# **Characterization of ignition and combustion characteristics of phenolic fber‑reinforced plastic with diferent thicknesses**

**Ruiyu Chen1,2,3 · Xiaokang Xu1 · Yang Zhang4 · Shouxiang Lu2 · Siuming Lo<sup>3</sup>**

Received: 20 May 2018 / Accepted: 5 October 2019 / Published online: 30 October 2019 © Akadémiai Kiadó, Budapest, Hungary 2019

## **Abstract**

The present study focuses on ignition and combustion characteristics of phenolic fber-reinforced plastic (FRP) with diferent thicknesses under diferent external heat fuxes using cone calorimeter, which receives little attention to date. A series of parameters including ignition time, thermal thickness, mass loss factor, mass loss rate (MLR), heat release rate (HRR), total heat release (THR), fire performance index (FPI) and fire growth index (FGI) are measured or calculated. Results indicate that the ignition time increases with the thickness, but decreases with the external heat fux. Phenolic FRP with thickness of 3 mm may be considered as thermally thin material. However, phenolic FRP with thickness of 5 and 8 mm is prone to be thermally thick material. The critical heat fux, minimum heat fux and ignition temperature are deduced and validated. The thermal thickness increases with the external heat fux. Linear correlations of the thermal thickness with the ratio of specimen density and external heat fux are demonstrated and presented. The mass loss factor decreases with the thickness. Three and two peak MLRs occur in the cases of low and high external heat fuxes, respectively. The average MLR increases with the external heat fux and thickness. The average and maximum HRR increases with the external heat fux. The FGI for the maximum HRR increases with the external heat fux. Linear correlations of the average MLR, the average and maximum HRR and the FGI for the maximum HRR with the external heat fux are demonstrated and presented.

**Keywords** Thickness · Cone calorimeter · Ignition characteristics · Combustion · Correlation · Phenolic FRP

# **Introduction**

Phenolic fber-reinforced plastic (FRP) is a typical thermosetting plastic. Owing to its prominent thermal insulation, outstanding impact resistance, and sound absorption characteristics, it is increasingly used as interior materials for

 $\boxtimes$  Ruiyu Chen crynjust@njust.edu.cn

- School of Chemical Engineering, Nanjing University of Science and Technology, Nanjing 210094, Jiangsu, People's Republic of China
- State Key Laboratory of Fire Science, University of Science and Technology of China, Hefei 230027, Anhui, People's Republic of China
- <sup>3</sup> Department of Civil and Architectural Engineering, City University of Hong Kong, Kowloon 999077, Hong Kong, People's Republic of China
- School of Science, Nanjing University of Science and Technology, Nanjing 210094, Jiangsu, People's Republic of China

buildings, aircrafts, ships, automobiles, etc. However, the fre hazard of phenolic FRP is relatively high, which may restrict its application range. It can be ignited and released large amounts of heat and poisonous gases, especially under high external heat fuxes or high-temperature conditions, such as the case of severe arson, probably involving in the combustion of other neighboring fammable materials, resulting in terrible casualties and property loss. Therefore, it is necessary and important to investigate the ignition and combustion characteristics of phenolic FRP, which are the key elements in the fre hazard evaluation of phenolic FRP.

Generally, solid combustibles can be divided into thermally thick or thermally thin material according to whether the physical thickness of the specimen is larger or less than the thermal thickness at ignition moment. If the solid combustibles are considered as thermally thick materials, heterogeneous temperature profle occurs inside the solid when they are exposed to heat. If the solid combustibles are regarded as thermally thin materials, temperature distributes almost homogeneously inside the solid when they are exposed to heat. Obviously, large diferences may



occur to the ignition and combustion characteristics of thermally thick and thermally thin materials. As a result, studies regarding the infuence of thickness on the ignition and combustion characteristics of solid combustibles, such as PS (polystyrene) [[1](#page-9-0)] and oil-impregnated transformer insulating paperboard [\[2\]](#page-9-1), have been reported employing cone calorimeter [[3](#page-9-2)[–11\]](#page-9-3).

Some studies focused on the ignition and combustion characteristics of phenolic FRP. Mouritz et al. [[12](#page-9-4), [13\]](#page-9-5) measured the ignition time of phenolic FRP under the external heat fux range of 25–100 kW m−2 employing cone calorimeter. However, combustion characteristics of phenolic FRP were not investigated in their study. In addition, Avila [[14\]](#page-9-6) investigated the efects of resin and glass content on the ignition and combustion characteristics of phenolic FRP under single external heat flux of 70 kW  $m^{-2}$ using cone calorimeter, which is generally used for determination of the ignition and combustion characteristics of solid combustibles [[15,](#page-9-7) [16\]](#page-9-8). Ignition time, mass loss rate (MLR) and heat release rate (HRR) were measured to reveal the diferences of the ignition and combustion characteristics of phenolic FRP with diferent resin and glass contents. Similarly, Ramsay et al. [[17](#page-9-9)] performed a study on the infuence of resin and glass content on the ignition and combustion characteristics of phenolic FRP under the external heat fluxes of 35, 50 and 75 kW m<sup>-2</sup> employing cone calorimeter. It should be noted that in the research of Avila  $[14]$  $[14]$  and Ramsay et al.  $[17]$ , the effects of external heat fux on the ignition and combustion characteristics of phenolic FRP were not revealed. Besides, Duggan [\[18\]](#page-9-10) measured the HRR of painted phenolic FRP under the external heat fux of 35 kW m−2. Efects of external heat fux on the ignition and combustion characteristics of phenolic FRP were not revealed either. It should be noted that all the above-mentioned studies did not focus on the efects of thickness on the ignition and combustion characteristics of phenolic FRP.

