:360–8.
- <span id="page-32-19"></span>34. Alarif IM, Alkouh AB, Ali V, Nguyen HM, Asadi A. On the rheological properties of MWCNT-TiO2/oil hybrid nanofuid: An experimental investigation on the efects of shear rate, temperature, and solid concentration of nanoparticles. Powder Technol. 2019;355:157–62.
- <span id="page-32-21"></span>35. Ruhani B, Barnoon P, Toghraie D. Statistical investigation for developing a new model for rheological behavior of Silica–ethylene glycol/Water hybrid Newtonian nanofuid using experimental data. Physica A. 2019;525:616–27.
- <span id="page-32-26"></span>36. Huminic A, Huminic G, Fleacă C, Dumitrache F, Morjan I. Thermo-physical properties of water based lanthanum oxide nanofuid. An experimental study. J Mol Liq. 2019;287:111013.
- <span id="page-32-22"></span>37. Esfe MH, Esfandeh S, Niazi S. An experimental investigation, sensitivity analysis and RSM analysis of MWCNT (10)-ZnO (90)/10W40 nanofuid viscosity. J Mol Liq. 2019;288:111020.
- <span id="page-32-18"></span>38. Esfe MH, Abad ATK, Fouladi M. Efect of suspending optimized ratio of nano-additives MWCNT-Al2O3 on viscosity behavior of 5W50. J Mol Liq. 2019;285:572–85.
- <span id="page-32-14"></span>39. Esfe MH, Esfandeh S. The statistical investigation of multi-grade oil based nanofuids: Enriched by MWCNT and ZnO nanoparticles. Phys A Stat Mech Appl. 2019;554:122159.
- <span id="page-32-10"></span>40. Li Z, Asadi S, Karimipour A, Abdollahi A, Tlili I. Experimental study of temperature and mass fraction efects on thermal conductivity and dynamic viscosity of SiO2-oleic acid/liquid paraffin nanofuid. Int Commun Heat Mass Trans. 2020;110:104436.
- <span id="page-32-11"></span>41. Sahoo RR, Kumar V. Development of a new correlation to determine the viscosity of ternary hybrid nanofuid. Int Commun Heat and Mass Trans. 2020;111:104451.
- <span id="page-32-12"></span>42. Tian Z, et al. Prediction of rheological behavior of a new hybrid nanofuid consists of copper oxide and multi wall carbon nanotubes suspended in a mixture of water and ethylene glycol using

curve-fitting on experimental data. Phys A Stat Mech Appl. 2020;554:124101.

- <span id="page-32-13"></span>43. Li Z, et al. Nanofuids as secondary fuid in the refrigeration system: Experimental data, regression, ANFIS, and NN modeling. Int J Heat Mass Trans. 2019;144:118635.
- <span id="page-32-15"></span>44. Kumar PG, Sakthivadivel D, Meikandan M, Vigneswaran V, Velraj R. Experimental study on thermal properties and electrical conductivity of stabilized H2O-solar glycol mixture based multiwalled carbon nanotube nanofuids: developing a new correlation. Heliyon. 2019;5(8):e02385.
- <span id="page-32-16"></span>45. Asadi A, Pourfattah F. Heat transfer performance of two oil-based nanofuids containing ZnO and MgO nanoparticles; a comparative experimental investigation. Powder Technol. 2019;343:296–308.
- <span id="page-32-17"></span>46. Shahsavar A, Khanmohammadi S, Karimipour A, Goodarzi M. A novel comprehensive experimental study concerned synthesizes and prepare liquid paraffin-Fe3O4 mixture to develop models for both thermal conductivity & viscosity: a new approach of GMDH type of neural network. Int J Heat Mass Transf. 2019;131:432–41.
- <span id="page-32-20"></span>47. Li F, Li L, Zhong G, Zhai Y, Li Z. Efects of ultrasonic time, size of aggregates and temperature on the stability and viscosity of Cu-ethylene glycol (EG) nanofuids. Int J Heat Mass Transf. 2019;129:278–86.