In summary, the effects of external heat flux and thickness on the ignition and combustion characteristics of phenolic FRP have not been revealed yet to date. The present study employs cone calorimeter to investigate the ignition and combustion characteristics of phenolic FRP with diferent thicknesses under diferent external heat fuxes. A series of parameters including ignition time, thermal thickness, mass loss factor, MLR, HRR, total heat release (THR), fre performance index (FPI) and fre growth index (FGI) are measured. The above-mentioned ignition and combustion parameters under diferent thicknesses and external heat fuxes are compared and analyzed. Correlations of the above ignition and combustion characteristics with the external heat fuxes are established. The critical heat fux, minimum heat fux and ignition temperature are deduced and validated.

### **Experimental**

#### <span id="page-1-1"></span>**Materials**

The phenolic FRP used for the present study was provided by Shanghai FRP Research Institute. According to the technical data of the specimen provided by the supplier, the phenolic FRP consists of approximately 50% phenolic resin and 50% fberglass (mass fraction). Phenolic resin in the phenolic FRP was obtained by condensation polymerization of phenol and formaldehyde. The fundamental properties of the phenolic FRP including the specifc heat, the thermal conductivity, the thermal difusivity, the density and the ignition temperature are shown in Table [1](#page-1-0). The values of the density  $\rho$  and the ignition temperature were provided by the supplier. The specific heat  $c$ , the thermal conductivity  $\lambda$  and the thermal diffusivity  $\alpha$  were measured using a hot-disk TPS2500 s. The thickness of the specimen used in the present study is 3, 5 and 8 mm, which are the common thickness of phenolic FRP composite in end use.

#### **Measurement**

The cone calorimeter experiments were carried out using an ISO 5660-1 standard Cone Calorimeter with a digital electronic balance (UX6200H) with the accuracy of 0.01 g. The specimen with the dimension of  $100 \times 100$  mm was used for the experiments. In order to eliminate the mass transfer along all the boundaries except the exposed face of the specimen to the external heat source, aluminum foil was used to wrap the edges and rear surface of the specimen. In addition, to prevent the specimen from intumescing, a wire grid which was made of 2-mm stainless steel rod with all intersections welded was used. Ceramic fber blanket was positioned underneath the specimen for thermal insulation. The specimen along with the specimen holder was positioned horizontally on a lifting platform. The distance between the cone heater and the top surface of the specimen was 25 mm. External heat fuxes including 30, 35, 40, 45, 50, 55, 60 and 65 kW  $m^{-2}$  were selected. Experiments were conducted with the ambient temperature of  $298 \pm 2$  K and the relative humidity of  $50 \pm 5\%$ . Cone calorimeter

<span id="page-1-0"></span>**Table 1** Fundamental properties of phenolic FRP

Elements	Value
Specific heat $c/J$ kg <sup>-1</sup> K <sup>-1</sup>	735.93
Thermal conductivity $\lambda$ /W m <sup>-1</sup> K <sup>-1</sup>	0.36
Thermal diffusivity $\alpha/m^2$ s <sup>-1</sup>	$2.97 \times 10^{-7}$
Density $\rho$ /kg m <sup>-3</sup>	1.63
Ignition temperature/K	803

was calibrated following the standard of ISO 5660-1 [[19\]](#page-9-11) before each test. Experiment was terminated manually if no ignition occurred in 32 min following the standard of ISO 17554 [\[20\]](#page-9-12).

# **Results and discussion**

#### <span id="page-2-1"></span>**Ignition characteristics**

Ignition time is one of the key parameters to characterize the fre hazard and thermal decomposition behaviors of solid combustibles. In general, specimen with high ignition time has low fre hazard and high thermal resistance. Correlation of the ignition time with the applied external heat fux can be used to determine whether the specimen behaves as thermally thick material or thermally thin material [\[21](#page-9-13)[–24](#page-10-0)]. Moreover, correlation of the ignition time with the applied external heat fux may be used to obtain the fammability properties of solid combustibles, such as the critical heat fux (CHF) and the ignition temperature.

The ignition time as a function of external heat fux in the case of diferent thicknesses is presented in Fig. [1a](#page-2-0). The ignition time corresponds to the start moment of the occurrence of sustained faming instead of transitory faming according to the fame image record. It should be noted that ignition did not occur in the case of 30 kW m−2. As shown in Fig. [1](#page-2-0)a, the ignition time decreases with the external heat fux. Besides, the ignition time increases with the thickness under the identical external heat fux. It may be due to that more energy is required for the decomposition of the thicker specimen, and more time is required to achieve the lower fammable limit of the combustible gases generated by the decomposition of the specimen. Furthermore, with the increase in the external heat fux, the difference of the ignition time under diferent thicknesses in the case of the identical external heat fux decreases with the external heat fux.

Based on Quintiere's model [[21\]](#page-9-13), correlation of the ignition time with the applied external heat fux may be used to determine whether the specimen behaves as thermally thick or thermally thin material when it is exposed to heat. The specifc procedure is illustrated as follows:

- 1. Correlation of the transformed ignition time  $(1/t_{ig})^n$  with the applied external heat fux using diferent values of *n*  $(t<sub>io</sub>$  denotes the ignition time. *n* is a coefficient.  $n=0.5$ and 1 correspond to the cases of thermally thick and thermally thin materials, respectively).
- 2. The least-squares method is used to obtain the value of the correlation coefficient  $R^2$ . The value of *n* with higher  $R^2$  is adopted. Based on the value of *n*, whether



<span id="page-2-0"></span>**Fig. 1** Ignition time versus external heat fux under diferent thicknesses

the specimen behaves as thermally thick or thermally thin material may be determined.