- <span id="page-32-23"></span>48. Esfe MH, Raki HR, Emami MRS, Afrand M. Viscosity and rheological properties of antifreeze based nanofuid containing hybrid nano-powders of MWCNTs and TiO2 under diferent temperature conditions. Powder Technol. 2019;342:808–16.
- <span id="page-32-24"></span>49. Soman DP, Karthika S, Kalaichelvi P, Radhakrishnan T. Impact of viscosity of nanofuid and ionic liquid on heat transfer. J Mol Liq. 2019;291:111349.
- <span id="page-32-25"></span>50. Ruhani B, Toghraie D, Hekmatifar M, Hadian M. Statistical investigation for developing a new model for rheological behavior of ZnO–Ag (50%–50%)/Water hybrid Newtonian nanofuid using experimental data. Physica A. 2019;525:741–51.
- <span id="page-32-27"></span>51. Elcioglu EB, Yazicioglu AG, Turgut A, Anagun AS. Experimental study and Taguchi analysis on alumina-water nanofuid viscosity. Appl Therm Eng. 2018;128:973–81.
- <span id="page-32-28"></span>52. Ghasemi S, Karimipour A. Experimental investigation of the efects of temperature and mass fraction on the dynamic viscosity of CuO-paraffin nanofluid. Appl Therm Eng. 2018;128:189-97.
- <span id="page-32-29"></span>53. Moldoveanu GM, Ibanescu C, Danu M, Minea AA. Viscosity estimation of Al2O3, SiO2 nanofuids and their hybrid: an experimental study. J Mol Liq. 2018;253:188–96.
- <span id="page-32-30"></span>54. Moldoveanu GM, Minea AA, Iacob M, Ibanescu C, Danu M. Experimental study on viscosity of stabilized Al2O3, TiO2 nanofuids and their hybrid. Thermochim Acta. 2018;659:203–12.
- <span id="page-32-31"></span>55. Saeedi AH, Akbari M, Toghraie D. An experimental study on rheological behavior of a nanofuid containing oxide nanoparticle and proposing a new correlation. Phys E. 2018;99:285–93.
- <span id="page-32-32"></span>56. Karimipour A, Ghasemi S, Darvanjooghi MHK, Abdollahi A. A new correlation for estimating the thermal conductivity and dynamic viscosity of CuO/liquid paraffin nanofluid using neural network method. Int Commun Heat Mass Transfer. 2018;92:90–9.
- <span id="page-32-33"></span>57. Alrashed AA, Gharibdousti MS, Goodarzi M, de Oliveira LR, Safaei MR, Bandarra Filho EP. Effects on thermophysical properties of carbon based nanofuids: experimental data, modelling using regression, ANFIS and ANN. Int J Heat Mass Trans. 2018;125:920–32.
- <span id="page-32-34"></span>58. Khodadadi H, Toghraie D, Karimipour A. Efects of nanoparticles to present a statistical model for the viscosity of MgO-Water nanofuid. Powder Technol. 2019;342:166–80.
- <span id="page-32-35"></span>59. Esfe MH, Arani AAA. An experimental determination and accurate prediction of dynamic viscosity of MWCNT (% 40)-SiO2 (% 60)/5W50 nano-lubricant. J Mol Liq. 2018;259:227–37.
- <span id="page-32-36"></span>60. Esfe MH, Reiszadeh M, Esfandeh S, Afrand M. Optimization of MWCNTs (10%)–Al2O3 (90%)/5W50 nanofuid viscosity

using experimental data and artifcial neural network. Phys A. 2018;512:731–44.

- <span id="page-33-0"></span>61. Hamid KA, Azmi W, Nabil M, Mamat R, Sharma K. Experimental investigation of thermal conductivity and dynamic viscosity on nanoparticle mixture ratios of TiO2-SiO2 nanofuids. Int J Heat Mass Transf. 2018;116:1143–52.