Figure [1](#page-2-0)b–d shows the correlation of the transformed ignition time  $(1/t_{ig})^n$  with the applied external heat flux under diferent thicknesses. The values of the slope and the intercept of the ftting line as well as the correlation coefficient are presented. According to Quintiere's model  $[21]$  $[21]$ , the specimen with the thickness of 3 mm is prone to be thermally thin material. However, the specimen with the thickness of 5 and 8 mm may be considered as thermally thick material.

Based on the opinions of Quintiere [\[21](#page-9-13)] and Luche et al. [\[22,](#page-9-14) [23](#page-10-1)], the value of the theoretical CHF  $\dot{q}$ <sup>*u*</sup></sup> can be calculated using Eq. [\(1](#page-3-0)). Thus, the value of the theoretical CHF  $\dot{q}$ <sup>''</sup><sub>cr</sub> in the cases of 3, 5 and 8 mm is calculated to be 20, 14.1 and 16.8 kW m−2, respectively. The average value of  $\dot{q}^{\prime\prime}_{\rm cr}$  for the three cases is about 16.9 kW m<sup>-2</sup>.

$$
CHF = \left[ -\frac{hboxIntercept}{Slope} \right] \tag{1}
$$

Besides the theoretical CHF  $\dot{q}^{\prime\prime}_{cr}$ , the minimum heat flux  $\dot{q}^{\prime\prime}_{\rm min}$  is also generally used to evaluate the ignition characteristics of solid combustibles. It should be noted that  $\dot{q}^{\prime\prime}_{cr}$  is generally determined from the curve-fitting of the ignition time with the applied external heat fux. However,  $\dot{q}$ <sup> $\prime\prime$ </sup><sub>min</sub> denotes the heat flux which is just sufficient to heat the material surface to attain the ignition temperature for considerably long exposure times (theoretically  $\infty$ ) [[22\]](#page-9-14). For engineering purpose,  $\dot{q}''_{\text{min}}$  may be considered as the average value of the lowest external heat fux at which ignition occurs and the highest external heat fux at which no ignition occurs for 32 min [[20](#page-9-12), [25](#page-10-2)]. Thus, the value of  $\dot{q}$ <sup>*''*</sup><sub>min</sub> is calculated to be 32.5 kW m<sup>-2</sup> in the present study. The ratio of  $\dot{q}''_{\text{cr}}$  and  $\dot{q}''_{\text{min}}$  in the cases of 3, 5 and 8 mm is 0.62, 0.44 and 0.52, respectively, which is consistent with the results found in the literature  $(0.11-0.7)$   $[25, 26]$  $[25, 26]$  $[25, 26]$  $[25, 26]$ . In addition, based upon  $\dot{q}''_{\text{min}}$ , the ignition temperature is calculated to be 813 K from Eq. ([2](#page-3-1)) using a MATLAB program, which is almost consistent with the experimental measured one (803 K), as presented in Table [1](#page-1-0) in ["Materi](#page-1-1)[als"](#page-1-1) section.

$$
\varepsilon q''_{\text{min}} = h_{\text{c}} \left( T_{\text{ig}} - T_{\infty} \right) + \varepsilon \sigma (T_{\text{ig}}^4 - T_{\infty}^4) \tag{2}
$$

where  $h_c$  denotes the convective heat transfer coefficient and is taken as 0.0135 kW m<sup>-2</sup> K<sup>-1</sup> [[25\]](#page-10-2) in the present study.  $\epsilon$ denotes the surface emissivity of the specimen at ignition moment and is taken as 0.88  $[25]$  $[25]$  in the present study.  $\sigma$  is the Stefan–Boltzmann constant  $(5.67 \times 10^{-11} \text{ kW m}^{-2} \text{K}^{-4})$ .  $T_{\text{ir}}$  and  $T_{\infty}$  denote the ignition temperature of the specimen and the ambient temperature (K), respectively.

#### $\mathcal{D}$  Springer

#### <span id="page-3-5"></span>**Thermal thickness**

The thermal thickness represents the thermal penetration depth at ignition moment, which is defned as the thickness of the specimen which has been heated to a certain temperature at ignition moment  $[25]$ . The thermal thickness can be calculated based on Eq.  $(3)$  $(3)$   $[25]$  $[25]$ :

<span id="page-3-2"></span>
$$
\delta_{\rm P} = A \sqrt{\frac{\lambda t_{\rm ig}}{\rho c}}\tag{3}
$$

where  $\delta_{\rm P}$  denotes the thermal thickness of the specimen  $(m)$ . *A* is a constant and taken as 1 in the present study based on the work of Mikkola and Wichman [\[27](#page-10-4)]. *λ*, *ρ* and *c* are the thermal conductivity (W m<sup>-1</sup> K<sup>-1</sup>), the density (kg m<sup>-3</sup>) and the specific heat (J kg<sup>-1</sup> K<sup>-1</sup>) of the specimen, respectively.

In addition to Eq.  $(3)$  $(3)$ , the thermal thickness of the specimen may be also estimated using Eq. [\(4](#page-3-3)) [\[25\]](#page-10-2).

<span id="page-3-3"></span><span id="page-3-0"></span>
$$
\delta_{\rm P} = B \frac{\rho}{\dot{q}_{\rm e}^{\prime\prime}} + C \tag{4}
$$

where both of *B* and *C* are constant.  $\dot{q}'_e$  denotes the external heat flux (kW m<sup> $-2$ </sup>).

Obviously, it is easier to obtain the value of the thermal thickness using Eq.  $(4)$  $(4)$  $(4)$  than Eq.  $(3)$  since Eq.  $(4)$  $(4)$  merely needs to know the specimen density and the applied external heat fux, and these two parameters are quite easy to get. Thus, the results based on Eqs.  $(3)$  $(3)$  and  $(4)$  are correlated and shown in Fig. [2](#page-3-4). It can be seen from Fig. [2](#page-3-4) that the thermal thickness  $\delta_{\rm p}$  is proportional to  $\rho / \dot{q}_{\rm e}^{\prime\prime}$  and high correlation coefficient  $R^2$  is demonstrated in the cases of 3, 5 and 8 mm. In addition, little diferences occur between the values of  $\delta_{\rm P}$  in the cases of 5 and 8 mm. Thus, the values of  $\delta_{\rm P}$  in the cases of 5 and 8 mm may be correlated with the

<span id="page-3-1"></span>

<span id="page-3-4"></span>**Fig. 2** Correlation among thermal thickness, density and external heat fux under diferent thicknesses

external heat fux together. The large diferences between the cases of 3 mm and 5, 8 mm are resulted by that the specimen with thickness of 3 mm is prone to be thermally thin material in which temperature distributes almost homogeneously when exposed to external heat [\[28](#page-10-5)]. However, the specimen with thickness of 5 and 8 mm may be considered as thermally thick material where heterogeneous temperature profle occurs when exposed to external heat [[28](#page-10-5)]. The correlation for the thermally thick specimen (5 and 8 mm) and thermally thin specimen (3 mm) is expressed as Eqs. ([5\)](#page-4-0) and [\(6](#page-4-1)), respectively.

$$
\delta_{\text{Philck}} = 0.3986 \rho / \dot{q}_e'' - 4.5588 \tag{5}
$$

$$
\delta_{\text{Pthin}} = 0.1782 \rho / \dot{q}_e'' + 0.6886 \tag{6}
$$

where  $\delta_{\text{Pthick}}$  and  $\delta_{\text{Pthin}}$  denote the thermal thickness in the cases of thermally thick (5 and 8 mm) and thermally thin phenolic FRP (kW s<sup>-1</sup> m<sup>-2</sup>), respectively.

#### **Mass loss factor and mass loss rate**

#### **Mass loss factor**

Mass loss factor  $\phi$  denotes the ratio of the total mass loss and the initial mass per unit area of the specimen [\[29](#page-10-6)]. It can be expressed as Eq. ([7\)](#page-4-2).

$$
\phi = \frac{m_0 - m}{m_0 A} \tag{7}
$$

where  $m_0$ ,  $m$  and  $A$  denote the initial mass (kg), the residue mass (kg) and the area of the specimen exposed to the cone heater  $(m^2)$ , respectively.

Figure [3](#page-4-3) shows the mass loss factor  $\phi$  as a function of external heat fux in the cases of 3, 5 and 8 mm. It is indicated that  $\phi$  decreases with the thickness under the identical external heat fux. This may be due to that more complete burning occurs in the specimen with smaller thickness.

#### **Mass loss rate**

Mass loss rate (MLR) is defned as the mass rate of solid or liquid fuel vaporized and burned [\[29\]](#page-10-6). It can be used to characterize the decomposition rate of the specimen and thus evaluate its fre hazard. Figure [4](#page-5-0)a–c shows the MLR against time under typical external heat fux and diferent thicknesses. It is indicated in Fig. [4](#page-5-0)a that there are three peaks under  $35 \text{ kW m}^{-2}$ for the cases of 3, 5 and 8 mm. However, as shown in Fig. [4b](#page-5-0), in the case of 50 kW  $m^{-2}$ , there are two peaks in the cases of 3 and 5 mm, while there are three peaks in the case of 8 mm. With the continuing increase in the external heat fux to 65 kW m−2, as shown in Fig. [4](#page-5-0)c, there are two peaks for the cases of 3, 5 and 8 mm. This may be due to that: After ignition, char layer was generated in the combustion process

ness

<span id="page-4-3"></span><span id="page-4-1"></span><span id="page-4-0"></span>**Fig. 3** Mass loss factor versus external heat fux under diferent thick-

<span id="page-4-2"></span>and prevented the continuing combustion. In the case of low external heat fluxes, the heat was not sufficient to rapidly penetrate into the char layer, leading to the decrease in MLR and the generation of the second peak MLR. However, in the case of high external heat fuxes, the heat was high enough to rapidly penetrate into the char layer and the continuing combustion may be maintained. The second peak MLR consequently disappeared. It should be noted that more char was generated in the case of 8 mm in comparison with that of 3 and 5 mm. It may need more time to penetrate into the generated char layer. As a consequence, just as Fig. [4](#page-5-0)b shows, three peaks occur in the case of 8 mm, while merely two peaks occur in the cases of 3 and 5 mm.

Table [2](#page-5-1) presents the average MLR under diferent external heat fuxes and thicknesses. Correlation of the average MLR with the external heat fux under diferent thicknesses is presented in Fig. [4](#page-5-0)d. As shown in Table [2](#page-5-1) and Fig. [4d](#page-5-0), the average MLR increases with the external heat fux and the thickness. The correlation of the average MLR with the external heat fux in the cases of 3, 5 and 8 mm is diferent, as presented as follows.

$$
\bar{m}_{a3}^{"'} = 0.0299 \dot{q}_e^{"} + 0.5434
$$
\n(8)

$$
\bar{m}_{a5}^{\prime\prime} = 0.0373 \dot{q}_e^{\prime\prime} + 0.3893 \tag{9}
$$

$$
\bar{m}_{\text{a8}}^{\prime\prime} = 0.0569 \dot{q}_{\text{e}}^{\prime\prime} + 0.1144 \tag{10}
$$

where  $\bar{m}''_{a3}$ ,  $\bar{m}''_{a5}$  and  $\bar{m}''_{a8}$  denote the average MLR of the specimen with the thickness of 3, 5 and 8 mm (g s<sup>-1</sup> m<sup>-2</sup>), respectively.