- <span id="page-33-1"></span>62. Nabil M, Azmi W, Hamid KA, Mamat R, Hagos FY. An experimental study on the thermal conductivity and dynamic viscosity of TiO2-SiO2 nanofuids in water: ethylene glycol mixture. Int Commun Heat Mass Transfer. 2017;86:181–9.
- <span id="page-33-2"></span>63. Żyła G, Fal J. Viscosity, thermal and electrical conductivity of silicon dioxide–ethylene glycol transparent nanofuids: an experimental studies. Thermochim Acta. 2017;650:106–13.
- <span id="page-33-3"></span>64. Amani M, Amani P, Kasaeian A, Mahian O, Kasaeian F, Wongwises S. Experimental study on viscosity of spinel-type manganese ferrite nanofuid in attendance of magnetic feld. J Magn Magn Mater. 2017;428:457–63.
- <span id="page-33-4"></span>65. Soltani O, Akbari M. Efects of temperature and particles concentration on the dynamic viscosity of MgO-MWCNT/ethylene glycol hybrid nanofluid: experimental study. Physica E. 2016;84:564–70.
- <span id="page-33-5"></span>66. Ilhan B, Kurt M, Ertürk H. Experimental investigation of heat transfer enhancement and viscosity change of hBN nanofuids. Exp Thermal Fluid Sci. 2016;77:272–83.
- <span id="page-33-6"></span>67. Esfe MH, Ahangar MRH, Rejvani M, Toghraie D, Hajmohammad MH. Designing an artifcial neural network to predict dynamic viscosity of aqueous nanofuid of TiO2 using experimental data. Int Commun Heat Mass Transfer. 2016;75:192–6.
- <span id="page-33-7"></span>68. Toghraie D, Alempour SM, Afrand M. Experimental determination of viscosity of water based magnetite nanofuid for application in heating and cooling systems. J Magn Magn Mater. 2016;417:243–8.
- <span id="page-33-8"></span>69. Abdolbaqi MK, et al. Experimental investigation and development of new correlation for thermal conductivity and viscosity of BioGlycol/water based SiO2 nanofuids. Int Commun Heat Mass Transfer. 2016;77:54–63.
- <span id="page-33-9"></span>70. Sundar LS, Hortiguela MJ, Singh MK, Sousa AC. Thermal conductivity and viscosity of water based nanodiamond (ND) nanofuids: An experimental study. Int Commun Heat Mass Transfer. 2016;76:245–55.
- <span id="page-33-10"></span>71. Mostafzur R, Aziz AA, Saidur R, Bhuiyan M. Investigation on stability and viscosity of SiO2–CH3OH (methanol) nanofuids. Int Commun Heat Mass Transfer. 2016;72:16–22.
- <span id="page-33-11"></span>72. Asadi M, Asadi A. Dynamic viscosity of MWCNT/ZnO–engine oil hybrid nanofuid: an experimental investigation and new correlation in diferent temperatures and solid concentrations. Int Commun Heat Mass Transfer. 2016;76:41–5.
- <span id="page-33-12"></span>73. Adio SA, Mehrabi M, Sharifpur M, Meyer JP. Experimental investigation and model development for efective viscosity of MgO–ethylene glycol nanofuids by using dimensional analysis, FCM-ANFIS and GA-PNN techniques. Int Commun Heat Mass Transfer. 2016;72:71–83.
- <span id="page-33-13"></span>74. Esfe MH, Afrand M, Gharehkhani S, Rostamian H, Toghraie D, Dahari M. An experimental study on viscosity of alumina-engine oil: efects of temperature and nanoparticles concentration. Int Commun Heat Mass Transfer. 2016;76:202–8.
- <span id="page-33-14"></span>75. Baratpour M, Karimipour A, Afrand M, Wongwises S. Efects of temperature and concentration on the viscosity of nanofuids made of single-wall carbon nanotubes in ethylene glycol. Int Commun Heat Mass Transfer. 2016;74:108–13.