<span id="page-5-0"></span>**Fig. 4** Typical MLR versus time: **a** 35 kW m−2, **b** 50 kW m−2 and **c** 65 kW m−2, and **d** average MLR versus external heat fux under diferent thicknesses

<span id="page-5-1"></span>



#### **Heat release rate and total heat release**

#### **Heat release rate**

Heat release rate (HRR) denotes the rate of thermal energy released from the combustion of the solid combustibles and is considered as the single most important variable in fre hazard evaluation [[22](#page-9-14), [23,](#page-10-1) [30\]](#page-10-7). The oxygen consumption calorimetry technique based on ISO 5660-1 standard [[19,](#page-9-11) [30–](#page-10-7)[32](#page-10-8)] was used to calculate the HRR by measuring the concentration of gaseous compounds  $(O_2, CO_2, CO_3)$ etc.) generated by the combustion of the specimen.

Figure [5](#page-6-0)a–c illustrates the HRR against time under typical external heat fux in the cases of 3, 5 and 8 mm. As shown in Fig. [5](#page-6-0)a–c, after ignition, a quasi-steady stage occurs before the HRR attains its maximum value. The occurrence of the quasi-steady stage may be due to the formation of the char layer. The gradual increase stage between the quasi-steady stage and the maximum HRR may be resulted by the crack of the formed char layer. In addition, it is indicated in Fig. [5](#page-6-0) that the increase in the maximum HRR with the external heat fux in the case of 3 mm is larger than that of 5 and 8 mm. This phenomenon may be resulted by that the specimen with the thickness of 3 mm is prone to be thermally thin material in which temperature distributes almost homogeneously when exposed to external heat [[28\]](#page-10-5). However, the specimen with thickness of 5 and 8 mm may be considered as thermally thick material where heterogeneous temperature profle occurs when exposed to external heat [[28](#page-10-5)]. With the increase in the external heat fux, it is easier for the specimen with the thickness of 3 mm to attain heat balance than that of 5 and 8 mm. The combustion efficiency in the case of 3 mm is larger than that of 5 and 8 mm.



<span id="page-6-0"></span>**Fig. 5** Typical HRR versus time: **a** 35 kW m−2, **b** 50 kW m−2 and **c** 65 kW m−2, and **d** average HRR versus external heat fux under diferent thicknesses

<span id="page-6-1"></span>**Table 3** Average HRR under diferent thicknesses and external heat fuxes

External heat flux/ $\mathrm{kW~m^{-2}}$	Average HRR/kW $m^{-2}$		
	$3 \text{ mm}$	$5 \text{ mm}$	$8 \text{ mm}$
35	26.1529	16.2457	34.0264
40	32.2438	22.2521	34.8392
45	35.6598	28.1409	48.1959
50	35,3601	30.1592	49.2479
55	39.7958	36.0601	56.1526
60	41.1417	37.8269	60.0656
65	42.8311	38.0738	64.0362

Table [3](#page-6-1) presents the average HRR under diferent external heat fuxes in the cases of 3, 5 and 8 mm. The correlation of the average HRR with the external heat fux in the cases of 3, 5 and 8 mm is presented in Fig. [5](#page-6-0)d. As illustrated in Table [3](#page-6-1) and Fig. [5](#page-6-0)d, the average HRR increases with the external heat fux. In addition, the average HRR in the case of 5 mm is the lowest and the average HRR in the case of 8 mm is the highest. This may be due to that the specimen with the thickness of 3 mm behaves as thermally thin material, while the specimens with the thickness of 5 and 8 mm are prone

to be thermally thick materials, as noted in "[Ignition char](#page-2-1)[acteristics"](#page-2-1) section. Compared with the case of 5 mm, more homogeneous temperature profle occurs inside the specimen with the thickness of 3 mm, generating larger HRR with more complete burning and higher combustion efficiency. However, when the thickness of the specimen is increased from 5 mm to 8 mm, more quantity of specimen is decomposed and more fammable gases for combustion are generated consequently. The quantity of the specimen instead of the combustion efficiency becomes the dominating factor infuencing the HRR. The correlation of the average HRR with the external heat flux in the cases of 3, 5 and 8 mm is diferent, as presented in the following.

$$
\bar{q}_{a3}^{"}=0.5141\dot{q}_{e}^{"}+10.4671\tag{11}
$$

$$
\bar{q}_{a5}^{"'} = 0.7468 \dot{q}_{e}^{"} - 7.5177
$$
\n(12)

$$
\bar{q}_{\text{a}8}^{\prime\prime} = 1.0603 \dot{q}_{\text{e}}^{\prime\prime} - 3.5047 \tag{13}
$$

where  $\bar{q}''_{a3}$ ,  $\bar{q}''_{a5}$  and  $\bar{q}''_{a8}$  denote the average HRR in the cases of 3, 5 and 8 mm ( $k\tilde{W}$  m<sup>-2</sup>), respectively.

Table [4](#page-7-0) presents the maximum HRR under diferent external heat fuxes in the cases of 3, 5 and 8 mm. The correlation of the maximum HRR with the external heat

<span id="page-7-0"></span>**Table 4** Maximum HRR and corresponding time under diferent thicknesses and external heat fuxes

External heat flux/kW $m^{-2}$	Maximum HRR/kW $m^{-2}/time/s$			
	3 mm	$5 \text{ mm}$	8 mm	
35	34.6201/707	49.518/1005	87.9587/1472	
40	47.8517/591	58.1471/1046	90.8257/1034	
45	64.4606/522	72.5199/672	107.6306/906	
50	79.6076/352	77.3637/556	114.1576/869	
55	90.1449/348	83.3135/486	121.5133/766	
60	92.2089/299	88.7529/508	128.7522/751	
65	99.0911/278	92.8354/483	134.1064/640	

fux in the cases of 3, 5 and 8 mm is presented in Fig. [6.](#page-7-1) As illustrated in Table [4](#page-7-0) and Fig. [6,](#page-7-1) the maximum HRR increases with the external heat fux and the thickness in the cases of external heat flux  $\leq 45$  kW m<sup>-2</sup>. However, in the cases of external heat flux > 45 kW m<sup>-2</sup>, similar to the case of the average HRR as presented in Table [3,](#page-6-1) the maximum HRR in the case of 5 mm is the lowest and the maximum HRR in the case of 8 mm is the highest. The correlation of the maximum HRR with the external heat fux in the cases of 3, 5 and 8 mm is presented as follows.

$$
\dot{q}_{\text{m3}}^{\prime\prime} = 2.1987 \dot{q}_{\text{e}}^{\prime\prime} - 37.3635\tag{14}
$$

 $\dot{q}$ <sup>*r*</sup><sub>m5</sub> = 1.4426 $\dot{q}$ <sup>*r*</sup><sub>e</sub> + 2.5082 (15)

$$
\dot{q}_{\text{m8}}'' = 1.6299 \dot{q}_{\text{e}}'' + 30.6425 \tag{16}
$$

where  $\dot{q}^{\prime\prime}_{\text{m3}}$ ,  $\dot{q}^{\prime\prime}_{\text{m5}}$  and  $\dot{q}^{\prime\prime}_{\text{m8}}$  denote the maximum HRR in the cases of 3, 5 and 8 mm (kW  $m^{-2}$ ), respectively.



<span id="page-7-1"></span>**Fig. 6** Maximum HRR versus external heat fux under diferent thicknesses

#### **Total heat release**

Total heat release (THR) denotes the total thermal energy released from the combustion of the solid combustibles and is sometimes used for the fire hazard evaluation. Figure [7](#page-7-2) illustrates the THR as a function of external heat fux under diferent thicknesses. It is indicated that the THR increases with the thickness and the external heat fux.

## **Fire performance index and fre growth index**

#### **Fire performance index**

Fire performance index (FPI) is generally used to characterize the fre hazard of solid combustibles. Solid combustibles with high fre hazard possess high FPI value. The value of FPI can be calculated by the following equation:

$$
FPI = pkHRR/t_{ig}
$$
 (17)

where pkHRR denote the peak HRR (kW m<sup>-2</sup>).

Figure [8](#page-8-0) shows the FPI for the maximum HRR FPI $<sub>m</sub>$  versus</sub> external heat fux under diferent thicknesses. More detailed information is presented in Table [5.](#page-8-1) As illustrated in Fig. [8](#page-8-0) and Table [5](#page-8-1), the value of  $FPI_m$  increases gradually with the external heat fux in the cases of 5 mm and 8 mm. However, little variations of the value of  $FPI_m$  with the external heat flux occur in the cases of 3 mm.

#### **Fire growth index**

Fire growth index (FGI) is generally used to characterize the fre development rate after ignition from the perspective of heat release. High fre hazard of material is indicated if the value of FGI is high. FGI is expressed as follows:

$$
FGI = pkHRR/tpkHRR
$$
 (18)



<span id="page-7-2"></span>**Fig. 7** THR versus external heat fux under diferent thicknesses



<span id="page-8-0"></span>**Fig. 8**  $FPI_m$  versus external heat flux under different thickness

<span id="page-8-1"></span>**Table 5**  $FPI_m$  data under different thicknesses and external heat fluxes

External heat flux/ $\mathrm{kW~m}^{-2}$	$FPI_m/kW s^{-1} m^{-2}$		
	$3 \text{ mm}$	$5 \text{ mm}$	8 mm
35	2.1754	1.4056	1.7338
40	1.9065	1.9018	1.5786
45	2.4279	1.7684	2.0685
50	2.1078	1.8847	2.6175
55	2.4000	2.3707	3.2596
60	2.2148	2.8864	3.9947
65	2.37607	3.7442	4.9231



<span id="page-8-2"></span>**Fig. 9**  $\text{FGI}_{\text{m}}$  versus external heat flux under different thicknesses

where  $t_{\text{pkHRR}}$  denote the corresponding time when the peak HRR occurs (s).

Figure [9](#page-8-2) shows the FGI for the maximum HRR  $FGI_m$ versus external heat fux under diferent thicknesses. More detailed information is presented in Table [6](#page-8-3). As illustrated

<span id="page-8-3"></span>**Table 6**  $\text{FGI}_{\text{m}}$  data under different thicknesses and external heat fuxes