- <span id="page-33-15"></span>76. Afrand M, Najafabadi KN, Akbari M. Efects of temperature and solid volume fraction on viscosity of SiO2-MWCNTs/SAE40 hybrid nanofuid as a coolant and lubricant in heat engines. Appl Therm Eng. 2016;102:45–54.
- <span id="page-33-16"></span>77. Abdolbaqi MK, et al. An experimental determination of thermal conductivity and viscosity of BioGlycol/water based TiO2 nanofuids. Int Commun Heat Mass Transfer. 2016;77:22–32.
- <span id="page-33-17"></span>78. Dalkilic A, et al. Prediction of graphite nanofuids' dynamic viscosity by means of artifcial neural networks. Int Commun Heat Mass Transfer. 2016;73:33–42.
- <span id="page-33-18"></span>79. Li X, Zou C, Lei X, Li W. Stability and enhanced thermal conductivity of ethylene glycol-based SiC nanofuids. Int J Heat Mass Transf. 2015;89:613–9.
- <span id="page-33-19"></span>80. Saltelli A, et al. Global sensitivity analysis: the primer. New Jersey: John Wiley & Sons; 2008.
- <span id="page-33-20"></span>81. Gangadevi R, Vinayagam B. Experimental determination of thermal conductivity and viscosity of diferent nanofuids and its efect on a hybrid solar collector. J Therm Anal Calorim. 2019;136(1):199–209.
- 82. Topuz A, Engin T, Özalp AA, Erdoğan B, Mert S, Yeter A. Experimental investigation of optimum thermal performance and pressure drop of water-based Al 2 O 3, TiO 2 and ZnO nanofuids fowing inside a circular microchannel. J Therm Anal Calorim. 2018;131(3):2843–63.
- 83. Ghodsinezhad H, Sharifpur M, Meyer JP. Experimental investigation on cavity fow natural convection of Al2O3–water nanofuids. Int Commun Heat Mass Transfer. 2016;76:316–24.
- <span id="page-33-21"></span>84. Sundar LS, Singh MK, Sousa AC. Turbulent heat transfer and friction factor of nanodiamond-nickel hybrid nanofluids flow in a tube: an experimental study. Int J Heat Mass Transf. 2018;117:223–34.
- <span id="page-33-22"></span>85. Zadeh AD, Toghraie D. Experimental investigation for developing a new model for the dynamic viscosity of silver/ethylene glycol nanofuid at diferent temperatures and solid volume fractions. J Therm Anal Calorim. 2018;131(2):1449–61.
- 86. Sundar LS, Singh MK, Ferro M, Sousa AC. Experimental investigation of the thermal transport properties of graphene oxide/ Co3O4 hybrid nanofluids. Int Commun Heat Mass Transfer. 2017;84:1–10.
- 87. Selvam C, Lal DM, Harish S. Heat transport and pressure drop characteristics of ethylene Glycol-based Nano fuid containing silver nanoparticles. IOP Conf Ser Mater Sci Eng. 2018;402(1):012005.
- <span id="page-33-23"></span>88. Nadooshan AA, Eshgarf H, Afrand M. Measuring the viscosity of Fe3O4-MWCNTs/EG hybrid nanofuid for evaluation of thermal efficiency: Newtonian and non-Newtonian behavior. J Mol Liq. 2018;253:169–77.
- <span id="page-33-24"></span>89. Wang X, Xu X, Choi SU. Thermal conductivity of nanoparticlefuid mixture. J Thermophys Heat Transfer. 1999;13(4):474–80.
- <span id="page-33-25"></span>90. Chen H, Ding Y, Tan C. Rheological behaviour of nanofuids. New J Phys. 2007;9(10):367.
- <span id="page-33-26"></span>91. Ho C, Liu W, Chang Y, Lin C. Natural convection heat transfer of alumina-water nanofuid in vertical square enclosures: an experimental study. Int J Therm Sci. 2010;49(8):1345–53.

**Publisher's Note** Springer Nature remains neutral with regard to jurisdictional claims in published maps and institutional afliations.