External heat flux/ $\rm kW~m^{-2}$	$FGI_m/kW s^{-1} m^{-2}$		
	$3 \text{ mm}$	$5 \text{ mm}$	$8 \text{ mm}$
35	0.0489	0.0493	0.0598
40	0.0809	0.0556	0.0878
45	0.1235	0.1079	0.1188
50	0.2262	0.1392	0.1314
55	0.2591	0.1714	0.1586
60	0.3084	0.1747	0.1714
65	0.3564	0.1922	0.2095

in Fig. [9](#page-8-2) and Table [6](#page-8-3), the FGI for the maximum HRR  $FGI_m$ increases with the external heat fux. Excellent linear relationship of  $FGI<sub>m</sub>$  with the external heat flux is indicated. Furthermore, little diferences occur between the values of  $FGI<sub>m</sub>$  in the cases of 5 and 8 mm. Thus, the values of  $FGI<sub>m</sub>$ in the cases of 5 and 8 mm may be correlated with the external heat fux together. It is similar to the case of the thermal thickness as illustrated in ["Thermal thickness](#page-3-5) section". The large diferences between the cases of 3 mm and 5, 8 mm are resulted by that the specimen with thickness of 3 mm is prone to be thermally thin material in which temperature distributes almost homogeneously when exposed to external heat [[28\]](#page-10-5). However, the specimen with thickness of 5 and 8 mm may be considered as thermally thick material where heterogeneous temperature profle occurs when exposed to external heat [[28\]](#page-10-5). The correlations for the thermally thick specimen (5 and 8 mm) and thermally thin specimen (3 mm) are expressed as Eqs.  $(19)$  $(19)$  and  $(20)$  $(20)$ , respectively.

<span id="page-8-4"></span> $FGI<sub>mthick</sub> = 0.0049\dot{q}''<sub>e</sub> - 0.1171$  (19)

<span id="page-8-5"></span>
$$
FGI_{\text{mthin}} = 0.0108\dot{q}_e'' - 0.3398\tag{20}
$$

where  $FGI<sub>mthick</sub>$  and  $FGI<sub>mthin</sub>$  denote the FGI in the cases of thermally thick (5 and 8 mm) and thermally thin FRP  $(kW s^{-1} m^{-2})$ , respectively.

## **Conclusions**

The present study investigates the ignition and combustion characteristics of phenolic fber-reinforced plastic with diferent thicknesses using cone calorimeter under piloted ignition. Ignition time, thermal thickness, mass loss factor, MLR, HRR, THR, FPI and FGI are measured and analyzed. The major conclusions are summarized as follows:

1. The ignition time increases with the thickness and decreases with the external heat fux. Phenolic FRP with thickness of 3 mm may be considered as thermally

thin material, while phenolic FRP with thickness of 5 and 8 mm is prone to be thermally thick material. The critical heat fux, minimum heat fux and ignition temperature are deduced from the correlation of the ignition time with the external heat fux and validated.

- 2. The thermal thickness increases with the external heat fux. The value of the thermal thickness of phenolic FRP with thickness of 5 and 8 mm is almost the same under the identical external heat fux. Linear correlations of the thermal thickness with the ratio of the specimen density and the applied external heat fux under diferent thicknesses are demonstrated and presented.
- 3. Mass loss factor decreases with the thickness. There are three peak MLRs under low external heat fuxes, while there are merely two peak MLRs under high external heat fuxes. The average MLR increases with the external heat fux and the thickness. Linear correlations of the average MLR with the external heat fux under diferent thicknesses are demonstrated and presented.
- 4. The value of the average HRR of phenolic FRP with diferent thicknesses in the order of most to least is 8 mm > 3 mm > 5 mm. In addition, the average and maximum HRR increases with the external heat fux. Moreover, the maximum HRR increases with the thickness in the cases of external heat flux  $\lt$  45 kW m<sup>-2</sup>. However, in the cases of external heat flux > 45 kW m<sup>-2</sup>, the value of the maximum HRR of phenolic FRP with diferent thicknesses in the order of most to least is 8 mm>3 mm>5 mm. Linear correlations of the average and maximum HRR with the external heat fux under diferent thicknesses are demonstrated and presented.
- 5. The FPI for the maximum HRR increases with the external heat fux in the cases of 5 mm and 8 mm. However, little variations of the FPI for the maximum HRR with the external heat fux occur in the cases of 3 mm. The FGI for the maximum HRR increases with the external heat fux. The value of FGI for the maximum HRR of phenolic FRP with 5 and 8 mm is almost the same under the identical external heat fux. Linear correlations of FGI for the maximum HRR with the external heat fux under diferent thicknesses are demonstrated and presented.

**Acknowledgements** This work was sponsored by National Natural Science Foundation of China (No. 51806106) and Natural Science Foundation of Jiangsu Province, China (No: BK20170838).

## **References**

<span id="page-9-0"></span>1. An W, Jiang L, Sun J, Liew K. Correlation analysis of sample thickness, heat fux, and cone calorimetry test data of polystyrene foam. J Therm Anal Calorim. 2015;119(1):229–38.

- <span id="page-9-1"></span>2. Zhang B, Zhang J, Wang L, Xie H, Fan M. Investigation on efects of thickness on ignition characteristics and combustion process of the oil-impregnated transformer insulating paperboard. J Therm Anal Calorim. 2018;132(1):29–38.
- <span id="page-9-2"></span>3. Shi L, Chew MYL. Experimental study of woods under external heat flux by autoignition. J Therm Anal Calorim. 2013;111(2):1399–407.
- 4. Xu Q, Jin C, Jiang Y. Compare the flammability of two extruded polystyrene foams with micro-scale combustion calorimeter and cone calorimeter tests. J Therm Anal Calorim. 2017;127(3):2359–66.
- 5. Xu Q, Jin C, Griffin G, Jiang Y. Fire safety evaluation of expanded polystyrene foam by multi-scale methods. J Therm Anal Calorim. 2014;115(2):1651–60.
- 6. Xu Q, Jin C, Jiang Y. Analysis of the relationship between MCC and thermal analysis results in evaluating fammability of EPS foam. J Therm Anal Calorim. 2014;118(2):687–93.
- 7. Xu Q, Majlingova A, Zachar M, Jin C, Jiang Y. Correlation analysis of cone calorimetry test data assessment of the procedure with tests of diferent polymers. J Therm Anal Calorim. 2012;110(1):65–70.
- 8. Jiao C, Wang H, Chen X. Preparation of modifed fy ash hollow glass microspheres using ionic liquids and its fame retardancy in thermoplastic polyurethane. J Therm Anal Calorim. 2018;10:1–10.
- 9. Shi L, Chew MYL. Fire behaviors of polymers under autoignition conditions in a cone calorimeter. Fire Saf J. 2013;61:243–53.
- 10. Li Z, Yuan T, Abu-Siada A, Masoum MAS, Li Z, Xu Y, et al. A new vibration testing platform for electronic current transformers. IEEE T Instrum Meas. 2019;68(3):704–12.
- <span id="page-9-3"></span>11. Li K, Pau DS, Wang J, Ji J. Modelling pyrolysis of charring materials: determining fame heat fux using bench-scale experiments of medium density fbreboard (MDF). Chem Eng Sci. 2015;123:39–48.
- <span id="page-9-4"></span>12. Mouritz A, Mathys Z. Post-fre mechanical properties of marine polymer composites. Compos Struct. 1999;47(1):643–53.
- <span id="page-9-5"></span>13. Mouritz A. Post-fire flexural properties of fibre-reinforced polyester, epoxy and phenolic composites. J Mater Sci. 2002;37(7):1377–86.
- <span id="page-9-6"></span>14. Avila MB. The efect of resin type and glass content on the fre engineering properties of typical FRP composites. Master thesis: University of California, Berkeley; 2007.
- <span id="page-9-7"></span>15. Hilal DemirbaŞ A. Yields and heating values of liquids and chars from spruce trunkbark pyrolysis. Energy Sources. 2005;27(14):1367–73.
- <span id="page-9-8"></span>16. Demirbas A. Determination of calorifc values of bio-chars and pyro-oils from pyrolysis of beech trunkbarks. J Anal Appl Pyrolysis. 2004;72(2):215–9.
- <span id="page-9-9"></span>17. Ramsay G, Dowling V, McKechnie B, Leonard J. Methods for assessing the fre performance of phenolic resins and composites. Fire Saf Sci. 1995;2:355–66.
- <span id="page-9-10"></span>18. Duggan G. Usage of ISO 5660 data in UK railway standards and fre safety cases. In: A One-Day Conference on Fire Hazards, Testing, Materials and Products. Shrewsbury, UK: Rapra Technology Ltd.; 1997.
- <span id="page-9-11"></span>19. ISO-5660-1. Reaction-to-Fire Tests-Heat Release, Smoke Production and Mass Loss Rate-Part 1: Heat Release Rate (Cone Calorimeter Method). International Organization for Standardization Geneva, Switzerland; 2002.
- <span id="page-9-12"></span>20. ISO-17554. Reaction to Fire-Mass Loss Measurement. Geneva: International Organization for Standardization; 1998.
- <span id="page-9-13"></span>21. Quintiere J. A theoretical basis for fammability properties. Fire Mater. 2006;30(3):175–214.
- <span id="page-9-14"></span>22. Luche J, Rogaume T, Richard F, Guillaume E. Characterization of thermal properties and analysis of combustion behavior of PMMA in a cone calorimeter. Fire Saf J. 2011;46(7):451–61.
- <span id="page-10-1"></span>23. Luche J, Mathis E, Rogaume T, Richard F, Guillaume E. Highdensity polyethylene thermal degradation and gaseous compound evolution in a cone calorimeter. Fire Saf J. 2012;54:24–35.
- <span id="page-10-0"></span>24. Quang Dao D, Luche J, Richard F, Rogaume T, Bourhy-Weber C, Ruban S. Determination of characteristic parameters for the thermal decomposition of epoxy resin/carbon fbre composites in cone calorimeter. Int J Hydrog Energy. 2013;38(19):8167–78.
- <span id="page-10-2"></span>25. Babrauskas V. Ignition handbook: principles and applications to fre safety engineering, fre investigation, risk management and forensic science. 2nd ed. Issaquah: Fire Science; 2003.
- <span id="page-10-3"></span>26. Delichatsios MA. Piloted ignition times, critical heat fluxes and mass loss rates at reduced oxygen atmospheres. Fire Saf J. 2005;40(3):197–212.
- <span id="page-10-4"></span>27. Mikkola E, Wichman IS. On the thermal ignition of combustible materials. Fire Mater. 1989;14(3):87–96.
- <span id="page-10-5"></span>28. Mouritz AP, Gibson A. Fire properties of polymer composite materials. Dordrecht: Springer; 2007.
- <span id="page-10-6"></span>29. Chen R, Lu S, Li C, Li M, Lo S. Characterization of thermal decomposition behavior of commercial fame-retardant ethylenepropylene-diene monomer (EPDM) rubber. J Therm Anal Calorim. 2015;122:449–61.
- <span id="page-10-7"></span>30. Babrauskas V, Peacock RD. Heat release rate: the single most important variable in fre hazard. Fire Saf J. 1992;18(3):255–72.
- 31. Thornton W. The relation of oxygen to the heat of combustion of organic compounds. Lond Edinb Dublin Philos Mag J Sci. 1917;33(194):196–203.
- <span id="page-10-8"></span>32. Janssens M. Measuring rate of heat release by oxygen consumption. Fire Technol. 1991;27(3):234–49.

**Publisher's Note** Springer Nature remains neutral with regard to jurisdictional claims in published maps and institutional afliations.